

June 7, 2016

Kleinfelder Project No.: 20163883.001A

Assistant Director for Permitting WV Department of Environmental Protection Division of Air Quality 601 57<sup>th</sup> Street, SE Charleston, WV 25304

SUBJECT: Antero Midstream LLC – West Mountain Compressor Station

West Virginia Department of Environmental Protection, Division of Air Quality,

45CSR13 Air Permit Modification, R13-3215

To Whom it May Concern:

On behalf of Antero Midstream LLC, please find attached the 45CSR13 Air Permit Modification for permit number R13-3215 for the West Mountain Compressor Station (Facility ID 085-00039) located in Ritchie County, West Virginia. A summary of the modifications in this application include:

- 1. Updating compressor engine emissions to reflect catalyst data based on a new catalyst design from the manufacturer.
- 2. New installation of a fuel conditioning heater (0.5 million BTU/hr capacity)
- 3. Eliminating the compressor fuel use limit and synthetic minor status,
- 4. Increasing the dehydrator throughput to 72.5 MMscfd per dehydrator, and
- 5. Modifying the dehydrator flash tank control efficiency based on new standardized guidance from WVDEP.
- 6. Increasing the number of pigging events to 52 per year.

Enclosed are one hard copy and two CDs containing the entire permit application including the application form and required attachments. Per 45CSR22, a \$4,500 application fee is also enclosed which covers the base 45CSR13 \$1,000 application fee, an additional \$1,000 for NSPS requirements, and an additional \$2,500 for Hazardous Air Pollutant requirements.

A copy of the Air Quality Permit Notice for the advertisement is included as Attachment P. As the Notice is being submitted simultaneously with the application, the official affidavit of publication will be submitted to the Division of Air Quality separately once it is completed.

Please call if you have any questions or if I can be of further assistance. I can be reached at (719) 632-3593 or by email at <a href="mailto:kmeszaros@kleinfelder.com">kmeszaros@kleinfelder.com</a>.

Sincerely,

**KLEINFELDER** 

Kaitlin Meszaros

Air Quality Professional

Kaitlin AMesgaros

Enclosure: West Mountain Compressor Station R13-3215 Air Permit Modification

### **Antero Midstream LLC**

### **West Mountain Compressor Station**

NSR Permit Modification Application
West Virginia Department of Environmental Protection
Division of Air Quality
45CSR13 – R13-3215

Ritchie County, West Virginia

June 2016

Prepared by:



1801 California Street, Suite 1100 Denver, CO 80202 (303) 237-6601 Fax (303) 237-6602 www.kleinfelder.com

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### **Table of Contents**

45CSR13 Application Form

Discussion of Nearby Facilities

Attachment A. Business Certificate

Attachment B. Area Map

Attachment C. Installation and Startup Schedule

Attachment D. Regulatory Discussion

Attachment E. Plot Plan

Attachment F. Process Flow Diagram Attachment G. Process Description

Attachment H. Material Safety Data Sheets

Attachment I. Emission Units Table

Attachment J. Emission Point Data Summary Sheet Fugitive Emissions Data Summary Sheet

Attachment L. Emissions Unit Data Sheets

a. Compressor Engines

b. Dehydrator

c. Fuel Conditioning Heater

d. Pigging Venting

Attachment M. Air Pollution Control Device Sheets

a. NSCR Catalysts

Attachment N. Supporting Emissions Calculations

a. Emission Calculations

b. GlyCalc

Attachment O. Monitoring, Recordkeeping, Reporting, and Testing Plans

Attachment P. Public Notice

Attachment R. Authority/Delegation of Authority

### WEST VIRGINIA DEPARTMENT OF **ENVIRONMENTAL PROTECTION**

### DIVISION OF AIR QUALITY

# APPLICATION FOR NSR PERMIT

601 57th Street, SE	ĭ		1	AND	
Charleston, WV 25304 (304) 926-0475		TITLE V PERMIT REVISION			
www.dep.wv.gov/dag			(OP)	TIONAL)	
PLEASE CHECK ALL THAT APPLY TO NSR (45CSR13) (IF KN	NOWN):	PLEASE CHECK	TYPE OF 450	SR30 (TITLE V) RE	EVISION (IF ANY):
☐ CONSTRUCTION ☐ MODIFICATION ☐ RELOCATION		☐ ADMINISTRAT		_	RMODIFICATION
CLASS I ADMINISTRATIVE UPDATE TEMPORARY		_		ED, INCLUDE TITLE	V REVISION
☐ CLASS II ADMINISTRATIVE UPDATE ☐ AFTER-THE-F	FACI			NT S TO THIS APPLI	
FOR TITLE V FACILITIES ONLY: Please refer to "Title V (Appendix A, "Title V Permit Revision Flowchart") and	/ Revisio ability to	on Guidance" in ord o operate with the d	der to determin changes reque	ne your Title V Revisested in this Permit	sion options Application.
Sec	ction I	. General			
Name of applicant (as registered with the WV Secretal     Antero Midstream LLC	ary of Sta	ate's Office):	2. Federal E	Employer ID No. <i>(F</i> 46-5517375	EIN):
3. Name of facility (if different from above):			4. The applic	cant is the:	
West Mountain Compressor Station		OPERATOR	⊠ вотн		
5A. Applicant's mailing address:  5B. Facility's present physical address:					
1615 Wynkoop Street Denver, CO 80202		739 Mountain Dri Pennsboro, WV 26			
6. West Virginia Business Registration. Is the applicant					$oxed{oxed}$ NO
<ul> <li>If YES, provide a copy of the Certificate of Incorpor change amendments or other Business Registration</li> </ul>				hip (one page) incl	uding any name
<ul> <li>If NO, provide a copy of the Certificate of Authority, amendments or other Business Certificate as Attach</li> </ul>	/Author	ity of L.L.C./Regi		e page) including ar	ny name change
7. If applicant is a subsidiary corporation, please provide	the nam	ne of parent corpo	ration:		
8. Does the applicant own, lease, have an option to buy $\boldsymbol{c}$	or otherv	vise have control o	of the <i>propose</i>	ed site? 🛛 YES	□ NO
- If <b>YES</b> , please explain: Antero Midstream LLC	owns th	e land for the site.			
<ul> <li>If NO, you are not eligible for a permit for this source</li> </ul>	€.				
9. Type of plant or facility (stationary source) to be <b>constructed</b> , <b>modified</b> , <b>relocated</b> , <b>administratively updated</b> or <b>temporarily permitted</b> (e.g., coal preparation plant, primary crusher, etc.): Natural Gas Compressor Station  10. North American Industry Classification System (NAICS) code for the facility:			System		
				221210	
11A. DAQ Plant ID No. (for existing facilities only): 085 – 00039  11B. List all current 45CSR13 and 45CSR30 (Title V) permit numbers associated with this process (for existing facilities only): R13-3215					
All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.					

12A.			
<ul> <li>For Modifications, Administrative Updates or Temporary permits at an existing facility, please provide directions to the present location of the facility from the nearest state road;</li> </ul>			
<ul> <li>For Construction or Relocation permits, please provide directions to the proposed new site location from the nearest state road. Include a MAP as Attachment B.</li> </ul>			
From Pennsboro, WV, head southeast on Collins Avenue Make a slight right onto WV-74N and continue for			
12.B. New site address (if applicable):	12C. Nearest city or town:	12D. County:	
1739 Mountain Drive	Pennsboro	Ritchie	
Pennsboro, WV 26415			
12.E. UTM Northing (KM): 4352.404	12F. UTM Easting (KM): 501.859	12G. UTM Zone: 17	
13. Briefly describe the proposed change(s) at the facilit The reduction efficiencies for the engine catalyst have be has been increased to 72.5 MMSCFD per dehydrator. A compressors has been removed so the facility is no long	een updated based on new catalyst infor fuel conditioning heater will be added. L		
<ul> <li>14A. Provide the date of anticipated installation or change.</li> <li>If this is an After-The-Fact permit application, providing did happen: / /</li> </ul>	•	14B. Date of anticipated Start-Up if a permit is granted: September 2016	
14C. Provide a <b>Schedule</b> of the planned <b>Installation</b> of/ <b>Change</b> to and <b>Start-Up</b> of each of the units proposed in this permit application as <b>Attachment C</b> (if more than one unit is involved).			
15. Provide maximum projected <b>Operating Schedule</b> of activity/activities outlined in this application:  Hours Per Day 24 Days Per Week 7 Weeks Per Year 52			
16. Is demolition or physical renovation at an existing fa	cility involved?		
17. Risk Management Plans. If this facility is subject to 112(r) of the 1990 CAAA, or will become subject due to proposed			
changes (for applicability help see www.epa.gov/ceppo), submit your <b>Risk Management Plan (RMP)</b> to U. S. EPA Region III.			
18. Regulatory Discussion. List all Federal and State air pollution control regulations that you believe are applicable to the			
proposed process (if known). A list of possible applica-	able requirements is also included in Atta	achment S of this application	
(Title V Permit Revision Information). Discuss applica	bility and proposed demonstration(s) of	compliance (if known). Provide this	
information as <b>Attachment D</b> .			
Section II. Additional att	achments and supporting de	ocuments.	
19. Include a check payable to WVDEP – Division of Air	Quality with the appropriate application	fee (per 45CSR22 and	
45CSR13).			
20. Include a Table of Contents as the first page of you	ır application package.		
21. Provide a <b>Plot Plan</b> , e.g. scaled map(s) and/or sketch(es) showing the location of the property on which the stationary source(s) is or is to be located as <b>Attachment E</b> (Refer to <b>Plot Plan Guidance</b> ).			
<ul> <li>Indicate the location of the nearest occupied structure</li> </ul>	e (e.g. church, school, business, residen	ce).	
<ol> <li>Provide a Detailed Process Flow Diagram(s) show device as Attachment F.</li> </ol>	ving each proposed or modified emission	ns unit, emission point and control	
23. Provide a Process Description as Attachment G.			
<ul> <li>Also describe and quantify to the extent possible</li> </ul>	all changes made to the facility since the	e last permit review (if applicable).	

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

24. Provide Material Safety Data Sheets (MSDS) for all materials processed, used or produced as Attachment H.			
For chemical processes, provide a MSDS for each compound emitted to the air.			
25. Fill out the E	mission Units Table and	provide it as <b>Attachment I.</b>	
26. Fill out the E	mission Points Data Sur	mmary Sheet (Table 1 and 1	Table 2) and provide it as Attachment J.
27. Fill out the F	ugitive Emissions Data	Summary Sheet and provide	e it as Attachment K.
28. Check all ap	plicable <b>Emissions Unit</b> I	Data Sheets listed below:	
☐ Bulk Liquid Tr	ansfer Operations	☐ Haul Road Emissions	☐ Quarry
☐ Chemical Pro	cesses	☐ Hot Mix Asphalt Plant	Solid Materials Sizing, Handling and Storage
☐ Concrete Bate	ch Plant	☐ Incinerator	Facilities
☐ Grey Iron and	Steel Foundry	☐ Indirect Heat Exchanger	☐ Storage Tanks
☐ General Emis	sion Unit, specify: Engine	s, Dehydrator, Fuel Condition	ning Heater
		ata Sheet(s) as Attachment	
29. Check all ap	plicable Air Pollution Co	ntrol Device Sheets listed be	elow:
☐ Absorption Sy	vstems	☐ Baghouse	☐ Flare
☐ Adsorption Sy	vstems	☐ Condenser	☐ Mechanical Collector
Afterburner		☐ Electrostatic Precip	itator
	ors, specify: Catalysts		
		rol Device Sheet(s) as Attac	
30. Provide all <b>Supporting Emissions Calculations</b> as <b>Attachment N</b> , or attach the calculations directly to the forms listed in Items 28 through 31.			
31. <b>Monitoring, Recordkeeping, Reporting and Testing Plans.</b> Attach proposed monitoring, recordkeeping, reporting and testing plans in order to demonstrate compliance with the proposed emissions limits and operating parameters in this permit application. Provide this information as <b>Attachment O.</b>			
Please be aware that all permits must be practically enforceable whether or not the applicant chooses to propose such measures. Additionally, the DAQ may not be able to accept all measures proposed by the applicant. If none of these plans are proposed by the applicant, DAQ will develop such plans and include them in the permit.			
32. Public Notic	ce. At the time that the ap	oplication is submitted, place	a Class I Legal Advertisement in a newspaper of general
circulation in the area where the source is or will be located (See 45CSR§13-8.3 through 45CSR§13-8.5 and <i>Example Legal</i>			
Advertisement for details). Please submit the Affidavit of Publication as Attachment P immediately upon receipt.			
33. Business C	onfidentiality Claims. Do	oes this application include co	onfidential information (per 45CSR31)?
	☐ YES	⊠ NO	
segment cla	▶ If YES, identify each segment of information on each page that is submitted as confidential and provide justification for each segment claimed confidential, including the criteria under 45CSR§31-4.1, and in accordance with the DAQ's "Precautionary Notice – Claims of Confidentiality" guidance found in the General Instructions as Attachment Q.		
	Sed	ction III. Certification	n of Information
34. Authority/Delegation of Authority. Only required when someone other than the responsible official signs the application. Check applicable Authority Form below:			
	orporation or Other Busin	ess Entity	☐ Authority of Partnership
☐ Authority of G	overnmental Agency		☐ Authority of Limited Partnership
Submit completed and signed <b>Authority Form</b> as <b>Attachment R</b> .			
All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.			
The state of the s			

35A. <b>Certification of Information.</b> To certify 2.28) or Authorized Representative shall check		sible Official (per 45CSR§13-2.22 and 45CSR§30-low.		
Certification of Truth, Accuracy, and Comp	Certification of Truth, Accuracy, and Completeness			
I, the undersigned Responsible Official / Authorized Representative, hereby certify that all information contained in this application and any supporting documents appended hereto, is true, accurate, and complete based on information and belief after reasonable inquiry I further agree to assume responsibility for the construction, modification and/or relocation and operation of the stationary source described herein in accordance with this application and any amendments thereto, as well as the Department of Environmental Protection, Division of Air Quality permit issued in accordance with this application, along with all applicable rules and regulations of the West Virginia Division of Air Quality and W.Va. Code § 22-5-1 et seq. (State Air Pollution Control Act). If the business or agency changes its Responsible Official or Authorized Representative, the Director of the Division of Air Quality will be notified in writing within 30 days of the official change.				
Compliance Certification				
Except for requirements identified in the Title V that, based on information and belief formed af compliance with all applicable requirements.		e is not achieved, I, the undersigned hereby certify taminant sources identified in this application are in		
SIGIVATORIE	use blue ink)	DATE: (Please use blue ink)		
35B. Printed name of signee: Ward McNeilly	Se oge im)	35C. Title: Vice President, Reserves Planning and Midstream		
35D. E-mail: wmcneilly@anteroresources.com	36E. Phone: (303) 357-6822	36F. FAX: (303)357-7315		
36A. Printed name of contact person (if differen	nt from above): Barry Schatz	36B. Title: Senior Environmental and Regulatory Manager		
36C. E-mail: bschatz@anteroresources.com	36D. Phone: 303-357-7276	36E. FAX: 303-357-7315		
	Attachment K:  Attachment L:  Attachment M:  Attachment M:  Attachment N:  Attachment O:  Attachment O:  Attachment O:  Attachment P:  Attachment P:  Attachment R:  Attachment R:  Attachment R:  Attachment R:  Attachment R:  Attachment R:  Complete permit application with	Fugitive Emissions Data Summary Sheet Emissions Unit Data Sheet(s) Air Pollution Control Device Sheet(s) Supporting Emissions Calculations Monitoring/Recordkeeping/Reporting/Testing Plans Public Notice Business Confidential Claims Authority Forms Title V Permit Revision Information  the signature(s) to the DAQ, Permitting Section, at the		
FOR AGENCY USE ONLY – IF THIS IS A TITLE V SOURCE:    Forward 1 copy of the application to the Title V Permitting Group and:   For Title V Administrative Amendments:   NSR permit writer should notify Title V permit writer of draft permit,   For Title V Minor Modifications:   Itile V permit writer should send appropriate notification to EPA and affected states within 5 days of receipt,   NSR permit writer should notify Title V permit writer of draft permit.   For Title V Significant Modifications processed in parallel with NSR Permit revision:   NSR permit writer should notify a Title V permit writer of draft permit,   Public notice should reference both 45CSR13 and Title V permits,   EPA has 45 day review period of a draft permit.				

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

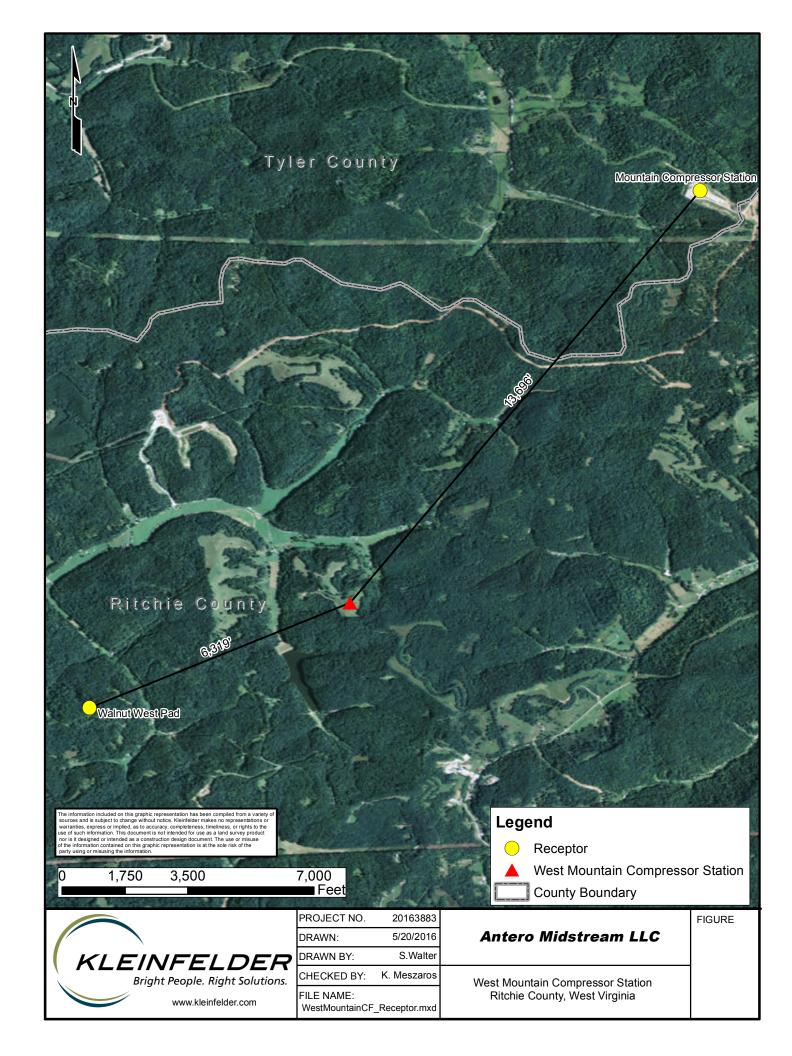
Discussion of Nearby Faciliti	es

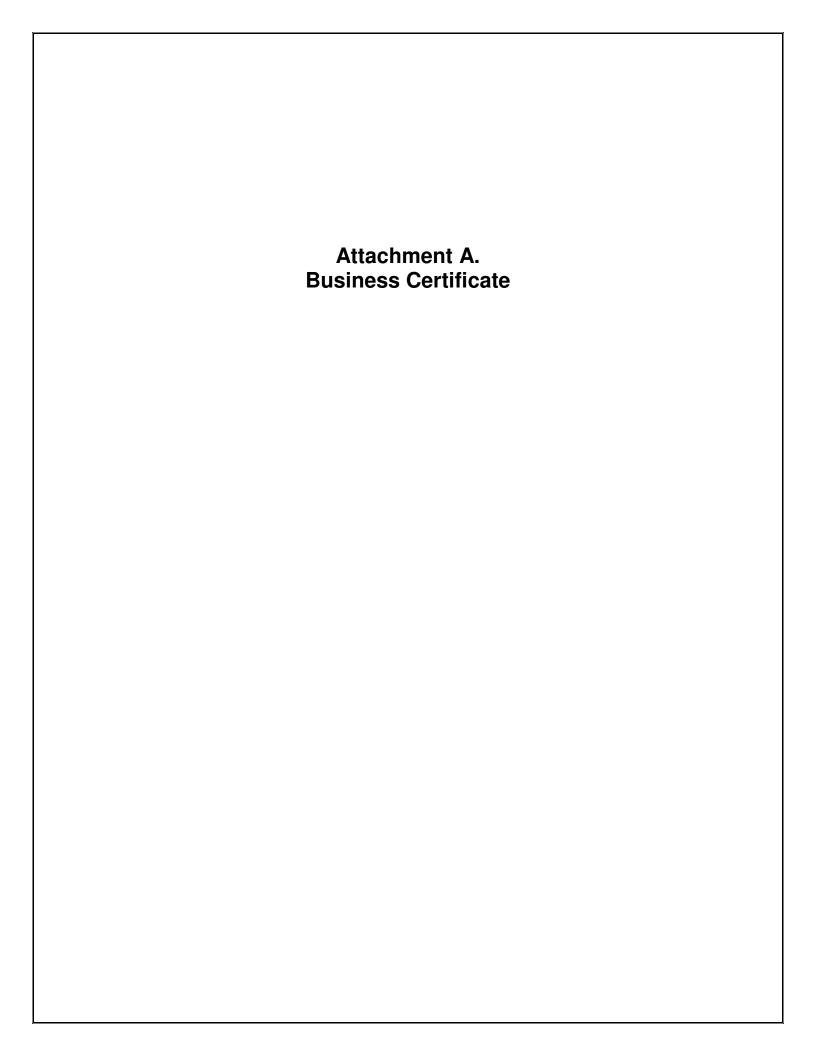
### **West Mountain Compressor Station – Closest Antero Facilities**

- 1. Common Control: Only those facilities that are owned and managed by Antero were included in the aggregation discussion. This includes Antero Resources Corporation production facilities in addition to the Antero Midstream LLC midstream facilities.
- 2. SIC Code: The West Mountain Compressor Station operates under SIC code 4923 (natural gas distribution). The closest Antero Midstream LLC operated facility with this SIC code is Mountain Compressor Station which is located approximately 2.60 miles northeast of the Facility. All Antero Resources Corporation production facilities operate under the SIC code of 1311 (crude petroleum and natural gas extraction). The closest facility operated by Antero Resources Corporation with the SIC code of 1311 is the Walnut West Pad 1.2 miles to the southwest.
- Contiguous or Adjacent: The land between the West Mountain Compressor Station and its nearest facility operating under SIC code 4923 is not owned or managed by Antero Midstream LLC or Antero Resources Corporation. Therefore, the two facilities are not contiguous or adjacent.

Based on this three-pronged evaluation, although the West Mountain Compressor Station and Mountain Compressor Station do belong to the same major industrial group, they should not be aggregated because they are not contiguous or adjacent.

The West Mountain Compressor Station and Walnut West Pad should not be aggregated because they do not belong to the same major industrial group and do not directly rely on each other nor are they contiguous or adjacent.







### I, Natalie E. Tennant, Secretary of State of the State of West Virginia, hereby certify that

### ANTERO MIDSTREAM LLC

Control Number: 9A5E1

a limited liability company, organized under the laws of the State of Delaware has filed its "Application for Certificate of Authority" in my office according to the provisions of West Virginia Code §31B-10-1002. I hereby declare the organization to be registered as a foreign limited liability company from its effective date of April 29, 2014, until a certificate of cancellation is filed with our office.

Therefore, I hereby issue this

# CERTIFICATE OF AUTHORITY OF A FOREIGN LIMITED LIABILITY COMPANY

to the limited liability company authorizing it to transact business in West Virginia



Given under my hand and the Great Seal of the State of West Virginia on this day of April 29, 2014

Secretary of State



IN THE OFFICE OF WY SECRETARY OF STATE

Submitted by: CT Corporation Rep-Terry Stamper Terry.Stamper@wolterskluwer.com 304-776-1152

Natafie E. Tennant Secretary of State 1900 Kanawha Blvd E Bldg 1, Suite 157-K. Charleston, WV 25305

FILE ONE ORIGINAL

FEE: \$150

(Two if you want a filed stamped copy returned to you)



WV APPLICATION FOR CERTIFICATE OF AUTHORITY OF LIMITED LIABILITY COMPANY

Penney Barker, Manager Corporations Division Tel: (304)558-8000 Fax: (304)558-8381 Website: www.wvsos.com E-mail: business@wvsos.com

Office Hours: Monday – Friday 8:30 a.m. – 5:00 p.m. ET Control #

1.	The name of the company as registered in its home state is:	Antero Midstream LLC
	and the state or country of organization is:	Delaware
$\geq$	EXISTENCE (GOOD STANDING), dated do	I and submitted with this application a <u>CERTIFICATE OF</u> uring the current tax year, from your home state of original plication. The certificate may be obtained by contacting the of original incorporation.
2.	The name to be used in West Virginia will be [The name must contain one of the required terms s as limited liability company" or abbreviations such as "LLC" or "PLLC". See instructions for complete list of acceptable terms and requirements for use of trade name.	(If name is not available, check DBA Name box below and follow special instructions in Section 2. attached.)
3.	The company will be a: [See instructions for limitar on professions which may form P.L.L.C. in WV. All ment must have WV professional license. In most cases, a Lette Authorization/Approval from the appropriate State Licensing Board is required to process the application.]	bers
4.	The street address of the principal office is:	No. & Street: 1625 17th Street, Suite 300  Denver, Colorado 80202
	and the mailing address (if different) is:	City/State/Zip:  Street/Box:  City/State/Zip:
5.	The address of the designated office of the company in WV, if any, will be:	No. & Street:  City/State/Zip:  5400 D Big Tyler Road  Charleston, West Virginia 25313
6.	Agent of Process: Properly designated person to whom notice of legal process may be sent, if any:	Name: C T Corporation System  Address: 5400 D Big Tyler Road  City/State/Zip: Charleston, West Virginia 25313
E-	rm LLF-1 Issued b	y the Office of the Secretary of State Revised &

WV045 - 09/04/2013 Wolters Kluwer Online

RECEIVED

Issued by the Office of the Secretary of State

Revised 8/13

Form LLF-I

APPL	ICATION FOR CERTIFICATE O	OF AUTHORITY OF LIMITED LIABILITY COMPANY Page 3	
[R <i>fili</i>	ne requested effective date is: equested date <u>may not be earlier than</u> ing nor later than 90 days after filing our office.	the date & time of filing in the Secretary of State's Office the following date and time	
16. Ce	ontact and Signature Informatio	on* (See below Important Legal Notice Regarding Signature):	
a.	Alvyn A. Schopp	(313) 357-7310	
	Contact Name	Phone Number	
ь.	Alvyn A. Schopp	Chief Administrative Officer and Regional Vice Pres	ident
	Print or type name of aignor	Title / Capacity of Signer	
c.	As Tochto	April 28, 2014	
C.	Signature /	Date	

\*Important Legal Notice Regarding Signature: Per West Virginia Code §31B-2-209. Liability for false statement in filed record. If a record authorized or required to be filed under this chapter contains a false statement, one who suffers loss by reliance on the statement may recover damages for the loss from a person who signed the record or caused another to sign it on the person's behalf and knew the statement to be false at the time the record was signed.

Delaware

PAGE :

### The First State

I, JEFFREY W. BULLOCK, SECRETARY OF STATE OF THE STATE OF

DELAWARE, DO HEREBY CERTIFY "ANTERO MIDSTREAM LLC" IS DULY

FORMED UNDER THE LAWS OF THE STATE OF DELAWARE AND IS IN GOOD

STANDING AND HAS A LEGAL EXISTENCE SO FAR AS THE RECORDS OF THIS

OFFICE SHOW, AS OF THE TWENTY-NINTH DAY OF APRIL, A.D. 2014.

AND I DO HEREBY FURTHER CERTIFY THAT THE ANNUAL TAXES HAVE NOT BEEN ASSESSED TO DATE.

5466900 8300

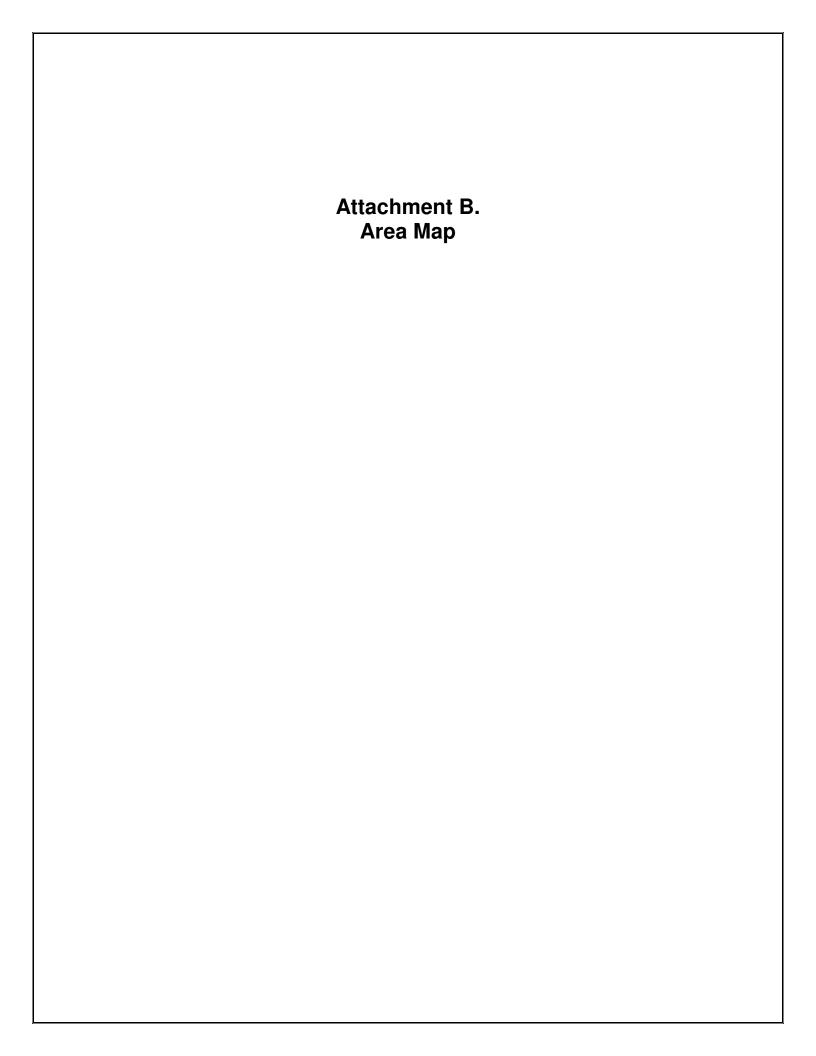
140532521

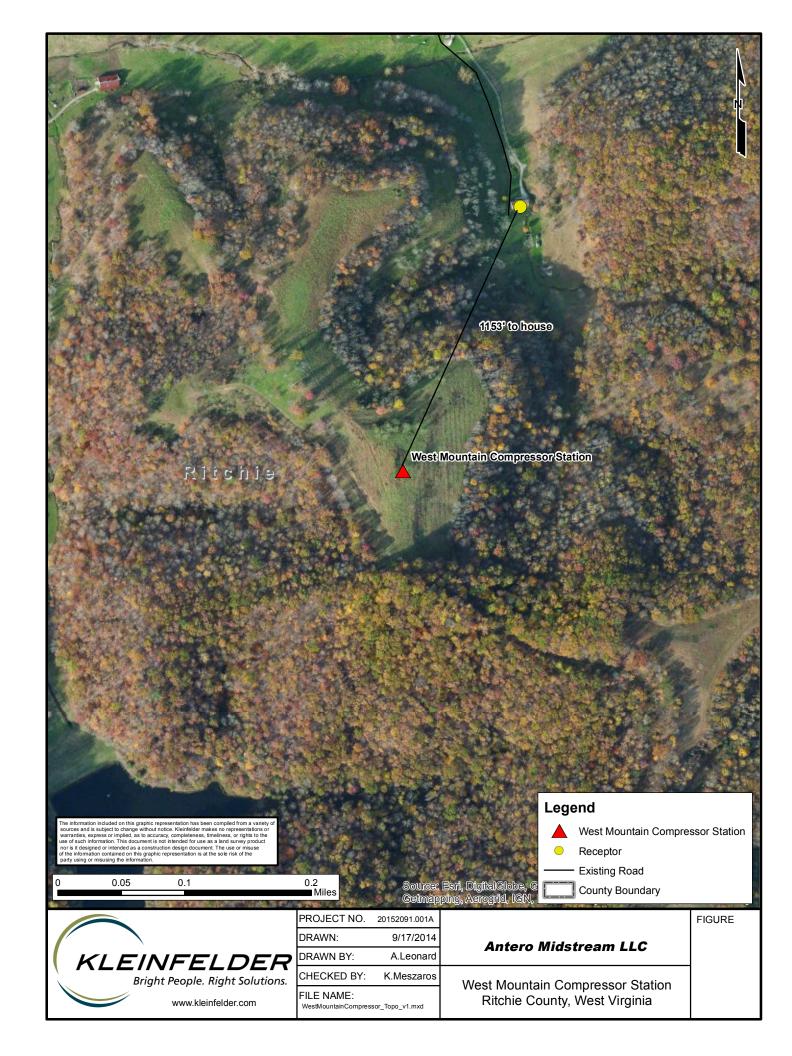
Jeffrey W. Bullock, Secretary of State

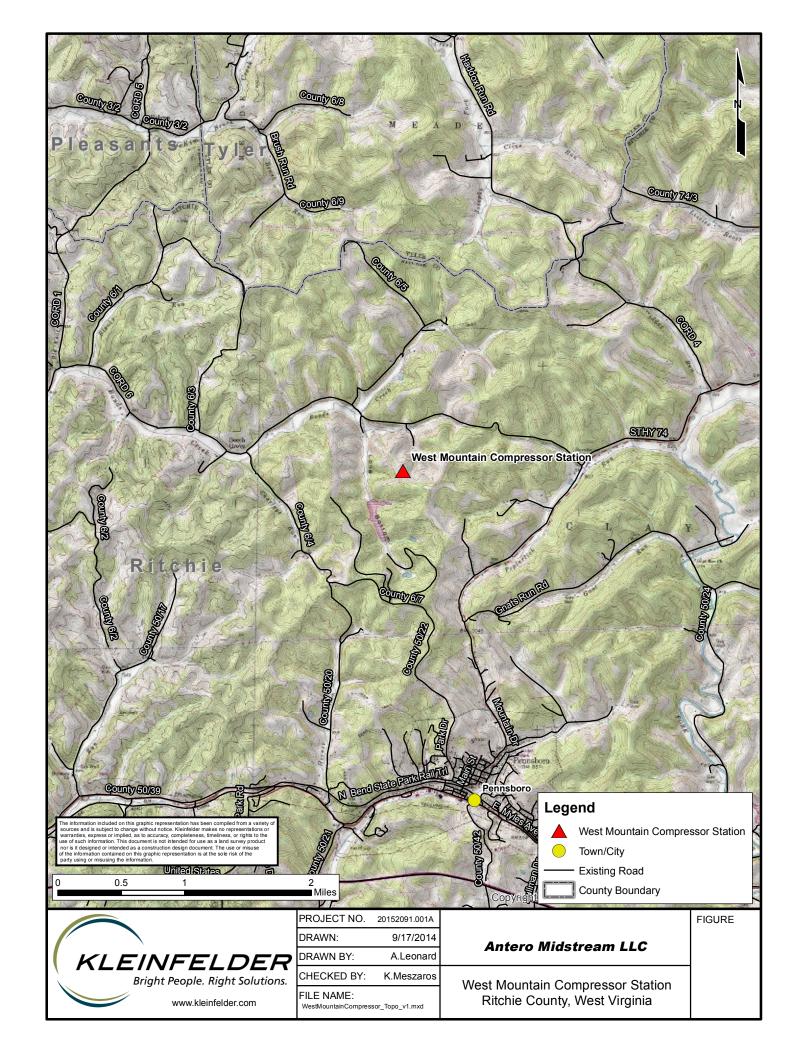
AUTHENT CATION: 1328067

DATE: 04-29-14

You may verify this certificate online at corp.delaware.gov/authver.shtml







Attachr Installation and S		

### **West Mountain Compressor Station – Installation and Startup Schedule**

The West Mountain Compressor Station is an existing facility located in Ritchie County, WV, approximately 2.5 miles north of Pennsboro, WV. Equipment is currently installed and operating per permit R13-3215. The proposed new equipment and modifications are scheduled to be installed and operational around September 1, 2016.

Attachment D. Regulatory Discussion	

### **West Mountain Compressor Station – Regulatory Discussion**

### **Federal Regulations**

### 40 CFR Part 60 – Standards of Performance for New Stationary Sources

I. Subpart Kb - Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984.

<u>Applicability:</u> Subpart Kb applies to volatile organic liquid storage tanks with a capacity greater than or equal to 75 m³ (§60.110b(a)). Storage vessels with a design capacity less than 1,589.874 m³ do not apply to this subpart if they are used store condensate prior to custody transfer. The condensate and produced water storage tanks at the West Mountain Compressor Station will be 64 m³. The settler tank is 79 m³, but stores condensate prior to custody transfer. Therefore, Subpart Kb does not apply to the West Mountain Compressor Station.

II. Subpart GG - Standards of Performance for Stationary Gas Turbines

<u>Applicability:</u> Subpart GG applies to all stationary gas turbines with a heat input at peak load equal to or greater than 10 million BTU per hour based on the lower heating value of the fuel (§60.330(a)). Since the microturbine generators at the West Mountain Compressor Station have a heat input rating less than 10 million Btu per hour, Subpart GG does not apply.

III. Subpart KKK - Standards of Performance for Equipment Leaks of VOC from Onshore Natural Gas Processing Plants for Which Construction, Reconstruction, or Modification Commenced After January 20, 1984, and on or Before August 23, 2011.

<u>Applicability:</u> Subpart KKK applies to facilities built or modified before August 23, 2011, so Subpart KKK will not apply as the West Mountain Compressor Station was constructed after August 23, 2011.

IV. Subpart LLL - Standards of Performance for SO<sub>2</sub> Emissions from Onshore Natural Gas Processing for Which Construction, Reconstruction, or Modification Commenced After January 20, 1984, and on or Before August 23, 2011.

<u>Applicability:</u> Subpart LLL applies to facilities built or modified before August 23, 2011, so Subpart LLL will not apply as the West Mountain Compressor Station was constructed after August 23, 2011.

V. Subpart JJJJ - Standards of Performance for Stationary Spark Ignition Internal Combustion Engines

Applicability: Subpart JJJJ applies to rich burn engines that were ordered after June 12, 2006 and manufactured on or after July 1, 2007 for engines with maximum power

greater than or equal to 500 hp (§60.4230(a)(4)(i)). Thus, Subpart JJJJ applies to the West Mountain Compressor Station as the compressor engines were installed after July 1, 2007 and were manufactured after July 1, 2010.

VI. Subpart KKKK - Standards of Performance for Stationary Combustion Turbines

<u>Applicability:</u> Subpart KKKK applies to all stationary combustion turbines with a heat input at peak load equal to or greater than 10 million BTU per hour based on the higher heating value of the fuel (§60.4305(a)). Since the microturbine generators at the West Mountain Compressor Station have a heat input rating less than 10 million Btu per hour, Subpart KKKK does not apply.

VII. Subpart OOOO - Standards of Performance for Crude Oil and Natural Gas Production, Transmission, and Distribution

Applicability: Subpart OOOO applies to reciprocating compressor facilities that were constructed, modified, or reconstructed after August 23, 2011 (§60.5365(c)). Additionally, Subpart OOOO applies to storage vessel affected facilities with individual tank emissions greater than 6 tons per year (§60.5365(e)). Thus, Subpart OOOO applies to the West Mountain Compressor Station as it was constructed after August 23, 2011 and has reciprocating compressors and a settler tank that's uncontrolled VOC potential to emit is greater than six (6) tons per year. The pneumatic controllers installed at West Mountain Compressor Station are air-actuated and therefore exempt from the requirements of this subpart.

### 40 CFR Part 61 – National Emission Standards for Hazardous Air Pollutants

I. Subpart V – National Emission Standard for Equipment Leaks (Fugitive Emission Sources)

<u>Applicability:</u> Subpart V applies to components such as compressors, valves, and pumps that are intended to operate in volatile hazardous air pollutant (VHAP) service (§61.240(a)). VHAP service means that a component contains or contacts a fluid that is at least 10 percent by weight a VHAP. Subpart V does not apply to the West Mountain Compressor Station because none of the components have fluid (natural gas, water, or condensate) that is over 10 percent by weight of any VHAP.

## 40 CFR Part 63 – National Emission Standards for Hazardous Air Pollutants for Source Categories

I. Subpart HH – National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities

<u>Applicability:</u> Subpart HH applies to oil and natural gas production facilities that are a major or area source of HAP emissions, and that process, upgrade, or store hydrocarbon liquids or natural gas prior to the transmission and storage source category

(§63.760(a)). Subpart HH does apply to the West Mountain Compressor Station, and because it is an area source of HAP emissions, the two (2) TEG dehydrators are applicable sources under Subpart HH (§63.760(b)(2)). However, actual benzene emissions from the dehydrators at the West Mountain Compressor Station will be less than 1 ton per year, so both dehydrators are exempt from all requirements except recordkeeping (§63.764(e)(1)(ii)).

II. Subpart HHH – National Emission Standards for Hazardous Air Pollutants from Natural Gas Transmission and Storage Facilities

<u>Applicability:</u> Subpart HHH applies to natural gas transmission and storage facilities that are a major source of HAP emissions (§63.1270(a)). Subpart HHH does not apply to the West Mountain Compressor Station as it is not a major source of HAP emissions. Further, the West Mountain Compressor Station is prior to the gas transmission and storage phase.

III. Subpart EEEE – National Emission Standards for Hazardous Air Pollutants: Organic Liquids Distribution (Non-Gasoline)

<u>Applicability:</u> Subpart EEEE applies to organic liquids distribution operations that are located at major source of HAP emissions (§63.2334(a)). Subpart EEEE does not apply to the West Mountain Compressor Station as it is not a major source of HAP emissions.

IV. Subpart YYYY – National Emission Standards for Hazardous Air Pollutants for Stationary Combustion Turbines

<u>Applicability:</u> Subpart YYYY applies to stationary combustion turbines located at major sources of HAP emissions (§63.6085(a)). Since the West Mountain Compressor Station is not a major source of HAP emissions, Subpart YYYY does not apply.

V. Subpart ZZZZ - National Emission Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines

<u>Applicability:</u> Subpart ZZZZ applies to stationary RICE at a major or area source of HAP emissions (§63.6585). Subpart ZZZZ applies to the West Mountain Compressor Station as the compressor engines are new RICE. The engines will meet Subpart ZZZZ by meeting 40 CFR Part 60, Subpart JJJJ as the West Mountain Compressor Station is an area source of HAP emissions (§63.6590(c)(1)).

VI. Subpart DDDDD – National Emission Standards for Hazardous Air Pollutants for Industrial, Commercial, and Institutional Boilers and Process Heaters

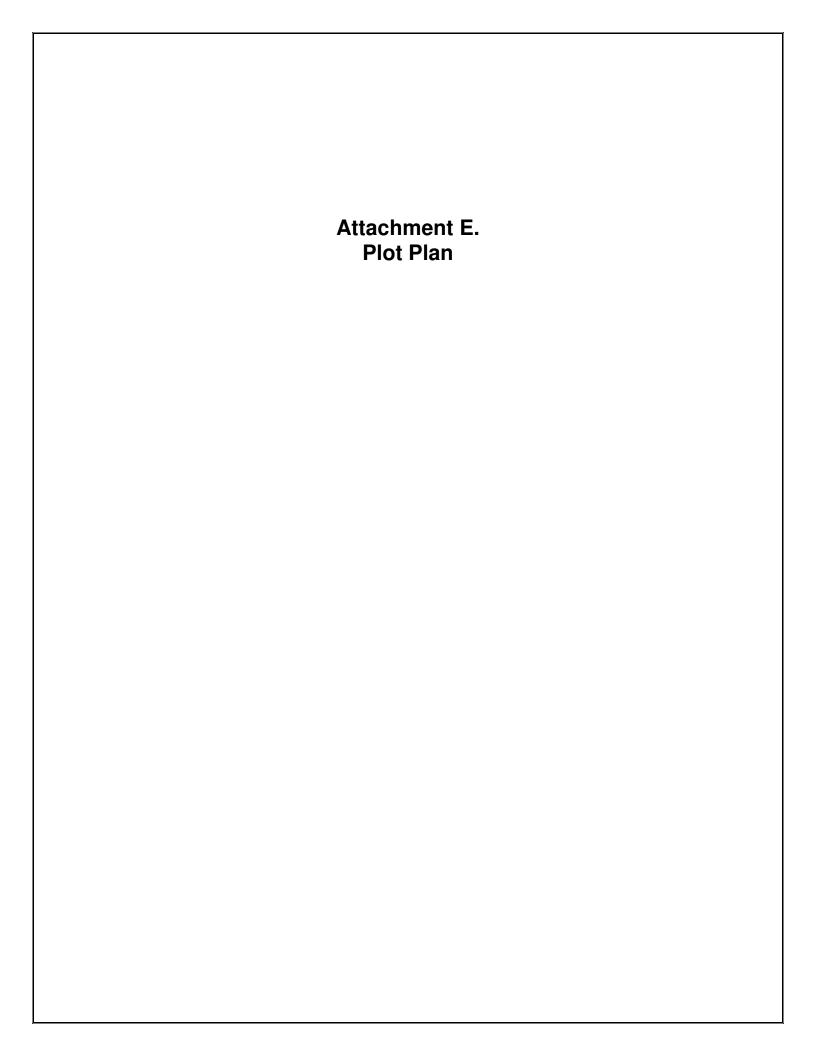
<u>Applicability:</u> Subpart DDDDD applies to process heaters at a major source of HAP emissions (§63.7485). Subpart DDDDD does not apply to the West Mountain Compressor Station as it is not a major source of HAP emissions.

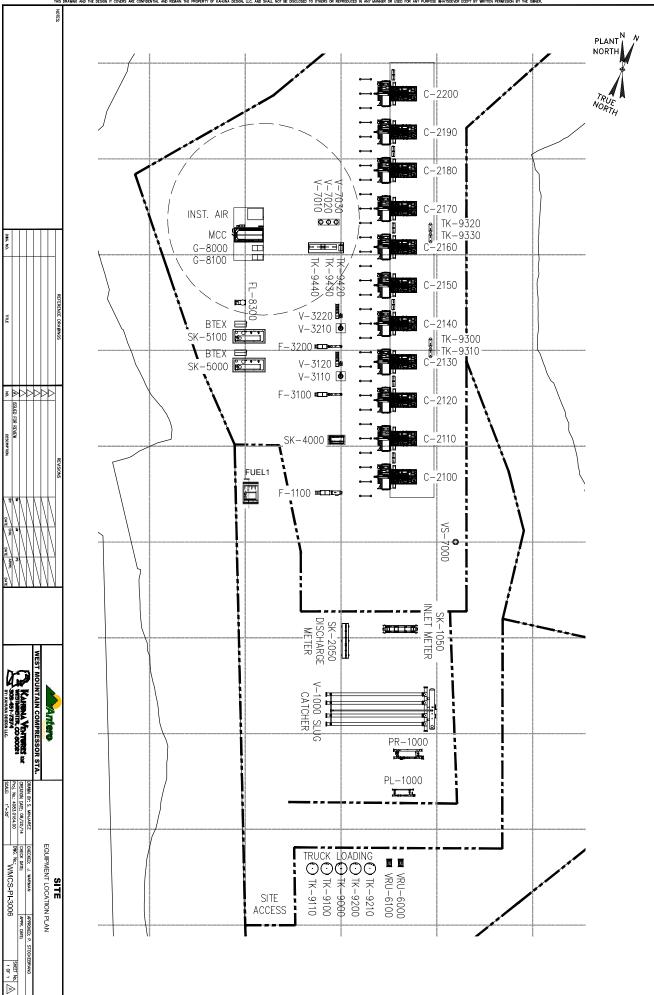
### **West Virginia State Regulations**

## Title 45 Legislative Rule – Division of Environmental Protection, Office of Air Quality

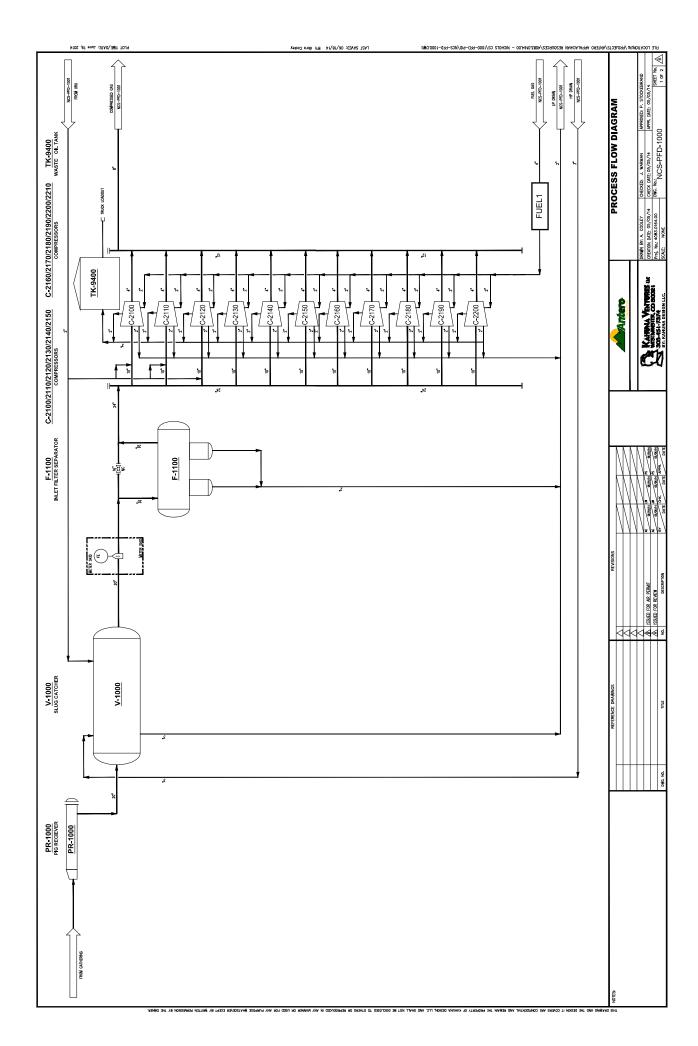
The following Title 45 Legislative Rules will be applicable to the West Mountain Compressor Station:

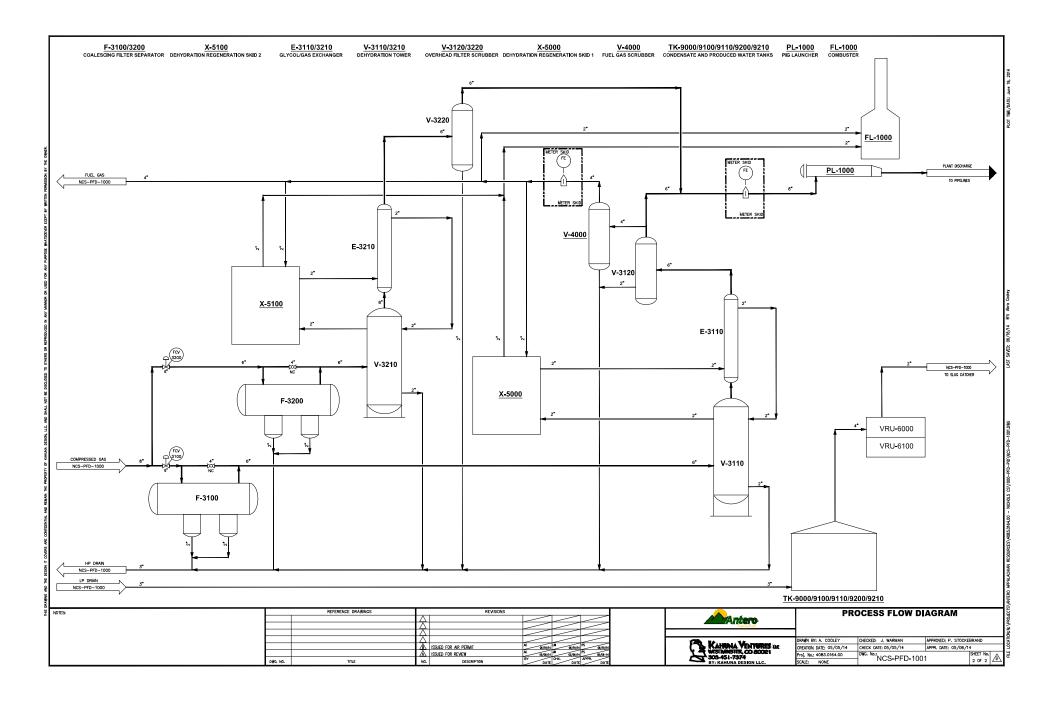
- I. 45CSR2 To Prevent and Control Particulate Air Pollution from Combustion of Fuel in Indirect Heat Exchangers
- II. 45CSR2A Testing, Monitoring, Recordkeeping and Reporting Requirements Under 45CSR2
- III. 45CSR4 To Prevent and Control the Discharge of Air Pollutants into the Open Air Which Causes or Contributes to an Objectionable Odor or Odors
- IV. 45CSR6 Control of Air Pollution from Combustion of Refuse
- V. 45CSR8 Ambient Air Quality Standards
- VI. 45CSR11 Prevention of Air Pollution Emergency Episodes
- VII. 45CSR13 Permits for Construction, Modification, Relocation and Operation of Stationary Sources of Air Pollutants, Notification Requirements, Administrative Updates, Temporary Permits, General Permits, and Procedures for Evaluation
- VIII. 45CSR16 Standards of Performance for New Stationary Sources Pursuant to 40 CFR, Part 60
- IX. 45CSR20 Good Engineering Practice as Applicable to Stack Heights
- X. 45CSR22 Air Quality Management Fee Program
- XI. 45CSR27 To Prevent and Control the Emissions of Toxic Air Pollutants
- XII. 45CSR33 Acid Rain Provisions and Permits
- XIII. 45CSR34 Emission Standards for Hazardous Air Pollutants for Source Categories Pursuant to 40 CFR, Part 63
- XIV. 45CSR38 Provisions for Determination of Compliance with Air Quality Management Rules
- XV. 45CSR42 Greenhouse Gas Emissions Inventory





Attachment F. Process Flow Diagram	





Attachment G. Process Description	

### **West Mountain Compressor Station – Process Description**

The West Mountain Compressor Station is located in Ritchie County, West Virginia. Gas from surrounding pipelines enters the facility through one (1) receiver and associated slug catcher. From there, the gas is metered and routed through a scrubber and filter separator. Any produced liquids from the scrubber or separator are sent to the 500 barrel settling tank (TK-9000). Gas from the filter separator is sent to one (1) of eleven (11) 1,680 hp Waukesha compressor engines (C-2100 - C-2200). The eleven (11) compressor engines are controlled with NSCR catalysts and air-fuel ratio controllers (1C - 11C). Fuel gas for the compressor engines will be treated prior to the engines by a fuel conditioning skid (FUEL1) to allow more complete combustion. Produced fluids are routed to the settling tank and gas goes to one of the two (2) TEG dehydrators.

Each TEG dehydrator (V-3110 & V-3210) contains a flash gas tank and 1.5 MMBtu/hr reboiler. Each dehydrator has a design rate of 72.5 MMscf/day. Within the dehydrator unit, vent gas from the flash gas tank (V-3120 & V-3220) is routed to the reboiler (F-3100 & F-3200) and used as fuel. In the case where the flash tank gas cannot be used by the reboiler due to excess gas or the reboiler being offline, the gas will be sent to the vapor recovery units (VRU-6000 and VRU-6100) via the storage tanks (TK-9000 through TK-9210) and thus controlled by 98%. Combustion emissions from each reboiler are routed to the atmosphere. The dehydrator still vents (V-3110 & V-3210) are controlled by a flare with at least 98% control efficiency (FL-8300). Produced fluids from the dehydrator are routed to the settling tank. The dry gas from the dehydration process is either routed to a fuel gas scrubber, metered, and routed to the fuel conditioning skid for fuel gas or metered and sent to facility discharge.

All produced fluids enter one (1) 500 barrel settling tank (TK-9000) where the fluids settle out as either condensate or produced water. The produced water goes to two (2) 400 barrel produced water tanks (TK-9100 – TK-9110) and the condensate goes to two (2) 400 barrel condensate tanks (TK-9200 – TK-9210). Flashing only occurs at the settling tank as the fluids stabilize in the settling tank before going to the other storage tanks. All five (5) tanks are connected to a primary vapor recovery unit (VRU-6000) where tank vapors are collected and recycled back into the gas system right before the initial filter scrubber. A second vapor recovery unit (VRU-6100) is used as back-up to the primary vapor recovery unit. The produced fluids are trucked out via tanker trucks, as needed (LDOUT1). The loading emissions are uncontrolled. Estimated production is 150 barrels per day of condensate and 45 barrels per day of produced water.

Three (3) natural gas microturbine generators, each rated at 200 kWe, supply power to the facility (G-8000 through G-8200). The fuel line for the generators are heated by a small catalytic heater (CATHT1) with a burner rating of 24,000 Btu/hr.

There are also small storage tanks (1,000 to 2,000 gallons) located at the facility. Their ID number, description, and exact size are listed in the table below.

Fugitive emissions from component leaks and emissions from venting or blowdown events also occur.

Tag Number	Description	Gallons
TK-9300 & TK-9320	Compressor Skid Oily Water Tanks	500 each
TK-9310 & TK-9330	Used Oil Tank	500 each
TK-9400	Compressor Waste Oil Tank	4,200
TK-9410	TEG Make-Up Tank	1,000
TK-9420	Compressor Coolant Tank	2,000
TK-9430	Engine Lube Oil Tank	2,000
TK-9440	Compressor Lube Oil Tank	2,000

Attachment H.  Material Safety Data Sheets		



**Material Name: Produced Water US GHS** 

Produced Brine Water, Brine, Brine Water, Formation Water SYNONYMS:

### \* \* \* Section 1 - PRODUCT AND COMPANY IDENTIFICATION \* \* \*

**Produced Water** (800) 878-1373 PRODUCT NAME: **EMERGENCY PHONE:** Mixture (800) 878-1373 PRODUCT CODES: AFTER HOURS:

PRODUCER: Antero Resources

1615 Wynkoop Street (800) 424-9300 ADDRESS: **CHEMTREC PHONE:** 

Denver, Colorado 80202

### \* \* \* Section 2 - HAZARDS IDENTIFICATION \* \* \*

### **GHS Classification:**

Eye Irritant – Category 2A.

### **GHS LABEL ELEMENTS** Symbol(s)



### Signal Word

Warning

### **Hazard Statements**

Causes serious eye irritation

### **Precautionary Statements**

### **Prevention**

Wear protective gloves/protective clothing/eye protection/face protection.

### Response

If on SKIN (or hair): Rinse skin with water / shower. Remove / Take off all contaminated clothing immediately.

Material Name: Produced Water US GHS

If in EYES: Rinse cautiously with water for at least fifteen (15) minutes. Remove Contact Lenses, if present and easy to do. Continue rinsing.

If EYE irritation persists, get medical advice / attention.

#### **Storage**

Store in a secure area.

## Disposal

Dispose of contents/containers in accordance with regulations.

# \* \* \* Section 3 - COMPOSITION / INFORMATION ON INGREDIENTS \* \* \*

CAS#	Component	Percent
7732-18-5	Water	80
7647-14-5	Sodium Chloride	20

Because brine water is a natural product, composition can vary greatly.

# \* \* \* Section 4 - FIRST AID MEASURES \* \* \*

#### First Aid: Eyes

Flush eyes with clean running water for at least fifteen (15) minutes. If irritation or redness develops from exposure, following flushing, seek medical attention.

#### First Aid: Skin

First aid is not required, normally. However, it is a good practice to wash any chemical from the skin.

#### First Aid: Ingestion (Swallowing)

First aid is not required, normally. If spontaneous vomiting occurs, lean the victim forward to reduce the risk of aspiration. Monitor for breathing difficulties. If symptoms develop, seek medical attention.

## First Aid: Inhalation (Breathing)

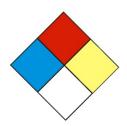
Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

Material Name: Produced Water US GHS

## Most important symptoms and effects

None known or anticipated.

## \* \* \* Section 5 - FIRE FIGHTING MEASURES \* \* \*



#### NFPA 704 Hazard Class

**Health: 1 Flammability: 0 Instability: 0** (0=Minimal, 1=Slight, 2=Moderate, 3=Serious, 4=Severe)

#### **General Fire Hazards**

No fire hazards are expected.

#### **General Fire Hazards**

No unusual fire or explosion hazards are expected. If container is not properly cooled, it can rupture in the heat of a fire.

#### **Extinguishing Media**

The material is non-flammable. Use extinguishing agent suitable for the type of surrounding fire.

## **Unsuitable Extinguishing Media**

None

#### Fire Fighting Equipment / Instructions

Small fires in the beginning stage may typically be extinguished using handheld portable fire extinguishers and other firefighting equipment. Isolate area around container involved in fire and keep unauthorized personnel out. Stop spill/release if it can be done safely. Move undamaged containers from the immediate hazard area if it can be done safely. Cool equipment exposed to fire with water, if it can be done safely.

#### **Hazardous Combustion Products**

None Anticipated. See Section 9 for Flammable Properties including Flash Point and Flammable (Explosive) Limits

Material Name: Produced Water US GHS

# \* \* \* Section 6 - ACCIDENTAL RELEASE MEASURES \* \* \*

#### **Recovery and Neutralization**

Contain and stop the source of the spill, if safe to do so.

# **Materials and Methods for Clean-Up**

Notify relevant authorities in accordance with all applicable regulations. Immediate cleanup of any spill is recommended. Dike far ahead of spill for later recovery or disposal. Absorb spill with inert material such as sand or vermiculite, and place in suitable container for disposal. If spilled on water remove with appropriate methods (e.g. skimming, booms or absorbents). In case of soil contamination, remove contaminated soil for remediation or disposal, in accordance with local regulations.

Recommended measures are based on the most likely spillage scenarios of this material. However, local conditions and regulations may influence or limit the choice of appropriate actions to be taken. See Section 13 for information on appropriate disposal.

# **Emergency Measures**

The material is not considered hazardous. Nevertheless, evacuate nonessential personnel and secure the area. Stay upwind and uphill, if possible.

#### **Personal Precautions and Protective Equipment**

Stay upwind and away from the spill/release. Avoid direct contact with the material. For large spillages, notify persons downstream of the spill/release. Isolate the immediate hazard area and keep unauthorized personnel out. Response and clean-up crews must be properly trained and must utilize proper protective equipment (see Section 8).

#### **Environmental Precautions**

Protect bodies of water by diking or absorbents, if possible. Do not flush down sewer or drainage systems. Use water sparingly to minimize environmental contamination and reduce disposal requirements. If a spill occurs on water, notify appropriate authorities and advise shipping of any hazard.

#### **Prevention of Secondary Hazards**

None

Material Name: Produced Water US GHS

# \* \* \* Section 7 - HANDLING AND STORAGE \* \* \*

#### **Handling Procedures**

Wash thoroughly after handling. Use good personal hygiene practices and wear appropriate personal protective equipment (see section 8).

Do not enter confined spaces such as tanks or pits without following proper entry procedures such as ASTM D-4276 and 29 CFR 1910.146. Do not wear contaminated clothing or shoes.

# **Storage Procedures**

Keep container(s) tightly closed and properly labeled. Use and store this material in cool, dry, well ventilated areas. Store only in approved containers. Keep away from any incompatible material (see Section 10). Protect container(s) against physical damage.

## Incompatibilities

Keep away from excessive heat to prevent rupture of container.

## \* \* \* Section 8 - EXPOSURE CONTROLS / PERSONAL PROTECTION \* \* \*

#### **Component Exposure Limits**

Water (7732-18-5)

ACGIH: Not listed

#### **Sodium Chloride (7647-14-5)**

ACGIH: Not listed

#### **Engineering Measures**

If current ventilation practices are not adequate to maintain airborne concentrations below the established exposure limits, additional engineering controls may be required.

#### Personal Protective Equipment: Respiratory

Emergencies or conditions that could result in significant airborne exposures may require the use of NIOSH approved respiratory protection. An industrial hygienist or other appropriate health and safety professional should be consulted for specific guidance under these situations.

A respiratory protection program that meets or is equivalent to OSHA 29 CFR

Material Name: Produced Water US GHS

1910.134 and ANSI Z88.2 should be followed whenever workplace conditions warrant a respirator's use.

## **Personal Protective Equipment: Skin and Hands**

The use of skin protection is not normally required; however, good industrial hygiene practice suggests the use of gloves or other appropriate skin protection whenever working with chemicals.

#### **Personal Protective Equipment: Eyes**

Safety glasses or goggles that meet or exceed ANSI Z-87.1 are recommended where there is a possibility of splashing or spraying.

# **Hygiene Measures**

Emergency eye wash capability should be available in the near proximity to operations presenting a potential splash exposure. Use good personal hygiene practices. Avoid repeated and/or prolonged skin exposure. Wash hands before eating, drinking, smoking, or using toilet facilities. Promptly remove contaminated clothing and launder before reuse.

## \* \* \* Section 9 - PHYSICAL AND CHEMICAL PROPERTIES \* \* \*

Appearance:	Clear to Brown	Odor:	Salty
Physical State:	Liquid	pH:	ND
Vapor Pressure:	< 0.36 psia @ 70°F / 21.1°C	Vapor Density:	> 1
<b>Boiling Point:</b>	212°F / 100°C	Melting Point:	2.4°F / -16.5°C
Solubility (H2O):	Complete	Specific Gravity:	1.1 @ 68°F / 20°C
<b>Evaporation Rate:</b>	Variable	VOC:	ND
Octanol / H2O Coeff.:	ND	Flash Point:	ND
Flash Point Method:	ND		
Lower Flammability Limit:	ND	Upper Flammability Limit:	ND
(LFL):		(UFL):	
Auto Ignition:	ND	Burning Rate:	ND

Material Name: Produced Water US GHS

## \* \* \* Section 10 - CHEMICAL STABILITY & REACTIVITY INFORMATION \* \* \*

#### **Chemical Stability**

This is a stable material.

#### **Hazardous Reaction Potential**

Will react with alkali and alkaline metals to form flammable hydrogen gas.

#### **Conditions to Avoid**

Avoid contact with alkali metals (lithium, sodium, potassium), alkaline metals (beryllium, magnesium, calcium, strontium, and barium), and metallic hydrides like lithium aluminum hydride.

#### **Hazardous Decomposition Products**

Not anticipated under normal conditions of use.

#### **Hazardous Polymerization**

Not known to occur.

## \* \* \* Section 11 - TOXICOLOGICAL INFORMATION \* \* \*

#### **Acute Toxicity**

#### A: General Product Information

Unlikely to be harmful.

#### B. Component Analysis - D50/LC50

Water (7732-18-5)

Oral LD50 Rat 90 g/kg

## **Sodium Chloride (7647-14-5)**

Oral LD50 Rat 3 g/kg

#### Potential Health Effects: Skin Corrosion Property / Stimulativeness

May cause skin irritation with prolonged or repeated contact. Not expected to be a skin sensitizer.

#### Potential Health Effects: Eye Critical Damage / Stimulativeness

Contact with eyes may cause moderate irritation.

Page 7 of 11

Material Name: Produced Water US GHS

## **Potential Health Effects: Ingestion**

Ingestion may result in nausea, vomiting, diarrhea, abdominal cramps, and dehydration (thirst).

#### Potential Health Effects: Inhalation

No information available on the mixture. However, none of the components have been classified for respiratory sensitization (or are below the concentration threshold for classification).

#### **Generative Cell Mutagenicity**

Not expected to cause genetic effects.

## Carcinogenicity

#### **General Product Information**

Not expected to cause cancer. This substance is not listed as a carcinogen by IARC. NTP or OSHA.

# **Reproductive Toxicity**

This product is not reported to have any reproductive toxicity effects.

#### Specified Target Organ General Toxicity: Single Exposure

This product is not reported to have any specific target organ general toxicity single exposure effects.

#### **Specified Target Organ General Toxicity: Repeated Exposure**

This product is not reported to have any specific target organ general toxicity multiple exposure effects.

#### **Aspiration Respiratory Organs Hazard**

The major health threat of ingestion occurs from the danger of aspiration (breathing) of liquid drops into the lungs, particularly from vomiting. Aspiration may result in chemical pneumonia (fluid in the lungs), severe lung damage, respiratory failure and even death.

## \* \* \* Section 12 - ECOLOGICAL INFORMATION \* \* \*

## **Ecotoxicity**

#### A: General Product Information

Keep out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

Material Name: Produced Water US GHS

## Persistence / Degradability

No information available

#### Bioaccumulation

No information available

## **Mobility in Soil**

No information available

## \* \* \* Section 13 - DISPOSAL CONSIDERATIONS \* \* \*

#### **Waste Disposal Instructions**

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

# **Disposal of Contaminated Containers or Packaging**

Recover or recycle if possible. It is the responsibility of the generator to determine the toxicity and physical properties of the material generated so as to properly classify the waste and ensure disposal methods comply with applicable regulations.

This material, if discarded as produced, is not a RCRA "listed" hazardous waste, and is not believed to exhibit characteristics of hazardous waste. Consult state and local regulations regarding the proper disposal of this material. Do not dispose of brine water by draining onto the ground. This will result in soil and groundwater contamination. Waste arising from spillage or tank cleaning should be disposed of in accordance with applicable regulations.

Container contents should be completely used and containers should be emptied prior to discard. Container rinsate should not be considered a RCRA hazardous waste but must be disposed of with care and in full compliance with federal, state and local regulations. Larger empty containers, such as drums, should be returned to the distributor or to a qualified drum reconditioner. To assure proper disposal of smaller empty containers, consult with state and local regulations and disposal authorities.

#### \* \* \* Section 14 - TRANSPORTATION INFORMATION \* \* \*

**DOT Information** 

Shipping Description: Not Regulated

**UN #:** Not Regulated

Page 9 of 11

Material Name: Produced Water US GHS

## \* \* \* Section 15 - REGULATORY INFORMATION \* \* \*

# CERCLA/SARA – Section 302 Extremely Hazardous Substances and TPQs (in pounds):

This material does not contain any chemicals subject to the reporting requirements of SARA 302 and 40 CFR 372.

## CERCLA/SARA – Section 313 and 40 CFR 372):

This material does not contain any chemicals subject to the reporting requirements of SARA 313 and 40 CFR 372.

#### **EPA (CERCLA) Reportable Quantity (in pounds):**

This material does not contain any chemicals with CERCLA Reportable Quantities.

#### **State Regulations**

#### **Component Analysis**

The following components appear on one or more of the following state hazardous substances list.

#### California Proposition 65:

This material does not contain any chemicals that are known to the State of California to cause cancer, birth defects or other reproductive harm at concentrations that trigger the warning requirements of California Proposition 65.

#### **National Chemical Inventories:**

All components are either listed on the US TSCA Inventory, or are not regulated under TSCA.

# **U.S. Export control classification Number:** EAR99.

# \* \* \* Section 16 - OTHER INFORMATION \* \* \*

#### **NFPA® Hazard Rating**

Health 1
Fire 0
Reactivity0

#### HMIS® Hazard Rating Health 1 Slight

Fire 0 Minimal Physical 0 Minimal

Material Name: Produced Water US GHS

#### Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act: ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

#### **Literature References**

None

#### Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: January 28, 2014

Date of Last Revision: March 4, 2014

End of Sheet



Material Name: Natural Gas Condensate US GHS

SYNONYMS: Drips; Condensate; Field Condensate; Gas Well Condensate; High

Pressure Inlet Liquids; Lease Condensate; Natural Gas Liquids; Pipeline

Liquids

## \* \* \* Section 1 - PRODUCT AND COMPANY IDENTIFICATION \* \* \*

PRODUCT NAME: Natural Gas Condensate EMERGENCY PHONE: (800) 878-1373
PRODUCT CODES: 64741-47-5 AFTER HOURS: (800) 878-1373

PRODUCER: Antero Resources

ADDRESS: 1615 Wynkoop Street CHEMTREC PHONE: (800) 424-9300

Denver, Colorado 80202

## \* \* \* Section 2 - HAZARDS IDENTIFICATION \* \* \*

#### **GHS Classification:**

Flammable Liquids – Category 2.

Acute Toxicity Inhalation - Category 3

Germ Cell Mutagenicity - Category 1B

Carcinogenicity - Category 1A

Specific Target Organ Systemic Toxicity (STOT) – Single Exposure Category 3

Specific Target Organ Systemic Toxicity (STOT) - Repeat Exposure Category 1

Aspiration Toxicity - Category 1

Toxic to the Aquatic Environment Acute – Category 3

# GHS LABEL ELEMENTS

Symbol(s)









Signal Word

Danger

Material Name: Natural Gas Condensate US GHS

#### **Hazard Statements**

Highly flammable liquid and vapor.

Toxic if inhaled.

May cause genetic defects.

May cause cancer.

May cause respiratory irritation.

May cause drowsiness or dizziness.

May cause damage to organs (liver, kidneys, blood, nervous system, and skin) through prolonged or repeated exposure.

May be fatal if swallowed and enters airways.

Harmful to aquatic life.

## **Precautionary Statements**

#### Prevention

Keep away from heat/sparks/open flames/hot surfaces. No smoking.

Keep container tightly closed.

Ground/bond container and receiving equipment.

Use explosion-proof electrical/ventilating/lighting equipment.

Use only non-sparking tools.

Take precautionary measures against static discharge.

Wear protective gloves/protective clothing/eye protection/face protection.

Do not breathe gas/mist/vapors/spray.

Do not handle until all safety precautions have been read and understood.

Wash thoroughly after handling.

Do not eat, drink or smoke when using this product.

Use only outdoors or in a well-ventilated area.

Avoid release to the environment.

#### Response

If on SKIN (or hair): Wash with plenty of soap and water. Remove / Take off all contaminated clothing immediately. Rinse skin with water/shower.

If INHALED: Remove victim to fresh air and keep comfortable for breathing. Call a poison center/doctor if the victim feels unwell.

If SWALLOWED: Immediately call a poison center or doctor / physician. Do not Induce vomiting.

If exposed or concerned: Get medical advice/attention.

In case of fire: Use water spray, fog or fire-fighting foam.

#### **Storage**

Store in a well-ventilated place. Keep cool.

Store in a secure area.

Material Name: Natural Gas Condensate US GHS

## Disposal

Dispose of contents/containers in accordance with local/regional/national/international regulations.

## \* \* \* Section 3 - COMPOSITION / INFORMATION ON INGREDIENTS \* \* \*

CAS#	Component	Percent
111-65-9	Octanes	25 - 95
142-82-5	Heptanes	25 - 95
110-54-3	Hexanes as n-Hexane	25 - 95
109-66-0	Pentanes as n-Pentane	5 - 70
106-97-8	N-butane	0 - 45
74-98-6	Propane	0 - 15
78-84-0	Ethane	0 - 5
71-43-2	Benzene	< 1
108-88-3	Toluene	< 1
1330-20-7	m-,o-,p-Xylene	< 1

Because natural gas condensate is a natural product, composition can vary greatly.

## \* \* \* Section 4 - FIRST AID MEASURES \* \* \*

#### First Aid: Eyes

Flush eyes with clean running water for at least fifteen (15) minutes. Following flushing, seek medical attention.

#### First Aid: Skin

Remove contaminated clothing. Wash contaminated areas thoroughly with soap and water or waterless hand cleanser. Obtain medical attention if irritation or redness develops. Wash contaminated clothing before reuse.

#### First Aid: Ingestion (swallowing)

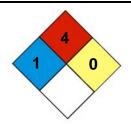
DO NOT INDUCE VOMITING. Do not give liquids. Obtain immediate medical attention. If spontaneous vomiting occurs, lean the victim forward to reduce the risk of aspiration. Monitor for breathing difficulties. Small amounts of material which enter the mouth should be rinsed out until the taste is dissipated.

Material Name: Natural Gas Condensate US GHS

## First Aid: Inhalation (breathing)

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

## \* \* \* Section 5 – FIRE FIGHTING MEASURES \* \* \*



#### **NFPA 704 Hazard Class**

**Health:** 1 **Flammability:** 4 **Instability:** 0 (0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

#### **General Fire Hazards**

See Section 9 for Flammability Properties.

Extremely flammable. Vapors may be ignited rapidly when exposed to heat, spark, open flame, or other source of ignition (e.g., static electricity, pilot lights, mechanical / electrical equipment, and electronic devices such as cell phones, computers, calculators, and pagers which have not been certified as intrinsically safe). Flammable vapors can burn in the open or explode in confined spaces. Vapors are heavier than air, and may travel distances to an ignition source and flash back. Runoff to sewer systems may cause fire or explosion.

#### **Hazardous Combustion Products**

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

#### **Extinguishing Media**

SMALL FIRES: Any extinguisher suitable for Class B fires, dry chemical, firefighting foam, water spray, carbon dioxide ( $CO_2$ ), or other gaseous extinguishing agents. Use caution when applying  $CO_2$  in confined spaces.

LARGE FIRES: Water spray, fog or fire-fighting foam. Water may be ineffective for fighting the fire, but may be used to cool fire-exposed containers.

## **Unsuitable Extinguishing Media**

None

Material Name: Natural Gas Condensate US GHS

#### **Fire Fighting Equipment / Instructions**

Small fires in the beginning stage may typically be extinguished using handheld portable fire extinguishers and other firefighting equipment. Isolate area around container involved in fire. Cool tanks, shells, and containers exposed to fire and excessive heat with water. For massive fires the use of unmanned hose holders or monitor nozzles may be advantageous to minimize personnel exposure. Major fires may require withdrawal, allowing the tank to burn. Large storage tank fires typically require specially trained personnel and equipment to extinguish the fire, often including the need for properly applied firefighting foam.

Firefighting activities that may result in potential exposure to high heat, smoke or toxic by-products of combustion should require NIOSH/MSHA- approved pressure-demand self-contained breathing apparatus with full face piece and full protective clothing.

# \* \* \* Section 6 - ACCIDENTAL RELEASE MEASURES \* \* \*

#### Recovery and Neutralization

Contain and stop the source of the spill, if safe to do so.

#### **Materials and Methods for Clean-Up**

Notify relevant authorities in accordance with all applicable regulations. Immediate cleanup of any spill is recommended. Dike far ahead of spill for later recovery or disposal. Absorb spill with inert material such as sand or vermiculite, and place in suitable container for disposal. If spilled on water remove with appropriate methods (e.g. skimming, booms or absorbents). In case of soil contamination, remove contaminated soil for remediation or disposal, in accordance with local regulations.

Recommended measures are based on the most likely spillage scenarios for this material; however local conditions and regulations may influence or limit the choice of appropriate actions to be taken.

## **Emergency Measures**

Evacuate nonessential personnel and secure all ignition sources. No road flares, smoking or flames in hazard area. Consider wind direction. Stay upwind and uphill, if possible. Vapor cloud may be white, but color will dissipate as cloud disperses. Fire and explosion hazard is still present.

#### **Personal Precautions and Protective Equipment**

Response and clean-up crews must be properly trained and must utilize proper protective equipment (see Section 8). Extremely flammable. Spillages of liquid product will create a fire hazard and may form an explosive atmosphere. Keep all sources of

#### Material Name: Natural Gas Condensate

**US GHS** 

ignition and hot metal surfaces away from spill/release if safe to do so.

The use of explosion-proof electrical equipment is recommended. Stay upwind and away from spill/release. Avoid direct contact with material. For large spillages, notify persons downwind of the spill/release, isolate immediate hazard area and keep unauthorized personnel out. Wear appropriate protective equipment, including respiratory protection, as conditions warrant (see Section 8). See Sections 2 and 7 for additional information on hazards and precautionary measures.

#### **Environmental Precautions**

Protect bodies of water by diking, absorbents, or absorbent boom, if possible. Do not flush down sewer or drainage systems, unless system is designed and permitted to handle such material. The use of firefighting foam may be useful in certain situations to reduce vapors. If spill occurs on water notify appropriate authorities and advise shipping of any hazard. Spills into or upon navigable waters, the contiguous zone, or adjoining shorelines that cause a sheen or discoloration on the surface of the water, may require notification of the National Response Center (phone number 800-424-8802).

## **Prevention of Secondary Hazards**

None

# \* \* \* Section 7 - HANDLING AND STORAGE \* \* \*

# **Handling Procedures**

Keep away from flame, sparks and excessive temperatures. Bond and ground containers. Use non-sparking tools. Use only outdoors or in well ventilated areas. Wear protective gloves / clothing and eye / face protection. Wash thoroughly after handling. Use good personal hygiene practices and wear appropriate personal protective equipment (see section 8).

#### **Storage Procedures**

Store only in approved containers. Bond and ground containers. Keep away from flame, sparks, excessive temperatures and open flames. Keep containers closed and clearly labeled. Empty product containers or vessels may contain explosive vapors. Do not pressurize, cut, heat, weld or expose containers to sources of ignition.

Store in a well-ventilated area. This storage area should comply with NFPA 30 "Flammable and Combustible Liquid Code". Avoid storage near incompatible materials. The cleaning of tanks previously containing this product should follow API Recommended Practice (RP) 2013 "Cleaning Mobile Tanks In Flammable and Combustible Liquid Service" and API RP 2015 "Cleaning Petroleum Storage Tanks."

Material Name: Natural Gas Condensate US GHS

## **Incompatibilities**

Keep away from strong oxidizers, ignition sources and heat.

# \* \* \* Section 8 - EXPOSURE CONTROLS / PERSONAL PROTECTION \* \* \*

# **Component Exposure Limits**

# Octanes (111-65-9)

ACGIH: 300 ppm TWA (listed under Octane, all isomers)

## Heptanes (142-82-5)

ACGIH: 400 ppm TWA (listed under n-Heptane)

# n-Hexane (110-54-3)

ACGIH: 20 ppm TWA (listed under n-Hexane)

#### n-Pentane (109-66-0)

ACGIH: 600 ppm TWA (listed under Pentane, all isomers)

#### n-Butane (106-97-8)

ACGIH: 600 ppm TWA (listed under n-Butane)

#### **Propane (74-98-6)**

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases C1-C4)

#### Ethane (74-84-0)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases C1-C4)

#### Benzene (71-43-2)

ACGIH: 0.5 ppm (TWA); NIOSH: 0.1 ppm (TWA); OSHA 1 ppm (TWA)

#### Toluene (108-88-3)

ACGIH: 20 ppm TWA (listed under Toluene)

#### m-, o-, p-Xylene (1330-20-7)

ACGIH: 100 ppm TWA (listed under Xylene o, m & p isomers)

Material Name: Natural Gas Condensate US GHS

#### **Engineering Measures**

Use adequate ventilation to keep vapor concentrations of this product below occupational exposure and flammability limits, particularly in confined spaces. Use explosion-proof equipment and lighting in classified / controlled areas.

#### **Personal Protective Equipment: Respiratory**

Use a NIOSH-approved positive-pressure, supplied air respirator with escape bottle or self-contained breathing apparatus (SCBA) for gas concentrations above occupational exposure limits, for potential for uncontrolled release, if exposure levels are not known, or in an oxygen-deficient atmosphere (oxygen content less than 19.5 percent). A respiratory program that meets or is equivalent to OSHA 29 CFR 1910.134 and ANSI Z88.2 should be followed whenever workplace conditions warrant the use of a respirator.

If benzene concentrations equal or exceed applicable exposure limits, OSHA requirements for personal protective equipment, exposure monitoring, and training may apply (29 CFR 1910.1028 – Benzene).

CAUTION: Flammability limits (i.e., explosion hazard should be considered when assessing the need to expose personnel to concentrations requiring respiratory protection.

#### **Personal Protective Equipment: Hands**

Gloves constructed of nitrile or neoprene are recommended.

## **Personal Protective Equipment: Eyes**

Safety glasses or goggles are recommended where there is a possibility of splashing or spraying. Eye protection that meets or exceeds ANSI Z.87.1 is recommended. Depending on conditions of use, a face shield may be necessary.

#### Personal Protective Equipment: Skin and Body

Chemical protective clothing such as of E.I. DuPont TyChem®, Saranex® or equivalent recommended based on degree of exposure. Note: The resistance of specific material may vary from product to product as well as with degree of exposure. Consult manufacturer specifications for further information.

## **Hygiene Measures**

Emergency eye wash capability should be available in the near proximity to operations presenting a potential splash exposure. Use good personal hygiene practices. Avoid repeated and/or prolonged skin exposure. Wash hands before eating, drinking, smoking, or using toilet facilities. Do not use as a cleaning solvent on the skin. Do not use gasoline or solvents (naphtha, kerosene, etc.) for washing this product from

Material Name: Natural Gas Condensate

**US GHS** 

exposed skin areas. Waterless hand cleaners are effective. Promptly remove contaminated clothing and launder before reuse. Use care when laundering to prevent the formation of flammable vapors which could ignite via washer or dryer. Consider the need to discard contaminated leather shoes and gloves.

#### \* \* \* Section 9 - PHYSICAL AND CHEMICAL PROPERTIES \* \* \*

**Appearance:** Colorless to straw yellow **Odor:** Aromatic, Gasoline;

Physical State: Liquid pH: ND

Vapor Pressure: 110 - 200 psia (Reid VP) Vapor Density (air = 1): > 1 @  $100^{\circ}\text{F}/37.8^{\circ}\text{C}$ 

**Boiling Point:** Approx. 85 - 437°F **Melting Point:** ND

(39 – 200°C)

Solubility (H2O): Insoluble to slightly Specific Gravity: AP 0.62-0.76 (varies)

soluble

Evaporation Rate:HighVOC:NDOctanol / H2O Coeff.:NDFlash Point:-40°F

-40°C

Flash Point Method: Tag Closed Cup (TCC)

Lower Flammability Limit: ND (NFPA Gasoline 1.4) Upper Flammability Limit: ND (NFPA Gasoline 7.6)

(LFL): (UFL):

Auto Ignition: AP 480°F (250°C) Burning Rate: ND

## \* \* \* Section 10 - CHEMICAL STABILITY & REACTIVITY INFORMATION \* \* \*

#### **Chemical Stability**

This is a stable material.

#### **Hazardous Reaction Potential**

Will not occur.

#### **Conditions to Avoid**

Keep away from ignition sources and high temperatures.

#### **Hazardous Decomposition Products**

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

Material Name: Natural Gas Condensate US GHS

# \* \* \* Section 11 - TOXICOLOGICAL INFORMATION \* \* \*

#### **Acute Toxicity**

#### A: General Product Information

Harmful if swallowed.

#### B. Component Analysis - LD50/LC50

#### Octanes (111-65-9)

Inhalation LC50 rat = 118,000 mg/m3 / 4H

#### **Heptanes (142-82-5)**

Inhalation LC50 rat = 103,000 mg/m3 / 4H

#### Hexanes as n-Hexane (110-53-3)

Inhalation LC50 rat = 48,000 ppm / 4H

## Pentanes as n-Pentane (109-66-0)

Inhalation LC50 rat = 364,000 mg/m3 / 4H

#### Butanes as n-Butane (106-97-8)

Inhalation LC50 rat 658,000 mg/l / 4H

#### **Propane (74-98-6)**

Inhalation LC50 Rat > 800,000 ppm / 0.25H

#### Ethane (74-84-0)

Inhalation LC50 Rat 658,000 mg/l / 4H

#### Benzene (71-43-2)

Inhalation LC50 Rat 44,700 mg/m3 /

#### Toluene (108-88-3)

Inhalation LD50 Rat 12/5 mg/l / 4H

#### m-, o-, p-Xylene (1330-20-7)

Inhalation LC50 Rat 5000 ppm / 4H

#### Potential Health Effects: Skin Corrosion Property / Stimulativeness

May cause skin irritation with prolonged or repeated contact. Liquid may be absorbed through the skin in toxic amounts if large areas of skin are exposed repeatedly.

Material Name: Natural Gas Condensate US GHS

#### Potential Health Effects: Eye Critical Damage / Stimulativeness

Contact with eyes may cause moderate irritation.

#### Potential Health Effects: Ingestion (swallowing)

Ingestion may cause gastrointestinal disturbances, including irritation, nausea, vomiting and diarrhea, and central nervous system (brain) effects similar to alcohol intoxication. In severe cases, tremors, convulsions, loss of consciousness, coma, respiratory arrest, and death may occur.

# Potential Health Effects: Inhalation (breathing)

Excessive exposure may cause irritations to the nose, throat, lungs and respiratory tract. Central nervous system (brain) effects may include headache, dizziness, loss of balance and coordination, unconsciousness, coma, respiratory failure, and death.

## **Respiratory Organs Sensitization / Skin Sensitization**

This product is not reported to have any skin sensitization effects.

#### **Generative Cell Mutagenicity**

May cause genetic defects. Some crude oils and crude oil fractions have been positive in mutagenicity studies.

#### Carcinogenicity

#### A: General Product Information

May cause cancer.

This product contains benzene, although at very low concentrations. Human health studies indicate that prolonged and/or repeated overexposure to benzene may cause damage to the blood-forming system (particularly bone marrow), and serious blood disorders such as aplastic anemia and leukemia. Benzene is listed as a human carcinogen by the NTP, IARC, OSHA and ACGIH.

Exposure to light hydrocarbons in the same boiling range as this product have been associated in animal studies with effects to the central nervous system, peripheral nervous system, liver, and kidneys. The significance of these animal models to predict similar human response is uncertain. Observing good work practices and personal hygiene procedures (Sections 7 and 8) can minimize potential risks to humans.

# **B: Component Carcinogenicity**

Benzene (71-43-2)

ACGIH: A1 - Confirmed Human Carcinogen

OSHA: 5 ppm STEL (Cancer hazard, Flammable, See 29 CFR 1910.1028,

15 min); 0.5 ppm Action Level; 1 ppm TWA

NIOSH: potential occupational carcinogen

NTP: Known Human Carcinogen (Select Carcinogen)

Page 11 of 17

Material Name: Natural Gas Condensate US GHS

IARC: Monograph 100F [in preparation]; Supplement 7 [1987]; Monograph

29 [1982] (Group 1 (carcinogenic to humans))

## **Reproductive Toxicity**

This product is not reported to have any reproductive toxicity effects.

#### **Specified Target Organ General Toxicity: Single Exposure**

This product is not reported to have any specific target organ general toxicity single exposure effects.

# **Specified Target Organ General Toxicity: Repeated Exposure**

May cause damage to organs (liver, kidneys, blood, nervous system and skin) through prolonged or repeated exposure.

#### **Aspiration Respiratory Organs Hazard**

The major health threat of ingestion occurs from the danger of aspiration (breathing) of liquid drops into the lungs, particularly from vomiting. Aspiration may result in chemical pneumonia (fluid in the lungs), severe lung damage, respiratory failure and even death.

# \* \* \* Section 12 - ECOLOGICAL INFORMATION \* \* \*

#### **Ecotoxicity**

#### A: General Product Information

Keep out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

# B: Component Analysis – Ecotoxicity – Aquatic Toxicity Benzene (71-43-2)

Test and Species	Conditions
96 Hr LC50 Pimephales promelas	10.7-14.7 mg/L [flow-through]
96 Hr LC50 Oncorhynchus mykiss	5.3 mg/L [flow-through]
96 Hr LC50 Lepomis macrochirus	22.49 mg/L [static]
96 Hr LC50 Poecilia reticulata	28.6 mg/L [static]
96 Hr LC50 Pimephales promelas	22330-41160 µg/L [static]
96 Hr LC50 Lepomis macrochirus	70000-142000 μg/L [static]
72 Hr EC50 Pseudokirchneriella subcapitata	29 mg/L
48 Hr EC50 Daphnia magna	8.76 - 15.6 mg/L [static]
48 Hr EC50 Daphnia magna	10 mg/L

Material Name: Natural Gas Condensate US GHS

## Natural Gas condensates (68919-39-1)

Test and Species

96 Hr LC50 Alburnus alburnus

96 Hr LC50 Cyprinodon variegatus

72 Hr EC50 Pseudokirchneriella

24 b applieds

56 mg/L

subcapitata 30 mg/L 24 Hr EC50 Daphnia magna 170 mg/L

#### Persistence / Degradability

No information available

#### **Bioaccumulation**

No information available

# **Mobility in Soil**

No information available

#### \* \* \* Section 13 - DISPOSAL CONSIDERATIONS \* \* \*

# **Waste Disposal Instructions**

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

## **Disposal of Contaminated Containers or Packaging**

Recover or recycle if possible. It is the responsibility of the generator to determine the toxicity and physical properties of the material generated so as to properly classify the waste and ensure disposal methods comply with applicable regulations. This material, if discarded should be fully characterized for ignitability (D001), reactivity (D003) and benzene (D018) prior to disposal (40 CFR261). Use which results in chemical or physical change or contamination may subject it to regulation as a hazardous waste. Along with properly characterizing all waste materials, consult state and local regulations regarding the proper disposal of this material. Do not dispose of by draining onto the ground. This will result in soil and groundwater contamination. Waste arising from spillage or tank cleaning should be disposed of in accordance with applicable regulations.

Container contents should be completely used and containers should be emptied prior to discard. Container rinsate could be considered a RCRA hazardous waste and must be disposed of with care and in full compliance with federal, state and local regulations. Larger empty containers, such as drums, should be returned to the distributor or to a qualified drum reconditioner. To assure proper disposal of smaller empty containers, consult with state and local regulations and disposal authorities.

Material Name: Natural Gas Condensate US GHS

#### \* \* \* Section 14 - TRANSPORTATION INFORMATION \* \* \*

#### **DOT Information**

**Shipping Name:** Petroleum Products, n.o.s. (condensate)

**UN #: 1268 Hazard Class: 3** 

**Additional Info.:** Dependent on the product's properties, the shipper may also elect to classify as Gasoline UN1203 or Petroleum Crude Oil UN1267 - reference 49 CFR

172.101 for further description (e.g., packing group determination).

Placard:



#### \* \* \* Section 15 - REGULATORY INFORMATION \* \* \*

# **Regulatory Information**

# **Component Analysis**

This material contains one or more of the following chemicals required to be identified under SARA Section 302 (40 CFR 355 Appendix A), SARA Section 313 (40 CFR 372.65) and/or CERCLA (40 CFR 302.4).

#### Benzene (71-43-2)

SARA 313: 0.1% de minimis concentration

CERCLA: 10 lb final RQ (received an adjusted RQ of 10 lbs based on

potential carcinogenicity in an August 14, 1989 final rule); 4.54 kg final RQ (received an adjusted RQ of 10 lbs based on potential

carcinogenicity in an August 14, 1989 final rule)

#### SARA Section 311/312 – Hazard Classes

Acute Health X X Sudden Release of Pressure Reactive X -- Reactive

#### SARA SECTION 313 – SUPPLIER NOTIFICATION

This product contains the following toxic chemicals subject to the reporting requirements of section 313 of the Emergency Planning and Community Right-To-Know Act (EPCRA) of 1986 and of 40 CFR 372:

Material Name: Natural Gas Condensate **US GHS** 

**CONCENTRATION PERCENT BY WEIGHT INGREDIENT NAME (CAS NUMBER)** 

Benzene (71-43-2) <0.1 to 2

**Canadian Regulatory Information** 

This product has been classified in accordance with the hazard criteria of the DSL/NDSL

Controlled Products Regulations (CPR) and the SDS contains all the Inventory

information required by the Regulations.

Workplace B2 - Flammable Liquid

Hazardous D1A – Material Causing Immediate and Serious Toxic Effects - Very Toxic

Materials Material

Information D2A: Material Causing Other Toxic Effects Very Toxic D2B - Material Causing Other Toxic Effects - Toxic Material System

**European Union Regulatory Information** 

Product is dangerous as defined by the European Union Dangerous

Substances / Preparations Directives. Labeling

Contains: Low Boiling Point Naphtha

**F+** Extremely Flammable

**T** Toxic Symbol

**N** Dangerous for the Environment

R12-45-38-65-67-51/53

Extremely flammable. May cause cancer. Irritating to skin. Harmful: may cause lung damage if swallowed. Vapors may cause drowsiness

**Risk Phrases** and dizziness. Toxic to aquatic organisms, may cause long-term

adverse effects in the aquatic environment.

S16-53-45-2-23-24-29-43-62

Keep away from sources of ignition – No smoking. Avoid exposure – obtain special instructions before use. In case of accident or if you feel

unwell, seek medical advice immediately (show the label where

possible). Keep out of reach of children. Do not breathe vapor. Avoid

contact with skin. Do not empty into drains. In case of fire use foam/dry powder/CO2. If swallowed, do not induce vomiting: seek

medical advice immediately and show this container or label.

Safety

**Phrases** 

Material Name: Natural Gas Condensate US GHS

# **State Regulations**

#### **Component Analysis - State**

The following components appear on one or more of the following state hazardous substances lists

Component	CAS	CA	MA	MN	NJ	РА	RI
Octanes	111-65-9	Yes	No	Yes	Yes	Yes	Yes
Heptanes	142-82-5	Yes	No	Yes	Yes	Yes	Yes
n-Hexane	110-54-3	Yes	Yes	Yes	Yes	Yes	Yes
n-Pentane	109-66-0	Yes	No	Yes	Yes	Yes	Yes
n-Butane	106-97-8	Yes	No	Yes	Yes	Yes	Yes
Propane	74-98-6	No	No	Yes	Yes	Yes	Yes
Ethane	78-84-0	No	No	Yes	Yes	Yes	No
Benzene	71-43-2	Yes	Yes	Yes	Yes	Yes	Yes
Toluene	108-88-3	Yes	Yes	Yes	Yes	Yes	Yes
m-, o-, p-Xylene	1330-20-7	Yes	Yes	Yes	Yes	Yes	Yes

The following statement(s) are provided under the California Safe Drinking Water and Toxic Enforcement Act of 1986 (Proposition 65):

WARNING! This product contains a chemical known to the state of California to cause cancer.

WARNING! This product contains a chemical known to the state of California to cause Reproductive / developmental effects.

#### Component Analysis - WHMIS IDL

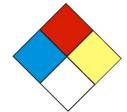
The following components are identified under the Canadian Hazardous Products Act Ingredient Disclosure List:

Component	CAS#	Minimum Concentration
Benzene	71-43-2	0.1%

* * * Section 16 - OTHER INFORMATION * * *	

NFPA® Hazard Rating Health 1

Fire 4 Reactivity 0



**HMIS**® **Hazard Rating** Health 1 Slight

Fire 4 Severe
Physical 0 Minimal

\* Chronic

Material Name: Natural Gas Condensate US GHS

#### Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act: ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

#### **Literature References**

None

#### Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: January 29, 2014

Date of Last Revision: March 4, 2014

End of Sheet



**Material Name: Wet Field Natural Gas** 

SYNONYMS: CNG, Natural Gas, Methane.

# \* \* \* Section 1 - PRODUCT AND COMPANY IDENTIFICATION \* \* \*

PRODUCT NAME: Wet Field Natural Gas EMERGENCY PHONE: (800) 878-1373
PRODUCT CODES: CAS Reg. No. 68410-63-9 AFTER HOURS: (800) 878-1373

PRODUCER: Antero Resources

ADDRESS: 1615 Wynkoop Street CHEMTREC PHONE: (800) 424-9300

Denver, Colorado 80202

#### \* \* \* Section 2 - HAZARDS IDENTIFICATION \* \* \*

#### **GHS Classification:**

Flammable Gas – Category 1.

Gases Under Pressure - Gas.

Specific Target Organ Systemic Toxicity (STOT) – Single Exposure Category 2.

# GHS LABEL ELEMENTS









#### **Signal Word**

Danger

#### **Hazard Statements**

Extremely flammable gas.

Contains gas under pressure, may explode if heated.

May cause damage to central nervous and respiratory systems.

#### **Precautionary Statements**

#### Prevention

Keep away from heat/sparks/open flames/hot surfaces. No smoking.

Do not breathe fume/gas/mist/vapors/spray.

Wash thoroughly after handling.

Do not eat, drink or smoke when using this product.

Material Name: Wet Field Natural Gas

#### Response

Leaking gas fire: Do not extinguish, unless leak can be stopped safely. Eliminate all ignition sources if safe to do so.

If exposed to gas, or concerned about possible exposure: Call a POISON CENTER or doctor/physician.

#### Storage

Protect from sunlight. Store in a well-ventilated place.

Store in a secure area.

#### Disposal

Dispose of contents/containers in accordance with local/regional/national/international regulations.

# \* \* \* Section 3 - COMPOSITION / INFORMATION ON INGREDIENTS \* \* \*

CAS#	Component	Percent
74-82-8	Methane	72 - 97
78-84-0	Ethane	2.2 - 14
74-98-6	Propane	0.0 - 8.0
106-97-8	Butanes	0.0 - 3.5
109-66-0	Pentanes	0.0 - 1.4
110-54-3	Hexanes	0.0 - 0.5
7727-37-9	Nitrogen	< 0.4
124-38-9	Carbon Dioxide	< 0.2
7782-44-7	Oxygen	< 0.04

Because natural gas is a natural product, composition can vary greatly.

## \* \* \* Section 4 - FIRST AID MEASURES \* \* \*

#### First Aid: Eyes

In case of freeze burn, cover eyes to protect from light. Flush eyes with running water for at least fifteen (15) minutes. Following flushing, seek medical attention.

#### First Aid: Skin

Remove contaminated clothing. In case of blistering, frostbite or freeze burns, seek immediate medical attention.

Material Name: Wet Field Natural Gas

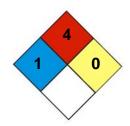
#### First Aid: Ingestion

Risk of ingestion is extremely low. However, if oral exposure occurs, seek immediate medical assistance.

#### First Aid: Inhalation

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

## \* \* \* Section 5 - FIRE FIGHTING MEASURES \* \* \*



#### **NFPA 704 Hazard Class**

Health: **1** Flammability: **4** Instability: **0** (0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

#### **General Fire Hazards**

See Section 9 for Flammability Properties.

Forms a flammable mixture with air. If released, the resulting vapors will disperse with the prevailing wind. If a source of ignition is present where the vapor exists at a 5 – 15% concentration in air, the vapor will burn along the flame front toward the source of the fuel.

## **Hazardous Combustion Products**

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

#### **Extinguishing Media**

Any extinguisher suitable for Class B fires, dry chemical, firefighting foam, CO2, and other gaseous agents. However, fire should not be extinguished unless flow of gas can be immediately stopped.

#### **Unsuitable Extinguishing Media**

None.

#### Fire Fighting Equipment / Instructions

Gas fires should not be extinguished unless flow of gas can be immediately stopped. Shut off gas source and allow gas to burn out. If spill or leak has not ignited, determine

Material Name: Wet Field Natural Gas

if water spray may assist in dispersing gas or vapor to protect personnel attempting to stop leak. Use water to cool equipment, surfaces and piping exposed to fire and excessive heat. For large fire, the use of unmanned hose holders or monitor nozzles may be advantageous to further minimize personnel exposure. Isolate area, particularly around piping. Let the fire burn unless leak can be stopped. Concentrate fire-fighting efforts on objects / materials ignited by the initial fire. Withdraw immediately in the event of a rising sound from a venting safety device.

Firefighting activities that may result in potential exposure to high heat, smoke or toxic by-products of combustion should require NIOSH-approved pressure-demand self-contained breathing apparatus with full facepiece and full protective clothing.

## \* \* \* Section 6 - ACCIDENTAL RELEASE MEASURES \* \* \*

#### Recovery and Neutralization

Stop the source of the release, if safe to do so.

#### **Materials and Methods for Clean-Up**

Consider the use of water spray to disperse gas vapors. Do not use water spray to direct gas vapors toward sewer or drainage systems. Isolate the area until gas has dispersed. Ventilate and gas test area before entering.

#### **Emergency Measures**

Evacuate nonessential personnel and secure all ignition sources. No road flares, smoking or flames in hazard area. Consider wind direction. Stay upwind and uphill, if possible. Vapor cloud may be white, but color will dissipate as cloud disperses. Fire and explosion hazard is still present.

#### **Personal Precautions and Protective Equipment**

Cooling effect of expanding gas from leak may present frostbite / freeze burn hazard. Wear flame retardant (FR) clothing around un-ignited leak. Wear fire protective clothing around an active fire.

#### **Environmental Precautions**

Do not flush gas vapors toward sewer or drainage systems.

## **Prevention of Secondary Hazards**

None.

Material Name: Wet Field Natural Gas

## \* \* \* Section 7 – HANDLING AND STORAGE \* \* \*

## **Handling Procedures**

Keep away from flame, sparks and excessive temperatures. Bond and ground containers. Use only in well ventilated areas.

## **Storage Procedures**

Natural gas will be contained in the pipeline. Keep away from flame, sparks, excessive temperatures and open flames. Empty pipeline segments may contain explosive residues from natural gas liquids. Do not cut, heat, weld or expose containers to sources of ignition sections of pipeline unless the sections have been purged of natural gas residues.

#### **Incompatibilities**

Keep away from strong oxidizers, ignition sources and heat.

# \* \* \* Section 8 - EXPOSURE CONTROLS / PERSONAL PROTECTION \* \* \*

#### **Component Exposure Limits**

#### Methane (74-82-8)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases: Alkane C1-4)

#### Ethane (74-84-0)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases: Alkane C1-4)

#### **Propane (74-98-6)**

ACGIH: 2500 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

#### **Butane (106-97-8)**

ACGIH: 800 ppm TWA (listed under Aliphatic hydrocarbon gases: Alkane C1-4)

## Pentanes (109-66-0)

ACGIH: 600 ppm TWA (listed under Pentane, all isomers)

#### Hexanes (110-54-3)

ACGIH: 50 ppm TWA (listed under n-Hexane)

Material Name: Wet Field Natural Gas

Nitrogen (7727-37-9)

Simple Asphyxiant

Carbon Dioxide (124-38-9)

ACGIH: 5000 ppm TWA (listed under Carbon Dioxide)

Oxygen (7782-44-7)

N/A – Necessary for life

## **Engineering Measures**

Use adequate ventilation to keep gas and vapor concentrations of this product below occupational exposure and flammability limits, particularly in confined spaces. Use explosion-proof equipment and lighting in classified / controlled areas.

# **Personal Protective Equipment: Respiratory**

Use a NIOSH approved positive-pressure, supplied air respirator with escape bottle or self-contained breathing apparatus (SCBA) for gas concentrations above occupational exposure limits, for potential for uncontrolled release, if exposure levels are not known, or in an oxygen-deficient atmosphere. CAUTION: Flammability limits (i.e., explosion hazard should be considered when assessing the need to expose personnel to concentrations requiring respiratory protection.

#### **Personal Protective Equipment: Hands**

Use cold-impervious, insulating flame-retardant (FR) gloves where contact with pressurized gas may occur.

#### **Personal Protective Equipment: Eyes**

Where there is a possibility of pressurized gas contact, wear splash-proof safety goggles and faceshield.

#### Personal Protective Equipment: Skin and Body

Where contact with pressurized gas may occur, wear flame-retardant (FR) and a faceshield.

## \* \* \* Section 9 - PHYSICAL AND CHEMICAL PROPERTIES \* \* \*

Odorless to slight

Appearance: Colorless Odor: petroleum odor

Physical State:GaspH:NDVapor Pressure:40 atm @ -187°F (-86°C)Vapor Density:0.6Boiling Point:-259°F (-162°C)Melting Point:ND

**Solubility (H2O):** 3.5% **Specific Gravity:** 0.4 @ -263°F (-164°C)

Material Name: Wet Field Natural Gas

Evaporation Rate: ND VOC: ND

Octanol / H2O Coeff.: ND Flash Point: Flammable Gas

Flash Point Method: N/A

Lower Flammability Limit: 3.8 – 6.5 Upper Flammability Limit: 13-17

(LFL): (UFL):

Auto Ignition: 900-1170°F (482-632°C) Burning Rate: ND

## \* \* \* Section 10 - CHEMICAL STABILITY & REACTIVITY INFORMATION \* \* \*

#### **Chemical Stability**

This is a stable material.

#### **Hazardous Reaction Potential**

Will not occur.

#### **Conditions to Avoid**

Keep away from strong oxidizers, ignition sources and heat.

# **Hazardous Decomposition Products**

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

#### \* \* \* Section 11 - TOXICOLOGICAL INFORMATION \* \* \*

#### **Acute Toxicity**

#### A: General Product Information

Methane and ethane, the main components of natural gas, are considered practically inert in terms of physiological effects. At high concentrations these materials act as simple asphyxiants and may cause death due to lack of oxygen.

#### B. Component Analysis – LD50/LC50

#### Methane (74-82-8)

Inhalation LC50 Mouse 326 g/m3 2h

#### Ethane (74-84-0)

Inhalation LC50 Rat 658 mg/l 4h

#### **Propane (74-98-6)**

Inhalation LC50 Rat 658 mg/l 4h

Material Name: Wet Field Natural Gas

**Butanes (106-97-8)** 

Inhalation LC50 Rat 658 g/m3 4h

Pentanes (109-66-0)

Inhalation LD50 Rat 364 g/m3 4h

**Hexanes (110-54-3)** 

Inhalation LC50 Rat > 20 mg/l 4h

Nitrogen (7727-37-9)

Simple Asphyxiant

Carbon Dioxide (124-38-9)

Inhalation LC50 Human 100,000 ppm 1minute

Oxygen (7782-44-7)

N/A – Necessary for life

Potential Health Effects: Skin Corrosion Property / Stimulativeness

This product is not reported to have any skin sensitization effects.

**Generative Cell Mutagenicity** 

This product is not reported to have any mutagenic effects.

Carcinogenicity

A: General Product Information

This product is not reported to have any carcinogenic effects.

**B:** Component Carcinogenicity

None of this product's components are listed by ACGIH, IARC, OSHA, NIOSH, or NTP.

**Reproductive Toxicity** 

This product is not reported to have any reproductive toxicity effects.

**Specified Target Organ General Toxicity: Single Exposure** 

This product may cause damage to the heart.

**Specified Target Organ General Toxicity: Repeated Exposure** 

This product is not reported to have any specific target organ repeat effects.

**Aspiration Respiratory Organs Hazard** 

This product is not reported to have any aspiration hazard effects.

Page 8 of 11

Material Name: Wet Field Natural Gas

## \* \* \* Section 12 - ECOLOGICAL INFORMATION \* \* \*

## **Ecotoxicity**

#### A: General Product Information

Keep gas and vapors out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

## B: Component Analysis – Ecotoxicity – Aquatic Toxicity

No ecotoxicity data are available for this product's components.

#### **Persistance / Degradability**

No information available.

#### Bioaccumulation

No information available.

## **Mobility in Soil**

No information available.

## \* \* \* Section 13 - DISPOSAL CONSIDERATIONS \* \* \*

## **Waste Disposal Instructions**

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

#### **Disposal of Contaminated Containers or Packaging**

Dispose of contents / container in accordance with local / regional / national / international regulations.

## \* \* \* Section 14 - TRANSPORTATION INFORMATION \* \* \*

#### **DOT Information**

Shipping Name: Natural Gas, Compressed

**UN #:** 1971 **Hazard Class:** 2.1

Placard:



Material Name: Wet Field Natural Gas

## \* \* \* Section 15 - REGULATORY INFORMATION \* \* \*

## **Regulatory Information**

## **Component Analysis**

None of this products components are listed under SARA Section 302 (40 CFR 355 Appendix A.

n-hexane is listed under SARA Section 313 (40 CFR 372.65). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

n-hexane is listed under CERCLA (40 CFR 302.4). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

#### SARA Section 311/312 – Hazard Classes

Acute Health	Chronic Health	<u>Fire</u>	Sudden Release of Pressure	<b>Reactive</b>
		Χ	X	

## **SARA Section 313 – Supplier Notification**

This product contains one chemical (n-Hexane) that is subject to the reporting requirements of section 313 of the Emergency Planning and Community Right-to-know act (EPCRA) of 1986 and of 40 CFR 372. However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

## **State Regulations**

## **Component Analysis – State**

The following components appear on one or more of the following state hazardous substances lists:

Component	CAS	CA	MA	MN	NJ	PA	RI
Methane	74-82-8	No	No	Yes	Yes	Yes	No
Ethane	78-84-0	No	No	Yes	Yes	Yes	No
Propane	74-98-6	No	No	Yes	Yes	Yes	Yes
Butane	106-97-8	Yes	No	Yes	Yes	Yes	Yes
Pentanes	109-66-0	Yes	No	Yes	Yes	Yes	Yes
Hexanes	110-54-3	Yes	Yes	Yes	Yes	Yes	Yes
Nitrogen	7727-37-9	No	No	No	No	No	No
Carbon Dioxide	124-38-9	Yes	No	Yes	Yes	Yes	Yes
Oxygen	7782-44-7	No	No	No	No	No	No

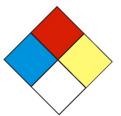
Material Name: Wet Field Natural Gas

## \* \* \* Section 16 - OTHER INFORMATION \* \* \*

NFPA® Hazard Rating Health 1

Fire 4

Reactivity 0



**HMIS® Hazard Rating** Health 1 Moderate

Fire 4 Severe
Physical 0 Minimal
\* Chronic

## Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act: ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

#### **Literature References**

None

#### Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: February 7, 2014

Date of Last Revision: March 4,, 2014

End of Sheet



Material Name: Dry Field Natural Gas US GHS

SYNONYMS: CNG, Natural Gas, Methane.

# \* \* \* Section 1 - PRODUCT AND COMPANY IDENTIFICATION \* \* \*

PRODUCT NAME: Dry Field Natural Gas EMERGENCY PHONE: (800) 878-1373
PRODUCT CODES: CAS Reg. No. 68410-63-9 AFTER HOURS: (800) 878-1373

PRODUCER: Antero Resources

ADDRESS: 1615 Wynkoop Street CHEMTREC PHONE: (800) 424-9300

Denver, Colorado 80202

#### \* \* \* Section 2 - HAZARDS IDENTIFICATION \* \* \*

#### **GHS Classification:**

Flammable Gas – Category 1.

Gases Under Pressure - Gas.

Specific Target Organ Systemic Toxicity (STOT) – Single Exposure Category 2.

# GHS LABEL ELEMENTS Symbol(s)







#### **Signal Word**

Danger

#### **Hazard Statements**

Extremely flammable gas.

Contains gas under pressure, may explode if heated.

May cause damage to central nervous and respiratory systems.

#### **Precautionary Statements**

#### Prevention

Keep away from heat/sparks/open flames/hot surfaces. No smoking.

Do not breathe fume/gas/mist/vapors/spray.

Wash thoroughly after handling.

Do not eat, drink or smoke when using this product.

Material Name: Dry Field Natural Gas US GHS

### Response

Leaking gas fire: Do not extinguish, unless leak can be stopped safely. Eliminate all ignition sources if safe to do so.

If exposed to gas, or concerned about possible exposure: Call a POISON CENTER or doctor/physician.

## **Storage**

Protect from sunlight. Store in a well-ventilated place.

Store in a secure area.

## **Disposal**

Dispose of contents/containers in accordance with local/regional/national/international regulations.

# \* \* \* Section 3 - COMPOSITION / INFORMATION ON INGREDIENTS \* \* \*

CAS#	Component	Percent
74-82-8	Methane	95.01
78-84-0	Ethane	3.99
74-98-6	Propane	0.32
106-97-8	Butanes	0.07
109-66-0	Pentanes	0.02
110-54-3	Hexanes	0.01
7727-37-9	Nitrogen	0.35
124-38-9	Carbon Dioxide	0.19
7782-44-7	Oxygen	0.03

Because natural gas is a natural product, composition can vary greatly.

## \* \* \* Section 4 - FIRST AID MEASURES \* \* \*

#### First Aid: Eyes

In case of freeze burn, cover eyes to protect from light. Flush eyes with running water for at least fifteen (15) minutes. Following flushing, seek medical attention.

#### First Aid: Skin

Remove contaminated clothing. In case of blistering, frostbite or freeze burns, seek immediate medical attention.

Material Name: Dry Field Natural Gas US GHS

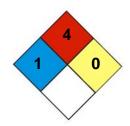
### First Aid: Ingestion

Risk of ingestion is extremely low. However, if oral exposure occurs, seek immediate medical assistance.

#### First Aid: Inhalation

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

## \* \* \* Section 5 - FIRE FIGHTING MEASURES \* \* \*



#### **NFPA 704 Hazard Class**

Health: 1 Flammability: 4 Instability: 0 (0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

#### **General Fire Hazards**

See Section 9 for Flammability Properties.

Forms a flammable mixture with air. If released, the resulting vapors will disperse with the prevailing wind. If a source of ignition is present where the vapor exists at a 5-15% concentration in air, the vapor will burn along the flame front toward the source of the fuel.

## **Hazardous Combustion Products**

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

#### **Extinguishing Media**

Any extinguisher suitable for Class B fires, dry chemical, fire fighting foam, CO2, and other gaseous agents. However, fire should not be extinguished unless flow of gas can be immediately stopped.

#### **Unsuitable Extinguishing Media**

None.

#### Fire Fighting Equipment / Instructions

Gas fires should not be extinguished unless flow of gas can be immediately stopped. Shut off gas source and allow gas to burn out. If spill or leak has not ignited, determine

Material Name: Dry Field Natural Gas US GHS

if water spray may assist in dispersing gas or vapor to protect personnel attempting to stop leak. Use water to cool equipment, surfaces and piping exposed to fire and excessive heat. For large fire, the use of unmanned hose holders or monitor nozzles may be advantageous to further minimize personnel exposure. Isolate area, particularly around piping. Let the fire burn unless leak can be stopped. Concentrate fire-fighting efforts on objects / materials ignited by the initial fire. Withdraw immediately in the event of a rising sound from a venting safety device.

Firefighting activities that may result in potential exposure to high heat, smoke or toxic by-products of combustion should require NIOSH-approved pressure-demand self-contained breathing apparatus with full facepiece and full protective clothing.

## \* \* \* Section 6 - ACCIDENTAL RELEASE MEASURES \* \* \*

### **Recovery and Neutralization**

Stop the source of the release, if safe to do so.

#### **Materials and Methods for Clean-Up**

Consider the use of water spray to disperse gas vapors. Do not use water spray to direct gas vapors toward sewer or drainage systems. Isolate the area until gas has dispersed. Ventilate and gas test area before entering.

#### **Emergency Measures**

Evacuate nonessential personnel and secure all ignition sources. No road flares, smoking or flames in hazard area. Consider wind direction. Stay upwind and uphill, if possible. Vapor cloud may be white, but color will dissipate as cloud disperses. Fire and explosion hazard is still present.

#### **Personal Precautions and Protective Equipment**

Cooling effect of expanding gas from leak may present frostbite / freeze burn hazard. Wear flame retardant (FR) clothing around un-ignited leak. Wear fire protective clothing around an active fire.

#### **Environmental Precautions**

Do not flush gas vapors toward sewer or drainage systems.

#### **Prevention of Secondary Hazards**

None.

Material Name: Dry Field Natural Gas US GHS

#### \* \* \* Section 7 – HANDLING AND STORAGE \* \* \*

## **Handling Procedures**

Keep away from flame, sparks and excessive temperatures. Bond and ground containers. Use only in well ventilated areas.

## **Storage Procedures**

Natural gas will be contained in the pipeline. Keep away from flame, sparks, excessive temperatures and open flames. Empty pipeline segments may contain explosive residues from natural gas liquids. Do not cut, heat, weld or expose containers to sources of ignition sections of pipeline unless the sections have been purged of natural gas residues.

### **Incompatibilities**

Keep away from strong oxidizers, ignition sources and heat.

# \* \* \* Section 8 - EXPOSURE CONTROLS / PERSONAL PROTECTION \* \* \*

#### **Component Exposure Limits**

### Methane (74-82-8)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases: Alkane C1-4)

#### Ethane (74-84-0)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases: Alkane C1-4)

#### **Propane (74-98-6)**

ACGIH: 2500 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

#### **Butane (106-97-8)**

ACGIH: 800 ppm TWA (listed under Aliphatic hydrocarbon gases: Alkane C1-4)

## Pentanes (109-66-0)

ACGIH: 600 ppm TWA (listed under Pentane, all isomers)

## Hexanes (110-54-3)

ACGIH: 50 ppm TWA (listed under n-Hexane)

Material Name: Dry Field Natural Gas US GHS

## Nitrogen (7727-37-9)

Simple Asphyxiant

#### Carbon Dioxide (124-38-9)

ACGIH: 5000 ppm TWA (listed under Carbon Dioxide)

## Oxygen (7782-44-7)

N/A – Necessary for life

## **Engineering Measures**

Use adequate ventilation to keep gas and vapor concentrations of this product below occupational exposure and flammability limits, particularly in confined spaces. Use explosion-proof equipment and lighting in classified / controlled areas.

# Personal Protective Equipment: Respiratory

Use a NIOSH approved positive-pressure, supplied air respirator with escape bottle or self-contained breathing apparatus (SCBA) for gas concentrations above occupational exposure limits, for potential for uncontrolled release, if exposure levels are not known, or in an oxygen-deficient atmosphere. CAUTION: Flammability limits (i.e., explosion hazard should be considered when assessing the need to expose personnel to concentrations requiring respiratory protection.

#### **Personal Protective Equipment: Hands**

Use cold-impervious, insulating flame-retardant (FR) gloves where contact with pressurized gas may occur.

#### **Personal Protective Equipment: Eyes**

Where there is a possibility of pressurized gas contact, wear splash-proof safety goggles and faceshield.

#### Personal Protective Equipment: Skin and Body

Where contact with pressurized gas may occur, wear flame-retardant (FR) and a faceshield.

## \* \* \* Section 9 - PHYSICAL AND CHEMICAL PROPERTIES \* \* \*

Odorless to slight

Appearance: Colorless Odor: petroleum odor

Physical State:GaspH:NDVapor Pressure:40 atm @ -187°F (-86°C)Vapor Density:0.6Boiling Point:-259°F (-162°C)Melting Point:ND

**Solubility (H2O):** 3.5% **Specific Gravity:** 0.4 @ -263°F (-164°C)

Material Name: Dry Field Natural Gas US GHS

Evaporation Rate: ND VOC: ND

Octanol / H2O Coeff.: ND Flash Point: Flammable Gas

Flash Point Method: N/A

Lower Flammability Limit: 3.8 – 6.5 Upper Flammability Limit: 13-17

(LFL): (UFL):

Auto Ignition: 900-1170°F (482-632°C) Burning Rate: ND

## \* \* \* Section 10 - CHEMICAL STABILITY & REACTIVITY INFORMATION \* \* \*

## **Chemical Stability**

This is a stable material.

### **Hazardous Reaction Potential**

Will not occur.

### **Conditions to Avoid**

Keep away from strong oxidizers, ignition sources and heat.

# **Hazardous Decomposition Products**

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

#### \* \* \* Section 11 - TOXICOLOGICAL INFORMATION \* \* \*

#### **Acute Toxicity**

#### A: General Product Information

Methane and ethane, the main components of natural gas, are considered practically inert in terms of physiological effects. At high concentrations these materials act as simple asphyxiants and may cause death due to lack of oxygen.

#### B. Component Analysis – LD50/LC50

#### Methane (74-82-8)

Inhalation LC50 Mouse 326 g/m3 2h

#### Ethane (74-84-0)

Inhalation LC50 Rat 658 mg/l 4h

#### **Propane (74-98-6)**

Inhalation LC50 Rat 658 mg/l 4h

Material Name: Dry Field Natural Gas US GHS

### **Butanes (106-97-8)**

Inhalation LC50 Rat 658 g/m3 4h

## Pentanes (109-66-0)

Inhalation LD50 Rat 364 g/m3 4h

## Hexanes (110-54-3)

Inhalation LC50 Rat > 20 mg/l 4h

### Nitrogen (7727-37-9)

Simple Asphyxiant

## Carbon Dioxide (124-38-9)

Inhalation LC50 Human 100,000 ppm 1minute

## Oxygen (7782-44-7)

N/A – Necessary for life

## Potential Health Effects: Skin Corrosion Property / Stimulativeness

This product is not reported to have any skin sensitization effects.

#### **Generative Cell Mutagenicity**

This product is not reported to have any mutagenic effects.

## Carcinogenicity

#### A: General Product Information

This product is not reported to have any carcinogenic effects.

#### **B:** Component Carcinogenicity

None of this product's components are listed by ACGIH, IARC, OSHA, NIOSH, or NTP.

#### **Reproductive Toxicity**

This product is not reported to have any reproductive toxicity effects.

#### Specified Target Organ General Toxicity: Single Exposure

This product may cause damage to the heart.

## **Specified Target Organ General Toxicity: Repeated Exposure**

This product is not reported to have any specific target organ repeat effects.

#### **Aspiration Respiratory Organs Hazard**

This product is not reported to have any aspiration hazard effects.

Page 8 of 11

Material Name: Dry Field Natural Gas US GHS

## \* \* \* Section 12 - ECOLOGICAL INFORMATION \* \* \*

## **Ecotoxicity**

#### A: General Product Information

Keep gas and vapors out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

# **B:** Component Analysis – Ecotoxicity – Aquatic Toxicity

No ecotoxicity data are available for this product's components.

## **Persistance / Degradability**

No information available.

#### Bioaccumulation

No information available.

## **Mobility in Soil**

No information available.

## \* \* \* Section 13 - DISPOSAL CONSIDERATIONS \* \* \*

## **Waste Disposal Instructions**

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

#### **Disposal of Contaminated Containers or Packaging**

Dispose of contents / container in accordance with local / regional / national / international regulations.

## \* \* \* Section 14 - TRANSPORTATION INFORMATION \* \* \*

#### **DOT Information**

Shipping Name: Natural Gas, Compressed

UN #: 1971 Hazard Class: 2.1

Placard:



Material Name: Dry Field Natural Gas US GHS

## \* \* \* Section 15 - REGULATORY INFORMATION \* \* \*

### **Regulatory Information**

# **Component Analysis**

None of this products components are listed under SARA Section 302 (40 CFR 355 Appendix A.

n-hexane is listed under SARA Section 313 (40 CFR 372.65). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

n-hexane is listed under CERCLA (40 CFR 302.4). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

#### SARA Section 311/312 – Hazard Classes

Acute Health	Chronic Health	<u>Fire</u>	Sudden Release of Pressure	<u>Reactive</u>
		Χ	X	

## SARA Section 313 – Supplier Notification

This product contains one chemical (n-Hexane) that is subject to the reporting requirements of section 313 of the Emergency Planning and Community Right-to-know act (EPCRA) of 1986 and of 40 CFR 372. However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

## **State Regulations**

### **Component Analysis – State**

The following components appear on one or more of the following state hazardous substances lists:

Component	CAS	CA	MA	MN	NJ	PA	RI
Methane	74-82-8	No	No	Yes	Yes	Yes	No
Ethane	78-84-0	No	No	Yes	Yes	Yes	No
Propane	74-98-6	No	No	Yes	Yes	Yes	Yes
Butane	106-97-8	Yes	No	Yes	Yes	Yes	Yes
Pentanes	109-66-0	Yes	No	Yes	Yes	Yes	Yes
Hexanes	110-54-3	Yes	Yes	Yes	Yes	Yes	Yes
Nitrogen	7727-37-9	No	No	No	No	No	No
Carbon Dioxide	124-38-9	Yes	No	Yes	Yes	Yes	Yes
Oxygen	7782-44-7	No	No	No	No	No	No

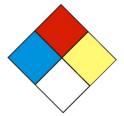
Material Name: Dry Field Natural Gas US GHS

## \* \* \* Section 16 - OTHER INFORMATION \* \* \*

NFPA® Hazard Rating Health 1

Fire 4

Reactivity 0



HMIS® Hazard Rating Health 1 Moderate

Fire 4 Severe
Physical 0 Minimal

\* Chronic

### Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act: ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

#### **Literature References**

None

#### Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: January 30, 2014

Date of Last Revision: March 4, 2014

**End of Sheet** 

# Material Safety Data Sheet (TRIETHYLENE GLYCOL (TEG))

#### **SECTION 1 – IDENTIFICATION OF CHEMICAL PRODUCT**

PRODUCT NAME:..... TRIETHYLENE GLYCOL (TEG)

EFFECTIVE DATE:..... October 1, 2007

**CHEMICAL FAMILY:** Glycol **FORMULA:**  $C_6H_{14}O_4$  **CAS NUMBER:** 112-27-6

#### **SECTION 2 – COMPOSITION / INFORMATION ON INGREDIENTS**

HAZARDOUS INGREDIENT PERCENT CAS NUMBER PEL

TRIETHYLENE GLYCOL > 99 112-27-6 None Established by ACGIH or OSHA.

The criteria for listing components in the composition section are as follows: Carcinogens are listed when present at 0.1% or greater; components which are otherwise hazardous according to OSHA are listed when present at 1.0% or greater. Non-hazardous components may be listed at 3.0% or greater if not proprietary in nature. This is not intended to be complete compositional disclosure. Refer to section 14 for applicable states right to know and other regulatory information.

#### **SECTION 3 – HAZARDS IDENTIFICATION**

#### **EMERGENCY OVERVIEW**

APPEARANCE / ODOR: ...... Clear Liquid / Mild Odor

**SHORT TERM EXPOSURE: Inhalation:** No adverse health effects expected from inhalation.

**Ingestion:** No adverse effects expected. **Skin Contact:** Prolonged exposure may cause skin irritation. **Eye Contact:** Splashing in eye causes irritation with transitory disturbances of corneal epithelium. However, these effects diminish and no permanent injury is expected. Vapors are non-irritating. **Chronic Exposure:** Possible skin irritation.

**Aggravation of Pre-existing Conditions:** No information found.

OSHA REGULATED: ..... No

LISTED CARCINOGEN: ...... NTP: No IARC MONOGRAPHS: No

#### POTENTIAL HEALTH EFFECTS

INHALATION: ...... Unlikely INGESTION: ...... Irritant

SKIN (DERMAL): ...... Slight Irritant After Prolonged Contact

# **Material Safety Data Sheet** (TRIETHYLENE GLYCOL (TEG))

**OVER EXPOSURE EFFECTS: Inhalation:** No adverse health effects expected from inhalation. **Ingestion:** No adverse effects expected. **Skin Contact:** Prolonged exposure may cause skin irritation. Eye Contact: Splashing in eye causes irritation with transitory disturbances of corneal epithelium. However, these effects diminish and no permanent injury is expected. Vapors are non-irritating. **Chronic Exposure:** Possible skin irritation. Aggravation of Pre-existing Conditions: No information found.

#### **SECTION 4 – FIRST AID MEASURES**

FIRST AID:

**SKIN CONTACT:** Remove contaminated clothing and shoes immediately. Wash affected area with soap or mild detergent and large amounts of water until no evidence of chemical remains (at least 15-20 minutes). Get medical attention immediately. EYE CONTACT: Flush eyes immediately with large amounts of water or normal saline solution, occasionally lifting upper and lower lids until no evidence of chemical remains (at least 15-20 minutes). Get medical attention immediately. INGESTION: Give large amounts of fresh water or milk immediately. Do not give anything by mouth if person is unconscious or otherwise unable to swallow. If vomiting occurs, keep head below hips to prevent aspiration. Treat symptomatically and supportively. Seek medical attention immediately. **INHALATION:** Remove from exposure area to fresh air immediately. If breathing has stopped, perform artificial resuscitation. Keep person warm and at rest. Treat symptomatically and supportively. Seek medical attention immediately. Qualified medical personnel should consider administering oxygen.

NOTE TO PHYSICIAN: ..... Ethylene Glycol (EG) and diethylene glycol (DEG) intoxication may initially produce behavioral changes, drowsiness, vomiting, diarrhea, thirst, and convulsions. EG and DEG are nephrotoxic. End stages of poisoning may include renal damage or failure with acidosis. Supportive measures, supplemented with hemodialysis if indicated, may limit the progression and severity of toxic effects. Primary toxic effects of EG when swallowed are kidney damage and metabolic acidosis. This product may contain trace amounts of Ethylene Glycol (EG) or Diethylene Glycol (DEG).

#### **SECTION 5 - FIRE FIGHTING MEASURES**

**FLASHPOINT:....** 350°F

Water fog or spray, Foam, Dry Powder, Carbon Dioxide (CO<sub>2</sub>). **EXTINGUISHING MEDIA:** 

DECOMPOSITION

**PRODUCTS:** From fire; Smoke, Carbon dioxide, & Carbon Monoxide

LOWER FLAME LIMIT:....< 0.9 HIGHER FLAME LIMIT:.....> 9

UNUSUAL FIRE AND

EXPLOSION HAZARDS:...... Toxic levels of carbon monoxide, carbon dioxide, irritation aldehydes

and ketones may be formed on burning. Heating in air may produce

irritating aldehydes, acids, and ketones.

FIRE FIGHTING

# **Material Safety Data Sheet** (TRIETHYLENE GLYCOL (TEG))

**EQUIPMENT:** Fire fighters and others exposed to products of combustion should wear self-contained breathing apparatus. Equipment should be thoroughly decontaminated after use.

#### SECTION 6 – ACCIDENTAL RELEASE MEASURES

**CHEMTEL EMERGENCY** 

NUMBER (24 Hour): ..... 1-800-255-3924

SPILL: Ventilate area of leak or spill. Wear appropriate personal protective

equipment as specified in Section 8. Isolate hazard area. Keep unnecessary and unprotected personnel from entering. Contain and recover liquid when possible. Collect liquid in an appropriate container or absorb with an inert material (e. g., vermiculite, dry sand, earth), and place in a chemical waste container. Do not use combustible materials,

such as saw dust. Do not flush to sewer!

RCRA STATUS: ...... None

#### **SECTION 7 – HANDLING AND STORAGE**

HANDLE IN ACCORDANCE WITH GOOD INDUSTRIAL HYGIENE AND SAFETY PRACTICES. THESE PRACTICES INCLUDE AVOIDING UNNECESSARY EXPOSURE AND PROMPT REMOVAL OF MATERIAL FROM EYES, SKIN, AND CLOTHING.

HANDLING AND STORAGE: .. No special storage requirements. Do not store above 120°F.

PRECAUTIONARY

container after each use. Avoid prolonged or repeated contact with skin. Avoid contact with skin, eyes, and clothing. After handling this product, wash hands before eating, drinking, or smoking. If needed, take first aid action shown in Section 4.

#### **SECTION 8 – EXPOSURE CONTROL / PERSONAL PROTECTION**

#### **GENERAL CONSIDERATIONS:**

Consider the potential hazards of this material (see section 3), applicable exposure limits, job activities, and other substances in the work place when designing engineering controls and selecting personal protective equipment.

**EYE PROTECTION:.....** Chemical safety goggles meeting the specifications of OSHA 29CFR

1910.133 / ANSI Standard Z87.1 should be worn whenever there is the possibility of splashing or other contact with the eyes. Wear safety glasses meeting the specifications of OSHA 29CFR 1910.133 / ANSI

Standard Z87.1 where no contact with the eye is anticipated.

RESPIRATORY

exposure is unknown or exceeds permissible limits. A respiratory protection program that meets OSHA's 29 CFR 1910.134 or ANSI Z88.2 requirements must be followed whenever workplace conditions

warrant respirator use.

Use NIOSH / MSHA approved respiratory protection equipment when airborne exposure limits are exceeded (see below). Consult the respirator manufacturer to determine appropriate type of

# Material Safety Data Sheet (TRIETHYLENE GLYCOL (TEG))

equipment for a given application. Observe respirator use limitations specified by NIOSH / MSHA or the manufacturer. Respiratory protection programs must comply with 29 CFR 1910.134. WARNING: Air-purifying respirators do not protect workers in oxygen-deficient atmospheres.

**PROTECTIVE GLOVES:.....** Wear impervious gloves

**VENTILATION:** A system of local and/or general exhaust is recommended to keep

employee exposures below the Airborne Exposure Limits. Local exhaust ventilation is generally preferred because it can control the emissions of the contaminant at its source, preventing dispersion of it into the general work area. Please refer to the ACGIH document, *Industrial Ventilation, A Manual of Recommended Practices*, most

recent edition, for details.

MECHANICAL EXHAUST: ..... Desired in closed places

LOCAL EXHAUST: ..... Recommended

VENTILATION NOTES: Provide natural or mechanical ventilation to control exposure levels below Airborne exposure limits (see below). The use of local mechanical exhaust ventilation is preferred at sources of air contamination such as open process equipment. Consult NFPA Standard 91 for design of exhaust systems.

THRESHOLD LIMIT VALUE: . None Established

**PROTECTIVE EQUIPMENT:...** HMIS PERSONAL PROTECTION: C: Safety Glasses, Gloves, Apron The user should read and understand all instructions and limitations supplied with the equipment since protection is usually provided for a limited time or under certain circumstances.

#### **SECTION 9 - PHYSICAL AND CHEMICAL PROPERTIES**

APPEARANCE / ODOR: ...... Clear Liquid / Mild Odor

**SOLUBILITY IN WATER: ......** Complete

#### **SECTION 10 – STABILITY AND REACTIVITY**

STABILITY: ..... Stable

HAZARDOUS

POLYMERIZATION: ..... Will Not Occur

POLYMERIZATION AVOID:... None

INCOMPATIBILITY: ...... Explosive decomposition may occur if combined with strong acids or

strong bases and subjected to elevated temperatures. Therefore, avoid strong acids and strong bases at elevated temperatures. Avoid

contamination with strong oxidizing agents and materials reactive with

hydroxyl compounds. Avoid burning or heating in air. This may

produce irritating aldehydes, acids, and ketones.

**CONDITIONS TO AVOID:......** Excessive heat. Will ignite in air at 700°F

# **Material Safety Data Sheet** (TRIETHYLENE GLYCOL (TEG))

#### **SECTION 11 – TOXICOLOGICAL INFORMATION**

#### **EYE EFFECTS:**

The eye irritation hazard is based on data from information supplied by raw material(s) supplier(s).

#### **SKIN EFFECTS:**

The skin irritation hazard is based on data from information supplied by raw material(s) supplier(s).

#### **ACUTE ORAL EFFECTS:**

The acute oral toxicity is based on data from information supplied by raw material(s) supplier(s).

#### **ACUTE INHALATION EFFECTS:**

The acute respiratory toxicity is based on data from information supplied by raw material(s) supplier(s).

#### **SECTION 12 - ECOLOGICAL INFORMATION**

Data from laboratory studies and from scientific literature is noted below if available.

#### **SECTION 13 DISPOSAL CONSIDERATIONS**

WASTE DISPOSAL: ...... Treatment, storage, transportation and disposal must be in accordance with Federal, State/Provincial and Local Regulations. Regulations may vary in different locations. Characterization and compliance with applicable laws are the responsibility solely of the generator. Whatever cannot be saved for recovery or recycling should be managed in an appropriate and approved waste disposal facility. Processing, use or contamination of this product may change the waste management options. State and local disposal regulations may differ from federal disposal regulations. Dispose of container and unused contents in accordance with federal, state and local requirements.

#### **SECTION 14- TRANSPORTATION INFORMATION**

The data provided in this section is for information only. The description shown may not apply to all shipping situations. Consult 49CFR, or appropriate regulations to properly classify your shipment for transportation.

PROPER SHIPPING NAME:..... DOT NON-REGULATED - TRIETHYLENE GLYCOL (TEG)

REPORTABLE QUANTITY:..... None

HAZARD CLASS AND LABEL: NON-REGULATED

UN NUMBER: ..... None NA NUMBER: ..... None

PACKAGING SIZE:..... Pail, Drum & Bulk

#### **SECTION 15 - REGULATORY INFORMATION**

#### SARA 311 CATEGORIES:

EPA ACUTE:..... Yes (Eyes)

# Material Safety Data Sheet (TRIETHYLENE GLYCOL (TEG))

EPA CHRONIC:
OF PRESSURE: No
CERCLA RQ VALUE: None
SARA TPQ: None
SARA RQ:None
EPA HAZARD WASTE #: None
CLEAN AIR: NA
CLEAN WATER:NA
SARA SECTION 313:No
NFPA HEALTH:2
NFPA FLAMMABILITY:1
NFPA REACTIVITY:0
DEA Chemical Trafficking Act: No
<b>TSCA STATUS:</b> All ingredients in this product are on the TSCA Inventory List.

#### **SECTION 16 - ADDITIONAL INFORMATION**

FOOT NOTES: NA - NOT APPLICABLE ND - NO DATA AVAILABLE > = GREATER THAN < = LESS THAN

Prepared according to the OSHA Hazard Communication Standard (29 CFR 1910.1200) and the ANSI MSDS Standard (Z400.1) by the Company Health and Risk Assessment Unit, PO Box 1519, Gretna, LA 70054-1519.

**REVISION STATEMENT:** Changes have been made throughout this Material Safety Data Sheet. Please read the entire document.

#### **DISCLAIMER:**

Although the information and recommendations set forth herein (hereinafter "Information") are presented in good faith and believed to be correct as of the date hereof, the Company makes no representations as to the completeness or accuracy thereof. Information is supplied upon the condition that the persons receiving this MSDS will make their own determination as to its suitability for their intended purposes prior to use. Since the product is within the exclusive control of the user, it is the user's obligation to determine the conditions of safe use of this product. Such conditions should comply with all Federal Regulations concerning the Product. It must be recognized that the physical and chemical properties of any product may not be fully understood and that new, possibly hazardous products may arise from reactions between chemicals. The information given in this data sheet is based on our present knowledge and shall not constitute a guarantee for any specific product features and shall not establish a legally valid contractual relationship. REPRESENTATIONS OR WARRANTIES, EITHER EXPRESS OR IMPLIED. MERCHANTABILITY, FITNESS FOR A PARTICULAR PURPOSE OR OF ANY OTHER NATURE ARE MADE HEREUNDER WITH RESPECT TO INFORMATION OR THE PRODUCT TO WHICH INFORMATION REFERS.

Attachment I. Emission Units Table	

## Attachment I

## **Emission Units Table**

# (includes all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status)

Emission Unit ID <sup>1</sup>	Emission Point ID <sup>2</sup>	Emission Unit Description	Year Installed/ Modified	Design Capacity	Type <sup>3</sup> and of Char		Control Device <sup>4</sup>
C-2100	1E	Compressor Engine #1	2016	1,680 hp	Modified	NS	SCR (1C)
C-2110	2E	Compressor Engine #2	2016	1,680 hp	Modified	NS	SCR (2C)
C-2120	3E	Compressor Engine #3	2016	1,680 hp	Modified	NS	SCR (3C)
C-2130	4E	Compressor Engine #4	2016	1,680 hp	Modified	NS	SCR (4C)
C-2140	5E	Compressor Engine #5	2016	1,680 hp	Modified	NS	SCR (5C)
C-2150	6E	Compressor Engine #6	2016	1,680 hp	Modified	NS	SCR (6C)
C-2160	7E	Compressor Engine #7	2016	1,680 hp	Modified	NS	SCR (7C)
C-2170	8E	Compressor Engine #8	2016	1,680 hp	Modified	NS	SCR (8C)
C-2180	9E	Compressor Engine #9	2016	1,680 hp	Modified	NS	SCR (9C)
C-2190	10E	Compressor Engine #10	2016	1,680 hp	Modified	NS	CR(10C)
C-2200	11E	Compressor Engine #11	2016	1,680 hp	Modified	NS	CR(11C)
G-8000	12E	Microturbine Generator #1	2015	200 kWe	NA		None
G-8100	13E	Microturbine Generator #2	2015	200 kWe	NA		None
G-8200	28E	Microturbine Generator #3	2015	200 kWe	NA		None
V-3110	14E	Dehydrator Still Vent #1	2016	72.5 MMscfd	Modified	FL-8	3300 (12C)
V-3120	15E	Dehydrator Flash Tank #1	2016	72.5 MMscfd	Modified		ontrol-16E or 3C&14C
F-3100	16E	Dehydrator Reboiler #1	2016	1.5 mmbtu/hr	Modified		None
V-3210	17E	Dehydrator Still Vent #2	2016	72.5 MMscfd	Modified	FL-8	3300 (12C)
V-3220	18E	Dehydrator Flash Tank #2	2016	72.5 MMscfd	Modified		ontrol-16E or 3C&14C
F-3200	19E	Dehydrator Reboiler #2	2016	1.5 mmbtu/hr	Modified		None
TK-9000	20E	Settling Tank 1	2015	500 barrel	NA		6000 & VRU- 13C & 14C)
TK-9200	21E	Condensate Tank 1	2015	400 barrel	NA		6000 & VRU- 13C & 14C)
TK-9210	22E	Condensate Tank 2	2015	400 barrel	NA		6000 & VRU- 13C & 14C)

Emission Units Table 03/2007

TK-9100	23E	Produced Water Tank 1	2015	400 barrel	NA	VRU-6000 & VRU-6100 (13C & 14C)
TK-9110	24E	Produced Water Tank 2	2015	400 barrel	NA	VRU-6000 & VRU-6100 (13C & 14C)
CATHT1	27E	Catalytic Heater for Generator Fuel	2015	0.024 MMBtu/hr	NA	None
LDOUT1	29E	Hydrocarbon Truck Loading	2015	195 bbl/day	NA	None
FUEL1	30E	Fuel Conditioning Heater	2016	0.50 MMBtu/hr	New	None
		NSCR Catalyst for Compressor #1	2016		Modified	1C
		NSCR Catalyst for Compressor #2	2016		Modified	2C
		NSCR Catalyst for Compressor #3	2016		Modified	3C
		NSCR Catalyst for Compressor #4	2016		Modified	4C
		NSCR Catalyst for Compressor #5	2016		Modified	5C
		NSCR Catalyst for Compressor #6	2016		Modified	6C
		NSCR Catalyst for Compressor #7	2016		Modified	7C
		NSCR Catalyst for Compressor #8	2016		Modified	8C
		NSCR Catalyst for Compressor #9	2016		Modified	9C
		NSCR Catalyst for Compressor #10	2016		Modified	10C
		NSCR Catalyst for Compressor #11	2016		Modified	11C
FL-8300	26E	Flare Combustion Device 1	2015	4.8 MMBtu/hr	NA	12C
		Vapor Recovery Unit 1	2015	40 Mscfd	NA	13C
		Vapor Recovery Unit 2	2015	40 Mscfd	NA	14C

<sup>&</sup>lt;sup>1</sup> For Emission Units (or <u>S</u>ources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation. <sup>2</sup> For <u>E</u>mission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation. <sup>3</sup> New, modification, removal <sup>4</sup> For <u>C</u>ontrol Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

Attachment J. Emission Point Data Summary Sheet	

# Attachment J EMISSION POINTS DATA SUMMARY SHEET

							Table ′	1: Emissions [	Data						
Emission Point ID No. (Must match Emission Units Table & Plot Plan)	Emission Point Type <sup>1</sup>	Emission Unit Vented Through This Point (Must match Emission Units Table & Plot Plan)		Air Pollution Control Device (Must match Emission Units Table & Plot Plan)		Vent Time for Emission Unit (chemical processes only)		All Regulated Pollutants - Chemical Name/CAS <sup>3</sup> (Speciate VOCs & HAPS)	Maximum Potential Uncontrolled Emissions <sup>4</sup>		Maximum Potential Controlled Emissions 5		Emission Form or Phase (At exit conditions, Solid, Liquid	Est. Method Used <sup>6</sup>	Emission Concentration <sup>7</sup> (ppmv or mg/m <sup>4</sup> )
		ID No.	Source	ID No.	Device Type	Short Term <sup>2</sup>	Max (hr/yr)		lb/hr	ton/yr	lb/hr	ton/yr	or Gas/Vapor)		
1E	Upward Vertical Stack	C-2100	Compressor engine 1	1C	NSCR catalyst	С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.37 47.41 1.52 0.27 0.008 0.35 0.19 2083	220.62 207.64 6.65 1.18 0.04 1.54 0.81 9125	1.26 1.19 0.24 0.27 0.008 0.18 0.02 1992	5.52 5.19 1.06 1.18 0.04 0.81 0.08 8725	Gas/Vapor	EE	
2E	Upward Vertical Stack	C-2110	Compressor engine 2	2C	NSCR catalyst	С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.37 47.41 1.52 0.27 0.008 0.35 0.19 2083	220.62 207.64 6.65 1.18 0.04 1.54 0.81 9125	1.26 1.19 0.24 0.27 0.008 0.18 0.02 1992	5.52 5.19 1.06 1.18 0.04 0.81 0.08 8725	Gas/Vapor	EE	
3E	Upward Vertical Stack	C-2120	Compressor engine 3	3C	NSCR catalyst	С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.37 47.41 1.52 0.27 0.008 0.35 0.19 2083	220.62 207.64 6.65 1.18 0.04 1.54 0.81 9125	1.26 1.19 0.24 0.27 0.008 0.18 0.02 1992	5.52 5.19 1.06 1.18 0.04 0.81 0.08 8725	Gas/Vapor	EE	

4E	Upward	C-2130	Com-	4C	NSCR	С	8,760	NOx	50.37	220.62	1.26	5.52	Gas/Vapor	EE	
4E	Vertical	C-2130	pressor	40	catalyst		0,/00	CO	47.41	220.62	1.26	5.52	Gas/ v apor	EE	
	Stack		engine 4					VOC	1.52	6.65	0.24	1.06			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.04	0.008	0.04			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.02	0.08			
								CO2e	2083	9125	1992	8725			
5E	Upward	C-2140	Com-	5C	NSCR	С	8,760	NOx	50.37	220.62	1.26	5.52	Gas/Vapor	EE	
	Vertical		pressor engine 5		catalyst			CO	47.41	207.64	1.19	5.19			
	Stack		engine e					VOC	1.52	6.65	0.24	1.06			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.04	0.008	0.04			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.02	0.08			
								CO2e	2083	9125	1992	8725			
6E	Upward	C-2150	Com-	6C	NSCR	C	8,760	NOx	50.37	220.62	1.26	5.52	Gas/Vapor	EE	
	Vertical		pressor engine 6		catalyst			CO	47.41	207.64	1.19	5.19			
	Stack							VOC	1.52	6.65	0.24	1.06			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.04	0.008	0.04			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.02	0.08			
								CO2e	2083	9125	1992	8725			
7E	Upward	C-2160	Com- pressor	7C	NSCR	C	8,760	NOx	50.37	220.62	1.26	5.52	Gas/Vapor	EE	
	Vertical Stack		engine 7		catalyst			CO	47.41	207.64	1.19	5.19			
	Stack							VOC	1.52	6.65	0.24	1.06			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.04	0.008	0.04			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.02	0.08			
								CO2e	2083	9125	1992	8725			

OE.	T T 1	C-2170	Com-	90	NCCD	C	0.760	NO-	50.27	220.62	1.26	5 50	CanNia	DE	
8E	Upward Vertical	C-21/0	pressor	8C	NSCR catalyst	С	8,760	NOx CO	50.37 47.41	220.62 207.64	1.26 1.19	5.52 5.19	Gas/Vapor	EE	
	Stack		engine 8					VOC	1.52	6.65	0.24	1.06			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.04	0.008	0.04			
								Total HAPs	0.35	1.54	0.000	0.81			
								Formaldehyde	0.19	0.81	0.02	0.01			
								CO2e	2083	9125	1992	8725			
9E	Upward	C-2180	Com-	9C	NSCR	С	8,760	NOx	50.37	220.62	1.26	5.52	Gas/Vapor	EE	
	Vertical		pressor engine 9		catalyst			CO	47.41	207.64	1.19	5.19			
	Stack		cligine y					VOC	1.52	6.65	0.24	1.06			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.04	0.008	0.04			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.02	0.08			
								CO2e	2083	9125	1992	8725			
10E	Upward	C-2190	Com-	10C	NSCR	C	8,760	NOx	50.37	220.62	1.26	5.52	Gas/Vapor	EE	
	Vertical		pressor engine		catalyst			CO	47.41	207.64	1.19	5.19			
	Stack		10					VOC	1.52	6.65	0.24	1.06			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.04	0.008	0.04			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.02	0.08			
								CO2e	2083	9125	1992	8725			
11E	Upward	C-2200	Com- pressor	11C	NSCR	C	8,760	NOx	50.37	220.62	1.26	5.52	Gas/Vapor	EE	
	Vertical		engine		catalyst			CO	47.41	207.64	1.19	5.19			
	Stack		11					VOC	1.52	6.65	0.24	1.06			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.04	0.008	0.04			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.02	0.08			
								CO2e	2083	9125	1992	8725			

12E	Upward Vertical Stack	G8000	Microtu rbine Genera tor 1			С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	0.08 0.22 0.02 0.01 0.007 0.002 0.001 266	0.35 0.96 0.09 0.06 0.03 0.009 0.006 1166	0.08 0.22 0.02 0.01 0.007 0.002 0.001 266	0.35 0.96 0.09 0.06 0.03 0.009 0.006 1166	Gas/Vapor	EE	
13E	Upward Vertical Stack	G8100	Microtu rbine Genera tor 2			С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	0.08 0.22 0.02 0.01 0.007 0.002 0.001 266	0.35 0.96 0.09 0.06 0.03 0.009 0.006 1166	0.08 0.22 0.02 0.01 0.007 0.002 0.001 266	0.35 0.96 0.09 0.06 0.03 0.009 0.006 1166	Gas/Vapor	EE	
28E	Upward Vertical Stack	G8200	Microtu rbine Genera tor 3			С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	0.08 0.22 0.02 0.01 0.007 0.002 0.001 266	0.35 0.96 0.09 0.06 0.03 0.009 0.006 1166	0.08 0.22 0.02 0.01 0.007 0.002 0.001 266	0.35 0.96 0.09 0.06 0.03 0.009 0.006 1166	Gas/Vapor	EE	
14E	Upward Vertical Stack	V-3110	Dehydr ator Still Vent 1	12C	Flare- 98% Control	С	8,760	VOC Total HAPs Benzene Toluene Ethylbenzene Xylenes n-Hexane CO2e	23.46 4.49 0.94 2.10 0.002 0.56 0.88 454	102.8 19.65 4.13 9.22 0.01 2.45 3.85 1989	0.47 0.09 0.02 0.04 <0.0001 0.01 0.02 9.36	2.06 0.39 0.08 0.18 0.0002 0.05 0.07 40.99	Gas/Vapor	EE	

15E	Used for fuel in 16E	V-3120	Dehydr ator Flash Gas 1	Used for Fuel in 16E or 13C&14 C	98% Control	С	8,760	VOC Total HAPs Benzene Toluene Ethylbenzene Xylenes n-Hexane CO2e	46.19 2.10 0.07 0.09 <0.0001 0.007 1.94 2501	205.1 9.19 0.30 0.38 0.0002 0.03 9.33 10296	0.94 0.04 0.001 0.002 <0.0001 0.0001 0.04 49.10	4.10 0.18 0.006 0.008 <0.0001 0.0006 0.17 215.1	Gas/Vapor	EE	
16E	Upward Vertical Stack	F-3100	Dehydr ator Reboile r 1			С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	0.18 0.15 0.01 0.01 0.001 0.003 0.0001 176	0.81 0.68 0.04 0.06 0.005 0.02 0.0006 771	0.18 0.15 0.01 0.01 0.001 0.003 0.0001 176	0.81 0.68 0.04 0.06 0.005 0.02 0.0006 771	Gas/Vapor	EE	
17E	Upward Vertical Stack	V-3210	Dehydr ator Still Vent 2	12C	Flare- 98% Control	С	8,760	VOC Total HAPs Benzene Toluene Ethylbenzene Xylenes n-Hexane CO2e	23.46 4.49 0.94 2.10 0.002 0.56 0.88 454	102.8 19.65 4.13 9.22 0.01 2.45 3.85 1989	0.47 0.09 0.02 0.04 <0.0001 0.01 0.02 9.36	2.06 0.39 0.08 0.18 0.0002 0.05 0.07 40.99	Gas/Vapor	EE	
18E	Used for fuel in 19E	V-3220	Dehydr ator Flash Gas 2	Used for Fuel in 19E or 13C&14 C	98% Control	С	8,760	VOC Total HAPs Benzene Toluene Ethylbenzene Xylenes n-Hexane CO2e	46.19 2.10 0.07 0.09 <0.0001 0.007 1.94 2501	205.1 9.19 0.30 0.38 0.0002 0.03 9.33 10296	0.94 0.04 0.001 0.002 <0.0001 0.0001 0.04 49.10	4.10 0.18 0.006 0.008 <0.0001 0.0006 0.17 215.1	Gas/Vapor	EE	

19E	Upward Vertical Stack	F-3200	Dehydr ator Reboile r 2			С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	0.18 0.15 0.01 0.01 0.001 0.003 0.0001 176	0.81 0.68 0.04 0.06 0.005 0.02 0.0006 771	0.18 0.15 0.01 0.01 0.001 0.003 0.0001 176	0.81 0.68 0.04 0.06 0.005 0.02 0.0006 771	Gas/Vapor	EE	
20E	Upward Vertical Stack	TK- 9000	Settler Tank	13C	VRU- 98% capture	С	8,760	VOC Total HAPs CO2e	90.83 7.16 250	397.83 31.38 1096	1.82 0.14 5.20	7.96 0.63 23	Gas/Vapor	EE	
21E	Upward Vertical Stack	TK- 9200	Conden sate Tank 1	13C	VRU- 98% capture	С	8,760	VOC Total HAPs CO2e	0.65 0.05 1.83	2.86 0.23 8.02	0.013 0.001 0.04	0.057 0.005 0.16	Gas/Vapor	EE	
22E	Upward Vertical Stack	TK- 9210	Conden sate Tank 2	13C	VRU- 98% capture	С	8,760	VOC Total HAPs CO2e	0.65 0.05 1.83	2.86 0.23 8.02	0.013 0.001 0.04	0.057 0.005 0.16	Gas/Vapor	EE	
23E	Upward Vertical Stack	TK- 9100	Produc ed Water Tank 1	13C	VRU- 98% capture	С	8,760	VOC Total HAPs CO2e	0.04 0.003 0.11	0.18 0.01 0.50	0.0008 0.0001 0.002	0.004 0.0003 0.01	Gas/Vapor	EE	
24E	Upward Vertical Stack	TK- 9110	Produc ed Water Tank 2	13C	VRU- 98% capture	С	8,760	VOC Total HAPs CO2e	0.04 0.003 0.11	0.18 0.01 0.50	0.0008 0.0001 0.002	0.004 0.0003 0.01	Gas/Vapor	EE	
26E	Upward Vertical Stack	FL- 8300	Flare combu stion device 1			С	8,760	NOx CO VOC PM10 Total HAPs CO2e	   	   	0.33 1.78 0.0001 0.0001 3.4E-5 565	1.44 7.79 0.0004 0.0006 0.0001 2475	Gas/Vapor	EE	

27E	Upward Vertical Stack	CATHT 1	Catalyti c Heater	 	С	8,760	NOx CO	0.0029 0.0025	0.013 0.011	0.0029 0.0025	0.013 0.011	Gas/Vapor	EE	
	Stack		for Genera tor Fuel				VOC PM10	1.6 E-4 2.2 E-4		1.6 E-4 2.2 E-4	7.1 E-4 0.001			
							SO2	1.8 E-5	7.7 E-5	1.8 E-5	7.7 E-5			
							Total HAPs Formaldehyde	6 E-5 2 E-6	2.4 E-4 1 E-5	6 E-5 2 E-6	2.4 E-4 1 E-5			
							CO2e	2.82	12	2.82	12			
30E	Upward Vertical	FUEL1	Fuel Conditi oning	 	С	8,760	NOx CO	0.06 0.05	0.27 0.23	0.06 0.05	0.27 0.23			
	Stack		Heater				VOC	0.003	0.02	0.003	0.02			
							PM10	0.005	0.02	0.005	0.02			
							SO2	0.0004	0.005		0.005			
							Total HAPs	0.001	0.02	0.001	0.02			
							Formaldehyde		0.0002	5E-5	0.0002			
							CO2e	58.7	257	58.7	257			

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit emissions are not typically considered to be fugitive and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugitive emission activities.

<sup>&</sup>lt;sup>1</sup> Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.

<sup>&</sup>lt;sup>2</sup> Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (ie., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).

<sup>&</sup>lt;sup>3</sup> List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. **LIST** Acids, CO, CS<sub>2</sub>, VOCs, H<sub>2</sub>S, Inorganics, Lead, Organics, O<sub>3</sub>, NO, NO<sub>2</sub>, SO<sub>2</sub>, SO<sub>3</sub>, all applicable Greenhouse Gases (including CO<sub>2</sub> and methane), etc. **DO NOT LIST** H<sub>2</sub>O, N<sub>2</sub>O, O<sub>2</sub>, and Noble Gases.

<sup>&</sup>lt;sup>4</sup> Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

<sup>&</sup>lt;sup>5</sup> Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

<sup>6</sup> Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmv) are used. If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m³) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO<sub>2</sub>, use units of ppmv (See 45CSR10).

# Attachment J EMISSION POINTS DATA SUMMARY SHEET

			Table 2: Re	lease Paramete	· Data			
Emission	Inner		Exit Gas		Emission Point Ele	vation (ft)	UTM Coordinate	s (km)
Point ID No.	Diameter (ft.)	Temp. (°F)	Volumetric Flow <sup>1</sup> (acfm)	Velocity (fps)	Ground Level (Height above MSL)	Stack Height <sup>2</sup>	Northing	Easting
1E/1C	1.1	1226	8820	187	1,194	TBD	4352.341	501.841
2E/2C	1.1	1226	8820	187	1,194	TBD	4352.348	501.835
3E/3C	1.1	1226	8820	187	1,194	TBD	4352.356	501.829
4E/4C	1.1	1226	8820	187	1,194	TBD	4352.364	501.823
5E/5C	1.1	1226	8820	187	1,194	TBD	4352.372	501.817
6E/6C	1.1	1226	8820	187	1,194	TBD	4352.380	501.812
7E/7C	1.1	1226	8820	187	1,194	TBD	4352.387	501.806
8E/8C	1.1	1226	8820	187	1,194	TBD	4352.394	501.801
9E/9C	1.1	1226	8820	187	1,194	TBD	4352.401	501.795
10E/10C	1.1	1226	8820	187	1,194	TBD	4352.407	501.790
11E/11C	1.1	1226	8820	187	1,194	TBD	4352.413	501.784
12E	TBD	535	1.3 kg/s mass flow	TBD	1,194	TBD	4352.456	501.873
13E	TBD	535	1.3 kg/s mass flow	TBD	1,194	TBD	4352.452	501.880
28E	TBD	535	1.3 kg/s mass flow	TBD	1,194	TBD	4352.448	501.887
14E/12C/26E	5	1400	TBD	TBD	1,194	15	4352.444	501.904
15E	Combusted in	n 16E	TBD	TBD	1,194	TBD	4352.403	501.854
16E	TBD		TBD	TBD	1,194	TBD	4352.398	501.858
17E/12C/26E	5	1400	TBD	TBD	1,194	15	4352.444	501.904
18E	Combusted in	n 19E	N/A	N/A	1,194	N/A	4352.389	501.876
19E	TBD	TBD	N/A	N/A	1,194	N/A	4352.385	501.880
20E-24E/13C-14C	TBD	TBD	27.78	TBD	1,194	N/A	4352.340	501.901
27E	TBD	TBD	TBD	TBD	1,194	TBD	4352.460	501.885
30E	TBD	TBD	TBD	TBD	1,194	TBD	4352.351	501.858

<sup>&</sup>lt;sup>1</sup> Give at operating conditions. Include inerts. <sup>2</sup> Release height of emissions above ground level.

Attachment K. Fugitive Emissions Data Summary Sheet	

#### Attachment K

#### **FUGITIVE EMISSIONS DATA SUMMARY SHEET**

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not typically considered to be fugitive, and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET.

Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

	APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS
1.)	Will there be haul road activities?
	⊠ Yes □ No
	☐ If YES, then complete the HAUL ROAD EMISSIONS UNIT DATA SHEET.
2.)	Will there be Storage Piles?
I	☐ Yes ☐ No
	$\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ $
3.)	Will there be Liquid Loading/Unloading Operations?
	⊠ Yes □ No
	$oxed{oxed}$ If YES, complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET.
4.)	Will there be emissions of air pollutants from Wastewater Treatment Evaporation?
	☐ Yes ☐ No
	☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
5.)	Will there be Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, open-ended valves, sampling connections, flanges, agitators, cooling towers, etc.)?
	⊠ Yes □ No
	$\hfill \square$ If YES, complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS UNIT DATA SHEET.
6.)	Will there be General Clean-up VOC Operations?
	☐ Yes ☐ No
	☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
7.)	Will there be any other activities that generate fugitive emissions?
	⊠ Yes □ No
	☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form.
	ou answered "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions

Page 1 of 2 Revision 2/11

FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants - Chemical Name/CAS 1	Maximum Uncontrolled	Emissions <sup>2</sup>	Maximum Po	issions <sup>3</sup>	Est. Method Used <sup>4</sup>
		lb/hr	ton/yr	lb/hr	10.00	0000
Haul Road/Road Dust Emissions Paved Haul Roads	PM-10 PM-2.5	0.00 0.00	0.00 0.00	0.00 0.00		EE
Unpaved Haul Roads	PM-10 PM-2.5	0.21 0.02	0.90 0.09	0.21 0.02		EE
Storage Pile Emissions						
Loading/Unloading Operations	VOCs Total HAPs CO2e	46.22 3.76 130	4.56 0.37 12.79	46.22 3.76 130	0.37	EE
Wastewater Treatment Evaporation & Operations						
Equipment Leaks	VOCs Total HAPs CO2e	0.89 0.04 19.51	3.91 0.18 85.45	0.89 0.04 19.51	0.18	EE
General Clean-up VOC Emissions						
Other – Venting Episodes	VOCs Total HAPs CO2e	Does not apply	8.28 0.30 701	Does not apply		EE

<sup>&</sup>lt;sup>1</sup> List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS<sub>2</sub>, VOCs, H<sub>2</sub>S, Inorganics, Lead, Organics, O<sub>3</sub>, NO, NO<sub>2</sub>, SO<sub>2</sub>, SO<sub>3</sub>, all applicable Greenhouse Gases (including CO<sub>2</sub> and methane), etc. DO NOT LIST H<sub>2</sub>, H<sub>2</sub>O, N<sub>2</sub>, O<sub>2</sub>, and Noble Gases.

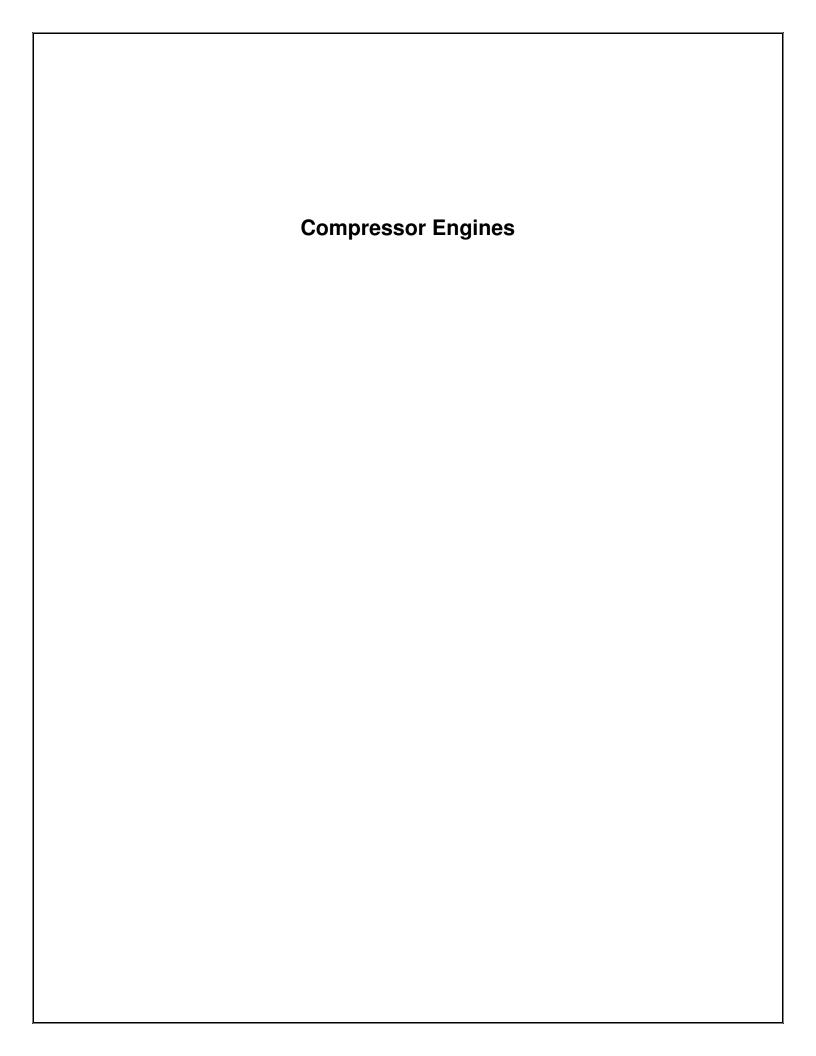
Page 2 of 2 Revision 2/11

<sup>&</sup>lt;sup>2</sup> Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

<sup>&</sup>lt;sup>3</sup> Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

<sup>&</sup>lt;sup>4</sup> Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

Attachment L.	
Emission Unit Data Sheets	



# NATURAL GAS COMPRESSOR/GENERATOR ENGINE DATA SHEET

Source Ide	Source Identification Number <sup>1</sup> 1E		2	2E		3E		
Engine Manufacturer and Model		Waukesha, 7044 GSI		Waukesha	Waukesha, 7044 GSI		Waukesha, 7044 GSI	
Manufactu	rer's Rated bhp/rpm	1680 bhp	/1200 rpm	1680 bhp	/1200 rpm	1680 bhp	1680 bhp/1200 rpm	
So	urce Status <sup>2</sup>	N	ИS	N	1S	N	1S	
Date Installe	d/Modified/Removed <sup>3</sup>	Septem	ber 2016	Septem	ber 2016	Septem	ber 2016	
Engine Manufact	ured/Reconstruction Date <sup>4</sup>	20	015	20	)15	20	)15	
Is this a Certified	Stationary Spark Ignition to 40CFR60 Subpart JJJJ?	1	No	1	No	No		
	Engine Type <sup>6</sup>	RI	B4S	RI	34S	RI	34S	
	APCD Type <sup>7</sup>	NS	SCR	NS	SCR	NS	SCR	
	Fuel Type <sup>8</sup>	F	PQ.	F	PQ.	F	PQ.	
Engine, Fuel and	H <sub>2</sub> S (gr/100 scf)		0		0		0	
Combustion Data	Operating bhp/rpm	1680 bhp/1200 rpm		1680 bhp	/1200 rpm	1680 bhp	/1200 rpm	
Data	BSFC (Btu/bhp-hr)	8,	289	8,	8,289		289	
	Fuel throughput (ft <sup>3</sup> /hr)	12,300		12,300		12,300		
	Fuel throughput (MMft <sup>3</sup> /yr)	10	7.75	10	7.75	107.75		
	Operation (hrs/yr)	8,	760	8,760		8,	760	
Reference <sup>9</sup>	Potential Emissions <sup>10</sup>	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr	
MD	NOx	1.26	5.52	1.26	5.52	1.26	5.52	
MD	СО	1.19	5.19	1.19	5.19	1.19	5.19	
MD	VOC	0.24	1.06	0.24	1.06	0.24	1.06	
AP	SO <sub>2</sub>	0.0082	0.036	0.0082	0.036	0.0082	0.036	
AP	PM <sub>10</sub>	0.27	1.18	0.27	1.18	0.27	1.18	
MD	Formaldehyde	0.019	0.081	0.019	0.081	0.019	0.081	

Source Ide	ntification Number <sup>1</sup>	4E		5E		6	6E	
Engine Mar	Engine Manufacturer and Model Waukesha		, 7044 GSI	Waukesha	, 7044 GSI	Waukesha	, 7044 GSI	
Manufactu	rer's Rated bhp/rpm	1680 bhp.	/1200 rpm	1680 bhp	/1200 rpm	1680 bhp/1200 rpi		
So	urce Status <sup>2</sup>	N	1S	N	IS	N	1S	
Date Installe	d/Modified/Removed <sup>3</sup>	Septeml	ber 2016	Septem	per 2016	Septem	ber 2016	
Engine Manufact	ured/Reconstruction Date <sup>4</sup>	20	)15	20	015	20	)15	
	Stationary Spark Ignition to 40CFR60 Subpart JJJJ?	N	No	N	lo	N	No	
	Engine Type <sup>6</sup>	RE	34S	RE	34S	RI	34S	
	APCD Type <sup>7</sup>	NS	CR	NS	CR	NS	SCR	
	Fuel Type <sup>8</sup>	P	'Q	P	Q	P	PQ	
Engine, Fuel and	H <sub>2</sub> S (gr/100 scf)	(	0		0		0	
Combustion Data	Operating bhp/rpm	1680 bhp.	1680 bhp/1200 rpm 1680 bhp/1200 rpm		/1200 rpm	1680 bhp/1200 rpm		
Data	BSFC (Btu/bhp-hr)	8,2	289	8,289		8,289		
	Fuel throughput (ft <sup>3</sup> /hr)	12,300		12,300		12,300		
	Fuel throughput (MMft <sup>3</sup> /yr)	107	7.75	107	7.75	107.75		
	Operation (hrs/yr)	8,760		8,7	760	8,	760	
Reference <sup>9</sup>	Potential Emissions <sup>10</sup>	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr	
MD	NO <sub>X</sub>	1.26	5.52	1.26	5.52	1.26	5.52	
MD	CO	1.19	5.19	1.19	5.19	1.19	5.19	
MD	VOC	0.24	1.06	0.24	1.06	0.24	1.06	
AP	SO <sub>2</sub>	0.0082	0.036	0.0082	0.036	0.0082	0.036	
AP	PM <sub>10</sub>	0.27	1.18	0.27	1.18	0.27	1.18	
MD	Formaldehyde	0.019	0.081	0.019	0.081	0.019	0.081	

Source Ide	entification Number <sup>1</sup>	7E		8	8E		ÞΕ
Engine Mar	nufacturer and Model	Waukesha, 7044 GSI		Waukesha, 7044 GSI		Waukesha, 7044 GSI	
Manufactu	rer's Rated bhp/rpm	1680 bhp	/1200 rpm	1680 bhp	/1200 rpm	1680 bhp/1200 rpn	
So	ource Status <sup>2</sup>	N	1S	N	1S	N	1S
Date Installe	d/Modified/Removed <sup>3</sup>	Septem	ber 2016	Septem	per 2016	Septem	ber 2016
Engine Manufact	tured/Reconstruction Date <sup>4</sup>	20	)15	20	015	20	)15
	Stationary Spark Ignition to 40CFR60 Subpart JJJJ?	N	No	N	lo	N	No
	Engine Type <sup>6</sup>	RE	34S	RE	34S	RI	34S
	APCD Type <sup>7</sup>	NS	CR	NS	CR	NS	SCR
	Fuel Type <sup>8</sup>	P	'Q	P	Q	P	PQ
Engine, Fuel and	H <sub>2</sub> S (gr/100 scf)		0		0		0
Combustion Data	Operating bhp/rpm	1680 bhp/1200 rpm 1680 bhp/1200 rpm 1680 b		1680 bhp	/1200 rpm		
Data	BSFC (Btu/bhp-hr) 8,289 8,289		289	8,289			
	Fuel throughput (ft <sup>3</sup> /hr)	12,300		12,300		12,300	
	Fuel throughput (MMft <sup>3</sup> /yr)	107	7.75	107	7.75	107.75	
	Operation (hrs/yr)	8,760		8,7	760	8,	760
Reference <sup>9</sup>	Potential Emissions <sup>10</sup>	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	$NO_X$	1.26	5.52	1.26	5.52	1.26	5.52
MD	CO	1.19	5.19	1.19	5.19	1.19	5.19
MD	VOC	0.24	1.06	0.24	1.06	0.24	1.06
AP	SO <sub>2</sub>	0.0082	0.036	0.0082	0.036	0.0082	0.036
AP	PM <sub>10</sub>	0.27	1.18	0.27	1.18	0.27	1.18
MD	Formaldehyde	0.019	0.081	0.019	0.081	0.019	0.081

Source Identification Number <sup>1</sup>		10E		11E			
Engine Manufacturer and Model		Waukesha, 7044 GSI		Waukesha, 7044 GSI			
Manufactur	er's Rated bhp/rpm	1680 bhp	/1200 rpm	1680 bhp	/1200 rpm		
Sou	urce Status <sup>2</sup>	N	AS .	N	1S		
Date Installed	d/Modified/Removed <sup>3</sup>	Septem	ber 2016	Septem	per 2016		
Engine Manufacti	ured/Reconstruction Date <sup>4</sup>	20	)15	20	)15		
Is this a Certified	Stationary Spark Ignition to 40CFR60 Subpart JJJJ?	Ν	No	N	lo		
	Engine Type <sup>6</sup>	RI	34S	RI	34S		
	APCD Type <sup>7</sup>	NS	SCR	NS	CR		
	Fuel Type <sup>8</sup>	P	PQ.	P	Q		
Engine, Fuel and	H <sub>2</sub> S (gr/100 scf)		0		0		
Combustion Data	Operating bhp/rpm	1680 bhp	/1200 rpm	1680 bhp/1200 rpm			
Data	BSFC (Btu/bhp-hr)	8,289		8,289			
	Fuel throughput (ft <sup>3</sup> /hr)	12,	,300	12,	300		
	Fuel throughput (MMft³/yr)	107.75		10′	7.75		
	Operation (hrs/yr)	8,	760	8,760			
Reference <sup>9</sup>	Potential Emissions <sup>10</sup>	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	$NO_X$	1.26	5.52	1.26	5.52		
MD	СО	1.19	5.19	1.19	5.19		
MD	VOC	0.24	1.06	0.24	1.06		
AP	SO <sub>2</sub>	0.0082	0.036	0.0082	0.036		
AP	PM <sub>10</sub>	0.27	1.18	0.27	1.18		
MD	Formaldehyde	0.019	0.081	0.019	0.081		

- 1. Enter the appropriate Source Identification Number for each natural gas-fueled reciprocating internal combustion compressor/generator engine located at the compressor station. Multiple compressor engines should be designated CE-1, CE-2, CE-3 etc. Generator engines should be designated GE-1, GE-2, GE-3 etc. If more than three (3) engines exist, please use additional sheets.
- 2. Enter the Source Status using the following codes:

NSConstruction of New Source (installation)ESExisting SourceMSModification of Existing SourceRSRemoval of Source

- 3. Enter the date (or anticipated date) of the engine's installation (construction of source), modification or removal.
- 4. Enter the date that the engine was manufactured, modified or reconstructed.
- 5. Is the engine a certified stationary spark ignition internal combustion engine according to 40CFR60 Subpart JJJJ. If so, the engine and control device must be operated and maintained in accordance with the manufacturer's emission-related written instructions. You must keep records of conducted maintenance to demonstrate compliance, but no performance testing is required. If the certified engine is not operated and maintained in accordance with the manufacturer's emission-related written instructions, the engine will be considered a non-certified engine and you must demonstrate compliance according to 40CFR§60.4243a(2)(i) through (iii), as appropriate.

#### Provide a manufacturer's data sheet for all engines being registered.

6. Enter the Engine Type designation(s) using the following codes:

LB2S Lean Burn Two Stroke RB4S Rich Burn Four Stroke LB4S Lean Burn Four Stroke

7. Enter the Air Pollution Control Device (APCD) type designation(s) using the following codes:

A/F Air/Fuel Ratio IR Ignition Retard

HEIS High Energy Ignition System SIPC Screw-in Precombustion Chambers

PSC Prestratified Charge LEC Low Emission Combustion

NSCR Rich Burn & Non-Selective Catalytic Reduction SCR Lean Burn & Selective Catalytic Reduction

8. Enter the Fuel Type using the following codes:

PQ Pipeline Quality Natural Gas RG Raw Natural Gas

9. Enter the Potential Emissions Data Reference designation using the following codes. Attach all referenced data to this *Compressor/Generator Data Sheet(s)*.

MD Manufacturer's Data AP AP-42
GR GRI-HAPCalc<sup>TM</sup> OT Other \_\_\_\_\_ (please list)

10. Enter each engine's Potential to Emit (PTE) for the listed regulated pollutants in pounds per hour and tons per year. PTE shall be calculated at manufacturer's rated brake horsepower and may reflect reduction efficiencies of listed Air Pollution Control Devices. Emergency generator engines may use 500 hours of operation when calculating PTE. PTE data from this data sheet shall be incorporated in the *Emissions Summary Sheet*.

Kaitlin Meszaros



# West Mountain Compressor Station - Ritchie County, WV

**VHP - L7044GSI** Gas Compression - Continuous

ENGINE SPEED (rpm):	1200		
DISPLACEMENT (in3):	7040	COOLING SYSTEM:	JW, IC + OC
COMPRESSION RATIO:	8:1	INTERCOOLER WATER INLET (°F):	130
IGNITION SYSTEM:	ESM	JACKET WATER OUTLET (°F):	180
EXHAUST MANIFOLD:	Water Cooled	JACKET WATER CAPACITY (gal):	100
COMBUSTION:	Rich Burn, Turbocharged	AUXILIARY WATER CAPACITY (gal):	11
ENGINE DRY WEIGHT (lbs):	21000	LUBE OIL CAPACITY (gal):	190
AIR/FUEL RATIO SETTING:	0.38% CO	MAX. EXHAUST BACKPRESSURE (in. H2O):	18
ENGINE SOUND LEVEL (dBA)	104	MAX. AIR INLET RESTRICTION (in. H2O):	15
		EXHAUST SOUND LEVEL (dBA)	111

SITE CONDITIONS:			
FUEL:		ALTITUDE (ft):	1194
FUEL PRESSURE RANGE (psig):	30 - 60	MAXIMUM INLET AIR TEMPERATURE (°F):	100
FUEL HHV (BTU/ft3):	1,250.1	FUEL WKI:	61.9
FUEL LUV (DTU/#2).	4 400 4		

FUEL LHV (BTU/ft3): 1,130.1						
SITE SPECIFIC TECHNICAL DATA			MAX RATING AT 100 °F	SITE RATING AT MAXIMUM INLET AIR TEMPERATURE OF 100 °F		
POWER RATING		UNITS	AIR TEMP	100%	75%	50%
CONTINUOUS ENGINE POWER OVERLOAD		BHP % 2/24 hr	1680 10	1680 10	1260 -	843
MECHANICAL EFFICIENCY (LHV)		%	30.7	30.7	29.5	28.6
CONTINUOUS POWER AT FLYWHEEL		ВНР	1680	1680	1260	843
based on no auxiliary engine driven equipment						
FUEL CONSUMPTION						
FUEL CONSUMPTION (LHV)		BTU/BHP-hr	8289	8289	8627	8912
FUEL CONSUMPTION (HHV)		BTU/BHP-hr	9169	9169	9544	9858
FUEL FLOW	based on fuel analysis LHV	SCFM	205	205	160	111
HEAT REJECTION						
JACKET WATER (JW)		BTU/hr x 1000	4164	4164	3402	2522
LUBE OIL (OC)		BTU/hr x 1000	572	572	520	434
INTERCOOLER (IC)		BTU/hr x 1000	271	271	185	92
EXHAUST		BTU/hr x 1000	4207	4207	3121	1924
RADIATION		BTU/hr x 1000	707	707	648	539
EMISSIONS						
NOx (NO + NO2)		g/bhp-hr	13.6	13.6	14.8	16.5
CO		g/bhp-hr	12.8	12.8	12.6	11.4
THC		g/bhp-hr	2.3	2.3	2.2	1.8
NMHC		g/bhp-hr	0.90	0.90	0.85	0.70
NM, NEHC		g/bhp-hr	0.41	0.41	0.39	0.32
CH4		g/bhp-hr	1.41	1.41	1.33	1.09
CO2		g/bhp-hr	527	527	549	567
CO2e		g/bhp-hr	557	557	577	590
CH2O		g/bhp-hr	0.05	0.05	0.05	0.05
AIR INTAKE / EXHAUST GAS						
INDUCTION AIR FLOW		SCFM	2550	2550	1991	1375
EXHAUST GAS MASS FLOW		lb/hr	11859	11859	9258	6395
EXHAUST GAS FLOW	at exhaust temp, 14.5 psia	ACFM	8876	8876	6727	4354
EXHAUST TEMPERATURE		°F	1224	1224	1175	1072

INDUCTION AIR FLOW		SCFM	2550	2550	1991	1375
EXHAUST GAS MASS FLOW		lb/hr	11859	11859	9258	6395
EXHAUST GAS FLOW	at exhaust temp, 14.5 psia	ACFM	8876	8876	6727	4354
EXHAUST TEMPERATURE		°F	1224	1224	1175	1072
LIEAT EXCLANACED ALTINIA						

HEAT EXHANGER SIZING		
TOTAL JACKET WATER CIRCUIT (JW)	BTU/hr x 1000	4722
TOTAL AUXILIARY WATER CIRCUIT (IC + OC)	BTU/hr x 1000	955
COOLING SYSTEM WITH ENGINE MOUNTED WATER DUMPS		

COOLING SYSTEM WITH ENGINE MOUNTED WATER PUMPS		
JACKET WATER PUMP MIN. DESIGN FLOW	GPM	450
JACKET WATER PUMP MAX. EXTERNAL RESTRICTION	psig	16
AUX WATER PUMP MIN. DESIGN FLOW	GPM	79
AUX WATER PUMP MAX. EXTERNAL RESTRICTION	psig	44



# West Mountain Compressor Station - Ritchie County, WV

**VHP - L7044GSI** 

nfelder Kaitlin Meszaros Gas Compression - Continuous

FUEL COMPOSITION					
HYDROCARBONS:	Mole or \	Volume %		FUEL:	
Methane	CH4	77.595		FUEL PRESSURE RANGE (psig):	30 - 60
Ethane	C2H6	14.268		FUEL WKI:	61.9
Propane	C3H8	4.142			
Iso-Butane	I-C4H10	0.57		FUEL SLHV (BTU/ft3):	1110.46
Normal Butane	N-C4H10	1.047		FUEL SLHV (MJ/Nm3):	43.67
Iso-Pentane	I-C5H12	0.31		,	
Normal Pentane	N-C5H12	0.31		FUEL LHV (BTU/ft3):	1130.12
Hexane	C6H14	0.27		FUEL LHV (MJ/Nm3):	44.44
Heptane	C7H16	0.2			
Ethene	C2H4	0		FUEL HHV (BTU/ft3):	1250.13
Propene	C3H6	0		FUEL HHV (MJ/Nm3):	49.16
	33.13	·		. 522 (6/ ).	
	SUM HYDROCARBONS	98.712		FUEL DENSITY (SG):	0.71
NON-HYDROCARBONS:					
Nitrogen	N2	0.792		Standard Conditions per ASTM D3588-91 [60°F an	id 14.696psia] and ISO
Oxygen	O2	0		6976:1996-02-01[25, V(0;101.325)].	d tomporature liquid
Helium	He	0		Based on the fuel composition, supply pressure an hydrocarbons may be present in the fuel. No liquid	
Carbon Dioxide	CO2	0.205		in the fuel. The fuel must not contain any liquid wat	
Carbon Monoxide	CO	0		Waukesha recommends both of the following:	
Hydrogen	H2	0		<ol> <li>Dew point of the fuel gas to be at least 20°F (11° temperature of the gas at the inlet of the engine fue</li> </ol>	
Water Vapor	H2O	0		A fuel filter separator to be used on all fuels exce	
·				natural gas.	
	TOTAL FUEL	99.709		Refer to the 'Fuel and Lubrication' section of 'Techr Waukesha Application Engineering Department for	
				fuels, or LHV and WKI* calculations.	additional information on
				* Trademark of General Electric Company	
-					
FUEL CONTAMINANTS					
Total Sulfur Compounds		0	% volume	Total Sulfur Compounds	0 μg/BTU
Total Halogen as Cloride		0	% volume	Total Halogen as Cloride	0 μg/BTU
Total Ammonia		0	% volume	Total Ammonia	0 μg/BTU
Siloxanes				Total Siloxanes (as Si)	0 μg/BTU
Tetramethyl silane		0	% volume		
Trimethyl silanol		0	% volume		
Hexamethyldisiloxane (L2)		0	% volume	Calculated fuel contaminant analysis	will depend on the
Hexamethylcyclotrisiloxane (D3)		0	% volume	entered fuel composition and selected	d engine model.
Octamethyltrisiloxane (L3)		0	% volume		
Octamethylcyclotetrasiloxane (D4)	)	0	% volume		
Decamethyltetrasiloxane (L4)		0	% volume		
Decamethylcyclopentasiloxane (D	5)	0	% volume		
Dodecamethylpentasiloxane (L5)		0	% volume		
Dodecamethylcyclohexasiloxane (	[D6)	0	% volume		
Others		0	% volume		

No water or hydrocarbon condensates are allowed in the engine. Requires liquids removal.

#### GE Power & Water

# 98)

#### West Mountain Compressor Station - Ritchie County, WV

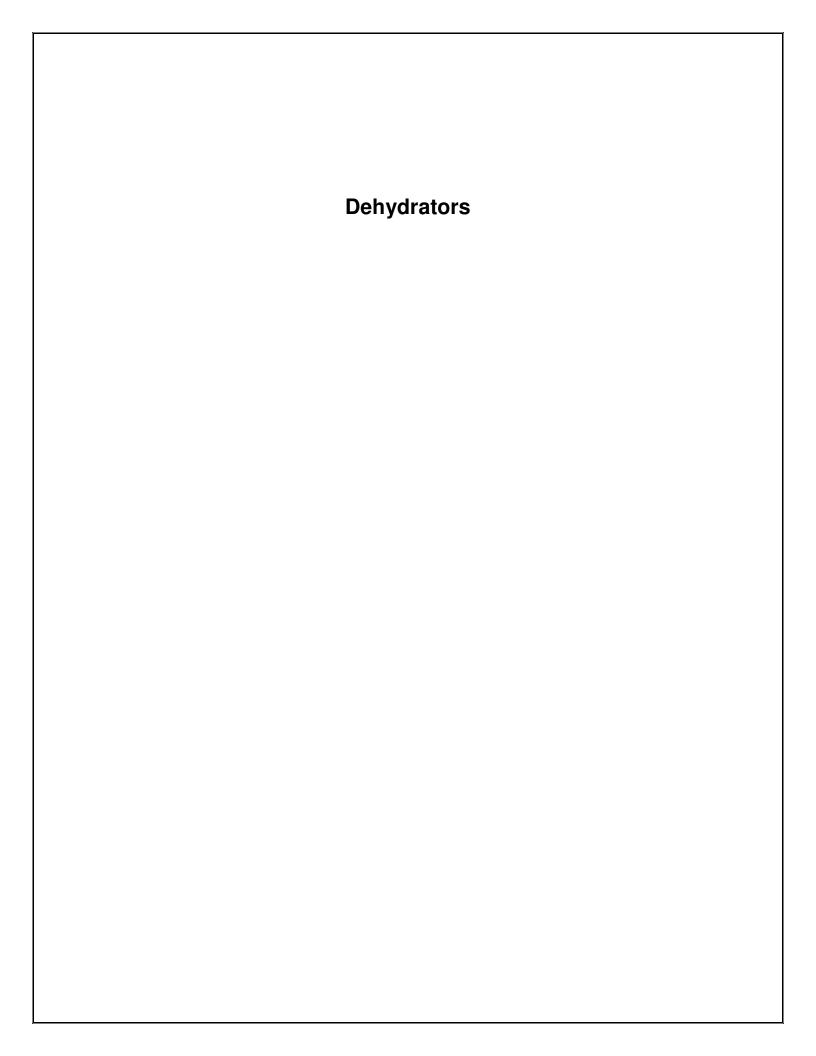
Kleinfelder Kaitlin Meszaros

VHP - L7044GSI
Gas Compression - Continuous

#### **NOTES**

- 1. All data is based on engines with standard configurations unless noted otherwise.
- 2. Power rating is adjusted for fuel, site altitude, and site air inlet temperature, in accordance with ISO 3046/1 with tolerance of ± 3%
- 3. Fuel consumption is presented in accordance with ISO 3046/1 with a tolerance of -0 / +5% at maximum rating. Fuel flow calculation based on fuel LHV and fuel consumption with a tolerance of -0/+5%. For sizing piping and fuel equipment, it is recommended to include the 5% tolerance.
- 4. Heat rejection tolerances are ± 30% for radiation, and ± 8% for jacket water, lube oil, intercooler, and exhaust energy.
- 5. Emission levels are given at engine exhaust outlet flange prior to any after treatment. Values are based on a new engine operating at indicated site conditions, and adjusted to the specified timing and air/fuel ratio at rated load. Emissions are at an absolute humidity of 75 grains H2O/lb (10.71 g H2O/kg) of dry air. Emission levels may vary subject to instrumentation, measurement, ambient conditions, fuel quality, and engine variation. Engine may require adjustment on-site to meet emission values, which may affect engine performance and heat output. NOx, CO, THC, and NMHC emission levels are listed as a not to exceed limit, all other emission levels are estimated. CO2 emissions based on EPA Federal Register/Vol. 74, No. 209/Friday, October 30, 2009 Rules and Regulations 56398, 56399 (3) Tier 3 Calculation Methodology, Equation C-5.
- 6. Air flow is based on undried air with a tolerance of ± 7%.
- 7. Exhaust temperature given at engine exhaust outlet flange with a tolerance of ± 75°F (42°C).
- 8. Exhaust gas mass flow value is based on a "wet basis" with a tolerance of ± 7%.
- 9. Inlet air restrictions based on full rated engine load. Exhaust backpressure based on 158 PSI BMEP and 1200 RPM. Refer to the engine specification section of Waukesha's standard technical data for more information.
- 10. Cooling circuit capacity, lube oil capacity, and engine dry weight values are typical.
- 11. Fuel must conform to Waukesha's "Gaseous Fuel Specification" S7884-7 or most current version. Fuel may require treatment to meet current fuel specification.
- 12. Heat exchanger sizing values given as the maximum heat rejection of the circuit, with applied tolerances and an additional 5% reserve factor.
- 13. Fuel volume flow calculation in english units is based on 100% relative humidity of the fuel gas at standard conditions of 60°F and 14.696 psia (29.92 inches of mercury: 101.325 kPa).
- 14. Fuel volume flow calculation in metric units is based on 100% relative humidity of the fuel gas at a combustion temperature of 25°C and metering conditions of 0°C and 101.325 kPa (14.696 psia; 29.92 inches of mercury). This is expressed as [25, V(0;101.325)].
- 15. Engine sound data taken with the microphone at 1 m (3.3 ft) from the side of the engine at the approximate front-to-back centerline. Microphone height was at intake manifold level. Engine sound pressure data may be different at front, back and opposite side locations. Exhaust sound data taken with microphone 1 meter (3.3 ft) away and 1 meter (3.3 ft) to the side of the exhaust outlet.
- 16. Due to variation between test conditions and final site conditions, such as exhaust configuration and background sound level, sound pressure levels under site conditions may be different than those tabulated above.
- 17. Cooling system design flow is based on minimum allowable cooling system flow. Cooling system maximum external restriction is defined as the allowable restriction at the minimum cooling system flow. Refer to technical data sheets S-5136-34 and S-6543-36 (or latest version) for more information.
- 18. Continuous Power Rating: The highest load and speed that can be applied 24 hours per day, seven days per week, 365 days per year except for normal maintenance at indicated ambient reference conditions and fuel. It is permissible to operate the engine at the indicated overload power, for two hours in every 24 hour period.

#### REQUIRED OPTION CODES



# NATURAL GAS GLYCOL DEHYDRATION UNIT DATA SHEET

		Manufact	urer and Model	Valerus, 72	.5 MMscfd	
		Max Dry Gas Fl	ow Rate (MMscf/day)	72	5	
		Design Heat	Input (MMBtu/hr)	1.5		
		Design Typ	e (DEG or TEG)	TE	EG	
	Glycol	Sour	ce Status <sup>2</sup>	M	S	
Dehydra Da		Date Installed/	Modified/Removed <sup>3</sup>	Septemb	per 2016	
		Regenerator	Still Vent APCD <sup>4</sup>	F	L	
		Fuel H	IV (Btu/scf)	1,1	30	
		H <sub>2</sub> S Cont	ent (gr/100 scf)	(	)	
		Opera	tion (hrs/yr)	8,7	60	
Source ID #1	Vent	Reference <sup>5</sup>	Potential Emissions <sup>6</sup>	lbs/hr	tons/yr	
		AP	NO <sub>X</sub>	0.18	0.81	
		AP	СО	0.15	0.68	
16E	Reboiler Vent	AP	VOC	0.010	0.044	
		AP	SO <sub>2</sub>	0.0011	0.0048	
		AP	$PM_{10}$	0.014	0.061	
		GRI-GLYCalc <sup>TM</sup>	VOC	0.47	2.06	
		GRI-GLYCalc <sup>TM</sup>	Benzene	0.019	0.082	
14E	Glycol Regenerator	GRI-GLYCalc <sup>™</sup>	Ethylbenzene	0.000	0.0002	
1412	Still Vent	GRI-GLYCalc <sup>™</sup>	Toluene	0.042	0.18	
		GRI-GLYCalc <sup>TM</sup>	Xylenes	0.011	0.049	
		GRI-GLYCalc <sup>TM</sup>	n-Hexane	0.018	0.077	
		GRI-GLYCalc <sup>TM</sup>	VOC	0.94	4.10	
		GRI-GLYCalc <sup>™</sup>	Benzene	0.0014	0.0059	
15E	Flash Gas	GRI-GLYCalc <sup>TM</sup>	Ethylbenzene	0.000	0.000	
1,712	Tank Vent	GRI-GLYCalc <sup>TM</sup>	Toluene	0.0017	0.0075	
		GRI-GLYCalc <sup>™</sup>	Xylenes	0.0001	0.0006	
		GRI-GLYCalc <sup>™</sup>	n-Hexane	0.039	0.17	

		Manufacturer and Model		Valerus, 72	.5 MMscfd
		Max Dry Gas Flow Rate (mmscf/day)		72	5
		Design Heat Input (mmBtu/hr)		1.5	
		Design Typ	e (DEG or TEG)	TEG	
	Glycol	Sour	ce Status <sup>2</sup>	M	S
	tion Unit ata	Date Installed/	Modified/Removed <sup>3</sup>	Septemb	per 2016
		Regenerator	Still Vent APCD <sup>4</sup>	F	L
		Fuel H	IV (Btu/scf)	1,1	30
		H <sub>2</sub> S Cont	ent (gr/100 scf)	(	)
		Opera	tion (hrs/yr)	8,7	60
Source ID #1	Vent	Reference <sup>5</sup>	Potential Emissions <sup>6</sup>	lbs/hr	tons/yr
		AP	NO <sub>X</sub>	0.18	0.81
		AP	СО	0.15	0.68
19E	Reboiler Vent	AP	VOC	0.010	0.044
		AP	$SO_2$	0.0011	0.0048
		AP	$PM_{10}$	0.014	0.061
		GRI-GLYCalc <sup>TM</sup>	VOC	0.47	2.06
		GRI-GLYCalc™	Benzene	0.019	0.082
17E	Glycol 17E Regenerator	GRI-GLYCalc™	Ethylbenzene	0.000	0.0002
1/12	Still Vent	GRI-GLYCalc™	Toluene	0.042	0.18
		GRI-GLYCalc™	Xylenes	0.011	0.049
		GRI-GLYCale <sup>TM</sup>	n-Hexane	0.018	0.077
		GRI-GLYCalc <sup>TM</sup>	VOC	0.94	4.10
		GRI-GLYCalc <sup>TM</sup>	Benzene	0.0014	0.0059
18E	Flash Gas	GRI-GLYCalc <sup>TM</sup>	Ethylbenzene	0.000	0.000
1012	Tank Vent	GRI-GLYCalc <sup>™</sup>	Toluene	0.0017	0.0075
		GRI-GLYCalc <sup>™</sup>	Xylenes	0.0001	0.0006
		GRI-GLYCalc <sup>™</sup>	n-Hexane	0.039	0.17

- 1. Enter the appropriate Source Identification Numbers for the glycol dehydration unit Reboiler Vent and glycol Regenerator Still Vent. The glycol dehydration unit Reboiler Vent and glycol Regenerator Still Vent should be designated RBV-1 and RSV-1, respectively. If the compressor station incorporates multiple glycol dehydration units, a *Glycol Dehydration Unit Data Sheet* shall be completed for each, using Source Identification #s RBV-2 and RSV-2, RBV-3 and RSV-3, etc.
- 2. Enter the Source Status using the following codes:

NS Construction of New Source ES Existing Source
MS Modification of Existing Source RS Removal of Source

	modification	or removal.			
4.	Enter the Air	Pollution Control Device	(APCD) type designation u	using the following	ng codes:
	NA	None	CD	Condenser	
	FL	Flare	CC	Condenser/Cor	mbustion Combination
	TO	Thermal Oxidizer			
5.	Enter the Po	tential Emissions Data Re	ference designation using th	e following code	s:
	MD	Manufacturer's Data	AP	AP-42	
	GR	GRI-GLYCalc <sup>TM</sup>	OT	Other	(please list)

3. Enter the date (or anticipated date) of the glycol dehydration unit's installation (construction of source),

6. Enter the Reboiler Vent and glycol Regenerator Still Vent Potential to Emit (PTE) for the listed regulated pollutants in lbs per hour and tons per year. The glycol Regenerator Still Vent potential emissions may be determined using the most recent version of the thermodynamic software model GRI-GLYCalc<sup>TM</sup> (Radian International LLC & Gas Research Institute). Attach all referenced Potential Emissions Data (or calculations) and the GRI-GLYCalc Aggregate Calculations Report to this Glycol Dehydration Unit Data Sheet(s). This PTE data shall be incorporated in the Emissions Summary Sheet.

Include a copy of the GRI-GLYCalc $^{\rm TM}$  analysis. This includes a printout of the aggregate calculations report, which shall include emissions reports, equipment reports, and stream reports.

\*An explanation of input parameters and examples, when using GRI-GLYCalc<sup>TM</sup> is available on our website.

## West Virginia Department of Environmental Protection

# **Division of Air Quality**

# 40 CFR Part 63; Subpart HH & HHH Registration Form

DIVISION OF AIR QUALITY: (304) 926-0475

Web Page: http://www.wvdep.org

Complete this form for any oil and natural gas production or natural gas transmission and storage facility that uses an affected unit under HH/HHH, whether subject or not.

Section A: Facility Description				
Affected facility actual annual average natural gas throughput (scf/day): 145,000,000				
Affected facility actual annual average hydrocarbon liquid throughput: (bbl/day): 195				
The affected facility processes, upgrades, or stores hydrocarbon liquids prior to custody transfer.  Yes  No				
The affected facility processes, upgrades, or stores natural gas prior to the point at which natural gas  No				
(NG) enters the NG transmission and storage source category or is delivered to the end user.				
The affected facility is:  prior to a NG processing plant  a NG processing plant				
prior to the point of custody transfer and there is no NG processing plant				
The affected facility transports or stores natural gas prior to entering the pipeline to a local Yes No				
distribution company or to a final end user (if there is no local distribution company).				
The affected facility exclusively processes, stores, or transfers black oil.  Yes				
Initial producing gas-to-oil ratio (GOR):scf/bbl API gravity:degrees				
Section B: Dehydration Unit (if applicable) 1				
Description: West Mountain Compressor Station Dehydrators (V-3110 & V-3210)				
Date of Installation: 2015 Annual Operating Hours: 8,760 Burner rating (MMbtu/hr): 1.5				
Exhaust Stack Height (ft): NA Stack Diameter (ft): NA Stack Temp. (°F): NA				
Glycol Type: 🛛 TEG 🔲 EG 🔲 Other:				
Glycol Pump Type:   Electric   Gas If gas, what is the volume ratio?0.032ACFM/gpm				
Condenser installed?				
Incinerator/flare installed?				
Other controls installed?				
Wet Gas <sup>2</sup> : Gas Temp.: _120_°F Gas Pressure _1,100 psig				
(Upstream of Contact Tower) Saturated Gas? Yes No If no, water content lb/MMSCF				
Dry Gas: Gas Flowrate(MMSCFD) Actual Design72.5 each				
(Downstream of Contact Tower) Water Content5.0 lb/MMSCF				
Lean Glycol: Circulation rate (gpm) Actual <sup>3</sup> Maximum <sup>4</sup> 7.5				
Pump make/model: Kimray 45015PV				
Glycol Flash Tank (if applicable): Temp.:80°F Pressure5 psig Vented? Yes \[ \sqrt{No} \sqrt{N}				
If no, describe vapor control: Vent gas used in reboiler as fuel and as backup would go to				
the VRU system via the storage tanks.				
Stripping Gas (if applicable): Source of gas: Dry gas, if used Rate _9_ scfm				

1.	applicant provide thi	ng the chain of custody in s level of detail for all sour	the following required dehydration unit information:  formation. See Page 43 of this document for an example of a gas flow schematic. It is not intended that the case. The level of detail that is necessary is to establish where the custody transfer points are located. This can be trained custody transfer points and the natural gas flow. However, the DAO reserves the right to request		
2.	accomplished by submitting a process flow diagram indicating custody transfer points and the natural gas flow. However, the DAQ reserves the right to request more detailed information in order to make the necessary decisions.  Extended gas analysis from the Wet Gas Stream including mole percents of C <sub>1</sub> -C <sub>8</sub> , benzene, ethylbenzene, toluene, xylene and n-Hexane, using Gas Processors Association (GPA) 2286 (or similar). A sample should be taken from the inlet gas line, downstream from any inlet separator, and using a manifold to remove entrained liquids from the sample and a probe to collect the sample from the center of the gas line. GPA standard 2166 reference method or a modified version of				
3.	GRI-GLYCalc Ver.		on maximum Lean Glycol circulation rate and maximum throughput.		
4.	Detailed calculations	of gas or hydrocarbon flov	on C: Facility NESHAPS Subpart HH/HHH status		
	Subject to Subpart HH - applies, but is exempt through < 1 tpy benzene exemption				
A	Affected facility Subject to Subpart HHH				
	status:				
(ch	noose only one)	because:	Affected facility exclusively handles black oil		
			☐ The facility wide actual annual average NG throughput is < 650 thousand		

☐ No affected source is present

scf/day and facility wide actual annual average hydrocarbon liquid is  $<\!250~\text{bpd}$ 

Fu	uel Conditioning Heater
1	

# Attachment L EMISSIONS UNIT DATA SHEET GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form):

Name or type and model of proposed affected source:
1. Name of type and model of proposed affected source.
Fuel Conditioning Heater - 500,000 Btu/hr
2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all
features of the affected source which may affect the production of air pollutants.
3. Name(s) and maximum amount of proposed process material(s) charged per hour:
N. ( ) 1 C
Natural Gas as fuel - 613 scf/hr
4. Name(s) and maximum amount of proposed material(s) produced per hour:
(e) produces per record
Heater is used to increase temperature of fuel before use by the compressor engines to allow more complete
combustion.
Comoustion
E. Civa abamical reactions if applicable, that will be involved in the generation of air pollutants.
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:
Combustion process

\* The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

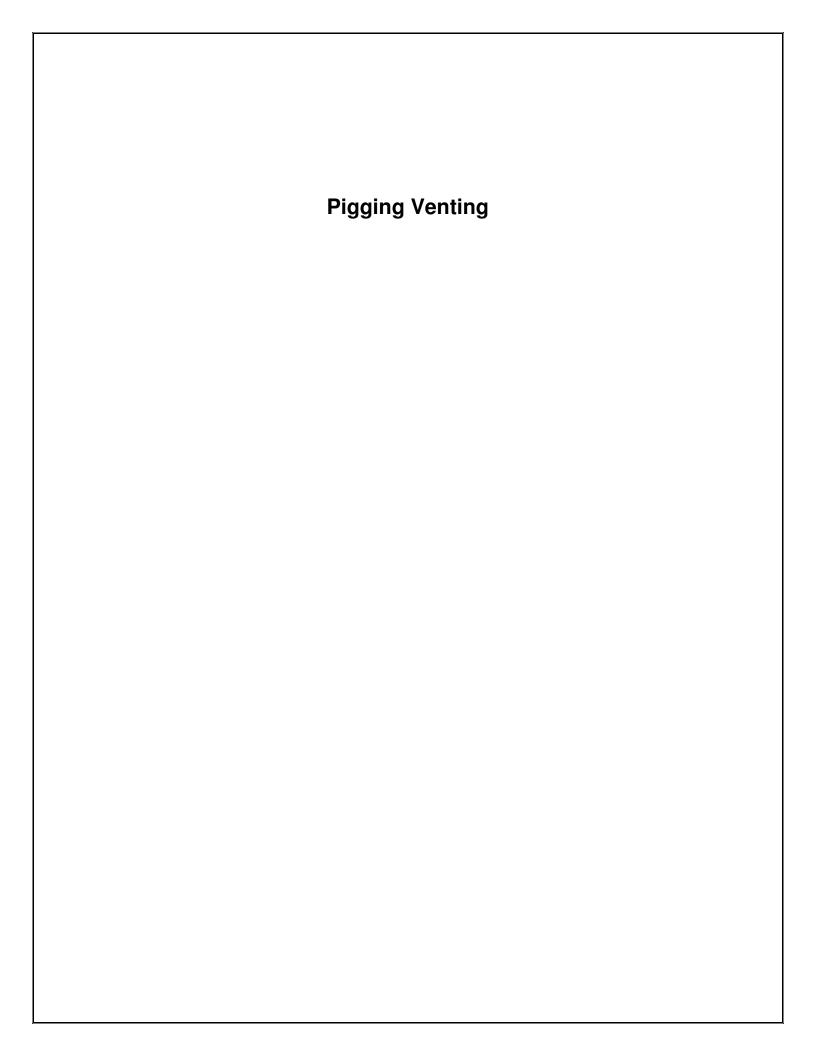
6.	Со	mbustion Data (if applic	able):			
	(a)	Type and amount in ap	propriate units of fu	el(s) to be bu	rned:	
Na	tura	l gas as fuel - 613 scf/hr				
	(b)	Chemical analysis of pland ash:	roposed fuel(s), exc	luding coal, in	cluding maxim	um percent sulfur
		and asm.				
Sa	me a	as onsite gas analysis - see A	ttachment N			
	(c)	Theoretical combustion	air requirement (A	CF/unit of fue	l)·	
	(0)		ran roquiromoni (r		.,,.	
		@		°F and		psia.
	(d)	Percent excess air:				
	(e)	Type and BTU/hr of bu	rners and all other f	iring equipme	nt planned to b	e used:
<b></b>	0.00	00 D. H. N				
50	0,00	00 Btu/hr. Natural gas.				
	(f)	If coal is proposed as a	source of fuel, ider	ntify supplier a	and seams and	give sizing of the
		coal as it will be fired:				
	(g)	Proposed maximum de	esign heat input:			× 10 <sup>6</sup> BTU/hr.
7.	Pro	jected operating sched	ule:			
Ηοι	ırs/	Day 24	Days/Week	7	Weeks/Year	52

8.	Projected amount of pollutants that would be emitted from this affected source if no control devices were used:			
@		°F and	I	psia
a.	NOx	0.061	lb/hr	grains/ACF
b.	SO <sub>2</sub>	0.00037	lb/hr	grains/ACF
c.	СО	0.051	lb/hr	grains/ACF
d.	PM <sub>10</sub>	0.0047	lb/hr	grains/ACF
e.	Hydrocarbons		lb/hr	grains/ACF
f.	VOCs	0.0034	lb/hr	grains/ACF
g.	Pb		lb/hr	grains/ACF
h.	Specify other(s)			
	Total HAP (including HCHO)	0.000046	lb/hr	grains/ACF
	CO2e	58.7	lb/hr	grains/ACF
			lb/hr	grains/ACF
			lb/hr	grains/ACF

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

<sup>(2)</sup> Complete the Emission Points Data Sheet.

<ol> <li>Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.</li> </ol>			
MONITORING	RECORDKEEPING		
see Attachment O	see Attachment O		
DEDORTING	TEOTINO		
REPORTING	TESTING		
see Attachment O	see Attachment O		
	E PROCESS PARAMETERS AND RANGES THAT ARE STRATE COMPLIANCE WITH THE OPERATION OF THIS CONTROL DEVICE.		
<b>RECORDKEEPING.</b> PLEASE DESCRIBE THE PROPMONITORING.	POSED RECORDKEEPING THAT WILL ACCOMPANY THE		
REPORTING. PLEASE DESCRIBE THE PRO	POSED FREQUENCY OF REPORTING OF THE		
	PROJED INEQUENCT OF REPORTING OF THE		
RECORDKEEPING.			
<b>TESTING.</b> PLEASE DESCRIBE ANY PROPOSED EMISPOLLUTION CONTROL DEVICE.	SSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR		
10 Describe all operating ranges and mainter	nance procedures required by Manufacturer to		
maintain warranty	iance procedures required by manaractarer to		
mamam wananty			



# Attachment L EMISSIONS UNIT DATA SHEET GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form): Fugitive so no number assigned

Name or type and model of proposed affected source:
Fugitive emissions from venting episodes such as plant shutdowns and compressor start ups/shut downs.
<ol> <li>On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of al features of the affected source which may affect the production of air pollutants.</li> </ol>
3. Name(s) and maximum amount of proposed process material(s) charged per hour:
4. Name(s) and maximum amount of proposed material(s) produced per hour:
- compressor blowdown - 0.048 tons VOC per event, 4.10 tons CO2e per event - compressor startup - 0.005 tons VOC per event, 0.43 tons CO2e per event - plant shutdown - 0.485 tons VOC per event, 41.01 tons CO2e per event - pigging venting - 0.005 tons VOC per event, 0.41 tons CO2e per event
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants
none

\* The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

6.	Combustio	n Data (if applic	able):			
	(a) Type a	nd amount in ap	propriate units o	f fuel(s) to be bu	rned:	
			oposed fuel(s),	excluding coal, in	cluding maxim	um percent sulfur
	and asl	n:				
	(c) Theore	tical combustion	air requirement	(ACF/unit of fue	 l):	
	(0)				.,.	
		@		°F and		psia.
	(d) Percen	t excess air:				
	(e) Type a	nd BTU/hr of bu	rners and all oth	er firing equipme	ent planned to t	be used:
	(f) If coal i	s proposed as a	source of fuel i	dentify supplier a	and seams and	give sizing of the
		it will be fired:		donary dapping, c	and obanno and	give eizing er are
	(g) Propos	ed maximum de	sign heat input:			× 10 <sup>6</sup> BTU/hr.
7.	Projected of	perating schedu	ule:			
	•	not a regular		not a regular	Weeks/Year	not a regular
пО	urs/Day	schedule	Days/Week	schedule	vveeks/ rear	schedule

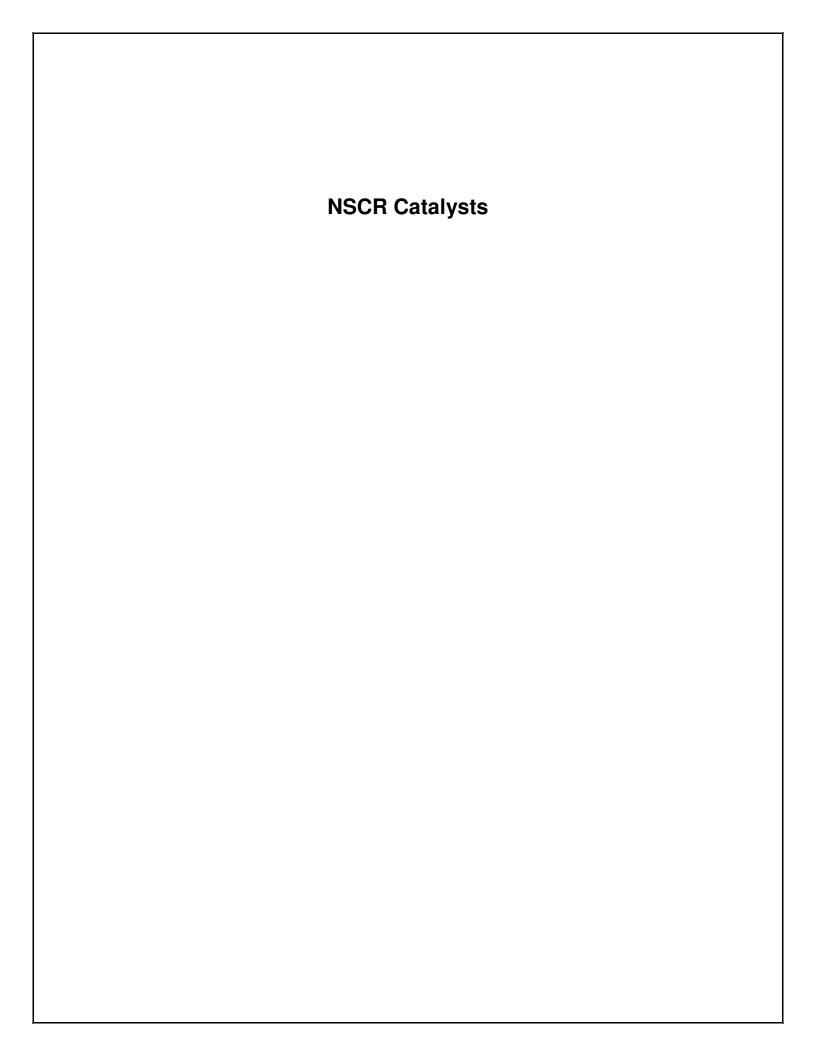
8.	3. Projected amount of pollutants that would be emitted from this affected source if no control devices were used:				
@	@ venting events are uncontrolled °F and psia				
a.	NOx	lb/hr	grains/ACF		
b.	SO <sub>2</sub>	lb/hr	grains/ACF		
c.	CO	lb/hr	grains/ACF		
d.	PM <sub>10</sub>	lb/hr	grains/ACF		
e.	Hydrocarbons	lb/hr	grains/ACF		
f.	VOCs	lb/hr	grains/ACF		
g.	Pb	lb/hr	grains/ACF		
h.	Specify other(s)				
		lb/hr	grains/ACF		
		lb/hr	grains/ACF		
		lb/hr	grains/ACF		
		lb/hr	grains/ACF		

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

(2) Complete the Emission Points Data Sheet.

	and reporting in order to demonstrate compliance Please propose testing in order to demonstrate
	· · - · · · · · · · · · · · · · · · ·
see Attachment O	see Attachment O
REPORTING	TESTING
see Attachment O	see Attachment O
MONITORING. PLEASE LIST AND DESCRIBE THE PROPOSED TO BE MONITORED IN ORDER TO DEMON PROCESS EQUIPMENT OPERATION/AIR POLLUTION	
<b>RECORDKEEPING.</b> PLEASE DESCRIBE THE PROPMONITORING.	OSED RECORDKEEPING THAT WILL ACCOMPANY THE
<b>REPORTING.</b> PLEASE DESCRIBE THE PRORECTOR RECORD KEEPING.	DPOSED FREQUENCY OF REPORTING OF THE
TESTING. PLEASE DESCRIBE ANY PROPOSED EMI	
POLLUTION CONTROL DEVICE.	SSIONS LESTING FOR THIS PROCESS EQUIPMENT/AIR
	nance procedures required by Manufacturer to
maintain warranty N/A	iando procederes required by Manarastaror to

Attachment M. Air Pollution Control Device Sheets	



# Attachment M Air Pollution Control Device Sheet

(OTHER COLLECTORS)

Control Device ID No. (must match Emission Units Table): 1C - 11C

#### **Equipment Information**

1.	Manufacturer: EMIT Technologies Model No. RT-3615-T		<ol> <li>Control Device Name: 1C – 11C –         Catalysts for C-2100 through C-2200         Type: NSCR Catalyst     </li> </ol>							
3.	Provide diagram(s) of unit describing capture system with duct arrangement and size of duct, air volume, capacity, horsepower of movers. If applicable, state hood face velocity and hood collection efficiency.									
4.	On a separate sheet(s) supply all data and ca	alculatio	ns used in selecting or de	esigning this collection device.						
5.	Provide a scale diagram of the control device	showin	g internal construction.							
6.	Submit a schematic and diagram with dimens	sions an	d flow rates.							
7. N/A	7. Guaranteed minimum collection efficiency for each pollutant collected: N/A – no capture of pollutants									
8.	8. Attached efficiency curve and/or other efficiency information.									
9.	Design inlet volume: 8,820	ACFM	10. Capacity:							
	11. Indicate the liquid flow rate and describe equipment provided to measure pressure drop and flow rate, if any. N/A									
12.	Attach any additional data including auxilia control equipment.	ry equip	oment and operation de	tails to thoroughly evaluate the						
	13. Description of method of handling the collected material(s) for reuse of disposal.  Replace Catalyst elements when necessary									
	Gas Si	tream C	Characteristics							
14.	Are halogenated organics present? Are particulates present? Are metals present?		<ul> <li>☐ Yes</li> <li>☐ No</li> <li>☐ Yes</li> <li>☐ No</li> </ul>							
15.	Inlet Emission stream parameters:		Maximum	Typical						
	Pressure (mmHg):		Not specified							
	Heat Content (BTU/scf):		1,400	1,130						
	Oxygen Content (%):		Not specified							
	Moisture Content (%):		Not specified							
	Relative Humidity (%):		Not specified							

Page 1 of 4 REVISED 03/15/2007

16.	Type of pollutant(s) o ☐ Particulate (type)		□ SO <sub>x</sub>	☐ Odor ☑ Other NOx	, CO, VOC, HCI	HO, CH4			
17.	Inlet gas velocity:		187 ft/sec	18. Pollutant	specific gravity:				
19.	Gas flow into the col 8,820 ACF @		PSIA	20. Gas strea	am temperature: Inlet: Outlet:	1,226 1,226	°F °F		
21.	Gas flow rate: Design Maximum: Average Expected:	8,82	0 ACFM ACFM	22. Particulat	e Grain Loading Inlet: Outlet:	in grains/scf: I	N/A		
23.	Emission rate of eac	h pollutant (spec	ify) into and out	of collector:					
	Pollutant	IN Pol	lutant	Emission	OUT Pollutant Conf				
		lb/hr	grains/acf	Capture Efficiency %	lb/hr	grains/acf	Efficiency %		
	A NOx	50.37			1.26		97.5		
	В СО	47.41			1.19		97.5		
	C VOC	1.52			0.24		84		
	D HCHO	0.19			0.019		90		
	E CH4	5.22			1.57		70		
24.	Dimensions of stack	: Heig	ht NA	ft.	Diameter	1.10	ft.		
25.	Supply a curve show rating of collector.	wing proposed co	ollection efficien	icy versus gas	volume from 25	to 130 perce	nt of design		

## **Particulate Distribution**

26. Complete the table:	Particle Size Distribution at Inlet to Collector	Fraction Efficiency of Collector
Particulate Size Range (microns)	Weight % for Size Range	Weight % for Size Range
0 – 2		
2 – 4		
4 – 6		
6 – 8		
8 – 10		
10 – 12		
12 – 16		
16 – 20		
20 – 30		
30 – 40		
40 – 50		
50 – 60		
60 – 70		
70 – 80		
80 – 90		
90 – 100		
>100		

27. Describe any air po reheating, gas humid		utlet gas conditioning processes (e.g., gas cooling, gas
28. Describe the collect materials are not dispose		Catalyst elements can be cleaned and/or replaced;
29. Have you included <b>C</b>	Other Collectores Control Devic	e in the Emissions Points Data Summary Sheet? yes
Please propose mo	parameters. Please propose	and Testing porting in order to demonstrate compliance with the testing in order to demonstrate compliance with the
MONITORING: see Atta	achment O	RECORDKEEPING: see Attachment O
REPORTING: see Attac	chment O	TESTING: see Attachment O
RECORDKEEPING:	monitored in order to demons equipment or air control device. Please describe the proposed rec	ocess parameters and ranges that are proposed to be trate compliance with the operation of this process cordkeeping that will accompany the monitoring.
TESTING:	pollution control device.	emissions testing for this process equipment on air emissions testing for this process equipment on air
NOx: 97.5%, CO: 97.5% Due to variable load	ranteed Control Efficiency for eac %, VOC: 84%, HCHO: 90%, CHo d conditions, the catalyst efficien bected operating conditions.	
32. Manufacturer's Guar	ranteed Control Efficiency for eac	h air pollutant.
Inlet temperature range controller must be set prothan 0.5 wt% sulfated as	is 750 F - 1250 F. Engine m roperly with fuel heating value of sh. Catalyst must not be exposed	dures required by Manufacturer to maintain warranty.  The state of the



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Prepared For: QUO-17302-L3Z6
Clayton Brown

ANTERO RESOURCES

#### INFORMATION PROVIDED BY WAUKESHA

Engine: L7044GSI
Horsepower: 1680
RPM: 1200
Compression Ratio: 8.0

Exhaust Flow Rate: 8820 CFM Exhaust Temperature: 1226 °F Reference: N/A

Fuel: Natural Gas

Annual Operating Hours: 8760

#### **Uncontrolled Emissions**

	<u>g/bhp-hr</u>	<u>Lb/Hr</u>	Tons/Year
NOx:	13.50	50.00	219.00
CO:	12.50	46.30	202.78
THC:	2.30	8.52	37.31
NMHC	0.90	3.33	14.60
NMNEHC:	0.48	1.78	7.79
HCHO:	0.05	0.19	0.81
O2:	0.30 %		

#### **POST CATALYST EMISSIONS**

#### % Reduction

NOx: >97.5% CO: >97.5% VOC: >84.0% HCHO: >90.0% CH4: >70.0%

#### **CONTROL EQUIPMENT**

## **Catalyst Element**

Model: RT-3615-T

Catalyst Type: NSCR, Standard Precious Group Metals

Substrate Type: BRAZED

Manufacturer: EMIT Technologies, Inc

Element Quantity: 6

Element Size: Rectangle 36" x 15" x 3.5"



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#### WARRANTY

EMIT Technologies, Inc. warrants that the goods supplied will be free from defects in workmanship by EMIT Technologies, Inc. for a period of two (2) years from date of shipment. EMIT Technologies, Inc. will not be responsible for any defects which result from imprope use, neglect, failure to properly maintain or which are attributable to defects, errors or omissions in any drawings, specifications, plans or descriptions, whether written or oral, supplied to EMIT Technologies, Inc. by Buyer.

Catalyst performance using an EMIT Air/Fuel ratio controller is dependent upon properly defined set-points, variable with engine and fuel gas composition. Air/fuel ratio controller performance is guaranteed, but not limited, to fuel gas with a HHV content of 1400 BTU/SCF.

Catalyst performance will be guaranteed for a period of 1 year from installation, or 8760 operating hours, whichever comes first. The catalyst shall be operated with an automatic air/fuel ratio controller. The performance guarantee shall not cover the effects of excessive ash masking due to operation at low load, improper engine maintenance, or inappropriate lubrication oil. The performance guarantee shall not cover the effects of continuous engine misfires (cylinder or ignition) exposing the catalyst to excessive exothermic reaction temperatures. In most cases, excluding thermal deactivation, catalyst be performance is redeemable by means of proper washing (refer to EMIT Catalyst/Silencer Housing Manual for element wash information, or contact a local EMIT Sales representative).

The exhaust temperature operating range at the converter inlet is a minimum of 600°F for oxidation catalyst and 750 °F for NSCR catalyst, and a maximum of 1250°F.

If a properly functioning, high temperature shut down switch is not installed, thermal deactivation of catalyst at sustained temperatures above 1250°F is not covered. If excessive exposure to over oxygenation of NSCR catalyst occurs due to improperly functioning or non-existent Air/Fuel ratio control, then deactivation of catalyst is not warranted.

The catalyst conversion efficiencies (% reduction) will be guaranteed for engine loads of 50 to 100 percent. Standard Oxidation Catalyst conversion efficiencies (% reduction) will be guaranteed for fuel gas containing less than 1.5% mole fraction of non-methane, non-ethane hydrocarbons. Applications where fuel gas exceeds this level will require a Premium Oxidation Catalyst to maintain guaranteed VOC conversion efficiencies.

Engine lubrication oil shall contain less than 0.5 wt% Sulfated Ash with a maximum allowable specific oil consumption of 0.7 g/bhp-hr. The catalyst shall be limited to a maximum ash loading of 0.022 lb/ft3. Phosphorous and zinc additives are limited to 0.03 wt%. New or Reconstructed engines must operate for a minimum of 50 hours prior to catalyst installation, otherwise the warranty is void.

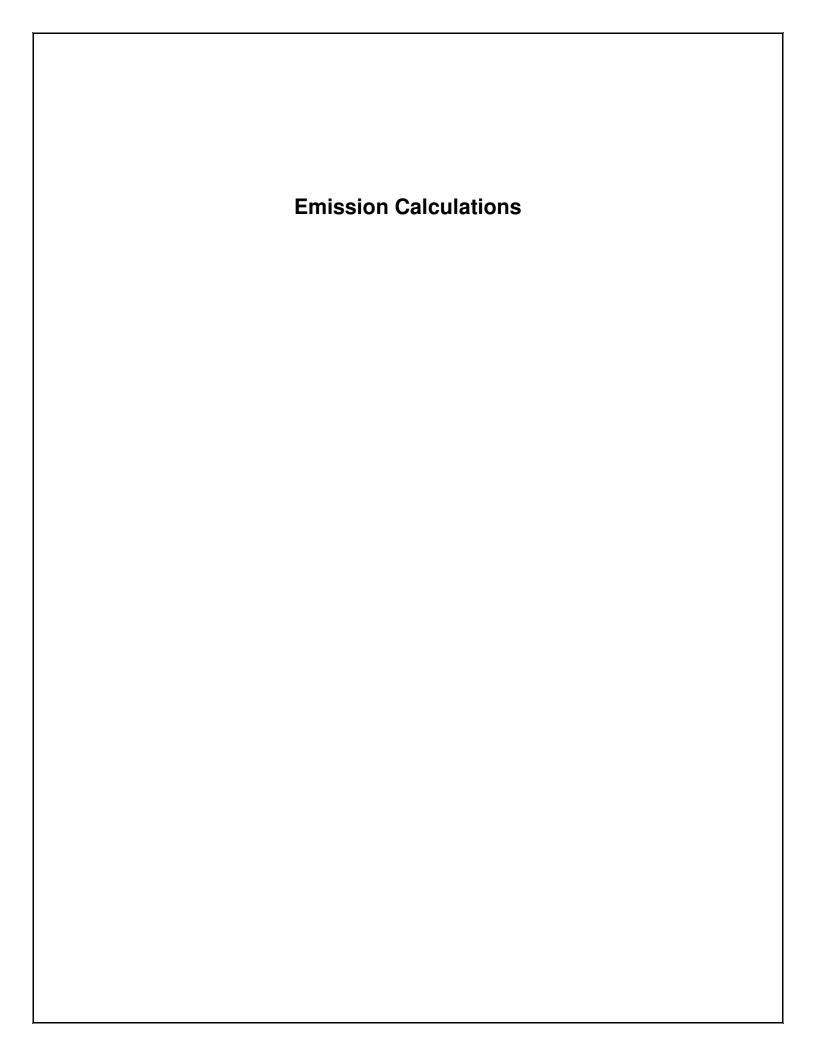
The catalyst must not be exposed to the following know poisoning agents, including: antimony, arsenic, chromium, copper, iron, lead, lithium, magnesium, mercury, nickel, phosphorous, potassium, silicon, sodium, sulfur, tin, and zinc. Total poison concentrations in the fuel gas must be limited to 0.25 ppm or less for catalyst to function properly.

Shipment - Promised shipping dates are approximate lead times from the point of manufacture and are not guaranteed. EMIT Technologies, Inc. will not be liable for any loss, damage or delay in manufacture or delivery resulting from any cause beyond its control including, but not limited to a period equal to the time lost by reason of that delay. All products will be crated as per best practice to prevent any damage during shipment. Unless otherwise specified, Buyer will pay for any special packing and shipping requirements. Acceptance of goods by common carrier constitutes delivery to Buyer. EMIT Technologies, Inc. shall not be responsible for goods damaged or lost in transit.

Terms: Credit is extended to purchaser for net 30 time period. If payment is not received in the net 30 timeframe, interest on the unpaid balance will accrue at a rate of 1.5% per month from the invoice date.

Order Cancellation Terms: Upon cancellation of an order once submittal of a Purchase Order has occurred, the customer will pay a 25% restocking fee for Catalyst Housings, Catalyst Elements, and Air/Fuel Ratio Controllers; 50% restocking fee for Cooler Top Solutions Exhaust System Accessories, and other Custom Built Products; 100% of all associated shipping costs incurred by EMIT; 100% of all project expenses incurred by EMIT for Field Services.

Attachme Supporting Emission	



# **EMISSIONS SUMMARY TOTAL**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia

#### **UNCONTROLLED POTENTIAL EMISSION SUMMARY**

NOX CO VOC SO PM-10 HAPS Formaldehyde CO-e															
Source										_	Formaldehyde		CO <sub>2</sub> e		
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	tpy
<u>Engines</u>															
Compressor Engine 1	50.37	220.62	47.41	207.64	1.52	6.65	0.0082	0.036	0.27	1.18	0.35	1.54	0.19	0.81	9,125
Compressor Engine 2	50.37	220.62	47.41	207.64	1.52	6.65	0.0082	0.036	0.27	1.18	0.35	1.54	0.19	0.81	9,125
Compressor Engine 3	50.37	220.62	47.41	207.64	1.52	6.65	0.0082	0.036	0.27	1.18	0.35	1.54	0.19	0.81	9,125
Compressor Engine 4	50.37	220.62	47.41	207.64	1.52	6.65	0.0082	0.036	0.27	1.18	0.35	1.54	0.19	0.81	9,125
Compressor Engine 5	50.37	220.62	47.41	207.64	1.52	6.65	0.0082	0.036	0.27	1.18	0.35	1.54	0.19	0.81	9,125
Compressor Engine 6	50.37	220.62	47.41	207.64	1.52	6.65	0.0082	0.036	0.27	1.18	0.35	1.54	0.19	0.81	9,125
Compressor Engine 7	50.37	220.62	47.41	207.64	1.52	6.65	0.0082	0.036	0.27	1.18	0.35	1.54	0.19	0.81	9,125
Compressor Engine 8	50.37	220.62	47.41	207.64	1.52	6.65	0.0082	0.036	0.27	1.18	0.35	1.54	0.19	0.81	9,125
Compressor Engine 9	50.37	220.62	47.41	207.64	1.52	6.65	0.0082	0.036	0.27	1.18	0.35	1.54	0.19	0.81	9,125
Compressor Engine 10	50.37	220.62	47.41	207.64	1.52	6.65	0.0082	0.036	0.27	1.18	0.35	1.54	0.19	0.81	9,125
Compressor Engine 11	50.37	220.62	47.41	207.64	1.52	6.65	0.0082	0.036	0.27	1.18	0.35	1.54	0.19	0.81	9,125
<u>Turbines</u>															
Microturbine Generator 1	0.080	0.35	0.22	0.96	0.020	0.088	0.0070	0.031	0.014	0.060	0.0021	0.0093	0.0015	0.0064	1,166
Microturbine Generator 2	0.080	0.35	0.22	0.96	0.020	0.088	0.0070	0.031	0.014	0.060	0.0021	0.0093	0.0015	0.0064	1,166
Microturbine Generator 3	0.080	0.35	0.22	0.96	0.020	0.088	0.0070	0.031	0.014	0.060	0.0021	0.0093	0.0015	0.0064	1,166
Catalytic Heater for Generator Fuel	0.0029	0.013	0.0025	0.011	0.00016	0.00071	0.000018	0.000077	0.00022	0.0010	0.000055	0.00024	0.0000022	0.000010	12
<u>Dehydrator</u>															
TEG Dehydrator 1					69.65	307.84					6.59	28.84			12,284
TEG Dehydrator 2					69.65	307.84					6.59	28.84			12,284
Reboiler 1	0.18	0.81	0.15	0.68	0.010	0.044	0.0011	0.0048	0.014	0.061	0.0035	0.015	0.00014	0.00060	771
Reboiler 2	0.18	0.81	0.15	0.68	0.010	0.044	0.0011	0.0048	0.014	0.061	0.0035	0.015	0.00014	0.00060	771
<u>Combustors</u>															
Flare and Pilot															
Hydrocarbon Loading															
Truck Loadout					46.22	4.56					3.76	0.37			13
<u>Heaters</u>															
Fuel Conditioning Heater	0.061	0.27	0.051	0.23	0.0034	0.015	0.00037	0.0016	0.0047	0.020	0.0012	0.0051	0.000046	0.00020	257
Fugitive Emissions															
Component Leak Emissions					0.89	3.91					0.0017	0.0073			85
Venting Emissions						8.28						0.012			701
Haul Road Dust Emissions									0.21	0.90					
Storage Tanks															
Produced Water Tanks					0.081	0.36					0.0066	0.029			1.0
Settler Tank					90.83	397.83					7.16	31.38			1,096
Condensate Tanks					1.31	5.72					0.11	0.46			16
Total Facility PTE =	554.75	2,429.79	522.50	2,288.57	295.42	1,109.85	0.11	0.50	3.25	14.25	28.07	106.95	2.04	8.94	132,169

## **EMISSIONS SUMMARY TOTAL**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia

#### CONTROLLED POTENTIAL EMISSION SUMMARY

CONTROLLED POTENTIAL EMISSION SUMMARY															
Source		Ox	C	:0	V	oc	S	$O_2$	PM-10 HAPs				Formal	CO₂e	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	tpy
<u>Engines</u>															
Compressor Engine 1	1.26	5.52	1.19	5.19	0.24	1.06	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,725
Compressor Engine 2	1.26	5.52	1.19	5.19	0.24	1.06	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,725
Compressor Engine 3	1.26	5.52	1.19	5.19	0.24	1.06	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,725
Compressor Engine 4	1.26	5.52	1.19	5.19	0.24	1.06	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,725
Compressor Engine 5	1.26	5.52	1.19	5.19	0.24	1.06	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,725
Compressor Engine 6	1.26	5.52	1.19	5.19	0.24	1.06	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,725
Compressor Engine 7	1.26	5.52	1.19	5.19	0.24	1.06	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,725
Compressor Engine 8	1.26	5.52	1.19	5.19	0.24	1.06	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,725
Compressor Engine 9	1.26	5.52	1.19	5.19	0.24	1.06	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,725
Compressor Engine 10	1.26	5.52	1.19	5.19	0.24	1.06	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,725
Compressor Engine 11	1.26	5.52	1.19	5.19	0.24	1.06	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,725
<u>Turbines</u>															
Microturbine Generator 1	0.080	0.35	0.22	0.96	0.020	0.088	0.0070	0.031	0.014	0.060	0.0021	0.0093	0.0015	0.0064	1,166
Microturbine Generator 2	0.080	0.35	0.22	0.96	0.020	0.088	0.0070	0.031	0.014	0.060	0.0021	0.0093	0.0015	0.0064	1,166
Microturbine Generator 3	0.080	0.35	0.22	0.96	0.020	0.088	0.0070	0.031	0.014	0.060	0.0021	0.0093	0.0015	0.0064	1,166
Catalytic Heater for Generator Fuel	0.0029	0.013	0.0025	0.011	0.00016	0.00071	0.000018	0.000077	0.00022	0.0010	0.000055	0.00024	0.0000022	0.000010	12
<u>Dehydrator</u>															
TEG Dehydrator 1					1.41	6.16					0.13	0.58			256
TEG Dehydrator 2					1.41	6.16					0.13	0.58			256
Reboiler 1	0.18	0.81	0.15	0.68	0.010	0.044	0.0011	0.0048	0.014	0.061	0.0035	0.015	0.00014	0.00060	771
Reboiler 2	0.18	0.81	0.15	0.68	0.010	0.044	0.0011	0.0048	0.014	0.061	0.0035	0.015	0.00014	0.00060	771
<u>Combustion</u>															
Flare and Pilot	0.33	1.44	1.78	7.79	0.00010	0.00044	0.000011	0.000048	0.00014	0.00060	0.000034	0.00015			2,475
<u>Hydrocarbon Loading</u>															
Truck Loadout					46.22	4.56					3.76	0.37			13
<u>Heaters</u>															
Fuel Conditioning Heater	0.061	0.27	0.051	0.23	0.0034	0.015	0.00037	0.0016	0.0047	0.020	0.0012	0.0051	0.000046	0.00020	257
<u>Fugitive Emissions</u>															
Component Leak Emissions					0.89	3.91					0.0017	0.0073			85
Venting Emissions						8.28						0.012			701
Haul Road Dust Emissions									0.21	0.90					
Storage Tanks															
Produced Water Tanks					0.0016	0.0071					0.00013	0.00058			0.02
Settler Tank					1.82	7.96					0.14	0.63			23
Condensate Tanks					0.026	0.11					0.0021	0.0093			0.3
Total Facility PTE =	14.85	65.05	15.84	69.37	54.52	49.21	0.11	0.50	3.25	14.25	6.16	11.15	0.21	0.91	105,094

# HAP EMISSIONS SUMMARY TOTAL

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia

#### **CONTROLLED POTENTIAL EMISSION SUMMARY**

Source	Benzene		Tolu	Toluene		Ethylbenzene		Xylenes		n-Hexane	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	
<u>Engines</u>				. ,		.,					
Compressor Engine 1	0.022	0.10	0.0078	0.034	0.00035	0.0015	0.0027	0.012			
Compressor Engine 2	0.022	0.10	0.0078	0.034	0.00035	0.0015	0.0027	0.012			
Compressor Engine 3	0.022	0.10	0.0078	0.034	0.00035	0.0015	0.0027	0.012			
Compressor Engine 4	0.022	0.10	0.0078	0.034	0.00035	0.0015	0.0027	0.012			
Compressor Engine 5	0.022	0.10	0.0078	0.034	0.00035	0.0015	0.0027	0.012			
Compressor Engine 6	0.022	0.10	0.0078	0.034	0.00035	0.0015	0.0027	0.012			
Compressor Engine 7	0.022	0.10	0.0078	0.034	0.00035	0.0015	0.0027	0.012			
Compressor Engine 8	0.022	0.10	0.0078	0.034	0.00035	0.0015	0.0027	0.012			
Compressor Engine 9	0.022	0.10	0.0078	0.034	0.00035	0.0015	0.0027	0.012			
Compressor Engine 10	0.022	0.10	0.0078	0.034	0.00035	0.0015	0.0027	0.012			
Compressor Engine 11	0.022	0.10	0.0078	0.034	0.00035	0.0015	0.0027	0.012			
<u>Turbines</u>											
Microturbine Generator 1	2.47E-05	1.08E-04	2.68E-04	1.17E-03	6.59E-05	2.89E-04	1.32E-04	5.77E-04			
Microturbine Generator 2	2.47E-05	1.08E-04	2.68E-04	1.17E-03	6.59E-05	2.89E-04	1.32E-04	5.77E-04			
Microturbine Generator 3	2.47E-05	1.08E-04	2.68E-04	1.17E-03	6.59E-05	2.89E-04	1.32E-04	5.77E-04			
Catalytic Heater for Generator Fuel											
<u>Dehydrator</u>											
TEG Dehydrator 1	0.020	0.088	0.044	0.19	0.000047	0.00020	0.011	0.050	0.056	0.25	
TEG Dehydrator 2	0.020	0.088	0.044	0.19	0.000047	0.00020	0.011	0.050	0.056	0.25	
Reboiler 1											
Reboiler 2											
<u>Combustion</u>											
Flare and Pilot											
<u>Hydrocarbon Loading</u>											
Truck Loadout	0.051	0.0050	0.089	0.0087			0.010	0.0010	3.61	0.36	
<u>Heaters</u>											
Fuel Conditioning Heater											
Fugitive Emissions											
Component Leak Emissions	5.47E-04	2.40E-03	9.68E-04	4.24E-03	5.81E-07	2.54E-06	1.40E-04	6.15E-04	3.89E-02	1.71E-01	
Venting Emissions		4.00E-03		6.99E-03		6.48E-06		1.15E-03		2.84E-01	
Haul Road Dust Emissions											
Storage Tanks											
Produced Water Tanks	1.78E-06	7.79E-06	3.12E-06	1.37E-05			3.56E-07	1.56E-06	1.27E-04	5.56E-04	
Settler Tank	1.95E-03	8.55E-03	3.42E-03	1.50E-02			3.91E-04	1.71E-03	1.39E-01	6.10E-01	
Condensate Tanks	2.86E-05	1.25E-04	5.01E-05	2.19E-04			5.73E-06	2.51E-05	2.04E-03	8.93E-03	
Total Facility PTE =	0.34	1.26	0.27	0.80	0.004	0.02	0.06	0.24	3.90	1.92	

## **Compressor Engine Emission Calculations**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia
Source Description:	Compressor Engines

#### Source Information-Per Engine

	9		
Emission Unit ID:	C-2100 - C-2200		
Engine Make/Model	Waukesh	a 7044 GSI	
Service	Comp	ression	
Controls - Y or N / Type	Y	NSCR/AFRC	
Site Horsepower Rating <sup>1</sup>	1,680	hp	
Fuel Consumption (BSFC) <sup>1</sup>	8,289	Btu/(hp-hr)	
Heat Rating <sup>2</sup>	13.93	MMBtu/hr	
Fuel Consumption <sup>2,3</sup>	107.75	MMscf/yr	
Fuel Consumption <sup>1</sup>	12,300	scf/hr	
Fuel Heating Value	1,130	Btu/scf	
Operating Hours	8,760	hrs/yr	

#### Notes:

- 1. Values from Waukesha specification sheet
- 2. Calculated values
- 3. Annual fuel consumption is 100% of maximum fuel consumption at 100% load.

#### Potential Emissions per Engine

	Uncontrolled Controlled										
Pollutant	Emissio (lb/MMBtu)	n Factor (g/bhp-hr)	Est (lb/hr)	imated Emissi (lb/yr)	ons <sup>2</sup> (tpy)	Emissio (lb/MMBtu)	n Factor (g/bhp-hr)	Est (lb/hr)	imated Emissi (lb/yr)	ons <sup>2</sup> (tpy)	Source of Emissions Factors
NOx		13.6	50.37		220.62		0.34	1.26		5.52	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled
СО		12.8	47.41		207.64		0.32	1.19		5.19	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled
VOC		0.41	1.52		6.65		0.066	0.24		1.06	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled
SO <sub>2</sub>	5.88E-04		0.0082		0.036	5.88E-04		0.0082		0.036	AP-42, Chapter 3.2, Table 3.2-3
PM <sub>2.5</sub> /PM <sub>10</sub>	1.94E-02		0.27		1.18	1.94E-02		0.27		1.18	AP-42, Chapter 3.2, Table 3.2-3
Total PM	1.94E-02		0.27		1.18	1.94E-02		0.27		1.18	AP-42, Chapter 3.2, Table 3.2-3
1,1,2,2-Tetrachloroethane	2.53E-05		0.00035	3.08	0.0015	2.53E-05		0.00035	3.08	0.0015	AP-42, Chapter 3.2, Table 3.2-3
1,3-Butadiene	6.63E-04		0.0092	80.73	0.040	6.63E-04		0.0092	80.73	0.040	AP-42, Chapter 3.2, Table 3.2-3
Acetaldehyde	2.79E-03		0.039	339.7	0.17	2.79E-03		0.039	339.7	0.17	AP-42, Chapter 3.2, Table 3.2-3
Acrolein	2.63E-03		0.037	320.2	0.16	2.63E-03		0.037	320.2	0.16	AP-42, Chapter 3.2, Table 3.2-3
Benzene	1.58E-03		0.022	192.4	0.096	1.58E-03		0.022	192.4	0.096	AP-42, Chapter 3.2, Table 3.2-3
Ethylbenzene	2.48E-05		0.00035	3.02	0.0015	2.48E-05		0.00035	3.02	0.0015	AP-42, Chapter 3.2, Table 3.2-3
Formaldehyde		0.05	0.19	1,622	0.81		0.005	0.019	162.2	0.081	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled
Methanol	3.06E-03		0.043	372.6	0.19	3.06E-03		0.043	372.6	0.19	AP-42, Chapter 3.2, Table 3.2-3
Methylene Chloride	4.12E-05		0.00057	5.02	0.0025	4.12E-05		0.00057	5.02	0.0025	AP-42, Chapter 3.2, Table 3.2-3
PAH	1.41E-04		0.0020	17.17	0.0086	1.41E-04		0.0020	17.17	0.0086	AP-42, Chapter 3.2, Table 3.2-3
Toluene	5.58E-04		0.0078	67.95	0.034	5.58E-04		0.0078	67.95	0.034	AP-42, Chapter 3.2, Table 3.2-3
Xylenes	1.95E-04		0.0027	23.74	0.012	1.95E-04		0.0027	23.74	0.012	AP-42, Chapter 3.2, Table 3.2-3
Other HAPs <sup>2</sup>	2.10E-04		0.0029	25.54	0.013	2.10E-04		0.0029	25.54	0.013	AP-42, Chapter 3.2, Table 3.2-3
Total HAPS			0.35	3,073	1.54			0.18	1,613	0.81	
Pollutant	Emissio (kg/MMBtu)	n Factor (g/bhp-hr)	Est (lb/hr)	imated Emissi (lb/yr) 4	ons <sup>2</sup> (tpy) <sup>4</sup>	Emissio (kg/MMBtu)	n Factor (g/bhp-hr)	Est (lb/hr)	imated Emissi	ons <sup>2</sup> (tpy) <sup>4</sup>	Source of Emissions Factors
CO <sub>2</sub>		527	1,952		8,549		527	1,952		8,549	Manufacturer's Specs
CH₄		1.41	5.22		22.87		0.42	1.57		6.86	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled
N₂O	0.0001		0.0031		0.013	0.0001		0.0031		0.013	40 CFR Part 98, Subpart C, Table C-2
CO <sub>2</sub> e <sup>2</sup>			2,083		9,125			1,992		8,725	40 CFR Part 98, Subpart A, Table A-1, effective January 2014

#### Example Calculations

lb/hr = (g/hp-hr) \* (hp) \* (1 lb/453.6 g) or (lb/MMBtu) \* (MMBtu/hr)

tpy = (lb/hr) \*(1 ton/2000 lb) \* (hr/yr)

#### **Microturbine Generator Emission Calculations**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia
Source Description:	Microturbine Generators

#### Source Information

Emission Unit ID:	G-8000 through G-8200		
Make/Model	Capstone C	200 Standard	
Microturbine Rating <sup>2</sup>	200	kWe	
Number of Microturbines <sup>2</sup>	3	units	
Net Heat Rate	10,300	Btu/kWhe	
Heat Input 1	2.06	MMBtu/hr	
Operating Hours <sup>2</sup>	8,760	hrs/yr	

# Notes:

1) Calculated

#### Potential Emissions per Generator

		U	ncontrolled			Controlled					
Pollutant	Emissio	n Factor	Esti	mated Emissi	ons <sup>1</sup>	Emissio	n Factor	Esti	mated Emissi	ons <sup>1</sup>	Source of Emissions Factors
Pollutarit	(lb/MMBtu)	(lb/MWhe)	(lb/hr)	(lb/yr)	(tpy)	(lb/MMBtu)	(lb/MWhe)	(lb/hr)	(lb/yr)	(tpy)	Source of Emissions Factors
NOx		0.40	0.080		0.35		0.40	0.080		0.35	Manufacturer Specifications
co		1.10	0.22		0.96		1.10	0.22		0.96	Manufacturer Specifications
VOC		0.10	0.020		0.088		0.10	0.020		0.088	Manufacturer Specifications
SO <sub>2</sub>	3.40E-03		0.0070		0.031	3.40E-03		0.0070		0.031	AP-42, Chapter 3.1, Table 3.1-2a
PM <sub>2.5</sub> /PM <sub>10</sub>	6.60E-03		0.014		0.060	6.60E-03		0.014		0.060	AP-42, Chapter 3.1, Table 3.1-2a
1,3-Butadiene	4.30E-07		8.86E-07	0.0078	3.88E-06	4.30E-07		8.86E-07	0.0078	3.88E-06	AP-42, Chapter 3.1, Table 3.1-3
Acetaldehyde	4.00E-05		8.24E-05	0.72	3.61E-04	4.00E-05		8.24E-05	0.72	3.61E-04	AP-42, Chapter 3.1, Table 3.1-3
Acrolein	6.40E-06		1.32E-05	0.12	5.77E-05	6.40E-06		1.32E-05	0.12	5.77E-05	AP-42, Chapter 3.1, Table 3.1-3
Benzene	1.20E-05		2.47E-05	0.22	1.08E-04	1.20E-05		2.47E-05	0.22	1.08E-04	AP-42, Chapter 3.1, Table 3.1-3
Ethylbenzene	3.20E-05		6.59E-05	0.58	2.89E-04	3.20E-05		6.59E-05	0.58	2.89E-04	AP-42, Chapter 3.1, Table 3.1-3
Formaldehyde	7.10E-04		1.46E-03	12.81	6.41E-03	7.10E-04		1.46E-03	12.81	6.41E-03	AP-42, Chapter 3.1, Table 3.1-3
Naphthalene	1.30E-06		2.68E-06	0.023	1.17E-05	1.30E-06		2.68E-06	0.023	1.17E-05	AP-42, Chapter 3.1, Table 3.1-3
PAH	2.20E-06		4.53E-06	0.040	1.99E-05	2.20E-06		4.53E-06	0.040	1.99E-05	AP-42, Chapter 3.1, Table 3.1-3
Propylene Oxide	2.90E-05		5.97E-05	0.52	2.62E-04	2.90E-05		5.97E-05	0.52	2.62E-04	AP-42, Chapter 3.1, Table 3.1-3
Toluene	1.30E-04		2.68E-04	2.35	1.17E-03	1.30E-04		2.68E-04	2.35	1.17E-03	AP-42, Chapter 3.1, Table 3.1-3
Xylenes	6.40E-05		1.32E-04	1.15	5.77E-04	6.40E-05		1.32E-04	1.15	5.77E-04	AP-42, Chapter 3.1, Table 3.1-3
Total HAPS			0.0021	18.54	0.0093			0.0021	18.54	0.0093	
Pollutant	Emissio	n Factor	Esti	mated Emissi	ons <sup>1</sup>	Emission	n Factor	Esti	mated Emissi	ons <sup>1</sup>	Source of Emissions Factors
Poliutarit	(kg/MMBtu)	(lb/MWhe)	(lb/hr)		(tpy)	(kg/MMBtu)	(lb/MWhe)	(lb/hr)		(tpy)	Source of Emissions Factors
CO <sub>2</sub>		1,330	266.0		1,165		1,330	266.0		1,165	Manufacturer Specifications
CH₄	0.001		0.0046		0.020	0.001		0.0046		0.020	40 CFR Part 98, Subpart C, Table C-2
N₂O	0.0001		0.00046		0.0020	0.0001		0.00046		0.0020	40 CFR Part 98, Subpart C, Table C-2
CO₂e			266.2		1,166			266.2		1,166	40 CFR Part 98, Subpart A, Table A-1, effective January 2014

#### Example Calculations

lb/hr = (lb/Mwhe) \* kWe \* (1 MWe/1000 kWe) or (lb/MMBtu) \* (MMBtu/hr) or (kg/MMBtu) \* (MMBtu/hr) \* (2.21 lb/kg)

tpy = (lb/hr) \* (hr/yr) \* (ton/2000 lb)

June 2016

# **Natural Gas Fueled Catalytic Heater Emissions**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Location:	Ritchie County, West Virginia
Source Description:	Catalytic Heater for Generator Fuel

#### Source Information

Emission Unit ID:	CATHT1		
Source Description:	Generator Fuel Heater		
Hours of Operation	8,760	hr/yr	
Design Heat Rate	0.024	MMBtu/hr	
Heater Efficiency	80%		
Fuel Heat Value	1,020	Btu/scf	
Fuel Use	0.26	MMscf/yr	

## Emission Calculations per Heater

Pollutant	Emission Factor	Emissions	Emissions	Emission Factor
1 ondtant	(lb/MMscf)	(lb/hr)	(tpy)	Source
$NO_X$	100	0.0029	0.013	AP-42 Ch. 1.4 Table 1.4-1
CO	84	0.0025	0.011	AP-42 Ch. 1.4 Table 1.4-1
VOC	5.5	0.00016	0.00071	AP-42 Ch. 1.4 Table 1.4-2
PM <sub>10</sub>	7.6	0.00022	0.0010	AP-42 Ch. 1.4 Table 1.4-2
SO <sub>2</sub>	0.6	0.000018	0.000077	AP-42 Ch. 1.4 Table 1.4-2
Formaldehyde	0.075	0.0000022	0.000010	AP-42 Ch. 1.4 Table 1.4-3
Total HAPs (including HCHO) <sup>1</sup>	1.9	0.00006	0.00024	AP-42 Ch. 1.4 Table 1.4-3
Pollutant	Emission Factor	Emissions	Emissions	Emission Factor
Pollutalit	(kg/MMBtu)	(lb/hr)	(tpy)	Source
Carbon Dioxide	53.06	2.81	12.3	40 CFR Part 98, Subpart C, Table C-1
Methane	0.001	0.000053	0.00023	40 CFR Part 98, Subpart C, Table C-2
Nitrous Oxide	0.0001	0.0000053	0.000023	40 CFR Part 98, Subpart C, Table C-2
CO₂e		2.82	12.3	40 CFR Part 98, Subpart A, Table A-1

<sup>1.</sup> Only those HAP pollutants above detection thresholds were included.

#### Sample Calculations:

Fuel Consumption (MMscf/yr) = Heater Size (MMBtu/hr) \* Hours of Operation (hrs/yr)

Fuel Heat Value (Btu/scf) \* Heater Efficiency

Emissions (tons/yr) = Emission Factor (lbs/MMscf) \* Fuel Consumption (MMscf/yr)

2,000 (lbs/ton)

# **Dehydrator Emissions**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia
Source Description:	Dehydrator Units

#### Potential Emissions per Dehydrator

	Emission Unit ID	: V-3110/V-3210	Emission Unit ID	): V-3120/V-3220	
Pollutant	Dehydrato	r Still Vent	Flash Tank Gas		
Pollutarit	(lb/hr)	(tpy)	(lb/hr)	(tpy)	
Uncontrolled Emissions 1					
VOC	23.46	102.8	46.19	205.07	
Total HAPs	4.49	19.65	2.10	9.19	
Benzene	0.94	4.13	0.068	0.30	
Toluene	2.10	9.22	0.086	0.38	
Ethylbenzene	0.0023	0.010	0.000046	0.00020	
Xylenes	0.56	2.45	0.0074	0.032	
n-Hexane	0.88	3.85	1.94	8.49	
Methane	18.15	79.50	99.94	411.45	
Carbon Dioxide	0.28	1.24	2.13	9.33	
CO <sub>2</sub> e	454.1	1,989	2,501	10,296	
Controlled Emissions 2,3					
VOC	0.47	2.06	0.94	4.10	
Total HAPs	0.090	0.39	0.042	0.18	
Benzene	0.019	0.082	0.0014	0.0059	
Toluene	0.042	0.18	0.0017	0.0075	
Ethylbenzene	0.000046	0.00020	0.00000091	0.0000040	
Xylenes	0.011	0.049	0.00010	0.00060	
n-Hexane	0.018	0.077	0.039	0.17	
Methane	0.36	1.59	1.88	8.23	
Carbon Dioxide	0.28	1.24	2.13	9.33	
CO <sub>2</sub> e	9.36	40.99	49.10	215.1	

	Dehydrator Er	mission Totals
Pollutant	(lb/hr)	(tpy)
Uncontrolled Emissions 1		
VOC	69.65	307.8
Total HAPs	6.59	28.84
Benzene	1.01	4.42
Toluene	2.19	9.59
Ethylbenzene	0.0023	0.010
Xylenes	0.57	2.48
n-Hexane	2.82	12.34
Methane	118.1	491.0
Carbon Dioxide	2.41	10.57
CO <sub>2</sub> e	2,955	12,284
Controlled Emissions 2,3		
VOC	1.41	6.16
Total HAPs	0.13	0.58
Benzene	0.020	0.088
Toluene	0.044	0.19
Ethylbenzene	0.000047	0.00020
Xylenes	0.011	0.050
n-Hexane	0.056	0.25
Methane	2.24	9.82
Carbon Dioxide	2.41	10.57
CO <sub>2</sub> e	58.46	256.0

Output from GRI-GLYCalc 4.0 for both the still vent and flash tank gas emissions

<sup>&</sup>lt;sup>2</sup>Controlled emissions assume that the glycol still vent is equipped with a condenser and is controlled by a combustor with 98% control efficiency.

<sup>&</sup>lt;sup>3</sup>Flash tank gas is used in the reboiler as the primary fuel source. However, in the case that gas cannot be used in the reboiler, the gas is sent to the primary/backup VRU system via the storage tanks for 98% control.

# **Natural Gas Fueled Dehydrator Reboiler Emissions**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Location:	Ritchie County, West Virginia
Source Description:	Dehydrator Reboilers

#### Source Information

Emission Unit ID:	F-3100 & F-3200			
Source Description:	Dehydrator Reboiler			
Hours of Operation	8,760 hr/yr			
Design Heat Rate	1.5	MMBtu/hr		
Heater Efficiency	0.8			
Fuel Heat Value	1,020	Btu/scf		
Fuel Use	16.1	MMscf/yr		

## Emission Calculations per Reboiler

Pollutant	Emission Factor	Emissions	Emissions	Emission Factor
	(lb/MMscf)	(lb/hr)	(tpy)	Source
$NO_X$	100	0.18	0.81	AP-42 Ch. 1.4 Table 1.4-1
CO	84	0.15	0.68	AP-42 Ch. 1.4 Table 1.4-1
VOC	5.5	0.010	0.044	AP-42 Ch. 1.4 Table 1.4-2
PM <sub>10</sub>	7.6	0.014	0.061	AP-42 Ch. 1.4 Table 1.4-2
SO <sub>2</sub>	0.6	0.0011	0.0048	AP-42 Ch. 1.4 Table 1.4-2
Formaldehyde	0.075	0.00014	0.00060	AP-42 Ch. 1.4 Table 1.4-3
Total HAPs (including HCHO)	1.9	0.0035	0.015	AP-42 Ch. 1.4 Table 1.4-3
Pollutant	Emission Factor	Emissions	Emissions	Emission Factor
Poliutarit	(kg/MMBtu)	(lb/hr)	(tpy)	Source
Carbon Dioxide	53.06	175.9	770.4	40 CFR Part 98, Subpart C, Table C-1
Methane	0.001	0.003	0.015	40 CFR Part 98, Subpart C, Table C-2
Nitrous Oxide	0.0001	0.0003	0.0015	40 CFR Part 98, Subpart C, Table C-2
CO <sub>2</sub> e		176.1	771.2	40 CFR Part 98, Subpart A, Table A-1

## Sample Calculations:

Fuel Consumption (MMscf/yr) = Heater Size (MMBtu/hr) \* Hours of Operation (hrs/yr)

Fuel Heat Value (Btu/scf) \* Heater Efficiency

Emissions (tons/yr) = Emission Factor (lbs/MMscf) \* Fuel Consumption (MMscf/yr)

2,000 (lbs/ton)

# **Flare Emissions**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia
Source Description:	Flare for Dehydrator Still Vent Gas
Emission Unit ID:	FL-8300

#### Combusted Gas Emissions

Flare Heat Input: 4.80 MMBtu/hr
Vent Gas to Flare Rate: 4,247 scf/hr
Gas Heating Value: 1,130 Btu/scf
Hours of Operation: 8,760 hr/yr

Pollutant	Emission Factor <sup>1</sup> (lb/MMBtu)	Emissions (lbs/hr)	Emissions (tons/yr)	
Particulate Matter (PM/PM <sub>10</sub> /PM <sub>2.5</sub> )	N/A - Smokeless Design			
Nitrogen Oxides (NO <sub>x</sub> )	0.068	0.33	1.43	
Carbon Monoxide (CO)	0.37	1.78	7.78	

<sup>&</sup>lt;sup>1</sup> Emission Factors from Table 13.5-1 of AP-42 Section 13.5 (Sept 1991)

#### **Pilot Emissions**

Pilot Heating Value: 1,130 Btu/scf
Hours of Operation: 8,760 hr/yr
Total Pilot Natural Gas Usage: 1.64E-05 MMscf/hr

Pollutant	Emission Factor (lb/MMscf)	Emissions (lbs/hr)	Emissions (tons/yr)
Particulate Matter (PM/PM <sub>10</sub> /PM <sub>2.5</sub> ) <sup>2</sup>	7.6	1.38E-04	6.05E-04
Nitrogen Oxides (NOx)	100	1.82E-03	7.96E-03
Sulfur Dioxide (SO <sub>2</sub> ) <sup>2</sup>	0.6	1.09E-05	4.78E-05
Carbon Monoxide (CO) <sup>2</sup>	84	1.53E-03	6.69E-03
Volatile Organic Compounds (VOC) <sup>2</sup>	5.5	9.99E-05	4.38E-04
Total HAPs <sup>2,3</sup>	1.88	3.42E-05	1.50E-04

<sup>&</sup>lt;sup>2</sup> Emission Factors from AP-42 Tables 1.4-1, 1.4-2, 1.4-3, and 1.4-4 (7/98).

#### **Total Flare Emissions**

Pollutant	Total Potential Emission Rate (tons/year)
Particulate Matter (PM/PM <sub>10</sub> /PM <sub>2.5</sub> )	6.05E-04
Nitrogen Oxides (NOx)	1.44
Sulfur Dioxide (SO <sub>2</sub> )	4.78E-05
Carbon Monoxide (CO)	7.79
Volatile Organic Compounds (VOC)	4.38E-04
Total HAPs	1.50E-04

#### Greenhouse Gas Emissions

Pollutant	Emission Factor (kg/MMBtu)	Emissions (lb/hr)	Emissions (tpy)	Emission Factor Source
Carbon Dioxide	53.06	565.0	2,475	40 CFR Part 98, Subpart C, Table C-1
Methane	0.001	0.011	0.047	40 CFR Part 98, Subpart C, Table C-2
Nitrogen Dioxide	0.0001	0.0011	0.0047	40 CFR Part 98, Subpart C, Table C-2
CO <sub>2</sub> e		565.0	2,475	40 CFR Part 98, Subpart A, Table A-1

<sup>&</sup>lt;sup>3</sup> Sum of Emissions Factors published for pollutants classified as "HAPS" under AP-42 Table 1.4-3.

# Storage Tank Flashing Emissions Calculated by ProMax Simulation

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia
Source Description:	Settling Tank
Emission Unit ID:	TK-9000

#### **Settling Tank Flashing Emissions**

Component	Uncontrolled Flashing Emissions <sup>1</sup> (lb/hr)	Uncontrolled Flashing Emissions (tons/yr)	Controlled Flashing Emissions <sup>2,3</sup> (lb/hr)	Controlled Flashing Emissions <sup>2,3</sup> (tons/yr)
Methane	9.89	43.33	0.20	0.87
Ethane	19.40	84.97	0.39	1.70
Propane	23.77	104.1	0.48	2.08
i-Butane	7.94	34.79	0.16	0.70
n-Butane	17.54	76.84	0.35	1.54
i-Pentane	9.19	40.24	0.18	0.80
n-Pentane	9.99	43.75	0.20	0.88
i-C6	5.31	23.28	0.11	0.47
n-Hexane	6.88	30.13	0.14	0.60
Benzene	0.10	0.42	0.0019	0.0084
Cyclohexane	0.00	0.00	0.00	0.00
i-C7	0.96	4.22	0.019	0.084
n-Heptane	4.94	21.66	0.10	0.43
Toluene	0.17	0.74	0.0034	0.015
i-Octane	0.35	1.51	0.0069	0.030
n-Octane	1.77	7.76	0.035	0.16
Ethylbenzene	0.00	0.00	0.00	0.00
o-Xylene	0.019	0.085	0.00039	0.0017
Nonane	0.014	0.060	0.00028	0.0012
Decane	0.87	3.80	0.017	0.076
Water	3.41	14.92	3.41	14.92
Nitrogen	0.055	0.24	0.055	0.24
Oxygen	0.00	0.00	0.00	0.00
Carbon Dioxide	0.20	0.86	0.20	0.86
VOC Subtotal	89.82	393.4	1.80	7.87
HAP Subtotal	7.16	31.38	0.14	0.63
CO₂e Subtotal	247.5	1,084	5.14	22.52
Total	122.8	537.7	6.04	26.45

#### Notes:

- 1. Flashing emissions calculated by ProMax 3.2. Flash gas is stream 43 of the associated ProMax simulation. Flashing only occurs in the settling tank as all pressurized fluids flow into the settling tank and then separate out at atmospheric conditions to the condensate and produced water tanks.
- 2. Tanks are controlled by a VRU with assumed 98% capture efficiency; but will likely be higher as vapors are recycled back into the system
- 3. VRU-6000 is the primary VRU to collect storage tank vapors and VRU-6100 is the backup VRU in times when the primary VRU is undergoing maintenance or shutdown. In the unlikely event that both VRU-6000 and VRU-6100 are under maintenance or are shutdown, a bypass system is in place to route tank vapors to the facility inlet. The VRU compressor is equipped to recover wet and dry gas and has a VFD to adapt the operating speed for varying environmental pressures and temperatures. Lastly, both VRUs are equipped with automatic monitoring, shutdown, and alert systems with sensors to detect temperature, pressure, liquid levels, suction pressure, and motor overload.

# **Storage Tank Working and Breathing Emissions**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia
Source Description:	Condensate, Settling, and Produced Water Tanks
Emission Unit ID:	TK-9000, TK-9100, TK-9110, TK-9200, TK-9201

	Uncontrolled	Uncontrolled	Uncontrolled	Uncontrolled	Uncontrolled	Uncontrolled	Uncontrolled	Uncontrolled
TANK	VOC	Benzene	Toluene	Ethylbenzene	Xylenes	n-Hexane	CH₄	CO <sub>2</sub> e
DESCRIPTION	Emissions <sup>1</sup>	Emissions <sup>4</sup>	Emissions	Emissions <sup>3</sup>				
	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)
400 bbl Hydrocarbon Storage Tank (TK-9200)	2.86	3.13E-03	5.49E-03		6.27E-04	0.22	0.32	8.02
400 bbl Hydrocarbon Storage Tank (TK-9210)	2.86	3.13E-03	5.49E-03		6.27E-04	0.22	0.32	8.02
500 bbl Settling Tank (TK-9000)	4.41	4.83E-03	8.46E-03		9.67E-04	0.34	0.49	12.37
400 bbl Produced Water Storage Tank <sup>2</sup> (TK-9100)	0.18	1.95E-04	3.41E-04		3.90E-05	0.014	0.020	0.50
400 bbl Produced Water Storage Tank <sup>2</sup> (TK-9110)	0.18	1.95E-04	3.41E-04		3.90E-05	0.014	0.020	0.50
TOTAL	10.49	0.011	0.020	0.00	0.0023	0.82	1.18	29.42

TANK DESCRIPTION	Controlled VOC Emissions <sup>5</sup>	Controlled Benzene Emissions <sup>5</sup>	Controlled Toluene Emissions <sup>5</sup>	Controlled Ethylbenzene Emissions <sup>5</sup>	Controlled Xylenes Emissions <sup>5</sup>	Controlled n-Hexane Emissions <sup>5</sup>	Controlled CH <sub>4</sub> Emissions <sup>5</sup>	Controlled CO <sub>2</sub> e Emissions <sup>5</sup>
	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)
400 bbl Hydrocarbon Storage Tank (TK-9200)	0.057	6.26E-05	1.10E-04		1.25E-05	4.46E-03	0.0064	0.16
400 bbl Hydrocarbon Storage Tank (TK-9210)	0.057	6.26E-05	1.10E-04		1.25E-05	4.46E-03	0.0064	0.16
500 bbl Settling Tank (TK-9000)	0.088	9.65E-05	1.69E-04		1.93E-05	6.88E-03	0.010	0.25
400 bbl Produced Water Storage Tank <sup>2</sup> (TK-9100)	0.0036	3.90E-06	6.83E-06		7.81E-07	2.78E-04	0.00040	0.010
400 bbl Produced Water Storage Tank <sup>2</sup> (TK-9110)	0.0036	3.90E-06	6.83E-06		7.81E-07	2.78E-04	0.00040	0.010
TOTAL	0.21	0.00023	0.00040	0.00	0.000046	0.016	0.024	0.59

#### Notes:

- 1. Tanks 4.0.9d used to calculate standing, working, and breathing (S,W,B) emissions.
- 2. Produced water assumed to have no more than 10% hydrocarbon liquid.
- 3. CO2e emissions estimated assuming 8% of the vent gas by weight is methane and 73% of the vent gas by weight is VOC (per ProMax simulation) and the global warming potential of methane as published in 40 CFR Part 98 Table A-1.
- 4. HAP emissions estimated assuming 6% by weight of the tank gas is HAPs and 73% by weight are VOCs (per ProMax simulation).
- 5. Tanks are controlled by a VRU with assumed 98% capture efficiency; but will likely be higher as vapors are recycled back into the system.
- 6. VRU-6000 is the primary VRU to collect storage tank vapors and VRU-6100 is the backup VRU in times when the primary VRU is undergoing maintenance or shutdown. In the unlikely event that both VRU-6000 and VRU-6100 are under maintenance or are shutdown, a bypass system is in place to route tank vapors to the facility inlet. The VRU compressor is equipped to recover wet and dry gas and has a VFD to adapt the operating speed for varying environmental pressures and temperatures. Lastly, both VRUs are equipped with automatic monitoring, shutdown, and alert systems with sensors to detect temperature, pressure, liquid levels, suction pressure, and motor overload.

# **Truck Loading Emissions**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia
Source Description:	Production Liquids Truck Loadout
Emission Unit ID:	LDOUT1

#### AP - 42, Chapter 5.2 $L_L = 12.46 \times S \times P \times M / T$

L<sub>L</sub> = Loading Loss Emission Factor (lbs VOC/1000 gal loaded)

S = Saturation Factor

P = True Vapor Pressure of the Loaded Liquid (psia)

M = Vapor Molecular Weight of the Loaded Liquid (lbs/lbmol)

 $T = Temperature of Loaded Liquid (<math>{}^{\circ}R$ )

VOC Emissions (tpy) = L<sub>L</sub> (lbs VOC/1000 gal) \* 42 gal/bbl \* 365 days/year \* production (bbl/day)

1000 gal \* 2000 lbs/ton

					_			Uncontrolled							
						7	Production	voc	HAP <sup>6</sup>	Benzene	Toluene	E-Benzene	Xylenes	n-Hexane	CO <sub>2</sub> e <sup>7</sup>
Source	S <sup>1</sup>	P (psia) <sup>2</sup>	$M^3$	T (ºF)⁴	T (ºR)	(lb/1000 gal)	(bbl/day)	(tpy)	(tpy)	(tpy)	(tpy)	(tpy)	(tpy)	(tpy)	(tpy)
Condensate	0.6	3.9	68	60	519.67	3.85	150	4.43	0.36	4.85E-03	8.49E-03		9.71E-04	3.46E-01	12.42
Produced Water <sup>5</sup>	0.6	3.9	68	60	519.67	0.38	45	0.13	0.011	1.44E-04	2.52E-04		2.89E-05	1.03E-02	0.37

#### Notes:

- 1. Saturation factor from AP-42, Table 5.2-1 (Submerged loading (bottom loading): dedicated normal service)
- 2. True vapor pressure is estimated from AP-42, Table 7.1-2 assuming an average daily temperature of 60 deg F and an RVP of 7.8.
- 3. Molecular weight liquid vapor is estimated from AP-42, Table 7.1-2 assuming an RVP of 7.8.
- 4. Temperature based on the annual average temperature for Charleston, West Virginia.
- 5. Produced water assumed to have no more than 10% hydrocarbon liquid.
- 6. HAP emissions estimated assuming 6% by weight of the tank gas is HAPs and 73% by weight are VOCs (per ProMax simulation). Speciated HAPs are calculated similarly.
- 7. CO2e emissions estimated assuming 8% of the vent gas by weight is methane and 73% of the vent gas by weight is VOC (per ProMax simulation) and the global warming potential of methane as published in 40 CFR Part 98 Table A-1.

#### Assume 1 truck loaded per hour, 260 bbl truck, for short term emissions

<u></u>											Unice	Jilli Olieu			
						7	Loading	voc	HAP <sup>6</sup>	Benzene	Toluene	E-Benzene	Xylenes	n-Hexane	CO <sub>2</sub> e <sup>7</sup>
Source	S <sup>1</sup>	P (psia) <sup>2</sup>	M <sup>3</sup>	T (ºF)⁴	T (ºR)	(lb/1000 gal)	bbl/hr	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)
Condensate	0.6	3.9	68	60	519.67	3.85	260	42.05	3.42	4.60E-02	8.07E-02		9.22E-03	3.28E+00	118.0
Produced Water <sup>5</sup>	0.6	3.9	68	60	519.67	0.38	260	4.17	0.34	4.56E-03	7.99E-03		9.14E-04	3.25E-01	11.69

Uncontrolled

# **Natural Gas Fueled Fuel Conditioning Heater Emissions**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Location:	Ritchie County, West Virginia
Source Description:	Fuel Conditioning Heater

#### Source Information

Emission Unit ID:	FUEL1					
Source Description:	Fuel Conditi	oning Heater				
Hours of Operation	8,760	hr/yr				
Design Heat Rate	0.50	MMBtu/hr				
Heater Efficiency	80%					
Fuel Heat Value	1,020	Btu/scf				
Fuel Use	5.37	MMscf/yr				

## Emission Calculations per Heater

Pollutant	Emission Factor	Emissions	Emissions	Emission Factor
Poliutant	(lb/MMscf)	(lb/hr)	(tpy)	Source
$NO_X$	100	0.061	0.27	AP-42 Ch. 1.4 Table 1.4-1
CO	84	0.051	0.23	AP-42 Ch. 1.4 Table 1.4-1
VOC	5.5	0.0034	0.015	AP-42 Ch. 1.4 Table 1.4-2
PM <sub>10</sub>	7.6	0.0047	0.020	AP-42 Ch. 1.4 Table 1.4-2
SO <sub>2</sub>	0.6	0.00037	0.0016	AP-42 Ch. 1.4 Table 1.4-2
Formaldehyde	0.075	0.000046	0.00020	AP-42 Ch. 1.4 Table 1.4-3
Total HAPs (including HCHO) <sup>1</sup>	1.9	0.0012	0.0051	AP-42 Ch. 1.4 Table 1.4-3
Pollutant	Emission Factor	Emissions	Emissions	Emission Factor
Poliutant	(kg/MMBtu)	(lb/hr)	(tpy)	Source
Carbon Dioxide	53.06	58.63	256.8	40 CFR Part 98, Subpart C, Table C-1
Methane	0.001	0.0011	0.0048	40 CFR Part 98, Subpart C, Table C-2
Nitrous Oxide	0.0001	0.00011	0.00048	40 CFR Part 98, Subpart C, Table C-2
CO <sub>2</sub> e		58.69	257.1	40 CFR Part 98, Subpart A, Table A-1

<sup>1.</sup> Only those HAP pollutants above detection thresholds were included.

#### Sample Calculations:

# **Component Fugitive Emissions**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia
Source Description:	Fugitive Emissions - Component Leaks

	VOC Fugitive Emissions						
Equipment Type and Service	Number of Units <sup>1</sup>	Hours of Operation (hours/yr)	THC Emission Factor <sup>2</sup> (kg/hr-unit)	VOC Weight Fraction <sup>3</sup>	THC Emissions (tpy)	VOC Emissions (tpy)	
Flanges - Gas Service	836	8,760	3.90E-04	0.18	3.16	0.57	
Valves - Gas Service	250	8,760	4.50E-03	0.18	10.89	1.96	
Compressor Seals Gas Service	33	8,760	8.80E-03	0.18	2.81	0.51	
Flanges - Liquid Service	175	8,760	1.10E-04	0.73	0.19	0.14	
Valves - Liquid Service	42	8,760	2.50E-03	0.73	1.02	0.74	
Total Emissions (tons/yr)					18.06	3.91	

	HAPs Fugitive Emissions									
Equipment Type and Service	Benzene Weight Fraction <sup>3</sup>	Benzene Emissions (tpy)	Toluene Weight Fraction <sup>2</sup>	Toluene Emissions (tpy)	Ethylbenzene Weight Fraction <sup>2</sup>	Ethylbenzene Emissions (tpy)	Xylene Weight Fraction <sup>2</sup>	Xylene Emissions (tpy)	n-Hexane Weight Fraction <sup>2</sup>	n-Hexane Emissions (tpy)
Flanges - Gas Service	8.54E-05	0.00027	1.52E-04	0.00048	1.41E-07	4.44E-07	2.51E-05	0.000079	6.06E-03	0.019
Valves - Gas Service	8.54E-05	0.00093	1.52E-04	0.0017	1.41E-07	1.53E-06	2.51E-05	0.00027	6.06E-03	0.066
Compressor Seals Gas Service	8.54E-05	0.00024	1.52E-04	0.00043	1.41E-07	3.96E-07	2.51E-05	0.000070	6.06E-03	0.017
Flanges - Liquid Service	7.97E-04	0.00015	1.40E-03	0.00026	1.41E-07	2.62E-08	1.60E-04	0.000030	5.68E-02	0.011
Valves - Liquid Service	7.97E-04	0.00081	1.40E-03	0.0014	1.41E-07	1.43E-07	1.60E-04	0.00016	5.68E-02	0.058
Total Emissions (tons/yr)		0.0024		0.0042		2.54E-06		0.00061		0.17

<sup>1)</sup> Component counts from Engineering Lists.

<sup>3)</sup> Gas and liquid weight fractions from representative analyses from nearby facility.

GHG Fugitive Emissions								
Equipment Type	Number of	Hours of Operation	Emission Factor <sup>2</sup>	CH₄ Concentration <sup>3</sup>	CO <sub>2</sub> Concentration <sup>3</sup>	CH₄ Emissions	CO <sub>2</sub> Emissions	CO₂e Emissions
	Units 1	(hours/yr)	(scf/hr-unit)			(tpy)	(tpy)	(tpy)
Flanges	1,011	8,760	0.003	0.98	0.011	0.50	0.015	12.45
Valves	292	8,760	0.027	0.98	0.011	1.29	0.040	32.36
Compressor Seals	33	8,760	0.300	0.98	0.011	1.62	0.050	40.64
Total Emissions (tons/yr)						3.41	0.11	85.45

<sup>1)</sup> Component counts from Engineering Lists.

<sup>2)</sup> API average emission factors are for oil and gas production operations - Table 2.4, EPA Protocol for Equipment Leak Emission Estimates - 1995.

<sup>2)</sup> Emission factors from 40 CFR Part 98 Subpart W, Table W1-A; Gas service where available, else light crude service

<sup>3)</sup> CH<sub>4</sub> and CO<sub>2</sub> concentrations as defined in 40 CFR Part 98.233(r)

# **Fugitive Emissions From Venting Episodes**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia
Source Description:	Fugitive Emissions-Venting Episodes

VOC Venting Emissions							
Type of Event <sup>1</sup>	Number Of Events (event/yr)	Amount Vented per Event (scf/event)	Molecular Weight of Vented Gas (lb/lb-mol)	Total Emissions (ton/yr)	VOC Weight Fraction⁴	VOC Emissions (ton/yr)	
Compressor Blowdown <sup>2</sup>	132	10,000	20.77	36.13	0.18	6.39	
Compressor Startup <sup>3</sup>	132	1,050	20.77	3.79	0.18	0.67	
Plant Shutdown	2	100,000	20.77	5.47	0.18	0.97	
Pigging Venting	52	1,000	20.77	1.42	0.18	0.25	
Total Emissions (tons/yr)						8.28	

	HAPs Venting Emissions									
Type of Event <sup>1</sup>	Benzene Weight Fraction <sup>4</sup>	Benzene Emissions (tpy)	Toluene Weight Fraction <sup>4</sup>	Toluene Emissions (tpy)	Ethylbenzene Weight Fraction <sup>4</sup>	Ethylbenzene Emissions (tpy)	Xylene Weight Fraction <sup>4</sup>	Xylene Emissions (tpy)	n-Hexane Weight Fraction <sup>4</sup>	n-Hexane Emissions (tpy)
Compressor Blowdown <sup>2</sup>	8.54E-05	0.0031	0.00015	0.0054	1.38E-07	0.0000050	2.46E-05	0.00089	6.06E-03	0.22
Compressor Startup <sup>3</sup>	8.54E-05	0.00032	0.00015	0.00057	1.38E-07	0.00000052	2.46E-05	0.000093	6.06E-03	0.023
Plant Shutdown	8.54E-05	0.00047	0.00015	0.00082	1.38E-07	0.00000076	2.46E-05	0.00013	6.06E-03	0.033
Pigging Venting	8.54E-05	0.00012	0.00015	0.00021	1.38E-07	0.00000020	2.46E-05	0.000035	6.06E-03	0.0086
Total Emissions (tons/yr)		0.0040		0.0070		6.48E-06		0.0012		0.28

GHG Venting Emissions								
Type of Event <sup>1</sup>	Number Of Events (event/yr)	Amount Vented per Event (scf/event)	Molecular Weight of Vented Gas (lb/lb-mol)	CH₄ Weight Fraction⁴	CO <sub>2</sub> Weight Fraction <sup>4</sup>	CH₄ Emissions (ton/yr)	CO <sub>2</sub> Emissions (ton/yr)	CO <sub>2</sub> e Emissions (tpy)
Compressor Blowdown <sup>2</sup>	132	10,000	20.77	0.60	0.0043	21.65	0.16	541.31
Compressor Startup <sup>3</sup>	132	1,050	20.77	0.60	0.0043	2.27	0.016	56.84
Plant Shutdown	2	100,000	20.77	0.60	0.0043	3.28	0.024	82.02
Pigging Venting	52	1,000	20.77	0.60	0.0043	0.85	0.0062	21.32
Total Emissions (tons/yr)						28.05	0.20	701.49

- 1) Estimated number of events and venting per event from engineering based on other facilities
- 2) Total number of compressor blowdowns based on 12 blowdowns per compressor.
- 3) Total number of compressor startups based on 12 starts per compressor.
- 4) Weight Fraction is from a gas analysis that will be typical for the facility

# **Fugitive Dust Emissions**

Company:	Antero Midstream LLC
Facility Name:	West Mountain Compressor Station
Facility Location:	Ritchie County, West Virginia
Source Description:	Fugitive Dust Emissions

Gravel Access Road	Loaded Truck Weight <sup>1</sup>	Trips per year <sup>2</sup>	Trips per day <sup>2</sup>	Distance per round trip (truck in and out) <sup>3</sup>		VMT per year <sup>4</sup>
	tons			feet	miles	miles
Condensate Tank Truck	40.00	365	1.0	11,000	2.08	760
Produced Water Tank Truck	40.00	365	1.0	11,000	2.08	760

Equation Parameter	PM-10/PM2.5	PM-Total
<b>E,</b> annual size-specific emission factor for PM <sub>10</sub> & PM <sub>2.5</sub> (upaved industrial roads) extrapolated for natural mitigation <sup>6</sup>	see table below	see table below
<b>k</b> , Particle size multiplier for particle size range (PM <sub>10</sub> ), (lb/VMT) (Source: AP-42 Table 13.2.2-2)	1.5	4.9
<b>k</b> , Particle size multiplier for particle size range (PM <sub>2.5</sub> ), (lb/VMT) (Source: AP-42 Table 13.2.2-2)	0.15	4.9
s, surface material silt content, (%) (Source: AP-42 Table 13.2.2-1)	4.8	4.8
W, mean weight (tons) of the vehicles traveling the road	40.00	40.00
<b>a</b> , constant for PM <sub>10</sub> and PM <sub>2.5</sub> on industrial roads (Source: AP-42 Table 13.2.2-2)	0.9	0.7
<b>b</b> , constant for PM <sub>10</sub> and PM <sub>2.5</sub> on industrial roads (Source: AP-42 Table 13.2.2-2)	0.45	0.45
<b>P</b> , number of "wet" days with at least 0.254 mm (0.01 in) of precipitation during the averaging period, based on AP-42 Figure 13.2.2-1.	160	160

$$E = \left[ k \left( \frac{s}{12} \right)^a \times \left( \frac{W}{3} \right)^b \right] \times (365 - P/365)$$

Source of Equation: AP-42 Section 13.2.2

#### PM<sub>10</sub> Emissions

Emission Factor (lb/VMT)	Vehicle miles traveled (VMT/yr) <sup>4</sup>	Annual Uncontrolled PM <sub>10</sub> Emissions (tpy)
1.18	1,520.83	0.90

#### PM<sub>2.5</sub> Emissions (tons/yr)

Emission Factor (lb/VMT)	Vehicle miles traveled (VMT/yr) <sup>4</sup>	Annual Uncontrolled PM <sub>2.5</sub> Emissions (tpy)
0.118	1,520.83	0.090

#### PM- Total Emissions (tons/yr)

Emission Factor (lb/VMT)	Vehicle miles traveled (VMT/yr) <sup>4</sup>	Annual Uncontrolled PM-Total Emissions (tpy)
4.65	1,520.83	3.53

#### Table Notes:

- 1. Loaded truck weight is based on typical weight limit for highway vehicles.
  2. Based on production, it's assumed a maximum of one condensate truck (200 ppi truck) and one produced water truck (200 ppi truck) will be onsite per day.
- 3. Distance per round trip is based on the proposed site layout. The one way distance is measured as 5,500 feet for the gravel access road.
- 4. VMT/yr = Trips/yr x Roundtrip Distance
- 5. Hourly emissions determined from tons per year calculation using 2,000 lb/ton and 8,760 hours per year.

# **Facility Gas Analysis**

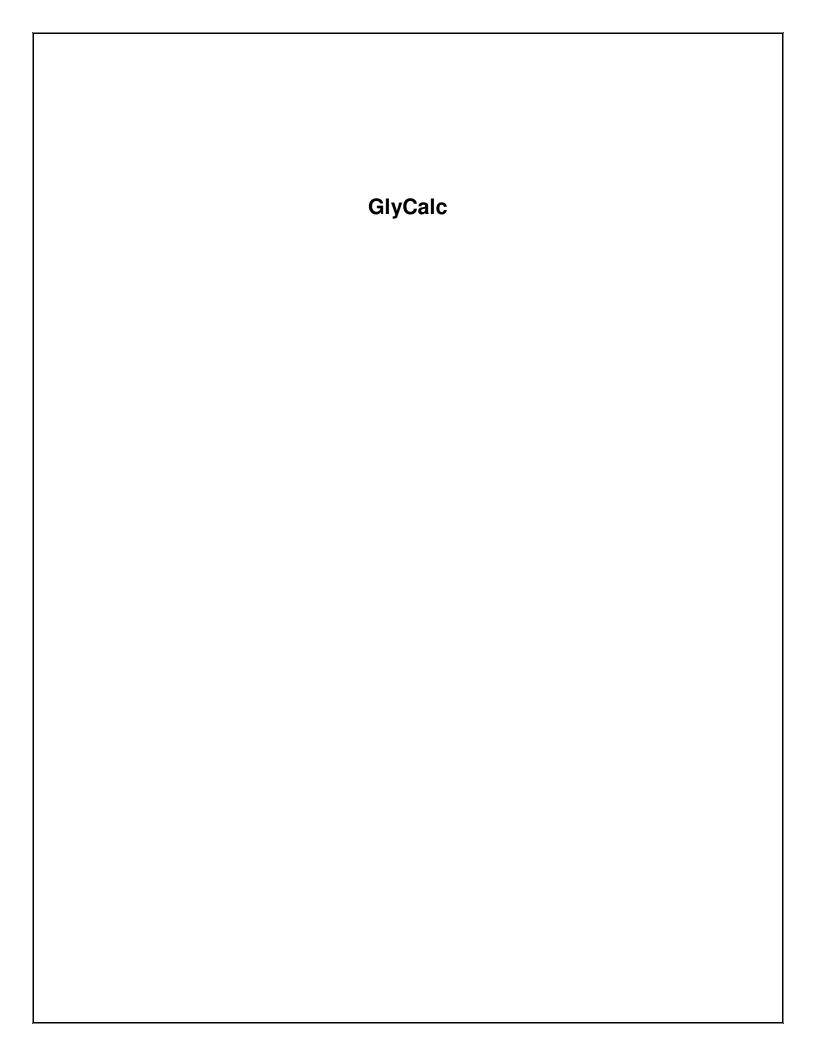
	MOL %	MW	Component Weight lb/lb-mol	Wt. Fraction
Methane	77.60	16.04	12.45	0.60
Ethane	14.27	30.07	4.29	0.21
Propane	4.14	44.10	1.83	0.088
i-Butane	0.57	58.12	0.33	0.016
n-Butane	1.05	58.12	0.61	0.029
i-Pentane	0.31	72.15	0.22	0.011
n-Pentane	0.31	72.15	0.22	0.011
Hexanes	0.12	86.18	0.10	0.0049
Heptanes	0.11	100.20	0.11	0.0051
Octanes	0.040	114.23	0.046	0.0022
Nonanes	0.00040	128.26	0.00051	0.000025
Decanes	0.051	142.28	0.072	0.0035
n-Hexane	0.15	86.18	0.13	0.0061
Benzene	0.0023	78.11	0.0018	0.000085
Toluene	0.0034	92.14	0.0031	0.00015
Ethylbenzene	0.0000027	106.17	0.0000029	0.0000014
Xylenes	0.00048	106.16	0.00051	0.000025
Nitrogen	0.79	28.01	0.22	0.011
Carbon Dioxide	0.20	44.01	0.090	0.0043
Water	0.29	18.02	0.053	0.0025
Totals	100.0		20.77	1.00

Heating Value (Btu/scf)	1,130.10
Molecular weight	20.77
-	
VOC weight fraction	0.18
Methane weight fraction	0.60
THC weight fraction	0.98
VOC of THC wt fraction	0.18
CH4 of THC wt fraction	0.61
Benzene of THC wt fraction	0.000087
Toluene of THC wt fraction	0.00015
E-benzene of THC wt fraction	0.00000014
Xylene of THC wt fraction	0.000025
n-Hexane of THC wt fraction	0.0062

# **Facility Liquids Analysis**

	MOL %	MW	Component Weight lb/lb-mol	Wt. Fraction
Methane	21.05	16.04	3.38	0.082
Ethane	22.03	30.07	6.62	0.16
Propane	18.41	44.10	8.12	0.20
i-Butane	4.66	58.12	2.71	0.066
n-Butane	10.30	58.12	5.99	0.14
i-Pentane	4.35	72.15	3.14	0.076
n-Pentane	4.73	72.15	3.41	0.083
Hexanes	4.96	86.18	4.28	0.10
n-Hexane	2.73	86.18	2.35	0.057
Benzene	0.042	78.11	0.033	0.00080
Toluene	0.063	92.14	0.058	0.0014
Ethylbenzene		106.17		
Xylenes	0.0062	106.16	0.0066	0.00016
Nitrogen	0.067	28.01	0.019	0.00046
Carbon Dioxide	0.15	44.01	0.067	0.0016
Water	6.46	18.02	1.16	0.028
Totals	100.00		41.34	1.00

Molecular weight	41.34
VOC weight fraction	0.73
Methane weight fraction	0.082
THC weight fraction	0.97
VOC of THC wt fraction	0.75
CH4 of THC wt fraction	0.084
Benzene of THC wt fraction	0.00082
Toluene of THC wt fraction	0.0014
E-benzene of THC wt fraction	
Xylene of THC wt fraction	0.00016
n-Hexane of THC wt fraction	0.059



#### GlyCalc Inputs\_West Mountain

#### GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES

Case Name: West Mountain Compressor Station File Name: W:\20163883\_Antero WV Synth Minor Mods\2.0 Technical Information\2.9 Deliverables to Client\West Mountain CS\Application - WVDEP\Attachment N\Dehy

Runs\West Mountain Dehy.ddf

Date: May 16, 2016

#### DESCRIPTION:

Description: Two (2) 72.5 MMscf/day TEG dehydration

Kimray 45015 PV glycol pump

Annual Hours of Operation: 8760.0 hours/yr

#### WET GAS:

Temperature: 120.00 deg. F Pressure: 1100.00 psig

Wet Gas Water Content: Saturated

Component	Conc. (vol %)
Carbon Dioxide	0.2047
Nitrogen	0.7919
Methane	77.5951
Ethane	14.2679
Propane	4.1421
Isobutane	0.5702
n-Butane	1.0474
Isopentane	0.3104
n-Pentane	0.3100
n-Hexane	0.1462
Other Hexanes	0.1176
Heptanes	0.1065
Benzene	0.0023
Toluene	0.0034
Ethylbenzene	0.0000
Xylenes	0.0005
C8+ Heavies	0.0907

DRY GAS:

Flow Rate: 72.5 MMSCF/day Water Content: 5.0 lbs. H2O/MMSCF

LEAN GLYCOL:

Glycol Type: TEG

GlyCalc Inputs\_West Mountain
Water Content: 1.5 wt% H2O
Recirculation Ratio: 3.0 gal/lb H2O

PUMP:		

Glycol Pump Type: Gas Injection
Gas Injection Pump Volume Ratio: 0.032 acfm gas/gpm glycol

FLASH TANK:

Flash Control: Combustion device Flash Control Efficiency: 98.00 %
Temperature: 80.0 deg. F
Pressure: 5.0 psig

STRIPPING GAS:

Source of Gas: Dry Gas Gas Flow Rate: 9.000 scfm

REGENERATOR OVERHEADS CONTROL DEVICE:

Control Device: Condenser

Temperature: 200.0 deg. F Pressure: 14.7 psia

 $\begin{array}{cccc} & \text{Control Device:} & \text{Combustion Device} \\ \text{Destruction Efficiency:} & 98.0 \% \\ & \text{Excess Oxygen:} & 0.0 \% \\ \text{Ambient Air Temperature:} & 0.0 \text{ deg. F} \\ \end{array}$ 

#### GlyCalc Outputs\_West Mountain

#### GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: West Mountain Compressor Station
File Name: W:\20163883\_Antero WV Synth Minor Mods\2.0 Technical Information\2.9
Deliverables to Client\West Mountain CS\Application - WVDEP\Attachment N\Dehy
Runs\West Mountain Dehy.ddf
Date: May 16, 2016

#### **DESCRIPTION:**

Description: Two (2) 72.5 MMscf/day TEG dehydration

Kimray 45015 PV glycol pump

Annual Hours of Operation: 8760.0 hours/yr

#### EMISSIONS REPORTS:

#### CONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.3630	8.712	1.5899
Ethane	0.1373	3.295	0.6013
Propane	0.0711	1.707	0.3114
Isobutane	0.0158	0.380	0.0693
n-Butane	0.0356	0.854	0.1559
Isopentane	0.0139	0.335	0.0611
n-Pentane	0.0174	0.418	0.0763
n-Hexane	0.0176	0.422	0.0770
Other Hexanes	0.0103	0.247	0.0451
Heptanes	0.0320	0.768	0.1402
Benzene	0.0188	0.452	0.0824
Toluene	0.0421	1.010	0.1842
Ethylbenzene	<0.0001	0.001	0.0002
Xylenes	0.0112	0.268	0.0490
C8+ Heavies	0.1833	4.399	0.8029
Total Emissions	0.9695	23.267	4.2463
Total Hydrocarbon Emissions	0.9695	23.267	4.2463
Total VOC Emissions	0.4692	11.261	2.0551
Total HAP Emissions	0.0897	2.153	0.3929
Total BTEX Emissions	0.0721	1.731	0.3158

#### UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane Ethane Propane Isobutane	18.1508 6.8649 3.5557 0.7911 Page 1	435.619 164.758 85.337 18.986	79.5004 30.0684 15.5740 3.4649

GlyCalo	c Outputs_Wes	st Mountain	7.7978
n-Butane	1.7803	42.728	
Isopentane	0.6974	16.737	3.0544
n-Pentane	0.8713	20.912	3.8164
n-Hexane	0.8794	21.105	3.8516
Other Hexanes	0.5143	12.344	2.2527
Heptanes	1.6008	38.418	7.0113
Benzene	0.9418	22.604	4.1252
Toluene	2.1044	50.505	9.2172
Ethylbenzene	0.0023	0.054	0.0099
Xylenes	0.5591	13.419	2.4490
C8+ Heavies	9.1659	219.981	40.1466
Total Emissions	48.4794	1163.506	212.3398
Total Hydrocarbon Emissions	48.4794	1163.506	212.3398
Total VOC Emissions	23.4637	563.129	102.7710
Total HAP Emissions	4.4870	107.687	19.6529
Total BTEX Emissions	3.6076	86.582	15.8013

#### FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	1.8788	45.090	8.2290
Ethane	0.8820	21.168	3.8632
Propane	0.4284	10.281	1.8762
Isobutane	0.0836	2.007	0.3662
n-Butane	0.1721	4.130	0.7538
Isopentane	0.0576	1.381	0.2521
n-Pentane	0.0637	1.529	0.2790
n-Hexane	0.0387	0.930	0.1697
Other Hexanes	0.0288	0.691	0.1262
Heptanes	0.0340	0.817	0.1490
Benzene	0.0014	0.033	0.0059
Toluene	0.0017	0.041	0.0075
Ethylbenzene	<0.0001	<0.001	<0.0001
Xylenes	0.0001	0.004	0.0006
C8+ Heavies	0.0263	0.630	0.1150
Total Emissions	3.6972	88.732	16.1936
Total Hydrocarbon Emissions	3.6972	88.732	16.1936
Total VOC Emissions	0.9364	22.473	4.1014
Total HAP Emissions	0.0420	1.007	0.1838
Total BTEX Emissions	0.0032	0.077	0.0141

#### FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Methane Ethane Propane Isobutane n-Butane	93.9385 44.1008 21.4179 4.1806 8.6047 Page 2	2254.525 1058.420 514.030 100.334 206.513	411.4507 193.1617 93.8105 18.3109 37.6886

# GlyCalc Outputs\_West Mountain

Isopentane	2.8775	69.061	12.6036
n-Pentane	3.1851	76.442	13.9507
n-Hexane	1.9372	46.493	8.4850
Other Hexanes	1.4404	34.570	6.3090
Heptanes	1.7014	40.834	7.4522
Benzene	0.0679	1.629	0.2973
Toluene	0.0856	2.055	0.3750
Ethylbenzene	<0.0001	0.001	0.0002
Xylenes	0.0074	0.177	0.0323
C8+ Heavies	1.3133	31.520	5.7524
Total Emissions	184.8585	4436.603	809.6801
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	184.8585	4436.603	809.6801
	46.8191	1123.659	205.0677
	2.0981	50.355	9.1897
	0.1609	3.862	0.7048

## COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	2.2418	53.802	9.8189
Ethane	1.0193	24.463	4.4645
Propane	0.4995	11.987	2.1877
Isobutane	0.0994	2.386	0.4355
n-Butane	0.2077	4.985	0.9097
Isopentane	0.0715	1.716	0.3132
n-Pentane	0.0811	1.947	0.3553
n-Hexane	0.0563	1.352	0.2467
Other Hexanes	0.0391	0.938	0.1712
Heptanes	0.0660	1.585	0.2893
Benzene	0.0202	0.484	0.0884
Toluene	0.0438	1.051	0.1917
Ethylbenzene	<0.0001	0.001	0.0002
Xylenes	0.0113	0.272	0.0496
C8+ Heavies	0.2096	5.030	0.9179
Total Emissions	4.6666	111.999	20.4399
Total Hydrocarbon Emissions	4.6666	111.999	20.4399
Total VOC Emissions	1.4056	33.734	6.1564
Total HAP Emissions	0.1317	3.160	0.5767
Total BTEX Emissions	0.0753	1.808	0.3299

## COMBINED REGENERATOR VENT/FLASH GAS EMISSION CONTROL REPORT:

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Component		ntrolled ( tons/yr	Controlled % tons/yr	Reduction
	Ethane	490.9511 223.2301 109.3845 Page 3	9.8189 4.4645 2.1877	98.00 98.00 98.00

GlyCalc Isobutane n-Butane	Outputs_West 21.7758 45.4864	Mountain 0.4355 0.9097	98.00 98.00
Isopentane	15.6580	0.3132	98.00
n-Pentane	17.7672	0.3553	98.00
n-Hexane	12.3366	0.2467	98.00
Other Hexanes	8.5617	0.1712	98.00
Heptanes	14.4635	0.2893	98.00
Benzene	4.4224	0.0884	98.00
Toluene	9.5922	0.1917	98.00
Ethylbenzene	0.0101	0.0002	98.00
Xylenes	2.4813	0.0496	98.00
C8+ Heavies	45.8990	0.9179	98.00
Total Emissions	1022.0199	20.4399	98.00
Total Hydrocarbon Emissions	1022.0199	20.4399	98.00
Total VOC Emissions	307.8387	6.1564	98.00
Total HAP Emissions	28.8426	0.5767	98.00
Total BTEX Emissions	16.5060	0.3299	98.00

#### EQUIPMENT REPORTS:

#### CONDENSER AND COMBUSTION DEVICE

Condenser Outlet Temperature: 200.00 deg. F Condenser Pressure: 14.70 psia Condenser Duty: 2.58e-001 MM BTU/hr Produced Water: 11.29 bbls/day

Ambient Temperature: 0.00 deg. F

Excess Oxygen: 0.00 %

Combustion Efficiency: 98.00 %

Supplemental Fuel Requirement: 2.58e-001 MM BTU/hr 0.00 % 98.00 %

Component	Emitted	Destroyed	
Methane Ethane Propane Isobutane n-Butane	2.00% 2.00% 2.00% 2.00% 2.00% 2.00%	98.00% 98.00% 98.00% 98.00% 98.00%	
Isopentane	2.00%	98.00%	
n-Pentane	2.00%	98.00%	
n-Hexane	2.00%	98.00%	
Other Hexanes	2.00%	98.00%	
Heptanes	2.00%	98.00%	
Benzene	2.00%	98.00%	
Toluene	2.00%	98.00%	
Ethylbenzene	2.00%	98.00%	
Xylenes	2.00%	98.00%	
C8+ Heavies	2.00%	98.00%	

Calculated Absorber Stages:
Specified Dry Gas Dew Point:
Temperature:
Pressure:
Dry Gas Flow Rate:
Glycol Losses With Dry Gas:
Temperature:
120.0 deg. F
1100.0 psig
72.5000 MMSCF/day
4.6796 lb/hr

Wet Gas Water Content: Saturated

Calculated Wet Gas Water Content: 95.21 lbs. H2O/MMSCF Specified Lean Glycol Recirc. Ratio: 3.00 gal/lb H2O

Component	Remaining in Dry Gas	Absorbed in Glycol
Water	5.24%	94.76%
Carbon Dioxide	99.75%	0.25%
Nitrogen	99.97%	0.03%
Methane	99.98%	0.02%
Ethane	99.94%	0.06%
Propane	99.92%	0.08%
Isobutane	99.90%	0.10%
n-Butane	99.88%	0.12%
Isopentane	99.89%	0.11%
n-Pentane	99.86%	0.14%
n-Hexane	99.81%	0.19%
Other Hexanes	99.85%	0.15%
Heptanes	99.70%	0.30%
Benzene	92.96%	7.04%
Toluene	91.25%	8.75%
Ethylbenzene	90.01%	9.99%
Xylenes	86.23%	13.77%
C8+ Heavies	99.24%	0.76%

#### FLASH TANK

Flash Control: Combustion device

Flash Control: Compuscion 25.0 Flash Control Efficiency: 98.00 %
Flash Temperature: 80.0 deg. F

Component	Left in Glycol	Removed in Flash Gas
Water Carbon Dioxide Nitrogen Methane Ethane	99.89% 6.77% 0.38% 0.41% 1.66%	0.11% 93.23% 99.62% 99.59% 98.34%
Propane Isobutane n-Butane Isopentane n-Pentane	4.25% 7.08% 9.59% 11.88% 15.06% Page 5	95.75% 92.92% 90.41% 88.12% 84.94%

#### GlyCalc Outputs\_West Mountain

n-Hexane	26.80%	73.20%
Other Hexanes	20.97%	79.03%
Heptanes	46.21%	53.79%
Benzene	93.60%	6.40%
Toluene	96.39%	3.61%
Ethylbenzene	98.20%	1.80%
Xylenes	98.86%	1.14%
C8+ Heavies	88.62%	11.38%

#### REGENERATOR

MEGLINEN TOK

#### Regenerator Stripping Gas:

Dry Product Gas

Stripping Gas Flow Rate: 9.0000 scfm

Component	Remaining in Glycol	Distilled Overhead
Water	29.65%	70.35%
Carbon Dioxide	0.00%	100.00%
Nitrogen	0.00%	100.00%
Methane	0.00%	100.00%
Ethane	0.00%	100.00%
Propane	0.00%	100.00%
Isobutane	0.00%	100.00%
n-Butane	0.00%	100.00%
Isopentane	2.53%	97.47%
n-Pentane	2.17%	97.83%
n-Hexane	1.35%	98.65%
Other Hexanes	3.23%	96.77%
Heptanes	0.87%	99.13%
Benzene	5.29%	94.71%
Toluene	8.14%	91.86%
Ethylbenzene	10.54%	89.46%
Xylenes	13.04%	86.96%
C8+ Heavies	12.53%	87.47%

#### STREAM REPORTS:

#### WET GAS STREAM

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Temperature: 120.00 deg. F Pressure: 1114.70 psia Flow Rate: 3.03e+006 scfh

Component Conc. Loading (vol%) (lb/hr)

Water 2.01e-001 2.88e+002
Page 6

```
GlyCalc Outputs_West Mountain
Carbon Dioxide 2.05e-001 7.19e+002
Nitrogen 7.93e-001 1.77e+003
Methane 7.77e+001 9.94e+004
Ethane 1.43e+001 3.43e+004

Propane 4.15e+000 1.46e+004
Isobutane 5.71e-001 2.65e+003
n-Butane 1.05e+000 4.86e+003
Isopentane 3.11e-001 1.79e+003
n-Pentane 3.10e-001 1.79e+003

Other Hexanes 1.18e-001 8.10e+002
Heptanes 1.07e-001 8.53e+002
Benzene 2.27e-003 1.42e+001
Toluene 3.37e-003 2.48e+001

Ethylbenzene 2.71e-006 2.30e-002
Xylenes 4.83e-004 4.09e+000
C8+ Heavies 9.08e-002 1.23e+003

Total Components 100.00 1.66e+005
```

#### DRY GAS STREAM

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Temperature: 120.00 deg. F Pressure: 1114.70 psia Flow Rate: 3.02e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	1.05e-002 2.05e-001 7.94e-001 7.78e+001 1.43e+001	7.18e+002 1.77e+003 9.94e+004
Isobutane n-Butane Isopentane	4.15e+000 5.71e-001 1.05e+000 3.11e-001 3.11e-001	2.64e+003 4.86e+003 1.79e+003
Other Hexanes Heptanes Benzene	1.46e-001 1.18e-001 1.07e-001 2.12e-003 3.08e-003	8.08e+002 8.50e+002 1.32e+001
Ethylbenzene Xylenes C8+ Heavies	4.17e-004	3.53e+000
Total Components	100.00	1.66e+005

LEAN GLYCOL STREAM

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Temperature: 120.00 deg. F

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Component	Conc. (wt%)	Loading (lb/hr)
Water Carbon Dioxide Nitrogen	9.85e+001 1.50e+000 2.30e-012 5.99e-013 9.65e-018	1.15e+002 1.76e-010 4.59e-011
Propane Isobutane	1.23e-007 6.24e-009 1.01e-009 1.93e-009 1.28e-004	4.78e-007 7.72e-008 1.48e-007
n-Hexane Other Hexanes Heptanes	1.60e-004 1.25e-004 1.61e-004 1.66e-004 6.84e-004	9.57e-003 1.23e-002 1.27e-002
Ethylbenzene	1.09e-003	2.67e-004 8.37e-002
Total Components	100.00	7.67e+003

#### RICH GLYCOL AND PUMP GAS STREAM

Temperature: 120.00 deg. F Pressure: 1114.70 psia Flow Rate: 1.46e+001 gpm NOTE: Stream has more than one phase.

Component		Loading (1b/hr)
Water Carbon Dioxide Nitrogen	9.27e+001 4.76e+000 2.80e-002 2.14e-002 1.16e+000	3.88e+002 2.29e+000 1.75e+000
Propane Isobutane	5.50e-001 2.74e-001 5.52e-002 1.17e-001 4.00e-002	2.24e+001 4.50e+000 9.52e+000
n-Hexane Other Hexanes Heptanes	4.60e-002 3.25e-002 2.24e-002 3.88e-002 1.30e-002	2.65e+000 1.82e+000 3.16e+000
Ethylbenzene	2.91e-002 3.16e-005 7.97e-003 Page 8	2.58e-003

# GlyCalc Outputs\_West Mountain C8+ Heavies 1.42e-001 1.15e+001 Total Components 100.00 8.15e+003

# FLASH TANK OFF GAS STREAM

\_\_\_\_\_

Temperature: 80.00 deg. F Pressure: 19.70 psia Flow Rate: 3.15e+003 scfh

Component	Conc. (vol%)	Loading (1b/hr)
Carbon Dioxide Nitrogen Methane	2.81e-001 5.83e-001 7.48e-001 7.05e+001 1.76e+001	2.13e+000 1.74e+000 9.39e+001
Isobutane n-Butane Isopentane	5.84e+000 8.65e-001 1.78e+000 4.80e-001 5.31e-001	4.18e+000 8.60e+000 2.88e+000
Other Hexanes Heptanes Benzene	2.70e-001 2.01e-001 2.04e-001 1.05e-002 1.12e-002	1.44e+000 1.70e+000 6.79e-002
Ethylbenzene Xylenes C8+ Heavies	8.36e-004	7.38e-003

# FLASH TANK GLYCOL STREAM

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Total Components 100.00 1.89e+002

Temperature: 80.00 deg. F Flow Rate: 1.42e+001 gpm

Component	Conc. (wt%)	Loading (1b/hr)
Water Carbon Dioxide Nitrogen	9.49e+001 4.87e+000 1.94e-003 8.35e-005 4.84e-003	3.88e+002 1.55e-001 6.65e-003
Propane Isobutane	9.33e-003 1.19e-002 4.00e-003 1.15e-002 4.87e-003	9.50e-001 3.18e-001 9.12e-001
	7.09e-003 8.91e-003 Page 9	

```
GlyCalc Outputs_West Mountain
Other Hexanes 4.80e-003 3.82e-001
Heptanes 1.83e-002 1.46e+000
Benzene 1.25e-002 9.92e-001

Toluene 2.87e-002 2.29e+000
Ethylbenzene 3.18e-005 2.53e-003
Xylenes 8.06e-003 6.42e-001
C8+ Heavies 1.28e-001 1.02e+001
Total Components 100.00 7.97e+003
```

#### FLASH GAS EMISSIONS

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Flow Rate: 1.21e+004 scfh

Control Method: Combustion Device

Control Efficiency: 98.00

Component	Conc. (vol%)	Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	6.22e+001 3.71e+001 1.95e-001 3.68e-001 9.21e-002	5.20e+002 1.74e+000 1.88e+000
Isobutane n-Butane Isopentane	3.05e-002 4.52e-003 9.30e-003 2.51e-003 2.77e-003	8.36e-002 1.72e-001 5.76e-002
Other Hexanes Heptanes Benzene	1.41e-003 1.05e-003 1.07e-003 5.46e-005 5.84e-005	2.88e-002 3.40e-002 1.36e-003
Ethylbenzene Xylenes C8+ Heavies Total Components	4.37e-006 4.84e-004	1.48e-004

#### REGENERATOR OVERHEADS STREAM

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Temperature: 212.00 deg. F Pressure: 14.70 psia Flow Rate: 6.38e+003 scfh

#### CONDENSER PRODUCED WATER STREAM

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Temperature: 200.00 deg. F Flow Rate: 3.29e-001 gpm

Compon	ent	Conc. (wt%)	Loading (1b/hr)	(ppm)
Car	bon Dioxide Nitrogen Methane	1.00e+002 5.62e-005 1.73e-005 1.04e-003 3.99e-004	9.25e-005 2.85e-005 1.72e-003	999962. 1. 0. 10.
	Isobutane n-Butane Isopentane	2.21e-004 4.31e-005 1.00e-004 3.69e-005 4.62e-005	7.11e-005 1.65e-004 6.07e-005	2. 0. 1. 0.
Ot	her Hexanes Heptanes Benzene	4.52e-005 2.61e-005 7.87e-005 4.14e-004 7.01e-004	4.29e-005 1.30e-004 6.82e-004	0. 0. 1. 4. 7.
	thylbenzene Xylenes C8+ Heavies	1.66e-004	2.73e-004	0. 2. 4.
Total	Components	100.00	1.65e+002	1000000.

#### CONDENSER RECOVERED OIL STREAM

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Temperature: 200.00 deg. F

The calculated flow rate is less than 0.000001 #mol/hr. The stream flow rate and composition are not reported.

#### CONDENSER VENT STREAM

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Temperature: 200.00 deg. F Pressure: 14.70 psia Flow Rate: 2.91e+003 scfh

Loading Component Conc. (vo1%) (lb/hr) Water 7.85e+001 1.08e+002 Carbon Dioxide 8.39e-002 2.83e-001
Nitrogen 1.51e-001 3.23e-001
Methane 1.48e+001 1.81e+001
Ethane 2.98e+000 6.86e+000 Propane 1.05e+000 3.56e+000 Isobutane 1.78e-001 7.91e-001 n-Butane 4.00e-001 1.78e+000 Isopentane 1.26e-001 6.97e-001 n-Pentane 1.58e-001 8.71e-001 n-Hexane 1.33e-001 8.79e-001 Other Hexanes 7.79e-002 5.14e-001 Heptanes 2.09e-001 1.60e+000 Benzene 1.57e-001 9.41e-001 Toluene 2.98e-001 2.10e+000 Ethylbenzene 2.79e-004 2.27e-003 Xylenes 6.87e-002 5.59e-001 C8+ Heavies 7.02e-001 9.17e+000 Total Components 100.00 1.57e+002

#### COMBUSTION DEVICE OFF GAS STREAM

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Temperature: 1000.00 deg. F Pressure: 14.70 psia Flow Rate: 1.24e+001 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Ethane Propane Isobutane	6.93e+001 1.40e+001 4.94e+000 8.34e-001 1.88e+000	1.37e-001 7.11e-002 1.58e-002
n-Hexane Other Hexanes	7.40e-001 6.25e-001	1.74e-002 1.76e-002 1.03e-002
Toluene Ethylbenzene	3.22e-001	4.21e-002 4.53e-005 1.12e-002
Total Components	100.00 Page 12	9.69e-001

Attachment O. Monitoring, Recordkeeping, Reporting, and Testing Plans	

# Monitoring, Recordkeeping, Reporting, and Testing Plans

The following is a summary of the methods to comply with the requirements of West Virginia Division of Air Quality (WVDAQ) 45CSR13 rules and regulations for the West Mountain Compressor Station, including federal and state regulatory requirements.

# 1. Summary of Key Operational Throughput Limits

- a. Maximum wet gas throughput into each Dehy: 72.5 MMscf/day or 26,462.5 MMscf/year.
- b. Maximum liquids loaded out: 2,989,350 gallons per year.
- c. Maximum fuel use for all compressor engines: 1,185,228,000 scf/year.

# 2. Operational Requirements

- a. Compressor engines will operate with the catalytic converter in place at all times and will be fueled by natural gas only.
- b. Catalysts installed on all compressor engines will be operated per manufacturer instructions.
- c. Reciprocating compressor rod packing will be replaced within 36 months of last packing/startup or within 26,000 operating hours, whichever comes first.
- d. Microturbines will be fueled by natural gas only.
- e. Each Dehy Reboiler will operate at no more than 1.5 MMBtu/hr and be fueled only by natural gas or off-gases from the Dehydrator flash tanks.
- f. No fuel-burning unit of any kind will have opacity greater than 10 percent based on a six minute block average observation.
- g. The Dehy Flare capacity will not exceed 4.80 MMBtu/hr, will achieve 98 percent destruction efficiency, will operate at all times that gas is vented to it, will have a flame present at all times, and will have no visible emissions other than for periods not to exceed a total of 5 minutes during any 2 consecutive hours.
- h. The flare will be operated per manufacturer instructions.
- i. Produced water, Condensate, and Settling storage tanks potential emissions will be routed to the VRU with recovery greater than 98 percent at all times.
- j. Storage tanks will be covered and routed to a closed vent system with no detectable emissions.
- k. Liquid loadout trucks will use the submerged-fill method.
- I. Dehydrator still vents will be controlled by the flare.
- m. Dehydrator flash tank vent gas will be used in the reboiler as fuel or routed to the VRU system.

#### 3. Monitoring

- Non-certified engines will be stack tested within 1 year of startup and every 8,760 hours of operation thereafter.
- b. Catalyst inlet temperature will be monitored.

- c. Compressor run time or number of months since compressor rod repacking will be monitored or tracked.
- Daily, monthly, and rolling 12-month average wet gas throughput for the Dehy will be monitored.
- e. Initial Method 22 observation of the Reboiler exhaust and flare will be conducted for a minimum of 2 hours.
- Monthly Method 22 observations of the Reboiler exhaust and flare will be conducted for a minimum of 10 minutes each.
- g. Monthly olfactory, visual, and auditory inspections will be conducted of the tanks closed vent and control system (flare) for leaks or defects that could result in emissions. Repair leaks as soon as practicable (no later than 5 days for first attempt).
- h. The presence of flare flame will continuously be monitored.
- i. Monthly and rolling twelve-month average amount of liquids loaded out will be monitored.

#### 4. Recordkeeping

- a. Records will be kept on-site for a minimum of 2 years, and in company records (on or off-site) for a minimum of 5 years.
- b. Records of inspection, observations, preventive maintenance, malfunctions, and shutdowns of all onsite equipment will be kept.
- c. Records of the date, time, duration of each time that a flame is not present at the flare and startup, shutdown, malfunctions of the flare will be kept.
- d. Records of engine maintenance and engine run time will be kept.
- e. Records of catalyst inlet temperature will be kept.
- Records of the actual annual average natural gas throughput in the dehy will be kept.

#### 5. Notifications and Reports

- a. WVDAQ will be notified within 30 calendar days of commencement of construction.
- b. WVDAQ will be notified within 30 calendar days of startup.
- c. Upon startup, a Certificate to Operate (CTO) application will be filed and fees to WVDAQ will be paid for the period from startup to the following June 30 and then the CTO and fees will be renewed and paid annually. CTO will be maintained on-site.
- d. An annual report of compliance with 40 CFR 60 Subpart OOOO for the compressors and storage tanks (for settling tank only) will be submitted within 90 days after one year of operation (i.e., within 90 days after 12 months after initial startup).
- e. For stack testing, a protocol will be filed at least 30 days prior to test and WVDAQ and EPA will be notified of the test at least 15 days prior to the test. Results will be reported within 60 days of the test.
- f. If operations are suspended for 60 days or more, WVDAQ will be notified within 2 weeks after the 60th day.

Attachment P. Public Notice

# AIR QUALITY PERMIT NOTICE Notice of Application – West Mountain Compressor Station

Notice is given that Antero Midstream LLC has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a 45CSR13 Construction Permit Modification (R13-3215) for a Natural Gas Compressor Station located at 1739 Mountain Drive in Pennsboro, West Virginia within Ritchie County. The latitude and longitude coordinates are: 39.321042N, 80.978431W.

The applicant estimates the difference in the potential to discharge of the following Regulated Air Pollutants will be:

Pollutant	Change in Annual Emissions (tpy)
Nitrogen Oxides (NOx)	-26.27
Carbon Monoxide (CO)	-24.75
Volatile Organic Compounds (VOC)	-29.23
Particulate Matter less than 10 μm (PM <sub>10</sub> )	1.35
Particulate Matter less than 2.5 μm (PM <sub>2.5</sub> )	1.35
Sulfur Dioxide (SO <sub>2</sub> )	0.04
Formaldehyde	-1.03
Benzene	0.14
Toluene	0.12
Ethylbenzene	0.003
Xylenes	0.04
Total HAPs	-0.03
Carbon Dioxide equivalent (CO₂e)	7,336

Note that negative numbers in the table above denote a decrease in potential emissions.

Startup of modified operation is planned to begin on or about the 1st day of September 2016. Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57<sup>th</sup> Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1250, during normal business hours.

Dated this the 7<sup>th</sup> day of June.

By: Antero Midstream LLC
Barry Schatz
Midstream Environmental Supervisor
1615 Wynkoop Street
Denver, CO 80202

Attachment R.			
	Authority/Delegation	of Authority	

# Attachment R AUTHORITY OF CORPORATION OR OTHER BUSINESS ENTITY (DOMESTIC OR FOREIGN)

TO;	The West Virginia Department of Environmental Protection, Division of Air Quality
DATE:	August 5 , 2015
ATTN.:	Director
Corporation's	s / other business entity's Federal Employer I.D. Number46-5517375
Protection, D	ndersigned hereby files with the West Virginia Department of Environmental Pivision of Air Quality, a permit application and hereby certifies that the said ade name which is used in the conduct of an incorporated business or other ity.
Furthe	er, the corporation or the business entity certifies as follows:
(1)	Luz Slauter and Barry Schatz (is/are) the authorized
	representative(s) and in that represent the interest of the corporation or the business entity and may legally bind the corporation or the business entity.
(2) State of Wes	The corporation or the business entity is authorized to do business in the st Virginia.
Virginia Depa such change	M.M. Gar
ward McNeill	ly, Vice President - Vice President Reserves Planning & Midstream
(Vice President official in character)	Other Authorized Officer lent, Secretary, Treasurer or other lrge of a principal business function of on or the business entity)
	resident, then the corporation or the business entity must submit certified ylaws stating legal authority of other authorized officer to bind the corporation ess entity).
Socretary	
Secretary	Antero Midstream LLC
	Name of Corporation or business entity