

Williams Ohio Valley Midstream LLC Park Place Corporate Center 2 2000 Commerce Drive Pittsburgh, PA 15275 (412) 787-7300 (412) 787-6002 fax

May 27, 2015 (Via Federal Express)

Beverly McKeone New Source Review Program Manager Division of Air Quality **West Virginia Department of Environmental Protection** 601 57th Street SE Charleston, WV 25304-2345

**Subject:** Application for 45CSR13 NSR Modification Permit

Williams Ohio Valley Midstream LLC YOHO COMPRESSOR STATION Wetzel County, West Virginia

Dear Ms. McKeone,

Williams Ohio Valley Midstream LLC (OVM) is submitting an Application for 45CSR13 New Source Review (NSR) Modification Permit for the existing Yoho Compressor Station, located approximately 3.0 Miles South-Southeast of New Martinsville, approximately 0.1 Mile Northwest of Slim Chance Road, Wetzel County, West Virginia.

This application for 45CSR13 NSR Modification Permit has been prepared and submitted to update the existing permit to reflect actual construction and operations, as follows:

- Updated the site's address, location, and directions data;
- Increased the Dehydrator's capacity from 1 MMscfd to 2 MMscfd;
- Reduced Flash Tank off-gas recycle from 85% to 50%;
- Used more conservative Dehydrator Operation parameters (temp and pressure);
- Corrected to show operation of the Dehydration Unit w/o Still Vent Condenser:
- Included Compressor Rod Packing and Engine Crankcase Emissions;
- Included Water/Oil Fugitive Emissions;
- Updated Extended Gas Analysis; and
- Updated emission factors and other emission estimating protocols.

The facility continues to qualify as a Minor Source under Non-Attainment New Source Review (NNSR), Prevention of Significant Deterioration (PSD), and Title V Operating Permits. The facility is also an Area Source for Hazardous Air Pollutants (HAP) under the National Emission Standards for Hazardous Air Pollutants (NESHAP) regulations.

Beverly McKeone WVDEP – Division of Air Quality May 27, 2015 Page 02 of 02

If you have any questions concerning this submittal or need additional information, please contact me at (412) 787-4259 or danell.zawaski@williams.com.

Sincerely,

R. Danell Zawaski, P.E. Environmental Specialist

Enclosures:

Application for NSR Modifications Permit Attachments A through S Check for Application Fee

# APPLICATION FOR 45CSR13 NEW SOURCE REVIEW MODIFICATION PERMIT

For the:

Williams Ohio Valley Midstream LLC

## YOHO COMPRESSOR STATION

Wetzel County, West Virginia

Submitted to:



# WEST VIRGINIA DEPARTMENT OF ENVIRONMENTAL PROTECTION DIVISION OF AIR QUALITY

Submitted by:



## Williams Ohio Valley Midstream LLC

Park Place Corporate Center 2 2000 Commerce Drive Pittsburgh, PA 15275

Prepared by:



**EcoLogic Environmental Consultants, LLC** 

864 Windsor Court Santa Barbara, CA 93111

# APPLICATION FOR 45CSR13 NEW SOURCE REVIEW MODIFICATION PERMIT

Williams Ohio Valley Midstream LLC

#### YOHO COMPRESSOR STATION

Wetzel County, West Virginia

#### TABLE OF CONTENTS

#### **COVER LETTER**

#### **APPLICATION FOR NSR MODIFICATION PERMIT**

SECTION I. General

SECTION II. Additional Attachments and Supporting Documents

• SECTION III. Certification of Information

#### ATTACHMENTS TO APPLICATION

•	ATTACHMENT A	Rusiness	Certificate
•	ALIACHINENIA	Dusilless	Certillicate

- ATTACHMENT B Location (Aerial) and Topographic Maps
- ATTACHMENT C Installation and Start-Up Schedule
- ATTACHMENT D Regulatory Discussion
- ATTACHMENT E Plot Plan
- ATTACHMENT F Detailed Process Flow Diagram (PFD)
- ATTACHMENT G Process Description
- ATTACHMENT H Material Safety Data Sheets (MSDS)

(And Representative Extended Gas Analysis)

- ATTACHMENT I Emission Units Table
- ATTACHMENT J Emission Points Data Summary Sheet(s)
- ATTACHMENT K Fugitive Emissions Data Summary Sheet(s)
- ATTACHMENT L Emissions Unit Data Sheet(s)
- ATTACHMENT M Air Pollution Control Device Sheet(s)
- ATTACHMENT N Supporting Emissions Calculations
- ATTACHMENT O Monitoring/Recordkeeping/Reporting/Testing Plans (NOT APPLICABLE)
- ATTACHMENT P Public Notice (Class I Legal Advertisement)
- ATTACHMENT Q Business Confidential Claims (NOT APPLICABLE)
- ATTACHMENT R Authority Forms (NOT APPLICABLE)
- ATTACHMENT S Title V Permit Revision Information (NOT APPLICABLE)

#### **APPLICATION FEE**

Williams Ohio Valley Midstream LLC

# APPLICATION FOR 45CSR13 NEW SOURCE REVIEW MODIFICATION PERMIT

• SECTION I. General

SECTION II. Additional Attachments and Supporting Documents

• SECTION III. Certification of Information

#### WEST VIRGINIA DEPARTMENT OF **ENVIRONMENTAL PROTECTION**

## **DIVISION OF AIR QUALITY**

# APPLICATION FOR NSR PERMIT AND

601 57" Street, SE Charleston, WV 25304 (304) 926-0475  www.dep.wv.gov/dag	TITLE V PERMIT REVISION (OPTIONAL)
PLEASE CHECK ALL THAT APPLY TO NSR (45CSR13) (IF KNOWN):  CONSTRUCTION MODIFICATION RELOCATION  CLASS I ADMINISTRATIVE UPDATE TEMPORARY  CLASS II ADMINISTRATIVE UPDATE AFTER-THE-FACT	PLEASE CHECK TYPE OF 45CSR30 (TITLE V) REVISION (IF ANY):  ADMINISTRATIVE AMENDMENT MINOR MODIFICATION SIGNIFICANT MODIFICATION IF ANY BOX ABOVE IS CHECKED, INCLUDE TITLE V REVISION INFORMATION AS ATTACHMENT S TO THIS APPLICATION
	on Guidance" in order to determine your Title V Revision options operate with the changes requested in this Permit Application.

Sec	tion I. General					
Name of applicant (as registered with the WV Secretary     WILLIAMS OHIO VALLEY MIDSTREAM LLC	y of State's Office):	2. Federal E	Employer ID No. <i>(F</i> . 2 7 – 0 8 5 6 7 0	•		
<ol> <li>Name of facility (if different from above):</li> <li>YOHO COMPRESSOR STATION</li> </ol>		4. The application of the appli	ant is the: ☐ <b>OPERATOR</b>	⊠ вотн		
5A. Applicant's mailing address:  WILLIAMS OHIO VALLEY MIDSTREAM LLC  100 TELETECH DRIVE  MOUNDSVILLE, WV 26041  5B. Facility's present physical address:  WV-20  NEW MARTINSVILLE, WETZEL COUNTY, WV						
6. West Virginia Business Registration. Is the applicant a resident of the State of West Virginia? YES NO  If YES, provide a copy of the Certificate of Incorporation/Organization/Limited Partnership (one page) including any name change amendments or other Business Registration Certificate as Attachment A.  If NO, provide a copy of the Certificate of Authority/Authority of L.L.C./Registration (one page) including any name change amendments or other Business Certificate as Attachment A.						
7. If applicant is a subsidiary corporation, please provide t	the name of parent corpo	ration: THE V	VILLIAMS COMPA	NIES, INC		
<ul> <li>8. Does the applicant own, lease, have an option to buy o</li> <li>If YES, please explain: APPLICANT OWNS THE S</li> <li>If NO, you are not eligible for a permit for this source.</li> </ul>	SITE	of the <i>propose</i>	ed site? 🛚 YES	□NO		
9. Type of plant or facility (stationary source) to be <b>constructed, modified, relocated, administratively updated</b> or <b>temporarily permitted</b> (e.g., coal preparation plant, primary crusher, etc.):  NATURAL GAS PRODUCTION FACILITY  10. North American Industry Classification System (NAICS) code for the facility:  213112 – SUPPORT ACTIVITIES FOR OIL AND GAS OPERATIONS						
11A. DAQ Plant ID No. (for existing facilities only): 103-00060  11B. List all current 45CSR13 and 45CSR30 (Title V) permit numbers associated with this process (for existing facilities only): R13-3063A						
All of the required forms and additional information can be for	ound under the Permitting	Section of DA	Q's website, or requ	uested by phone.		

12A						
-	For <b>Modifications</b> , <b>Administrative Updates</b> or <b>Te</b> <i>present location</i> of the facility from the nearest state		please provide directions to the			
-	For Construction or Relocation permits, please proad. Include a MAP as Attachment B.	provide directions to the proposed new s	ite location from the nearest state			
	FROM NEW MARTINSVILLE, DEPART WV-2/WV TURN LEFT ONTO WV-7 AND PROCEED 3 MILE RIGHT ONTO UNNAMED ROAD AND ARRIVE A	S. TURN RIGHT ONTO WV-20 AND IN				
12.E	3. New site address (if applicable):	12C. Nearest city or town:	12D. County:			
	NA	NEW MARTINSVILLE	WETZEL			
12.E	E. UTM Northing (KM):	12F. UTM Easting (KM):	12G. UTM Zone:			
	4,383.333	514.862	17			
13.	Briefly describe the proposed change(s) at the facili	ty:				
	<ul> <li>Reduced Flash Tank off-gas recycle from 85</li> <li>Increased the Dehydrator's capacity from 1 I</li> <li>Used more conservative Dehydrator Operati</li> <li>Corrected to show no Still Vent Condenser of Included Rod Packing and Crankcase Emiss</li> <li>Included Water/Oil Fugitive Emissions;</li> <li>Updated Extended Gas Analysis; and</li> <li>Updated emission factors and other emission</li> </ul>	MMscfd to 2 MMscfd; ng parameters (temp and pressure); on the Dehydration Unit; ions;				
14A	. Provide the date of anticipated installation or change	ge:	14B. Date of anticipated Start-Up			
-	<ul> <li>If this is an After-The-Fact permit application, provide the date upon which the proposed change did happen: NA</li> <li>if a permit is granted: Immediate</li> </ul>					
140	c. Provide a Schedule of the planned Installation of/ application as Attachment C (if more than one unit		units proposed in this permit			
15.	Provide maximum projected <b>Operating Schedule</b> of Hours Per Day: <b>24</b> Days Per Week: <b>7</b>	f activity/activities outlined in this applica Weeks Per Year: <b>52</b>	ation:			
16.	Is demolition or physical renovation at an existing fac-	cility involved?				
17.	Risk Management Plans. If this facility is subjection changes (for applicability help see www.epa.gov/cep					
18.	<b>Regulatory Discussion.</b> List all Federal and Sta proposed process <i>(if known)</i> . A list of possible application (Title V Permit Revision Information). Discuss application that the process of the proces	olicable requirements is also included i	in Attachment S of this application			
	Section II. Additional atta	achments and supporting d	ocuments.			
19.	Include a check payable to WVDEP – Division of Air 45CSR13).	Quality with the appropriate application	fee (per 45CSR22 and			
20.	Include a Table of Contents as the first page of you	ır application package.				
21.	Provide a <b>Plot Plan</b> , e.g. scaled map(s) and/or sketo source(s) is or is to be located as <b>Attachment E</b> (Re		rty on which the stationary			

Also describe and quantify to the extent possible all changes made to the facility since the last permit review (if applicable).
 All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

22. Provide a Detailed Process Flow Diagram(s) showing each proposed or modified emissions unit, emission point and control

Indicate the location of the nearest occupied structure (e.g. church, school, business, residence).

device as Attachment F.

23. Provide a Process Description as Attachment G.

24.	Provide Material Safety Data Sheets	(MSDS) for all materials proc	cessed, used or produced as Attachment H.
	For chemical processes, provide a MSD	•	d to the air.
25.	Fill out the <b>Emission Units Table</b> and	provide it as <b>Attachment I.</b>	
26.	Fill out the Emission Points Data Sun	nmary Sheet (Table 1 and T	Table 2) and provide it as Attachment J.
27.	Fill out the <b>Fugitive Emissions Data S</b>	Summary Sheet and provide	e it as <b>Attachment K.</b>
28.	Check all applicable Emissions Unit D	Oata Sheets listed below:	
$\boxtimes$	Bulk Liquid Transfer Operations	☐ Haul Road Emissions	☐ Quarry
	Chemical Processes	☐ Hot Mix Asphalt Plant	Solid Materials Sizing, Handling and Storage
	Concrete Batch Plant	☐ Incinerator	Facilities
	Grey Iron and Steel Foundry	☐ Indirect Heat Exchanger	⊠ Storage Tanks
$\boxtimes$	General Emission Unit, specify:		
	NATURAL GAS FIRED COMPRESSO	R ENGINE	
	TEG DEHYDRATION UNIT		
Fill	out and provide the Emissions Unit Da	ta Sheet(s) as Attachment	L.
29.	Check all applicable Air Pollution Con	trol Device Sheets listed be	elow:
	Absorption Systems	☐ Baghouse	☐ Flare
	Adsorption Systems	☐ Condenser	
	Afterburner	☐ Electrostatic Precipi	itator
$\boxtimes$	Other Collectors, specify:		
	NON-SELECTIVE CATALYTIC REDUC	CTION (NSCR)	
Fill	out and provide the Air Pollution Contr	ol Device Sheet(s) as Attac	chment M.
30.	Provide all <b>Supporting Emissions Ca</b> Items 28 through 31.	Iculations as Attachment N	I, or attach the calculations directly to the forms listed in
31.		ompliance with the proposed	ch proposed monitoring, recordkeeping, reporting and emissions limits and operating parameters in this permit
>		not be able to accept all mea	nether or not the applicant chooses to propose such asures proposed by the applicant. If none of these plans clude them in the permit.
32.	circulation in the area where the source	e is or will be located (See 4	a <b>Class I Legal Advertisement</b> in a newspaper of genera 45CSR§13-8.3 through 45CSR§13-8.5 and <b>Example Lega</b> ation as <b>Attachment P</b> immediately upon receipt.
33.	. Business Confidentiality Claims. Do	es this application include co	onfidential information (per 45CSR31)?
		YES 🛛 NO	
>		the criteria under 45CSR§3	submitted as confidential and provide justification for each s1-4.1, and in accordance with the DAQ's " <i>Precautionary al Instructions</i> as <b>Attachment Q</b> .
	Sec	tion III. Certification	of Information
34.	Authority/Delegation of Authority. C Check applicable Authority Form belo		other than the responsible official signs the application.
	Authority of Corporation or Other Busine	ess Entity [	☐ Authority of Partnership
	Authority of Governmental Agency	_	☐ Authority of Limited Partnership
Sub	omit completed and signed <b>Authority Fc</b>	orm as Attachment R.	
AII	of the required forms and additional infor	mation can be found under the	e Permitting Section of DAQ's website, or requested by phone.

35A. Certification of Information. To certify 2.28) or Authorized Representative shall check	this permit application, a Responsible 0 the appropriate box and sign below.	Official (per 45CSR§13-2.22 and 45CSR§30-				
Certification of Truth, Accuracy, and Completeness						
application and any supporting documents appreasonable inquiry I further agree to assume re stationary source described herein in accordan Environmental Protection, Division of Air Qualit and regulations of the West Virginia Division of	the undersigned Responsible Official / Authorized Representative, hereby certify that all information contained in this application and any supporting documents appended hereto, is true, accurate, and complete based on information and belief after easonable inquiry I further agree to assume responsibility for the construction, modification and/or relocation and operation of the stationary source described herein in accordance with this application and any amendments thereto, as well as the Department of Environmental Protection, Division of Air Quality permit issued in accordance with this application, along with all applicable rules and regulations of the West Virginia Division of Air Quality and W.Va. Code § 22-5-1 et seq. (State Air Pollution Control Act). If the business or agency changes its Responsible Official or Authorized Representative, the Director of the Division of Air Quality will be					
Compliance Certification						
Except for requirements identified in the Title V that, based on information and belief formed afficompliance with all applicable requirements.  SIGNATURE (Please)	Application for which compliance is no ter reasonable inquiry, all air contaminates and the second s	t achieved, I, the undersigned hereby certify ant sources identified in this application are in  DATE:				
35B. Printed name of signee:		35C. Title:				
DON WICBURG		VICE PRESIDENT AND GENERAL MANAGER				
35D. E-mail:	36E. Phone:	36F. FAX:				
DON WICBURG@WILLIAMS.COM	(304) 843-3158	(304) 843-3131				
36A. Printed name of contact person (if differen	t from above):	36B. Title:				
BILL THOMPSON		ENVIRONMENTAL SPECIALIST				
36C. E-mail:	36D. Phone:	36E. FAX:				
BILL.THOMPSON@WILLIAMS.COM	(304) 843-3103	(304) 843-3131				
PLEASE CHECK ALL APPLICABLE ATTACHMENT	S INCLUDED WITH THIS PERMIT APPLIC	CATION:				
Attachment A: Business Certificate  ☐ Attachment B: Map(s) ☐ Attachment C: Installation and Start Up Schedule ☐ Attachment D: Regulatory Discussion ☐ Attachment N: Supporting Emissions Calculations ☐ Attachment F: Detailed Process Flow Diagram(s) ☐ Attachment G: Process Description ☐ Attachment H: Material Safety Data Sheets (MSDS) ☐ Attachment H: Emission Units Table ☐ Attachment J: Emission Points Data Summary Sheet ☐ Attachment S: Title V Permit Revision Information ☐ Application Fee						
	copies of the complete permit applicatio d on the first page of this application. Pl					
FOR AGENCY USE ONLY - IF THIS IS A TITLE V	SOURCE:					
☐ Forward 1 copy of the application to the Title ☐ For Title V Administrative Amendments: ☐ NSR permit writer should notify Title V	V Permitting Group and:					
☐ NSR permit writer should notify fille V ☐ For Title V Minor Modifications: ☐ Title V permit writer should send appro ☐ NSR permit writer should notify Title V ☐ For Title V Significant Modifications processed ☐ NSR permit writer should notify a Title ☐ Public notice should reference both 45 ☐ EPA has 45 day review period of a drain	opriate notification to EPA and affected s permit writer of draft permit. d in parallel with NSR Permit revision: V permit writer of draft permit, iCSR13 and Title V permits,	tates within 5 days of receipt,				
		ction of DAQ's website, or requested by phone.				

#### **ATTACHMENT A**

#### **Business Certificate**

"6. **West Virginia Business Registration**. Provide a copy of the Certificate of Authority/Authority of L.L.C./Registration (one page) including any name change amendments or other Business Certificate as Attachment A."

• Certificate of Amendment to the Certificate of Authority

From: CAIMAN EASTERN MIDSTREAM, LLC

To: WILLIAMS OHIO VALLEY MIDSTREAM LLC

Date: May 15, 2012

Certificate of Authority of a Foreign Limited Liability Company

To: CAIMAN EASTERN MIDSTREAM, LLC

Date: September 11, 2009



# I, Natalie E. Tennant, Secretary of State of the State of West Virginia, hereby certify that

the attached true and exact copy of the Articles of Amendment to the Articles of Organization of

#### CAIMAN EASTERN MIDSTREAM, LLC

are filed in my office, signed and verified, as required by the provisions of West Virginia Code §31B-2-204 and conform to law. Therefore, I issue this

# CERTIFICATE OF AMENDMENT TO THE CERTIFICATE OF AUTHORITY

changing the name of the limited liability company to

WILLIAMS OHIO VALLEY MIDSTREAM LLC



Given under my hand and the Great Seal of the State of West Virginia on this day of May 15, 2012

Secretary of State



# I, Natalie E. Tennant, Secretary of State of the State of West Virginia, hereby certify that

#### CAIMAN EASTERN MIDSTREAM, LLC

Control Number: 99GIS

a limited liability company, organized under the laws of the State of Texas has filed its "Application for Certificate of Authority" in my office according to the provisions of West Virginia Code §31B-10-1002. I hereby declare the organization to be registered as a foreign limited liability company from its effective date of September 11, 2009, until a certificate of cancellation is filed with our office.

Therefore, I hereby issue this

# CERTIFICATE OF AUTHORITY OF A FOREIGN LIMITED LIABILITY COMPANY

to the limited liability company authorizing it to transact business in West Virginia



Given under my hand and the Great Seal of the State of West Virginia on this day of September 11, 2009

Clemant

Secretary of State

#### **ATTACHMENT B**

# **Location (Aerial) and Topographic Maps**

"12A. For **Modifications, Administrative Updates** or **Temporary** permits at an existing facility, please provide directions to the present location of the facility from the nearest state road. Include a MAP as Attachment B."

#### Address:

~3.0 Miles South-Southeast of New Martinsville

~0.1 Mile Northwest of Slim Chance Road New Martinsville, Wetzel County, WV 26033

## • Latitude and Longitude:

39°35'59.00"North x -80°49'41.50"West (39.6000°N and -80.8281°W

#### UTM:

514.75 km Easting x 4,383.35 km Northing x Zone 17S

#### Elevation:

~865'

#### Directions:

From Virginia St in New Martinsville:

a.	Head south on 3rd St (WV-2/WV-7)	~0.5 Mi;
b.	Turn left onto Mountaineer Hwy (WV-7)	~2.8 Mi;
C.	Turn right onto Main St/Shortline Hwy (WV-20)	~1.6 Mi;
d.	Turn right onto Slim Chance Rd	~0.2 Mi;
e.	Slight right onto gravel access road	~0.1 Mi;

f. Site is on the left

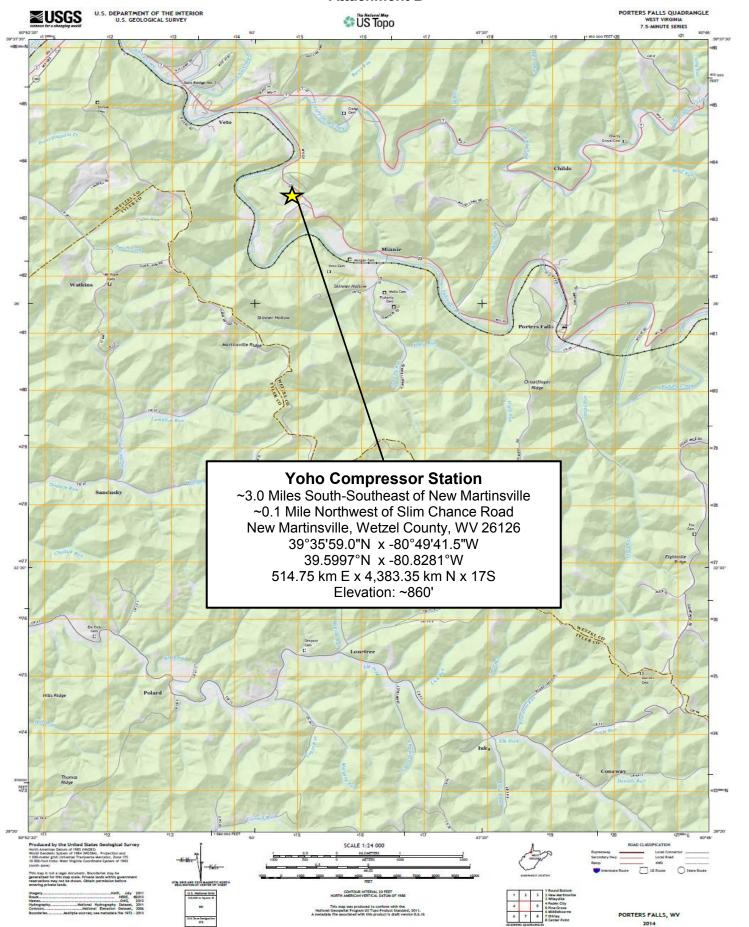
#### USGS:

7.5" Topographic – Porter Falls, WV (2014)

#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### **Attachment B**



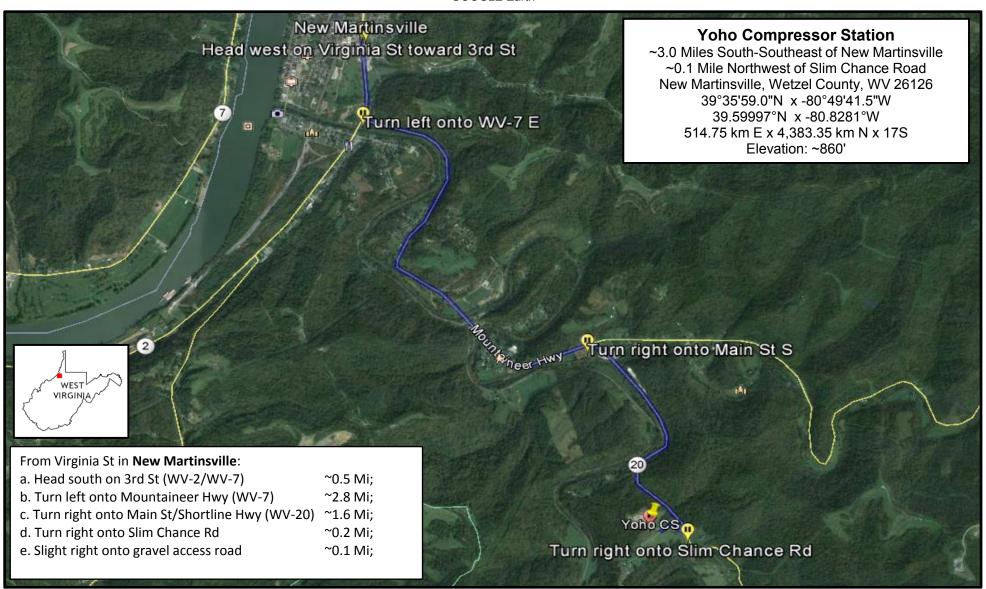
#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### **Attachment B**

## **Location (Aerial) Map**

**GOOGLE Earth** 



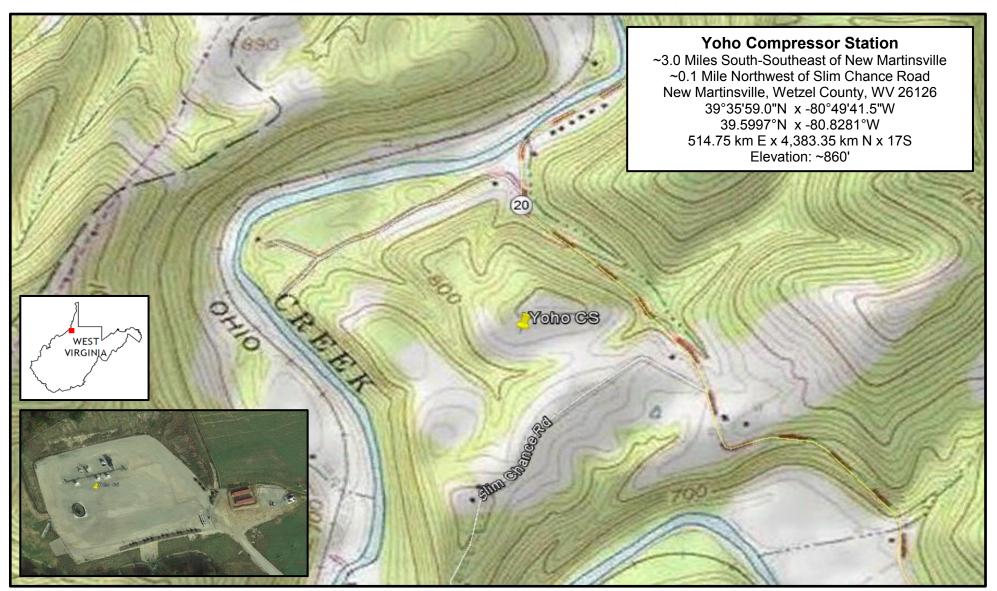
#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### Attachment E

#### **Topographic Map**

USGS TOPOGRAPHIC - 7.5-MINUTE SERIES, PORTERS FALLS QUADRANGLE, WEST VIRGINIA



#### **ATTACHMENT C**

## Installation and Start-Up Schedule

"14C. Provide a **Schedule** of the planned **Installation** of/**Change** to and **Start-Up** of each of the units proposed in this permit application as Attachment C."

The OVM Yoho Compressor Station is an existing operation. This application is prepared and submitted to update the existing permit to reflect actual construction and operations, as follows:

- Reduced Flash Tank off-gas recycle from 85% to 50%;
- Increased the Dehydrator's capacity from 1 MMscfd to 2 MMscfd;
- Used more conservative Dehydrator Unit operation parameters (temp and pressure);
- Corrected to show no Still Vent Condenser on the Dehydration Unit;
- Included Water/Oil Fugitive Emissions;
- Included Compressor Rod Packing and Engine Crankcase Emissions;
- Updated Extended Gas Analysis; and
- Updated emission factors and other emission estimating protocols

#### **ATTACHMENT D**

## **Regulatory Discussion**

"18. **Regulatory Discussion**. List all Federal and State air pollution control regulations that you believe are applicable to the proposed process (if known). Discuss applicability and proposed demonstration(s) of compliance (if known). Provide this information as Attachment D."

#### • Regulatory Discussion

- A. Applicability of New Source Review (NSR) Regulations
- B. Applicability of Federal Regulations
- C. Applicability of Source Aggregation
- D. Applicability of State Regulations

#### YOHO COMPRESSOR STATION

Application for 45CSR13 Modification Permit

# Attachment D REGULATORY DISCUSSION

#### A. Applicability of New Source Review (NSR) Regulations

The following New Source Review (NSR) regulations are potentially applicable to natural gas production facilities. Applicability to the subject facility has been determined as follows:

#### 1. Prevention of Significant Deterioration (PSD)

[Not Applicable]

This rule <u>does not apply</u>. The facility is a "PSD Minor Source" for each regulated pollutant, as follows:

NOx: PSD Natural Minor Source with Pre-Controlled PTE < 250 tpy</li>
 CO: PSD Natural Minor Source with Pre-Controlled PTE < 250 tpy</li>
 VOC: PSD Natural Minor Source with Pre-Controlled PTE < 250 tpy</li>
 SO2: PSD Natural Minor Source with Pre-Controlled PTE < 250 tpy</li>
 PM10/2.5: PSD Natural Minor Source with Pre-Controlled PTE < 250 tpy</li>

(Note: Fugitive emissions of criteria pollutants from natural gas compressor stations are **ex**cluded in the PSD and TVOP Major Source Determinations.)

(Note: On June 23, 2014, the U.S. Supreme Court said that EPA may not treat greenhouse gases (e.g., CO2e) as an air pollutant for purposes of determining whether a source is a major source required to obtain a PSD permit or TVOP.)

#### 2. Non-Attainment New Source Review (NNSR)

[Not Applicable]

This rule <u>does not apply</u>. The facility is in a county that is classified as Non-Attainment for Fine Particulates and as Attainment for all other criteria pollutants. With the requested Federally Enforceable Limits (FEL) the facility qualifies as an "NNSR Minor Source" as follows:

PM10/2.5: NNSR Natural Minor Source with Pre-Controlled PTE < 100 tpy</li>
 NOx: NNSR Natural Minor Source with Pre-Controlled PTE < 100 tpy</li>
 SO2: NNSR Natural Minor Source with Pre-Controlled PTE < 100 tpy</li>

#### 3. Major Source of Hazardous Air Pollutants (HAPs)

[Not Applicable]

This rule does not apply. The facility qualifies as a "HAP Area Source" as follows:

- Each HAP: HAP Area Source with Controlled Individual HAP PTE < 10 tpy</li>
- Total HAPs: HAP Area Source with Controlled Total of All HAPs PTE < 25 tpy</li>

#### 4. Title V Operating Permit (TVOP)

[Not Applicable]

This rule does not apply. The facility qualifies as a "Title V Minor Source" as follows:

- NOx: Title V Natural Minor Source with Pre-Controlled PTE < 100 tpy</li>
- CO: Title V Natural Minor Source with Pre-Controlled PTE < 100 tpy
- VOC: Title V Synthetic Minor Source with Controlled PTE < 100 tpy
- SO2: Title V Natural Minor Source with Pre-Controlled PTE < 100 tpy
- PM10/2.5: Title V Natural Minor Source with Pre-Controlled PTE < 100 tpy</li>
- Each HAP: Title V Area Source with Controlled PTE < 10 tpy</li>
- Total HAPs: Title V Area Source with Controlled PTE < 25 tpy</li>

(Note: Fugitive emissions of criteria pollutants from natural gas compressor stations are **ex**cluded in the PSD and TVOP Major Source Determinations.)

(Note: On June 23, 2014, the U.S. Supreme Court said that EPA may not treat greenhouse gases (e.g., CO2e) as an air pollutant for purposes of determining whether a source is a major source required to obtain a PSD permit or TVOP.)

#### B. Applicability of Federal Regulations

The following federal regulations are potentially applicable to natural gas production facilities. Applicability to the facility has been determined as follows:

#### 1. NSPS A, General Provisions

40CFR§60.1-§60.19

[Applicable]

This rule <u>does apply</u> to all sources subject to an NSPS (unless a specific provision is excluded within the source NSPS), including the 203 bhp CAT G3306TA (4SRB) compressor engine (CE-01). Requirements include notification, monitoring, and recordkeeping.

#### 2. NSPS A, Control Devices - Flares

40CFR§60.18(b)

[Not Applicable]

This rule does not apply because there is no flare at the facility.

#### 3. NSPS Dc, Steam Generating Units

40CFR§60.40c-§60.48c

[Not Applicable]

This rule <u>does not apply</u> because there is no steam generating unit (including line heaters) at the facility with a maximum design heat input capacity  $\geq$  10 MMBtu/hr and  $\leq$  100 MMBtu/hr ( $\S$ 60.40c(a)).

#### 4. NSPS Kb, Volatile Organic Liquid Storage Vessels

40CFR§60.110b-§60.117b

[Not Applicable]

This rule <u>does not apply</u> because there is no tank used to store volatile organic liquids (VOL) with a design capacity  $\geq$  75 m3 (19,815 gal, 471.79 bbl) (§60.110b(a)).

#### 5. NSPS GG, Stationary Gas Turbines

40CFR§60.330-§60.335

[Not Applicable]

This rule <u>does not apply</u> because there is no stationary gas turbine at the facility (§60.330).

#### 6. NSPS KKK, Leaks from Natural Gas Processing Plants

40CFR§60.630-§60.636

[Not Applicable]

This rule <u>does not apply</u> because the facility is not a natural gas processing plant (§60.630(b)).

#### 7. NSPS LLL, Onshore Natural Gas Processing: SO2 Emissions

40CFR§60.640-§60.648

[Not Applicable]

This rule <u>does not apply</u> because there is no gas sweetening operation at the facility (§60.640(a)).

#### 8. NSPS IIII, Compression Ignition Reciprocating Internal Combustion Engines

40CFR§60.4200-§60.4219

[Not Applicable]

This rule <u>does not apply</u> because there is no stationary compression ignition engine at the facility (§60.4200(a)).

#### 9. NSPS JJJJ, Stationary Spark Ignition (SI) Internal Combustion Engines (ICE)

40CFR§60.4230-§60.4248

[Applicable]

This rule <u>does apply</u> to the 203 bhp CAT G3306TA (4SRB) compressor engine (CE-01) because its maximum engine power is less than 500 HP and manufactured on or after 07/01/08 (§60.4230(a)(4)(iii)).

Requirements include NOx, CO and VOC emission limits (§60.4233(e-f)); operating limits (§60.4243); performance testing (§60.4244); and notification and recordkeeping (§60.4245).

#### 10. NSPS KKKK, Stationary Combustion Turbines

40CFR§60.4300-§60.4420

[Not Applicable]

This rule <u>does not apply</u> because there is no stationary combustion turbine at the facility (§60.4300).

#### 11. NSPS OOOO, Crude Oil and Natural Gas Production

40CFR§60.5360-§60.5430

[Not Applicable]

This rule <u>does not apply</u> to the reciprocating compressor (associated w/ engine CE-01) because it was constructed prior to 08/23/11 (§60.5360 and §60.5365(c)).

This rule <u>does not apply</u> to the storage vessel (TK-01) because it has a VOC PTE < 6 tpy (§60.5395). However, records of VOC emissions must be retained to demonstrate continuing exemption status (§60.5420(b)(6)(ii) and (§60.5420 (c)(5)(ii)).

This rule <u>does not apply</u> to the pneumatic controllers because they are located between the wellhead and point of custody transfer, are not located at a natural gas processing plant, and their bleed rate is  $\leq 6$  scfh ( $\S 60.5365(d)(i)$ ).

#### 12. NESHAP, Designated Source Standards

40CFR§61.01-§61.359

[Not Applicable]

This rule <u>does not apply</u> because the facility is not a designated facility (or source) subject to any requirements of the National Emissions Standards for Hazardous Air Pollutants (NESHAP).

#### 13. NESHAP A, General Provisions (aka MACT)

40CFR§63.1-§63.16

[Applicable]

This rule <u>does apply</u> to the 203 bhp CAT G3306TA (4SRB) compressor engine (CE-01) and to the 2.0 MMscfd TEG Dehydrator (RSV-1) because they are subject to NESHAP ZZZZ and NESHAP HH, respectively. Requirements include notification, monitoring, and recordkeeping.

#### 14. NESHAP HH, Oil and Natural Gas Production Facilities

40CFR§63.760-§63.779

[Applicable]

This rule <u>does apply</u> to the 2.0 MMscfd TEG Dehydrator (RSV-1). However, because the dehydrator has an actual annual average flowrate of natural gas < 3 MMscfd it is exempt from all requirements except to maintain records of actual annual average flowrate of natural gas to demonstrate continuing exemption status (§63.764(e)(1)).

This rule <u>does not apply</u> to storage vessels (tanks), compressors, or ancillary equipment because the facility is an area source of HAP emissions (§63.760(b)(2)). In no case does this rule apply to engines or turbines.

#### 15. NESHAP HHH, Natural Gas Transmission and Storage Facilities

40CFR§63.1270-§63.1289

[Not Applicable]

This rule <u>does not apply</u> because the facility is not a natural gas transmission or storage facility transporting or storing natural gas prior to local distribution (§63.1270(a)).

#### 16. NESHAP YYYY, Stationary Combustion Turbines

40CFR§63.6080-§63.6175

[Not Applicable]

This rule <u>does not apply</u> because there is no stationary gas turbine at the facility (§63.6080).

# 17. NESHAP ZZZZ, Stationary Reciprocating Internal Combustion Engines (RICE)

40CFR§63.6580-§63.6675

[Applicable]

This rule <u>does apply</u> to the compressor engine; however, because it is "new"; i.e., commenced construction or reconstruction on or after 06/12/06 (§63.6590(a)(2)(iii)), the only requirement is compliance with 40CFR§60.4230-§60.4248 (NSPS JJJJ) for Spark Ignition Internal Combustion Engines

# 18. NESHAP DDDDD, Industrial, Commercial, and Institutional Boilers and Process Heaters – Major Sources

40CFR§63.7480 - §63.7575

[Not Applicable]

This rule does not apply because the facility is not a major source of HAP (§63.7485).

# 19. NESHAP JJJJJJ, Industrial, Commercial, and Institutional Boilers – Area Sources 40CFR§63.11193 – §63.11237 [Not Applicable]

This rule <u>does not apply</u> because gas-fired boilers are not subject to the requirements of this subpart (§63.11195(e)). Specifically, "boiler" is defined as an enclosed device using controlled flame combustion in which water is heated to recover thermal energy in the form of steam and/or hot water.

#### 20. Chemical Accident Prevention Provisions

40CFR§68.1-§68.220

[Not Applicable]

This rule <u>does not apply</u> because the facility does not store more than a threshold quantity of a regulated substance in a process (§68.115).

#### 21. Compliance Assurance Monitoring (CAM)

40CFR§64.1-§64.10

[Not Applicable]

This rule <u>does not apply</u>. Although there are pollutant specific emission units subject to an emissions limitation and a control device is used to achieve compliance, the potential pre-control emissions do not exceed 100 tpy.

#### 22. Mandatory Greenhouse Gases (GHG) Reporting

40CFR§98.1-§98.9

[Not Applicable]

This rule <u>does not apply</u>. The facility is not subject to a listed source category and the aggregate maximum heat input capacity is < 30 MMBtu/hr from all stationary fuel combustion sources combined (§98.2(a)).

#### C. Applicability of Source Aggregation

For New Source Review (NSR) and Title V permitting, the three-part regulatory criteria to determine whether emissions from two or more facilities should be aggregated and treated as a single source is whether the activities:

- i) Belong to the same industrial grouping; and
- ii) Are located on one or more contiguous or adjacent properties; and
- iii) Are under control of the same person (or persons under common control).

#### i) Same Industrial Grouping

The subject facility shares the same two-digit major SIC code of 13 as the upstream gas production wells and other Williams' facilities.

#### ii) Contiguous or Adjacent

The determination of whether two or more facilities are "contiguous" or "adjacent" is made on a case-by-case basis. This determination is proximity based, and it is important to focus on this

criterion and whether two contiguous or adjacent facilities, considered as a single source, meet the common sense notion of a plant. The functional interrelationship of the two or more facilities is not a relevant inquiry in determining whether the facilities are "contiguous" or "adjacent."

Neither West Virginia nor federal regulations define the terms "contiguous" or "adjacent." It is clear, however, that the determination of whether two or more facilities are "contiguous" or "adjacent" is based on the plain meaning of the terms "adjacent" and "contiguous", which consider the physical distance between the facilities. The term contiguous is defined in the dictionary as being in actual contact; touching along a boundary or at a point. The term adjacent" is defined in the dictionary as not distant, nearby, having a common endpoint or border.

The closest Williams-owned facility to the Yoho Compressor Station is the Nice Compression Station, which is located 4.8 miles away. The Nice Compressor Station does not meet the common sense definition of being "contiguous" with or "adjacent" to the Yoho Compressor Station.

The Yoho Compressor Station compresses and dehydrates gas produced from an upstream production well located in northern West Virginia. The subject facility is located on a parcel that is directly adjacent to a pre-existing upstream production wellpad operated by Chevron and is located less than ½ mile from that wellpad.

The location of the subject facility was chosen because of suitable characteristics for construction and operation, such as the availability of a reasonably flat grade and accessibility for large trucks and equipment. Williams' business model is to construct scalable capacity that contemplates additional production from multiple operators and the initial configuration is merely a foundation for additional opportunities in the area. The subject facility does not need to be located in the immediate vicinity of the upstream wells in order to operate properly. Had suitable land been available elsewhere, the subject facility could have been located farther from the upstream wells and could theoretically be moved farther from the wells without affecting operations. Therefore, despite the fact that the subject facility is located in close proximity to one or many upstream production sources, aggregation of the subject facility with upstream wells does not meet the common sense notion of a plant.

#### iii) Common Control

Williams OVM operates under its parent company The Williams Companies, Inc. (Williams) and is the sole operator of the subject facility. The closest Williams-operated facility to the subject facility is the Nice Compressor Station, located approximately 4.8 miles away. This facility is the closest to Yoho to have common ownership but it is not "contiguous" with or "adjacent" to the Yoho facility.

The production wells, including the Chevron wellpad, that send natural gas to the subject facility are owned and operated by other companies, which are unaffiliated with Williams. Williams has no ownership stake in the Chevron wellpad or in any production well or company in West Virginia that may send natural gas to the subject facility.

Furthermore, neither Williams OVM, nor Williams, exercise operational control over any equipment owned or operated by any natural gas producer upstream of the subject facility. All employees at the subject facility are under the exclusive direction of Williams and are not under

the control of any other entity. Similarly, Williams has no authority over employees of the production wells. These companies operate wholly independent of one another. No employees are expected to shuttle back and forth between the subject facility and any production well.

At this time, contracts are in place for the subject facility to process natural gas produced from multiple upstream production wells located throughout the region. As future commercial opportunities are identified, the subject facility will potentially receive gas from other producers. Williams will not have ownership or control of any future wellhead facilities. The producers are, and will be responsible for, any decisions to produce or shut-in wellhead facilities and have no control over the equipment installed, owned, and operated by Williams. Similarly, Williams cannot control the installation or operation of any equipment located at a well site that may be considered an air contamination source.

For the reason above, it is clear that Williams does not have common control of any production wells including the Chevron well.

#### **Summary**

The subject facility and the upstream production wells should not be aggregated and treated as a single source of emissions because the subject facility is not under common control with any of the upstream wells. Additionally, the subject facility and the upstream production wells, considered together, do not meet the common sense notion of a plant because the subject facility is expected to service multiple production wells and because the location of the facility was selected for reasons unrelated to the location of the production wells. Accordingly, the subject facility should not be aggregated with the upstream wells in determining major source or PSD status.

#### D. Applicability of State Regulations

The following State regulations are potentially applicable to natural gas production facilities. Applicability to the facility has been determined as follows:

# Particulate Air Pollution from Combustion of Fuel in Indirect Heat Exchangers 45CSR2 [Applicable]

This <u>rule does apply</u>, however, because the dehydrator reboiler (BLR-01) has a maximum design heat input (MDHI) rating < 10 MMBtu/hr, the only requirement is to limit visible emissions to < 10% opacity during normal operations (§45-02-3.1). The reboiler combusts only natural gas which inherently conforms to the visible emission standards.

# 2. Prevent and Control the Discharge of Air Pollutants into the Open Air which Causes or Contributes to an Objectionable Odor or Odors 45CSR4 [Applicable]

This rule <u>does apply</u> and states that an objectionable odor is an odor that is deemed objectionable when in the opinion of a duly authorized representative of the Air Pollution Control Commission (Division of Air Quality), based upon their investigations and complaints, such odor is objectionable. No odors have been deemed objectionable.

#### 3. Control of Air Pollution from Combustion of Refuse

45CSR6 [Not Applicable]

This rule <u>does not apply</u> because there is no refuse combustion performed at the facility.

4. Prevent and Control Air Pollution from the Emission of Sulfur Oxides

45CSR10 [Not Applicable]

This rule <u>does not apply</u> because each "fuel burning unit" at the facility has a Maximum Design Heat Input (MDHI) rating < 10 MMBtu/hr.

5. Permits for Construction, Modification, Relocation and Operation of Stationary Sources of Air Pollutants, Notification Requirements, Administrative Updates, Temporary Permits, General Permits, and Procedures for Evaluation

[Applicable]

This rule <u>does apply</u>. Williams OVM has received a 45CSR13 Permit for the subject facility and has published the required Class I legal advertisement notifying the public of this application to modify the existing permit; and paid the appropriate application fee.

6. Permits for Construction and Major Modification of Major Stationary Sources of Air Pollutants

45CSR14 [Not Applicable]

The rule <u>does not apply</u> because the facility is neither a new major source of pollutants nor is the proposed modification a modification to an existing major source.

7. Standards of Performance for New Stationary Sources Pursuant to 40 CFR Part 60 45CSR16 [Applicable]

This rule <u>does apply</u> by reference of §40CFR60, Subpart JJJJ. Williams OVM is subject to the recordkeeping, monitoring, and testing required of this Subpart.

8. Permits for Construction and Major Modification of Major Stationary Sources of Air Pollution which Cause or Contribute to Nonattainment

45CSR19 [Not Applicable]

This rule <u>does not apply</u> because the facility is a minor (or "deferred") source of all regulated pollutants. Furthermore, this rule <u>does not apply</u> because the facility location is designated as either "Maintenance" or "Attainment/Unclassified" for all criteria pollutants.

9. Regulation of Volatile Organic Compounds (VOC)

45CSR21 [Not Applicable]

This rule <u>does not apply</u> because the facility is not located in Putnam County, Kanawha County, Cabell County, Wayne County, or Wood County

10. Air Quality Management Fees Program

45CSR22 [Applicable]

This rule <u>does apply</u>. It establishes a program to collect fees for certificates to operate and for permits to construct, modify or relocate sources of air pollution.

#### 11. Prevent and Control Emissions of Toxic Air Pollutants

45CSR27 [Not Applicable]

This rule <u>does not apply</u> because equipment used in the production and distribution of petroleum products is exempt, provided that the product contains no more than 5% benzene by weight (§45-22-2.4).

#### 12. Air Pollution Emissions Banking and Trading

45CSR28 [Not Applicable]

This rule <u>does not apply</u>. The facility does not choose to participate in the voluntarily statewide air pollutant emissions trading program.

#### 13. Emission Statements for VOC and NOX

45CSR29

[Not Applicable]

This rule <u>does not apply</u> because facility is not located in Putnam, Kanawha, Cabell, Wayne, Wood, or Greenbrier Counties (§45-29-1).

#### 14. Requirements for Title V Operating Permits (TVOP)

45CSR30 [Not Applicable]

This rule <u>does not apply</u> because the facility is a non-major (or "deferred") source of all regulated pollutants.

Pursuant to the authority granted in West Virginia 45CSR§30-3.2 and 45CSR§30A-3.1, the DAQ is extending the deferral, which was set to expire December 15, 2000, of non-major sources subject to West Virginia 45CSR30 (Title V Program) from the obligation to submit an operating permit application.

#### 15. Emission Standards for Hazardous Air Pollutants (HAP)

45CSR34 [Applicable]

This rule <u>does apply</u> by reference of §40CFR63, Subparts HH and ZZZZ. Williams OVM is subject to the recordkeeping, monitoring, and testing required of these Subparts.

# ATTACHMENT E Plot Plans

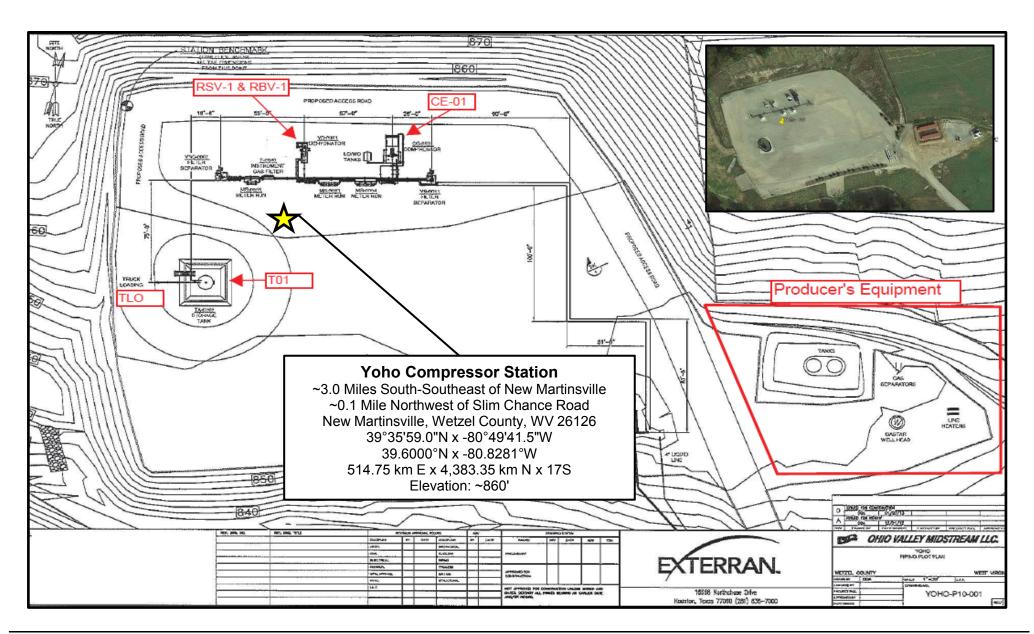
"21. Provide a <b>Plot Plan</b> , e.g. scaled map(s) and/or sketch(es) showing the location of the property on which the stationary source(s) is or is to be located as Attachment E."
Plot Plan – Yoho Compressor Station

#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### Attachment E

#### **Plot Plan**



# **ATTACHMENT F**

# **Detailed Process Flow Diagram**

	Provide a <b>Detailed Process Flow Diagram(s)</b> showing each proposed or modified ssions unit, emission point and control device as Attachment F."
•	Process Flow Diagram (PFD) – Yoho Compressor Station

#### YOHO COMPRESSOR STATION

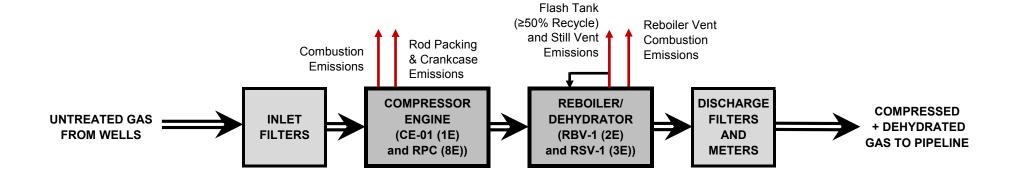
Application for 45CSR13 NSR Modification Permit

#### Attachment F

## **Process Flow Diagram (PFD)**



Storage Tank



<u>Unit No.</u>	Company ID - Description	Working , Standing, and Flash Losses	Truck Loading Emissions
CE-01 (1E)	Compressor Engine CE-01 - 203 bhp CAT G3306TA	Tank 01	<u> </u>
RBV-1 (2E)	TEG Dehydrator - Reboiler Vent		
RSV-1 (3E)	TEG Dehydrator - Flash Tank and Still Vent		
T01 (4E)	Produced Water Storage Tank - 210 bbl	!	
TLO (5E)	Produced Water - Truck Load-Out	- ;	
SSM (6E)	Startup/Shutdown/Maintenance (Includes Blowdown)		
FUG (7E)	Piping and Equipment Fugitives	PRODUCED WATER	PRODUCED WATER
RPC (8E)	Rod Packing and Crankcase Emissions	STORAGE TANK	TRUCK LOAD-OUT
		(T01 (4E))	(TLO (5E)

#### **ATTACHMENT G**

## **Process Description**

"23. Provide a Process Description as Attachment G. Also describe and quantify to the extent possible all changes made to the facility since the last permit review (if applicable). "

#### • Process Description

- A. Project Overview
- B. Compressor Engine
- C. Triethylene Glycol (TEG) Dehydrator
- D. Triethylene Glycol (TEG) Reboiler
- E. Storage Tanks
- F. Truck Load-Out
- G. Startup/Shutdown/Maintenance
- H. Compressor Rod Packing and Crankcase Emission
- I. Piping and Equipment Fugitive Emissions

# ATTACHMENT G Process Description

## Williams Ohio Valley Midstream LLC YOHO COMPRESSOR STATION Application for 45CSR13 NSR Permit

#### A. Project Overview

Williams Ohio Valley Midstream LLC is proposing to construct and operate the Yoho Compressor Station to be located along off WV-20 in Wetzel County (See Appendix B – Site Location Maps). The facility will receive natural gas from local production wells then compress and dehydrate the gas for delivery to a gathering pipeline.

This application has been prepared and submitted to provide for the following equipment and operations at the facility:

- One 203 bhp Caterpillar G3306TA Compressor Engine w/ NSCR (CE-01)
- One 2.0 MMscfd TEG dehydrator w/ 0.14 MMBtu/hr Reboiler (RBV-1 and RSV-1)
- One 210 bbl produced water storage tank (T01)
- Truck Load-out (TLO) emissions
- Startup/Shutdown/Maintenance (SSM) emissions.
- Fugitive emissions from process piping and equipment (FUG)
- Compressor Rad Packing and Engine Crankcase Leaks (RPC)
- Other ancillary equipment and operations with de minimis emissions

#### **B.** Compressor Engine

One (1) natural gas-fueled compressor engine will be utilized at the facility. The engine is equipped with state-of-the art emission control technology applicable to the operation. The rich-burn engine (CE-01) utilizes non-selective catalytic reduction (NSCR) to control pollutant emissions.

#### C. Dehydrator

One (1) Triethylene Glycol (TEG) Dehydrator is utilized at the facility. The dehydrator is comprised of a Contactor/Absorber Tower (no vented emissions), a Flash Tank, and a Regenerator/Still Vent.

The TEG Dehydrator is used to remove water vapor from the inlet wet gas stream to meet pipeline specifications. In the dehydration process, the wet inlet gas stream flows through a contactor tower where the gas is contacted with lean glycol. The lean glycol absorbs the water in the gas stream and becomes rich glycol laden with water and trace amounts of hydrocarbons.

The rich glycol is then routed to a flash tank where the glycol pressure is reduced to liberate the lighter end hydrocarbons (especially methane). Whenever practical, the lighter end hydrocarbons are routed from the flash tank to the Reboiler for use as fuel; otherwise these off-gases are vented to the atmosphere.

#### D. Reboiler

A Reboiler is utilized to supply heat for the Triethylene Glycol (TEG) Regenerator/Still Vent.

#### E. Produced Water Tank

There are tanks at the facility used to store various materials, including produced water, lube oil, fresh and spent TEG, etc. All of these tanks, except for the produced water storage tanks, generate de-minimis (insignificant) emissions.

The produced water tank receives liquids from the dehydrator and inlet separator. Liquids removed through the dehydration process are cooled, condensed and sent to the 210 barrel atmospheric storage tank (T01). The inlet separator removes produced fluids (primarily water) and these liquids are also sent to the 210 bbl atmospheric storage tank.

#### F. Truck Load-Out

Loading of produced water into tanker trucks will produce small quantities of VOC emissions from the displacement of vapors inside the tanker trucks (TLO).

#### G. Startup, Shutdown and Maintenance

During routine operation of the facility the compressor engine will undergo periods of startup and shutdown. Often when the engine is shutdown, the natural gas contained within the compressor and associated piping is vented to atmosphere. Additionally, there will be other infrequent and (often) de-minimis emissions from various maintenance activities at the facility that are not necessarily associated with compressor blowdowns (e.g., pig launching). These emissions associated with startup, shutdown and maintenance are assigned a Unit ID of SSM.

#### H. Compressor Rod Packing and Crankcase Emissions

The compressor and engine operation results in emissions from the wear of mechanical joints, seals, and rotating surfaces over time.

#### I. Piping and Equipment Fugitive Emissions

Piping and process equipment generate from leaks from different component types (connectors, valves, pumps, etc.) in gas-vapor service and water/oil service.

## **ATTACHMENT H**

# **Material Safety Data Sheets (MSDS)**

# (And Representative Gas Analysis)

"24. Provide **Material Safety Data Sheets (MSDS)** for all materials processed, used or produced as Attachment H. For chemical processes, provide a MSDS for each compound emitted to the air."

#### NATURAL GAS

- Natural Gas Composition
- Extended Gas Analysis

#### • MATERIAL SAFETY DATA SHEETS (MSDS):

- Natural Gas
- Triethylene Glycol (TEG)
- Produced Water/Condensate

#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### **Attachment H**

#### **Gas Analysis Summary**

Representative Gas Analysis - Sampled 06/25/14

Component	Formula	Molecular Weight (MW)	Mole % (M%)	Mole Fraction (M%/Sum-M%)	Weighted Sum (MW*MF)	Weight % (WS/Sum-WS)	lb/MMscf (WS/UGC#)
Oxygen	O2	32.00	0.0011	0.00001	0.0004	0.002	0.93
Nitrogen	N2	28.01	0.4580	0.00458	0.1283	0.606	338.10
Carbon Dioxide	CO2	44.01	0.1537	0.00154	0.0676	0.319	178.25
Carbon Monoxide	CO	28.01					
Hydrogen Sulfide	H2S	34.08					
Methane*	CH4	16.04	78.0288	0.78029	12.5177	59.114	32,986.38
Ethane*	C2H6	30.07	13.0780	0.13078	3.9324	18.570	10,362.62
Propane**	C3H8	44.10	5.1090	0.05109	2.2528	10.639	5,936.63
i-Butane**	C4H10	58.12	0.6003	0.00600	0.3489	1.648	919.43
n-Butane**	C4H10	58.12	1.4055	0.01406	0.8169	3.858	2,152.69
i-Pentane**	C5H12	72.15	0.3321	0.00332	0.2396	1.132	631.40
n-Pentane**	C5H12	72.15	0.3827	0.00383	0.2761	1.304	727.61
Cyclohexane**	C6H12	84.16	0.0130	0.00013	0.0109	0.052	28.83
i-Hexanes**	C6H14	86.18				-	
i-Heptanes**	C7H16	100.20				-	
n-Heptane**	C7H16	100.20	0.0252	0.00025	0.0253	0.119	66.54
i-Octanes**	C8H18	114.23					
i-Nonanes**	C9H20	128.26					
n-Nonane**	C9H20	128.26					
i-Decanes**	C10H22	142.28					
n-Decane**	C10H22	142.28				-	
i-Undecanes+**	C11H24	156.31	0.2880	0.00288	0.4502	2.126	1,186.27
Benzene***	C6H6	78.11	0.0022	0.00002	0.0017	0.008	4.53
Ethylbenzene***	C8H10	106.17	0.0005	0.00001	0.0005	0.003	1.40
Toluene***	C7H8	92.14	0.0027	0.00003	0.0025	0.012	6.56
2,2,4-TMP***	C8H18	114.23	0.0033	0.00003	0.0038	0.018	9.93
n-Hexane***	C6H14	86.18	0.1154	0.00115	0.0994	0.470	262.06
Xylenes***	C8H10	106.17	0.0005	0.00001	0.0005	0.003	1.40
		Totals:	100.00	1.000	21.18	100.00	55,801.56
		Total VOC:	8.28	0.083	4.53	21.39	11,935.28
		Total HAP:	0.12	0.001	0.11	0.51	285.87

To be conservative, and to account for potential future changes in the gas quality, the following "worst-case" values were assumed:

Component	Formula	Representative Gas Analysis		Assumed "Worst-Case" Gas Analysis			
	Formula	Mole %	Wgt %	lb/MMscf	Mole %	Wgt %	lb/MMscf
Carbon Dioxide	CO2	0.15	0.32	178	0.22	0.45	250
Methane	CH4	78.03	59.11	32,986	100.00	100.00	42,275
VOC	C3 thru C10+	8.28	21.39	11,935	10.00	25.00	15,000
Benzene	C6H6	0.002	0.01	5	0.01	0.04	20
Ethylbenzene	C8H10	0.001	0.003	1	0.01	0.04	20
n-Hexane	C6H14	0.12	0.47	262	0.25	0.90	500
Toluene	C7H8	0.003	0.01	7	0.01	0.04	20
2,2,4-TMP***	C8H10	0.003	0.018	10	0.01	0.04	20
Xylenes	C8H10	0.001	0.003	1	0.01	0.04	20
Total HAP	C6 thru C8	0.12	0.51	286	0.50	1.50	600

## Williams Ohio Valley Midstream LLC (OVM)

## YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

## **Attachment H**

## **Gas Analysis**

## Legacy Measurement Solutions

Good

Canonsburg, PA 724-749-5180

Customer	: 2259 - WILLIAMS	Date Sampled	: 06/25/2014
Station ID	: 52214-50	Date Analyzed	: 07/03/2014
Cylinder ID	: W7080	Effective Date	: 07/01/2014
Producer	:	Cyl Pressure	: 976
Lease	: YOHO MASTER	Temp	: 83
Area	: 500 - OHIO VALLEY MID	Cylinder Type	: Spot
State	: WV	Sample By	: MC

: WV			: MC
COMPONENT	MOL%	GPM@14.73(PSIA)	<u>WT%</u>
Oxygen	0.0011	0.000	0.002
Nitrogen	0.4580	0.000	0.611
Methane	78.0288	0.000	59.658
Carbon-Dioxide	0.1537	0.000	0.322
Ethane	13.0878	3.512	18.756
Propane	5.1094	1.412	10.738
Iso-Butane	0.6003	0.197	1.663
Normal-Butane	1.4055	0.445	3.893
Iso-Pentane	0.3321	0.122	1.142
Normal-Pentane	0.3827	0.139	1.316
2,2-Dimethylbutane	0.0083	0.003	0.034
2,3-Dimethylbutane/CycloC5	0.0186	0.006	0.076
2-methylpentane	0.0828	0.034	0.340
3-methylpentane	0.0483	0.020	0.198
Normal-Hexane	0.1154	0.048	0.474
2,2-Dimethylpentane	0.0000	0.000	0.000
Methylcyclopentane	0.0151	0.005	0.061
BENZENE	0.0022	0.001	0.008
3,3-Dimethylpentane CYCLOHEXANE	0.0000	0.000	0.000
	0.0130	0.004	0.052
2-Methylhexane	0.0530	0.025	0.253
2,3-Dimethylpentane 3-Methylhexane	0.0000	0.000	0.000
•	0.0349 0.0000	0.016 0.000	0.167 0.000
1,t2-DMCYC5 / 2,2,4-TMC5	0.0003		0.000
1,t3-Dimethylcyclopentane	0.0003	0.000 0.012	0.120
N-Heptane			
METHYLCYCLOHEXANE	0.0150 0.0000	0.007 0.000	0.070 0.000
2,5-Dimethylhexane 2,3-Dimethylhexane	0.0000		0.000
TOLUENE	0.0007	0.000 0.001	0.000
	0.0027		0.000
2-Methylheptane	0.0000	0.000	0.000
4-Methylheptane	0.0000	0.000	0.000
3-Methylheptane	0.0005	0.000	0.000
1,t4-Dimethylcyclohexane	0.0025	0.001	0.013
N-OCTANE / 1,T2-DMCYC6 1.t3-DMCYC6/1,C4-	0.0033	0.002	0.000
DMCYC6/1,C2,C3-TMCYC5	0.0000	0.000	0.000
2,4,4 TMC6	0.0000	0.000	0.000
2,6-Dimethylheptane / 1,C2- DMCYC6	0.0000	0.000	0.000
Ethylcyclohexane	0.0000	0.000	0.000
ETHYLBENZENE	0.0000	0.000	0.000
M-XYLENE	0.0000	0.000	0.000
P-XYLENE	0.0000	0.000	0.000
O-XYLENE	0.0000	0.000	0.000
NONANE	0.0000	0.000	0.000
N-DECANE	0.0000	0.000	0.000
N-UNDECANE	0.0000	0.000	0.000
TOTAL	100.0000	6.012	99.998



## SAFETY DATA SHEET

#### 1. Identification

**Product identifier** 

**Natural Gas** 

Other means of identification

Not available.

**Synonyms** 

Methane, Natural Gas Sweet, Fuel Gas, Petroleum Gas, Methyl Hydride

Recommended use

Fuel.

Recommended restrictions

None known.

Manufacturer / Importer / Supplier / Distributor information

Company name

Williams, Inc.

**Address** 

One Williams Center Tulsa, OK 74172

US

Telephone

800-688-7507

E-mail

enterpriseehs@williams.com

Emergency phone number

888-677-2370

## 2. Hazard(s) identification

Physical hazards

Flammable gases

Category 1

Gases under pressure

Compressed gas

Health hazards
OSHA hazard(s)

Not classified.

Simple asphyxiant

Label elements

Hazard symbol



Signal word

Danger

Hazard statement

Extremely flammable gas. Contains gas under pressure; may explode if heated. May displace

oxygen and cause rapid suffocation.

**Precautionary statement** 

Prevention

Keep away from heat/sparks/open flames/hot surfaces. - No smoking.

Response

Leaking gas fire: Do not extinguish, unless leak can be stopped safely. Eliminate all ignition

sources if safe to do so.

Storage

Protect from sunlight. Store in a well-ventilated place.

Disposal

Dispose of contents/container in accordance with local/regional/national/international regulations.

Hazard(s) not otherwise

classified (HNOC)

Not classified.

## 3. Composition/information on ingredients

## Substance

Hazardous components

 Chemical name
 Common name and synonyms
 CAS number
 %

 Natural gas
 8006-14-2
 100

Composition comments

All concentrations are in percent by weight unless ingredient is a gas. Gas concentrations are in percent by volume.

4. First-aid measures

Inhalation

Move injured person into fresh air and keep person calm under observation. If breathing is difficult, give oxygen. Get medical attention if any discomfort continues.

Skin contact

Frostbite: Do not remove clothes, but flush with copious amounts of lukewarm water. Call an ambulance and continue to flush during transportation to hospital.

Eye contact

Immediately flush eyes with plenty of water for at least 15 minutes. Get medical attention if

irritation develops or persists.

Natural Gas 910557 Version #: 01 Revision date: - Issue date: 11-08-2012 SDS US

Ingestion

Most important symptoms/effects, acute and delayed

Indication of immediate medical attention and special treatment needed

Treat symptomatically.

General information Ensure that medical personnel are aware of the material(s) involved, and take precautions to protect themselves.

Narcosis. Behavioral changes. Decrease in motor functions.

### 5. Fire-fighting measures

Suitable extinguishing media Unsuitable extinguishing media Extinguish with foam, carbon dioxide, dry powder or water fog.

None.

Specific hazards arising from the chemical

Extremely flammable gas. Closed containers can burst violently when heated, due to excess pressure build-up. Gas may travel considerable distance to a source of ignition and flash back. Gases may form explosive mixtures with air. Fire or high temperatures create: Carbon monoxide. Carbon oxides. Sulfur oxides.

This material is a gas under normal atmospheric conditions and ingestion is unlikely. Natural Gas - Page 2 of 7

Special protective equipment and precautions for firefighters

Selection of respiratory protection for firefighting: follow the general fire precautions indicated in the workplace. Fire-fighters should wear appropriate protective equipment and self-contained breathing apparatus (SCBA) with full face-piece operated in positive pressure mode. Use approved gas detectors in confined spaces.

Fire-fighting equipment/instructions

Evacuate area. Move container from fire area if it can be done without risk. Stay away from ends of tanks. If a leak or spill has not ignited, use water spray to disperse the vapors and to protect men attempting to stop a leak. Cool equipment exposed to flames with water, if it can be done without risk. Close the valve if no risk is involved. Do not extinguish a leaking gas fire unless leak can be stopped. If leak cannot be stopped and no danger to surrounding area allow the fire to burn out. Fight fire from a protected location. Prevent buildup of vapors or gases to explosive concentrations.

## 6. Accidental release measures

Personal precautions, protective equipment and emergency procedures Extremely flammable. Spillages of liquid product will create a fire hazard and may form an explosive atmosphere. Keep all sources of ignition and hot metal surfaces away from spill/release if safe to do so. The use of explosion-proof electrical equipment is recommended. Beware of accumulation in low areas or contained areas, where explosive concentrations may occur. Prevent from entering drains or any places where accumulation may occur. Ventilate well and allow to evaporate. Stay upwind. Avoid inhalation and contact with skin and eyes. For large spillages notify persons down wind of the spill/release, isolate immediate hazard area and keep unauthorized personnel out. Wear appropriate personal protective equipment (See Section 8).

Methods and materials for containment and cleaning up Environmental precautions In the event of a spill or accidental release, notify relevant authorities in accordance with all applicable regulations.

Stop leak if possible without any risk. Water may be useful in minimizing or dispersing vapors. If spill occurs on water notify appropriate authorities in accordance with all applicable regulations.

### 7. Handling and storage

Precautions for safe handling

Keep away from sources of ignition - No smoking. Take precautionary measures against static discharges. Observe good industrial hygiene practices. Wear appropriate personal protective equipment (See Section 8).

Contents under pressure. Gas can accumulate in confined spaces and limit oxygen available for breathing. Use only with adequate ventilation. Use non-sparking hand tools and explosion-proof electrical equipment. The product can accumulate electrostatic charges, which may cause an electrical spark (ignition source). Ground container and transfer equipment to eliminate static electric sparks. Before entering storage tanks and commencing any operation in a confined area, check the atmosphere for oxygen content, hydrogen sulfide (H2S) and flammability. Cold burns may occur during filling operations. Containers and delivery lines may become cold enough to present cold burn hazard.

The use hydrocarbon fuel in an area without adequate ventilation may result in hazardous levels of incomplete combustion products (e.g. carbon monoxide, oxides of sulfur and nitrogen, benzene and other hydrocarbons) and/or dangerously low oxygen levels.

Natural Gas SDS US

Conditions for safe storage, including any incompatibilities Keep container(s) tightly closed and properly labeled. Use and store this material in cool, dry. well-ventilated areas away from heat, direct sunlight, hot metal surfaces, and all sources of ignition. Store only in approved containers. Post areas "No Smoking or Open Flame." Store away from incompatible materials. Protect against physical damage. Outdoor or detached storage is preferred. Indoor storage should meet OSHA standards and appropriate fire codes.

Empty containers may contain flammable product residues. Do not pressurize, cut, weld, braze, solder, drill, grind or expose empty containers to heat, flame, sparks, static electricity, or other sources of ignition; they may explode and cause injury or death.

## 8. Exposure controls/personal protection

### Occupational exposure limits

#### **US. ACGIH Threshold Limit Values**

Components	Туре	Value	
Natural gas (CAS	TWA	1000 ppm	

**Biological limit values** 

No biological exposure limits noted for the ingredient(s).

Exposure guidelines

No exposure standards allocated.

Appropriate engineering controls

Provide shower facilities near the work place. In confined spaces, make sure the area is well-ventilated and sufficient oxygen (19.5%) exists before entry. Good general ventilation (typically 10 air changes per hour) should be used. Ventilation rates should be matched to conditions. If applicable, use process enclosures, local exhaust ventilation, or other engineering controls to maintain airborne levels below recommended exposure limits. If exposure limits have not been established, maintain airborne levels to an acceptable level. Use explosion-proof

equipment.

Individual protection measures, such as personal protective equipment

Eye/face protection Wear approved safety glasses as a good hygiene practice.

Skin protection

Hand protection Wear suitable gloves as a good hygiene practice.

Other

Wear suitable protective clothing.

Respiratory protection

A NIOSH approved, self-containing breathing apparatus (SCBA) or equivalent operated in a pressure demand or other positive pressure mode should be used in situations of oxygen deficiency (oxygen content less than 19.5 percent), unknown exposure concentrations, or situations that are immediately dangerous to life or health (IDLH). A respiratory protection program that meets OSHA's 29 CFR 1910.134 and ANSI Z88.2 requirements must be followed

whenever work place conditions warrant a respirator's use.

Thermal hazards

Wear appropriate thermal protective clothing, when necessary.

General hygiene considerations

Handle in accordance with good industrial hygiene and safety practice.

### 9. Physical and chemical properties

**Appearance** Colorless gas.

Physical state

Gas Compressed.

**Form** 

Gas. Colorless.

Color

Odor

Odorless to slight, sweet.

**Odor threshold** 

Not available. Not applicable.

Melting point/freezing point

Not available.

Initial boiling point and boiling range

-259.6 °F (-162 °C)

Flash point

-304.6 °F (-187 °C)

**Evaporation rate** 

Not available.

Flammability (solid, gas)

Extremely flammable gas.

Upper/lower flammability or explosive limits

Flammability limit - lower

5 %

(%)

Flammability limit - upper

15 %

Explosive limit - lower (%) Not available. Explosive limit - upper (%) Not available.

Natural Gas SDS US 910557 Version #: 01 Revision date: -Issue date: 11-08-2012 3/7

Vapor pressure

40 mm Hg (77°F/25°C)

Slightly soluble in water.

Vapor density

0.55 Approximate.

Relative density

Solubility(ies)

Not available.

Partition coefficient (n-octanol/water)

1.81

Auto-ignition temperature

> 550.4 °F (> 288 °C)

Decomposition temperature

Not available.

Viscosity

Not available.

Other information

Percent volatile

100

### 10. Stability and reactivity

Reactivity

The product is non-reactive under normal conditions of use, storage and transport.

Chemical stability

Stable under normal temperature conditions and recommended use.

Possibility of hazardous

Polymerization will not occur.

reactions

Conditions to avoid

Heat, sparks, flames, elevated temperatures. Do not pressurize, cut, weld, braze, solder, drill, grind or expose empty containers to heat, flame, sparks, static electricity, or other sources of

ignition; they may explode and cause injury or death.

Incompatible materials

Oxidizing agents.

Hazardous decomposition

Carbon oxides. Sulfur oxides.

products

### 11. Toxicological information

### Information on likely routes of exposure

Ingestion

This material is a gas under normal atmospheric conditions and ingestion is unlikely.

Inhalation

High concentrations: Suffocation (asphyxiant) hazard - if allowed to accumulate to concentrations that reduce oxygen below safe breathing levels. In high concentrations, vapors are narcotic and

may cause headache, fatigue, dizziness and nausea.

Skin contact

Contact with liquefied gas can cause damage (frostbite) due to rapid evaporative cooling.

Eye contact

Contact with liquefied gas can cause damage (frostbite) due to rapid evaporative cooling.

Symptoms related to the physical, chemical and toxicological characteristics

Exposure to rapidly expanding gas or vaporizing liquid may cause frostbite ("cold burn"). Contact with evaporating liquid may cause frostbite or freezing of skin. Symptoms of overexposure can include shortness of breath, drowsiness, headaches, confusion, decreased coordination, visual disturbances and vomiting, and are reversible if exposure is stopped. Continued exposure can lead to hypoxia (inadequate oxygen), rapid breathing, cyanosis (bluish discoloration of skin), numbness of the extremities, unconsciousness and death.

## Information on toxicological effects

Acute toxicity

Suffocation (asphyxiant) hazard - if allowed to accumulate to concentrations that reduce oxygen below safe breathing levels. Exposure to rapidly expanding gas or vaporizing liquid may cause frostbite ("cold burn").

**Product** Natural gas (CAS 8006-14-2)

Acute

Oral

LD50

Rat

> 5 g/kg

**Test Results** 

Skin corrosion/irritation

Not classified.

Not classified.

**Species** 

Serious eye damage/eye

irritation

Respiratory sensitization

Not classified.

Skin sensitization Germ cell mutagenicity Not a skin sensitizer. Not classified.

Carcinogenicity

Not classified.

Reproductive toxicity

Not classified.

Specific target organ toxicity -

single exposure

Not classified.

Specific target organ toxicity -

repeated exposure

Not classified.

Natural Gas 910557

Version #: 01

Revision date: -

Issue date: 11-08-2012

SDS US

Aspiration hazard

Not applicable.

Chronic effects

Prolonged exposure may cause chronic effects.

### 12. Ecological information

**Ecotoxicity** 

Not expected to be harmful to aquatic organisms.

Persistence and degradability

The hydrocarbons in this material are expected to be inherently biodegradable. In practice, hydrocarbon gases are not likely to remain in solution long enough for biodegradation to be a significant loss process. Hydrogen sulfide, if present in refinery gas streams, will be oxidized in water and insoluble sulfides precipitated from water when metallic radicals are present.

Bioaccumulative potential

The product is not expected to bioaccumulate.

Partition coefficient n-octanol / water (log Kow)

Natural gas

1.81

Mobility in soil

Not relevant, due to the form of the product.

Mobility in general

The product is a volatile substance, which may spread in the atmosphere.

Other adverse effects

The product is a volatile organic compound which has a photochemical ozone creation potential.

## 13. Disposal considerations

Disposal instructions

This material is a gas and would not typically be managed as a waste.

Local disposal regulations

Disposal recommendations are based on material as supplied. Disposal must be in accordance with current applicable laws and regulations, and material characteristics at time of disposal.

Hazardous waste code

D001

Waste from residues / unused

products

Dispose of in accordance with local regulations.

Contaminated packaging

Since emptied containers may retain product residue, follow label warnings even after container is

emptied.

### 14. Transport information

#### DOT

**UN number** 

UN1971

UN proper shipping name

Natural gas, compressed

Transport hazard class(es)

2.1

Subsidary class(es)

Not available.

Packing group

Not available.

Special precautions for user Not available.

Labels required

2.1

Packaging exceptions

306 302

Packaging non bulk Packaging bulk

**UN** number

302

IATA

UN1971

UN proper shipping name

Natural gas, compressed

Transport hazard class(es)

Subsidary class(es)

Packaging group

Not available. No

**Environmental hazards** Labels required

2.1

**ERG Code** 

10L

Special precautions for user Not available.

#### **IMDG**

**UN** number

UN1971

UN proper shipping name

NATURAL GAS, COMPRESSED

Transport hazard class(es)

Subsidary class(es)

Packaging group **Environmental hazards** 

Marine pollutant Labels required

No 2,1

F-D, S-U

Special precautions for user Not available.

Transport in bulk according to

Not available.

Annex II of MARPOL 73/78 and

No information available.

the IBC Code

Natural Gas

910557 Version #: 01

Revision date: - Issue date: 11-08-2012

SDS US

### 15. Regulatory information

US federal regulations

This product is a "Hazardous Chemical" as defined by the OSHA Hazard Communication

Standard, 29 CFR 1910.1200.

All components are on the U.S. EPA TSCA Inventory List.

TSCA Section 12(b) Export Notification (40 CFR 707, Subpt. D)

Not regulated.

US. OSHA Specifically Regulated Substances (29 CFR 1910.1001-1050)

Not on regulatory list.

CERCLA Hazardous Substance List (40 CFR 302.4)

Natural gas (CAS 8006-14-2)

LISTED

Superfund Amendments and Reauthorization Act of 1986 (SARA)

Hazard categories

Immediate Hazard - Yes Delayed Hazard - No Fire Hazard - Yes Pressure Hazard - Yes Reactivity Hazard - No

**SARA 302 Extremely** 

hazardous substance SARA 311/312 Hazardous

Yes

No

chemical

### Other federal regulations

Clean Air Act (CAA) Section 112 Hazardous Air Pollutants (HAPs) List

Not regulated.

Clean Air Act (CAA) Section 112(r) Accidental Release Prevention (40 CFR 68.130)

Not regulated.

Safe Drinking Water Act

Not regulated.

(SDWA)

Drug Enforcement Administration (DEA). List 2, Essential Chemicals (21 CFR 1310.02(b) and 1310.04(f)(2) and Chemical **Code Number** 

Not listed.

Drug Enforcement Administration (DEA). List 1 & 2 Exempt Chemical Mixtures (21 CFR 1310.12(c))

Not regulated.

**DEA Exempt Chemical Mixtures Code Number** 

Not regulated.

Food and Drug

Not regulated.

Administration (FDA) US state regulations

This product does not contain a chemical known to the State of California to cause cancer, birth

defects or other reproductive harm.

US. Massachusetts RTK - Substance List

Natural gas (CAS 8006-14-2)

US. New Jersey Worker and Community Right-to-Know Act

Not regulated.

US. Pennsylvania RTK - Hazardous Substances

Natural gas (CAS 8006-14-2)

US. Rhode Island RTK

Not regulated.

**US. California Proposition 65** 

US - California Proposition 65 - Carcinogens & Reproductive Toxicity (CRT): Listed substance

Not listed.

### International Inventories

Country(s) or region	Inventory name	On inventory (yes/no)*
Australia	Australian Inventory of Chemical Substances (AICS)	Yes
Canada	Domestic Substances List (DSL)	Yes
Canada	Non-Domestic Substances List (NDSL)	No
China	Inventory of Existing Chemical Substances in China (IECSC)	Yes
Europe	European Inventory of Existing Commercial Chemical Substances (EINECS)	Yes
Europe	European List of Notified Chemical Substances (ELINCS)	No

**Natural Gas** SDS US

Yes

Country(s) or region Inventory name On inventory (yes/no)\* Japan Inventory of Existing and New Chemical Substances (ENCS) No Korea Existing Chemicals List (ECL) Yes New Zealand New Zealand Inventory Yes **Philippines** Philippine Inventory of Chemicals and Chemical Substances No (PICCS)

\*A "Yes" indicates this product complies with the inventory requirements administered by the governing country(s)

Toxic Substances Control Act (TSCA) Inventory

## 16. Other information, including date of preparation or last version

Issue date

11-08-2012

Revision date

...

Version #

01

Further information

United States & Puerto Rico

Not available.

References

Registry of Toxic Effects of Chemical Substances (RTECS)

Disclaimer

This information is provided without warranty. The information is believed to be correct. This information should be used to make an independent determination of the methods to safeguard

workers and the environment.

 Natural Gas
 SDS US

 910557
 Version #: 01
 Revision date: - Issue date: 11-08-2012
 7 / 7

1



# MATERIAL SAFETY DATA SHEET

### PRODUCT AND COMPANY IDENTIFICATION

Product Name: Natural Gas Condensate

Synonyms: Condensate, Gas Condensate, Distillate, Pipeline Drip, Natural gasoline, Casinghead gasoline,

Straight-run gasoline, Isoparaffin mixture, and Drip gas

Manufacturer Name: Emergency Telephone:

Williams, Inc. 888-677-2370 One Williams Center

Tulsa, OK 74172

Non-emergency Telephone:
800-688-7507

Intended Use: Industrial use

## HAZARDS IDENTIFICATION

# Emergency Overview

Physical State: Liquid

Color: Colorless to brownish-black

**Odor:** Petroleum

## DANGER!

2

Harmful if inhaled or absorbed through skin. Harmful if swallowed - may enter lungs if swallowed or vomited. Causes skin and eye irritation. High vapor concentrations may cause drowsiness and irritation of the eyes or respiratory tract.

Extremely flammable liquid and vapor - vapor may cause flash fire.

## **Potential Health Effects**

**Inhalation:** Harmful if inhaled. May cause central nervous system effects.

Eye Contact: Causes eye irritation. High vapor concentrations may cause irritation.

**Skin Contact:** Harmful if absorbed through skin. Causes skin irritation.

**Ingestion:** Harmful if swallowed - may enter lungs if swallowed or vomited.

**Chronic Health Effects:** Long-term exposure to condensate vapor has caused kidney and liver cancer in laboratory animals. Case reports of chronic condensate abuse (such as sniffing) and chronic misuse as a solvent or as a cleaning agent have shown a range of nervous system effects, sudden deaths from heart attacks, blood effects and leukemia. These effects are not expected to occur at exposure levels encountered in the distribution and use of condensate as a motor fuel. Prolonged and repeated exposure to benzene may

cause serious injury to blood forming organs and is associated with anemia and to the later development of acute myelogenous leukemia (AML).

**Target Organ(s):** | Central nervous system | Eye | Kidney | Liver | Skin | Blood and/or blood-forming organs |

**OSHA Regulatory Status:** This product is hazardous according to OSHA 29CFR 1910.1200.

## 3 COMPOSITION / INFORMATION ON INGREDIENTS

**General Information:** Condensate is a complex mixture of volatile hydrocarbons, primarily in the C3 to C8 range. The composition varies depending on the natural gas source and processing, but typically includes some concentration of benzene.

Chemical Name	CAS-No.	Concentration*
†Natural gas condensates (petroleum)	68919-39-1	97.9 - 99.6%
†Benzene	71-43-2	0.4 - 2.1%

<sup>\*</sup> All concentrations are in percent by weight unless ingredient is a gas. Gas concentrations are in percent by volume.

## 4 FIRST AID MEASURES

**Inhalation:** Move to fresh air. If not breathing, give artificial respiration. If breathing is difficult, give oxygen. Get medical attention immediately.

**Eye Contact:** Immediately flush with plenty of water for at least 15 minutes. If easy to do, remove contact lenses. Get medical attention. In case of irritation from airborne exposure, move to fresh air. Get medical attention if symptoms persist.

**Skin Contact:** Immediately flush with plenty of water for at least 15 minutes while removing contaminated clothing and shoes. Get medical attention immediately. Wash contaminated clothing before reuse. Destroy or thoroughly clean contaminated shoes.

**Ingestion:** Call a physician or poison control center immediately. DO NOT induce vomiting. if victim is fully conscious, give a cupful of water. Never give anything by mouth to an unconscious person. If vomiting occurs, keep head lower than the hips to help prevent aspiration.

## 5 FIRE-FIGHTING MEASURES

**Extinguishing Media:** Extinguish with foam, carbon dioxide, dry powder or water fog.

**Unsuitable Extinguishing Media:** Not applicable.

**Special Fire Fighting Procedures:** Self-contained breathing apparatus and full protective clothing should be worn when fighting chemical fires. Use water spray to keep fire-exposed containers cool.

**Unusual Fire & Explosion Hazards:** Material will float and may ignite on surface of water. Vapors may travel considerable distance to a source of ignition and flash back. Vapors may cause a flash fire or ignite explosively.

Hazardous Combustion Products: Carbon Oxides

<sup>†</sup> This chemical is hazardous according to OSHA/WHMIS criteria.

## 6 ACCIDENTAL RELEASE MEASURES

**Personal Precautions:** Wear protective clothing as described in Section 8 of this safety data sheet.

**Spill Cleanup Methods:** Eliminate all ignition sources. Small Liquid Spills: Use a non-combustible material like vermiculite, sand or earth to soak up the product and place into a container for later disposal. Large Spillages: Use water spray to disperse vapors and flush spill area. Prevent runoff from entering drains, sewers, or streams. Dike for later disposal.

## 7 HANDLING AND STORAGE

**Handling:** Do not breathe mist or vapor. Do not get in eyes, on skin, on clothing. Do not taste or swallow. Use only with adequate ventilation. Wash thoroughly after handling.

**Storage:** Keep away from heat, sparks and open flame. Keep container tightly closed and in a well-ventilated place. Comply with all national, state, and local codes pertaining to the storage, handling, dispensing, and disposal of flammable liquids. Keep away from food, drink and animal feed. Store away from incompatible materials.

## EXPOSURE CONTROLS / PERSONAL PROTECTION

## **Exposure Limits:**

8

Chemical Name	Source	Type	<b>Exposure Limits</b>	Notes
Benzene	CA. Alberta OELs	STEL	16 mg/m <sup>3</sup> 5 ppm	Skin
Benzene	CA. Alberta OELs	TWA	3.2 mg/m <sup>3</sup> 1 ppm	Skin
Benzene	CA. British Columbia	TWA	0.5 ppm	Skin
	OELs			
Benzene	CA. British Columbia	STEL	2.5 ppm	Skin
	OELs			
Benzene	CA. Ontario OELs	STEL	2.5 ppm	
Benzene	CA. Ontario OELs	TWA	0.5 ppm	
Benzene	CA. Quebec OELs	TWA	3 mg/m³ 1 ppm	
Benzene	CA. Quebec OELs	STEL	15.5 mg/m <sup>3</sup> 5 ppm	
Benzene	MEX. OELs	STEL	16 mg/m <sup>3</sup> 5 ppm	
Benzene	MEX. OELs	TWA	3.2 mg/m <sup>3</sup> 1 ppm	
Benzene	US. ACGIH TLV	STEL	2.5 ppm	Skin
Benzene	US. ACGIH TLV	TWA	0.5 ppm	Skin
Benzene	US. NIOSH Guide	IDLH	500 ppm	
Benzene	US. OSHA Spec. Reg.	OSHA	0.5 ppm	
		Action		
		level		
Benzene	US. OSHA Spec. Reg.	STEL	5 ppm	
Benzene	US. OSHA Spec. Reg.	TWA	1 ppm	
Benzene	US. OSHA Z-2 PEL	TWA	10 ppm	
Benzene	US. OSHA Z-2 PEL	Maximum	50 ppm	
		concentrati		
		on		
Benzene	US. OSHA Z-2 PEL	Ceiling	25 ppm	

**Engineering Controls:** Good general ventilation (typically 10 air changes per hour) should be used. Ventilation rates should be matched to conditions. If applicable, use process enclosures, local exhaust ventilation, or other engineering controls to maintain airborne levels below recommended exposure limits.

If exposure limits have not been established, maintain airborne levels to an acceptable level.

**Respiratory Protection:** If engineering controls do not maintain airborne concentrations below recommended exposure limits (where applicable) or to an acceptable level (in countries where exposure limits have not been established), an approved respirator must be worn. In the United States of America, if respirators are used, a program should be instituted to assure compliance with OSHA Standard 63 FR 1152, January 8, 1998. Respirator type: Air-purifying respirator with an appropriate, government approved (where applicable), air-purifying filter, cartridge or canister. Contact health and safety professional or manufacturer for specific information.

**Eye Protection:** Wear safety glasses with side shields (or goggles). Wear a full-face respirator, if needed.

Hand Protection: Wear chemical-resistant gloves. Contact glove manufacturer for specific information.

**Skin Protection:** Wear appropriate chemical resistant clothing to prevent any possibility of skin contact.

**Hygiene Measures:** Always observe good personal hygiene measures, such as washing after handling the material and before eating, drinking, and/or smoking. Routinely wash work clothing and protective equipment to remove contaminants.

**Environmental Exposure Controls:** Environmental manager must be informed of all major spillages.

## PHYSICAL AND CHEMICAL PROPERTIES

**Color:** Colorless to brownish-black

**Odor:** Petroleum

**Odor Threshold:** No data available.

Physical State: LiquidpH: Not applicable

**Melting Point:** No data available. **Freezing Point:** No data available.

**Boiling Point:**  $45^{\circ}\text{C} (113^{\circ}\text{F}) - 404^{\circ}\text{C} (759^{\circ}\text{F})$ **Flash Point:**  $<-18^{\circ}\text{C} (0^{\circ}\text{F}) \text{ (Approximate)}$ 

**Evaporation Rate:** >100 [vs. n-Butyl Acetate = 1]

Flammability (Solid): No data available.

Flammability Limit - Upper (%): 10 (Approximate)
Flammability Limit - Lower (%): 1 (Approximate)
Vapor Pressure: 51 mmHg - 857 mmHg @100°F [Reid]

Vapor Density (Air=1): > 1 Specific Gravity: 0.766 - 0.87 Solubility in Water: Negligible Solubility (Other): No data available.

Partition Coefficient (n-Octanol/water): No data available.

**Autoignition Temperature:** No data available. **Decomposition Temperature:** No data available.

**Viscosity:** < 1 cst @38°C **Percent Volatile:** 100 %vol

Explosive Properties: No data available

## 10 STABILITY AND REACTIVITY

**Stability:** Stable under the prescribed storage conditions.

**Conditions to Avoid:** Keep away from heat, sparks and open flame. Prevent buildup of vapors or gases to explosive concentrations.

**Incompatible Materials:** Strong oxidizing agents.

**Hazardous Decomposition Products:** No data available.

## 11 TOXICOLOGICAL INFORMATION

## **Specified Substance(s)**

**Acute Toxicity:** 

### **Test Results:**

Chemical Name	Test Results
Natural gas condensates (petroleum)	Dermal LD50 (Rabbit): > 3750 mg/kg
Natural gas condensates (petroleum)	Inhalation LC50 (Rat): > 5.2 mg/l
Natural gas condensates (petroleum)	Oral LD50 (Rat): > 5000 mg/kg

**Chronic Toxicity:** Contains benzene. Human epidemiology studies indicate that prolonged and/or repeated overexposure to benzene may cause damage to the blood-producing system and serious blood disorders, including leukemia. Animal tests suggest that prolonged and/or repeated overexposure to benzene may damage the embryo/fetus. The relevance of these animal studies to humans has not been fully established.

### **Listed Carcinogens:**

Chemical Name	IARC	NTP	OSHA	ACGIH
Benzene	1	Listed	Listed	A1

IARC: 1 = Carcinogenic to Humans; 2A = Probably Carcinogenic to Humans; 2B = Possibly Carcinogenic to Humans; 3 = Not classifiable as to carcinogenicity to humans; 4 = Probably not carcinogenic to humans; Not listed = Not evaluated by IARC. ACGIH: A1 = Confirmed Human Carcinogen; A2 = Suspected Human Carcinogen; A3 = Confirmed Animal Carcinogen; A4 = Not classifiable as a human carcinogen; A5 = Not suspected to be a human carcinogen; Not listed = Not evaluated by ACGIH.

## **Product Information**

**Acute Toxicity:** 

**Test Results:** No test data available for the product.

**Other Acute:** Harmful if inhaled or absorbed through skin. Harmful if swallowed - may enter lungs if swallowed or vomited. Causes severe skin and eye irritation. High vapor concentrations may cause drowsiness and irritation of the eyes or respiratory tract.

**Chronic Toxicity:** Long-term exposure to gasoline vapor has caused kidney and liver cancer in laboratory animals. Case reports of chronic gasoline abuse (such as sniffing) and chronic misuse as a solvent or as a cleaning agent have shown a range of nervous system effects, sudden deaths from heart attacks, blood effects and leukemia. These effects are not expected to occur at exposure levels encountered in the distribution and use of gasoline as a motor fuel.

## 12 ECOLOGICAL INFORMATION

**Ecotoxicity:** There are no data on the ecotoxicity of this product.

Mobility: No data available.

Persistence and Degradability: No data available.

Bioaccumulation Potential: No data available.

## 13 DISPOSAL CONSIDERATIONS

**General Information:** Dispose of waste and residues in accordance with local authority requirements.

**Disposal Methods:** No specific disposal method required.

**Container:** Since emptied containers retain product residue, follow label warnings even after container is emptied.

## 14 TRANSPORT INFORMATION

### DOT

UN No.: UN1993

**Proper Shipping Name:** Flammable liquids, n.o.s. (Natural gas condensates)

Class: 3

Packing Group: II

Label(s): 3

## **TDG**

UN No.: UN1993

**Proper Shipping Name:** Flammable liquid, n.o.s. (Natural gas condensates)

Class: 3

Packing Group: II

### **IATA**

UN No.: UN1993

**Proper Shipping Name:** Flammable liquid, n.o.s. (Natural gas condensates)

Class: 3

Packing Group: II

Label(s): 3

## <u>IMDG</u>

UN No.: UN1993

**Proper Shipping Name:** Flammable liquid, n.o.s. (Natural gas condensates)

Class: 3

**Packing Group:** II **EmS No.:** F-E, S-E

## 15 REGULATORY INFORMATION

**Canadian Controlled Products Regulations:** This product has been classified according to the hazard criteria of the Canadian Controlled Products Regulations, Section 33, and the MSDS contains all required information.

WHMIS Classification: B2, D2A, D2B

**Mexican Dangerous Statement:** This product is dangerous according to Mexican regulations.

### OSHA Specifically Regulated Substances (29 CFR 1910.1001-.1052):

Chemical Name	CAS-No.		
Benzene	71-43-2		

## **Inventory Status**

This product or all components are listed or exempt from listing on the following inventory: TSCA

## **US Regulations**

**CERCLA Hazardous Substance List (40 CFR 302.4):** 

Chemical Name	RQ
Benzene	10 lbs

## **SARA** Title III

Section 302 Extremely Hazardous Substances (40 CFR 355, Appendix A): Not regulated.

X	Acute (Immediate)	X Chronic (Delayed)	X Fire	Reactive		Pressure Generating
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## Section 313 Toxic Release Inventory (40 CFR 372):

Chemical Name		for other users	Reporting threshold for manufacturing and processing
Benzene	71-43-2	10000 lbs	25000 lbs

For reporting purposes: the De Minimis Concentration for a toxic chemical in a mixture is 0.1% for carcinogens as defined in 29 CFR 1910.1200(d)(4) or 1% for others.

Clean Air Act (CAA) Section 112(r) Accidental Release Prevention (40 CFR 68.130): Not regulated.

Clean Water Act Section 311 Hazardous Substances (40 CFR 117.3): Benzene

**<u>Drug Enforcement Act:</u>** Not regulated.

## **TSCA**

TSCA Section 4(a) Final Test Rules & Testing Consent Orders: Not regulated.

TSCA Section 5(a)(2) Final Significant New Use Rules (SNURs) (40CFR 721, Subpt. E): Not regulated.

TSCA Section 5(e) PMN-Substance Consent Orders: Not regulated.

TSCA Section 12(b) Export Notification (40 CFR 707, Subpt. D): Not regulated.

## **State Regulations**

California Safe Drinking Water and Toxic Enforcement Act of 1986 (Proposition 65): Benzene

Massachusetts Right-To-Know List: Benzene

Michigan Critical Materials List (Michigan Natural Resources and Environmental Protection Act

(Act. 451 of 1994)): Benzene

Minnesota Hazardous Substances List: Benzene

New Jersey Right-To-Know List: Benzene

Pennsylvania Right-To-Know List: Benzene

Rhode Island Right-To-Know List: Benzene

## 16 OTHER INFORMATION

## **HAZARD RATINGS**

	Health Hazard	Fire Hazard	Instability	Special Hazard
NFPA	2	4	0	NONE

Hazard rating: 0 - Minimal; 1 - Slight; 2 - Moderate; 3 - Serious; 4 - Severe

NFPA Label colored diamond code: Blue - Health; Red - Flammability; Yellow - Instability; White - Special Hazards

	Health Hazard	Flammability	Physical Hazard	<b>Personal Protection</b>
HMIS	2*	4	0	

Hazard rating: 0 - Minimal; 1 - Slight; 2 - Moderate; 3 - Serious; 4 - Severe \*- Chronic Health Effect HMIS Label colored bar code: Blue - Health; Red - Flammability; Orange - Physical Hazards; White - Special

**Issue Date:** 31-Mar-2009 **Supercedes Date:** 28-Jul-1999

**SDS No.:** 1023419

**Disclaimer:** This information is provided without warranty. The information is believed to be correct. This information should be used to make an independent determination of the methods to safeguard workers and the environment.







# Material Safety Data Sheet Triethylene glycol MSDS

## **Section 1: Chemical Product and Company Identification**

Product Name: Triethylene glycol

Catalog Codes: SLT2644

CAS#: 112-27-6

**RTECS:** YE4550000

TSCA: TSCA 8(b) inventory: Triethylene glycol

CI#: Not available.

**Synonym:** 2,2'-[1,2-Ethanediylbis(oxy)]bisethanol

Chemical Formula: C6H14O4

**Contact Information:** 

Sciencelab.com, Inc. 14025 Smith Rd. Houston, Texas 77396

US Sales: 1-800-901-7247

International Sales: 1-281-441-4400

Order Online: ScienceLab.com

CHEMTREC (24HR Emergency Telephone), call:

1-800-424-9300

International CHEMTREC, call: 1-703-527-3887

For non-emergency assistance, call: 1-281-441-4400

## Section 2: Composition and Information on Ingredients

## Composition:

Name	CAS#	% by Weight
Triethylene glycol	112-27-6	100

Toxicological Data on Ingredients: Triethylene glycol: ORAL (LD50): Acute: 17000 mg/kg [Rat].

### Section 3: Hazards Identification

### **Potential Acute Health Effects:**

Very hazardous in case of eye contact (irritant), of ingestion. Slightly hazardous in case of inhalation. Inflammation of the eye is characterized by redness, watering, and itching.

### **Potential Chronic Health Effects:**

Very hazardous in case of eye contact (irritant). Slightly hazardous in case of inhalation. CARCINOGENIC EFFECTS: Not available. MUTAGENIC EFFECTS: Not available. TERATOGENIC EFFECTS: Not available. DEVELOPMENTAL TOXICITY: Not available. The substance is toxic to kidneys, the nervous system. Repeated or prolonged exposure to the substance can produce target organs damage.

## **Section 4: First Aid Measures**

### **Eye Contact:**

Check for and remove any contact lenses. Immediately flush eyes with running water for at least 15 minutes, keeping eyelids open. Cold water may be used. Do not use an eye ointment. Seek medical attention.

**Skin Contact:** No known effect on skin contact, rinse with water for a few minutes.

Serious Skin Contact: Not available.

**Inhalation:** Allow the victim to rest in a well ventilated area. Seek immediate medical attention.

Serious Inhalation: Not available.

## Ingestion:

Do not induce vomiting. Loosen tight clothing such as a collar, tie, belt or waistband. If the victim is not breathing, perform mouth-to-mouth resuscitation. Seek immediate medical attention.

Serious Ingestion: Not available.

## **Section 5: Fire and Explosion Data**

Flammability of the Product: May be combustible at high temperature.

**Auto-Ignition Temperature:** 371°C (699.8°F)

Flash Points: CLOSED CUP: 177°C (350.6°F). OPEN CUP: 165.5°C (329.9°F).

Flammable Limits: LOWER: 0.9% UPPER: 9.2%

**Products of Combustion:** These products are carbon oxides (CO, CO2).

Fire Hazards in Presence of Various Substances: Not available.

## **Explosion Hazards in Presence of Various Substances:**

Risks of explosion of the product in presence of mechanical impact: Not available. Risks of explosion of the product in presence of static discharge: Not available.

### **Fire Fighting Media and Instructions:**

SMALL FIRE: Use DRY chemical powder. LARGE FIRE: Use water spray, fog or foam. Do not use water jet.

Special Remarks on Fire Hazards: Not available.

Special Remarks on Explosion Hazards: Not available.

## Section 6: Accidental Release Measures

#### Small Spill:

Dilute with water and mop up, or absorb with an inert dry material and place in an appropriate waste disposal container. Finish cleaning by spreading water on the contaminated surface and dispose of according to local and regional authority requirements.

#### Large Spill:

Absorb with an inert material and put the spilled material in an appropriate waste disposal. Finish cleaning by spreading water on the contaminated surface and allow to evacuate through the sanitary system.

## **Section 7: Handling and Storage**

### Precautions:

Keep away from heat. Keep away from sources of ignition. Empty containers pose a fire risk, evaporate the residue under a fume hood. Ground all equipment containing material. Do not ingest. Do not breathe gas/fumes/ vapour/spray. Avoid contact with eyes If ingested, seek medical advice immediately and show the container or the label.

### Storage:

Keep container dry. Keep in a cool place. Ground all equipment containing material. Keep container tightly closed. Keep in a cool, well-ventilated place. Combustible materials should be stored away from extreme heat and away from strong oxidizing agents.

## **Section 8: Exposure Controls/Personal Protection**

### **Engineering Controls:**

Provide exhaust ventilation or other engineering controls to keep the airborne concentrations of vapors below their respective threshold limit value. Ensure that eyewash stations and safety showers are proximal to the work-station location.

Personal Protection: Splash goggles. Lab coat.

## Personal Protection in Case of a Large Spill:

Splash goggles. Full suit. Boots. Gloves. Suggested protective clothing might not be sufficient; consult a specialist BEFORE

handling this product.

**Exposure Limits:** Not available.

## **Section 9: Physical and Chemical Properties**

Physical state and appearance: Liquid. (Hygroscopic liquid.)

Odor: Not available.

Taste: Not available.

Molecular Weight: 150.18 g/mole

Color: Colorless.

pH (1% soln/water): Not available.

Boiling Point: 285°C (545°F)

Melting Point: -5°C (23°F)

Critical Temperature: Not available.

Specific Gravity: 1.1274 (Water = 1)

Vapor Pressure: Not available. Vapor Density: 5.17 (Air = 1)

Volatility: Not available.

Odor Threshold: Not available.

Water/Oil Dist. Coeff.: Not available. lonicity (in Water): Not available.

**Dispersion Properties:** See solubility in water.

Solubility: Easily soluble in cold water.

## Section 10: Stability and Reactivity Data

Stability: The product is stable.

Instability Temperature: Not available.Conditions of Instability: Not available.

Incompatibility with various substances: Not available.

Corrosivity: Non-corrosive in presence of glass.

Special Remarks on Reactivity: Not available.

Special Remarks on Corrosivity: Not available.

Polymerization: No.

## **Section 11: Toxicological Information**

Routes of Entry: Eye contact. Ingestion.

Toxicity to Animals: Acute oral toxicity (LD50): 17000 mg/kg [Rat].

Chronic Effects on Humans: The substance is toxic to kidneys, the nervous system.

Other Toxic Effects on Humans:

Very hazardous in case of ingestion. Slightly hazardous in case of inhalation.

Special Remarks on Toxicity to Animals: Not available.

Special Remarks on Chronic Effects on Humans: Not available.

Special Remarks on other Toxic Effects on Humans: Not available.

## **Section 12: Ecological Information**

**Ecotoxicity:** Not available.

BOD5 and COD: Not available.

Products of Biodegradation:

Possibly hazardous short term degradation products are not likely. However, long term degradation products may arise.

**Toxicity of the Products of Biodegradation:** The products of degradation are more toxic.

Special Remarks on the Products of Biodegradation: Not available.

## **Section 13: Disposal Considerations**

Waste Disposal:

## **Section 14: Transport Information**

**DOT Classification:** Not a DOT controlled material (United States).

Identification: Not applicable.

Special Provisions for Transport: Not applicable.

## **Section 15: Other Regulatory Information**

**Federal and State Regulations:** 

Pennsylvania RTK: Triethylene glycol TSCA 8(b) inventory: Triethylene glycol

Other Regulations: OSHA: Hazardous by definition of Hazard Communication Standard (29 CFR 1910.1200).

Other Classifications:

WHMIS (Canada): Not controlled under WHMIS (Canada).

DSCL (EEC): R41- Risk of serious damage to eyes.

HMIS (U.S.A.):

Health Hazard: 1

Fire Hazard: 1

Reactivity: 0

Personal Protection: i

National Fire Protection Association (U.S.A.):

Health: 1

Flammability: 1

Reactivity: 0

Specific hazard:

**Protective Equipment:** 

Not applicable. Lab coat. Not applicable. Splash goggles.

## **Section 16: Other Information**

References: Not available.

Other Special Considerations: Not available.

Created: 10/10/2005 08:31 PM

Last Updated: 05/21/2013 12:00 PM

The information above is believed to be accurate and represents the best information currently available to us. However, we make no warranty of merchantability or any other warranty, express or implied, with respect to such information, and we assume no liability resulting from its use. Users should make their own investigations to determine the suitability of the information for their particular purposes. In no event shall ScienceLab.com be liable for any claims, losses, or damages of any third party or for lost profits or any special, indirect, incidental, consequential or exemplary damages, howsoever arising, even if ScienceLab.com has been advised of the possibility of such damages.

## **ATTACHMENT I**

# **Emission Units Table**

"25. Fill out the <b>Emission Units Table</b> and provide it as Attachment I."
Emissions Unit Table

## Williams Ohio Valley Midstream LLC (OVM)

## YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

### Attachment I

## **EMISSION UNITS TABLE**

(Include all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status.)

Unit ID <sup>1</sup>	Point ID <sup>2</sup>	Description	Installed	Capacity	Type <sup>3</sup> and Date	Control <sup>4</sup>
CE-01	1E	CAT G3306TA Compressor Engine	2013	203 bhp	Existing	01-NSCR
RBV-1	2E	TEG Dehydrator - Reboiler	2013	0.14 MMBtu/hr	Existing	na
RSV-1	3E	TEG Dehydrator - Flash Tank and Still Column	2013	2.0 MMscfd	Modifed	na
T01	4E	Produced Water - Storage Tank	2013	210 bbl	Exisiting	na
TLO	5E	Produced Water - Truck Loadout	2013		Exisiting	na
SSM	6E	Startup, Shutdown and Maintenance (Blowdown)	2013		Exisiting	na
FUG	7E	Process Piping and Equipment Fugitives	2013		Exisiting	na
RPC	8E	Compressor Rod Packing and Crankcase Leaks	2013		Exisiting	na

<sup>&</sup>lt;sup>1</sup> For Emission Units (or <u>Sources</u>) use the following numbering system: 1S, 2S, 3S, ... or other appropriate designation.

Emissions Units Table 03/2007

<sup>&</sup>lt;sup>2</sup> For Emission Points use the following numbering system: 1E, 2E, 3E, ... or other appropriate designation.

<sup>&</sup>lt;sup>3</sup> New, modification, removal, etc.

<sup>&</sup>lt;sup>4</sup> For Control Devices use the following numbering system: 1C, 2C, 3C, ... or other appropriate designation.

## **ATTACHMENT J**

## **Emission Points Data Summary Sheet**

"26. Fill out the **Emission Points Data Summary Sheet** (Table 1 and Table 2) and provide it as Attachment J."

### Table 1 – Emissions Data

- o 203 bhp CAT G3306TA (4SRB@1800 rpm) Compressor Engine (CE-01 (1E))
- o 0.14 MMBtu/hr TEG Dehydrator Reboiler (RBV (2E))
- 2.0 MMscfd TEG Dehydrator Flash Tank and Still Vent (RSV-1 (3E))
- 210 bbl Produced Water Storage Tank (T01 (4E))
- Produced Water Truck Load-Out (TLO (5E))
- Start-Up, Shut-Down, and Maintenance (Includes Blowdown) (SSM (6E))
- Process Piping and Equipment Fugitive Emissions (FUG(7E))
- o Compressor Rod Packing and Engine Crankcase Leaks Emissions (RPC (8E)
- Facility-Wide Total Emissions (Including Fugitives)
- Table 2 Release Parameter Data

Application for 45CSR13 NSR Modification Permit

#### Attachment J

#### **EMISSION POINTS DATA SUMMARY SHEET**

### **CAT G3306TA Compressor Engine**

						٦	able 1: Emis	sions Data							
Emission Point ID No. (Must match Emission Units Table &	Emission Point Type <sup>1</sup>	Through (Must match E		(Must match E	Control Device Emission Units Plat Plan)	(Chemical Processes Only)		All Regulated Pollutants - Chemical Name/CAS <sup>3</sup> (Speciate VOC	Maximum Uncontrolled	n Potential d Emissions <sup>4</sup>	Maximum Controlled	n Potential Emissions <sup>5</sup>	Emission Form or Phase (At exit conditions. (Solid,	Est. Method Used <sup>6</sup>	Emissions Concen- tration <sup>7</sup> (ppmv or
Plat Plan)		ID No.	Source	ID No.	Device Type	Short Term <sup>2</sup>	Max (hr/yr)	and HAPS)	lb/hr	ton/yr	lb/hr	ton/yr	Liquid or Gas/Vapor)		mg/m3)
								NOx	7.42	32.48	0.89	3.90	Gas	O-Vendor	
								CO	7.42	32.48	1.78	7.80	Gas	O-Vendor	
			p CAT G33061					VOC	0.37	0.73	0.17	0.73	Gas	O-Vendor	
		•	Compressor E		R			SOx	2.4E-03	4.7E-03	1.1E-03	4.7E-03	Gas	O-AP-42	
	(CE-01 (1E))							PM10/2.5	0.08	0.15	0.04	0.15	Solid/Gas	O-AP-42	
								Benzene	0.01	0.01	2.9E-03	0.01	Gas	O-AP-42	
								Ethylbenzene	1.0E-04	2.0E-04	4.5E-05	2.0E-04	Gas	O-AP-42	
			CAT					HCHO (HAP)	0.25	0.49	0.11	0.49	Gas	O-Vendor	
	Upward		CAT G3306TA					n-Hexane					Gas	O-AP-42	
CE-01	Vertical Stack	1E	Compressor	01-NSCR	NSCR	С	8,760	Methanol	0.01	0.02	0.01	0.02	Gas	O-AP-42	
	Stack		Engine					Toluene	2.3E-03	4.5E-03	1.0E-03	4.5E-03	Gas	O-AP-42	
								2,2,4-TMP					Gas	O-AP-42	
								Xylenes	8.0E-04	1.6E-03	3.6E-04	1.6E-03	Gas	O-AP-42	
								Other HAP	0.03	0.05	0.01	0.05	Gas	O-AP-42	
								Total HAP	0.30	0.58	0.13	0.58	Gas	O-AP-42	
								CO2	229	1,002	229	1,002	Gas	O-Vendor	
								CH4	0.5	2	0.5	2	Gas	O-Vendor	
								N2O	4.0E-04	1.8E-03	4.0E-04	1.8E-03	Gas	O-EPA	
								CO2e	240	1,052	240	1,052	Gas	O-EPA	

- 1 Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.
- 2 Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (i.e.,., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).
- 3 List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS2, VOCs, H2S, Inorganics, Lead, Organics, O3, NO, NO2, SO2, SO3, all applicable Greenhouse Gases (including CO2 and methane), etc. DO NOT LIST H2, H2O, N2, O2, and Noble Gases.
- 4 Give maximum potential emission rate with no control equipment operating.

  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 5 Give maximum potential emission rate with proposed control equipment operating.

  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 6 Indicate method used to determine emission rate as follows:
  MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).
- 7 Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmvd).

  If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m3) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO2, use units of ppmvd (See 45CSR10).

Application for 45CSR13 NSR Modification Permit

#### Attachment J

#### **EMISSION POINTS DATA SUMMARY SHEET**

### **TEG Dehydrator - Reboiler**

						٦	able 1: Emis	sions Data							
Emission Point ID No. (Must match Emission Units Table &	Emission Point Type <sup>1</sup>	Through (Must match E		(Must match E	Control Device Emission Units Plat Plan)	(Chemical Processes Only)		All Regulated Pollutants - Chemical Name/CAS <sup>3</sup> (Speciate VOC		n Potential d Emissions <sup>4</sup>	Maximum Controlled	n Potential Emissions <sup>5</sup>	Emission Form or Phase (At exit conditions. (Solid,	Est. Method Used <sup>6</sup>	Emissions Concen- tration <sup>7</sup> (ppmv or
Plat Plan)		ID No.	Source	ID No.	Device Type	Short Term <sup>2</sup>	Max (hr/yr)	and HAPS)	lb/hr	ton/yr	lb/hr	ton/yr	Liquid or Gas/Vapor)		mg/m3)
								NOx	0.01	0.06	0.01	0.06	Gas	O-AP-42	
								CO	0.01	0.05	0.01	0.05	Gas	O-AP-42	
		0.	14 MMBtu/hr	TEG Dehydrat	or			VOC	7.5E-04	3.3E-03	7.5E-04	3.3E-03	Gas	O-AP-42	
				oiler				SOx	8.2E-05	3.6E-04	8.2E-05	3.6E-04	Gas	O-AP-42	
			(RBV-	1 (2E))				PM10/2.5	1.0E-03	4.6E-03	1.0E-03	4.6E-03	Solid/Gas	O-AP-42	
								Benzene	2.9E-07	1.3E-06	2.9E-07	1.3E-06	Gas	O-AP-42	
			1					Ethylbenzene					Gas	O-AP-42	
								HCHO (HAP)	1.0E-05	4.5E-05	1.0E-05	4.5E-05	Gas	O-AP-42	
	Upward		TEG					n-Hexane	2.5E-04	1.1E-03	2.5E-04	1.1E-03	Gas	O-AP-42	
RBV-1	Vertical	2E	Dehydrator -	na	na	С	8,760	Methanol					Gas	O-AP-42	
	Stack		Reboiler					Toluene	4.7E-07	2.0E-06	4.7E-07	2.0E-06	Gas	O-AP-42	
								2,2,4-TMP					Gas	O-AP-42	
								Xylenes					Gas	O-AP-42	
								Other HAP	2.6E-07	1.1E-06	2.6E-07	1.1E-06	Gas	O-AP-42	
								Total HAP	2.6E-04	1.1E-03	2.6E-04	1.1E-03	Gas	O-AP-42	
								CO2	16	72	16	72	Gas	O-AP-42	
								CH4	3.1E-04	1.4E-03	3.1E-04	1.4E-03	Gas	O-AP-42	
								N2O	3.1E-05	1.4E-04	3.1E-05	1.4E-04	Gas	O-EPA	
								CO2e	16	72	16	72	Gas	O-EPA	

- 1 Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.
- 2 Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (i.e.,., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).
- 3 List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS2, VOCs, H2S, Inorganics, Lead, Organics, O3, NO, NO2, SO2, SO3, all applicable Greenhouse Gases (including CO2 and methane), etc. DO NOT LIST H2, H2O, N2, O2, and Noble Gases.
- 4 Give maximum potential emission rate with no control equipment operating.
  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 5 Give maximum potential emission rate with proposed control equipment operating.

  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 6 Indicate method used to determine emission rate as follows:
  MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).
- 7 Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmvd).

  If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m3) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO2, use units of ppmvd (See 45CSR10).

Application for 45CSR13 NSR Modification Permit

#### Attachment J

#### **EMISSION POINTS DATA SUMMARY SHEET**

### **TEG Dehydrator - Flash Tank and Still Vent**

						٦	Table 1: Emis	sions Data							
Emission Point ID No. (Must match Emission Units Table &	Emission Point Type <sup>1</sup>	Through (Must match E	Unit Vented This Point Emission Units Plat Plan)	,		Unit (Chemical Processes Only)		All Regulated Pollutants - Chemical Name/CAS <sup>3</sup> (Speciate VOC	Maximum Uncontrolled	n Potential d Emissions <sup>4</sup>		n Potential Emissions <sup>5</sup>	Emission Form or Phase (At exit conditions. (Solid,	Est. Method Used <sup>6</sup>	Emissions Concen- tration <sup>7</sup> (ppmv or
Plat Plan)		ID No.	Source	ID No.	Device Type	Short Term <sup>2</sup>	Max (hr/yr)	and HAPS) lb/hr		ton/yr	lb/hr ton/yr		Liquid or Gas/Vapor)		mg/m3)
								NOx					Gas		
								CO					Gas		
			2.0 MMscfd TE	•	•			VOC	5.15	22.55	5.15	22.55	Gas	O-GLYCalc	
				and Still Vent				SOx					Gas		
			(RSV-	1 (3E))				PM10/2.5					Solid/Gas		
								Benzene	0.10	0.44	0.10	0.44	Gas	O-GLYCalc	
								Ethylbenzene	0.05	0.20	0.05	0.20	Gas	O-GLYCalc	
								HCHO (HAP)					Gas	O-GLYCalc	
	Upward		TEG Dehydrator -					n-Hexane	0.14	0.61	0.14	0.61	Gas	O-GLYCalc	
RSV-1	Vertical Stack	3E	Flash Tank and	na	na	С	8,760	Methanol					Gas		
	Stack		Still Vent					Toluene	0.19	0.82	0.19	0.82	Gas	O-GLYCalc	
								2,2,4-TMP	0.00	0.02	0.00	0.02	Gas	O-GLYCalc	
								Xylenes	0.06	0.26	0.06	0.26	Gas	O-GLYCalc	
								Other HAP					Gas		
								Total HAP	0.54	2.34	0.54	2.34	Gas	O-GLYCalc	
								CO2					Gas		
								CH4	6	28	6.39	28	Gas	O-GLYCalc	
								N2O					Gas		
								CO2e	160	700	160	700	Gas	O-EPA	

- 1 Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.
- 2 Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (i.e.,., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).
- 3 List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS2, VOCs, H2S, Inorganics, Lead, Organics, O3, NO, NO2, SO2, SO3, all applicable Greenhouse Gases (including CO2 and methane), etc. DO NOT LIST H2, H2O, N2, O2, and Noble Gases.
- 4 Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 5 Give maximum potential emission rate with proposed control equipment operating.

  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 6 Indicate method used to determine emission rate as follows:
  MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).
- 7 Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmvd).

  If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m3) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO2, use units of ppmvd (See 45CSR10).

Application for 45CSR13 NSR Modification Permit

#### Attachment J

#### **EMISSION POINTS DATA SUMMARY SHEET**

### **Produced Water - Storage Tank**

						٦	able 1: Emis	sions Data							
Emission Point ID No. (Must match Emission Units Table &	Emission Point Type <sup>1</sup>	Through (Must match E		(Must match E	Control Device Emission Units Plat Plan)		nit	All Regulated Pollutants - Chemical Name/CAS <sup>3</sup> (Speciate VOC	Maximum Uncontrolled	n Potential d Emissions <sup>4</sup>		n Potential Emissions <sup>5</sup>	Emission Form or Phase (At exit conditions. (Solid,	Est. Method Used <sup>6</sup>	Emissions Concen- tration <sup>7</sup> (ppmv or
Plat Plan)		ID No.	Source	ID No.	Device Type	Short Term <sup>2</sup>	Max (hr/yr)	and HAPS)	lb/hr	ton/yr	lb/hr	ton/yr	Liquid or Gas/Vapor)		mg/m3)
								NOx					Gas		
								CO					Gas		
		Produ	iced Water - 2	10 bbl Storage	Tank			VOC	0.05	0.22	0.05	0.22	Gas	EE	
		Fiout		(4E))	FIGIIK			SOx					Gas		
			(	(//				PM10/2.5					Solid/Gas		
								Benzene	0.00	0.01	0.00	0.01	Gas	EE	
								Ethylbenzene	0.00	0.01	0.00	0.01	Gas	EE	
								HCHO (HAP)					Gas		
	Upward		Produced					n-Hexane	0.00	0.01	0.00	0.01	Gas	EE	
T01	Vertical Stack	4E	Water Storage Tank	na	na	С	8,760	Methanol					Gas		
	Stack		Tarik					Toluene	0.00	0.01	0.00	0.01	Gas	EE	
								2,2,4-TMP	0.00	0.01	0.00	0.01	Gas	EE	
								Xylenes	0.00	0.01	0.00	0.01	Gas	EE	
								Other HAP					Gas		
								Total HAP	0.01	0.03	0.01	0.03	Gas	EE	
								CO2					Gas		
								CH4	0.20	0.89	0.20	0.89	Gas	EE	
								N2O					Gas		
								CO2e	5.08	22.25	5.08	22.25	Gas	EE	

- 1 Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.
- 2 Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (i.e.,., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).
- 3 List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS2, VOCs, H2S, Inorganics, Lead, Organics, O3, NO, NO2, SO2, SO3, all applicable Greenhouse Gases (including CO2 and methane), etc. DO NOT LIST H2, H2O, N2, O2, and Noble Gases.
- 4 Give maximum potential emission rate with no control equipment operating.
  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 5 Give maximum potential emission rate with proposed control equipment operating.

  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 6 Indicate method used to determine emission rate as follows:
  MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).
- 7 Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmvd).

  If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m3) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO2, use units of ppmvd (See 45CSR10).

Application for 45CSR13 NSR Modification Permit

#### Attachment J

#### **EMISSION POINTS DATA SUMMARY SHEET**

#### **Produced Water - Truck Load-Out**

						7	able 1: Emis	sions Data							
Emission Point ID No. (Must match Emission Units Table &	Emission Point Type <sup>1</sup>	Through (Must match E		(Must match E	Emission Units	(Chemical Processes Only)		All Regulated Pollutants - Chemical Name/CAS <sup>3</sup> (Speciate VOC	Maximum Uncontrolled	n Potential d Emissions <sup>4</sup>		n Potential Emissions <sup>5</sup>	Emission Form or Phase (At exit conditions. (Solid,	Est. Method Used <sup>6</sup>	Emissions Concen- tration <sup>7</sup> (ppmv or
Plat Plan)		ID No.	Source	ID No.	Device Type	Short Term <sup>2</sup>	Max (hr/yr)	and HAPS)	lb/hr	ton/yr	lb/hr	ton/yr	Liquid or Gas/Vapor)		mg/m3)
								NOx					Gas		
								CO					Gas		
		Dro	oduced Water	- Truck Load-	Out			VOC		0.55		0.55	Gas	EE	
				(5E))	Out			SOx					Gas		
	(120 (32))							PM10/2.5					Solid/Gas		
							ļ	Benzene		0.01		0.01	Gas	EE	
								Ethylbenzene		0.01		0.01	Gas	EE	
								HCHO (HAP)					Gas		
			Produced					n-Hexane		0.01		0.01	Gas	EE	
TLO		5E	Water Truck Load-Out	na	na	'		Methanol					Gas		
			Load Out					Toluene		0.01		0.01	Gas	EE	
								2,2,4-TMP		0.01		0.01	Gas	EE	
								Xylenes		0.01		0.01	Gas	EE	
								Other HAP					Gas		
								Total HAP		0.08		0.08	Gas	EE	
								CO2					Gas		
								CH4					Gas		
								N2O					Gas		
								CO2e					Gas		

- 1 Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.
- 2 Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (i.e.,., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).
- 3 List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS2, VOCs, H2S, Inorganics, Lead, Organics, O3, NO, NO2, SO2, SO3, all applicable Greenhouse Gases (including CO2 and methane), etc. DO NOT LIST H2, H2O, N2, O2, and Noble Gases.
- 4 Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 5 Give maximum potential emission rate with proposed control equipment operating.
  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 6 Indicate method used to determine emission rate as follows:
  MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).
- 7 Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmvd).

  If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m3) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO2, use units of ppmvd (See 45CSR10).

Application for 45CSR13 NSR Modification Permit

#### Attachment J

#### **EMISSION POINTS DATA SUMMARY SHEET**

#### Start-Up, Shut-Down, and Maintenance (Includes Blowdown)

						٦	able 1: Emis	sions Data							
Emission Point ID No. (Must match Emission Units Table &	Emission Point Type <sup>1</sup>	Emission L Through <sup>1</sup> (Must match E Table & F	Emission Units	(Must match E	Control Device Emission Units Plat Plan)	(Chemical Processes Only)		All Regulated Pollutants - Chemical Name/CAS <sup>3</sup> (Speciate VOC		n Potential d Emissions <sup>4</sup>		n Potential Emissions <sup>5</sup>	Emission Form or Phase (At exit conditions. (Solid,	Est. Method Used <sup>6</sup>	Emissions Concen- tration <sup>7</sup> (ppmv or
Plat Plan)		ID No.	Source	ID No.	Device Type	Short Term <sup>2</sup>	Max (hr/yr)	and HAPS)	lb/hr	ton/yr	lb/hr	ton/yr	Liquid or Gas/Vapor)		mg/m3)
								NOx					Gas		
								CO					Gas		
		Start-	Up, Shut-Dow		nance			VOC		1.53		1.53	Gas	EE	
			(Includes I	,				SOx					Gas		
	(SSM (6E))							PM10/2.5					Solid/Gas		
							<u> </u>	Benzene		2.0E-03		2.0E-03	Gas	EE	
								Ethylbenzene		2.0E-03		2.0E-03	Gas	EE	
								HCHO (HAP)					Gas		
			Start-Up,					n-Hexane		0.05		0.05	Gas	EE	
SSM	na	6E	Shut-Down,	na	na	I	na	Methanol					Gas		
			Maintenance					Toluene		2.0E-03		2.0E-03	Gas	EE	
								2,2,4-TMP		2.0E-03		2.0E-03	Gas		
								Xylenes		2.0E-03		2.0E-03	Gas	EE	
								Other HAP					Gas		
								Total HAP		0.06		0.06	Gas	EE	
								CO2					Gas		
								CH4		4		4	Gas		
								N2O					Gas		
								CO2e		108		108	Gas		

- 1 Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.
- 2 Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (i.e.,., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).
- 3 List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS2, VOCs, H2S, Inorganics, Lead, Organics, O3, NO, NO2, SO2, SO3, all applicable Greenhouse Gases (including CO2 and methane), etc. DO NOT LIST H2, H2O, N2, O2, and Noble Gases.
- 4 Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 5 Give maximum potential emission rate with proposed control equipment operating.

  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 6 Indicate method used to determine emission rate as follows:
  MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).
- 7 Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmvd).

  If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m3) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO2, use units of ppmvd (See 45CSR10).

Application for 45CSR13 NSR Modification Permit

#### Attachment J

#### **EMISSION POINTS DATA SUMMARY SHEET**

### **Process Piping and Equipment Fugitive Emissions**

	Table 1: Emissions Data														
Emission Point ID No. (Must match Emission Units Table &	Emission Point Type <sup>1</sup>	Emission Unit Vented Through This Point (Must match Emission Units Table & Plat Plan)		Air Pollution Control Device (Must match Emission Units Table & Plat Plan)				Pollutants -	Maximum Potential Uncontrolled Emissions <sup>4</sup>		Maximum Potential Controlled Emissions <sup>5</sup>		Emission Form or Phase (At exit conditions. (Solid,	Est. Method Used <sup>6</sup>	Emissions Concen- tration <sup>7</sup> (ppmv or
Plat Plan)		ID No.	Source	ID No.	Device Type	Short Term <sup>2</sup>	Max (hr/yr)	and HAPS)	lb/hr	ton/yr	lb/hr	ton/yr	Liquid or Gas/Vapor)		mg/m3)
								NOx					Gas		
	Process Piping and Equipment Fugitive Emissions							CO					Gas		
								VOC	1.50	6.55	1.50	6.55	Gas	EE	
								SOx					Gas		
	(FUG(7E))							PM10/2.5					Solid/Gas		
							ļ	Benzene	0.02	0.10	0.02	0.10	Gas	EE	
	Fugitive		Process Piping and Equipment Fugitive		na	С		Ethylbenzene	0.02	0.10	0.02	0.10	Gas	EE	
								HCHO (HAP)					Gas		
		7E					C 8,760	n-Hexane	0.02	0.10	0.02	0.10	Gas	EE	
FUG								Methanol					Gas		
			Emissions					Toluene	0.02	0.10	0.02	0.10	Gas	EE	
								2,2,4-TMP	0.02	0.10	0.02	0.10	Gas		
								Xylenes	0.02	0.10	0.02	0.10	Gas	EE	
								Other HAP					Gas		
								Total HAP	0.14	0.63	0.14	0.63	Gas	EE	
								CO2	0.02	0.07	0.02	0.07	Gas		
								CH4	4	16	4	16	Gas		
								N2O					Gas		
								CO2e	91	397	91	397	Gas		

- 1 Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.
- 2 Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (i.e.,., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).
- 3 List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS2, VOCs, H2S, Inorganics, Lead, Organics, O3, NO, NO2, SO2, SO3, all applicable Greenhouse Gases (including CO2 and methane), etc. DO NOT LIST H2, H2O, N2, O2, and Noble Gases.
- 4 Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 5 Give maximum potential emission rate with proposed control equipment operating.

  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 6 Indicate method used to determine emission rate as follows:
  MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).
- 7 Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmvd).

  If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m3) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO2, use units of ppmvd (See 45CSR10).

Application for 45CSR13 NSR Modification Permit

#### Attachment J

#### **EMISSION POINTS DATA SUMMARY SHEET**

### Compressor Rod Packing and Engine Crankcase Leaks (RPC)

	Table 1: Emissions Data														
Emission Point ID No. (Must match Emission Units Table &	Emission Point Type <sup>1</sup>	Emission Unit Vented Through This Point (Must match Emission Units Table & Plat Plan)		Air Pollution Control Device (Must match Emission Units Table & Plat Plan)				Pollutants -	Maximum Potential Uncontrolled Emissions <sup>4</sup>		Maximum Potential Controlled Emissions <sup>5</sup>		Emission Form or Phase (At exit conditions. (Solid,	Est. Method Used <sup>6</sup>	Emissions Concen- tration <sup>7</sup> (ppmv or
Plat Plan)		ID No.	Source	ID No.	Device Type	Short Term <sup>2</sup>	Max (hr/yr)	and HAPS)	lb/hr	ton/yr	lb/hr	ton/yr	Liquid or Gas/Vapor)		mg/m3)
								NOx					Gas		
	Compressor Rod Packing and Engine Crankcase Leaks Emissions							CO					Gas		
								VOC	8.2E-04	3.6E-03	8.2E-04	3.6E-03	Gas	EE	
								SOx					Gas		
	(RPC (8E))							PM10/2.5					Solid/Gas		
								Benzene	1.1E-04	4.8E-04	1.1E-04	4.8E-04	Gas	EE	
	Fugitive		Compressor Rod Packing and Engine Crankcase Leaks		na	С		Ethylbenzene	1.1E-04	4.8E-04	1.1E-04	4.8E-04	Gas	EE	
							C 8,760	HCHO (HAP)	5.5E-04	2.4E-03	5.5E-04	2.4E-03	Gas		
								n-Hexane	1.1E-04	4.8E-04	1.1E-04	4.8E-04	Gas	EE	
RPC		8E		na				Methanol					Gas		
								Toluene	1.1E-04	4.8E-04	1.1E-04	4.8E-04	Gas	EE	
								2,2,4-TMP	1.1E-04	4.8E-04	1.1E-04	4.8E-04	Gas		
								Xylenes	1.1E-04	4.8E-04	1.1E-04	4.8E-04	Gas	EE	
								Other HAP					Gas		
								Total HAP	6.6E-04	2.9E-03	6.6E-04	2.9E-03	Gas	EE	
								CO2	1	5	1	5	Gas		
								CH4	3	13	3	13	Gas		
								N2O					Gas		
								CO2e	74	325	74	325	Gas		

- 1 Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.
- 2 Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (i.e.,., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).
- 3 List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS2, VOCs, H2S, Inorganics, Lead, Organics, O3, NO, NO2, SO2, SO3, all applicable Greenhouse Gases (including CO2 and methane), etc. DO NOT LIST H2, H2O, N2, O2, and Noble Gases.
- 4 Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 5 Give maximum potential emission rate with proposed control equipment operating.

  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 6 Indicate method used to determine emission rate as follows:
  MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).
- 7 Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmvd).

  If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m3) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO2, use units of ppmvd (See 45CSR10).

Application for 45CSR13 NSR Modification Permit

#### Attachment J

#### **EMISSION POINTS DATA SUMMARY SHEET**

### **Facility-Wide Total Emissions**

	Table 1: Emissions Data														
Emission Point ID No. (Must match Emission Units Table &	Emission Point Type <sup>1</sup>	Emission Unit Vented Through This Point (Must match Emission Units Table & Plat Plan)		Air Pollution Control Device (Must match Emission Units Table & Plat Plan)				Pollutants -	Maximum Potential Uncontrolled Emissions <sup>4</sup>		Maximum Potential Controlled Emissions <sup>5</sup>		Emission Form or Phase (At exit conditions. (Solid,	Est. Method Used <sup>6</sup>	Emissions Concen- tration <sup>7</sup> (ppmv or
Plat Plan)		ID No.	Source	ID No.	Device Type	Short Term <sup>2</sup>	Max (hr/yr)	and HAPS)	lb/hr	ton/yr	lb/hr	ton/yr	Liquid or Gas/Vapor)		mg/m3)
								NOx	7.43	32.54	0.90	3.96	Gas		
								CO	7.43	32.53	1.79	7.85	Gas		
		Facility-Wide						VOC	7.07	32.13	6.86	32.13	Gas		
	Total Emissions (Includes Fugitives)					SOx	2.5E-03	0.01	1.2E-03	0.01	Gas				
						PM10/2.5	0.08	0.16	0.04	0.16	Solid/Gas				
						Benzene	0.13	0.57	0.13	0.57	Gas				
								Ethylbenzene	0.07	0.33	0.07	0.33	Gas		
								HCHO (HAP)	0.25	0.49	0.11	0.49	Gas		
								n-Hexane	0.16	0.79	0.16	0.79	Gas		
								Methanol	0.01	0.02	0.01	0.02	Gas		
								Toluene	0.21	0.95	0.21	0.95	Gas		
								2,2,4-TMP	0.03	0.14	0.03	0.14	Gas		
								Xylenes	0.08	0.39	0.08	0.39	Gas		
								Other HAP	0.03	0.05	0.01	0.05	Gas		
								Total HAP	0.98	3.74	0.82	3.74	Gas		
								CO2	246	1,079	246	1,079	Gas		
								CH4	14	64	14	64	Gas		
								N2O	4.3E-04	1.9E-03	4.3E-04	1.9E-03	Gas		
								CO2e	586	2,675	586	2,675	Gas		

- 1 Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.
- 2 Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (i.e.,., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).
- 3 List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS2, VOCs, H2S, Inorganics, Lead, Organics, O3, NO, NO2, SO2, SO3, all applicable Greenhouse Gases (including CO2 and methane), etc. DO NOT LIST H2, H2O, N2, O2, and Noble Gases.
- 4 Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 5 Give maximum potential emission rate with proposed control equipment operating.

  If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- 6 Indicate method used to determine emission rate as follows:
  MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).
- 7 Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmvd).

  If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m3) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO2, use units of ppmvd (See 45CSR10).

### Williams Ohio Valley Midstream LLC (OVM)

## YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### Attachment J

### **EMISSION POINTS DATA SUMMARY SHEET**

Table 2: Release Parameter Data									
Emission Point ID No.	Inner		Exit Gas		Emission Po	oint Elevation (ft)	UTM Coordinates (km)		
(Must match Emission Units Table)	Diameter (ft)	Temperature (oF)	Volumateric Flow <sup>1</sup> (acfm) (At operating conditions)	Velocity (fps)	Ground Level (Height above mean sea level)	Stack Height <sup>2</sup> (Release height above ground level)	Northing	Easting	
CE-01 (1E)	0.5 ft	1,064 oF	970 acfm	na	860 ft	8 ft	4,383.35 km N	514.75 km E	
RBV-1 (2E)	0.6 ft	na	na	na	860 ft	8 ft	4,383.35 km N	514.75 km E	
RSV-1 (3E)	0.5 ft	212 oF	na	na	860 ft	8 ft	4,383.35 km N	514.75 km E	
T01 (4E)	na	Ambient	na	na	860 ft	15 ft	4,383.35 km N	514.75 km E	
TLO (5E)	na	Ambient	na	na	860 ft	8 ft	4,383.35 km N	514.75 km E	
SSM (6E)	na	70 oF	na	na	860 ft	na	4,383.35 km N	514.75 km E	
FUG (7E)	na	70 oF	na	na	860 ft	na	4,383.35 km N	514.75 km E	
RPC (8E)	na	Varies	na	na	860 ft	na	4,383.35 km N	514.75 km E	

<sup>1</sup> Give at operating conditions. Include inerts.

<sup>2</sup> Release height of emissions above ground level.

## **ATTACHMENT K**

## **Fugitive Emissions Data Summary Sheet**

"27. Fill out the **Fugitive Emissions Data Summary Sheet** and provide it as Attachment K."

- Application Forms Checklist
- Fugitive Emissions Summary
- Leak Source Data Sheet

## Williams Ohio Valley Midstream LLC (OVM)

## YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

### Attachment K

## **FUGITIVE EMISSIONS DATA SUMMARY SHEET**

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not considered to be fugitive, and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET.

Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

		APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS
1.)	Will there be	haul road activities?
	□ Yes	☑ No
	☐ If Yes, the	n complete the HAUL ROAD EMISSIONS UNIT DATA SHEET.
2.)	Will there be	Storage Piles?
	□ Yes	☑ No
	☐ If Yes, the	n complete Table 1 of the NONMETALLIC MINERALS PROCESSING EMISSIONS UNIT DATA SHEET.
3.)	Will there be	Liquid Loading/Unloading Operations?
	□ Yes	☑ No (( Truck Load-Out (TLO (5E)) is include in the Point Source Emissions ))
	☐ If Yes, th	nen complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET.
4.)	Will there be	emissions of air pollutants from Wastewater Treatment Evaporation?
	□ Yes	☑ No
	☐ If Yes, the	n complete the GENERAL EMISSIONS UNIT DATA SHEET.
		Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, open-ended valves, ctions, flanges, agitators, cooling towers, etc.)?
	☑ Yes	□ No
	☑ If Yes, the DATA SHI	en complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS EET.
6.)	Will there be	General Clean-up VOC Operations?
	□ Yes	☑ No
	☐ If Yes, the	n complete the GENERAL EMISSIONS UNIT DATA SHEET.
7.)	Will there be	any other activities that generate fugitive emissions?
	□ Yes	☑ No
	☐ If Yes, the	n complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form.
	If you answe	red "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions Summary."

# YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### Attachment K

# **FUGITIVE EMISSIONS DATA SUMMARY SHEET - Continued**

FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants Chemical Name/CAS <sup>1</sup>	Maximum Potential Pre-Controlled Emissions <sup>2</sup>		Maximum Potential Controlled Emissions <sup>3</sup>		Est. Method Used <sup>4</sup>	
	Name/CAS	lb/hr	ton/yr	lb/hr	ton/yr	Useu	
Paved Haul Roads	na						
Unpaved Haul Roads	na						
Storage Pile Emissions	na						
Loading/Unloading Operations	(( Truck Load-Out (TLO (5E)) is include in the Point Source Emissions ))						
Wastewater Treatment	na						
	VOC	1.50	6.55	1.50	6.55	O - AP-42	
	Benzene	0.02	0.02	0.02	0.02	O - AP-42	
	Ethylbenzene	0.02	0.02	0.02	0.02	O - AP-42	
	Formaldehyde						
	n-Hexane	0.02	0.02	0.02	0.02	O - AP-42	
	Methanol						
Process and Piping Fugitives	Toluene	0.02	0.02	0.02	0.02	O - AP-42	
(FUG-G (7E) and FUG-W (7E)	2,2,4-TMP	0.02	0.02	0.02	0.02	O - AP-42	
(Total Combined)	Xylenes	0.02	0.02	0.02	0.02	O - AP-42	
	Other HAP						
	Total HAP	0.14	0.63	0.14	0.63	O - AP-42	
	CO2	0.02	0.1	0.02	0.1	O - AP-42	
	CH4	4	16	4	16	O - AP-42	
	N2O						
	CO2e	91	397	91	397	O - GWP	
General Clean-up VOC Emissions	na						
Other	na						

<sup>&</sup>lt;sup>1</sup> List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS<sub>2</sub>, VOCs, H<sub>2</sub>S, Inorganics, Lead, Organics, O<sub>3</sub>, NO, NO<sub>2</sub>, SO<sub>2</sub>, SO<sub>3</sub>, all applicable Greenhouse Gases, etc. DO NOT LIST H<sub>2</sub>, H<sub>2</sub>O, N<sub>2</sub>, O<sub>2</sub>, and Noble Gases.

<sup>&</sup>lt;sup>2</sup> Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in min (e.g. 5 lb VOC/20 min batch).

<sup>&</sup>lt;sup>3</sup> Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in min (e.g. 5 lb VOC/20 min batch).

<sup>&</sup>lt;sup>4</sup> Indicate method used to determine emission rate as follows:

MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

# YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

# Attachment K

# **FUGITIVE EMISSIONS DATA SUMMARY SHEET - Continued**

		LEAK SOURC	E DATA SHEET					
Soure Category	Pollutant	Number of Source Components <sup>1</sup>	Number of Components Monitored by Frequency <sup>2</sup>	Average Time to Repair (Days) <sup>3</sup>	Estimated Annual Emission Rate (lb/yr)			
Pumps <sup>5</sup>	Light Liquid VOC <sup>6,7</sup>							
	Heavy Liquid VOC8							
	Non-VOC <sup>9</sup>							
Valves <sup>10</sup>	Gas VOC							
	Light Liquid VOC	***	* NOT APPLICABLE ***					
	Heavy Liquid VOC							
	Non-VOC	TAC	CILIY IS NOT SUBJECT TO					
Safety Relief Valves <sup>11</sup>	Gas VOC							
	Light Liquid VOC	LEAK DETECT	LEAK DETECTION AND REPAIR REQUIREMENTS					
	Non-VOC	<del>                                     </del>						
Open Ended Lines <sup>12</sup>	Gas VOC							
	Light Liquid VOC							
	Non-VOC							
Sampling Connections <sup>13</sup>	Gas VOC							
	Light Liquid VOC							
	Non-VOC							
Compressors	Gas VOC							
	Non-VOC							
Flanges	Gas VOC							
	Light Liquid VOC							
	Non-VOC							
Other (Connectors)	Gas VOC							
	Light Liquid VOC							
	Non-VOC							
	•	•		TOTAL (lb/yr)	0			
				TOTAL (tpy)	0.00			

#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

# Attachment K FUGITIVE EMISSIONS DATA SUMMARY SHEET - Continued

#### **Notes for Leak Source Data Sheet**

- 1. For VOC sources include components on streams and equipment that contain greater than 10% VOC, including feed streams, reaction/separation facilities, and product/by-product delivery lines. Do not include certain leakless equipment as defined below by category.
- 2. By monitoring frequency, give the number of sources routinely monitored for leaks, using a portable detection device that measures concentration in visual or soap-bubble leak detection ppm. Do not include monitoring by methods. "M/Q(M)/Q/SA/A/0" means the time period between inspections as follows:

  Monthly/Quarterly, with Monthly follow-up of repaired leakers/Quarterly/Semi-annual/Annually/other (specify time period)

If source category is not monitored, a single zero in the space will suffice. For example, if 50 gas-service valves are monitored quarterly, with monthly follow-up of those repaired, 75 are monitored semi-annually, and 50 are checked bimonthly (alternate months), with non checked at any other frequency, you would put in the category valves, gas service: 0/50/0/75/0/50 (bimonthly).

- 3. Give the average number of days, after a leak is discovered, that an attempt will be made to repair the leak.
- 4. Note the method used: MB material balance; EE engineering estimate; EPA emission factors established by EPA (cite document used); 0 other method, such as in-house emission factor (specify).
- 5. Do not include in the equipment count seal-less pumps (canned motor or diaphragm) or those with enclosed venting to a control device. (Emissions from vented equipment should be included in the estimates given in the Emission Points Data Sheet.)
- 6. Volatile organic compounds (VOC) means the term as defined in 40 CFR. 51.100 (s).
- 7. A light liquid is defined as a fluid with vapor pressure equal to or greater than 0.04 psi (0.3 Kpa) at 20°C. For mixtures, if 20% w/w or more of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20°C, then the fluid is defined as a light liquid.
- 8. A heavy liquid is defined as a fluid with a vapor pressure less than 0.04 psi (0.3 Kpa) at 20°c. For mixtures, if less than 20% w/w of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20°C. then the fluid is defined as a heavy liquid.
- 9. LIST CO, H2S, mineral acids, NO, NO, SO, etc. DO NOT LIST CO, H, H20, N, O, and Noble Gases.
- 10. Include all process valves whether in-line or on an open-ended line such as sample, drain and purge valves. Do not include safety-relief valves, or leakless valves such as check, diaphragm, and bellows seal valves.
- 11. Do not include a safety-relief valve if there is a rupture disk in place upstream of the valve, or ifthe valve vents to a control device.
- 12. Open-ended lines include purge, drain and vent lines. Do not include sampling connections, or lines sealed by plugs, caps, blinds or second valves.
- 13. Do not include closed-purge sampling connections.

# ATTACHMENT L

# **Emissions Unit Data Sheet(s)**

"28. Fill out the Emissions Unit Data Sheet(s) as Attachment L."

- Natural Gas Compressor/Generator Engine Data Sheet
  - 203 bhp Caterpillar G3306TA Compressor Engine Vendor Data
- Natural Gas Glycol Dehydration Unit Data Sheet
  - OGlycol Dehydration Unit 2.0 MMscfd w/ 0.14 MMBtu/hr Reboiler Vendor Data
- 40 CFR Part 63; Subpart HH & HHH Registration Form
- Storage Tank Data Sheet
- Bulk Liquid Transfer Operations

# YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

# Attachment L

# NATURAL GAS COMPRESSOR/GENERATOR ENGINE DATA SHEET

Source Ident	ification Number <sup>1</sup>	CE-01 (1E)					
Engine Manuf	acturer and Model	Caterpillar (CAT)					
N	Model	G3306TALE (4SRB)					
Manufacture	's Rated bhp/rpm	203	1,800				
Sourc	ce Status <sup>2</sup>	E	S				
Date Installed/	Modified/Removed <sup>3</sup>	01/1	6/13				
Manufactured/R	Reconstruction Date <sup>4</sup>	07/0	3/08				
Certified Engine (4	40CFR60 NSPS JJJJ) <sup>5</sup>	2	10				
	Engine Type <sup>6</sup>	RE	348				
	APCD Type <sup>7</sup>	A/F and	d NSCR				
	Fuel Type <sup>8</sup>	P	Q				
Engine Fuel and	H <sub>2</sub> S (gr/100 scf)	0	.2				
Engine, Fuel and Combustion Data	Operating bhp/rpm	203	1,800				
30	BSFC (Btu/bhp-hr)	8,9	978				
	Fuel (ft <sup>3</sup> /hr)	1,7	787				
	Fuel (MMft <sup>3</sup> /yr)	15.7					
	Operation (hrs/yr)	8,760					
Reference <sup>9</sup>	PTE <sup>10</sup>	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	NOX	0.89	3.90				
MD	СО	1.78	7.80				
MD	VOC w/o HCHO	0.05	0.24				
MD	VOC w/ HCHO	0.17	0.73				
AP	SOX	1.1E-03	4.7E-03				
AP	PM10/2.5	0.04	0.15				
AP	Benzene	2.9E-03	0.01				
AP	Ethylbenzene	4.5E-05	2.0E-04				
MD	Formaldehyde (HCHO)	0.11	0.49				
AP	n-Hexane						
AP	Methanol	5.6E-03	0.02				
AP	Toluene	1.0E-03	4.5E-03				
AP	2,2,4-TMP						
AP	Xylenes	3.6E-04	1.6E-03				
AP	Other HAP	0.01	0.05				
SUM	Total HAP	0.13	0.58				
40CFR98	CO2	229	1,002				
MD	CH4	0.5	2				
40CFR98	N2O	4.0E-04	1.8E-03				
40CFR98	CO2e	240	1,052				

#### Notes to NATURAL GAS COMPRESSOR/GENERATOR ENGINE DATA SHEET

- 1. Enter the appropriate Source Identification Number for each natural gas-fueled reciprocating internal combustion compressor/generator engine located at the compressor station. Multiple compressor engines should be designated CE-1, CE-2, CE-3 etc. Generator engines should be designated GE-1, GE-2, GE-3 etc. If more than three (3) engines exist, please use additional sheets.
- 2. Enter the Source Status using the following codes:

NS = Construction of New Source (installation)

ES = Existing Source

MS = Modification of Existing Source

RS = Removal of Source

- 3. Enter the date (or anticipated date) of the engine's installation (construction of source), modification or removal.
- 4. Enter the date that the engine was manufactured, modified or reconstructed.
- 5. Is the engine a certified stationary spark ignition internal combustion engine according to 40CFR60 Subpart JJJJ. If so, the engine and control device must be operated and maintained in accordance with the manufacturer's emission-related written instructions. You must keep records of conducted maintenance to demonstrate compliance, but no performance testing is required. If the certified engine is not operated and maintained in accordance with the manufacturer's emission-related written instructions, the engine will be considered a non-certified engine and you must demonstrate compliance according to 40CFR§60.4243a(2)(i) through (iii), as appropriate.

#### Provide a manufacturer's data sheet for all engines being registered.

6. Enter the Engine Type designation(s) using the following codes:

LB2S = Lean Burn Two Stroke

RB4S = Rich Burn Four Stroke

LB4S = Lean Burn Four Stroke

7. Enter the Air Pollution Control Device (APCD) type designation(s) using the following codes:

A/F = Air/Fuel Ratio

IR = Ignition Retard

HEIS = High Energy Ignition System

SIPC = Screw-in Precombustion Chambers

PSC = Prestratified Charge

LEC = Low Emission Combustion

NSCR = Non-Selective Catalytic Reduction

SCR = Lean Burn & Selective Catalytic Reduction

8. Enter the Fuel Type using the following codes:

PQ = Pipeline Quality Natural Gas

RG = Raw Natural Gas

9. Enter the Potential Emissions Data Reference designation using the following codes. Attach all referenced data to this Compressor/Generator Data Sheet(s).

MD = Manufacturer's Data	
AP = AP-42	
GR = GRI-HAPCalcTM	
OT - Other (please list)	

10. Enter each engine's Potential to Emit (PTE) for the listed regulated pollutants in pounds per hour and tons per year. PTE shall be calculated at manufacturer's rated brake horsepower and may reflect reduction efficiencies of listed Air Pollution Control Devices. Emergency generator engines may use 500 hours of operation when calculating PTE. PTE data from this data sheet shall be incorporated in the Emissions Summary Sheet.

From: Chris Magee [mailto:CMagee@usacompression.com]

Sent: Tuesday, September 03, 2013 9:30 AM

**To:** Turchin, John; Thompson, Bill **Subject:** RE: Yoho Cat 3306

Importance: High

Bill/John,

Below is the information for the Yoho unit (USAC #2062). If there is anything else let me know.

Information needed if the unit was operated for another company other than Williams is when was it operated –

Company: Crimson Exploration

Location: Liberty Co., TX

Start date(s): 6/22/2009

Duration or time of operation(s) and

• end date: 4/20/2011.

Chris Magee
Emissions Compliance, N.E. Region
USA Compression
21722 Route 6, LL East
Warren, PA 16365
814-746-6942- mobile
814-723-2431 - fax
cmagee@usacompression.com



The gas compressor was operated at another location prior to 08/23/11 and as provided in the NSPS General Provisions at 40 CFR 60.14(e)(6), relocation of an existing facility is not a modification.



	USA Com	pression Unit 2062 Cat	erpillar G3306T	A Engine Emissions	
Date of Manufacture	July 3, 2008	Engine Serial Number	G6X04853	Date Modified/Reconstructed	N/A
Driver Rated HP	203	Rated Speed in RPM	1800	Combustion Type	Spark Ignited 4 Stroke
Number of Cylinders	6	<b>Compression Ratio</b>	10.5:1	Combustion Setting	Rich Burn
Displacement, in <sup>3</sup>	640	Fuel Delivery Method	Carburetor	Combustion Air Treatment	T.C/ Aftercooled

# Raw Engine Emissions (905 LHV BTU/SCF Fuel Gas with little to no H2S)

Fuel Consumption 8098 LHV BTU/bhp-hr or 8908 HHV BTU/bhp-hr

Altitude 1500 ft Maximum Air Inlet Temp 77 F

	g/bhp-hr <sup>1</sup>	lb/MMBTU <sup>2</sup>	lb/hr	TPY
Nitrogen Oxides (NOx)	16.57		7.416	32.480
Carbon Monoxide (CO)	16.57		7.416	32.480
Volatile Organic Compounds (VOC or NMNEHC excluding CH2O)	0.37		0.166	0.725
Formaldehyde (CH2O)	0.25		0.112	0.490
Particulate Matter (PM) Filterable+Condensable		1.94E-02	0.035	0.154
Sulfur Dioxide (SO2)		5.88E-04	0.001	0.005
	g/bhp-hr <sup>1</sup>	lb/MMBTU <sup>2</sup>	lb/hr	Metric Tonne/yr
Carbon Dioxide (CO2)	511	110.0	199	790
Methane (CH4)	1.02	0.23	0.416	1.652

<sup>&</sup>lt;sup>1</sup> g/bhp-hr are based on Caterpillar Specifications. Note that g/bhp-hr values are based on 100% Load Operation. It is recommended to add a safety margin to emissions to allow for operational flexibility and fuel gas composition variability.

#### **Catalytic Converter Emissions**

Catalytic Converter Make amd Model: Maxim, EAC4-290-5

Element Type: 3-Way
Number of Elements in Housing: 1

Air/Fuel Ratio Control Compliance Controls, AFR-9

	% Reduction	lb/hr	TPY
Nitrogen Oxides (NOx)	88 or 2 g/bhp-hr	0.89	3.90
Carbon Monoxide (CO)	76.0 or 4 g/bhp-hr	1.78	7.80
Volatile Organic Compounds (VOC or NMNEHC)	0 or 1 g/bhp-hr	0.17	0.73
Formaldehyde (CH2O)	0	0.11	0.49
Particulate Matter (PM)	0	3.51E-02	1.54E-01
Sulfur Dioxide (SO2)	0	1.06E-03	4.66E-03
	% Reduction	lb/hr	Metric Tonne/yr
Carbon Dioxide (CO2)	0	199	790
Methane (CH4)	0	0.42	1.65

<sup>&</sup>lt;sup>2</sup> Emission Factor obtained from EPA's AP-42, Fifth Edition, Volume I, Chapter 3: Stationary Internal Combution Sources (Section 3.2 Natural Gas-Fired Reciprocating Engines, Table 3.2-3).

# GAS ENGINE SITE SPECIFIC TECHNICAL DATA Williams OVM Yoho



GAS COMPRESSION APPLICATION

FUEL SYSTEM: ENGINE SPEED (rpm): 1800 **HPG IMPCO** 8:1 SCAC COMPRESSION RATIO: WITH CUSTOMER SUPPLIED AIR FUEL RATIO CONTROL AFTERCOOLER TYPE: SITE CONDITIONS:

AFTERCOOLER WATER INLET (°F): 130 FUEL: Nat Gas FUEL PRESSURE RANGE(psig): FUEL METHANE NUMBER: JACKET WATER OUTLET (°F): 210 12.0-24.9 ASPIRATION: 84.8 TA JW+OC, AC COOLING SYSTEM: FUEL LHV (Btu/scf): 905 ALTITUDE(ft): IGNITION SYSTEM: MAG 1500 EXHAUST MANIFOLD: WC 77

MAXIMUM INLET AIR TEMPERATURE(°F): STANDARD RATED POWER: 203 bhp@1800rpm COMBUSTION: Catalyst Setting EXHAUST OXYGEN (% O2): SET POINT TIMING: 0.5

35

OLITOIN TIMINO.						
			MAXIMUM		TING AT MA	
			RATING	INLET A	IR TEMPER	RATURE
RATING	NOTES	LOAD	100%	100%	75%	50%
ENGINE POWER (WITHOUT FAN)	(1)	bhp	203	203	152	101
INLET AIR TEMPERATURE		°F	77	77	77	77
ENGINE DATA						
FUEL CONSUMPTION (LHV)	(2)	Btu/bhp-hr	8098	8098	8442	9195
FUEL CONSUMPTION (HHV)	(2)	Btu/bhp-hr	8983	8983	9364	10199
AIR FLOW (@inlet air temp, 14.7 psia) (WET)	(3)(4)	ft3/min	305	305	243	178
AIR FLOW (WET)	(3)(4)	lb/hr	1351	1351	1080	788
FUEL FLOW (60°F, 14.7 psia)		scfm	30	30	24	17
INLET MANIFOLD PRESSURE	(5)	in Hg(abs)	38.5	38.5	32.3	24.9
EXHAUST TEMPERATURE - ENGINE OUTLET	(6)	°F	1064	1064	1030	988
EXHAUST GAS FLOW (@engine outlet temp, 14.5 (WET)	(7)(4)	ft3/min	970	970	756	536
psia)						
EXHAUST GAS MASS FLOW (WET)	(7)(4)	lb/hr	1434	1434	1144	835
EMISSIONS DATA - ENGINE OUT						
NOx (as NO2)	(8)(9)	g/bhp-hr	16.57	16.57	16.26	13.78
co	(8)(9)	g/bhp-hr	16.57	16.57	16.26	13.78
THC (mol. wt. of 15.84)	(8)(9)	g/bhp-hr	1.20	1.20	1.39	1.67
NMHC (mol. wt. of 15.84)	(8)(9)	g/bhp-hr	0.18	0.18	0.21	0.25
NMNEHC (VOCs) (mol. wt. of 15.84)	(8)(9)(10)	g/bhp-hr	0.12	0.12	0.14	0.17
HCHO (Formaldehyde)	(8)(9)	g/bhp-hr	0.25	0.25	0.25	0.25
CO2	(8)(9)	g/bhp-hr	511	511	548	607
EXHAUST OXYGEN	(8)(11)	% DRY	0.5	0.5	0.5	0.5
HEAT REJECTION						
HEAT REJ. TO JACKET WATER (JW)	(12)	Btu/min	9045	9044	7544	6039
HEAT REJ. TO ATMOSPHERE	(12)	Btu/min	1095	1095	856	622
HEAT REJ. TO LUBE OIL (OC)	(12)	Btu/min	1430	1430	1193	955
HEAT REJ. TO AFTERCOOLER (AC)	(12)(13)	Btu/min	593	593	241	35
COOLING SYSTEM SIZING CRITERIA		-	•			
TOTAL JACKET WATER CIRCUIT (JW+OC)	(14)	Btu/min	11665			
TOTAL JACKET WATER CIRCUIT (JW+0C)	(13)(14)	Btu/min	623			
A cooling system safety factor of 0% has been added to the cooling system sizing crite		Dlu/IIIII	023			
A cooling system salety factor of the speem added to the cooling system sizing the	ııa.					

CONDITIONS AND DEFINITIONS

Engine rating obtained and presented in accordance with ISO 3046/1, adjusted for fuel, site altitude and site inlet air temperature. 100% rating at maximum inlet air temperature is the maximum engine capability for the specified fuel at site altitude and maximum site inlet air temperature. Max. rating is the maximum capability for the specified fuel at site altitude and reduced inlet air temperature. Lowest load point is the lowest continuous duty operating load allowed. No overload permitted at rating shown.

For notes information consult page three.

# YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

# Attachment L

# NATURAL GAS GLYCOL DEHYDRATION UNIT DATA SHEET

		Manufacturer and Model		KW International		
Max Dry Gas Flow Rat		Rate (MMscf/day)	2.0			
	Design Heat Inpu		(MMBtu/hr) - HHV	0.14		
Gene	ral Glycol	Design Type	(DEG or TEG)	TEG		
	ration Unit	Source	Status <sup>2</sup>	E	S	
	Data		odified/Removed <sup>3</sup>	20	13	
		Regenerator S	Still Vent APCD <sup>4</sup>	N.	A	
		Fuel HV (Bt	u/scf) - HHV	1,0	20	
		H₂S Conten	t (gr/100 scf)	0.	2	
		•	on (hrs/yr)	8,7	60	
Source ID #1	Vent	Reference <sup>5</sup>	PTE <sup>6</sup>	lbs/hr	tons/yr	
		AP	NOX	0.01	0.06	
		AP	CO	0.01	0.05	
		AP	VOC	7.5E-04	3.3E-03	
		AP	SOX	8.2E-05	3.6E-04	
		AP	PM10/2.5	1.0E-03	4.6E-03	
		AP	Benzene	2.9E-07	1.3E-06	
		AP	Ethylbenzene			
		AP	Formaldehyde	1.0E-05	4.5E-05	
		AP	n-Hexane	2.5E-04	1.1E-03	
RBV-1 (2E)	Reboiler Vent	AP	Methanol			
		AP	Toluene	4.7E-07	2.0E-06	
		AP	2,2,4-TMP			
		AP	Xylenes			
		AP	Other HAP	2.6E-07	1.1E-06	
		AP	Total HAP	2.6E-04	1.1E-03	
		40CFR98	CO2	16	72	
		40CFR98	CH4	3.1E-04	1.4E-03	
		40CFR98	N2O	3.1E-05	1.4E-04	
		40CFR98	CO2e	16	72	
		GR	VOC	5.15	22.55	
		GR	Benzene	0.10	0.44	
		GR	Ethylbenzene	0.05	0.20	
		GR	Formaldehyde			
		GR	n-Hexane	0.14	0.61	
	Chroal Baganaratar Still	GR	Methanol			
RSV-1 (3E)	Glycol Regenerator Still Vent	GR	Toluene	0.19	0.82	
		GR	2,2,4-TMP	0.00	0.02	
		GR	Xylenes	0.06	0.26	
		GR	Other HAP			
		GR	Total HAP	0.54	2.34	
		GR	CH4	6	28	
		40CFR98	CO2e	160	700	

#### Notes to NATURAL GAS GLYCOL DEHYDRATION UNIT DATA SHEET

- 1. Enter the appropriate Source Identification Numbers for the glycol dehydration unit Reboiler Vent and glycol Regenerator Still Vent. The glycol dehydration unit Reboiler Vent and glycol Regenerator Still Vent should be designated RBV-1 and RSV-1, respectively. If the compressor station incorporates multiple glycol dehydration units, a Glycol Dehydration Unit Data Sheet shall be completed for each, using Source Identification #s RBV-2 and RSV-3, etc.
- 2. Enter the Source Status using the following codes:

NS = Construction of New Source

ES = Existing Source

MS = Modification of Existing Source

RS = Removal of Source

- 3. Enter the date (or anticipated date) of the glycol dehydration unit's installation (construction of source), modification or removal.
- 4. Enter the Air Pollution Control Device (APCD) type designation using the following codes:

NA = None

CD = Condenser

FL = Flare

CC = Condenser/Combustion Combination

TO = Thermal Oxidizer

<ol><li>Enter the Potential</li></ol>	Emissions Data	Reference of	designation	using the	following	codes:

MD = Manufacturer's Data

AP = AP-42

GR = GRI-GLYCalcTM

OT = Other (please list):

6. Enter the Reboiler Vent and glycol Regenerator Still Vent Potential to Emit (PTE) for the listed regulated pollutants in lbs per hour and tons per year. The glycol Regenerator Still Vent potential emissions may be determined using the most recent version of the thermodynamic software model GRI-GLYCalcTM (Radian International LLC & Gas Research Institute). Attach all referenced Potential Emissions Data (or calculations) and the GRI-GLYCalc Aggregate Calculations Report to this Glycol Dehydration Unit Data Sheet(s). This PTE data shall be incorporated in the Emissions Summary Sheet.

Include a copy of the GRI-GLYCalcTM analysis. This includes a printout of the aggregate calculations report, which shall include emissions reports, equipment reports, and stream reports.

\*An explanation of input parameters and examples, when using GRI-GLYCalcTM is available on our website.



# KWI QUOTE # 1200382 REV 1

October 18, 2012

Williams Midstream One Williams Center Tulsa, OK 74172

Attn: Brenda Rexroat

Dear Mrs. Rexroat,

KW International, LLC is pleased to offer the following firm proposal for your consideration.

Thank you for considering KW International, LLC and we look forward to working with you on this project.

Please contact me if you have any questions or require additional information.

Regards,

Wee-Sim "Ni" Tooh

Account Manager 713-468-9581 | Office 281-773-4765 |Mobile wsteoh@kwintl.com | Email www.kwintl.com | Web

# **ITEM 9:**

# **DESIGN DATA:**

Required Gas Flow: 2 MMSCFD
Operating Pressure: 1000 psig
Operating Temp: 120 °F

# NEW, KWI 8 5/8" OD x 20'-0" S/S x 1440# MAWP X-PACKED ABSORBER / SCRUBBER

### **Vessel Data:**

Code: ASME Section VIII Division I & National Board Registered

Packed section: 9' X 5/8" Pall rings

Redistributor: Yes

Mist Extractor: (2) 304 ss wire mesh

Corrosion Allowance: None

# **CONNECTIONS**

Gas Inlet 2" 3000# NPT Gas Outlet 2" 3000# NPT 2" 3000# NPT Liquid level controller Oil Outlet 1" 3000# NPT Glycol Inlet 3/4" 3000# NPT Glycol Outlet 3/4" 3000# NPT Pressure Gauge 1/2" 3000# NPT Thermometer 3/4" 3000# NPT Gauge Glass (2) 3/4" 3000# NPT Relief Valve 1" 3000# NPT Drain 1" 3000# NPT (2)

#### **HEAT EXCHANGER**

External Glycol/Gas Heat Exchanger

# **Accessories**

2" NPT Norriseal 1001A Liquid Level Controller (Low Bleed Type)

1" NPT Norriseal 2220 Diaphragm Operated Dump Valve

0-2000# pressure gauge w/1/2" isolation valve

Reflex gauge glass assembly with steel gauge cocks

Relief Valve - 1" NPT steel Relief Valve, set at vessel MAWP

- 1 1/4" Fisher 67AFR Regulator
- 1 0-250 Degree F thermometer with thermowell

#### **PAINT**:

Primer and Williams Rainforest Green (SW #4071)

# KWI 87,500 BTU/HR. SKID MOUNTED REGENERATION UNIT

# **REBOILER**

20" x 6' w/ integral storage/surge tank

1 - 6 5/8" O.D. Flanged removable "U" firetube w/ 6 5/8" O.D. x 6'-0" removable stack (7000 Flux)

1 - 6 5/8" O.D. x 4'-3" flanged removable still column packed with ceramic saddles

# **ACCESSORIES**

Kimray T12M high temperature shutdown

Kimray T12 Temperature controller

Fisher 119 Temperature control valve

0-60# fuel gas pressure gauge

Fuel gas pressure regulator

High pressure fuel gas regulator

0-200# fuel gas pressure gauge

50-550 deg. F thermometer w/ss thermowell

2- "Y" Strainer (Rich & Lean)

One burner and pilot assembly with flame arrestor cell

5/8" tubular gauge glass assembly

1/2" NPT ball valve

One set fuel and instrument gas piping

# GLYCOL/GLYCOL HEAT EXCHANGER

1 - Section of panel coil, 22" x 47"

# **GLYCOL PUMP**

1 - Kimray 1720 PV Glycol Pump with piping manifold

# **GLYCOL FILTER**

2 -Sock type filter with bypass (Rich & Lean)

1 – Charcoal filter with bypass

## **PIPING**

1/2" glycol piping assembly complete for unit operation

# **INSULATION**

Reboiler shell insulated with Calcium Silicate w/ Aluminum Jacket

#### SKID

3'-0" x 10'-0" approximate size

#### **PAINT**

Uninsulated areas coated with Primer and Williams Rainforest Green (SW #4071)

# 18" OD X 4' S/S X 125# MAWP, ASME CODE CONSTRUCTED AND STAMPED, HORIZONTAL 3 PHASE PUMP GAS SEPARATOR WITH 2-PHASE ACCESSORIES

# **VESSEL OPENING**

Glycol Inlet 1" 3000# Threaded Gas Outlet 1" 3000# Threaded Glycol Outlet 1" 3000# Threaded Liquid Level Controller (2) 2" 3000# Threaded Gauge Glass (4) 1/2" 3000# Threaded Pressure Gauge 1/2" 3000# Threaded Thermometer 3/4" 3000# Threaded Condensate Outlet 1" 3000# Threaded

# 2-PHASE ACCESSORIES

Liquid Level Control: 2" NPT Norriseal 1001A (Low Bleed Type) Glycol Dump Valve: 1" NPT Kimray 112 SMT with 1" NPT block valve

Condensate Dump Valve: Manual

Back Pressure Valve: 1-1" NPT Fisher 1805 Relief Valve: 1-1" NPT relief valve set at 125# Gauge Glass: 5/8" tubular with gauge cocks Thermometer: 1- 20-240o F with ss thermowell

Fuel Gas Scrubber: 10" x 2'2" x 250# ASME Code with relief valve set at 125#, pressure gauge 0-200# with

isolation valve

Instrument Gas Regulator Make-Up Gas Regulator

Supply Gas: 1- 0-200# pressure gauge with 1/2" isolation valve, tubing and fittings

#### **PIPING**

As required for unit operation

# **INSULATION**

Calcium Silicate w/ Aluminum Jacket

# **PAINT**

Primer and Williams Rainforest Green (SW #4071)

# YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

# Attachment L

# 40 CFR Part 63; Subpart HH & HHH Registration Form

**West Virginia Department of Environmental Protection** 

**Division of Air Quality**DIVISION OF AIR QUALITY: (304) 926-0475

40 CFR Part 63; Subpart HH & HHH Registration Form

Complete this form for any oil and natural gas production or natural gas transmission and storage facility that uses an affected unit under HH/HHH, whether subject or not.

**Section A: Facility Description** 

WEB PAGE: http://www.wvdep.org

Affected facility actual annual average natura	gas throughput (scf/day):	2.0 MMscfd			
Affected facility actual annual average hydroc	ffected facility actual annual average hydrocarbon liquid throughput: (bbl/day):				
The affected facility processes, upgrades, or	stores hydrocarbon liquids prior to custody transfer.	☑ Yes ☐ No			
The affected facility processes, upgrades, or NG transmission and storage source category	stores natural gas prior to the point at which natural gas (NG) enters the $\gamma$ or is delivered to the end user.	☑ Yes □ No			
The affected facility is: ☑ prior to a	NG processing plant ☐ NG processing plant				
☐ prior to th	e point of custody transfer and there is no NG processing plant				
The affected facility transports or stores natur a final end user (if there is no local distribution	al gas prior to entering the pipeline to a local distribution company or to company).	□ Yes ☑ No			
The affected facility exclusively processes, sto	ores, or transfers black oil	□ Yes ☑ No			
with an initial producing gas-to-oil ratio (GOR)	na scf/bbl API gravity: na degrees	□ Yes ☑ No			
	Section B: Dehydration Unit (if applicable) <sup>1</sup>				
Description: 2.0 MMsc	fd - TEG Dehy 01 (RSV-1 (3E)				
Date of Installation: 2013	Annual Operating Hours: 8,760 Burner rating (N	MMbtu/hr): <b>0.14</b>			
Exhaust Stack Height (ft): 10.0	Stack Diameter (ft): 0.6 Stack Te	emp. (oF): <b>120</b>			
Glycol Type: ☑ TEG	□ EG □ Other: <b>na</b>				
Glycol Pump Type: ☐ Elect	☐ Gas If Gas, what is the volume ratio?: 0.08 acfm/gpm				
Condenser installed? ☐ Yes	☑ No Exit Temp: <b>na</b> Condenser Pressure:	na			
Incinerator/flare installed? ☐ Yes	☑ No Destruction Eff.: <b>na</b>				
Other controls installed? ☐ Yes	☑ No Describe: <b>na</b>				
Wet Gas <sup>2</sup> :	Gas Temperature: <b>70oF</b> Gas Pressure: <b>1,000 psig</b>				
(Upstream of Contact Tower)	Saturated Gas?: ☑ Yes ☐ No If no, water content?:	na			
Dry Gas:	Gas Flowrate: Actual: 2.0 MMscfd Design:	2.0 MMscfd			
(Downstream of Contact Tower)	Water Content: 7.0 lb/MMscf				
Lean Glycol:	Circulation Rate: Actual <sup>3</sup> : <b>0.67 gpm</b> Max <sup>4</sup> :	0.67 gpm			
Edan Glyddi.	Pump make/model: Kimray 4020PV				
Glycol Flash Tank (if applicable):	Temp: 120 oF Pressure: 60 psig Vented:	☑ Yes □ No			
2., 350. 1. 1251. Tallik (ii appiloabio).	If no, describe vapor control: At least 50% of flash tank vapors				
	reboiler fuel, the remainder is vented	to atmosphere.			
Stripping Gas (if applicable):	Source of Gas na Rate: na				

# YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### Attachment L

# 40 CFR Part 63; Subpart HH & HHH Registration Form - Continued

#### Please attach the following required dehydration unit information:

- 1. System map indicating the chain of custody information. See Page 43 of this document for an example of a gas flow schematic. It is not intended that the applicant provide this level of detail for all sources. The level of detail that is necessary is to establish where the custody transfer points are located. This can be accomplished by submitting a process flow diagram indicating custody transfer points and the natural gas flow. However, the DAQ reserves the right to request more detailed information in order to make the necessary decisions.
- 2. Extended gas analysis from the Wet Gas Stream, including mole percent of C1-C8, benzene, ethylbenzene, toluene, xylene and n-hexane, using Gas Processors Association (GPA) 2286 (or similar). A sample should be taken from the inlet gas line, downstream from any inlet separator, and using a manifold to remove entrained liquids from the sample and a probe to collect the sample from the center of the gas line. GPA standard 2166 reference method or a modified version of EPA Method TO-14, (or similar) should be used.
- 3. GRI-GLYCalc Ver. 3.0 aggregate report based on maximum Lean Glycol circulation rate and maximum throughput.
- 4. Detailed calculations of gas or hydrocarbon flow rate.

	Section C: Facility NESHAPS Subpart HH/HHH status					
	of HAP emissions <u>a</u>	nd the actuative vent to the a	ver, <u>EXEMPT</u> because the facility is an area source at average emissions of benzene from the glycol dehy- atmosphere is < 0.90 megagram per year (1.0 tpy);			
Affected facility status: - (choose only one)	☐ Subject to Subpart H	□ Subject to Subpart HHH				
	□ Not Subject Because:	_ _ _	< 10/25 TPY Affected facility exclusively handles black oil.  Facility-wide actual annual average NG throughput is < 650 thousand scf/day and facility-wide actual annual average hydrocarbon liquid is < 250 bpd.  No affected source is present.			

# STORAGE TANK DATA SHEET

Source ID #1	Status <sup>2</sup>	Content <sup>3</sup>	Volume <sup>4</sup> (gal)	Dia <sup>5</sup> (ft)	Throughput <sup>6</sup> (gal/yr)	Orientation <sup>7</sup>	Ave Liq Ht <sup>8</sup> (Ft)
TK-01		Produced Water	8,820	10	105,840	VERT	8
TK-02		Lube Oil	500	4	6,000	HORZ	2
TK-03		Waste Oil	500	4	6,000	HORZ	2
TK-04		Glycol	225	4	2,700	HORZ	2
TK-05		Methanol	130	4	1,560	HORZ	2
TK-06		Methanol	130	4	1,560	HORZ	2

# **Notes to STORAGE TANK DATA SHEET**

- 1. Enter the appropriate Source Identification Numbers (Source ID #) for each storage tank located at the compressor station. Tanks should be designated T01, T02, T03, etc.
- 2. Enter storage tank Status using the following:

EXIST Existing Equipment

NEW Installation of New Equipment

REM Equipment Removed

- 3. Enter storage tank content such as condensate, pipeline liquids, glycol (DEG or TEG), lube oil, etc.
- 4. Enter storage tank volume in gallons.
- 5. Enter storage tank diameter in feet.
- 6. Enter storage tank throughput in gallons per year.
- 7. Enter storage tank orientation using the following:

VERT Vertical Tank

HORZ Horizontal Tank

8. Enter storage tank average liquid height in feet.

# Attachment L EMISSIONS UNIT DATA SHEET STORAGE TANKS

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <a href="https://www.epa.gov/tnn/tanks.html">www.epa.gov/tnn/tanks.html</a>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<a href="https://www.epa.gov/tnn/chief/">http://www.epa.gov/tnn/chief/</a>).

# I. GENERAL INFORMATION (required)

1.	Bulk Storage Area Name	2.	Tank Name			
			210 bbl Produced Water Tank			
3.	Tank Equipment Identification No. (as assigned on <i>Equipment List Form</i> ) T01	4.	Emission Point Identification No. (as assigned on <i>Equipment List Form</i> ) 5E			
5.	Date of Commencement of Construction (for existing	tank	as)			
6.	Type of change ⊠ New Construction □ N	lew	Stored Material			
7.	7. Description of Tank Modification (if applicable)					
	Does the tank have more than one mode of operation (e.g. Is there more than one product stored in the tan	k?)	☐ Yes			
	If YES, explain and identify which mode is covere completed for each mode).	ed b	y this application (Note: A separate form must be			
	Provide any limitations on source operation affecting variation, etc.):	emi	ssions, any work practice standards (e.g. production			
	II. TANK INFORM	ATIO	ON (required)			
	height.	the 0 bar	internal cross-sectional area multiplied by internal rels			
9A.	Tank Internal Diameter (ft)	9B.	Tank Internal Height (or Length) (ft)			
	10		15			
10A	Maximum Liquid Height (ft)	10E	3. Average Liquid Height (ft)			
	14		8			
11A	Maximum Vapor Space Height (ft)	11E	3. Average Vapor Space Height (ft)			
12.	liquid levels and overflow valve heights.	s als	so known as "working volume" and considers design			

13A. Maximum annual throughput (gal/yr)	13B. Maximum daily throughput (gal/day)					
229,320  14. Number of Turnovers per year (annual net throughput)	ut/maximum tank liquid volume)					
14. Number of Furnovers per year (annual net unoughpo	26					
15. Maximum tank fill rate (gal/min)						
16. Tank fill method Submerged	☐ Splash ☐ Bottom Loading					
17. Complete 17A and 17B for Variable Vapor Space Ta	nk Systems Does Not Apply					
17A. Volume Expansion Capacity of System (gal)	17B. Number of transfers into system per year					
18. Type of tank (check all that apply):  Fixed Roof vertical horizontal other (describe)  External Floating Roof pontoon roof Domed External (or Covered) Floating Roof Internal Floating Roof vertical column so	double deck roof					
☐ Variable Vapor Space lifter roof ☐ Pressurized spherical cylindrica ☐ Underground ☐ Other (describe)	diaphragm					
III. TANK CONSTRUCTION & OPERATION INFORM	IATION (optional if providing TANKS Summary Sheets)					
<ul><li>19. Tank Shell Construction:</li><li>☐ Riveted ☐ Gunite lined ☐ Epoxy-coate</li></ul>	d rivete					
☐ Riveted ☐ Gunite lined ☐ Epoxy-coate  20A. Shell Color 20B. Roof Colo	, ,					
21. Shell Condition (if metal and unlined):	<u> </u>					
☐ No Rust ☐ Light Rust ☐ Dense R	Rust					
22A. Is the tank heated?  YES NO						
22B. If YES, provide the operating temperature (°F)						
22C. If YES, please describe how heat is provided to	tank.					
23. Operating Pressure Range (psig): to						
24. Complete the following section for Vertical Fixed Ro	pof Tanks Does Not Apply					
24A. For dome roof, provide roof radius (ft)						
24B. For cone roof, provide slope (ft/ft)						
25. Complete the following section for Floating Roof Ta	nks 🖂 Does Not Apply					
25A. Year Internal Floaters Installed:						
25B. Primary Seal Type:	· ·					
25C. Is the Floating Roof equipped with a Secondary	Seal? YES NO					
25D. If YES, how is the secondary seal mounted? (ch	eck one)					
25E. Is the Floating Roof equipped with a weather shi	eld? YES NO					

25F. Describe deck fittings; indicate the number of each type of fitting:						
20. : Doscribe dock fittings, filaleate		S HATCH				
BOLT COVER, GASKETED:	UNBOLTED COVI		UNBOLTED COVER, UNGASKETED:			
BOLT COVER, GASKETED:	AUTOMATIC GAL UNBOLTED COVI	JGE FLOAT WELL ER, GASKETED:	UNBOLTED COVER, UNGASKETED:			
BUILT-UP COLUMN – SLIDING COVER, GASKETED:			PIPE COLUMN – FLEXIBLE FABRIC SLEEVE SEAL:			
PIP COLUMN – SLIDING COVER, G		R WELL   PIPE COLUMN	SLIDING COVER, UNGASKETED:			
SLIDING COVER, GASKETED:	GAUGE-HATCH	/SAMPLE PORT   SLIDING COVER,	UNGASKETED:			
WEIGHTED MECHANICAL ACTUATION, GASKETED:	1	HANGER WELL MECHANICAL GASKETED:	SAMPLE WELL-SLIT FABRIC SEAL (10% OPEN AREA)			
WEIGHTED MECHANICAL ACTUAT		BREAKER   WEIGHTED MECHA	ANICAL ACTUATION, UNGASKETED:			
WEIGHTED MECHANICAL ACTUAT		VENT   WEIGHTED MECHANICAL ACTUATION, UNGASKETED:				
OPEN:	DECK DRAIN (3-I	-INCH DIAMETER)   90% CLOSED:				
STUB DRAIN 1-INCH DIAMETER:						
OTHER (DESCRIBE, ATTACH ADDITIONAL PAGES IF NECESSARY)						

26. Complete the follow	ng section for Internal	Floating Ro	oof Tanl	ks	□ Does Not Apple	ply
26A. Deck Type:	☐ Bolted ☐ We	elded				
26B. For Bolted deck	s, provide deck constru	iction:				
26C. Deck seam:						
_	t construction 5 feet wid t construction 6 feet wid					
_	t construction 7 feet with					
. =	t construction $5 \times 7.5$ fe					
Other (describe)	t construction 5 x 12 fe	eet wide				
		1				
26D. Deck seam leng	* *		26E.		of deck (ft <sup>2</sup> )	
For column supported to			26G.	Dian	neter of each colum	ın:
26F. Number of colur		/		TA	NIKO O Ol	(-)
27. Provide the city and	SITE INFORMANTION	` .	•			eets)
27. Flovide the city and	State on which the data	a III IIIIS SEI	cuon an	e Dasi	eu.	
28. Daily Average Ambi	ent Temperature (°F)					
29. Annual Average Ma	ximum Temperature (°F	F)				
30. Annual Average Mir	imum Temperature (°F	-)				
31. Average Wind Spee	d (miles/hr)					
32. Annual Average Sol	ar Insulation Factor (BT	ΓU/(ft²⋅day)	)			
33. Atmospheric Pressu	re (psia)					
V. L	QUID INFORMATION	(optional if	providi	ng TA	NKS Summary Sho	eets)
34. Average daily temper	erature range of bulk liq	juid:				
34A. Minimum (°F)			34B.	Maxi	imum (°F)	
35. Average operating p	ressure range of tank:					
35A. Minimum (psig)			35B.	Max	imum (psig)	
36A. Minimum Liquid	Surface Temperature (	(°F)	36B.	Corr	esponding Vapor P	ressure (psia)
		o=)				
37A. Average Liquid	Surface Temperature (°	°F)	37B.	Corr	esponding Vapor P	ressure (psia)
38A. Maximum Liquid	Surface Temperature	(°F)	38B.	Corr	esponding Vapor P	ressure (psia)
39. Provide the following	g for <u>each</u> liquid or gas	to be store	d in tan	k. Ac	ld additional pages	if necessary.
39A. Material Name of	or Composition					
39B. CAS Number						
39C. Liquid Density (I	b/gal)					
39D. Liquid Molecula	r Weight (lb/lb-mole)					
39E. Vapor Molecula	r Weight (lb/lb-mole)		· · · · · · · · · · · · · · · · · · ·			

Maximum Vapor Press 39F. True (psia) 39G. Reid (psia)	sure			•		
39G. Reid (psia)	34.0					
Months Storage per Ye	ear					
39H. From	- <del></del> -					
39I. To						
	VI. EMISSIONS A	ND CONTR	OL DEVICE	E DATA (required)		
40. Emission Control Devices (check as many as apply): ☑ Does Not Apply						
☐ Carbon Adsorption <sup>1</sup>						
☐ Condenser <sup>1</sup>						
☐ Conservation V	/ent (psig)					
Vacuum S	Setting		Pressure Se	etting		
☐ Emergency Re	lief Valve (psig)					
☐ Inert Gas Blank	ket of					
☐ Insulation of Ta	ank with					
Liquid Absorpti	on (scrubber) <sup>1</sup>					
☐ Refrigeration of	f Tank					
Rupture Disc (p	osig)					
☐ Vent to Incinera	ator <sup>1</sup>					
☐ Other¹ (describ	e):					
<sup>1</sup> Complete approp	oriate Air Pollution Cont	trol Device S	Sheet.			
41. Expected Emission	n Rate (submit Test Da	ta or Calcul	ations here	or elsewhere in the app	olication).	
Material Name &	Breathing Loss	Workin	g Loss	Annual Loss	1	
CAS No.	(lb/hr)	Amount	_		Estimation Method <sup>1</sup>	
		Aillouit	Units	(lb/yr)		
VOC		Amount	Units			
VOC		Amount	Units	(lb/yr) 220	EPA-450/3-85-001a	
VOC		Amount	Units			
VOC		Amount	Units			
VOC		Amount	Units			
VOC		Amount	Units			
VOC		Amount	Units			
VOC		Amount	Units			
VOC		Amount	Units			
VOC		Amount	Units			
VOC		Amount	Units			
VOC		Amount	Units			
VOC		Amount	Units			
				220		

# Attachment L EMISSIONS UNIT DATA SHEET BULK LIQUID TRANSFER OPERATIONS

Furnish the following information for each new or modified bulk liquid transfer area or loading rack, as shown on the *Equipment List Form* and other parts of this application. This form is to be used for bulk liquid transfer operations such as to and from drums, marine vessels, rail tank cars, and tank trucks.

Identification Number (as assigned on Equipment List Form): TLO					
1. Loading Area	Name:				
2. Type of cargo as apply): <b>N/A</b>	vessels accommo	odated at this rack	d at this rack or transfer point (check as many		
G Drums	G Marine Vessels	G Rail	Tank Cars	G Tank Trucks	
3. Loading Rack or Transfer Point Data:					
Number of pu	mps	1			
Number of liqu	uids loaded	1			
Maximum nun	nber of marine	1			
·	trucks, tank cars, loading at one tim	e			
4. Does ballastin	ng of marine vess		oading area? es not apply		
5. Describe cleatransfer point: N/	nning location, con	npounds and proc	cedure for cargo v	essels using this	
6. Are cargo vessels pressure tested for leaks at this or any other location? <b>N/A</b> G Yes  G No  If YES, describe:					
7. Projected Ma	ximum Operating	Schedule (for rac	k or transfer point	as a whole):	
Maximum	Jan Mar.	Apr June	July - Sept.	Oct Dec.	
hours/day	24	24	24	24	
days/week	7	7	7	7	
weeks/quarter         13         13         13					

8. Bulk Liquid Data (add pages as necessary):						
Pump ID No.		1				
Liquid Name		Prod. H2O				
Max. daily thro	oughput (1000 gal/day)	0.628				
Max. annual t	hroughput (1000 gal/yr)	229.3				
Loading Method <sup>1</sup>		SP				
Max. Fill Rate (gal/min)		200				
Average Fill Time (min/loading)		60				
Max. Bulk Liquid Temperature (°F)		60				
True Vapor P	ressure <sup>2</sup>	1.5				
Cargo Vessel	Condition <sup>3</sup>	U				
Control Equip	ment or Method <sup>4</sup>	None				
Minimum con	trol efficiency (%)	N/A				
Maximum	Loading (lb/hr)					
Emission Rate (VOC)	Annual (lb/yr)	1,100				
Estimation Method <sup>5</sup>		EPA				
1		_	_			

<sup>&</sup>lt;sup>1</sup> BF = Bottom Fill SP = Splash Fill SUB = Submerged Fill

MB = Material Balance

TM = Test Measurement based upon test data submittal

O = other (describe)

<sup>&</sup>lt;sup>2</sup> At maximum bulk liquid temperature

 $<sup>^3</sup>$  B = Ballasted Vessel, C = Cleaned, U = Uncleaned (dedicated service), O = other (describe)

<sup>&</sup>lt;sup>4</sup> List as many as apply (complete and submit appropriate *Air Pollution Control Device Sheets*):CA = Carbon Adsorption LOA = Lean Oil AdsorptionCO = Condensation SC = Scrubber (Absorption)CRA = Compressor-Refrigeration-Absorption TO = Thermal Oxidation or Incineration CRC = Compression-Refrigeration-Condensation VB = Dedicated Vapor Balance (closed system) O = other (descibe)

<sup>&</sup>lt;sup>5</sup> EPA = EPA Emission Factor as stated in AP-42

9.	<b>Proposed</b>	Monitoring,	Recordkeeping,	Reporting,	and	Testing
• •						

Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

MONITORING	RECORDKEEPING
REPORTING	TESTING

**MONITORING.** PLEASE LIST AND DESCRIBE THE PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OPERATION OF THIS

**RECORDKEEPING.** PLEASE DESCRIBE THE PROPOSED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.

**REPORTING.** PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORDKEEPING.

**TESTING.** PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR POLLUTION CONTROL DEVICE.

10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty

# ATTACHMENT M

# **Air Pollution Control Device Sheet(s)**

'29	Fill out the	Air Pollution	<b>Control Device</b>	Sheet(s) as	Attachment M "
<b>Z</b> J.	I III OUL LIIC	All Fullution	COILLIOI DEVICE	311661131 as	Allacillicit ivi.

- 203 bhp Caterpillar G3306TA Compressor Engine EMIT NSCR
  - o Non-Selective Catalytic Reduction (NSCR) Vendor Data

# Attachment M Air Pollution Control Device Sheet

(OTHER COLLECTORS)

Control Device ID No. (must match Emission Units Table):

# **Equipment Information**

1.	Manufacturer: EMIT Technologies Model No. EAH-1450T-0505F-20CEE (or equiv.	.)	Control Device Nan Type: NSCR	ne: Catalytic Converter	
3.	Provide diagram(s) of unit describing capture system with duct arrangement and size of duct, air volume, capacity, horsepower of movers. If applicable, state hood face velocity and hood collection efficiency.				
4.	On a separate sheet(s) supply all data and calculate	ulatio	ns used in selecting or de	esigning this collection device.	
5.	Provide a scale diagram of the control device sh	nowin	g internal construction.		
6.	Submit a schematic and diagram with dimension	ns an	d flow rates.		
7.	Guaranteed minimum collection efficiency for ea	ach p	ollutant collected:		
NO	x (≥88%) and CO (≥76%)				
8.	Attached efficiency curve and/or other efficiency	/ info	rmation.		
9.	Design inlet volume: SC	FM	10. Capacity:		
11.	Indicate the liquid flow rate and describe equipment of the liquid flow	nent p	provided to measure pres	sure drop and flow rate, if any.	
12.	Attach any additional data including auxiliary control equipment.	equip	oment and operation de	tails to thoroughly evaluate the	
13.	Description of method of handling the collected	mate	rial(s) for reuse of dispos	al.	
	Gas Strea	am C	haracteristics		
14.	Are halogenated organics present? Are particulates present? Are metals present?		☐ Yes ☐ No ☐ Yes ☐ No ☐ Yes ☐ No		
15.	Inlet Emission stream parameters:		Maximum	Typical	
	Pressure (mmHg):				
	Heat Content (BTU/scf):				
	Oxygen Content (%):				
	Moisture Content (%):				
	Relative Humidity (%):				

Page 1 of 3 REVISED 03/15/2007

16.	Type of pollutant(s) o		□ SO <sub>x</sub>	☐ Odor ☑ Other NOx	, CO, VOC and	НСНО	
17.	Inlet gas velocity:		ft/sec	18. Pollutant	specific gravity:		
19.	Gas flow into the coll 970 ACFM @		PSIA	20. Gas strea	m temperature: Inlet: Outlet:	1064	°F °F
21.	Gas flow rate: Design Maximum: Average Expected:	970 970	ACFM ACFM	22. Particulat	e Grain Loading Inlet: Outlet:	in grains/scf:	
23.	Emission rate of eac	h pollutant (speci	fy) into and out	of collector:			
	Pollutant	IN Pol	lutant	Emission	OUT Po	llutant	Control
		g/bhp-hr	grains/acf	Capture Efficiency %	g/bhp-hr	grains/acf	Efficiency %
	NOx	16.57		88	≤2.00		
	CO	16.57		76	≤4.00		
	NMNEHC	0.12		0	0.12		
	НСНО	0.25		0	0.25		
24.	Dimensions of stacks	Heigl	ht	ft.	Diameter		ft.
25.	Supply a curve show rating of collector.	ving proposed co	ollection efficien	cy versus gas	volume from 25	5 to 130 perce	nt of design

# **Particulate Distribution**

26. Complete the table:	Particle Size Distribution at Inlet to Collector	Fraction Efficiency of Collector
Particulate Size Range (microns)	Weight % for Size Range	Weight % for Size Range
0 – 2		
2 – 4		
4 – 6		
6 – 8		
8 – 10		
10 – 12		
12 – 16		
16 – 20		
20 – 30		
30 – 40		
40 – 50		
50 – 60		
60 – 70		
70 – 80		
80 – 90		
90 – 100		
>100		

27. Describe any air preheating, gas hun		utlet gas conditioning processes (e.g., gas cooling, gas
28. Describe the collect	ction material disposal system:	
29. Have you included	Other Collectores Control Device	e in the Emissions Points Data Summary Sheet?
Please propose r	ng parameters. Please propose	and Testing eporting in order to demonstrate compliance with the testing in order to demonstrate compliance with the
MONITORING:		RECORDKEEPING:
REPORTING:		TESTING:
MONITORING:		ocess parameters and ranges that are proposed to be strate compliance with the operation of this process
RECORDKEEPING: REPORTING:	Please describe the proposed re Please describe any proposed	cordkeeping that will accompany the monitoring. emissions testing for this process equipment on air
TESTING:	pollution control device.  Please describe any proposed pollution control device.	emissions testing for this process equipment on air
31. Manufacturer's Gu	aranteed Control Efficiency for each	h air pollutant.
NOx (≥88%) and C	CO (≥76%)	
32. Manufacturer's Gu	aranteed Control Efficiency for eac	h air pollutant.
33. Describe all operat	ting ranges and maintenance proce	edures required by Manufacturer to maintain warranty.



#### Maxim Silencers, Inc.

10035 Brighton Lame Stafford, Texas 77477 Phone: 802 554 0990 Fax: 802 554 0990

Customer: USA COMPRESSION		Project:	Date: 9/14/2012
Sales Person:	Ste Elevation:	ft Contact:	Order/Quote #: 0

#### Engine Data:

Engine Model:	Caterpillar	G3306TA	Speed:	1800	RPM
Fuel & Operating Type:	Natural Ga	s Rich Bum	Engine Power:	203 152	Hp KW
Exhaust Flow Rate:	970 1648 1512	acfm m²/hr lbs/hr	Exhaust Temperature:	1064 573	°F

#### QAC (Quick Access Catalyst) Data:

Model: QAC4-29-5

Grade: Super Critical Body Diameter: 18

Estimated weight: 147 67



Inlet Stre: 5 in Outlet Stre: 5 in Estimated Back Pressure: 6.80 16.9 In of WC

Speed through inlet: 7499

Min. Temp. at Core Face: 1022 °F 550 °C Max. Temp. at Core Face: 1094 °F 590 °C

Catalyst Type: 3-Way

Engine Out / Pre Emission: Post Emission:

3	що	NMHC/VOC	CO	NDX
g/bhp-hr	0.25	0.12	16.57	16.57
g/bhp-hr	0.200	0.096	2.000	2.000
% Reduction	20.0	20.0	87.9	87.9
bhr	0.09	0.04	0.90	0.90
tons/year operation	0.39	0.19	3.93	3.93
ppmv	36.6	17.6	367.2	367.2
ppmvd @ 15% O2	11.7	5.6	117.1	117.1

8760 hr/year

Prequency Band (Hz): Estimated Attenuation (dB):	63 18	125	250	500	1000	2000	4000	8000 20	No Flement
Plus: Plus:	19	40 41	41 42	41	31 35	27 31	26 30	25 29	One Element Layer Two Element(s) Layers

# Warranty & Notes:

- If Pre-Emission levels are not as noted above, conject Maxim for a re-quoje.
  To achieve Prot Emissions levels distalled above, exhaust inerpensive and Pre-Emission dela must be as specified.
  Maximum allowable exhaust inerpensive an atenual score less in 1907-7.
  If applicable, the engine will require an atenual ratio controller to meet above emission levels. For Rich Burn engines A must in applicable, the engine will require an atenual ratio backgrousser increases by 2° of W.C.
  Engine operation to be statele and reproductive.
  OAC is not designed to withstand a backfire, therefore measures should be below prior to QAC and to alleviate backfire present the production of consumption rate to be less than 0,0015 bibliophy.
  Lube oil subfide sub-contents should not encode 0,0%.
  In the contents about of encode 0,0%.

- Libro off suffice and contents should not encoded D.FK.
   Phosphorus and/or Zinc should not encoded 5 ppms in the exhaust shown.
   A high temperature alternishmetical to be maintained at desentinean of catalyst at 1000 °C.
   Four not to contain heavy or harvation mateix such as Pib, Ar, Zin, Cu, So, Fo, Ru, Ni, Cordic.
   Chlorivated or Sittems containing compounds in the exhaust of to the extend 1 ppms.
   Suffer compounds in the exhaust gas stream not to exceed 25 ppms.
   Performance guarantes is voicided should the catalyst become masted or de-activated by any contaminant in the exhaust a Engrise to be maintained and operated in accordance within manufactural variance and practice.
   Under no condition will Maxim Sitemons inc. susures any contingent labilities.
   Operating menual is available online at www.mai.imaltences.com or contains the Maxim Sitemon for the way and insuffered to the Contains and expensionable on the stream maintences com or contains the containstalled and it is flange claim.
   Maximis standard one year secretly applies.

# **ATTACHMENT N**

# **Supporting Emissions Calculations**

"30. Provide all **Supporting Emissions Calculations** as Attachment N."

# Emission Summary Spreadsheets

- Controlled Emissions
- PRE-Controlled Emissions
- Greenhouse Gas Emissions

# Unit-Specific Emission Spreadsheets

- o Compressor Engine 203 bhp Caterpillar G3306TA Compressor Engine
- o Triethylene Glycol (TEG) Reboiler 0.14 MMBtu/hr
- o Triethylene Glycol (TEG) Dehydrator 2.0 MMscfd
- o Produce Water Storage Tank 210 bbl capacity
- o Produced Water Truck Load-Out 5,460 bbl/yr
- Startup/Shutdown/Maintenance (SSM)
- o Process Piping Fugitives Gas & Water/Oil
- Compressor Rod Packing Leaks and Engine Crankcase Leaks

# AP-42 and GHG Emission Factors

# Model Results

- Dehydrator GRI-GLYCalc 4.0
  - Summary of Emissions
  - Summary of Input Values
  - Aggregate Calculations Report
- Storage Tank Promax
  - Plant Schematic
  - Process Stream Report

#### YOHO COMPRESSOR STATION

#### Application for 45CSR13 NSR Modification Permit

# **Attachment N - Supporting Emissions Calculations**

#### **Controlled Emissions**

#### Controlled Potential to Emit (PTE) Summary - Criteria Polutants

Unit ID	Unit ID Point Control	Description	Conceity	NO	Эx	С	0	VC	C	SC	Эx	PM1	0/2.5	CC	)2e	
Official	ID	ID	Description	Capacity	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
CE-01	1E	01-NSCR	Caterpillar Engine	203 bhp	0.89	3.90	1.78	7.80	0.17	0.73	1.1E-03	4.7E-03	0.04	0.15	240	1,052
RBV-1	2E	na	TEG Dehydrator - Reboiler	0.14 MMBtu/hr	0.01	0.06	0.01	0.05	7.5E-04	3.3E-03	8.2E-05	3.6E-04	1.0E-03	4.6E-03	16	72
RSV-1	3E	na	TEG Dehydrator - Flash Tank/Still Vent	2.0 MMscfd					5.15	22.55					160	700
T01	4E	na	Produced Water - Storage Tank	210 bbl					0.05	0.22						
TLO	5E	na	Produced Water - Truck Loadout	5,460 bbl/yr						0.55						
SSM	6E	na	Startup/Shutdown/Maintenance							1.53						108
FUG	7E	na	Piping and Equipment Fugitives						1.50	6.55					91	397
RPC	8E	na	Rod Packing/Crankcase Emissions						8.2E-04	3.6E-03					74	325
	TOTAL PTE:					3.96	1.79	7.85	6.86	32.13	1.2E-03	0.01	3.6E-02	0.16	581	2,653
	WV-DEP Permit Threshold:					ND 10	6 AN	ID 10	6 AN	ID 10	6 AN	ND 10	6 <u>AN</u>	<u>ID</u> 10	r	na
	Title V Permit Threshold:				100		100		100		100		100	r	na	

#### Controlled Potential to Emit (PTE) Summary - Hazardous Air Pollutants (HAPs)

Unit ID	Benz	zene	Ethylbe	enzene	НСНО	(HAP)	n-He	xane	Metha	nol	Tolu	iene	2,2,4	-TMP	Xyle	enes	Other	HAP	Total	I HAP
Official	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
CE-01	2.9E-03	0.01	4.5E-05	0.00	0.11	0.49			0.01	0.02	1.0E-03	4.5E-03			3.6E-04	1.6E-03	0.01	0.05	0.13	0.58
RBV-1	2.9E-07	1.3E-06			1.0E-05	4.5E-05	2.5E-04	1.1E-03			4.7E-07	2.0E-06					2.6E-07	1.1E-06	2.6E-04	1.1E-03
RSV-1	0.10	0.44	0.05	0.20			0.14	0.61			0.19	0.82	4.3E-03	0.02	0.06	0.26			0.54	2.34
T01	1.3E-03	0.01	1.3E-03	0.01			1.3E-03	0.01			1.3E-03	0.01	1.3E-03	0.01	1.3E-03	0.01			0.01	0.03
TLO		0.01		0.01				0.01				0.01		0.01		0.01				0.08
SSM		2.0E-03		2.0E-03				0.05				2.0E-03		2.0E-03		2.0E-03				0.06
FUG	0.02	0.10	0.02	0.10			0.02	0.10			0.02	0.10	0.02	0.10	0.02	0.10			0.14	0.63
RPC	1.1E-04	4.8E-04	1.1E-04	4.8E-04	5.5E-04	2.4E-03	1.1E-04	4.8E-04			1.1E-04	4.8E-04	1.1E-04	4.8E-04	1.1E-04	4.8E-04			6.6E-04	2.9E-03
PTE:	0.13	0.57	0.07	0.33	0.11	0.49	0.16	0.79	5.6E-03	0.02	0.21	0.95	0.03	0.14	0.08	0.39	0.01	0.05	0.82	3.74
WV-DEP:	2 <u>O</u> F	0.5	2 <u>O</u>	<u>R</u> 5	2 <u>O</u> F	<u>R</u> 0.5	2 <u>C</u>	<u>)R</u> 5	2 OF	8 5	2 O	R 5	2 O	R 5	2 O	R 5	2 O	R 5	2 0	R 5
Title V:		10		10		10		10		10		10		10		10		10		25

- Notes: 1 Emissions are based on operation at 100% of rated load for 8,760 hrs/yr.
  - 2 VOC is volatile organic compounds, as defined by EPA, and includes HCHO (formaldehyde).
  - 3 PM10/2.5 is filterable and condensable particulate matter; including PM10 and PM2.5.
  - 4 HCHO is formaldehyde
  - 5 Other HAP includes acetaldehyde, acrolein, and traces of othr Hazardous air pollutants.

#### YOHO COMPRESSOR STATION

#### Application for 45CSR13 NSR Modification Permit

# **Attachment N - Supporting Emissions Calculations**

#### **PRE-Controlled Emissions**

#### PRE-Controlled Potential to Emit (PTE) Summary - Criteria Polutants

Unit ID	Unit ID	Control	Description	Capacity	N(	Оx	С	0	VC	C	SC	Эx	PM10	0/2.5	CC	)2e
Official	ID	ID	Description	Сараспу	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
CE-01	1E	01-NSCR	Caterpillar Engine	203 bhp	7.42	32.48	7.42	32.48	0.17	0.73	1.1E-03	4.7E-03	0.04	0.15	240	1,052
RBV-1	2E	na	TEG Dehydrator - Reboiler	0.14 MMBtu/hr	0.01	0.06	0.01	0.05	7.5E-04	3.3E-03	8.2E-05	3.6E-04	1.0E-03	4.6E-03	16	72
RSV-1	3E	na	TEG Dehydrator - Flash Tank/Still Vent	2.0 MMscfd					5.15	22.55					160	700
T01	4E	na	Produced Water - Storage Tank	210 bbl					0.05	0.22						
TLO	5E	na	Produced Water - Truck Loadout	5,460 bbl/yr						0.55						
SSM	6E	na	Startup/Shutdown/Maintenance							1.53						108
FUG	7E	na	Piping and Equipment Fugitives						1.50	6.55					91	397
RPC	C 8E na Rod Packing/Crankcase Emissions							8.2E-04	3.6E-03					7.4E+01	3.2E+02	
•	1		TOTAL PTE:	7.43	32.54	7.43	32.53	6.86	32.13	1.2E-03	0.01	3.6E-02	0.16	581	2,653	
	WV-DEP Permit Threshold:			P Permit Threshold:	6 AI	ND 10	6 AN	ID 10	6 AN	ID 10	6 AN	ID 10	6 <u>AN</u>	<u>ID</u> 10	r	na

100

100

100

100

Title V Permit Threshold:

PRE-Controlled Potential to Emit (PTE) Summary - Hazardous Air Pollutants (HAPs)

Unit ID	Benz	zene	Ethylb	enzene	НСНО	(HAP)	n-He	xane	Meth	anol	Tolu	iene	2,2,4-	TMP	Xyle	enes	Other	HAP	Total	I HAP
Official	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
CE-01	2.9E-03	0.01	4.5E-05	2.0E-04	0.11	0.49			0.01	0.02	1.0E-03	4.5E-03			3.6E-04	1.6E-03	0.01	0.05	0.13	0.58
RBV-1	2.9E-07	1.3E-06			1.0E-05	4.5E-05	2.5E-04	1.1E-03			4.7E-07	2.0E-06					2.6E-07	1.1E-06	2.6E-04	1.1E-03
RSV-1	0.10	0.44	0.05	0.20			0.14	0.61			0.19	0.82	0.00	0.02	0.06	0.26			0.54	2.34
T01	0.00	0.01	0.00	0.01			0.00	0.01			0.00	0.01	0.00	0.01	0.00	0.01			0.01	0.03
TLO		0.01		0.01				0.01				0.01		0.01		0.01				0.08
SSM		2.0E-03		2.0E-03				0.05				2.0E-03		0.00		2.0E-03				0.06
FUG	0.02	0.10	0.02	0.10			0.02	0.10			0.02	0.10	0.02	0.10	0.02	0.10			0.14	0.63
RPC	1.1E-04	4.8E-04	1.1E-04	4.8E-04	5.5E-04	2.4E-03	1.1E-04	4.8E-04			1.1E-04	4.8E-04	1.1E-04	4.8E-04	1.1E-04	4.8E-04			6.6E-04	2.9E-03
PTE:	0.13	0.57	0.07	0.33	0.11	0.49	0.16	0.79	0.01	0.02	0.21	0.95	0.03	0.14	0.08	0.39	0.01	0.05	0.82	3.74
WV-DEP:	2 <u>O</u> F	0.5	2 <u>O</u>	<u>R</u> 5	2 <u>OF</u>	0.5	2 <u>C</u>	<u>)R</u> 5	2 0	R 5	2 O	R 5	2 0	R 5	2 C	)R 5	2 C	R 5	2 0	DR 5
Title V:		10		10		10		10		10		10		10		10		10		25

Notes: 1 - Emissions are based on operation at 100% of rated load for 8,760 hrs/yr.

- 2 VOC is volatile organic compounds, as defined by EPA, and includes HCHO (formaldehyde).
- 3 PM10/2.5 is filterable and condensable particulate matter; including PM10 and PM2.5.
- 4 HCHO is formaldehyde
- 5 Other HAP includes acetaldehyde, acrolein, and traces of othr Hazardous air pollutants.

100

na

#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### **Attachment N - Supporting Emissions Calculations**

# **Greenhouse Gas (GHG) Emissions**

#### Greenhouse Gas (GHG) Emissions Summary

Unit ID	Point ID	Control ID	Description	Heat Input MMBtu/hr (HHV)	Hours of Operation	kg/MMBtu: GWP: CO2	53.06 1 CO2e	kg/MMBtu: GWP: CH4	1.00E-03 25 CO2e	kg/MMBtu: GWP: N2O	1.00E-04 298 CO2e	TOTAL CO2e
					hr/yr	tpy	tpy	tpy	tpy	tpy	tpy	tpy
CE-01	1E	01-NSCR	Caterpillar Engine	1.82	8,760	1,002	1,002	2	50	1.8E-03	1	1,052
RBV-1	2E	na	TEG Dehydrator - Reboiler	0.14	8,760	72	72	1.4E-03	0.03	1.4E-04	0.04	72
RSV-1	3E	na	TEG Dehydrator - Flash Tank/Still		8,760			28	700			700
T01	4E	na	Produced Water - Storage Tank		8,760			0.9	22			22
TLO	5E	na	Produced Water - Truck Loadout		Intermittent							
SSM	6E	na	Startup/Shutdown/Maintenance		Intermittent			4	108			108
FUG	7E	na	Piping and Equipment Fugitives		8,760	0.1	0.1	16	397			397
RPC	8E	na	Rod Packing/Crankcase Emission		8,760	5	5	13	320			325

TOTAL FACILITY-WIDE PTE:	1,079		64		1.9E-03	] [	2,675
NNSR/PSD Threshold: (	na	- OR -	na	- OR -	na	) - AND -	na
Title V Major Source Threshold:	na		na		na		na

Notes: 1 - Emissions are based on operation at 100% of rated load.

- 2 Engine CO2 and CH4 emissions are based on vendor specifications.
- 3 Fugitive CH4 emissions are based on EPA Fugitive Emission Factors for Oil and Gas Production Operations.
- 4 All other GHG emissions are based on default values in 40CFR98, Subpart C, Table C-1.
- 5 High Heat Value (HHV) = Low Heat Value (LHV) / 0.90.

#### YOHO COMPRESSOR STATION

#### Application for 45CSR13 NSR Modification Permit

#### **Attachment N - Supporting Emissions Calculations**

#### Compressor Engine – 203 bhp CAT G3306TALE (4SRB w/ NSCR)

Unit	Description	Reference	Pollutant	Pre-Controlled Emissions			Control Efficiency	Controlled Emissions		
				g/bhp-hr	lb/hr	tpy	%	g/bhp-hr	lb/hr	tpy
	Caterpillar (CAT)	Vendor Data	NOx	16.57	7.42	32.48	88.0%	1.99	0.89	3.90
	G3306TALE (4SRB)	Vendor Data	CO	16.57	7.42	32.48	76.0%	3.98	1.78	7.80
	203 bhp	Vendor Data	THC	1.20	0.54	2.35		1.20	0.54	2.35
	1,800 rpm	Vendor Data	NMHC	0.18	0.08	0.35		0.18	0.08	0.35
	107 in3/cyl	Vendor Data	NMNEHC	0.12	0.05	0.24		0.12	0.05	0.24
		NMNEHC+HCHO	VOC	0.37	0.17	0.73		0.37	0.17	0.73
	Three-Way Catalyst (NSCR)	AP-42 Table 3.2-3	SOX	2.4E-03	1.1E-03	4.7E-03		2.4E-03	1.1E-03	4.7E-03
	NSPS JJJJ Affected	AP-42 Table 3.2-3	PM10/2.5	0.08	0.04	0.15		0.08	0.04	0.15
	NESHAP ZZZZ - No Req'ts	AP-42 Table 3.2-3	Benzene	0.01	2.9E-03	0.01		6.4E-03	2.9E-03	0.01
Compressor	Constructed ≥ 06/12/06	AP-42 Table 3.2-3	Ethylbenzene	1.0E-04	4.5E-05	2.0E-04		1.0E-04	4.5E-05	2.0E-04
Engine		Vendor Data	HCHO	0.25	0.11	0.49		0.25	0.11	0.49
05.04.(45)	8,760 hr/yr	AP-42 Table 3.2-3	n-Hexane							
CE-01 (1E)	920 Btu/scf (LHV)	AP-42 Table 3.2-3	Methanol	0.01	0.01	0.02		0.01	5.6E-03	0.02
	1,020 Btu/scf (HHV)	AP-42 Table 3.2-3	Toluene	2.3E-03	1.0E-03	4.5E-03		2.3E-03	1.0E-03	4.5E-03
	8,098 Btu/bhp-hr (LHV)	AP-42 Table 3.2-3	2,2,4-TMP							
	8,978 Btu/bhp-hr (HHV)	AP-42 Table 3.2-3	Xylene	8.0E-04	3.6E-04	1.6E-03		8.0E-04	3.6E-04	1.6E-03
	1.64 MMBtu/hr (LHV)	AP-42 Table 3.2-3	Other HAP	0.03	0.01	0.05		0.03	0.01	0.05
	1.82 MMBtu/hr (HHV)	SUM	Total HAP	0.30	0.13	0.58		0.30	0.13	0.58
	1,787 scf/hr	Vendor Data	CO2	511	229	1,002		511	229	1,002
	15.65 MMscf/yr	Vendor Data	CH4	1.02	0.46	2.00		1.02	0.46	2.00
	31.4% Nominal Efficiency	40CFR98 - Table C-2	N2O	9.0E-04	4.0E-04	1.8E-03		9.0E-04	4.0E-04	1.8E-03
		40CFR98 - Table A-1	CO2e	537	240	1,052		537	240	1,052

#### Notes:

- 1 The Pre-Controlled emissions are based on operation at 100% of rated load for 8,760 hrs/yr.
- 2 As per vendor specifications, NMNEHC (non-methane non-ethane hydrocarbon) does not include HCHO. VOC is the sum of NMNEHC and HCHO.
- 3 PM10/2.5 is filterable and condensable particulate matter; including PM10 and PM2.5
- 4 HCHO is formaldehyde.
- 5 Other HAP includes Acetaldehyde, Acrolein, 1,3-Butadiene, Chloride Methylene Chloride, and traces of other HAP.
- 6 The control efficiency (CE) for each HAP is assumed to be the same as the CE for NMNEHC, except for HCHO where the vendor provides specific data.
- 7 The fuel heating value will vary, 920 Btu/scf (LHV) is at the low end of the range and results in a high (conservative) fuel consumption estimate.
- 8 The emission estimates are based on operation at 100% of rated load.

#### YOHO COMPRESSOR STATION

#### Application for 45CSR13 NSR Modification Permit

#### **Attachment N - Supporting Emissions Calculations**

#### Dehydrator - 0.14 MMBtu/hr Reboiler

Unit ID	Description	Capacity	Reference	Pollutant		ssion ctor		ntrolled sions	Control Efficiency		rolled sions													
					lb/MMscf	lb/MMBtu	lb/hr	tpy	%	lb/hr	tpy													
			EPA AP-42 Table 1.4-1	NOx	100.00	0.10	0.01	0.06	na	0.01	0.06													
		Heat Input	EPA AP-42 Table 1.4-1	CO	84.00	0.08	0.01	0.05	na	0.01	0.05													
			EPA AP-42 Table 1.4-2	VOC	5.50	0.01	7.5E-04	3.3E-03	na	7.5E-04	3.3E-03													
		0.125	EPA AP-42 Table 1.4-2	SOx	0.60	5.9E-04	8.2E-05	3.6E-04	na	8.2E-05	3.6E-04													
		MMBtu/hr	EPA AP-42 Table 1.4-2	PM10/2.5	7.60	0.01	1.0E-03	4.6E-03	na	1.0E-03	4.6E-03													
		(LHV)	EPA AP-42 Table 1.4-3	Benzene	2.1E-03	2.1E-06	2.9E-07	1.3E-06	na	2.9E-07	1.3E-06													
			EPA AP-42 Table 1.4-3	Ethylbenzene																				
		0.140	EPA AP-42 Table 1.4-3	HCHO	0.08	7.4E-05	1.0E-05	4.5E-05	na	1.0E-05	4.5E-05													
	Reboiler 01 (RBV-1)	MMBtu/hr	EPA AP-42 Table 1.4-3	n-Hexane	1.80	1.8E-03	2.5E-04	1.1E-03	na	2.5E-04	1.1E-03													
RBV-1 (2E)		(HHV) 8,760		8,760	8,760	8,760	(HHV)	(HHV)	(HHV)	(HHV)	(HHV)	(HHV)	(HHV)	(HHV)	(HHV)	EPA AP-42 Table 1.4-3	Methanol							
	Reboiler Combustion Emissions																EPA AP-42 Table 1.4-3	Toluene	3.4E-03	3.3E-06	4.7E-07	2.0E-06	na	4.7E-07
							EPA AP-42 Table 1.4-3	2,2,4-TMP																
		hr/yr	EPA AP-42 Table 1.4-3	Xylenes																				
			EPA AP-42 Table 1.4-3	Other HAP	1.9E-03	1.9E-06	2.6E-07	1.1E-06	na	2.6E-07	1.1E-06													
			EPA AP-42 Table 1.4-3	Tot HAP	1.88	1.8E-03	2.6E-04	1.1E-03	na	2.6E-04	1.1E-03													
			40CFR98 - Table C-1	CO2	119,226	117	16	72	na	16	72													
			40CFR98 - Table C-2	CH4	2.25	2.2E-03	3.1E-04	1.4E-03	na	3.1E-04	1.4E-03													
			40CFR98 - Table C-2	N2O	0.22	2.2E-04	3.1E-05	1.4E-04	na	3.1E-05	1.4E-04													
			40CFR98 - Table A-1	CO2e	119,349	117	16	72	na	16	72													

Notes:

- 1 The combustion emission factors are based on a default fuel heat content of 1,020 Btu/scf (HHV).
- 2 PM10/2.5 is filterable and condensable particulate matter; including PM10 and PM2.5.
- 3 HCHO is formaldehyde.
- 4 Other HAP includes Acetaldehyde, Acrolein, 1,3-Butadiene, Chloride Methylene Chloride, and traces of other HAP.

#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### Attachment N

#### **Dehydrator - 2.0 MMscfd Capacity**

Unit ID	Description	Capacity	Reference	Pollutant		ssion		ntrolled ssions	Control Efficiency	Controlled Emissions	
					lb/MMscf	lb/MMBtu	lb/hr	tpy	%	lb/hr	tpy
			GRI-GLYCalc 4.0	VOC			5.15	22.55		5.15	22.55
			GRI-GLYCalc 4.0	Benzene			0.10	0.44		0.10	0.44
		Flow Rate	GRI-GLYCalc 4.0	Ethylbenzene			0.05	0.20		0.05	0.20
		2.0	GRI-GLYCalc 4.0	HCHO							
		MMscfd	GRI-GLYCalc 4.0	n-Hexane			0.14	0.61		0.14	0.61
			GRI-GLYCalc 4.0	Methanol							
RSV-1 (3E)	(Minimum of 50% of	8,760	GRI-GLYCalc 4.0	Toluene			0.19	0.82		0.19	0.82
	Flash Tank Off-Gas is Used as Reboiler Fuel)	hr/yr	GRI-GLYCalc 4.0	2,2,4-TMP			0.00	0.02		0.00	0.02
	Osed as Repoller Fuel)		GRI-GLYCalc 4.0	Xylenes			0.06	0.26		0.06	0.26
			GRI-GLYCalc 4.0	Other HAP							
			GRI-GLYCalc 4.0	Tot HAP			0.54	2.34		0.54	2.34
			GRI-GLYCalc 4.0	CH4			6	28		6	28
			40CFR98 - Table A-1	CO2e			160	700		160	700

Notes:

- 1 Dehydrator flash tank off-gases are usually burned as fuel in the reboiler. However, to be conservative, it is estimated 50% of the flash tank is vented to atmosphere.
- 2 To be conservative, and to account for potential future changes in gas quality, the following worst-case emissions were assumed:

2.0 MMscfd Dehydrator 01	GRI-GLYCalc 4.0* Model Results	Worst-Case Assumption (120%)		*Dehydrator Opera (See Attac	· ·	
VOC	18.79 tpy	22.55 tpy	Flow Rate:	2.0 MMscfd	Gas Analysis:	06/25/14
Benzene	0.36 tpy	0.44 tpy	Wet Gas Temperature:	70 oF	Flash Tank Temperature:	120 oF
Ethylbenzene	0.17 tpy	0.20 tpy	Wet Gas Presssure:	1,000 psig	Flash Tank Pressure:	60 psig
HCHO	tpy	tpy	Wet Gas Water Content:	Saturated	Flash Tank Off-Gas Control:	50% Recycle
n-Hexane	0.51 tpy	0.61 tpy	Dry Gas Water Content:	7.0 lb H2O/MMsc	f Stripping Gas:	na
Methanol	tpy	tpy	Lean Glycol Water Content:	1.5 wt% H2O	Stripping Gas:	na
Toluene	0.68 tpy	0.82 tpy	Glycol Pump:	Gas Injection	Regen Off-Gas Control:	na
2,2,4-TMP	0.02 tpy	0.02 tpy	Glycol Pump:	Kimray 4020PV	Condenser Temperature:	na
Xylenes	0.22 tpy	0.26 tpy	Lean Glycol Flow Rate:	0.67 gpm	Condenser Pressure:	na
Other HAP	tpy	tpy		Additional Mo	del Results:	
Total HAP	1.95 tpy	2.34 tpy	Regen Off-Gas Flow:	50 scfh	Wet Gas Water Conten	: 23.7 lb-H2O/MMscf
CH4	23.33 tpy	27.99 tpy	Flash Tank Off-Gas Flow:	334 scfh	Lean Glycol Recirc Ratio	: 21.1 gal/lb-H2O

<sup>3 -</sup> A 20% contingency has been added to the GRI-GLYCalc model results to account for potential future changes in gas quality.

#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### Attachment N - Supporting Emissions Calculations

#### **Produced Water Storage Tank**

Unit ID	Tank ID	per Year (Working and	ProMax VOC Emission Factor (Flashing Losses)	V	С	n-Hex, 2,2,4-Ti 2.50%	,	Total HAP							
			gal	bbl		gal/yr	bbl/yr	Breathing Losses)	(i labiling 20000)	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
T01 (4E)	Tank 01	Produced Water	8,820	210	26	229,320	5,460	0.039 lb/bbl	0.042 lb/bbl	0.05	0.22	0.00	0.01	0.01	0.03

TOTAL VOLUME:

8.820 210 229,320 5.460 26

**TOTAL EMISSIONS:** 

0.05 0.22 0.00 0.01 0.01 0.03

Unit ID	nit ID Tank ID Material Stored		Capa	city	Turnovers per Year	Throu	ghput	Methane Emission Factor (ProMax Model)	Methane		
			gal bbl		gal/yr	bbl/yr	, ,	lb/hr	tpy		
T01 (4E)	Tank 01	nk 01 Produced Water		210	26	229,320 5,460		0.326 lb/bbl	0.20	0.89	

**TOTAL VOLUME:** 

8,820 210 26 229,320 5,460 TOTAL EMISSIONS:

0.20 0.89

- Notes: 1 EPA-450/3-85-001a "Volatile Organic Compound Emissions from Petroleum Refinery Wastewater Systems Background Information for Proposed Standards" is a reasonable protocol for estimating potential produced water storage tank working and breathing losses. EPA-450/3-85-001a, page 3-39, gives a VOC emission factor of 420 kg/MMgal wastewater produced in an oil-water separator. (0.420 g/gal \* 0.0022 lb/g \* 42 gal/bbl = 0.039 lb/bbl)
  - 2 These emission estimates are nearly 4X more conservative than emission factors required by the TCEQ on the Barnett Shale produced water tanks at gas-only sites. (http://www.tceq.texas.gov/assets/public/implementation/air/ie/pseiforms/producedwaterstoragetank.pdf):

Table 1. Produced Water Storage Tank Flash Loss Emissions Factors for Barnett Shale Special Inventory Purposes ONLY

Pollutant	Average Produc	ed Water Emission Factor (lb/bbl)
	Gas Production Only Sites	Liquid Hydrocarbon and Gas Production Sites
VOC	0.01	0.0402
Benzene	0.0001	0.000054
Toluene	0.0003	0.000130
Ethylbenzene	0.000006	0.000003
Xylene(s)	0.00006	0.000049
n-Hexane	NA	0.000987

- 3 Total HAP is estimated at 30.0% of VOC emissions. This is a very conservative estimate based on an investigation of other produced water emission estimating protocols, as exemplified above (e.g., (0.0001+0.0003+0.00006+0.00006)/0.01 = 4.7%).
- 4 The ProMax simulation software is used to estimate flashing losses from the produced water storage tank.
- 5 To be conservative, the following liquid characteristics were assumed:

Pollutant	Light Liquid
1 Onutant	Estimated
Carbon Dioxide	Wgt%
Methane	Wgt%
VOC	100.00 Wgt%
Total HAP	15.00 Wgt%

#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### **Attachment N - Supporting Emissions Calculations**

#### **Produced Water Truck Load-Out**

I I with I ID	Description	s	Р	MW	т	CE	L	T-Put	voc	n-Hex, BTEX, 2,2,4-TMP (ea)	Total HAP
Unit ID	Description								AP-42 Sect 5.2	2.50% of VOC	15.00% of VOC
		sat. fac.	psia	lb/lb-mol	°R	%	lb/kgal	kgal/yr	tpy	tpy	tpy
TLO (5E)	Truck Load-Out	1.45	1.5	92	520	0.0%	4.79	229	0.55	0.01	0.08

Notes: 1 - Emission factors and formulas are from AP-42 Section 5.2 "Transportation and Marketing of Petroleum Liquids":

 $L_L = 12.46 \times S \times P \times MW / T \times (1 - CE)$ 

where:  $L_L = Loading loss, lb/1000 gal of liquid loaded.$ 

S = Saturation factor, use 1.45 for "splash loading".

P = True vapor pressure of liquid loaded, psia.

MW = molecular weight of vapors, lb/lb-mol. (Assumed MW of toluene as it has similar RVP and density as anticipated liquids.)

T = Temperature of bulk liquid loaded, °R = °F + 460. (Conservatively assumed 60 °F.)

CE = Overall emission reduction efficiency (collection efficiency x control efficiency).

2 - It is estimated that the tank will be emptied up to:

times per year.

3 - The total produced water storage tank capacity at the facility is:

4 - Emissions adjusted to account for the high-water/low-oil content in the produced water. Further, it is anticipated that the majority of VOC (and HAP) constituents will evaporate in the storage tanks and be de minimis or negligible in the truck load-out operations.

#### YOHO COMPRESSOR STATION

#### Application for 45CSR13 NSR Modification Permit

#### **Attachment N - Supporting Emissions Calculations**

#### Startup, Shutdown and Maintenance (SSM)

Unit ID	Description	No of Units	Total bhp	a. "Cold-S	Start" Gas	b. Blowd	lown Gas	Site-Wide SSM Events	Total Gas Vented
		<b>-</b>	Jp	scf/Unit	scf/SSM	scf/bhp	scf/SSM	SSM/yr	MMscf/yr
SSM (6E)	a. Cold-Start Engine	1	na	700	700	na	na	104	0.07
33W (0E)	b. Compressor Blowdown	1	203	na	na	6.22	1,262	104	0.13

	CO2	CH4	CO2e	VOC	Benzene	Ethylbenzene	n-Hexane	Toluene	2,2,4-TMP	Xylenes	Total HAP
Unit ID	250 lb/MMscf	42,275 lb/MMscf	1,057,125 lb/MMscf	15,000 lb/MMscf	20 lb/MMscf	20 lb/MMscf	500 lb/MMscf	20 lb/MMscf	20 lb/MMscf	20 lb/MMscf	600 lb/MMscf
	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy
SSM (6E)	0.01	2	38	0.55	7.3E-04	7.3E-04	0.02	7.3E-04	7.3E-04	7.3E-04	0.02
33W (6E)	0.02	3	69	0.98	1.3E-03	1.3E-03	0.03	1.3E-03	1.3E-03	1.3E-03	0.04
-											

TOTAL: 0.03 4 108 1.53 2.0E-03 2.0E-03 0.05 2.0E-03 2.0E-03 0.06

Notes:

- 1 SSM Emissions are the sum of:
  - a. Unburned fuel resulting from "cold-start" of idle gas-fired engine; and
  - b. Natural gas that is purged (aka blowdown) from the compressor and associated piping and equipment.
- 2 Starting gas quantity and blowdown (B-D) gas quantity as per engineering department. (e.g., 8,577 scf/B-D of a compressor with a 1,380 bhp engine equals 6.22 scf/bhp/B-D.)
- 3 To be conservative, the following gas characteristics were assumed:

Pollutant	Analysis	Assumed
CO2	178 lb/MMscf	250 lb/MMscf
CH4	32,986 lb/MMscf	42,275 lb/MMscf
VOC	11,935 lb/MMscf	15,000 lb/MMscf
Benzene	5 lb/MMscf	20 lb/MMscf
E-benzene	1 lb/MMscf	20 lb/MMscf
n-Hexane	262 lb/MMscf	500 lb/MMscf
Toluene	7 lb/MMscf	20 lb/MMscf
2,2,4-TMP	10 lb/MMscf	20 lb/MMscf
Xylenes	1 lb/MMscf	20 lb/MMscf
Total HAP	286 lb/MMscf	600 lb/MMscf
4. To be seened	the three COM actions to a second and	2.0

<sup>4 -</sup> To be conservative, these SSM estimates are based on

facility-wide blowdowns each week.

<sup>5 -</sup> This estimate of SSM emissions is sufficient to account for other infrequent and (often) de-minimis emissions from various activities (e.g., pig launching) at the facility that are not necessarily associated with compressor blowdowns.

#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

#### **Attachment N - Supporting Emissions Calculations**

#### Process Piping and Equipment Fugitives - Gas and Water/Oil

Unit Description	Description	Component (Unit) Type	Unit Count	THC Factor	Tot Hydro (TH		VC 25.00	OC Wgt%		X,TMP-ea Wgt%	Total 1.50	HAP Wgt%	0.45	D2 Wgt%	CI 100.00		CO GWP	
	(Gas)	Count	lb/hr/Unit	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	
		Valves	257	0.00992	2.55	11.17	0.64	2.79	6.4E-03	0.03	0.04	0.17	0.01	0.05	2.55	11.17	64	279
	Process Piping	Pump Seals																
FUG-G	and Equipment	Other	30	0.01940	0.58	2.55	0.15	0.64	1.5E-03	0.01	0.01	0.04	2.6E-03	0.01	0.58	2.55	15	64
(7E)	Fugitives	Connectors	737	0.00044	0.32	1.42	0.08	0.36	8.1E-04	0.00	0.00	0.02	1.5E-03	0.01	0.32	1.42	8	36
	(Gas)	Flanges	120	0.00086	0.10	0.45	0.03	0.11	2.6E-04	1.1E-03	1.5E-03	0.01	4.6E-04	2.0E-03	0.10	0.45	3	11
		Open-ended lines	14	0.00441	0.06	0.27	0.02	0.07	1.5E-04	6.8E-04	9.3E-04	0.00	2.8E-04	0.00	0.06	0.27	2	7
-	Total:		1,158		3.62	15.86	0.91	3.97	0.01	0.04	0.05	0.24	0.02	0.07	3.62	15.86	91	397

		Component	11	THC	Tot Hydro	ocarbons	VC	C	Hex,BTE	(,TMP(ea)	Total	HAP	CC	)2	CH	14	CO	)2e
Unit	Description	(Unit) Type	Unit Count	Factor	(TF	IC)	100.00	Wgt%	2.50	Wgt%	15.00	Wgt%		Wgt%		Wgt%	GWP	= 25
		(Light Liquid)	Count	lb/hr/Unit	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
		Valves	150	0.00022	0.03	0.14	0.03	0.14	8.1E-04	3.5E-03	4.9E-03	0.02						
	Process Piping	Pump Seals	5	0.00005	2.6E-04	1.2E-03	2.6E-04	1.2E-03	6.6E-06	2.9E-05	4.0E-05	1.7E-04						
FUG-W	and Equipment	Other	15	0.03086	0.46	2.03	0.46	2.03	0.01	0.05	0.07	0.30						
(7E)	Fugitives	Connectors	369	0.00024	0.09	0.39	0.09	0.39	2.2E-03	0.01	0.01	0.06						
	(Water/Oil)	Flanges	120	0.00001	7.7E-04	3.4E-03	7.7E-04	3.4E-03	1.9E-05	8.4E-05	1.2E-04	5.0E-04						
		Open-ended lines	7	0.00055	3.9E-03	0.02	3.9E-03	0.02	9.6E-05	4.2E-04	5.8E-04	2.5E-03						
		Total:	666		0.59	2.58	0.59	2.58	0.01	0.06	0.09	0.39						

TOTAL FUGITIVE EMISSIONS: 4.21 18.44 1.50 6.55 0.02 0.10 0.14 0.63 0.02 0.07 3.62 15.86 91 397

- Notes: 1 Assumed 8,760 hours per year of fugitive emissions.
  - 2 Component in Gas Service are based on GRI-HAPCalc estimates
  - 3 Water/Oil Component counts are estimated at 50%

of Gas Components, except valves and flanges which are estimated at 150 and 120, respectively.

4 - Gas and Water/Oil emissions calculated using EPA Protocol for Equipment Leak Emission Estimates, EPA-453/R-95-017, Nov 1995.

TABLE 2.4	G	as	Water/Oil			
O&G PROD (AVE)	kg/hr	lb/hr	kg/hr	lb/hr		
Valves	0.00450	0.00992	9.80E-05	0.00022		
Pump Seals	na	na	2.40E-05	0.00005		
Others	0.00880	0.01940	1.40E-02	0.03086		
Connectors	0.00020	0.00044	1.10E-04	0.00024		
Flanges	0.00039	0.00086	2.90E-06	0.00001		
Open-Ended Lines	0.00200	0.00441	2.50E-04	0.00055		

- 5 "Other" components include compressor seals, relief valves, diaphragms, drains, meters, etc.
- 5 To be conservative, the following gas asn water/oil characteristics were assumed:

Pollutant	Gas	(Inlet)	Water/Oil
Foliutalit	Analysis	Estimated	Estimated
Carbon Dioxide	0.32 Wgt%	0.45 Wgt%	Wgt%
Methane	59.11 Wgt%	100.00 Wgt%	Wgt%
VOC	21.39 Wgt%	25.00 Wgt%	100.00 Wgt%
n-Hex, BTEXm TMP (ea)	varies	0.25 Wgt%	2.50 Wgt%
Total HAP	0.51 Wgt%	1.50 Wgt%	15.00 Wgt%

#### YOHO COMPRESSOR STATION

#### Application for 45CSR13 NSR Modification Permit

#### **Attachment N - Supporting Emissions Calculations**

#### Compressor Rod Packing Leaks and Engine Crankcase Leaks (RPC)

#### Compressor Rod Packing Leaks (Natural Gas)

	No. of	Cyl per			T-1-1	VC	C	HC	НО	nex, bit	•	Total	HAP	CC	)2	CH	14	СО	2e
Unit Description	Recip	Recip	scfh per	Contin-	Total Leak Rate	15,0	000	-		10		60	0	25	60	42,2	275	CH4 GV	VP = 25
	Comp-	Comp- Cylinder	Cylinder gency		Ib/MI	<b>Mscf</b>	lb/MI	Mscf	Ib/MI	Viscf	lb/MI	Viscf	Ib/MI	Viscf	Ib/MI	Mscf	lb/MI	Viscf	
	ressors	ressor			MMscf/yr	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Compressor Rod Packing	1	4.0	15	15%	0.60											2.92	12.78	73	319

#### **Engine Crankcase Emissions (Combustion Gas)**

	CE-01 Horsepower	Leak Rate		V	C	HC	НО	Hex, BTE	X, TMP-Ea	Total	HAP	CC	)2	СН	4	СО	)2e
Unit Description		0.50	Safety	8.	06	5.	45	1.	08	6.	50	11,1	135	22	2	CH4 GV	NP = 25
		scf/bhp-hr F	Factor	lb/M	Mscf	lb/M	Mscf	lb/M	Mscf	Ib/MI	Mscf	lb/MI	Viscf	Ib/MN	<b>Iscf</b>	lb/MI	Mscf
	(bhp)	MMscf/yr		lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Engine Crankcase	203	0.89	250%	8.2E-04	3.6E-03	5.5E-04	2.4E-03	1.1E-04	4.8E-04	6.6E-04	2.9E-03	1	5	2.3E-03	0.01	1	5

**Total Plant-Wide RPC Emissions:** 

8.2E-04 3.6E-03	5.5E-04 2.4E-03	1.1E-04 4.8E-04	6.6E-04 2.9E-03	1 5	3 13	74 325

#### Notes:

- 1 Misc. equipment leaks is a broad category covering leaks of natural gas from sealed surfaces, such as packing and gaskets, resulting from the wear of mechanical joints, seals, and rotating surfaces over time. It also includes the crankcase emissions from reciprocating engines.
- 2 To be conservative, and to account for potential future changes, the following "worst-case" Residue gas characteristics were assumed:

Pollutant	Representative Gas Analysis	Worst-Case Assumption
VOC	11,935 lb/MMscf	15,000 lb/MMscf
Total HAP	286 lb/MMscf	600 lb/MMscf
CH4	32,986 lb/MMscf	42,275 lb/MMscf
CO2	178 lb/MMscf	250 lb/MMscf

- 3 Estimates of Recip Compressor Leaks are based on vendor data w/ an appropriate contingency.
- 4 Engine crankcase emissions are based on vendor data: "As a general rule, blow-by (i.e., crankcase emissions) on a <u>new</u> engine is approximately 0.5 scf/bhp-hr." A "safety factor" is used to account for increasing blow-by as the engines "wear".

5 - Crankcase emissions, from compressor engine (CE-01 (1E)), are estimated as follows:

(Data from CAT G3306TA Data Sheet and Emissions Calculation Spreadsheet.)

Tot Engine Exhaust (TEEx) (Vol)	988 acf/min	180 MMscf/yr TEEx*
<u>Pollutant</u>	GE-01 PTE	Crankcase Emission Factor**
Crankcase THC emissions (Mass)	2.35 tpy THC	26.15 lb THC / MMscf TEEx
Crankcase VOC emissions (Mass)	0.73 tpy VOC	8.06 lb VOC / MMscf TEEx
Crankcase HCHO emissions (Mass)	0.49 tpy HCHO	5.45 lb HCHO / MMscf TEEx
Crankcase BTEX (ea) emissions (Mass)	0.02 tpy BTEX	0.17 lb BTEX / MMscf TEEx
Crankcase HAP (tot) emissions (Mass)	0.58 tpy HAP	6.50 lb HAP / MMscf TEEx
Crankcase CO2 emissions (Mass)	1,002 tpy CO2	11,135 lb CO2 / MMscf TEEx
Crankcase CH4 emissions (Mass)	2 tpy CH4	22 lb CH4 / MMscf TEEx
Crankcase N2O emissions (Mass)	1.8E-03 tpy N2O	0 lb CH4 / MMscf TEEx
Crankcase CO2e emissions (Mass)	1,052 tpy CO2e	11,697 lb CO2e /MMscf TEEx

 $<sup>^{\</sup>star}$  Conversion from acf/min to scf/yr based on 8,760 hr/yr, 1,064 oF exhaust temp, and 68 oF std temp.

<sup>\*\*</sup> Crankcase EmFact = PTE (tpy) from a G3306TA Engine ÷ Tot Engine Exhaust (TEEx) (MMsf/yr).

#### **AP-42 and GHG EMISSION FACTORS**

(Preferentially use test data or vendor data where available)

		(	cicicitially asc test date		,		
			GAS-FIRED ENGINES			GAS-FIRED TURBINE	S
	Pollutant	<u>AP-42 1</u>	Table 3.2-1; 3.2-2; 3.2-3	<u>3 07/00</u>	<u>AP-42 T</u>	<u>able 3.1-1; 3.1-2a; 3.1-</u>	<u>3 04/00</u>
	Pollutarit	2SLB	4SLB	4SRB	Uncontrolled	Water Injection	Lean Pre-Mix#
		lb/MMBtu	lb/MMBtu	lb/MMBtu	lb/MMBtu	lb/MMBtu	lb/MMBtu
	NOX (≥ 90% Load)	3.17E+00	4.08E+00	2.21E+00	3.20E-01	1.30E-01	9.90E-02
	CO (≥ 90% Load)	3.86E-01	3.17E-01	3.72E+00	8.20E-02	3.00E-02	1.50E-02
≤	THC (TOC)	1.64E+00	1.47E+00	3.58E-01	1.10E-02	1.10E-02	1.10E-02
ER	NMHC (THC-CH4)	1.90E-01	2.20E-01	1.28E-01	2.40E-03	2.40E-03	2.40E-03
CRITERIA	NMNEHC (NMHC-C2H6)	1.19E-01	1.15E-01	5.76E-02	2.10E-03	2.10E-03	2.10E-03
Ö	VOC	1.20E-01	1.18E-01	2.96E-02	2.10E-03	2.10E-03	2.10E-03
	SO2*** (2,000 gr-S/MMscf)	5.88E-04	5.88E-04	5.88E-04	5.88E-04	5.88E-04	5.88E-04
	PM10/2.5 (Filter+Cond)	4.83E-02	9.99E-03	1.94E-02	6.60E-03	6.60E-03	6.60E-03
	Benzene	1.94E-03	4.40E-04	1.58E-03	1.20E-05	1.20E-05	9.10E-07
	Ethylbenzene	1.08E-04	3.97E-05	2.48E-05	3.20E-05	3.20E-05	3.20E-05
	Formaldehyde (HCHO)	5.52E-02	5.28E-02	2.05E-02	7.10E-04	7.10E-04	2.00E-05
S	n-Hexane	4.45E-04	1.11E-03				
HAPs	Methanol	2.48E-03	2.50E-03	3.06E-03			
	Toluene	9.63E-04	4.08E-04	5.58E-04	1.30E-04	1.30E-04	1.30E-04
	TMP, 2,2,4- (i-Octane)	8.46E-04	2.50E-04				
	Xylenes	2.68E-04	1.84E-04	1.95E-04	6.40E-05	6.40E-05	6.40E-05
	Other HAPs	1.72E-02	1.44E-02	6.36E-03	1.06E-04	1.06E-04	1.06E-04
	CO2**** (GWP=1)	1.17E+02	1.17E+02	1.17E+02	1.17E+02	1.17E+02	1.17E+02
GHG	CH4 (GWP=25)	1.45E+00	1.25E+00	2.30E-01	8.60E-03	8.60E-03	8.60E-03
ᅙ	N2O (GWP=298)	2.20E-04	2.20E-04	2.20E-04	3.00E-03	3.00E-03	3.00E-03
	CO2e	1.53E+02	1.48E+02	1.23E+02	1.18E+02	1.18E+02	1.18E+02

(#Lean Pre-Mix - aka: Dry Low Emissions (DLE or DLN) and SoLoNOX)

		GAS-FIF	RED EXTERNAL COME	BUSTION	FLARES	DIESEL ENGINES
	Belledont	AP-42 Table 1.4	-1; 1.4-2; 1.4-3 (<100 N	IMBtu/hr) 07/98	<u>13.5-1 01/95</u>	3.3-1; 3.3-2 10/96
	Pollutant	Uncontrolled	LoNOX Burners	Flue Gas Recirc	(Combustion)	Uncontrolled
		lb/MMBtu	lb/MMBtu	lb/MMBtu	lb/MMBtu	lb/MMBtu
	NOX	9.80E-02	4.90E-02	3.14E-02	6.80E-02	4.41E+00
	CO	8.24E-02	8.24E-02	8.24E-02	3.70E-01	9.50E-01
≤	THC (TOC)	1.08E-02	1.08E-02	1.08E-02	1.40E-01	3.60E-01
CRITERIA	NMHC (THC-CH4)	8.53E-03	8.53E-03	8.53E-03	1.38E-01	3.53E-01
Ε	NMNEHC (NMHC-C2H6)	5.49E-03	5.49E-03	5.49E-03	5.49E-03	3.50E-01
ਹ	VOC	5.56E-03	5.56E-03	5.56E-03	5.56E-03	3.60E-01
	SO2 (2,000 gr-S/MMscf)	5.88E-04	5.88E-04	5.88E-04	5.88E-04	2.90E-01
	PM10/2.5 (Filter+Condense)	7.45E-03	7.45E-03	7.45E-03	7.45E-03	3.10E-01
	Benzene	2.06E-06	2.06E-06	2.06E-06	2.06E-06	9.33E-04
	Ethylbenzene					
	HCHO (Formaldehyde)	7.35E-05	7.35E-05	7.35E-05	7.35E-05	1.18E-03
S	n-Hexane	1.76E-03	1.76E-03	1.76E-03	1.76E-03	
HAPs	Methanol					
	Toluene	3.33E-06	3.33E-06	3.33E-06	3.33E-06	4.09E-04
	2,2,4-TMP (i-Octane)					
	Xylenes					2.85E-04
	Other HAPs	1.86E-06	1.86E-06	1.86E-06	1.86E-06	1.05E-03
	CO2 (GWP=1)	1.18E+02	1.18E+02	1.18E+02	1.18E+02	1.64E+02
GHG	CH4 (GWP=25)	2.25E-03	2.25E-03	2.25E-03	2.25E-03	6.61E-03
Ġ	N2O (GWP=298)	2.16E-03	6.27E-04	6.27E-04	2.16E-03	1.32E-03
	CO2e	1.18E+02	1.18E+02	1.18E+02	1.18E+02	1.65E+02

40 CFR 98 - DEFAULT EMISSION FACTORS								
	Table C-1 to Sub	opart C of Part 98	Table C-2 to Subpart C of Part 98					
Fuel Type	Default HHV	Carbon Dioxide	Methane	Nitrous Oxide				
	Delault HHV	lb CO2/MMBtu	lb CH4/MMBtu	lb N2O/MMBtu				
Fuel Oil No. 2 (Diesel)	0.138 MMBtu/gal	1.61E+02	6.61E-03	1.32E-03				
Natural Gas	1,026 Btu/scf	1.17E+02	2.20E-03	2.20E-04				

Global Warming Potential (100 Yr) (GWP)									
Table A-1 to Subpart A of Part 98									
CO2	CH4*	N2O#							
1	1 25 298								
	"D : II E	DA 44/00/40							

<sup>#</sup>Revised by EPA on 11/29/13

#### Conversion Factors

Conversion Factors			
http://www.on	lineconversion.com/		
1.0 lb =	453.592 g		
1.0 kg =	2.205 lb		
1.0 hp =	2,544.433 Btu/hr		
1.0 hp =	745.700 Watt		
1.0 kW =	3,412.142 Btu/hr		
1.0 kW-hr =	1.340 hp-hr		
1.0 cf =	7.481 gal		
.0 gal H2O =	8.338 gal		
1.0 cf H2O =	62.371 gal		
1.0 m =	3.281 gal		
1.0 km =	0.621 gal		
1.0 acre =	43560.174 gal		
1.0 °F =	(°C*9/5)+32		
$1.0  {}^{\circ}R =$	°F+459.67		
1.0 % =	10,000 ppm		
UGC (stp) =	379.48 scf/lb-mol		

 $<sup>^{\</sup>star}$ Converted Ext Comb Emission Factors to lb/MMBtu by dividing lb/MMscf by AP-42 default HHV of 1,020 Btu/scf.

<sup>\*\*</sup>Converted GHG Emission Factors to lb/MMBtu by multiplying kg/MMBtu by 2.2046 lb/kg.

<sup>\*\*\*</sup>Assumes 100% conversion of fuel sulfur to SO2 (2,000 gr/MMscf).

<sup>\*\*\*\*\*</sup>Assumes 99.5% conversion of fuel carbon to CO2 for natural gas.

#### GRI-GLYCalc VERSION 4.0 - EMISSIONS SUMMARY

Case Name: Yoho CS - 2 MMscfd TEG Dehydrator

File Name: C:\projects2\wfs\OVM\Yoho\R13 Application #2\00 - Att-Nb - Yoho - NSR -

GRIGLYCalc - 05.15.15.ddf Date: May 15, 2015

#### UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane Ethane Propane	0.0800 0.1101 0.1399	1.920 2.643 3.358	0.3504 0.4823 0.6128
Isobutane n-Butane	0.1355 0.0360 0.1215	0.863 2.915	0.1575 0.5321
Isopentane n-Pentane n-Hexane Cyclohexane Heptanes	0.0394 0.0628 0.0467 0.0390 0.0281	0.946 1.508 1.122 0.936 0.674	0.1726 0.2751 0.2047 0.1709 0.1231
2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene Xylenes C8+ Heavies	0.0015 0.0790 0.1515 0.0376 0.0485	0.036 1.895 3.636 0.903 1.165	0.0065 0.3459 0.6636 0.1647 0.2126
Total Emissions	2.1209	50.903	9.2897
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	2.1209 1.9308 0.3648 0.3166	50.903 46.340 8.756 7.599	9.2897 8.4570 1.5980 1.3868

#### FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	5.2456	125.894	5.1688
Ethane	1.9263	46.231	
Propane	1.1801	28.322	
Isobutane	0.1946	4.669	
n-Butane	0.4971	11.931	
Isopentane	0.1384	3.321	0.6060
n-Pentane	0.1746	4.192	0.7650
n-Hexane	0.0692	1.662	0.3033
Cyclohexane	0.0139	0.334	0.0610
Heptanes	0.0194	0.466	0.0850
2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene Xylenes	0.0021 0.0040 0.0047 0.0007 0.0006	0.050 0.096 0.114 0.016 0.014	0.0029 0.0026
C8+ Heavies Total Emissions	0.0607  9.5320	1.456 228.768	0.2658 41.7501
Total Hydrocarbon Emissions	9.5320	228.768	41.7501
Total VOC Emissions	2.3601	56.642	10.3372

			Page: 2
Total HAP Emissions	0.0813	1.951	0.3561
Total BTEX Emissions	0.0100	0.239	0.0437

#### FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Methane	10.4912	251.788	45.9513
Ethane	3.8526	92.463	16.8745
Propane	2.3602	56.644	10.3376
Isobutane	0.3891	9.339	1.7043
n-Butane	0.9943	23.862	4.3549
Isopentane	0.2767	6.641	1.2120
n-Pentane	0.3493	8.383	1.5299
n-Hexane	0.1385	3.324	0.6066
Cyclohexane	0.0279	0.669	0.1220
Heptanes	0.0388	0.931	0.1699
2,2,4-Trimethylpentane	0.0041	0.099	0.0181
Benzene	0.0080	0.192	0.0350
Toluene	0.0095	0.227	0.0415
Ethylbenzene	0.0013	0.031	0.0057
Xylenes	0.0012	0.028	0.0052
C8+ Heavies	0.1214	2.913	0.5316
Total Emissions	19.0640	457.535	83.5002
Total Hydrocarbon Emissions	19.0640	457.535	83.5002
Total VOC Emissions	4.7202	113.284	20.6744
Total HAP Emissions	0.1626	3.902	0.7121
Total BTEX Emissions	0.0200	0.479	0.0874

#### COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	5.3256	127.814	23.3261
Ethane	2.0364	48.874	8.9195
Propane	1.3200	31.680	5.7816
Isobutane n-Butane		5.533 14.847	1.0097
Isopentane	0.1778		0.7786
n-Pentane	0.2375		1.0401
n-Hexane	0.1160		0.5080
Cyclohexane	0.0529		0.2319
Heptanes	0.0475	1.140	0.2080
2,2,4-Trimethylpentane	0.0036	0.085	0.0156
Benzene	0.0830	1.991	0.3634
Toluene	0.1563	3.750	0.6844
Ethylbenzene		0.918	0.1676
Xylenes		1.179	0.2151
C8+ Heavies		27.840	5.0807
Total Emissions	11.6529	279.670	51.0398
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	11.6529 4.2909 0.4461 0.3266	102.982	18.7942

#### GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES

Case Name: Yoho CS - 2 MMscfd TEG Dehydrator

File Name: C:\projects2\wfs\OVM\Yoho\R13 Application #2\00 - Att-Nb - Yoho - NSR -

GRIGLYCalc - 05.15.15.ddf Date: May 15, 2015

DESCRIPTION:

\_\_\_\_\_

Description: Wet Gas: 70 oF, 1,000 psig

Pump: Gas Injection, 0.67 gpm

Flash Tank: 120oF, 60 psig, 50% Recycle

Annual Hours of Operation: 8760.0 hours/yr

WET GAS:

Temperature: 70.00 deg.
1000.00 psig 70.00 deg. F

Wet Gas Water Content: Saturated

Component	Conc. (vol %)
Carbon Dioxide	0.1537
Nitrogen	0.4580
Methane	78.0288
Ethane	13.0780
Propane	5.1090
Isobutane	0.6003
n-Butane	1.4055
Isopentane	0.3321
n-Pentane	0.3827
n-Hexane	0.1154
Cyclohexane	0.0130
Heptanes	0.0252
2,2,4-Trimethylpentane	0.0033
Benzene	0.0022
Toluene	0.0027
Ethylbenzene	0.0005
Xylenes	0.0005
C8+ Heavies	0.2880

DRY GAS:

Flow Rate: 2.0 MMSCF/day Water Content: 7.0 lbs. H2O/MMSCF

LEAN GLYCOL:

\_\_\_\_\_\_

Glycol Type: TEG

Water Content: 1.5 wt% H2O Flow Rate: 0.7 gpm

PUMP:

Page: 2

Glycol Pump Type: Gas Injection Gas Injection Pump Volume Ratio: 0.080 acfm gas/gpm glycol

FLASH TANK:

\_\_\_\_\_\_

Flash Control: Combustion device
Flash Control Efficiency: 50.00 %
Temperature: 120.0 deg. F
Pressure: 60.0 psig

>50% Recycle

Page: 1

#### GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: Yoho CS - 2 MMscfd TEG Dehydrator

File Name: C:\projects2\wfs\OVM\Yoho\R13 Application #2\00 - Att-Nb - Yoho - NSR -

GRIGLYCalc - 05.15.15.ddf Date: May 15, 2015

#### DESCRIPTION:

Description: Wet Gas: 70 oF, 1,000 psig

Pump: Gas Injection, 0.67 gpm

Flash Tank: 120oF, 60 psig, 50% Recycle

Annual Hours of Operation: 8760.0 hours/yr

#### EMISSIONS REPORTS:

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#### UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.0800	1.920	0.3504
Ethane	0.1101	2.643	0.4823
Propane Isobutane	0.1399	3.358	0.6128
n-Butane	0.0360 0.1215	0.863 2.915	0.1575 0.5321
II-Bucane	0.1215	2.915	0.5321
Isopentane	0.0394	0.946	0.1726
n-Pentane	0.0628	1.508	0.2751
n-Hexane	0.0467	1.122	0.2047
Cyclohexane	0.0390	0.936	0.1709
Heptanes	0.0281	0.674	0.1231
2,2,4-Trimethylpentane	0.0015	0.036	0.0065
Benzene	0.0790	1.895	0.3459
Toluene	0.1515	3.636	0.6636
Ethylbenzene	0.0376	0.903	0.1647
Xylenes	0.0485	1.165	0.2126
C8+ Heavies	1.0993	26.383	4.8149
Total Emissions	2.1209	50.903	9.2897
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	2.1209 1.9308 0.3648 0.3166	50.903 46.340 8.756 7.599	9.2897 8.4570 1.5980 1.3868
TOCAL DILL LINIBBIONS	0.5100	,	1.5500

#### FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	5.2456	125.894	22.9757
Ethane	1.9263	46.231	8.4372
Propane	1.1801	28.322	5.1688
Isobutane	0.1946	4.669	0.8522
n-Butane	0.4971	11.931	2.1774
Isopentane	0.1384	3.321	0.6060
n-Pentane	0.1746	4.192	0.7650
n-Hexane	0.0692	1.662	0.3033
Cyclohexane	0.0139	0.334	0.0610
Heptanes	0.0194	0.466	0.0850

			Page: 2
2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene Xylenes  C8+ Heavies	0.0021	0.050	0.0091
	0.0040	0.096	0.0175
	0.0047	0.114	0.0208
	0.0007	0.016	0.0029
	0.0006	0.014	0.0026
Total Emissions	9.5320	228.768	41.7501
Total Hydrocarbon Emissions	9.5320	228.768	41.7501
Total VOC Emissions	2.3601	56.642	10.3372
Total HAP Emissions	0.0813	1.951	0.3561
Total BTEX Emissions	0.0100	0.239	0.0437

#### FLASH TANK OFF GAS

Component	lbs/nr	lbs/day	tons/yr
Methane	10.4912	251.788	45.9513
	3.8526		
Propane	2.3602	56.644	
Isobutane		9.339	
n-Butane	0.9943	23.862	4.3549
Isopentane	0.2767	6.641	1.2120
n-Pentane	0.3493		
n-Hexane	0.1385		
Cyclohexane	0.0279		
Heptanes	0.0388	0.931	0.1699
2,2,4-Trimethylpentane	0.0041	0.099	0.0181
Benzene	0.0080	0.192	0.0350
Toluene	0.0095	0.227	0.0415
Ethylbenzene	0.0013	0.031	0.0057
Xylenes	0.0012	0.028	0.0052
C8+ Heavies	0.1214	2.913	0.5316
Total Emissions	19.0640	457.535	83.5002
Total Hydrocarbon Emissions	19.0640	457.535	83.5002
Total VOC Emissions	4.7202	113.284	20.6744
Total HAP Emissions	0.1626	3.902	0.7121
Total BTEX Emissions	0.0200	0.479	0.0874

#### COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	5.3256	127.814	23.3261
Ethane	2.0364	48.874	8.9195
Propane	1.3200	31.680	5.7816
Isobutane	0.2305	5.533	1.0097
n-Butane	0.6186	14.847	2.7095
Isopentane	0.1778	4.267	0.7786
n-Pentane	0.2375	5.699	1.0401
n-Hexane	0.1160	2.784	0.5080
Cyclohexane	0.0529	1.271	0.2319
Heptanes	0.0475	1.140	0.2080
2,2,4-Trimethylpentane	0.0036	0.085	0.0156
Benzene	0.0830	1.991	0.3634
Toluene	0.1563	3.750	0.6844

Ethylbenzene Xylenes	0.0383 0.0491	0.918 1.179	Page: 3 0.1676 0.2151
C8+ Heavies	1.1600	27.840	5.0807
Total Emissions	11.6529	279.670	51.0398
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	11.6529 4.2909 0.4461 0.3266	279.670 102.982 10.707 7.838	51.0398 18.7942 1.9541 1.4305

#### COMBINED REGENERATOR VENT/FLASH GAS EMISSION CONTROL REPORT:

Component	Uncontrolled tons/yr	Controlled tons/yr	% Reduction
Methane	46.3017	23.3261	49.62
Ethane	17.3568	8.9195	48.61
Propane	10.9504	5.7816	47.20
Isobutane	1.8619	1.0097	45.77
n-Butane	4.8870	2.7095	44.56
Isopentane	1.3847	0.7786	43.77
n-Pentane	1.8050	1.0401	42.38
n-Hexane	0.8113	0.5080	37.38
Cyclohexane	0.2929	0.2319	20.83
Heptanes	0.2930	0.2080	29.00
2,2,4-Trimethylpentane Benzene Toluene Ethylbenzene Xylenes C8+ Heavies	0.0246 0.3808 0.7051 0.1705 0.2177	0.0156 0.3634 0.6844 0.1676 0.2151	36.81 4.59 2.94 1.69 1.19
Total Emissions	92.7899	51.0398	44.99
Total Hydrocarbon Emissions	92.7899	51.0398	44.99
Total VOC Emissions	29.1314	18.7942	35.48
Total HAP Emissions	2.3101	1.9541	15.41
Total BTEX Emissions	1.4742	1.4305	2.96

EQUI PMENT.	REPORTS:			

ABSORBER

 ${\tt NOTE:}$  Because the Calculated Absorber Stages was below the minimum allowed, GRI-GLYCalc has set the number of Absorber Stages to 1.25 and has calculated a revised Dry Gas Dew Point.

Calculated Absorber Stages: 1.25
Calculated Dry Gas Dew Point: 0.80 lbs. H2O/MMSCF

Temperature: 70.0 deg. F
Pressure: 1000.0 psig
Dry Gas Flow Rate: 2.0000 MMSCF/day

Page: 4

Glycol Losses with Dry Gas: 0.0202 lb/hr

Wet Gas Water Content: Saturated

Calculated Wet Gas Water Content: 23.65 lbs. H2O/MMSCF Calculated Lean Glycol Recirc. Ratio: 21.10 gal/lb H2O

Component	Remaining in Dry Gas	Absorbed in Glycol
Water	3.37%	96.63%
Carbon Dioxide	99.41%	0.59%
Nitrogen	99.95%	0.05%
Methane	99.96%	0.04%
Ethane	99.89%	0.11%
Propane	99.84%	0.16%
Isobutane	99.79%	0.21%
n-Butane	99.72%	0.28%
Isopentane	99.74%	0.26%
n-Pentane	99.67%	0.33%
n-Hexane	99.50%	0.50%
Cyclohexane	97.56%	2.44%
Heptanes	99.14%	0.86%
2,2,4-Trimethylpentane	99.67%	0.33%
Benzene	77.32%	22.68%
Toluene	70.90%	29.10%
Ethylbenzene	66.99%	33.01%
Xylenes	57.73%	42.27%
C8+ Heavies	99.21%	0.79%

#### FLASH TANK

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Flash Control: Combustion device
Flash Control Efficiency: 50.00 %
Flash Temperature: 120.0 deg. F
Flash Pressure: 60.0 psig

Component	Left in Glycol	Removed in Flash Gas
Water	99.78%	0.22%
Carbon Dioxide	8.61%	91.39%
Nitrogen	0.74%	99.26%
Methane	0.76%	99.24%
Ethane	2.78%	97.22%
Propane	5.60%	94.40%
Isobutane	8.46%	91.54%
n-Butane	10.89%	89.11%
Isopentane	12.65%	87.35%
n-Pentane	15.45%	84.55%
n-Hexane	25.46%	74.54%
Cyclohexane	59.52%	40.48%
Heptanes	42.21%	57.79%
2,2,4-Trimethylpentane	26.93%	73.07%
Benzene	91.27%	8.73%
Toluene	94.57%	5.43%
Ethylbenzene	96.98%	3.02%
Xylenes	97.93%	2.07%
C8+ Heavies	90.92%	9.08%

No Stripping Gas used in regenerator.

Component	Remaining in Glycol	Distilled Overhead
Water Carbon Dioxide Nitrogen Methane Ethane	74.88% 0.00% 0.00% 0.00% 0.00%	100.00%
Propane Isobutane n-Butane Isopentane n-Pentane	0.00% 0.00% 0.00% 1.68% 1.59%	100.00%
n-Hexane Cyclohexane Heptanes 2,2,4-Trimethylpentane Benzene	1.17% 4.73% 0.85% 2.76% 5.40%	98.83% 95.27% 99.15% 97.24% 94.60%
Toluene Ethylbenzene Xylenes C8+ Heavies	8.26% 10.63% 13.09% 9.52%	91.74% 89.37% 86.91% 90.48%

#### STREAM REPORTS:

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#### WET GAS STREAM

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Temperature: 70.00 deg. F Pressure: 1014.70 psia Flow Rate: 8.34e+004 scfh

Component		Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	4.98e-002 1.54e-001 4.58e-001 7.80e+001 1.31e+001	1.49e+001 2.82e+001 2.75e+003
Isobutane n-Butane Isopentane	5.11e+000 6.00e-001 1.40e+000 3.32e-001 3.83e-001	7.67e+001 1.80e+002 5.27e+001
Cyclohexane Heptanes 2,2,4-Trimethylpentane	2.52e-002	2.40e+000 5.55e+000 8.28e-001
Ethylbenzene	5.00e-004	1.17e-001 1.17e-001

Total Components 100.00 4.66e+003

#### DRY GAS STREAM

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Temperature: 70.00 deg. F Pressure: 1014.70 psia Flow Rate: 8.33e+004 scfh

Component Conc. Loading (vol%) (lb/hr) -----Water 1.68e-003 6.66e-002 Carbon Dioxide 1.53e-001 1.48e+001 Nitrogen 4.58e-001 2.82e+001 Methane 7.81e+001 2.75e+003 Ethane 1.31e+001 8.63e+002 Propane 5.10e+000 4.94e+002 Isobutane 5.99e-001 7.65e+001 n-Butane 1.40e+000 1.79e+002 Isopentane 3.31e-001 5.25e+001 n-Pentane 3.82e-001 6.05e+001 n-Hexane 1.15e-001 2.17e+001 Cyclohexane 1.27e-002 2.35e+000 Heptanes 2.50e-002 5.50e+000 2,2,4-Trimethylpentane 3.29e-003 8.26e-001 Benzene 1.70e-003 2.92e-001 Toluene 1.92e-003 3.88e-001 Ethylbenzene 3.35e-004 7.82e-002 Xylenes 2.89e-004 6.74e-002 C8+ Heavies 2.86e-001 1.07e+002 Total Components 100.00 4.66e+003

#### LEAN GLYCOL STREAM

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Temperature: 70.00 deg. F Flow Rate: 6.70e-001 gpm

Component		Loading (lb/hr)
Water Carbon Dioxide Nitrogen	9.85e+001 1.50e+000 2.32e-012 3.59e-013 9.56e-018	5.66e+000 8.74e-012 1.35e-012
Propane Isobutane	1.22e-007 8.53e-009 1.28e-009 3.26e-009 1.79e-004	3.22e-008 4.81e-009 1.23e-008
n-Hexane Cyclohexane	6.36e-005	5.51e-004 1.94e-003 2.40e-004
Toluene Ethylbenzene	1.20e-003 3.62e-003 1.19e-003 1.94e-003	1.36e-002 4.47e-003

Total Components 100.00 3.77e+002

#### RICH GLYCOL AND PUMP GAS STREAM

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Temperature: 70.00 deg. F Pressure: 1014.70 psia Flow Rate: 7.21e-001 gpm

NOTE: Stream has more than one phase.

Component	Conc. (wt%)	Loading (lb/hr)
Water Carbon Dioxide Nitrogen	9.27e+001 1.89e+000 3.46e-002 2.77e-002 2.64e+000	7.57e+000 1.39e-001 1.11e-001
Propane Isobutane	9.90e-001 6.24e-001 1.06e-001 2.79e-001 7.91e-002	2.50e+000 4.25e-001 1.12e+000
n-Hexane Cyclohexane	1.68e-002	1.86e-001 6.88e-002 6.71e-002
Toluene Ethylbenzene	1.42e-002	1.75e-001 4.34e-002 5.70e-002
Total Components	100.00	4.00e+002

#### FLASH TANK OFF GAS STREAM

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Temperature: 120.00 deg. F Pressure: 74.70 psia Flow Rate: 3.34e+002 scfh

Component		Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	1.05e-001 3.28e-001 4.47e-001 7.44e+001 1.46e+001	1.27e-001 1.10e-001 1.05e+001
Isobutane n-Butane Isopentane	6.09e+000 7.61e-001 1.95e+000 4.36e-001 5.51e-001	3.89e-001 9.94e-001 2.77e-001
Cyclohexane Heptanes 2,2,4-Trimethylpentane	4.40e-002	2.79e-002 3.88e-002 4.14e-003

Page: 8

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Toluene 1.17e-002 9.48e-003
Ethylbenzene 1.41e-003 1.31e-003
Xylenes 1.26e-003 1.18e-003
C8+ Heavies 8.10e-002 1.21e-001
Total Components 100.00 1.93e+001
```

#### FLASH TANK GLYCOL STREAM

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Temperature: 120.00 deg. F Flow Rate: 6.78e-001 gpm

Component		Loading (lb/hr)
Water Carbon Dioxide Nitrogen	9.74e+001 1.98e+000 3.13e-003 2.15e-004 2.10e-002	7.55e+000 1.19e-002 8.21e-004
Propane Isobutane	2.89e-002 3.67e-002 9.44e-003 3.19e-002 1.05e-002	1.40e-001 3.60e-002 1.21e-001
n-Hexane Cyclohexane	7.44e-003	4.73e-002 4.10e-002 2.83e-002
Toluene Ethylbenzene Xylenes C8+ Heavies	1.47e-002 3.19e-001	1.65e-001 4.21e-002 5.58e-002 1.22e+000
Total Components	100.00	3.810+002

#### FLASH GAS EMISSIONS

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Flow Rate: 8.02e+002 scfh

Control Method: Combustion Device

Control Efficiency: 50.00

Component		Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	4.98e+001 2.93e+001 1.86e-001 1.55e+001 3.03e+000	2.73e+001 1.10e-001 5.25e+000
Isobutane n-Butane Isopentane	1.27e+000 1.58e-001 4.05e-001 9.08e-002 1.15e-001	1.95e-001 4.97e-001 1.38e-001
Cyclohexane	3.80e-002 7.83e-003 9.16e-003	1.39e-002

```
2,2,4-Trimethylpentane 8.58e-004 2.07e-003
Benzene 2.42e-003 3.99e-003

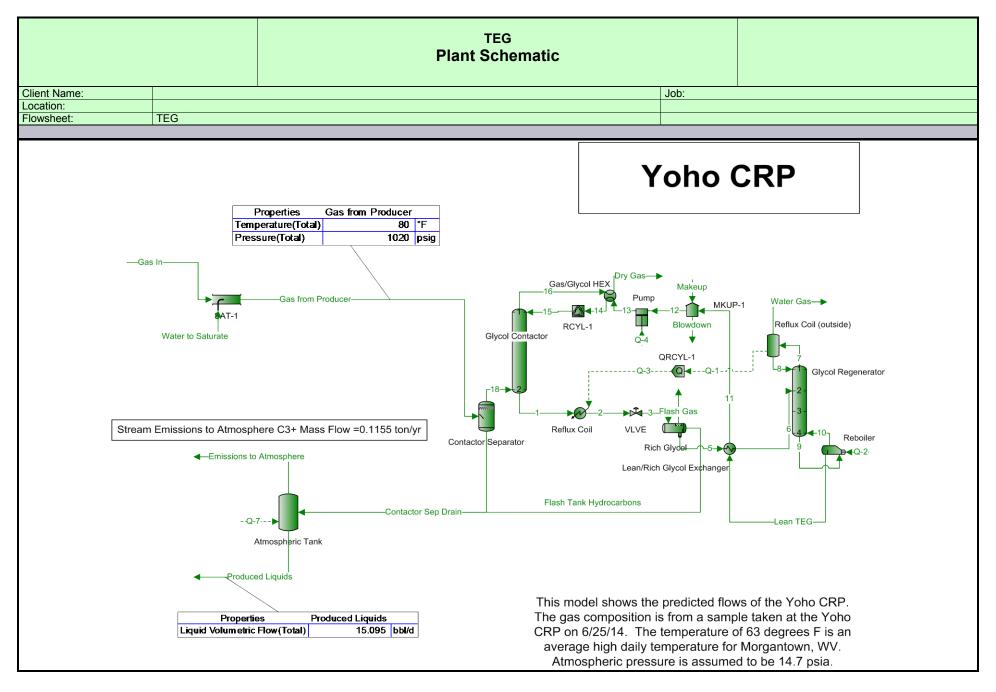
Toluene 2.43e-003 4.74e-003
Ethylbenzene 2.93e-004 6.56e-004
Xylenes 2.63e-004 5.89e-004
C8+ Heavies 1.69e-002 6.07e-002
Total Components 100.00 5.59e+001
```

#### REGENERATOR OVERHEADS STREAM

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Temperature: 212.00 deg. F Pressure: 14.70 psia Flow Rate: 5.04e+001 scfh

Component		Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	7.93e+001 2.04e-001 2.21e-002 3.76e+000 2.76e+000	1.19e-002 8.21e-004 8.00e-002
Isobutane n-Butane Isopentane	2.39e+000 4.66e-001 1.57e+000 4.11e-001 6.56e-001	3.60e-002 1.21e-001 3.94e-002
Cyclohexane Heptanes 2,2,4-Trimethylpentane	2.11e-001	3.90e-002 2.81e-002 1.48e-003
Ethylbenzene Xylenes C8+ Heavies	3.44e-001 4.86e+000	3.76e-002 4.85e-002 1.10e+000
Total Components	100.00	4.03e+000



<sup>\*</sup> User Specified Values

### **Process Streams Report** All Streams Tabulated by Total Phase

Client Name: Job: Location: Flowsheet: TEG

#### Connections

	Blowdown	Contactor Sep Drain	Dry Gas	Emissions to Atmosphere	Flash Gas
From Block	MKUP-1	Contactor Separator	Gas/Glycol HEX	Atmospheric Tank	Rich Glycol
To Block		Atmospheric Tank			

Stream Composition	า
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Stream Composition							
	Blowdown	Contactor Sep	Dry Gas	Emissions to	Flash Gas		
Mana Flore	11- /1-	Drain	11- /1-	Atmosphere	11- 0-		
Mass Flow	lb/h	lb/h	lb/h	lb/h	lb/h		
Water	0	220.129	4.69351	0.00544806	0.0241729		
TEG	0	0	0.1552	0	6.30581E-05		
Oxygen	0	6.85451E-06	2.31877	6.71397E-06	7.43035E-05		
Nitrogen	0	0.00135173	845.206	0.00133826	0.0270288		
Methane	0	0.209275	82455	0.205034	9.62299		
CO2	0	0.0185501	444.966	0.0128468	0.345653		
Ethane	0	0.0479087	25916.7	0.0467425	7.14572		
Propane	0	0.0203544	14834.2	0.0197573	5.32394		
i-Butane	0	0.000803333	2297.32	0.00079522	0.714712		
n-Butane	0	0.00393712	5377.45	0.00385293	1.99922		
i-Pentane	0	0.000528711	1576.77	0.000520489	0.545777		
n-Pentane	0	0.000616595	1816.46	0.000607493	0.683166		
2,2-Dimethylbutane	0	4.65458E-06	47.0525	4.62951E-06	0.0162946		
2,3-Dimethylbutane	0	2.17624E-05	105.395	2.14861E-05	0.0371906		
2-Methylpentane	0	5.87735E-05	469.248	5.83624E-05	0.15798		
3-Methylpentane	0	9.14313E-05	273.597	8.96536E-05	0.0959928		
Hexane	0	5.90469E-05	653.779	5.87144E-05	0.213071		
2,2-Dimethylpentane	0	0	0	0	0		
Methylcyclopentane	0	8.70056E-05	82.9338	8.15018E-05	0.0359888		
Benzene	0	0.000668587	10.5751	0.000157937	0.00567251		
Cyclohexane	0	0.000114417	71.5704	0.000104158	0.0281314		
2-Methylhexane	0	2.38136E-05	348.865	2.36446E-05	0.0967282		
2,3-Dimethylpentane	0	0	0	0	0		
3-Methylhexane	0	1.66344E-05	229.59	1.65122E-05	0.0652996		
1,t-2-Dimethylcyclopentane	0	0	5.41075E-06	0	2.10541E-10		
1,t-3Dimethylcyclopentane	0	1.13464E-06	1.70398	1.07213E-06	0.000658941		
Heptane	0	1.06295E-05	165.789	1.05428E-05	0.0435432		
Methylcyclohexane	0	4.81557E-05	96.274	4.62014E-05	0.0309311		
Toluene	0	0.000553471	14.8541	0.000150734	0.00609163		
1,t-4-Dimethylcyclohexane	0	1.36154E-10	17.0571	1.36154E-10	0.00439871		
Octane	0	7.83848E-07	24.7205	7.8037E-07	0.00502988		
Cotano		7.000402 07	24.7200	7.0007 E 07	0.0000E000		

Remarks

Total VOC = 0.1155 TPY

#### **ATTACHMENT O**

## Monitoring/Recordkeeping/Reporting/Testing Plans (NOT APPLICABLE)

"31.	Monitoring,	Recordke	eping, R	eporting a	nd Testing	Plans.	Attach	proposed
monito	oring, recordke	eeping, rep	orting and	testing pla	ans in order	to demo	nstrate c	compliance
with t	ne proposed	emissions	limits and	l operating	parameters	in this	permit a	application.
Provid	le this informa	tion as Atta	chment O	) <u>.</u> "				

•	Monitoring	/Recordkee	ping/Re	porting/1	<b>Testing</b>	<b>Plans</b>

No changes to the current Monitoring/Recordkeeping/Reporting/Testing requirements are proposed.

#### ATTACHMENT P

#### **Public Notice**

"32. **Public Notice**. At the time that the application is submitted, place a **Class I Legal Advertisement** in a newspaper of general circulation in the area where the source is or will be located (See 45CSR§13-8.3 through 45CSR§13-8.5 and Example Legal Advertisement for details). Please submit the **Affidavit of Publication** as Attachment P immediately upon receipt."

The applicant shall cause such legal advertisement to appear a minimum of one (1) day in the newspaper most commonly read in the area where the facility exists or will be constructed. The notice must be published no earlier than five (5) working days of receipt by this office of your application. The original affidavit of publication must be received by this office no later than the last day of the public comment period.

Types and amounts of pollutants discharged must include all regulated pollutants (PM, PM10, VOC, SO2, Xylene, etc.) and their potential to emit or the permit level being sought in units of tons per year (including fugitive emissions).

- Legal Advertisement (as shown) will be placed in a newspaper of general circulation in the area where the source is located (See 45CSR§13-8.3 thru 45CSR§13-8.5).
- An Affidavit of Publication shall be submitted immediately upon receipt.

#### YOHO COMPRESSOR STATION

Application for 45CSR13 NSR Modification Permit

### Attachment P LEGAL ADVERTISEMENT

### AIR QUALITY PUBLIC NOTICE Notice of Application

Notice is given that Williams Ohio Valley Midstream LLC has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a 45CSR13 New Soure Source Review (NSR) Modification Permit for the existing Yoho Compressor Station, located ~3.0 Miles South-Southeast of New Martinsville, ~0.1 Mile Northwest of Slim Chance Road, New Martinsville, Wetzel County, WV.

Latitude and longitude coordinates are 39.5997 degrees North and -80.8281 degrees West, respectively.

The applicant estimates the increase/(decrease) in the potential to discharge the following regulated air pollutants will be:

- 1.95 tons of nitrogen oxides per year
- 3.90 tons of carbon monoxide per year
- 18.62 tons of volatile organic compounds per year
- 0.36 tons of benzene per year
- 0.20 tons of ethylbenzene per year
- 0.25 tons of formaldehyde per year
- 0.45 tons of n-hexane per year
- 0.02 tons of methanol per year
- 0.58 tons of toluene per year
- 0.14 tons of 2,2,4-trimethylpentane per year
- (0.23) tons of xylenes per year
- 0.05 tons of other hazardous air pollutants per year
- 1.62 tons of total hazardous air pollutants per year
- 866 tons of carbon dioxide equivalent per year

Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1227, during normal business hours.

Dated this	the day of 20
Ву:	Mr. Don Wicburg, Vice President and General Manager Williams Ohio Valley Midstream LLC
	100 Teletech Drive Suite 2

Moundsville, WV 26041

# ATTACHMENT Q Business Confidential Claims (NOT APPLICABLE)

also

# ATTACHMENT R Authority Forms (NOT APPLICABLE)

also

# ATTACHMENT S Title V Permit Revision Information (NOT APPLICABLE)

#### **APPLICATION FEE**

Include a check payable to WVDEP – Division of Air Quality.

- As per WV Rule 22 (45CSR22) filed on May 6, 1991, a **minimum fee of \$1,000** must be submitted for each 45CSR13 permit application filed with the WVDEP-DAQ.
- **Additional charges** may apply, depending on the nature of the application as outlined in Section 3.4.b. of Regulation 22, and shown below:

NSPS Requirements: \$1,500 Not Applicable
 NESHAP Requirements: \$2,500 Not Applicable

• Total application fee is \$1,000 [= \$1,000 minimum fee + \$0 additional charges

The glycol dehydrator is an existing exempt source and the compressor engine is an existing NSPS JJJJ affected unit.

***** End of Application	n for 45CSR13 NS	R Modification Perm	i <b>t</b> ****



WILLIAMS FIELD SERVICES GROUP, INC PO BOX 21218 TULSA, OK 74121-1218 COMPANY NUMBER: 4000

CHECK NUMBER: 4000107785

PAY DATE	SUPPLIER NO.	SUPPLIER NAME	CHECK TOTAL
08-MAY-15	401733	STATE OF WEST VIRGINIA	1,000.00

Invoice Date	Invoice Or Credit Memo / Invoice Description	Gross	Discount	Net
07-MAY-15	Invoice Description 07-MAY-2015 / AIR PERMIT APPLICATION FEE FOR YOHO	1,000.00	0.00	1,000.00
		1		
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	at the state of th			
16				
	Supplier Support 1-866-778-2665	Page Totals	0.00	1,000.00

VERIFY THE AUTHENTICITY OF THIS MULTI-TONE SECURITY DOCUMENT.

■ CHECK BACKGROUND AREA CHANGES COLOR GRADUALLY FROM TOP TO BOTTOM.

Williams

WILLIAMS FIELD SERVICES GROUP, INC

PO BOX 21218

TULSA, OK 74121-1218 Company Number: 4000 JPMorgan Chase Bank, N.A. 70-2322/719 Chicago, IL

Check Number: 4000107785 Check Date: 08-MAY-15

One Thousand Dollars And Zero Cents

Pay To The Order Of:
STATE OF WEST VIRGINIA
WV DEP - DIVISION OF AIR QUALITY
601 57TH ST SE
CHARLESTON, WV 25304 United States

PAY (USD) \$1,000.00

Authorized Signature

From: (412) 787-4197 Danell Zawaski WLLIAMS 2000 Commerce Drive Park Place 2 Pittsburgh, PA 15275

Origin ID: OILA



Ship Date: 27MAY15 ActWgt: 1.0 LB CAD: 104269589/INET3610

Delivery Address Bar Code



60000006200060034.6228.8325

BILL SENDER

Ref#

htvoice # PO # Dept #

**Beverly McKeone** WV Div of Air Quality - Permitting 601 57th Street, SE

Charleston, WV 25304

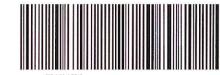
SHIP TO: (304) 926 0499 X 1260

FRI - 29 MAY AA \*\* 2DAY \*\*

TRK# 7736 8804 2500

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  1. Use the "Print" button on this page to print your label to your laser or inkjet printer.

  2. Fold the printed page along the horizontal line.

  3. Place label in shipping pouch and affix it to your shipment so that the barcode portion of the label can be read and scanned.

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Use of this system consistutes your agreement to the service conditions in the current Fedex Service Guide, available on fedex.com.Fedex will not be responsible for any claim in excess of \$100 per package, whether the result of loss, damage, delay, non-delivery,misdelivery,or misinformation, unless you declare a higher value, pay an additional charge, document your actual loss and file a timely claim.Limitations found in the current Fedex Service Guide apply. Your right to recover from Fedex for any loss, including intrinsic value of the package, loss of sales, income interest, profit, attorney's fees, costs, and other forms of damage whether direct, incidental, consequential, or special is limited to the greater of \$100 or the authorized declared value. Recovery cannot exceed actual documented loss.Maximum for items of extraordinary value is \$1,000, e.g. jewelry, precious metals, negotiable instruments and other items listed in our ServiceGuide. Written claims must be filed within strict time limits, see current Fedex Service Guide.