

JAY-BEE OIL & GAS, INC.

APPLICATION FOR MODIFICATION OF GENERAL PERMIT

**Larry Well Pad Production Facility
Tyler County, West Virginia**



98 Vanadium Road
Bridgeville, PA 15017
(412) 221-1100

APPLICATION FOR G70-D GENERAL PERMIT

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility

Tyler County, West Virginia

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SECTION I

Application Form



west virginia department of environmental protection

Division of Air Quality
601 57th Street SE
Charleston, WV 25 4
Phone (304) 926-0475
Fax (304) 926-0479
www.dep.wv.gov

G70-D GENERAL PERMIT REGISTRATION APPLICATION

PREVENTION AND CONTROL OF AIR POLLUTION IN REGARD TO THE CONSTRUCTION, MODIFICATION,
RELOCATION, ADMINISTRATIVE UPDATE AND OPERATION OF
NATURAL GAS PRODUCTION FACILITIES LOCATED AT THE WELL SITE

☐ CONSTRUCTION
☒ MODIFICATION
☐ RELOCATION

☐ CLASS I ADMINISTRATIVE UPDATE
☐ CLASS II ADMINISTRATIVE UPDATE

SECTION 1. GENERAL INFORMATION

Name of Applicant (as registered with the WV Secretary of State's Office): **Jay-Bee Oil & Gas, Inc.**

Federal Employer ID No. (FEIN): **55-073-8862**

Applicant's Mailing Address: **3570 Shields Hill Rd**

City: **Cairo**

State: **WV**

ZIP Code: **26337**

Facility Name: **Larry Well Pad Production Facility**

Operating Site Physical Address: Off Klondike Acres Rd
If none available, list road, city or town and zip of facility.

City: **Middlebourne**

Zip Code: **26149**

County: **Tyler**

Latitude & Longitude Coordinates (NAD83, Decimal Degrees to 5 digits):

Latitude: **39.47509**

Longitude: **-80.88063**

SIC Code: **1311**

SIC Code: **1311**

NAICS Code: **211111**

NAICS Code: **211111**

CERTIFICATION OF INFORMATION

This G70-D General Permit Registration Application shall be signed below by a Responsible Official. A Responsible Official is a President, Vice President, Secretary, Treasurer, General Partner, General Manager, a member of the Board of Directors, or Owner, depending on business structure. A business may certify an Authorized Representative who shall have authority to bind the Corporation, Partnership, Limited Liability Company, Association, Joint Venture or Sole Proprietorship. Required records of daily throughput, hours of operation and maintenance, general correspondence, compliance certifications and all required notifications must be signed by a Responsible Official or an Authorized Representative. If a business wishes to certify an Authorized Representative, the official agreement below shall be checked off and the appropriate names and signatures entered. **Any administratively incomplete or improperly signed or unsigned G70-D Registration Application will be returned to the applicant. Furthermore, if the G70-D forms are not utilized, the application will be returned to the applicant. No substitution of forms is allowed.**

I hereby certify that _____ is an Authorized Representative and in that capacity shall represent the interest of the business (e.g., Corporation, Partnership, Limited Liability Company, Association Joint Venture or Sole Proprietorship) and may obligate and legally bind the business. If the business changes its Authorized Representative, a Responsible Official shall notify the Director of the Division of Air Quality immediately.

I hereby certify that all information contained in this G70-D General Permit Registration Application and any supporting documents appended hereto is, to the best of my knowledge, true, accurate and complete, and that all reasonable efforts have been made to provide the most comprehensive information possible.

Responsible Official Signature: _____

Name and Title: **Shane Dowell, Office Manager**

Phone: **304-628-3119**

Fax: _____

Email: **sdowell@jaybeeoil.com**

Date: _____

If applicable:

Authorized Representative Signature: _____

Name and Title: _____

Phone: _____

Fax: _____

Email: _____

Date: _____

If applicable:

Environmental Contact

Name and Title: _____

Phone: _____

Fax: _____

Email: _____

Date: _____

OPERATING SITE INFORMATION	
Briefly describe the proposed new operation and/or any change(s) to the facility: Jay-Bee is seeking approval for installation of a compressor engine. There are no other proposed changes to the facility at this time.	
<p>Directions to the facility: From Middlebourne, proceed southwest on State Route 18 (Main Street) out of town. Turn right onto Bridgeway Rd. Turn left onto Wick Rd and follow for approximately 2.0 miles. Turn left onto Klondike Acres Rd and follow for approximately 1.5 miles to well pad entrance.</p>	
ATTACHMENTS AND SUPPORTING DOCUMENTS	
I have enclosed the following required documents:	
<p>Check payable to WVDEP – Division of Air Quality with the appropriate application fee (per 45CSR13 and 45CSR22).</p> <p> <input checked="" type="checkbox"/> Check attached to front of application. <input type="checkbox"/> I wish to pay by electronic transfer. Contact for payment (incl. name and email address): <input type="checkbox"/> I wish to pay by credit card. Contact for payment (incl. name and email address): </p> <p> <input checked="" type="checkbox"/> \$500 (Construction, Modification, and Relocation) <input type="checkbox"/> \$300 (Class II Administrative Update) <input checked="" type="checkbox"/> \$1,000 NSPS fee for 40 CFR60, Subpart IIII, JJJJ, OOOO and/or OOOOa ¹ <input type="checkbox"/> \$2,500 NESHAP fee for 40 CFR63, Subpart ZZZZ and/or HH ² </p> <p> ¹ Only one NSPS fee will apply. ² Only one NESHAP fee will apply. The Subpart ZZZZ NESHAP fee will be waived for new engines that satisfy requirements by complying with NSPS, Subparts IIII and/or JJJJ. <i>NSPS and NESHAP fees apply to new construction or if the source is being modified.</i> </p>	
<input checked="" type="checkbox"/> Responsible Official or Authorized Representative Signature (if applicable)	
<input checked="" type="checkbox"/> Single Source Determination Form (must be completed) – Attachment A	
<input type="checkbox"/> Siting Criteria Waiver (if applicable) – Attachment B	<input checked="" type="checkbox"/> Current Business Certificate – Attachment C
<input checked="" type="checkbox"/> Process Flow Diagram – Attachment D	<input checked="" type="checkbox"/> Process Description – Attachment E
<input checked="" type="checkbox"/> Plot Plan – Attachment F	<input checked="" type="checkbox"/> Area Map – Attachment G
<input checked="" type="checkbox"/> G70-D Section Applicability Form – Attachment H	<input checked="" type="checkbox"/> Emission Units/ERD Table – Attachment I
<input checked="" type="checkbox"/> Fugitive Emissions Summary Sheet – Attachment J	
<input checked="" type="checkbox"/> Gas Well Affected Facility Data Sheet (if applicable) – Attachment K	
<input type="checkbox"/> Storage Vessel(s) Data Sheet (include gas sample data, USEPA Tanks, simulation software (e.g. ProMax, E&P Tanks, HYSYS, etc.), etc. where applicable) – Attachment L	
<input type="checkbox"/> Natural Gas Fired Fuel Burning Unit(s) Data Sheet (GPUs, Heater Treaters, In-Line Heaters if applicable) – Attachment M	
<input checked="" type="checkbox"/> Internal Combustion Engine Data Sheet(s) (include manufacturer performance data sheet(s) if applicable) – Attachment N	
<input type="checkbox"/> Tanker Truck/Rail Car Loading Data Sheet (if applicable) – Attachment O	
<input type="checkbox"/> Glycol Dehydration Unit Data Sheet(s) (include wet gas analysis, GRI- GLYCalc™ input and output reports and information on reboiler if applicable) – Attachment P	
<input checked="" type="checkbox"/> Pneumatic Controllers Data Sheet – Attachment Q	
<input checked="" type="checkbox"/> Pneumatic Pump Data Sheet – Attachment R	
<input type="checkbox"/> Air Pollution Control Device/Emission Reduction Device(s) Sheet(s) (include manufacturer performance data sheet(s) if applicable) – Attachment S	
<input checked="" type="checkbox"/> Emission Calculations (please be specific and include all calculation methodologies used) – Attachment T	
<input checked="" type="checkbox"/> Facility-wide Emission Summary Sheet(s) – Attachment U	
<input checked="" type="checkbox"/> Class I Legal Advertisement – Attachment V	
<input checked="" type="checkbox"/> One (1) paper copy and two (2) copies of CD or DVD with pdf copy of application and attachments	

All attachments must be identified by name, divided into sections, and submitted in order.

SECTION II

Attachments

ATTACHMENT A - SINGLE SOURCE DETERMINATION FORM

Classifying multiple facilities as one “stationary source” under 45CSR13, 45CSR14, and 45CSR19 is based on the definition of Building, structure, facility, or installation as given in §45-14-2.13 and §45-19-2.12. The definition states:

“Building, Structure, Facility, or Installation” means all of the pollutant-emitting activities which belong to the same industrial grouping, are located on one or more contiguous or adjacent properties, and are under the control of the same person (or persons under common control). Pollutant-emitting activities are a part of the same industrial grouping if they belong to the same “Major Group” (i.e., which have the same two (2)-digit code) as described in the Standard Industrial Classification Manual, 1987 (United States Government Printing Office stock number GPO 1987 0-185-718:QL 3).

The Source Determination Rule for the oil and gas industry was published in the Federal Register on June 3, 2016 and will become effective on August 2, 2016. EPA defined the term “adjacent” and stated that equipment and activities in the oil and gas sector that are under common control will be considered part of the same source if they are located on the same site or on sites that share equipment and are within ¼ mile of each other.

Is there equipment and activities in the same industrial grouping (defined by SIC code)?

Yes ☐ No ☒

Is there equipment and activities under the control of the same person/people?

Yes ☐ No ☒

Is there equipment and activities located on the same site or on sites that share equipment and are within ¼ mile of each other?

Yes ☐ No ☒

The proposed modification to this facility will not change the previous single source determination. Additionally, there have been no other Jay-Bee facilities installed in proximity to this facility since that previous determination.

ATTACHMENT C – CURRENT BUSINESS CERTIFICATE

If the applicant is a resident of West Virginia, the applicant should provide a copy of the current Business Registration Certificate issued to them from the West Virginia Secretary of State's Office. If the applicant is not a resident of the State of West Virginia, the registrant should provide a copy of the Certificate of Authority/Authority of LLC/Registration. This information is required for all sources to operate a business in West Virginia regardless of whether it is a construction, modification, or administrative update.

If you are a new business to West Virginia and have applied to the West Virginia Secretary of State's Office for a business license, please include a copy of your application.

Please note: Under the West Virginia Bureau of Employment Programs, 96CSR1, the DAQ may not grant, issue, or renew approval of any permit, general permit registration, or Certificate to Operate to any employing unit whose account is in default with the Bureau of Employment Programs Unemployment Compensation Division.

**WEST VIRGINIA
STATE TAX DEPARTMENT
BUSINESS REGISTRATION
CERTIFICATE**

ISSUED TO:
**JAY-BEE OIL & GAS INC
RR 1 BOX 5
CAIRO, WV 26337-9701**

BUSINESS REGISTRATION ACCOUNT NUMBER 1043-4424

This certificate is issued on: **06/11/2010**

This certificate is issued by
the West Virginia State Tax Commissioner
in accordance with W. Va. Code § 11-12

The person or organization identified on this certificate is registered
to conduct business in the State of West Virginia at the location above.

This certificate is not transferrable and must be displayed at the location for which issued.

This certificate shall be permanent until cessation of the business for which the certificate of registration
was granted or until it is suspended, revoked, or cancelled by the Tax Commissioner.

Change in name or change of location shall be considered a cessation of the business and a new
certificate shall be required.

TRAVELING STREET VENDORS: Must carry a copy of this certificate in every vehicle operated by them.

CONTRACTORS, DRILLING OPERATORS, TIMBER/LOGGING OPERATIONS: Must have a copy of
this certificate displayed at every job site within West Virginia.

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L1388180484

SCANNED

JUN 14 10

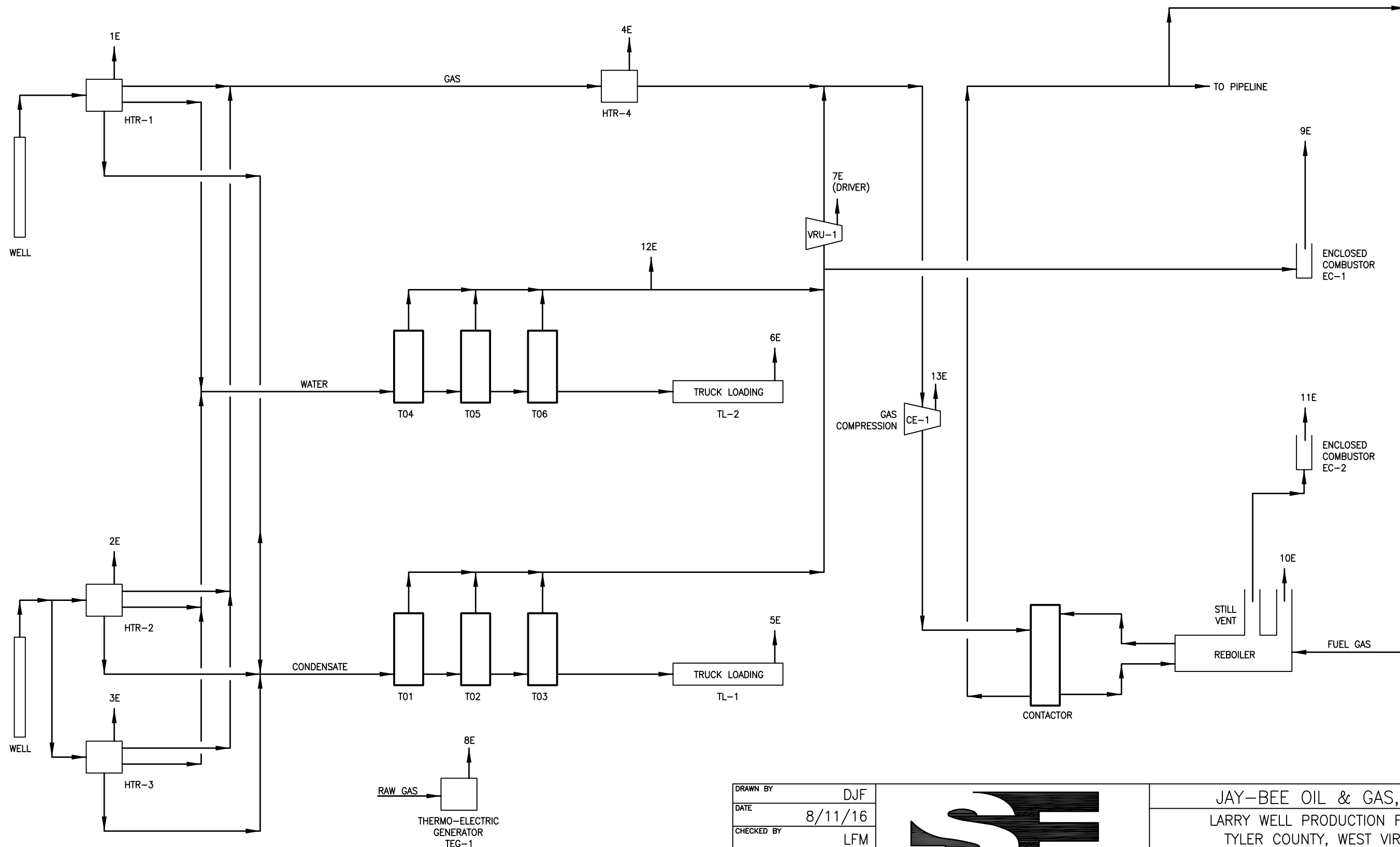
JUN 14 2010
WV

ATTACHMENT D – PROCESS FLOW DIAGRAM

Provide a diagram or schematic that supplements the process description of the operation. The process flow diagram must show all sources, components or facets of the operation in an understandable line sequence of operation. The process flow diagram should include the emission unit ID numbers, the pollution control device ID numbers, and the emission point ID numbers consistent with references in other attachments of the application. For a proposed modification, clearly identify the process areas, emission units, emission points, and/or control devices that will be modified, and specify the nature and extent of the modification.

Use the following guidelines to ensure a complete process flow diagram:

- The process flow diagram shall logically follow the entire process from beginning to end.
- Identify each emission source and air pollution control device with proper and consistent emission unit identification numbers, emission point identification numbers, and control device identification numbers.
- The process flow lines may appear different for clarity. For example, dotted lines may be used for vapor flow and solid lines used for liquid flow and arrows for direction of flow.
- The process flow lines may be color coded. For example: new or modified equipment may be red; old or existing equipment may be blue; different stages of preparation such as raw material may be green; and, finished product or refuse, another color.



DRAWN BY	DJF
DATE	8/11/16
CHECKED BY	LFM
SET JOB NO.	214054-18
SET DWG FILE	LARRY FDb01.dwg
DRAWING SCALE	N.T.S.



98 Vanadium Road Bridgeville, PA 15017 (412) 221-1100

JAY-BEE OIL & GAS, INC.
LARRY WELL PRODUCTION FACILITY
TYLER COUNTY, WEST VIRGINIA
PROCESS FLOW DIAGRAM

DRAWING NAME

FIGURE 3

REV.

2

ATTACHMENT E – PROCESS DESCRIPTION

Provide a detailed written description of the operation for which the applicant is seeking a permit. The process description is used in conjunction with the process flow diagram to provide the reviewing engineer a complete understanding of the activity at the operation. Describe in detail and order the complete process operation.

Use the following guidelines to ensure a complete Process Description:

- The process flow diagram should be prepared first and used as a guide when preparing the process description. The written description shall follow the logical order of the process flow diagram.
- All emission sources, emission points, and air pollution control devices must be included in the process description.
- When modifications are proposed, describe the modifications and the effect the changes will have on the emission sources, emission points, control devices and the potential emissions.
- Proper emission source ID numbers must be used consistently in the process description, the process flow diagram, the emissions calculations, and the emissions summary information provided.
- Include any additional information that may facilitate the reviewers understanding of the process operation.

The process description is required for all sources regardless of whether it is a construction, modification, or administrative update.

Jay-Bee Oil & Gas, Incorporated
Larry Well Pad Production Facility
Attachment E
Process Description

Jay-Bee is seeking approval for installation of a compressor engine. There are no other proposed changes to the facility at this time.

Currently, Natural gas and Produced Fluids (condensate and water) are received from three wells and passed through Gas Processing Units (one per Marcellus well and two per Utica well) to avoid ice formation during subsequent pressure drops. These materials pass through a three-way separator where gas, condensate and water are separated. All gas fired equipment use natural gas produced at the site as fuel. The Facility will then compress (proposed modification) and then dehydrate the gas. The gas is then injected into a gathering pipeline owned and operated by others.

Both Condensate and Produced Water are accumulated in six (6) 210 BBL tanks (three for Condensate and three for Produced Water), pending truck transportation by others. The Condensate is transported to a regional processing facility and the Produced Water is transported to a regional disposal facility. Flash, working and breathing losses from these tanks is routed to a Vapor Recovery Unit (VRU) with the captured vapors routed back to the raw gas discharge line. An enclosed combustor is utilized as a backup control device for times when the VRU is not available, and is also utilized if a large slug of condensate production generates flash gas in excess of the capacity of the VRU. A capture and control efficiency of 98% is being claimed for this overall combination of controls.

The dehydration unit generates emissions from the still vent and re-boiler. There is no flash tank. Vapors from the still vent are comprised of water and various low molecular weight hydrocarbons. Still vent vapors are routed to an enclosed combustor. A capture and control efficiency of 98% is being claimed for the combustor. Although needs are anticipated to be minimal, supplemental re-boiler fuel is available from the dehydrated gas stream prior to injection into the sales line. Any water condensing in the still vent column is routed to the wastewater tanks.

A Thermo-electric generator to meet the minor electric demands for various monitoring and data tracking equipment has also been installed at this facility.

In summary, upon approval of this application, emission sources at this facility will include the following:

- Three Gas Processing Units (GPUs), each with a 1.5 MMBTU/hr heater (Sources 1E, 2E and 3E).
- One Line Heater (Source 4E).
- Condensate Truck Loading (Source 5E)
- Produced Water Truck Loading (Source 6E)
- One Vapor Recovery Unit (VRU) with driver engine (Source 7E), controlling emissions from T01-T06.
- One Thermo-electric Generator (Source 8E)
- Backup Enclosed Combustor for VRU (Source 9E)
- Three Produced Water Tanks (T01-T03)
- Three Condensate Tanks (T04-T06)
- Dehydration Unit (Source 10E – reboiler vent and 11E – still vent)
- Enclosed Combustor for control of still vent (Source 11E)
- Un-captured/un-controlled emissions associated with VRU (Source 12E)
- One Caterpillar G2516BLE compressor engine (Source 13E) – **NEW SOURCE**

ATTACHMENT F – PLOT PLAN

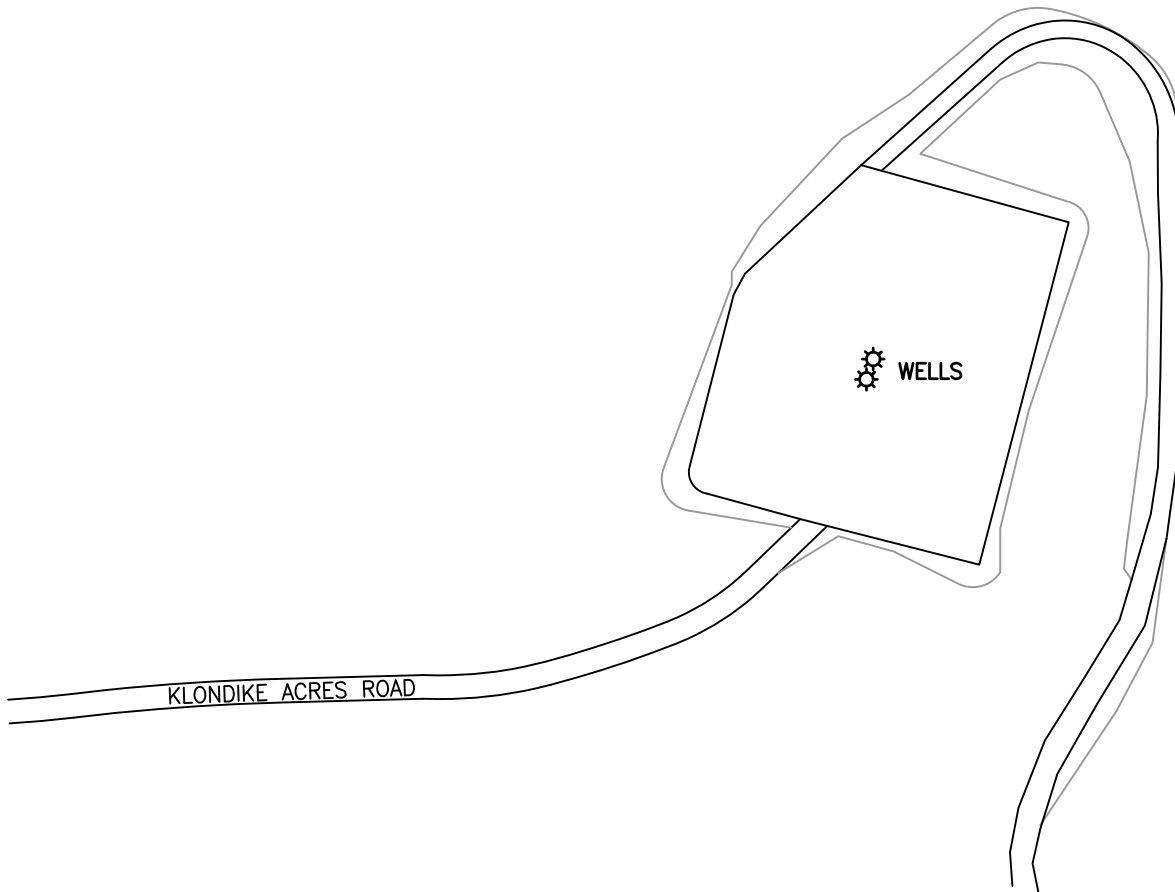
Provide an accurately scaled and detailed Plot Plan showing the locations of all emission units, emission points, and air pollution control devices. Show all emission units, affected facilities, enclosures, buildings and plant entrances and exits from the nearest public road(s) as appropriate. Note height, width and length of proposed or existing buildings and structures.

A scale between 1"=10' and 1"=200' should be used with the determining factor being the level of detail necessary to show operation or plant areas, affected facilities, emission unit sources, transfer points, etc. An overall small scale plot plan (e.g., 1"=300') should be submitted in addition to larger scale plot plans for process or activity areas (e.g., 1"=50') if the plant is too large to allow adequate detail on a single plot plan. Process or activity areas may be grouped for the enlargements as long as sufficient detail is shown.

Use the following guidelines to ensure a complete Plot Plan:

- Facility name
- Company name
- Company facility ID number (for existing facilities)
- Plot scale, north arrow, date drawn, and submittal date.
- Facility boundary lines
- Base elevation
- Lat/Long reference coordinates from the area map and corresponding reference point elevation
- Location of all point sources labeled with proper and consistent source identification numbers

This information is required for all sources regardless of whether it is a construction, modification, or administrative update.



DRAWN BY	DJF
DATE	8/11/16
CHECKED BY	LFM
SET JOB NO.	214054-18
SET DWG FILE	LARRYa01.dwg
DRAWING SCALE	N.T.S.



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JAY-BEE OIL & GAS, INC.
LARRY WELL PRODUCTION FACILITY
TYLER COUNTY, WEST VIRGINIA
SITE LAYOUT PLAN

DRAWING NAME

FIGURE 2

REV.

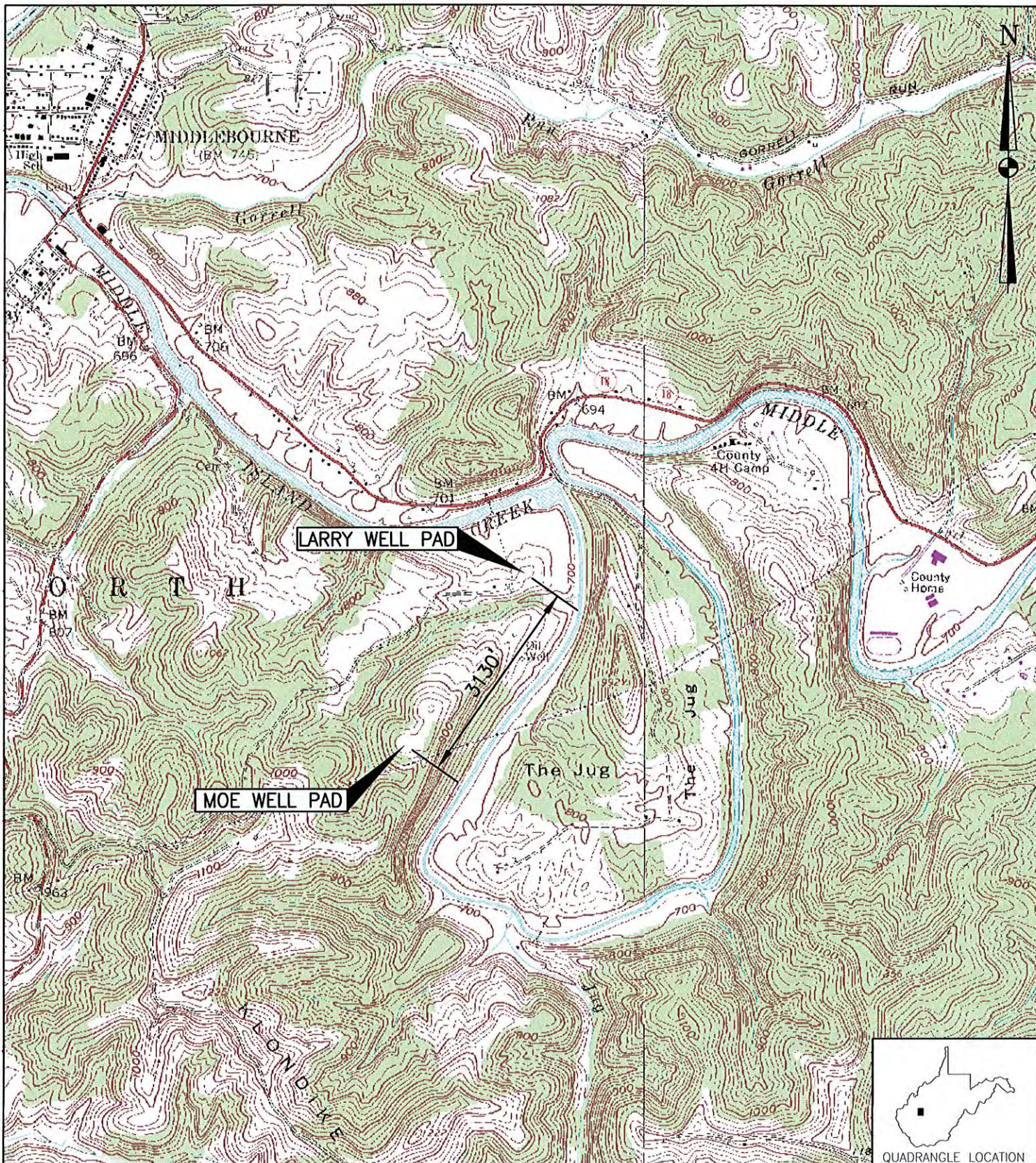
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ATTACHMENT G – AREA MAP

Provide an Area Map showing the current or proposed location of the operation. On this map, identify plant or operation property lines, access roads and any adjacent dwelling, business, public building, school, church, cemetery, community or institutional building or public park within a 300' boundary circle of the collective emission units.

Please provide a 300' boundary circle on the map surrounding the proposed emission units collectively.

This information is required for all sources regardless of whether it is a construction, modification, or administrative update.



REFERENCE: USGS 7.5' QUADRANGLE MAP OF: MIDDLEBOURNE, WEST VIRGINIA; DATED 1960, PHOTOREVISED 1976.

DRAWN BY DJF
DATE 7/11/16
CHECKED BY RAD
SET JOB NO. 214054
SET DWG FILE LARRY & MOEm01.dwg
DRAWING SCALE 1"=2000'



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JAY-BEE OIL & GAS, INC.

LARRY & MOE WELL PADS
TYLER COUNTY, WEST VIRGINIA
SITE LOCATION MAP

DRAWING NO.

FIGURE 1



REV.

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Radius Map - 300 ft

Larry Well Pad Production Facility

Legend

-  300 ft Radius
-  Larry

Larry

Google earth

© 2016 Google

500 ft



ATTACHMENT H – G70-D SECTION APPLICABILITY FORM

General Permit G70-D Registration Section Applicability Form

General Permit G70-D was developed to allow qualified applicants to seek registration for a variety of sources. These sources include gas well affected facilities, storage vessels, gas production units, in-line heaters, heater treaters, glycol dehydration units and associated reboilers, pneumatic controllers, pneumatic pumps, reciprocating internal combustion engines (RICEs), tank truck/rail car loading, fugitive emissions, completion combustion devices, flares, enclosed combustion devices, and vapor recovery systems. All registered facilities will be subject to Sections 1.0, 2.0, 3.0, and 4.0.

General Permit G70-D allows the registrant to choose which sections of the permit they are seeking registration under. Therefore, please mark which additional sections that you are applying for registration under. If the applicant is seeking registration under multiple sections, please select all that apply. Please keep in mind, that if this registration is approved, the issued registration will state which sections will apply to your affected facility.

GENERAL PERMIT G70-D APPLICABLE SECTIONS	
<input checked="" type="checkbox"/> Section 5.0	Gas and Oil Well Affected Facility (NSPS, Subpart OOOO/OOOOa)
<input checked="" type="checkbox"/> Section 6.0	Storage Vessels Containing Condensate and/or Produced Water ¹
<input type="checkbox"/> Section 7.0	Storage Vessel Affected Facility (NSPS, Subpart OOOO/OOOOa)
<input checked="" type="checkbox"/> Section 8.0	Control Devices and Emission Reduction Devices not subject to NSPS Subpart OOOO/OOOOa and/or NESHAP Subpart HH
<input checked="" type="checkbox"/> Section 9.0	Small Heaters and Reboilers not subject to 40CFR60 Subpart Dc
<input type="checkbox"/> Section 10.0	Pneumatic Controllers Affected Facility (NSPS, Subpart OOOO/OOOOa)
<input type="checkbox"/> Section 11.0	Pneumatic Pump Affected Facility (NSPS, Subpart OOOOa)
<input checked="" type="checkbox"/> Section 12.0	Fugitive Emissions GHG and VOC Standards (NSPS, Subpart OOOOa)
<input checked="" type="checkbox"/> Section 13.0	Reciprocating Internal Combustion Engines, Generator Engines
<input checked="" type="checkbox"/> Section 14.0	Tanker Truck/Rail Car Loading ²
<input checked="" type="checkbox"/> Section 15.0	Glycol Dehydration Units ³

- 1 Applicants that are subject to Section 6 may also be subject to Section 7 if the applicant is subject to the NSPS, Subparts OOOO or OOOOa control requirements or the applicable control device requirements of Section 8.*
- 2 Applicants that are subject to Section 14 may also be subject to control device and emission reduction device requirements of Section 8.*
- 3 Applicants that are subject to Section 15 may also be subject to the requirements of Section 9 (reboilers). Applicants that are subject to Section 15 may also be subject to control device and emission reduction device requirements of Section 8.*

ATTACHMENT I – EMISSION UNITS / EMISSION REDUCTION DEVICES (ERD) TABLE

Include ALL emission units and air pollution control devices/ERDs that will be part of this permit application review. Do not include fugitive emission sources in this table. Deminimis storage tanks shall be listed in the Attachment L table. This information is required for all sources regardless of whether it is a construction, modification, or administrative update.

Emission Unit ID ¹	Emission Point ID ²	Emission Unit Description	Year Installed	Manufac. Date ³	Design Capacity	Type ⁴ and Date of Change	Control Device(s) ⁵	ERD(s) ⁶
HTR-1	1E	Gas Processing Unit	2016		1.5 MMBTU/hr	Existing	None	None
HTR-2	2E	Gas Processing Unit	2016		1.5 MMBTU/hr	Existing	None	None
HTR-3	3E	Gas Processing Unit	2016		1.5 MMBTU/hr	Existing	None	None
HTR-4	4E	Line Heater	2016		0.5 MMBTU/hr	Existing	None	None
TL-1	5E	Condensate Truck Loading	2016		30,000 BBL/yr	Existing	None	None
TL-2	6E	Produced Water Truck Loading	2016		63,600 BBL/yr	Existing	None	None
VRU-1	7E	VRU Driver	2016	3/19/2012	84 HP	Existing	1C	None
TEG-1	8E	Thermoelectric Generator	2016		4.4 KW/hr	Existing	None	None
EC-1	9E	Enclosed Combustor	2016		10.0 MMBTU/hr	Existing	N/A	None
T01	7E/9E	Condensate Tank	2016		210 BBL	Existing	EC-1	VRU-1
T02	7E/9E	Condensate Tank	2016		210 BBL	Existing	EC-1	VRU-1
T03	7E/9E	Condensate Tank	2016		210 BBL	Existing	EC-1	VRU-1
T04	7E/9E	Produce Water Tank	2016		210 BBL	Existing	EC-1	VRU-1
T05	7E/9E	Produced Water Tank	2016		210 BBL	Existing	EC-1	VRU-1
T06	7E/9E	Produced Water Tank	2016		210 BBL	Existing	EC-1	VRU-1
RBV-1	10E	Dehydration Unit Re-boiler Vent	2016		0.500 MMBTU/hr	Existing	None	None
RSV-1	11E	Dehydration Unit Still Vent	2016		40 MMSCFD	Existing	EC-2	None
EC-2	11E	Enclosed Combustor	2016		10.0 MMBTU/hr	Existing	None	None
T01-T06	12E	Un-captured/Un-controlled VRU-1 Emissions	2016			Existing	None	None
CE-1	13E	Compressor Engine	Pending Approval	3/21/2012	1,380 HP	New	2C	None

¹ For Emission Units (or Sources) use the following numbering system: 1S, 2S, 3S,... or other appropriate designation.

² For Emission Points use the following numbering system: 1E, 2E, 3E, ... or other appropriate designation.

³ When required by rule

⁴ New, modification, removal, existing

⁵ For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

⁶ For ERDs use the following numbering system: 1D, 2D, 3D,... or other appropriate designation.

ATTACHMENT J – FUGITIVE EMISSIONS SUMMARY SHEET							
Sources of fugitive emissions may include loading operations, equipment leaks, blowdown emissions, etc.							
Source/Equipment:							
Leak Detection Method Used		<input checked="" type="checkbox"/> Audible, visual, and olfactory (AVO) inspections		<input type="checkbox"/> Infrared (FLIR) cameras		<input type="checkbox"/> Other (please describe)	
						<input type="checkbox"/> None required	
Component Type	Closed Vent System	Count	Source of Leak Factors (EPA, other (specify))	Stream type (gas, liquid, etc.)	Estimated Emissions (tpy)		
					VOC	HAP	GHG (methane, CO ₂ e)
Pumps	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	1	API	<input checked="" type="checkbox"/> Gas <input type="checkbox"/> Liquid <input type="checkbox"/> Both	<0.01	<0.01	0.34
Valves	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	56	EPA	<input type="checkbox"/> Gas <input type="checkbox"/> Liquid <input checked="" type="checkbox"/> Both	0.28	<0.01	3.87
Safety Relief Valves	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	3	EPA	<input type="checkbox"/> Gas <input type="checkbox"/> Liquid <input checked="" type="checkbox"/> Both	0.01	<0.01	0.45
Open Ended Lines	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	20	EPA	<input checked="" type="checkbox"/> Gas <input type="checkbox"/> Liquid <input type="checkbox"/> Both	0.06	<0.01	4.60
Sampling Connections	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	17	TECQ	<input type="checkbox"/> Gas <input type="checkbox"/> Liquid <input checked="" type="checkbox"/> Both	1.16	0.01	23.60
Connections (Not sampling)	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	237	EPA	<input type="checkbox"/> Gas <input type="checkbox"/> Liquid <input checked="" type="checkbox"/> Both	0.13	<0.01	2.00
Compressors	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	1	API	<input checked="" type="checkbox"/> Gas <input type="checkbox"/> Liquid <input type="checkbox"/> Both	0.02	<0.01	1.26
Flanges	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	120	API	<input type="checkbox"/> Gas <input type="checkbox"/> Liquid <input checked="" type="checkbox"/> Both	0.09	<0.01	4.47
Other ¹	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	16	n/a	<input checked="" type="checkbox"/> Gas <input type="checkbox"/> Liquid <input type="checkbox"/> Both	0.04	<0.01	0.055

¹ Other equipment types may include compressor seals, relief valves, diaphragms, drains, meters, etc.

Please provide an explanation of the sources of fugitive emissions (e.g. pigging operations, equipment blowdowns, pneumatic controllers, etc.): **Blowdowns**

Please indicate if there are any closed vent bypasses (include component): **No**

Specify all equipment used in the closed vent system (e.g. VRU, ERD, thief hatches, tanker truck/rail car loading, etc.)
Thief Hatch, VRU, Enclosed Combustors

ATTACHMENT K – GAS WELL AFFECTED FACILITY DATA SHEET

Complete this data sheet if you are the owner or operator of a gas well affected facility for which construction, modification or reconstruction commenced after August 23, 2011. This form must be completed for natural gas well affected facilities regardless of when flowback operations occur (or have occurred).

API Number	Date of Flowback	Date of Well Completion	Green Completion and/or Combustion Device	Subject to OOOO or OOOOa?
47-095-02315	December 2016	TBD	Flow to separator and into gathering line as soon as practical.	47-095-02315
47-095-02334	December 2016	TBD	Flow to separator and into gathering line as soon as practical.	47-095-02334

Note: If future wells are planned and no API number is available please list as PLANNED. If there are existing wells that commenced construction prior to August 23, 2011, please acknowledge as existing.

This is the same API (American Petroleum Institute) well number(s) provided in the well completion notification and as provided to the WVDEP, Office of Oil and Gas for the well permit. The API number may be provided on the application without the state code (047).

Every oil and gas well permitted in West Virginia since 1929 has been issued an API number. This API is used by agencies to identify and track oil and gas wells.

The API number has the following format: 047-001-00001

Where,

047 = State code. The state code for WV is 047.
 001 = County Code. County codes are odd numbers, beginning with 001 (Barbour) and continuing to 109 (Wyoming).
 00001= Well number. Each well will have a unique well number.

ATTACHMENT N – INTERNAL COMBUSTION ENGINE DATA SHEET

Complete this data sheet for each internal combustion engine at the facility. Include manufacturer performance data sheet(s) or any other supporting document if applicable. Use extra pages if necessary. *Generator(s) and microturbine generator(s) shall also use this form.*

Emission Unit ID# ¹	VRU-1	CE-1					
Engine Manufacturer/Model	Cummins G5.9	Caterpillar G3516 BLE					
Manufacturers Rated bhp/rpm	84 @ 1800	1380 @ 1400					
Source Status ²	ES	NS					
Date Installed/ Modified/Removed/Relocated ³	2016	Upon Receipt of Permit					
Engine Manufactured /Reconstruction Date ⁴	After 3/1/2013	3/21/2012					
Check all applicable Federal Rules for the engine (include EPA Certificate of Conformity if applicable) ⁵	<input checked="" type="checkbox"/> 40CFR60 Subpart JJJJ <input type="checkbox"/> JJJJ Certified? <input type="checkbox"/> 40CFR60 Subpart IIII <input type="checkbox"/> IIII Certified? <input type="checkbox"/> 40CFR63 Subpart ZZZZ <input type="checkbox"/> NESHAP ZZZZ/ NSPS JJJJ Window <input type="checkbox"/> NESHAP ZZZZ Remote Sources	<input checked="" type="checkbox"/> 40CFR60 Subpart JJJJ <input type="checkbox"/> JJJJ Certified? <input type="checkbox"/> 40CFR60 Subpart IIII <input checked="" type="checkbox"/> IIII Certified? <input type="checkbox"/> 40CFR63 Subpart ZZZZ <input type="checkbox"/> NESHAP ZZZZ/ NSPS JJJJ Window <input type="checkbox"/> NESHAP ZZZZ Remote Sources	<input type="checkbox"/> 40CFR60 Subpart JJJJ <input type="checkbox"/> JJJJ Certified? <input type="checkbox"/> 40CFR60 Subpart IIII <input type="checkbox"/> IIII Certified? <input type="checkbox"/> 40CFR63 Subpart ZZZZ <input type="checkbox"/> NESHAP ZZZZ/ NSPS JJJJ Window <input type="checkbox"/> NESHAP ZZZZ Remote Sources				
Engine Type ⁶	4SRB	4SLB					
APCD Type ⁷	NSCR	OxCat					
Fuel Type ⁸	RG	RG					
H ₂ S (gr/100 scf)	<1	<1					
Operating bhp/rpm	84 @ 1800	1380 @ 1400					
BSFC (BTU/bhp-hr)	7914	8256					
Hourly Fuel Throughput	526.4 ft ³ /hr gal/hr	9,020.65 ft ³ /hr gal/hr	ft ³ /hr gal/hr				
Annual Fuel Throughput (Must use 8,760 hrs/yr unless emergency generator)	4.62 MMft ³ /yr gal/yr	79.02 MMft ³ /yr gal/yr	MMft ³ /yr gal/yr				
Fuel Usage or Hours of Operation Metered	Yes <input checked="" type="checkbox"/> No <input type="checkbox"/>	Yes <input checked="" type="checkbox"/> No <input type="checkbox"/>	Yes <input type="checkbox"/> No <input type="checkbox"/>				
Calculation Methodology ⁹	Pollutant ¹⁰	Hourly PTE (lb/hr) ¹¹	Annual PTE (tons/year) ¹¹	Hourly PTE (lb/hr) ¹¹	Annual PTE (tons/year) ¹¹	Hourly PTE (lb/hr) ¹¹	Annual PTE (tons/year) ¹¹
AP	NO _x	0.19	0.81	1.52	6.66		
AP	CO	0.37	1.62	0.52	2.27		
AP	VOC	0.04	0.18	1.40	6.13		
AP	SO ₂	<0.01	<0.01	<0.01	0.03		
AP	PM ₁₀	0.013	0.06	0.11	0.50		
AP	Formaldehyde	0.015	0.065	0.32	1.41		
AP	Total HAPs	0.022	0.10	0.53	2.31		
AP	GHG (CO ₂ e)	89.7	393	1,750	7,666		

1 Enter the appropriate Source Identification Number for each natural gas-fueled reciprocating internal combustion engine/generator engine located at the well site. Multiple engines should be designated CE-1, CE-2, CE-3 etc. Generator engines should be designated GE-1, GE-2, GE-3 etc. Microturbine generator engines should be designated MT-1, MT-2, MT-3 etc. If more than three (3) engines exist, please use additional sheets.

2 Enter the Source Status using the following codes:

NS Construction of New Source (installation) ES Existing Source

MS	Modification of Existing Source	RS	Relocated Source
REM	Removal of Source		

- 3 Enter the date (or anticipated date) of the engine's installation (construction of source), modification, relocation or removal.
- 4 Enter the date that the engine was manufactured, modified or reconstructed.
- 5 Is the engine a certified stationary spark ignition internal combustion engine according to 40CFR60 Subpart IIII/JJJJ? If so, the engine and control device must be operated and maintained in accordance with the manufacturer's emission-related written instructions. You must keep records of conducted maintenance to demonstrate compliance, but no performance testing is required. If the certified engine is not operated and maintained in accordance with the manufacturer's emission-related written instructions, the engine will be considered a non-certified engine and you must demonstrate compliance as appropriate.

Provide a manufacturer's data sheet for all engines being registered.

- 6 Enter the Engine Type designation(s) using the following codes:

2SLB	Two Stroke Lean Burn	4SRB	Four Stroke Rich Burn
4SLB	Four Stroke Lean Burn		
- 7 Enter the Air Pollution Control Device (APCD) type designation(s) using the following codes:

A/F	Air/Fuel Ratio	IR	Ignition Retard
HEIS	High Energy Ignition System	SIPC	Screw-in Precombustion Chambers
PSC	Prestratified Charge	LEC	Low Emission Combustion
NSCR	Rich Burn & Non-Selective Catalytic Reduction	OxCat	Oxidation Catalyst
SCR	Lean Burn & Selective Catalytic Reduction		
- 8 Enter the Fuel Type using the following codes:

PQ	Pipeline Quality Natural Gas	RG	Raw Natural Gas /Production Gas	D	Diesel
----	------------------------------	----	---------------------------------	---	--------
- 9 Enter the Potential Emissions Data Reference designation using the following codes. Attach all reference data used.

MD	Manufacturer's Data	AP	AP-42	
GR	GRI-HAPCalc TM	OT	Other	(please list)
- 10 Enter each engine's Potential to Emit (PTE) for the listed regulated pollutants in pounds per hour and tons per year. PTE shall be calculated at manufacturer's rated brake horsepower and may reflect reduction efficiencies of listed Air Pollution Control Devices. Emergency generator engines may use 500 hours of operation when calculating PTE. PTE data from this data sheet shall be incorporated in the *Emissions Summary Sheet*.
- 11 PTE for engines shall be calculated from manufacturer's data unless unavailable.

Engine Air Pollution Control Device (Emission Unit ID# VRU-1) – No Changes Since Initial Permit

Air Pollution Control Device Manufacturer's Data Sheet included?

Yes ☒ No ☐

☒ NSCR

☐ SCR

☐ Oxidation Catalyst

Provide details of process control used for proper mixing/control of reducing agent with gas stream: n/a

Manufacturer: **Miratech**

Model #: **VXC-1408-04-HSG**

Design Operating Temperature: 1000 °F

Design gas volume: **430 + scfm**

Service life of catalyst: **2+ years, depending on site conditions**

Provide manufacturer data? ☒ Yes ☐ No

Volume of gas handled: **430 acfm at 1078 °F**

Operating temperature range for NSCR/Ox Cat:
From 750 °F to 1250 °F

Reducing agent used, if any: **None**

Ammonia slip (ppm): **N/A**

Pressure drop against catalyst bed (delta P): **3.0 inches of H₂O**

Provide description of warning/alarm system that protects unit when operation is not meeting design conditions: **Part of the routine maintenance inspection to warn or alert operations of emissions control degradation is a task called the post-PM emissions check.**

Is temperature and pressure drop of catalyst required to be monitored per 40CFR63 Subpart ZZZZ?

☐ Yes ☒ No

How often is catalyst recommended or required to be replaced (hours of operation)?

Because there are so many factors that impact life of a catalyst, the vendor does not recommend "hours of operation prior to replacement." The routine post-PM emissions check task (every 60 days or 1440 hrs of operation, whichever comes first) determines when the catalyst needs to be serviced or replaced.

How often is performance test required?

☐ Initial

☐ Annual

☐ Every 8,760 hours of operation

☐ Field Testing Required

☒ No performance test required. If so, why (please list any maintenance required and the applicable sections in NSPS/GACT)? **Per 40 CFR 60.4243(a)(iii), an owner or operator of a stationary SI internal combustion engine less than 100 HP, must keep a maintenance plan and records of conducted maintenance to demonstrate compliance and must, to the extent practicable, maintain and operate the engine in a manner consistent with good air pollution control practice for minimizing emissions, but no performance testing is required for an owner or operator.**

Engine Air Pollution Control Device (Emission Unit ID# CE-1)	
Air Pollution Control Device Manufacturer's Data Sheet included? Yes <input checked="" type="checkbox"/> No <input type="checkbox"/>	
<input type="checkbox"/> NSCR <input type="checkbox"/> SCR <input checked="" type="checkbox"/> Oxidation Catalyst	
Provide details of process control used for proper mixing/control of reducing agent with gas stream: n/a	
Manufacturer: EMIT Technologies, Inc.	Model #: ELX-4200Z-1616F-31CEO-36P
Design Operating Temperature: 1000 °F	Design gas volume: 9126 + scfm
Service life of catalyst: 2+ years, depending on site conditions	Provide manufacturer data? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No
Volume of gas handled: 9126 acfm at 1078 °F	Operating temperature range for NSCR/Ox Cat: From 750 °F to 1250 °F
Reducing agent used, if any: None	Ammonia slip (ppm): N/A
Pressure drop against catalyst bed (delta P): 3.0 inches of H₂O	
Provide description of warning/alarm system that protects unit when operation is not meeting design conditions: Part of the routine maintenance inspection to warn or alert operations of emissions control degradation is a task called the post-PM emissions check.	
Is temperature and pressure drop of catalyst required to be monitored per 40CFR63 Subpart ZZZZ? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	
How often is catalyst recommended or required to be replaced (hours of operation)? Because there are so many factors that impact life of a catalyst, the vendor does not recommend "hours of operation prior to replacement." The routine post-PM emissions check task (every 60 days or 1440 hrs of operation, whichever comes first) determines when the catalyst needs to be serviced or replaced.	
How often is performance test required? <input checked="" type="checkbox"/> Initial <input type="checkbox"/> Annual <input checked="" type="checkbox"/> Every 8,760 hours of operation <input type="checkbox"/> Field Testing Required <input type="checkbox"/> No performance test required. If so, why (please list any maintenance required and the applicable sections in NSPS/GACT)?	

**ATTACHMENT Q – PNEUMATIC CONTROLLERS
DATA SHEET**

Are there any continuous bleed natural gas driven pneumatic controllers at this facility that commenced construction, modification or reconstruction after August 23, 2011, and on or before September 18, 2015?

☐ Yes ☒ No

Please list approximate number.

Are there any continuous bleed natural gas driven pneumatic controllers at this facility that commenced construction, modification or reconstruction after September 18, 2015?

☐ Yes ☒ No

Please list approximate number.

Are there any continuous bleed natural gas driven pneumatic controllers at this facility with a bleed rate greater than 6 standard cubic feet per hour that are required based on functional needs, including but not limited to response time, safety and positive actuation that commenced construction, modification or reconstruction after August 23, 2011, and on or before September 18, 2015?

☐ Yes ☒ No

Please list approximate number.

Are there any continuous bleed natural gas driven pneumatic controllers at this facility with a bleed rate greater than 6 standard cubic feet per hour that are required based on functional needs, including but not limited to response time, safety and positive actuation that commenced construction, modification or reconstruction after September 18, 2015?

☐ Yes ☒ No

Please list approximate number.

**ATTACHMENT R – PNEUMATIC PUMP
DATA SHEET**

Are there any natural gas-driven diaphragm pumps located at a well site that commenced construction, modification or reconstruction after September 18, 2015?

☐ Yes ☒ No

Please list.

Source ID #	Date	Pump Make/Model	Pump Size

ATTACHMENT T – EMISSIONS CALCULATIONS

Provide detailed potential to emit (PTE) emission calculations for criteria and hazardous air pollutants (HAPs) for each emission point identified in the application. For hazardous air pollutants and volatile organic compounds (VOCs), the speciated emission calculations must be included.

Use the following guidelines to ensure complete emission calculations:

- All emission sources and fugitive emissions are included in the emission calculations, as well as all methods used to calculate the emissions.
- Proper emission point identification numbers and APCD and ERD identification numbers are used consistently in the emission calculations that are used throughout the application.
- A printout of the emission summary sheets is attached to the registration application.
- Printouts of any modeling must be included with the emission calculations. The modeling printout must show all inputs/outputs or assumptions that the modeled emissions are based upon.
- If emissions are provided from the manufacturer, the manufacturer's documentation and/or certified emissions must also be included.
- The emission calculations results must match the emissions provided on the emissions summary sheet.
- If calculations are based on a compositional analysis of the gas, attach the laboratory analysis. Include the following information: the location that the sample was taken (and whether the sample was taken from the actual site or a representative site); the date the sample was taken; and, if the sample is considered representative, the reasons that it is considered representative (same gas field, same formation and depth, distance from actual site, etc.).
- Provide any additional clarification as necessary. Additional clarification or information is especially helpful when reviewing modeling calculations to assist the engineer in understanding the basis of assumptions and/or inputs.

Please follow specific guidance provided on the emissions summary sheet when providing the calculations.



USA Compression Unit 2302 Caterpillar G3516BLE Engine Emissions

Date of Manufacture	<u>March 22, 2012</u>	Engine Serial Number	<u>JEF01613</u>	Date Modified/Reconstructed	<u>Not Any</u>
Driver Rated HP	<u>1380</u>	Rated Speed in RPM	<u>1400</u>	Combustion Type	<u>Spark Ignited 4 Stroke</u>
Number of Cylinders	<u>16</u>	Compression Ratio	<u>8:1</u>	Combustion Setting	<u>Ultra Lean Burn</u>
Total Displacement (in ³)	<u>4230</u>	Fuel Delivery Method	<u>Carburetor</u>	Combustion Air Treatment	<u>T.C./Aftercooled</u>

Raw Engine Emissions (905 LHV BTU/SCF Fuel Gas with little to no H2S)

Fuel Consumption 7443 LHV BTU/bhp-hr or 8256 HHV BTU/bhp-hr
Altitude 1200 ft
Maximum Air Inlet Temp 105 F

	<u>g/bhp-hr¹</u>	<u>lb/MMBTU²</u>	<u>lb/hr</u>	<u>TPY</u>
Nitrogen Oxides (NOx)	0.5		1.52	6.66
Carbon Monoxide (CO)	2.43		7.39	32.38
Volatile Organic Compounds (VOC or NMNEHC)	0.92		2.80	12.26
Formaldehyde (CH2O)	0.44		1.34	5.86
Particulate Matter (PM) <small>Filterable+Condensable</small>		9.99E-03	1.14E-01	4.98E-01
Sulfur Dioxide (SO2)		5.88E-04	6.70E-03	2.93E-02
	<u>g/bhp-hr¹</u>		<u>lb/hr</u>	<u>Metric Tonne/yr</u>
Carbon Dioxide (CO2)	474		1442	5729
Methane (CH4)	4.05		12.32	48.95

¹ g/bhp-hr are based on Caterpillar Specifications (GERP) assuming 905 LHV BTU/SCF fuel gas, 1200 ft elevation, and 105 F Max Air Inlet Temperature. Note that g/bhp-hr values are based on 100% Load Operation. For Air Permitting, it is recommended to add a safety margin to CO, VOC, and Formaldehyde to account for variations in fuel gas composition and load.

² Emission Factor obtained from EPA's AP-42, Fifth Edition, Volume I, Chapter 3: Stationary Internal Combustion Sources (Section 3.2 Natural Gas-Fired Reciprocating Engines, Table 3.2-2).

Catalytic Converter Emissions

Catalytic Converter Make and Model: *EMIT ELX-4200Z-1616F-31CEO-36P*
Element Type: *EMIT RE-3615Z*
Number of Elements in Housing: *1.5*
Air/Fuel Ratio Control *Caterpillar ADEM3, NOx Feedback*

	<u>% Reduction</u>		<u>lb/hr</u>	<u>TPY</u>
Nitrogen Oxides (NOx)	0		1.52	6.66
Carbon Monoxide (CO)	93		0.52	2.27
Volatile Organic Compounds (VOC or NMNEHC)	50	(use 30% DRE for High BTU Fuels)	1.40	6.13
Formaldehyde (CH2O)	76		0.32	1.41
Particulate Matter (PM)	0		1.14E-01	4.98E-01
Sulfur Dioxide (SO2)	0		6.70E-03	2.93E-02
	<u>% Reduction</u>		<u>lb/hr</u>	<u>Metric Tonne/yr</u>
Carbon Dioxide (CO2)	0		1442	5729
Methane (CH4)	0		12.32	48.95

ENGINE SPEED (rpm): 1400
 COMPRESSION RATIO: 8:1
 AFTERCOOLER - STAGE 2 INLET (°F): 130
 AFTERCOOLER - STAGE 1 INLET (°F): 201
 JACKET WATER OUTLET (°F): 210
 COOLING SYSTEM: JW+OC+1AC, 2AC
 IGNITION SYSTEM: ADEM3
 EXHAUST MANIFOLD: DRY
 COMBUSTION: Ultra Lean Burn
 NOx EMISSION LEVEL (g/bhp-hr NOx): 0.5
 SET POINT TIMING: 30.0

FUEL SYSTEM:

CAT WIDE RANGE
WITH AIR FUEL RATIO CONTROLSITE CONDITIONS:

FUEL: Nat Gas
 FUEL PRESSURE RANGE (psig): 7.0-50.0
 FUEL METHANE NUMBER: 84.8
 FUEL LHV (Btu/scf): 905
 ALTITUDE (ft): 1200
 MAXIMUM INLET AIR TEMPERATURE (°F): 105
 NAMEPLATE RATING: 1380 bhp@1400rpm

RATING	NOTES	LOAD	MAXIMUM RATING	SITE RATING AT MAXIMUM INLET AIR TEMPERATURE		
			100%	100%	75%	50%
ENGINE POWER	(1)	bhp	1380	1380	1035	690
INLET AIR TEMPERATURE		°F	106	105	105	105

ENGINE DATA						
FUEL CONSUMPTION (LHV)	(2)	Btu/bhp-hr	7443	7443	7972	8562
FUEL CONSUMPTION (HHV)	(2)	Btu/bhp-hr	8256	8256	8843	9498
AIR FLOW	(3)(4)	lb/hr	13863	13863	10874	7602
AIR FLOW WET (77°F, 14.7 psia)	(3)(4)	scfm	3126	3126	2452	1715
INLET MANIFOLD PRESSURE	(5)	in Hg(abs)	94.6	94.6	76.8	54.0
EXHAUST STACK TEMPERATURE	(6)	°F	992	992	986	1006
EXHAUST GAS FLOW (@ stack temp, 14.5 psia)	(7)(4)	ft ³ /min	9126	9126	7138	5065
EXHAUST GAS MASS FLOW	(7)(4)	lb/hr	14380	14380	11290	7900

EMISSIONS DATA						
NOx (as NO ₂)	(8)	g/bhp-hr	0.50	0.50	0.50	0.50
CO	(8)	g/bhp-hr	2.43	2.43	2.61	2.56
THC (mol. wt. of 15.84)	(8)	g/bhp-hr	4.77	4.77	5.11	5.19
NMHC (mol. wt. of 15.84)	(8)	g/bhp-hr	0.72	0.72	0.77	0.78
NMNEHC (VOCs) (mol. wt. of 15.84)	(8)(9)	g/bhp-hr	0.48	0.48	0.51	0.52
HCHO (Formaldehyde)	(8)	g/bhp-hr	0.44	0.44	0.43	0.42
CO ₂	(8)	g/bhp-hr	474	474	506	550
EXHAUST OXYGEN	(10)	% DRY	9.0	9.0	8.7	8.3

HEAT REJECTION						
HEAT REJ. TO JACKET WATER (JW)	(11)	Btu/min	23438	23438	21564	19970
HEAT REJ. TO ATMOSPHERE	(11)	Btu/min	6110	6110	5092	4074
HEAT REJ. TO LUBE OIL (OC)	(11)	Btu/min	4449	4449	3947	3323
HEAT REJ. TO A/C - STAGE 1 (1AC)	(11)(12)	Btu/min	12934	12934	10814	3965
HEAT REJ. TO A/C - STAGE 2 (2AC)	(11)(12)	Btu/min	5679	5679	5341	3462

HEAT EXCHANGER SIZING CRITERIA			
TOTAL JACKET WATER CIRCUIT (JW+OC+1AC)	(12)(13)	Btu/min	44701
TOTAL AFTERCOOLER CIRCUIT (2AC)	(12)(13)	Btu/min	5963
A cooling system safety factor of 0% has been added to the heat exchanger sizing criteria.			

CONDITIONS AND DEFINITIONS

Engine rating obtained and presented in accordance with ISO 3048/1, adjusted for fuel, site altitude and site inlet air temperature.

100% rating at maximum inlet air temperature is the maximum engine capability for the specified fuel at site altitude and maximum site inlet air temperature.

Max. rating is the maximum capability for the specified fuel at site altitude and reduced inlet air temperature.

Lowest load point is the lowest continuous duty operating load allowed. No overload permitted at rating shown.

For notes information consult page three.



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Prepared For:

Joel LeBlanc

USA COMPRESSION

INFORMATION PROVIDED BY CATERPILLAR

Engine:	G3516B
Horsepower:	1380
RPM:	1400
Compression Ratio:	8.0:1
Exhaust Flow Rate:	9126 CFM
Exhaust Temperature:	992 °F
Reference:	DM8800-04
Fuel:	Natural Gas
Annual Operating Hours:	8760

Uncontrolled Emissions

NOx:	0.50 g/bhp-hr
CO:	2.43 g/bhp-hr
THC:	4.77 g/bhp-hr
NMHC:	0.72 g/bhp-hr
NMNEHC:	0.48 g/bhp-hr
HCHO:	0.44 g/bhp-hr
Oxygen:	9.00 %

POST CATALYST EMISSIONS

NOx:	Unaffected by Oxidation Catalyst
CO:	>93% Reduction
VOC:	>50% Reduction
HCHO:	>76% Reduction

CONTROL EQUIPMENT

Catalytic Converter

Model:	ELX-4200Z-1616F-31CE0-36P
Catalyst Type:	Oxidation, Precious group metals
Manufacturer:	EMIT Technologies, Inc.
Element Size:	1 - Rectangle 38 x 15 x 3.5 1 - Rectangle 18 x 15 x 3.5
Catalyst Elements:	2
Housing Type:	3 Element Capacity
Catalyst Installation:	Accessible Housing
Construction:	10 gauge Carbon Steel
Sample Ports:	6 (0.5" NPT)
Inlet Connections:	16" Flat Face Flange
Outlet Connections:	16" Flat Face Flange
Configuration:	End In / Side Out
Silencer:	Integrated
Silencer Grade:	Hospital Enhanced
Insertion Loss:	35-50 dBA

Jay-Bee Oil & Gas, Inc.
EMISSIONS SUMMARY

Larry Well Pad Production Facility
Tyler County, WV

Emission Point ID	Emission Unit ID	Description	NOx lb/hr	CO lb/hr	CO2e lb/hr	CH4 ¹ lb/hr	VOC ⁴ lb/hr	SO2 lb/hr	PM lb/hr	Benzene lb/hr	Ethylbenzene lb/hr	Xylenes lb/hr	n-Hexane lb/hr	Toluene lb/hr	Formaldehyde lb/hr	Total HAPs lb/hr
13E	CE-1	Compressor Engine (Controlled) NEW	1.52	0.52	1,750	12.32	1.40	0.007	0.11	0.005	0.000	0.002	0.01	0.005	0.321	0.53
1E	HTR-1	GPU #1	0.15	0.13	181.1	0.003	0.01	0.001	0.011				0.003		0.000	0.003
2E	HTR-2	GPU #2	0.15	0.13	181.1	0.003	0.01	0.001	0.011				0.003		0.000	0.003
3E	HTR-3	GPU #3	0.15	0.13	181.1	0.003	0.01	0.001	0.011				0.003		0.000	0.003
4E	HTR-4	Line Heater	0.05	0.04	60.4	0.00	0.00	0.000	0.004				0.001		0.000	0.001
5E	TL-1	Truck Loading - Condensate ²					2.96						0.16			0.16
6E	TL-2	Truck Loading - Produced Water ²					0.08						0.01			0.01
7E	VRU-1	VRU Compressor	0.19	0.37	89.7	0.13	0.04	0.000	0.013	0.001	0.000	0.000		0.000	0.015	0.022
8E	TEG-1	Thermoelectric Generator	0.00	0.00	1.6	0.00	0.00	0.000	0.000				0.000		0.000	0.000
12E	T01-T06	Condensate Tanks + Water Tanks ³			6.5	0.26	1.83			0.00	0.00	0.002	0.055	0.002		0.060
9E	EC-1	Condensate Tanks + Water Tanks ¹	0.29	1.10	446.6	0.26	1.84	0.001	0.017				0.004		0.000	0.00
10E	RBV-1	500 MBTU/hr Reboiler	0.05	0.04	60.4	0.00	0.003	0.000	0.004				0.001		0.000	0.001
11E	EC-2	Dehydration Unit Combustor	0.27	1.03	417.4	0.01	0.81	0.001	0.037	0.010			0.02	0.034	0.000	0.06
---	---	Truck Traffic Fugitive Dust							12.90							
---	---	Fugitive Emissions			9.3	0.37	0.41									0.004
Total (Excluding Fugitive Emissions)			2.82	3.48	3376.13	12.73	7.16	0.01	0.22	0.02	0.00	0.00	0.27	0.04	0.34	0.86
Total			2.82	3.48	3385.41	13.10	7.57	0.01	13.12	0.02	0.00	0.00	0.27	0.04	0.34	0.86

Emission Point ID	Emission Unit ID	Description	NOx tpy	CO tpy	CO2e tpy	CH4 ¹ tpy	VOC ⁴ tpy	SO2 tpy	PM tpy	Benzene tpy	Ethylbenzene tpy	Xylenes tpy	n-Hexane tpy	Toluene tpy	Formaldehyde tpy	Total HAPs tpy
13E	CE-1	Compressor Engine (Controlled) NEW	6.66	2.27	7,666	53.97	6.13	0.029	0.50	0.022	0.002	0.009	0.06	0.020	1.407	2.31
1E	HTR-1	GPU #1	0.66	0.55	793	0.02	0.04	0.004	0.05				0.01		0.000	0.01
2E	HTR-2	GPU #2	0.66	0.55	793	0.02	0.04	0.004	0.05				0.01		0.000	0.01
3E	HTR-3	GPU #3	0.66	0.55	793	0.02	0.04	0.004	0.05				0.01		0.000	0.01
4E	HTR-4	Line Heater	0.22	0.18	264	0.01	0.01	0.001	0.02				0.00		0.000	0.00
5E	TL-1	Truck Loading - Condensate ²					0.91						0.05			0.05
6E	TL-2	Truck Loading - Produced Water ²					0.04						0.00			0.00
7E	VRU-1	VRU Compressor	0.81	1.62	393	0.55	0.18	0.002	0.06	0.005	0.000	0.001		0.002	0.065	0.10
8E	TEG-1	Thermoelectric Generator	0.01	0.00	7	0.00	0.00	0.000	0.00				0.00		0.000	0.00
12E	T01-T06	Condensate Tanks + Water Tanks ³			28	1.14	8.03			0.00	0.00	0.01	0.24	0.01		0.26
9E	EC-1	Condensate Tanks + Water Tanks ¹	1.25	4.81	1956	0.07	0.43	0.00	0.07				0.01		0.001	0.02
10E	RBV-1	500 MBTU/hr Reboiler	0.22	0.18	264.5	0.01	0.01	0.001	0.017				0.004		0.000	0.004
11E	EC-2	Dehydration Unit Combustor	1.19	4.50	1828.1	0.03	3.54	0.003	0.161	0.04			0.09	0.15	0.002	0.28
---	---	Truck Traffic Fugitive Dust							2.56							
---	---	Fugitive Emissions			40.65	1.63	1.78									0.018
Total (Excluding Fugitive Emissions)			12.33	15.23	14787.43	55.81	19.38	0.05	0.97	0.07	0.00	0.02	0.50	0.18	1.48	3.07
Total			12.33	15.23	14828.08	57.44	21.16	0.05	3.54	0.07	0.00	0.02	0.50	0.18	1.48	3.09
Previous Emissions			5.67	12.96	7160.64	3.40	15.01	0.02	3.04	0.05	0.00	0.01	0.44	0.16	0.07	0.78
Increase/Decrease			6.66	2.27	7667.44	54.04	6.15	0.03	0.50	0.02	0.00	0.01	0.06	0.02	1.41	2.31

¹ Condensate and water tank emissions are currently controlled by a VRU + Enclosed Combustor at 98%. This line represents the un-controlled 2%.

² Truck loading is un-controlled.

³ This line represents the 2% Un-captured/Controlled associated with the VRU.

⁴ VRU-1 and EC-1 would not run concurrent so hourly VOC and CH4 emissions for these sources are only accounted for once.

Jay-Bee Oil & Gas, LLC
ENGINE EMISSIONS

Larry Well Pad Production Facility
Tyler County, WV

Controlled Emissions

Source CE-1

Engine Data:

Engine Manufacturer	Caterpillar
Engine Model	G3516 BLE
Type (Rich-burn or Low Emission)	Lean
Aspiration (Natural or Turbocharged)	Turbo
Turbocharge Cooler Temperature	130 deg. F
Manufacturer Rating	1,380 hp
Speed at Above Rating	1,400 rpm
Configuration (In-line or Vee)	In-Line
Number of Cylinders	16
Fuel Heat Content (HHV)	1,263 BTU/scf
Fuel Consumption (HHV)	8,256 Btu/bhp-hr

Emission Rates:

	g/bhp-hr	lb/hr	tons/year	g/hr	lb/day	AP-42 4Stroke Lean lb/mmbtu
Oxides of Nitrogen, NOx	0.50	1.52	6.66	690	36.51	
Carbon Monoxide CO	0.17	0.52	2.27	235	12.42	
VOC (NMNEHC)	0.46	1.40	6.13	635	33.59	
CO2e		1750.13	7665.57			

Comment

453.59 grams = 1 pound
2,000 pounds = 1 ton

Total Annual Hours of Operation

8,760						
SO2	0.006699	0.0293			0.000588	Mfg. Data
PM2.5	0.000878	0.0038			0.0000771	
PM	0.113819	0.4985			0.00999	Mfg. Data
CO2	474	1442.09	6316.35			Mfg. Data
Methane	4.05	12.32	53.97			Mfg. Data
acrolein		0.058561	0.2565		0.00514	
acetaldehyde		0.095248	0.4172		0.00836	
formaldehyde	0.106	0.32127	1.4072		0.02820	Mfg. Data
benzene		0.005013	0.0220		0.00044	
ethylbenzene		0.000452	0.0020		0.0000397	
methanol		0.028483	0.1248		0.00250	
toluene		0.004648	0.0204		0.00041	
xylene		0.002096	0.0092		0.00018	
n-Hexane		0.012647	0.0554		0.00111	
total HAPs		0.528419	2.3145		0.045270384	

Jay-Bee Oil & Gas, LLC
ENGINE EMISSIONS

Larry Well Pad Production Facility
Tyler County, WV

Un-controlled Emissions

Source CE-1

Engine Data:

Engine Manufacturer	Caterpillar
Engine Model	G3516 BLE
Type (Rich-burn or Low Emission)	Lean
Aspiration (Natural or Turbocharged)	Turbo
Turbocharge Cooler Temperature	130 deg. F
Manufacturer Rating	1,380 hp
Speed at Above Rating	1,400 rpm
Configuration (In-line or Vee)	In-Line
Number of Cylinders	16
Fuel Heat Content (HHV)	1,263 BTU/scf
Fuel Consumption (HHV)	8,256 Btu/bhp-hr

Emission Rates:

	g/bhp-hr	lb/hr	tons/year	g/hr	lb/day	AP-42 4Stroke Lean lb/mmbtu
Oxides of Nitrogen, NOx	0.50	1.52	6.66	690	36.51	
Carbon Monoxide CO	2.43	7.39	32.38	3,353	177.43	
VOC (NMNEHC)	0.92	2.80	12.26	1,270	67.18	
CO2e		1750.13	7665.57			

Comment

453.59 grams = 1 pound
2,000 pounds = 1 ton

Total Annual Hours of Operation

8,760						
SO2		0.006699	0.0293			0.000588
PM2.5		0.000878	0.0038			0.0000771
PM		0.113819	0.4985			0.00999
CO2	474	1442.09	6316.35			
Methane	4.05	12.32	53.97			
acrolein		0.058561	0.2565			0.00514
acetaldehyde		0.095248	0.4172			0.00836
formaldehyde	0.440	1.338624	5.8632			0.11749
benzene		0.005013	0.0220			0.00044
ethylbenzene		0.000452	0.0020			0.0000397
methanol		0.028483	0.1248			0.00250
toluene		0.004648	0.0204			0.00041
xylenes		0.002096	0.0092			0.00018
n-Hexane		0.012647	0.0554			0.00111
total HAPs		1.545774	6.7705			0.134566219

Mfg. Data

Mfg. Data

Mfg. Data

Jay-Bee Oil & Gas, LLC

Larry Well Pad Production Facility Tyler County, WV

Controlled Emission Rates

Source VRU-1

Engine Data:

Engine Manufacturer	Cummins
Engine Model	G5.9
Type (Rich-burn or Low Emission)	Rich Burn
Aspiration (Natural or Turbocharged)	Natural

Manufacturer Rating	84	hp
Speed at Above Rating	1,800	rpm
Configuration (In-line or V)	In-line	
Number of Cylinders	6	
Engine Bore	4.020	inches
Engine Stroke	4.720	inches

Engine Displacement	359	cu. in.
Engine BMEP	103	psi
Fuel Consumption (HHV)	7,914	Btu/bhp-hr

Emission Rates:

	g/bhp-hr	lb/hr	tpy	g/hr	lb/day	AP-42 4strokerich lb/MMBtu
Oxides of Nitrogen, NOx	1.000	0.19	0.81	84	4.44	
Carbon Monoxide CO	2.000	0.37	1.62	168	8.89	
VOC (NMNEHC)	0.220	0.04	0.18	18	0.98	
CO2	449	83	364	37,716	1,996	
CO2e		90	393			

Comment
453.59 grams = 1 pound
2,000 pounds = 1 ton

Total Annual Hours of Operation

	8,760				
SO2		0.0004	0.0017		0.0006
PM2.5		0.00632	0.0277		0.0095
PM (Condensable)		0.00659	0.0289		0.00991
CH4		0.12623	0.5529		0.0022
N2O		0.01148	0.0503		0.0002
acrolein		0.00175	0.0077		0.00263
acetaldehyde		0.00185	0.0081		0.00279
formaldehyde	0.080	0.0148	0.0649		
benzene		0.00105	0.0046		0.00158
toluene		0.00037	0.0016		0.000558
ethylbenzene		1.6E-05	0.0001		0.0000248
xylene		0.00013	0.0006		0.000195
methanol		0.00203	0.0089		0.00306
Total HAPs		0.02202	0.0964		

Factor From 40 CFR 98, Table C-2
Factor From 40 CFR 98, Table C-2

Per Mfg.

Exhaust Parameters:

Exhaust Gas Temperature	1,078	deg. F
Exhaust Gas Mass Flow Rate		lb/hr
Exhaust Gas Mass Flow Rate	430	acfm

Exhaust Stack Height	96	inches
	8.00	feet

Exhaust Stack Inside Diameter	4	inches
	0.333	feet

Exhaust Stack Velocity	82.1	ft/sec
	4,927.4	ft/min

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

Potential Emission Rates

Source HTR-1 Through HTR-3

***Emissions shown below are for each Gas Processing Unit**

Burner Duty Rating 1500.0 Mbtu/hr
Burner Efficiency 98.0 %
Gas Heat Content (HHV) 1263.0 Btu/scf
Total Gas Consumption 29,084.8 scfd
H2S Concentration 0.000 Mole %
Hours of Operation 8760

Average heating value of natural gas
1020 Btu/scf

NOx	0.1501	lb/hr	0.657	tpy
CO	0.1261	lb/hr	0.552	tpy
CO2	180.1	lb/hr	788.7	tpy
CH4	0.003	lb/hr	0.015	tpy
CO2e	181	lb/hr	793	tpy
VOC	0.0083	lb/hr	0.036	tpy
SO2	0.0009	lb/hr	0.004	tpy
H2S	0.0000	lb/hr	0.000	tpy
PM10	0.0114	lb/hr	0.050	tpy
CHOH	0.0001	lb/hr	0.000	tpy
Benzene	0.0000	lb/hr	0.000	tpy
N-Hexane	0.0027	lb/hr	0.012	tpy
Toluene	0.0000	lb/hr	0.000	tpy
Total HAPs	0.0028	lb/hr	0.012	tpy

AP-42 Factors Used

NOx	100 lb/MMCF	
CO	84 lb/MMCF	
CO ₂	120,000 lb/MMCF	Global Warming Potential = 1
VOC	5.5 lb/MMCF	
PM	7.6 lb/MMCF	
SO ₂	0.6 lb/MMCF	
CH ₄	2.3 lb/MMCF	Global Warming Potential = 25
N ₂ O	2.2 lb/MMCF	Global Warming Potential =298
HCOH	0.075 lb/MMCF	
Benzene	0.0021 lb/MMCF	
n-Hexane	1.8 lb/MMCF	
Toluene	0.0034 lb/MMCF	

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

Potential Emission Rates

Source HTR-4 Line Heater

Burner Duty Rating	500.0 Mbtu/hr	
Burner Efficiency	98.0 %	Average heating value of natural gas
Gas Heat Content (HHV)	1263.0 Btu/scf	1020 Btu/scf
Total Gas Consumption	9,694.9 scfd	
H2S Concentration	0.000 Mole %	
Hours of Operation	8760	

NOx	0.0500	lb/hr	0.219	tpy
CO	0.0420	lb/hr	0.184	tpy
CO2	60.0	lb/hr	262.9	tpy
CH4	0.001	lb/hr	0.01	tpy
CO2e	60.4	lb/hr	264	tpy
VOC	0.0028	lb/hr	0.012	tpy
SO2	0.0003	lb/hr	0.001	tpy
H2S	0.0000	lb/hr	0.000	tpy
PM10	0.0038	lb/hr	0.017	tpy
CHOH	0.0000	lb/hr	0.000	tpy
Benzene	0.0000	lb/hr	0.000	tpy
N-Hexane	0.0009	lb/hr	0.004	tpy
Toluene	0.0000	lb/hr	0.000	tpy
Total HAPs	0.0009	lb/hr	0.004	tpy

AP-42 Factors Used

NOx	100 lb/MMCF	
CO	84 lb/MMCF	
CO ₂	120,000 lb/MMCF	Global Warming Potential = 1
VOC	5.5 lb/MMCF	
PM	7.6 lb/MMCF	
SO ₂	0.6 lb/MMCF	
CH ₄	2.3 lb/MMCF	Global Warming Potential = 25
N ₂ O	2.2 lb/MMCF	Global Warming Potential = 298
HCOH	0.075 lb/MMCF	
Benzene	0.0021 lb/MMCF	
n-Hexane	1.8 lb/MMCF	
Toluene	0.0034 lb/MMCF	

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

Potential Emission Rates

Source TEG-1

Burner Duty Rating	13.0 MBtu/hr	
Burner Efficiency	98.0 %	
Gas Heat Content (HHV)	1263.0 Btu/scf	Average heating value of natural gas
Total Gas Consumption	252.1 scfd	1020 Btu/scf
H2S Concentration	0.000 Mole %	
Hours of Operation	8760	

NOx	0.0013	lb/hr	0.006	tpy
CO	0.0011	lb/hr	0.005	tpy
CO2	1.6	lb/hr	6.8	tpy
CH4	0.000	lb/hr	0.000	tpy
CO2e	1.6	lb/hr	7	tpy
VOC	0.0001	lb/hr	0.000	tpy
SO2	0.0000	lb/hr	0.000	tpy
H2S	0.0000	lb/hr	0.000	tpy
PM10	0.0001	lb/hr	0.000	tpy
CHOH	0.0000	lb/hr	0.000	tpy
Benzene	0.0000	lb/hr	0.000	tpy
N-Hexane	0.0000	lb/hr	0.000	tpy
Toluene	0.0000	lb/hr	0.000	tpy
Total HAPs	0.0000	lb/hr	0.000	tpy

AP-42 Factors Used

NOx	100 lb/MMCF	
CO	84 lb/MMCF	
CO ₂	120,000 lb/MMCF	Global Warming Potential = 1
VOC	5.5 lb/MMCF	
PM	7.6 lb/MMCF	
SO ₂	0.6 lb/MMCF	
CH ₄	2.3 lb/MMCF	Global Warming Potential = 25
N ₂ O	2.2 lb/MMCF	Global Warming Potential = 298
HCOH	0.075 lb/MMCF	
Benzene	0.0021 lb/MMCF	
n-Hexane	1.8 lb/MMCF	
Toluene	0.0034 lb/MMCF	

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility Tyler County, WV

Potential Emission Rates

Source EC-1 Enclosed Combustor Pilot

Burner Duty Rating	985.1 MBtu/hr
Burner Efficiency	98.0 %
Gas Heat Content (HHV)	1263.0 Btu/scf
Total Gas Consumption	19100.9 scfd
H2S Concentration	0.000 Mole %
Hours of Operation	8760

NOx	0.0985	lb/hr	0.432	tpy
CO	0.0828	lb/hr	0.363	tpy
CO2	118.3	lb/hr	518.0	tpy
CH4	0.002	lb/hr	0.01	tpy
CO2e	119	lb/hr	521	tpy
VOC	0.0054	lb/hr	0.024	tpy
SO2	0.0006	lb/hr	0.003	tpy
H2S	0.0000	lb/hr	0.000	tpy
PM10	0.0075	lb/hr	0.033	tpy
CHOH	0.0001	lb/hr	0.000	tpy
Benzene	0.0000	lb/hr	0.000	tpy
N-Hexane	0.0018	lb/hr	0.008	tpy
Toluene	0.0000	lb/hr	0.000	tpy
Total HAPs	0.0019	lb/hr	0.008	tpy

AP-42 Factors Used (Tables 1.4.1-1.4.3)

NOx	100 lb/MMCF	
CO	84 lb/MMCF	
CO ₂	120,000 lb/MMCF	Global Warming Potential = 1
VOC	5.5 lb/MMCF	
PM	7.6 lb/MMCF	
SO ₂	0.6 lb/MMCF	
CH ₄	2.3 lb/MMCF	Global Warming Potential = 25
N ₂ O	2.2 lb/MMCF	Global Warming Potential = 298
HCOH	0.075 lb/MMCF	
Benzene	0.0021 lb/MMCF	
n-Hexane	1.8 lb/MMCF	
Toluene	0.0034 lb/MMCF	

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

Potential Emission Rates

Source EC-1 Enclosed Vapor Combustor - Control of Tank Emissions

Destruction Efficiency	98.0 %		
Gas Heat Content (HHV)	2313.1 Btu/scf		
Max Flow to T-E	0.028 MMSCFD	10.401 MMSCF/yr	
Max BTUs to Flare	2.746 MMBTU/hr	24,058 MMBTU/yr	

NOx	0.19	lb/hr	0.82	tpy
CO	1.02	lb/hr	4.45	tpy
CO2	321.02	lb/hr	1,406.07	tpy
CO2e	327.68	lb/hr	1,435.26	tpy
VOC	1.83	lb/hr	0.40	tpy
CH4	0.26	lb/hr	0.06	tpy
N2O	0.0006	lb/hr	0.0026	tpy
PM	0.0090	lb/hr	0.0395	tpy
CHOH	0.0001	lb/hr	0.0004	tpy
Benzene	0.0000	lb/hr	0.0000	tpy
n-Hexane	0.0021	lb/hr	0.0094	tpy
Toluene	0.0000	lb/hr	0.0000	tpy
Total HAP	0.0022	lb/hr	0.0098	tpy

Notes: VOC, Total HAP, N-Hexane and CH4 emissions are taken from the Condensate and Produced Water Tank Emissions

Factors Used

AP-42 Table 13.5-1	NOx	0.068 lb/MMBTU	
AP-42 Table 13.5-1	CO	0.37 lb/MMBTU	
40 CFR 98 Table C-1	CO2	116.89 lb/MMBTU	Global Warming Potential = 1
40 CFR 98 Table C-2	CH4	0.0022 lb/MMBTU	Global Warming Potential = 25
40 CFR 98 Table C-2	N2O	0.00022 lb/MMBTU	Global Warming Potential = 298
AP-42 Table 1.4-2	PM	7.6 lb/MMSCF	
AP-42 Table 1.4-3	Benzene	0.0021 lb/MMSCF	
AP-42 Table 1.4-3	Toluene	0.0034 lb/MMSCF	
AP-42 Table 1.4-3	Hexane	1.8 lb/MMSCF	
AP-42 Table 1.4-3	CHOH	0.075 lb/MMSCF	

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

Source RBV-1

Burner Duty Rating 500.0 MBtu/hr
Burner Efficiency 98.0 %
Gas Heat Content (HHV) 1263.0 Btu/scf
Total Gas Consumption 9,695 scfd
H2S Concentration 0.000 Mole %
Hours of Operation 8760

NOx	0.0500	lb/hr	0.219	tpy
CO	0.0420	lb/hr	0.184	tpy
CO2	60.0	lb/hr	262.9	tpy
CH4	0.001	lb/hr	0.01	tpy
CO2e	60.4	lb/hr	264.5	tpy
VOC	0.0028	lb/hr	0.012	tpy
SO2	0.0003	lb/hr	0.001	tpy
H2S	0.0000	lb/hr	0.000	tpy
PM10	0.0038	lb/hr	0.017	tpy
CHOH	0.0000	lb/hr	0.000	tpy
Benzene	0.0000	lb/hr	0.000	tpy
N-Hexane	0.0009	lb/hr	0.004	tpy
Toluene	0.0000	lb/hr	0.000	tpy
Total HAPs	0.0009	lb/hr	0.004	tpy

AP-42 Factors Used

NOx	100 lb/MMCF	
CO	84 lb/MMCF	
CO ₂	120,000 lb/MMCF	Global Warming Potential = 1
VOC	5.5 lb/MMCF	
PM	7.6 lb/MMCF	
SO ₂	0.6 lb/MMCF	
CH ₄	2.3 lb/MMCF	Global Warming Potential = 25
N ₂ O	2.2 lb/MMCF	Global Warming Potential = 298
HCOH	0.075 lb/MMCF	
Benzene	0.0021 lb/MMCF	
n-Hexane	1.8 lb/MMCF	
Toluene	0.0034 lb/MMCF	

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

Potential Emission Rates

Source EC-2 Enclosed Combustor Pilot

Burner Duty Rating 985.1 MBtu/hr
Burner Efficiency 98.0 %
Gas Heat Content (HHV) 1263.0 Btu/scf
Total Gas Consumption 19100.9 scfd
H2S Concentration 0.000 Mole %
Hours of Operation 8760

NOx	0.0985	lb/hr	0.432	tpy
CO	0.0828	lb/hr	0.363	tpy
CO2	118.3	lb/hr	518.0	tpy
CH4	0.002	lb/hr	0.01	tpy
CO2e	119	lb/hr	521	tpy
VOC	0.0054	lb/hr	0.024	tpy
SO2	0.0006	lb/hr	0.003	tpy
H2S	0.0000	lb/hr	0.000	tpy
PM10	0.0075	lb/hr	0.033	tpy
CHOH	0.0001	lb/hr	0.000	tpy
Benzene	0.0000	lb/hr	0.000	tpy
N-Hexane	0.0018	lb/hr	0.008	tpy
Toluene	0.0000	lb/hr	0.000	tpy
Total HAPs	0.0019	lb/hr	0.008	tpy

AP-42 Factors Used (Tables 1.4.1-1.4.3)

NOx	100 lb/MMCF	
CO	84 lb/MMCF	
CO ₂	120,000 lb/MMCF	Global Warming Potential = 1
VOC	5.5 lb/MMCF	
PM	7.6 lb/MMCF	
SO ₂	0.6 lb/MMCF	
CH ₄	2.3 lb/MMCF	Global Warming Potential = 25
N ₂ O	2.2 lb/MMCF	Global Warming Potential = 298
HCOH	0.075 lb/MMCF	
Benzene	0.0021 lb/MMCF	
n-Hexane	1.8 lb/MMCF	
Toluene	0.0034 lb/MMCF	

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility Tyler County, WV

Potential Emission Rates

Source EC-2 Enclosed Vapor Combustor

Destruction Efficiency	98.0 %	
Gas Heat Content (HHV)	660.7 Btu/scf	
Max Flow to T-E	0.09264 MMSCFD	811.526 MMSCF/yr
Max BTUs to Flare	2.55 MMBtu/hr	22,341 MMBtu/yr

NOx	0.17	lb/hr	0.76	tpy
CO	0.94	lb/hr	4.13	tpy
CO2	298.11	lb/hr	1,305.74	tpy
CO2e	298.42	lb/hr	1,307.09	tpy
VOC	0.80	lb/hr	3.51	tpy
CH4	0.01	lb/hr	0.0246	tpy
N2O	0.001	lb/hr	0.0025	tpy
PM	0.029	lb/hr	0.128	tpy
Benzene	0.010	lb/hr	0.042	tpy
CHOH	0.000	lb/hr	0.001	tpy
n-Hexane	0.020	lb/hr	0.086	tpy
Toluene	0.034	lb/hr	0.147	tpy
Total HAPs	0.063	lb/hr	0.276	tpy

Note: VOCs and HAPs are set at 2% of the still vent emissions in the Glycalc Report.

Factors Used

AP-42 Table 13.5-1	NOx	0.068 lb/MMBTU	
AP-42 Table 13.5-1	CO	0.37 lb/MMBTU	
40 CFR 98 Table C-1	CO2	116.89 lb/MMBTU	Global Warming Potential = 1
40 CFR 98 Table C-2	CH4	0.0022 lb/MMBTU	Global Warming Potential = 25
40 CFR 98 Table C-2	N2O	0.00022 lb/MMBTU	Global Warming Potential = 298
AP-42 Table 1.4-2	PM	7.6 lb/MMSCF	
AP-42 Table 1.4-3	CHOH	0.075 lb/MMSCF	

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

TL-1 Truck Loading - Condensate

Per AP-42, Chapter 5.2.2.1.1, the uncontrolled loading loss emission factor LL can be estimated as follows:

$$L_L = 12.46 * (SPM/T)$$

Where,

Loading Loss	$L_L =$	2.979 lb/1000 gallons
Saturation Factor	$S =$	0.6
True Vapor Pressure	$P =$	3.1 psia
Molecular Weight of Vapors	$M =$	66.84 lb/lb-mol
Temperature	$T =$	520 deg R

Maximum Daily Loading	100	BBL/day
	4,200	gpd
Hours of Loading	3	hr

Total VOC	8.9	lb/day	2.96	lb/hr
Total HAP	0.5	lb/day	0.16	lb/hr

Maximum Annual Loading	20,400	BBL/yr
	856,800	gpy

Total VOC	1813.7	lb/yr	0.91	tpy
Total HAP	98.0	lb/yr	0.05	tpy

Emissions

Total VOC	71.059	%
Total HAP	3.841	%

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

TL-2 Truck Loading - Produced Water

Per AP-42, Chapter 5.2.2.1.1, the uncontrolled loading loss emission factor LL can be estimated as follows:

$$L_L = 12.46 * (SPM/T)$$

Where,

Loading Loss	$L_L =$	0.132 lb/1000 gallons
Saturation Factor	$S =$	0.6
True Vapor Pressure	$P =$	0.3 psia
Molecular Weight of Vapors	$M =$	30.68 lb/lb-mol
Temperature	$T =$	520 deg R

Maximum Daily Loading	120	BBL/day
	5,040	gpd
Hours of Loading	3	hr

Total VOC	0.2	lb/day	0.08	lb/hr
Total HAP	0.0	lb/day	0.009	lb/hr

Maximum Annual Loading	43,200	BBL/yr
	1,814,400	gpy

Total VOC	87.3	lb/yr	0.04	tpy
Total HAP	9.6	lb/yr	0.00	tpy

Emissions

Total VOC	36.376	%
Total HAP	4.009	%

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

Truck Loading Fugitive Dust

Item Number	Description	Number of Wheels	Mean Vehicle Weight (tons)	Mean Vehicle Speed (mph)	Miles per Trip	Maximum Trips per Hour	Truck Capacity (BBL/Truck)	Maximum Trips per Year	Control	Control Efficiency (%)
1	Produced Water Transportation Trucks	18	27	10	0.75	1	80	540	None	---
2	Condensate Transportation Trucks	18	27	10	0.75	1	80	255	None	---
			54000	lbs						

		PM	PM-10
k =	Particle size multiplier	0.8	0.36
s =	Silt content of road surface material (%)	10	3
S =	Mean vehicle speed (mph)	10	10
W =	Mean vehicle weight (tons)	27	27
w =	Mean number of wheels per vehicle	18	27
p =	Number of days per year with precipitation >0.01 in.	157	157

$$E (\text{lb/ vehicle mile traveled}) = k \times 5.9 \times (s \div 12) \times (S \div 30) \times (W \div 3)^{0.7} \times (w \div 4)^{0.5} \times ((365 - p) \div 365)$$

Item 1 - Produced Water		PM	PM-10
E	lb/vmt	7.378804125	1.220015589
E	$[\text{lb} \div \text{VMT}] \times [\text{VMT} \div \text{trip}] \times [\text{Trips} \div \text{Hour}] = \text{lb/hr}$	5.534	0.915
E	$[\text{lb} \div \text{VMT}] \times [\text{VMT} \div \text{trip}] \times [\text{Trips} \div \text{Hour}] \times [\text{Ton} \div 2000 \text{ lb}] = \text{tpy}$	1.494	0.247

Item 2 - Condensate		PM	PM-10
E	lb/vmt	7.378804125	1.220015589
E	$[\text{lb} \div \text{VMT}] \times [\text{VMT} \div \text{trip}] \times [\text{Trips} \div \text{Hour}] = \text{lb/hr}$	5.534	0.915
E	$[\text{lb} \div \text{VMT}] \times [\text{VMT} \div \text{trip}] \times [\text{Trips} \div \text{Hour}] \times [\text{Ton} \div 2000 \text{ lb}] = \text{tpy}$	0.706	0.117

Flash Emission Calculations - Condensate

Using Gas-Oil Ratio Method

Un-Controlled

Site specific data

Gas-Oil-ratio	=	500 scf/bbl	Using GOW from comparable well pads.
Throughput	=	20,400 bbl/yr	
Stock tank gas molecular weight	=	39.56 g/mole	

Conversions

1 lb	=	453.6 g
1 mole	=	22.4 L
1 scf	=	28.32 L
1 ton	=	2000 lb

Equations

$$E_{TOT} = Q \frac{(bbl)}{(yr)} \times R \frac{(scf)}{(bbl)} \times \frac{28.32(L)}{1(scf)} \times \frac{1(mole)}{22.4(L)} \times MW \frac{(g)}{(mole)} \times \frac{1(lb)}{453.6(g)} \times \frac{1(ton)}{2000(lb)}$$

E_{TOT} = Total stock tank flash emissions (TPY)

R = Measured gas-oil ratio (scf/bbl)

Q = Throughput (bbl/yr)

MW = Stock tank gas molecular weight (g/mole)

$$E_{spec} = E_{TOT} \times X_{spec}$$

E_{spec} = Flash emission from constituent

X_{spec} = Weight fraction of constituent in stock tank gas

Flash Emissions

Constituent	TPY
Total	562.3396
VOC	394.5881
Nitrogen	1.41E-01
Carbon Dioxide	8.83E-01
Methane	5.58E+01
Ethane	1.11E+02
Propane	1.46E+02
Isobutane	3.94E+01
n-Butane	9.07E+01
2,2 Dimethylpropane	1.11E+00
Isopentane	3.10E+01
n-Pentane	3.26E+01
2,2 Dimethylbutane	1.18E+00
Cyclopentane	0.00E+00
2,3 Dimethylbutane	1.70E+00
2 Methylpentane	9.04E+00
3 Methylpentane	5.40E+00
n-Hexane	1.18E+01
Methylcyclopentane	8.60E-01
Benzene	2.02E-01
Cyclohexane	1.22E+00
2-Methylhexane	2.62E+00
3-Methylhexane	2.58E+00
2,2,4 Trimethylpentane	0.00E+00
Other C7's	2.45E+00
n-Heptane	3.79E+00
Methylcyclohexane	2.36E+00
Toluene	4.61E-01
Other C8's	3.85E+00
n-Octane	1.28E+00
Ethylbenzene	2.81E-02
M & P Xylenes	3.32E-01
O-Xylene	4.50E-02
Other C9's	1.60E+00
n-Nonane	3.82E-01
Other C10's	6.02E-01
n-Decane	7.87E-02
Undecanes (11)	8.44E-02

E_{TOT}

Sum of C3+

HAP

HAP

HAP

HAP

HAP

HAP

Flash Emission Calculations - Produced Water

Using Gas-Water Ratio Method

Un-Controlled

Site specific data

Gas-Water-ratio	=	4.06 scf/bbl	Using GOW from comparable well pads.
Throughput	=	43,200 bbl/yr	
Stock tank gas molecular weight	=	30.68 g/mole	

Conversions

1 lb	=	453.6 g
1 mole	=	22.4 L
1 scf	=	28.32 L
1 ton	=	2000 lb

Equations

$$E_{TOT} = Q \frac{(bbl)}{(yr)} \times R \frac{(scf)}{(bbl)} \times \frac{28.32(L)}{1(scf)} \times \frac{1(mole)}{22.4(L)} \times MW \frac{(g)}{(mole)} \times \frac{1(lb)}{453.6(g)} \times \frac{1(ton)}{2000(lb)}$$

E_{TOT} = Total stock tank flash emissions (TPY)

R = Measured gas-oil ratio (scf/bbl)

Q = Throughput (bbl/yr)

MW = Stock tank gas molecular weight (g/mole)

$$E_{spec} = E_{TOT} \times X_{spec}$$

E_{spec} = Flash emission from constituent

X_{spec} = Weight fraction of constituent in stock tank gas

Flash Emissions

Constituent	TPY
Total	7.4991
VOC	3.8354
Nitrogen	1.25E-01
Carbon Dioxide	1.13E-01
Methane	2.22E+00
Ethane	1.21E+00
Propane	8.62E-01
Isobutane	2.15E-01
n-Butane	6.07E-01
2,2 Dimethylpropane	9.52E-03
Isopentane	3.05E-01
n-Pentane	4.24E-01
2,2 Dimethylbutane	1.58E-02
Cyclopentane	0.00E+00
2,3 Dimethylbutane	3.05E-02
2 Methylpentane	1.70E-01
3 Methylpentane	1.10E-01
n-Hexane	2.96E-01
Methylcyclopentane	2.76E-02
Benzene	5.40E-03
Cyclohexane	3.80E-02
2-Methylhexane	8.26E-02
3-Methylhexane	8.59E-02
2,2,4 Trimethylpentane	0.00E+00
Other C7's	7.90E-02
n-Heptane	1.44E-01
Methylcyclohexane	7.63E-02
Toluene	1.18E-02
Other C8's	1.31E-01
n-Octane	4.11E-02
Ethylbenzene	8.25E-04
M & P Xylenes	6.75E-03
O-Xylene	7.50E-04
Other C9's	3.97E-02
n-Nonane	7.42E-03
Other C10's	8.70E-03
n-Decane	1.50E-03
Undecanes (11)	1.42E-03

E_{TOT}
Sum of C3+

HAP

HAP

HAP

HAP

HAP

HAP

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility

Tyler County, WV

Fugitive VOC Emissions

Volatile Organic Compounds, NMNEHC from gas analysis: 18.40 weight percent
Methane from gas analysis: 59.35 weight percent
Carbon Dioxide from gas analysis: 0.32 weight percent
HAPs from gas analysis:
Hexane 0.62 weight percent
Gas Density: 0.0580 lb/scf

Emission Source:	Count	Oil & Gas Production*	VOC %	VOC (lb/hr)	VOC (tpy)	CO2 (lb/hr)	CO2 (tpy)	CH4 (lb/hr)	CH4 (tpy)	CO2e (tpy)	Hexane (tpy)
Pump Seals:											
Gas:	1	0.00529 lb/hr	18.4	0.001	0.004	0.000	0.000	0.003	0.0138	0.344	0.000
Valves:											
Gas/Vapor:	38	0.02700 scf/hr	18.4	0.011	0.048	0.000	0.001	0.035	0.1546	3.867	0.002
Light Liquid:	18	0.05000 scf/hr	100.0	0.052	0.229						
Low Bleed Pneumatic	-	1.39000 scf/hr	18.4	0.000	0.000	0.000	0.000	0.000	0.0000	0.000	0.000
Relief Valves:	3	0.04000 scf/hr	18.4	0.001	0.006	0.000	0.000	0.004	0.0181	0.452	0.000
Open-ended Lines, gas:	20	0.06100 scf/hr	18.4	0.013	0.057	0.000	0.001	0.042	0.1839	4.598	0.002
Sampling Connectors:											
Gas:	11	0.03300 lb/hr	18.4	0.067	0.293	0.001	0.005	0.215	0.9436	23.595	0.010
Light Liquid:	6	0.03300 lb/hr	100.0	0.198	0.867						
Connectors:											
Gas:	177	0.00300 scf/hr	18.4	0.006	0.025	0.000	0.000	0.018	0.0800	2.001	0.001
Light Liquid:	60	0.00700 scf/hr	100.0	0.024	0.107						
Compressor Seals, Gas:	1	0.01940 lb/hr	18.4	0.004	0.016	0.000	0.000	0.012	0.0504	1.261	0.001
Flanges:											
Gas:	80	0.00086 lb/hr	18.4	0.013	0.055	0.000	0.001	0.041	0.1788	4.472	0.002
Light Liquid:	40	0.00300 scf/hr	100.0	0.007	0.030						

Blowdowns:

	Pressure (psig)	Internal Volume (scf)	Projected Blowdown Events (per year)	Gas Released Per Year (scf)	Gas Released Per Year (lbs)	Composition of Gas (% by volume)	Released (lb/hr)	Released (tpy)	CO2e (tpy)
VOC	300	65	16	1040	124.8	0.70	0.0100	0.0438	
CH4	300	65	16	1040	44.0	0.10	0.0005	0.0022	0.0546
HAPs	300	65	16	1040	116.3	0.02	0.0003	0.0013	

Fugitive Calculations:

	lb/hr	tpy
VOC	0.406	1.780
CH4	0.371	1.625
CO2	0.002	0.009
CO2e	9.280	40.645
HAPs	0.004	0.018

Notes:

Factors are from 40 CFR 98, Table W-1A (scf/hr), where available. Remaining are API (lb/hr)
Sampling Connectors are from TECQ. Remaining are API (lb/hr)

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

Inlet Gas Composition Information:

	Fuel Gas mole %	Fuel M.W. lb/lb-mole	Fuel S.G.	Fuel Wt. %	LHV, dry Btu/scf	HHV, dry Btu/scf	AFR vol/vol	VOC NM / NE	Z Factor	GPM
Nitrogen, N2	0.394	0.110	0.004	0.530			-		0.0039	
Carbon Dioxide, CO2	0.151	0.066	0.002	0.319			-		0.0015	
Hydrogen Sulfide, H2S	-	-	-	-			-		-	
Helium, He	-	-	-	-			-		-	
Oxygen, O2	-	-	-	-			-		-	
Methane, CH4	77.080	12.366	0.427	59.347	701.0	778.5	7.346		0.7693	
Ethane, C2H6	14.832	4.460	0.154	21.405	240.1	262.5	2.474		0.1471	3.945
Propane	4.967	2.190	0.076	10.512	115.0	125.0	1.183	10.512	0.0488	1.361
Iso-Butane	0.616	0.358	0.012	1.718	18.5	20.0	0.191	1.718	0.0060	0.200
Normal Butane	1.210	0.703	0.024	3.375	36.4	39.5	0.375	3.375	0.0117	0.379
Iso Pentane	0.266	0.192	0.007	0.921	9.8	10.6	0.101	0.921	0.0027	0.097
Normal Pentane	0.262	0.189	0.007	0.907	9.7	10.5	0.100	0.907	0.0026	0.094
Hexane	0.151	0.130	0.004	0.625	6.6	7.2	0.068	0.625	0.0015	0.062
Heptane	0.071	0.071	0.002	0.341	3.6	3.9	0.037	0.341	0.0007	0.033
	100.000	20.837	0.719		1,140.8	1,257.7	11.875	18.400	0.9958	6.172

Gas Density (STP) = 0.058

Ideal Gross (HHV)	1,257.7
Ideal Gross (sat'd)	1,236.6
GPM	-
Real Gross (HHV)	1,263.0
Real Net (LHV)	1,145.6

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

Condensate Tank Flash Vapor Composition Information:

	Fuel Gas mole %	Fuel M.W. lb/lb-mole	Fuel S.G.	Fuel Wt. %	LHV, dry Btu/scf	HHV, dry Btu/scf	AFR vol/vol	VOC NM / NE	Z Factor	GPM
Nitrogen, N2	0.036	0.009	0.000	0.022			-		0.0003	
Carbon Dioxide, CO2	0.141	0.041	0.001	0.103			-		0.0009	
Hydrogen Sulfide, H2S	-	0.000	0.000	0.000	0.0	0.0	0.000		0.0000	
Helium, He	-	-	-	-			-		-	
Oxygen, O2	-	-	-	-			-		-	
Methane, CH4	24.485	3.370	0.116	8.458	191.0	212.2	2.002		0.2096	
Ethane, C2H6	25.943	8.112	0.280	20.358	436.7	477.4	4.500		0.2676	7.176
Propane	23.253	11.311	0.391	28.386	593.8	645.4	6.110	28.386	0.2520	7.030
Iso-Butane	4.773	3.064	0.106	7.690	158.2	171.4	1.633	7.690	0.0512	1.715
Normal Butane	10.980	6.916	0.239	17.357	358.3	388.2	3.685	17.357	0.1150	3.731
Iso Pentane	3.135	2.367	0.082	5.941	121.4	131.3	1.250	5.941	0.0328	1.195
Normal Pentane	3.175	2.307	0.080	5.791	118.5	128.2	1.219	5.791	0.0320	1.152
Hexane	2.378	1.531	0.053	3.841	78.2	84.5	0.804	3.841	0.0175	0.726
Heptane	1.701	0.818	0.028	2.052	41.6	44.9	0.428	2.052	0.0081	0.374
	100.000	39.846	1.376		2,097.7	2,283.4	21.630	71.059	0.9872	23.100

Gas Density (STP) = 0.111

Ideal Gross (HHV)	2,283.4
Ideal Gross (sat'd)	2,244.3
GPM	-
Real Gross (HHV)	2,313.1
Real Net (LHV)	2,124.9

Jay-Bee Oil & Gas, Inc.

**Larry Well Pad Production Facility
Tyler County, WV**

Water Tank Flash Vapor Composition Information:

	Fuel Gas mole %	Fuel M.W. lb/lb-mole	Fuel S.G.	Fuel Wt. %	LHV, dry Btu/scf	HHV, dry Btu/scf	AFR vol/vol	VOC NM / NE	Z Factor	GPM
Nitrogen, N2	1.821	0.161	0.006	0.652			-		0.0057	
Carbon Dioxide, CO2	1.049	0.705	0.024	2.855			-		0.0160	
Hydrogen Sulfide, H2S	-	0.000	0.000	0.000	0.0	0.0	0.000		0.0000	
Helium, He	-	-	-	-			-		-	
Oxygen, O2	-	-	-	-			-		-	
Methane, CH4	56.602	11.902	0.411	48.188	674.7	749.3	7.070		0.7404	
Ethane, C2H6	16.424	2.946	0.102	11.929	158.6	173.4	1.634		0.0972	2.606
Propane	8.000	1.933	0.067	7.827	101.5	110.3	1.044	7.827	0.0431	1.202
Iso-Butane	1.516	1.070	0.037	4.332	55.2	59.9	0.570	4.332	0.0179	0.599
Normal Butane	4.274	1.187	0.041	4.808	61.5	66.6	0.633	4.808	0.0197	0.641
Iso Pentane	1.784	0.942	0.033	3.812	48.3	52.2	0.497	3.812	0.0131	0.475
Normal Pentane	2.405	0.670	0.023	2.711	34.4	37.2	0.354	2.711	0.0093	0.334
Hexane	2.953	0.990	0.034	4.009	50.6	54.6	0.520	4.009	0.0114	0.470
Heptane	3.172	2.192	0.076	8.877	111.6	120.4	1.147	8.877	0.0218	1.004
100.000	24.699	0.853			1,296.4	1,424.0	13.469	36.376	0.9954	7.331

Gas Density (STP) = 0.069

Ideal Gross (HHV)	1,424.0
Ideal Gross (sat'd)	1,399.9
GPM	-
Real Gross (HHV)	1,430.5
Real Net (LHV)	1,302.3

Jay-Bee Oil & Gas, Inc.

Larry Well Pad Production Facility
Tyler County, WV

Still Vent Gas Composition Information:

	Fuel Gas mole %	Fuel M.W. lb/lb-mole	Fuel S.G.	Fuel Wt. %	LHV, dry Btu/scf	HHV, dry Btu/scf	AFR vol/vol	VOC NM / NE	Z Factor	GPM
Nitrogen, N ₂	0.158	0.044	0.002	0.211	0.0	0.0	-		0.0016	
Carbon Dioxide, CO ₂	0.164	0.072	0.002	0.343	0.0	0.0	0.012		0.0016	
Hydrogen Sulfide, H ₂ S	-	-	-	-	0.0	0.0	-		-	
Water	54.800	9.864	0.341	46.930	0.0	0.0	-		0.5483	
Oxygen, O ₂	-	-	-	-	0.0	0.0	-		-	
Methane, CH ₄	30.600	4.909	0.170	23.356	278.3	309.1	5.104		0.3054	
Ethane, C ₂ H ₆	7.680	2.309	0.080	10.987	124.3	135.9	1.829		0.0762	2.043
Propane	3.300	1.455	0.050	6.923	76.4	83.0	1.022	6.923	0.0324	0.904
Iso-Butane	0.506	0.294	0.010	1.399	15.2	16.5	0.157	1.399	0.0049	0.165
Normal Butane	1.190	0.692	0.024	3.291	35.8	38.8	0.454	3.291	0.0115	0.373
Iso Pentane	0.278	0.201	0.007	0.954	10.3	11.1	0.113	0.954	0.0028	0.101
Normal Pentane	0.328	0.237	0.008	1.126	12.2	13.1	0.133	1.126	0.0033	0.118
Hexane	0.406	0.350	0.012	1.665	17.9	19.3	0.197	1.665	0.0040	0.166
Heptane	0.590	0.591	0.020	2.813	30.1	32.5	1.310	2.813	0.0059	0.271
	100.000	21.018	0.726		600.4	659.3	10.330	18.172	0.9979	4.141

Gas Density (STP) = 0.058

Ideal Gross (HHV)	659.3
Ideal Gross (sat'd)	648.7
GPM	-
Real Gross (HHV)	660.7
Real Net (LHV)	601.7

Jay-Bee Oil & Gas, Inc.

Specific Gravity of Air, @ 29.92 in. Hg and 60 -F, 28.9625
 One mole of gas occupies, @ 14.696 psia & 32 -F, 359.2 cu ft. per lb-mole
 One mole of gas occupies, @ 14.696 psia & 60 -F, 379.64 cu ft. per lb-mole

Hydrogen Sulfide (H₂S) conversion chart:

Q grains H ₂ S/100 scf	=	$\frac{Q}{37.35}$ mole % H ₂ S
		$\frac{Q}{37.35}$ ppmv H ₂ S
Q mole % H ₂ S	=	Q grains H ₂ S/100 scf
		$\frac{Q}{37.35}$ ppmv H ₂ S
Q ppmv H ₂ S	=	$\frac{Q}{37.35}$ grains H ₂ S/100 scf
		$\frac{Q}{37.35}$ mole % H ₂ S

Ideal Gas at 14.696 psia and 60°F

		MW lb/mol	Specific Gravity	Lb per Cu Ft	Cu Ft per Lb	LHV, dry Btu/scf	HHV, dry Btu/scf	LHV Btu/lb	HHV Btu/lb	cu ft of air / 1 cu ft of gas	Z factor
Nitrogen	N ₂	28.013	0.9672	0.0738	13.552	0	0	0	0	0	0.9997
Carbon Dioxide	CO ₂	44.010	1.5196	0.1159	8.626	0	0	0	0	0	0.9964
Hydrogen Sulfide	H ₂ S	34.076	1.1766	0.0898	11.141	587	637	6,545	7,100	7.15	0.9846
Water	H ₂ O	18.000	0.6215	0.0474	21.091	0	0	0	0	0	1.0006
Oxygen	O ₂	31.999	1.1048	0.0843	11.864	0	0	0	0	0	0.9992
Methane	CH ₄	16.043	0.5539	0.0423	23.664	909.4	1,010.0	21,520	23,879	9.53	0.9980
Ethane	C ₂ H ₆	30.070	1.0382	0.0792	12.625	1,618.7	1,769.6	20,432	22,320	16.68	0.9919
Propane	C ₃ H ₈	44.097	1.5226	0.1162	8.609	2,314.9	2,516.1	19,944	21,661	23.82	0.9825
Iso-Butane	C ₄ H ₁₀	58.124	2.0069	0.1531	6.532	3,000.4	3,251.9	19,629	21,257	30.97	0.9711
Normal Butane	C ₄ H ₁₀	58.124	2.0069	0.1531	6.532	3,010.8	3,262.3	19,680	21,308	30.97	0.9667
Iso Pentane	C ₅ H ₁₂	72.151	2.4912	0.1901	5.262	3,699.0	4,000.9	19,478	21,052	38.11	1.0000
Normal Pentane	C ₅ H ₁₂	72.151	2.4912	0.1901	5.262	3,706.9	4,008.9	19,517	21,091	38.11	1.0000
Hexane	C ₆ H ₁₄	86.178	2.9755	0.2270	4.405	4,403.8	4,755.9	19,403	20,940	45.26	0.9879
Heptane	C ₇ H ₁₆	100.205	3.4598	0.2639	3.789	5,100.0	5,502.5	22,000	23,000	52.41	0.9947

Real Gas at 14.696 psia and 60°F

		MW lb/mol	Specific Gravity	Lb per Cu Ft	Cu Ft per Lb	LHV, dry Btu/scf	HHV, dry Btu/scf	LHV Btu/lb	HHV Btu/lb	cu ft of air / 1 cu ft of gas	Gal/Mole
Nitrogen	N ₂	28.013	0.9672	0.0738	13.552	0	0	0	0	0	4.1513
Carbon Dioxide	CO ₂	44.010	1.5196	0.1159	8.626	0	0	0	0	0	6.4532
Hydrogen Sulfide	H ₂ S	34.076	1.1766	0.0898	11.141	621	672	6,545	7,100	7.15	5.1005
Water	H ₂ O	18.000	0.6215	0.0474	21.091						3.8376
Oxygen	O ₂	31.999	1.1048	0.0843	11.864	0	0	0	0	0	3.3605
Methane	CH ₄	16.043	0.5539	0.0423	23.664	911	1,012	21,520	23,879	9.53	6.4172
Ethane	C ₂ H ₆	30.070	1.0382	0.0792	12.625	1,631	1,783	20,432	22,320	16.68	10.126
Propane	C ₃ H ₈	44.097	1.5226	0.1162	8.609	2,353	3,354	19,944	21,661	23.82	10.433
Iso-Butane	C ₄ H ₁₀	58.124	2.0069	0.1531	6.532	3,101	3,369	19,629	21,257	30.97	12.386
Normal Butane	C ₄ H ₁₀	58.124	2.0069	0.1531	6.532	3,094	3,370	19,680	21,308	30.97	11.937
Iso Pentane	C ₅ H ₁₂	72.151	2.4912	0.1901	5.262	3,709	4,001	19,478	21,052	38.11	13.86
Normal Pentane	C ₅ H ₁₂	72.151	2.4912	0.1901	5.262	3,698	4,009	19,517	21,091	38.11	13.713
Hexane	C ₆ H ₁₄	86.178	2.9755	0.2270	4.405	4,404	4,756	19,403	20,940	45.26	15.566
Heptane	C ₇ H ₁₆	100.205	3.4598	0.2639	3.789	5,101	5,503	22,000	23,000	52.41	17.468

ATTACHMENT U – FACILITY-WIDE CONTROLLED EMISSIONS SUMMARY SHEET

List all sources of emissions in this table. Use extra pages if necessary.

Emission Point ID#	NO _x		CO		VOC		SO ₂		PM ₁₀		PM _{2.5}		CH ₄		GHG (CO ₂ e)	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
1E	0.15	0.66	0.13	0.55	0.01	0.04	<0.01	<0.01	0.01	0.05	0.01	0.05	<0.01	0.02	181.1	793
2E	0.15	0.66	0.13	0.55	0.01	0.04	<0.01	<0.01	0.01	0.05	0.01	0.05	<0.01	0.02	181.1	793
3E	0.15	0.66	0.13	0.55	0.01	0.04	<0.01	<0.01	0.01	0.05	0.01	0.05	<0.01	0.02	181.1	793
4E	0.05	0.22	0.04	0.18	<0.01	0.01	<0.01	<0.01	<0.01	0.02	<0.01	0.02	<0.01	0.01	60.4	264
5E					2.96	0.91										
6E					0.08	0.04										
7E	0.19	0.81	0.37	1.62	0.04	0.18	<0.01	<0.01	0.01	0.06	0.01	0.06	0.13	0.55	89.7	393
8E	<0.01	0.01	<0.01	0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	1.6	7
9E	0.29	1.25	1.10	4.81	1.84	0.43	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	0.26	0.07	446.7	1956
10E	0.05	0.22	0.04	0.18	<0.01	0.01	<0.01	<0.01	<0.01	0.02	<0.01	0.02	<0.01	0.01	60.4	264.5
11E	0.27	1.19	1.03	4.5	0.81	3.54	<0.01	<0.01	0.04	0.16	0.04	0.16	0.01	0.03	417.4	1828.1
12E					1.83	8.03							0.26	1.14	6.5	28
13E	1.52	6.66	0.52	2.27	1.40	6.13	<0.01	0.03	0.11	0.50	0.11	0.50	12.32	53.97	1,750	7,666
TOTAL	2.82	12.33	3.48	15.23	7.16	19.38	0.01	0.05	0.22	0.97	0.22	0.97	12.73	55.81	3,376	14,787

Annual emissions shall be based on 8,760 hours per year of operation for all emission units except emergency generators.

According to 45CSR14 Section 2.43.e, fugitive emissions are not included in the major source determination because it is not listed as one of the source categories in Table 1. Therefore, fugitive emissions shall not be included in the PTE above.

ATTACHMENT U – FACILITY-WIDE HAP CONTROLLED EMISSIONS SUMMARY SHEET

List all sources of emissions in this table. Use extra pages if necessary.

Emission Point ID#	Formaldehyde		Benzene		Toluene		Ethylbenzene		Xylenes		Hexane		Total HAPs	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
1E											<0.01	0.01	<0.01	0.01
2E											<0.01	0.01	<0.01	0.01
3E											<0.01	0.01	<0.01	0.01
4E											<0.01	<0.01	<0.01	<0.01
5E											0.16	0.05	0.16	0.05
6E											0.01	<0.01	0.01	<0.01
7E	0.015	0.065	<0.01	<0.01									0.02	0.10
8E														
9E	<0.01	<0.01									<0.01	0.01	<0.01	0.02
10E	<0.01	<0.01									<0.01	<0.01	<0.01	<0.01
11E	<0.01	<0.01	0.01	0.04	0.03	0.15					0.02	0.09	0.06	0.28
12E			<0.01	<0.01	<0.01	0.01	<0.01	<0.01	<0.01	0.01	0.06	0.24	0.06	0.26
13E	0.32	1.41	<0.01	0.02	<0.01	0.02	<0.01	<0.01	<0.01	0.01	0.01	0.06	0.53	2.31
TOTAL	0.34	1.48	0.02	0.07	0.04	0.18	<0.01	<0.01	<0.01	0.02	0.27	0.50	0.86	3.07

Annual emissions shall be based on 8,760 hours per year of operation for all emission units except emergency generators.

According to 45CSR14 Section 2.43.e, fugitive emissions are not included in the major source determination because it is not listed as one of the source categories in Table 1. Therefore, fugitive emissions shall not be included in the PTE above.

ATTACHMENT V – CLASS I LEGAL ADVERTISEMENT

Publication of a proper Class I legal advertisement is a requirement of the G70-D registration process. In the event the applicant's legal advertisement fails to follow the requirements of 45CSR13, Section 8 or the requirements of Chapter 59, Article 3, of the West Virginia Code, the application will be considered incomplete and no further review of the application will occur until this is corrected.

The applicant, utilizing the format for the Class I legal advertisement example provided on the following page, shall have the legal advertisement appear a minimum of one (1) day in the newspaper most commonly read in the area where the facility exists or will be constructed. The notice must be published no earlier than five (5) working days of receipt by this office of your application. The original affidavit of publication must be received by this office no later than the last day of the public comment period.

The advertisement shall contain, at a minimum, the name of the applicant, the type and location of the source, the type and amount of air pollutants that will be discharged (excluding fugitive emissions), the nature of the permit being sought, the proposed start-up date for the source, and a contact telephone number for more information.

The location of the source should be as specific as possible starting with: 1.) the street address of the source; 2.) the nearest street or road; 3.) the nearest town or unincorporated area, 4.) the county, and 5.) latitude and longitude coordinates in decimal format.

Types and amounts of pollutants discharged **must include** all regulated pollutants (Nitrogen Oxides, Carbon Monoxide, Particulate Matter-2.5, Particulate Matter-10, Volatile Organic Compounds, Sulfur Dioxide, Carbon Dioxide Equivalents, Methane, Formaldehyde, Benzene, Toluene, Ethylbenzene, Xylenes, Hexane, Total Hazardous Air Pollutants and their potential to emit or the permit level being sought in units of tons per year.

In the event the 30th day is a Saturday, Sunday, or legal holiday, the comment period will be extended until 5:00 p.m. on the following regularly scheduled business day.

A list of qualified newspapers that are eligible to publish legal ads may be found:

<http://www.sos.wv.gov/elections/resource/Documents/Qualified%20Newspapers.pdf>

**Affidavit Notice Will Be Submitted
Upon Receipt**

AIR QUALITY PERMIT NOTICE

Notice of Application

Notice is given that Jay-Bee Oil & Gas, Inc. has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a modification of the G70-C General Permit Registration and conversion to a G70-D General Permit Registration for its Larry Well Pad Production Facility located off Klondike Acres Rd near Middlebourne in Tyler County, West Virginia. The latitude and longitude coordinates are: 39.47509, -80.88063.

The applicant estimates an increase in potential emissions of the following regulated air pollutants:

- 6.66 tons of Nitrogen Oxides per year
- 6.15 tons of Volatile Organics per year
- 2.27 tons of Carbon Monoxide per year
- 0.50 tons of Particulate Matter per year
- 0.03 tons of Sulfur Dioxide per year
- 1.41 tons of Formaldehyde per year
- 0.02 tons of Benzene per year
- 0.06 tons of n-Hexane per year
- 0.01 tons of Xylene per year
- 0.02 tons of Toluene per year
- 2.31 tons of Total Hazardous Air Pollutants per year
- 54.04 tons of Methane per year
- 7,668 tons of Greenhouse Gases per year

Startup of operation is planned to begin on or about the 24th day of January, 2017. Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1227, during normal business hours.

Dated this the **(Day)** day of **(Month)**, **(Year)**.

By: Mr. Shane Dowell
Office Manager
Jay-Bee Oil & Gas, Inc.