CONESTOGA-ROVERS
& ASSOCIATES

6320 Rothway, Suite 100, Houston, Texas 77040
Telephone: (713) 734-3090 Fax: (713) 734-3391
www.CRAworld.com

June 26, 2015 Reference No. 082715

Mr. Jay Fedczak
Assistant Director for Permitting
Division of Air Quality
WV Department of Environmental Protection
601 57th Street, SE
Charleston, West Virginia 25304

Dear Mr. Jay Fedczak:

Re: General Permit Application G70-A
Stanley Well Pad
Antero Resources Corporation

Conestoga-Rovers & Associates (CRA) would like to submit this General Permit application that we prepared on behalf of Antero Resources Corporation for an oil and gas facility identified as Stanley Well Pad.

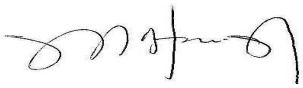
Enclosed are the following documents:

- Original copy of the G70-A General Permit Application
- Two CD copies of the G70-A General Permit Application
- The application fee with check no. 407684 in the amount of $1,500.00.

Please let us know if you have any questions or require additional information.

Sincerely,

CONESTOGA-ROVERS & ASSOCIATES



Manuel Bautista

Encl.

cc: Barry Schatz, Antero Resources Corporation

CONESTOGA-ROVERS & ASSOCIATES

www.CRAworld.com



DŜyŜNJl-f tŜNJY'ƛű !LJLJfƛŎl-űƛ2y' Dтлπ !

Stanley Well Pad

Prepared for: Antero Resources Corporation

Conestoga-Rovers & Associates
6320 Rothway, Suite 100
Houston, Texas 77040

June 2015 • 082715 • Report No. 206

Partners in Sustainability

Table of Contents

WEST VIRGINIA
DEPARTMENT OF ENVIRONMENTAL PROTECTION
DIVISION OF AIR QUALITY
601 57th Street, SE
Charleston, WV 25304
Phone: (304) 926-0475 • *www.dep.wv.gov/daq*

APPLICATION FOR GENERAL PERMIT REGISTRATION

CONSTRUCT, MODIFY, RELOCATE OR ADMINISTRATIVELY UPDATE

A STATIONARY SOURCE OF AIR POLLUTANTS

☒ CONSTRUCTION ☐ MODIFICATION ☐ RELOCATION ☐ CLASS I ADMINISTRATIVE UPDATE
☐ CLASS II ADMINISTRATIVE UPDATE

CHECK WHICH TYPE OF GENERAL PERMIT REGISTRATION YOU ARE APPLYING FOR:

☐ **G10-D –** Coal Preparation and Handling
☐ **G20-B –** Hot Mix Asphalt
☐ **G30-D –** Natural Gas Compressor Stations
☐ **G33-A –** Spark Ignition Internal Combustion Engines
☐ **G35-A –** Natural Gas Compressor Stations (Flare/Glycol Dehydration Unit)
☐ **G40-C –** Nonmetallic Minerals Processing
☐ **G50-B –** Concrete Batch
☐ **G60-C –** Class II Emergency Generator
☐ **G65-C –** Class I Emergency Generator
☒ **G70-A –** Class II Oil and Natural Gas Production Facility

SECTION I. GENERAL INFORMATION

1. Name of applicant (as registered with the WV Secretary of State's Office):
Antero Resources Corporation

2. Federal Employer ID No. **(FEIN):**
80-0162034

3. Applicant's mailing address:
1615 Wynkoop St.
Denver, CO, 80202

4. Applicant's physical address:
0.20 mile south from the intersection of Taylor Drain Rte. 19 and Cabin Run Rte. 21/1.

5. If applicant is a subsidiary corporation, please provide the name of parent corporation:

6. **WV BUSINESS REGISTRATION.** Is the applicant a resident of the State of West Virginia? ☐ **YES** ☒ **NO**

- IF **YES,** provide a copy of the Certificate of **Incorporation/ Organization / Limited Partnership** (one page) including any name change amendments or other Business Registration Certificate as **Attachment A**.
- IF **NO,** provide a copy of the **Certificate of Authority / Authority of LLC / Registration** (one page) including any name change amendments or other Business Certificate as **Attachment A**.

SECTION II. FACILITY INFORMATION

7. Type of plant or facility (stationary source) to be constructed, modified, relocated or administratively updated (e.g., coal preparation plant, primary crusher, etc.):
Natural Gas and Oil Production facility

8a. Standard Industrial Classification (SIC) code: 1311

AND

8b. North American Industry System (NAICS) code: 211111

9. DAQ Plant ID No. (for existing facilities only):
N/A

10. List all current 45CSR13 and other General Permit numbers associated with this process (for existing facilities only):
N/A

A: PRIMARY OPERATING SITE INFORMATION

11A. Facility name of primary operating site:	12A. Address of primary operating site:
Stanley Well Pad	Mailing: N/A Physical: 0.20 mile south from the intersection of Taylor Drain Rte. 19 and Cabin Run Rte. 21/1.

13A. Does the applicant own, lease, have an option to buy, or otherwise have control of the proposed site? ☒ **YES** ☐ **NO**

- IF **YES**, please explain: Antero is leasing the mineral rights for this site
- IF **NO**, YOU ARE NOT ELIGIBLE FOR A PERMIT FOR THIS SOURCE.

14A.
- For **Modifications or Administrative Updates** at an existing facility, please provide directions to the present location of the facility from the nearest state road;
- For Construction or Relocation permits, please provide directions to the proposed new site location from the nearest state road. Include a **MAP** as **Attachment F**.

From US 50 W, turn left onto Old US 50 E/Sunnyside Rd. Follow for 1.9 miles and turn left onto Oxford Rd. After 2.0 miles, turn right onto Cabin Run. In 0.4 miles turn right onto the access road and follow 1.4 miles to the pad.

15A. Nearest city or town:	16A. County:	17A. UTM Coordinates:
West Union	Doddridge	Northing (KM): 4343.0694 Easting (KM): 510.4028 Zone: 17 N

18A. Briefly describe the proposed new operation or change (s) to the facility:	19A. Latitude & Longitude Coordinates (NAD83, Decimal Degrees to 5 digits):
Construction of a new natural gas and oil production facility.	Latitude: 39.236867 Longitude: -80.879461

B: 1ST ALTERNATE OPERATING SITE INFORMATION (only available for G20, G40, & G50 General Permits)

11B. Name of 1st alternate operating site:	12B. Address of 1st alternate operating site:
	Mailing: Physical:

13B. Does the applicant own, lease, have an option to buy, or otherwise have control of the proposed site? ☐ **YES** ☐ **NO**

- IF **YES**, please explain:
- IF **NO**, YOU ARE NOT ELIGIBLE FOR A PERMIT FOR THIS SOURCE.

14B.
- For **Modifications or Administrative Updates** at an existing facility, please provide directions to the present location of the facility from the nearest state road;
- For Construction or Relocation permits, please provide directions to the proposed new site location from the nearest state road. Include a **MAP** as **Attachment F**.

15B. Nearest city or town:	16B. County:	17B. UTM Coordinates: Northing (KM): _____ Easting (KM): _____ Zone: _____
18B. Briefly describe the proposed new operation or change (s) to the facility:		19B. Latitude & Longitude Coordinates (NAD83, Decimal Degrees to 5 digits): Latitude: _____ Longitude: _____

C: 2ND ALTERNATE OPERATING SITE INFORMATION (only available for G20, G40, & G50 General Permits):

11C. Name of 2nd alternate operating site: _____ _____	12C. Address of 2nd alternate operating site: Mailing:_____ Physical:_____ _____

13C. Does the applicant own, lease, have an option to buy, or otherwise have control of the proposed site? ☐ **YES** ☐ **NO**

- IF **YES**, please explain: _____

  _____

- IF **NO**, YOU ARE NOT ELIGIBLE FOR A PERMIT FOR THIS SOURCE.

14C. – For **Modifications or Administrative Updates** at an existing facility, please provide directions to the present location of the facility from the nearest state road;

– For Construction or Relocation permits, please provide directions to the proposed new site location from the nearest state road. Include a **MAP** as **Attachment F**.

_____

_____

_____

15C. Nearest city or town:	16C. County:	17C. UTM Coordinates: Northing (KM): _____ Easting (KM): _____ Zone: _____
18C. Briefly describe the proposed new operation or change (s) to the facility:		19C. Latitude & Longitude Coordinates (NAD83, Decimal Degrees to 5 digits): Latitude: _____ Longitude: _____

20. Provide the date of anticipated installation or change: 04/01/2016 ☐ If this is an **After-The-Fact** permit application, provide the date upon which the proposed change did happen: : _____/_____/_____	21. Date of anticipated Start-up if registration is granted: 05/01/2016

22. Provide maximum projected **Operating Schedule** of activity/activities outlined in this application if other than 8760 hours/year. (Note: anything other than 24/7/52 may result in a restriction to the facility's operation).

Hours per day_____ Days per week _____ Weeks per year _____ Percentage of operation _____

SECTION III. ATTACHMENTS AND SUPPORTING DOCUMENTS

23. Include a check payable to WVDEP – Division of Air Quality with the appropriate **application fee** (per 45CSR22 and 45CSR13).

24. Include a **Table of Contents** as the first page of your application package.

All of the required forms and additional information can be found under the Permitting Section (General Permits) of DAQ's website, or requested by phone.

25. Please check all attachments included with this permit application. Please refer to the appropriate reference document for an explanation of the attachments listed below.

- ☒ ATTACHMENT A : CURRENT BUSINESS CERTIFICATE
- ☒ ATTACHMENT B: PROCESS DESCRIPTION
- ☒ ATTACHMENT C: DESCRIPTION OF FUGITIVE EMISSIONS
- ☒ ATTACHMENT D: PROCESS FLOW DIAGRAM
- ☒ ATTACHMENT E: PLOT PLAN
- ☒ ATTACHMENT F: AREA MAP
- ☒ ATTACHMENT G: EQUIPMENT DATA SHEETS AND REGISTRATION SECTION APPLICABILITY FORM
- ☒ ATTACHMENT H: AIR POLLUTION CONTROL DEVICE SHEETS
- ☒ ATTACHMENT I: EMISSIONS CALCULATIONS
- ☒ ATTACHMENT J: CLASS I LEGAL ADVERTISEMENT
- ☐ ATTACHMENT K: ELECTRONIC SUBMITTAL
- ☒ ATTACHMENT L: GENERAL PERMIT REGISTRATION APPLICATION FEE
- ☐ ATTACHMENT M: SITING CRITERIA WAIVER
- ☒ ATTACHMENT N: MATERIAL SAFETY DATA SHEETS (MSDS)
- ☒ ATTACHMENT O: EMISSIONS SUMMARY SHEETS
- ☒ OTHER SUPPORTING DOCUMENTATION NOT DESCRIBED ABOVE (Equipment Drawings, Aggregation Discussion, etc.)

Please mail an original and two copies of the complete General Permit Registration Application with the signature(s) to the DAQ Permitting Section, at the address shown on the front page of this application. Please DO NOT fax permit applications. For questions regarding applications or West Virginia Air Pollution Rules and Regulations, please refer to the website shown on the front page of the application or call the phone number also provided on the front page of the application.

SECTION IV. CERTIFICATION OF INFORMATION

This General Permit Registration Application shall be signed below by a Responsible Official. A Responsible Official is a President, Vice President, Secretary, Treasurer, General Partner, General Manager, a member of a Board of Directors, or Owner, depending on business structure. A business may certify an Authorized Representative who shall have authority to bind the Corporation, Partnership, Limited Liability Company, Association, Joint Venture or Sole Proprietorship. Required records of daily throughput, hours of operation and maintenance, general correspondence, Emission Inventory, Certified Emission Statement, compliance certifications and all required notifications must be signed by a Responsible Official or an Authorized Representative. If a business wishes to certify an Authorized Representative, the official agreement below shall be checked off and the appropriate names and signatures entered. Any administratively incomplete or improperly signed or unsigned Registration Application will be returned to the applicant.

FOR A CORPORATION (domestic or foreign)

☐ I certify that I am a President, Vice President, Secretary, Treasurer or in charge of a principal business function of the corporation

FOR A PARTNERSHIP

☐ I certify that I am a General Partner

FOR A LIMITED LIABILITY COMPANY

☐ I certify that I am a General Partner or General Manager

FOR AN ASSOCIATION

☐ I certify that I am the President or a member of the Board of Directors

FOR A JOINT VENTURE

☐ I certify that I am the President, General Partner or General Manager

FOR A SOLE PROPRIETORSHIP

☐ I certify that I am the Owner and Proprietor

☐ *I hereby certify that* (please print or type) _____

is an Authorized Representative and in that capacity shall represent the interest of the business (e.g., Corporation, Partnership, Limited Liability Company, Association Joint Venture or Sole Proprietorship) and may obligate and legally bind the business. If the business changes its Authorized Representative, a Responsible Official shall notify the Director of the Office of Air Quality immediately, and/or,

I hereby certify that all information contained in this General Permit Registration Application and any supporting documents appended hereto is, to the best of my knowledge, true, accurate and complete, and that all reasonable efforts have been made to provide the most comprehensive information possible

Signature _____
(please use blue ink) Responsible Official Date

Name & Title Barry Schatz, Senior Environmental & Regulatory Manager
(please print or type)

Signature Barry Schatz 6-26-2015
(please use blue ink) Authorized Representative (if applicable) Date

Applicant's Name Antero Resources Corporation

Phone & Fax 303-357-7276 303-357-7315
Phone Fax

Email bschatz@anteroresources.com

Attachment R
AUTHORITY OF CORPORATION
OR OTHER BUSINESS ENTITY (DOMESTIC OR FOREIGN)

TO: The West Virginia Department of Environmental Protection, Division of Air Quality

DATE: January 23, 2015

ATTN.: Director

Corporation's / other business entity's Federal Employer I.D. Number 80-0162034

The undersigned hereby files with the West Virginia Department of Environmental Protection, Division of Air Quality, a permit application and hereby certifies that the said name is a trade name which is used in the conduct of an incorporated business or other business entity.

Further, the corporation or the business entity certifies as follows:

(1) Barry Schatz (is/are) the authorized representative(s) and in that capacity may represent the interest of the corporation or the business entity and may obligate and legally bind the corporation or the business entity.

(2) The corporation or the business entity is authorized to do business in the State of West Virginia.

(3) If the corporation or the business entity changes its authorized representative(s), the corporation or the business entity shall notify the Director of the West Virginia Department of Environmental Protection, Division of Air Quality, immediately upon such change.

President or Other Authorized Officer
(Vice President, Secretary, Treasurer or other official in charge of a principal business function of the corporation or the business entity)

(If not the President, then the corporation or the business entity must submit certified minutes or bylaws stating legal authority of other authorized officer to bind the corporation or the business entity).

Secretary

Name of Corporation or business entity

Attachment A

Current Business Certificate

State of West Virginia

Certificate

I, Natalie E. Tennant, Secretary of State of the State of West Virginia, hereby certify that

ANTERO RESOURCES CORPORATION

a corporation formed under the laws of Delaware, which is authorized to transact business in West Virginia by a Certificate of Authority has filed in my office as required by the provisions of the West Virginia Code, a copy of an amendment to its Articles of Incorporation authenticated by the proper office of the state or country of its incorporation and was found to conform to law.

Therefore, I issue this

CERTIFICATE OF AMENDMENT TO CERTIFICATE OF AUTHORITY

Given under my hand and the Great Seal of the State of West Virginia on this day of June 10, 2013

Natalie E Tennant

Secretary of State

FILED

JUN 10 2013

IN THE OFFICE OF SECRETARY OF STATE

Natalie E. Tennant
Secretary of State
1900 Kanawha Blvd E
Bldg 1, Suite 157-K
Charleston, WV 25305

Penney Barker, Manager
Corporations Division
Tel: (304)558-8000
Fax: (304)558-8381
Website: www.wvsos.com
E-mail: business@wvsos.com

Office Hours: Monday – Friday
8:30 a.m. – 5:00 p.m. ET

FILE ONE ORIGINAL
(Two if you want a filed stamped copy returned to you)
FEE: $25.00

APPLICATION FOR AMENDED CERTIFICATE OF AUTHORITY

****** In accordance with the provisions of the West Virginia Code, the undersigned corporation hereby **** applies for an Amended Certificate of Authority and submits the following statement:**

1. Name under which the corporation was authorized to transact business in WV: Antero Resources Appalachian Corporation

2. Date Certificate of Authority was issued in West Virginia: 6/25/2008

3. Corporate name has been changed to: Antero Resources Corporation
(Attach one Certified Copy of Name Change as filed in home State of incorporation.)

4. Name the corporation elects to use in WV: Antero Resources Corporation
(due to home state name not being available)

5. Other amendments:
(attach additional pages if necessary)

6. **Name and phone number of contact person.** (This is optional, however, if there is a problem with the filing, listing a contact person and phone number may avoid having to return or reject the document.)

Alvyn A. Schopp — Contact Name
(303) 357-7310 — Phone Number

7. **Signature information** (See below ******Important Legal Notice Regarding Signature*):

Print Name of Signer: Alvyn A. Schopp Title/Capacity: Authorized Person

Signature: Alvyn A. Schopp **Date:** June 10, 2013

******Important Legal Notice Regarding Signature*: **Per West Virginia Code §31D-1-129. Penalty for signing false document. Any person who signs a document he or she knows is false in any material respect and knows that the document is to be delivered to the secretary of state for filing is guilty of a misdemeanor and, upon conviction thereof, shall be fined not more than one thousand dollars or confined in the county or regional jail not more than one year, or both.**

Delaware

The First State

I, JEFFREY W. BULLOCK, SECRETARY OF STATE OF THE STATE OF DELAWARE, DO HEREBY CERTIFY THE ATTACHED IS A TRUE AND CORRECT COPY OF THE CERTIFICATE OF AMENDMENT OF "ANTERO RESOURCES APPALACHIAN CORPORATION", CHANGING ITS NAME FROM "ANTERO RESOURCES APPALACHIAN CORPORATION" TO "ANTERO RESOURCES CORPORATION", FILED IN THIS OFFICE ON THE TENTH DAY OF JUNE, A.D. 2013, AT 9:37 O'CLOCK A.M.

A FILED COPY OF THIS CERTIFICATE HAS BEEN FORWARDED TO THE NEW CASTLE COUNTY RECORDER OF DEEDS.

Jeffrey W. Bullock, Secretary of State

4520810 8100

130754186

AUTHENTICATION: 0496546

DATE: 06-10-13

You may verify this certificate online at corp.delaware.gov/authver.shtml

State of Delaware
Secretary of State
Division of Corporations
Delivered 09:37 AM 06/10/2013
FILED 09:37 AM 06/10/2013
SRV 130754186 - 4520810 FILE

AMENDMENT TO THE AMENDED AND RESTATED CERTIFICATE OF INCORPORATION OF ANTERO RESOURCES APPALACHIAN CORPORATION

Antero Resources Appalachian Corporation (the "Corporation"), a corporation organized and existing under the laws of the State of Delaware, hereby certifies as follows:

1. The original Certificate of Incorporation of the Corporation was filed under the name Antero Resources Barnett Corporation with the filing of the original Certificate of Incorporation of the Corporation with the Secretary of State of the State of Delaware on March 18, 2008.

2. This Amendment to the Amended and Restated Certificate of Incorporation has been duly adopted and approved in accordance with Sections 242 of the General Corporation Law of the State of Delaware.

3. Article FIRST of the Amended and Restated Certificate of Incorporation is hereby amended to read in its entirety as follows:

FIRST. The name of the Corporation is Antero Resources Corporation.

IN WITNESS WHEREOF, the Corporation has caused this Certificate of Amendment to be executed by its duly authorized officer on the 10th day of June, 2013.

ANTERO RESOURCES APPALACHIAN CORPORATION

By: _____
Name: Alvyn A. Schopp
Title: Vice President of Accounting & Administration / Treasurer

Attachment B

Process Description

Attachment B

Process Description
Stanley Well Pad
Antero Resources Corporation
Doddridge County, West Virginia

A mixture of condensate and entrained gas from the wells enters the facility through a number of three phase low pressure separators where the gas phase is separated from the condensate and produced water. Gas Processing Units (GPU) heaters (H001-H008) are used in conjunction with the separators to help separate the gas from the liquid phases. These heaters are fueled by a slip stream of the separated gas. The separated gas from the three phase low pressure separators is sent to a compressor (ENG001). The compressed gas is then metered and sent to the sales gas pipeline. The separated water flow to the produced water storage tanks (TANKPW001-002). The separated condensate is then sent to two phase low pressure separators where gas is further separated from the condensate. The separated gas is routed to the compressor (ENG001), compressed, sent to the sales gas line. The condensate from the two phase separators flow to the condensate storage tanks (TANKCOND001-010).

The facility has ten (10) tanks (TANKCOND001-010) on site to store condensate and two (2) tanks (TANKPW001-002) to store produced water prior to removal from the site. Flashing, working, and breathing losses from the tanks are routed to the enclosed combustor (EC001) to control the emissions. The enclosed combustors (EC001-EC002) that will be used to control emissions are designed to achieve a VOC destruction efficiency of 98 percent. EC002 only operates as a backup enclosed combustor

Condensate and produced water are transported off site on an as needed basis via tanker truck. Truck loading connections are in place to pump condensate (L001) and produced water (L002) from the storage tanks into tanker trucks. Emissions from the loading operations are vented to the atmosphere.

Emissions from the facility's emission sources were calculated using the extended analysis of the condensate and gas from Prunty No. 1H, one of the wells in the Lockhart Heirs Pad. The extended analyses are considered representative of the materials from Stanley well pad, being in the same Marcellus rock formation.The flashing, working and breathing losses from the tanks are sent to the enclosed combustor. The enclosed combustor that will be used to control emissions is designed to achieve a VOC destruction efficiency of 98 percent.

Stanley Well pad calculation of potential to emit included all of the emission sources that belong to the same industrial grouping, are located on contiguous or adjacent properties, and are under the control of the same person. The nearest emission source that belongs to the same industrial grouping and under the control of the same person but not located on contiguous or adjacent property is the James Webb Well Pad. This operates independently and is approximately 0.35 miles northeast of the facility.

Attachment C

Description of Fugitive Emissions

Attachment C

Description of Fugitive Emissions
Stanley Well Pad
Antero Resources Corporation
Doddridge County, West Virginia

Sources of fugitive emissions include loading operations, haul road emissions, equipment leaks, and pneumatic control valves. Fugitive emissions were calculated using AP-42 factors. Routine equipment leaks are assumed to be occurring continuously throughout the year. Loading operations and haul road emissions only occur when tanker trucks are onsite. The fugitive emissions summary is also located in Attachment O.

Equipment Leaks

Equipment includes valves, flanges, and connectors installed in various process equipments such as heater treaters, pipelines, compressors, and separators. Emissions are assumed to be occurring throughout the year. Detailed calculations are shown on Table 4.

Pneumatic Control Valves

Pneumatic control valves are part of the heater treaters. These are intermittent low bleed valves and their emissions are assumed to be occurring throughout the year. Detailed calculations are shown on Table 5.

Loading Operations

Loading emissions occur when condensate and produced water are transferred out of the well site via tanker trucks. Fugitive emissions were estimated using AP-42 loading loss formula, L= 12.46*SPM/T, and Bryan & Engineering (BR&E) software known as Promax. Detailed calculations are shown in Table 8.

Haul Road Emissions

Haul road emissions are emitted when tanker trucks or service vehicles enter the facility. The facility is flat and unpaved. Detailed calculations are shown on Table 12.

Attachment C/O: G70-A Emissions Summary Sheet

Fugitive Emissions Data Summary Sheet

FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants Chemical Name/CAS [1]	Maximum Potential Uncontrolled Emissions [2]		Maximum Potential Controlled Emissions [3]		Est. Method Used [4]
		lb/hr	ton/yr	lb/hr	ton/yr	
Haul Road/Road Dust Emissions Paved Haul Roads	n/a					
Unpaved Haul Roads	PM, PM10, PM2.5	4.6795	11.7405	2.3397	5.8702	MB
Loading/Unloading Operations	VOCs	8.6819	5.2868	8.6819	5.2868	MB
	toluene (108883)	1.28E-03	7.83E-04	1.28E-03	7.83E-04	
	ethyl benzene (100414)	6.34E-04	3.86E-04	6.34E-04	3.86E-04	
	hexane (110543)	0.0203	0.0123	0.0203	0.0123	
	o,m,p-xylenes (95476,108383,106423)	1.87E-03	1.14E-03	1.87E-03	1.14E-03	
	CO2 Equivalent CO2 (124389), CH4	3.0944	4.7720	3.0944	4.7720	
	benzene (71432)	6.84E-04	4.25E-04	6.84E-04	4.25E-04	
	TAPs (benzene)	6.84E-04	4.25E-04	6.84E-04	4.25E-04	
Equipment Leaks (Components)	Benzene (71432)	Does not apply	0.0229	Does not apply	0.0229	MB
	Toluene (108883)		0.0709		0.0709	
	Ethyl benzene (100414)		0.0560		0.0560	
	Hexane (110543)		0.9596		0.9596	
	o,m,p-xylenes (95476,108383,106423)		0.1723		0.1723	
	CO2 Equivalent CO2 (124389)), CH4		282.8590		282.8590	
	VOCs		13.3250		13.3250	
	TAPs (benzene)		0.0229		0.0229	
Equipment Leaks (PCVs)	hexane (110543)	0.0109	0.0477	0.0109	0.0477	MB
	CO2 Equivalent CO2 (124389)), CH4	7.2262	31.6506	7.2262	31.6506	
	VOCs	0.0916	0.4012	0.0916	0.4012	

[1] List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS_2, VOCs, H_2S, Inorganics, Lead, Organics, O_3, NO, NO_2, SO_2, SO_3, all applicable Greenhouse Gases (including CO_2 and methane), etc. DO NOT LIST H_2, H_2O, N_2, O_2, and Noble Gases.

[2] Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

[3] Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

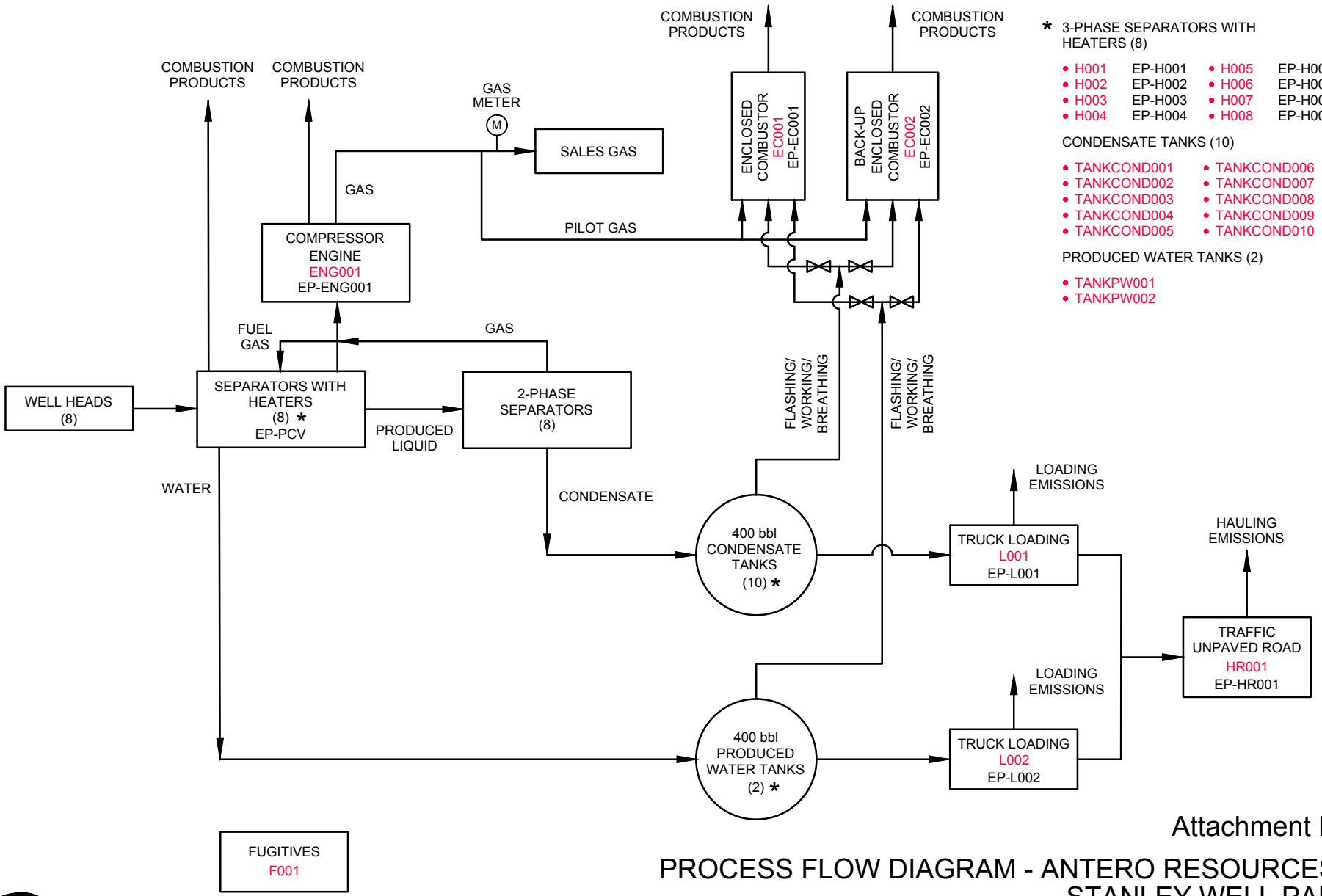
[4] Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

Attachment C: Leak Source Data Sheet

Source Category	Pollutant	Number of Source Components (1)	Number of Components Monitored by Frequency (2)	Average Time to Repair (days) (3)	Estimated Annual Emission Rate (lb/yr) (4)
Pumps (5)	light liquid VOC [6,7]				
	heavy liquid VOC[8]				
	Non-VOC[9]				
Valves (10)	Gas VOC	400		First attempt within 5 days of detection and final repair within 15 days	6,624.61
	Light Liquid VOC	416		First attempt within 5 days of detection and final repair within 15 days	19,528.73
	Heavy Liquid VOC	--			--
	Non-VOC	--			--
Safety Relief Valves (11)	Gas VOC	See Valves		First attempt within 5 days of detection and final repair within 15 days	see Valves
	Non VOC	See Valves		First attempt within 5 days of detection and final repair within 15 days	see Valves
Open-ended Lines (12)	VOC				
	Non-VOC				
Sampling Connections (13)	VOC				
	Non-VOC				
Compressors	VOC				
	Non-VOC				
Flanges	VOC	104		First attempt within 5 days of detection and final repair within 15 days	149.27
	Non-VOC			First attempt within 5 days of detection and final repair within 15 days	632.40
Other	VOC	472		First attempt within 5 days of detection and final repair within 15 days	347.42
	Non-VOC				1,471.85

Attachment D

Process Flow Diagram



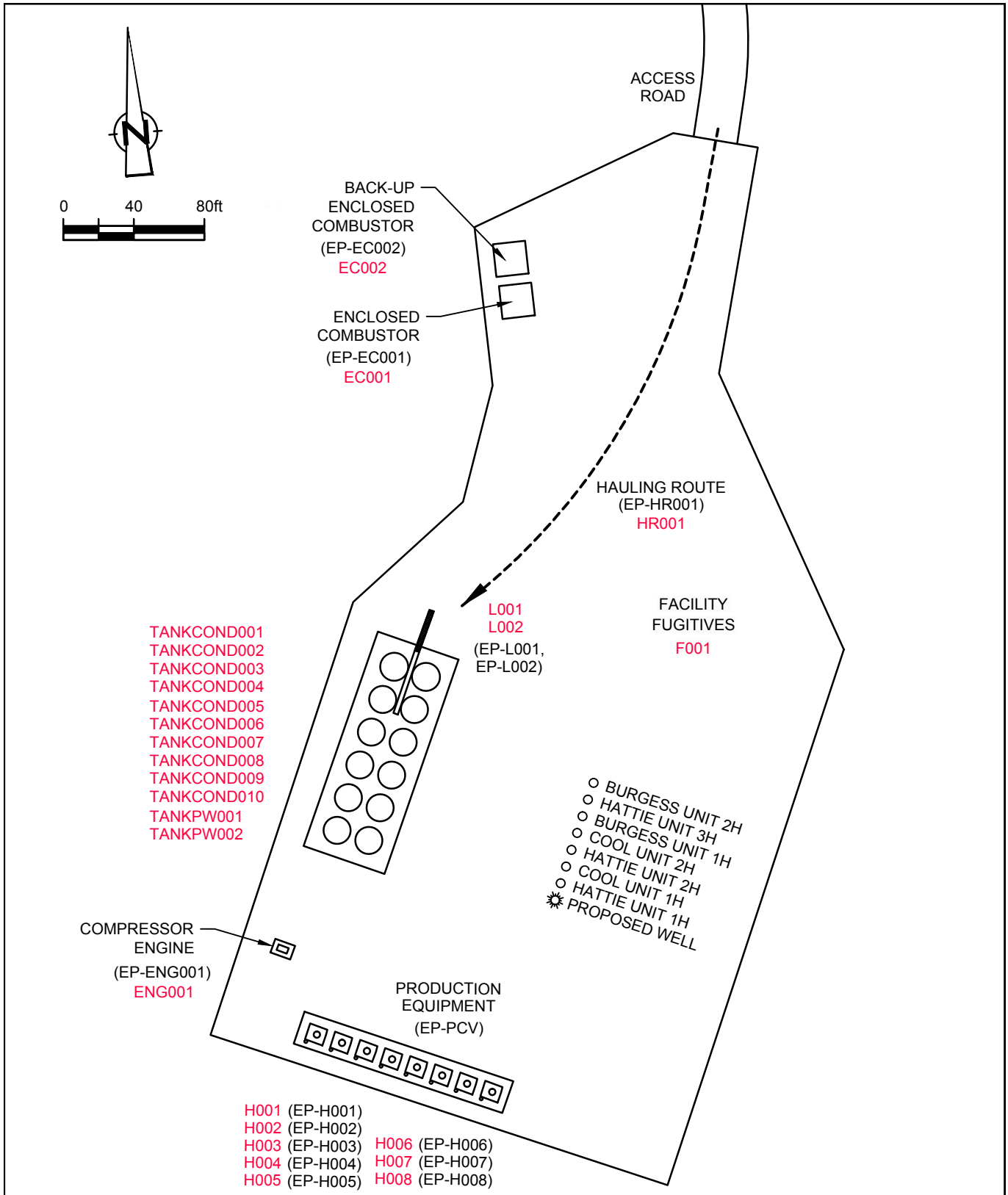
Attachment D

PROCESS FLOW DIAGRAM - ANTERO RESOURCES STANLEY WELL PAD

Doddridge County, West Virginia

Attachment E

Plot Plan



LEGEND

- ○ EXISTING WELL LOCATION
- ✡ PROPOSED WELL LOCATION

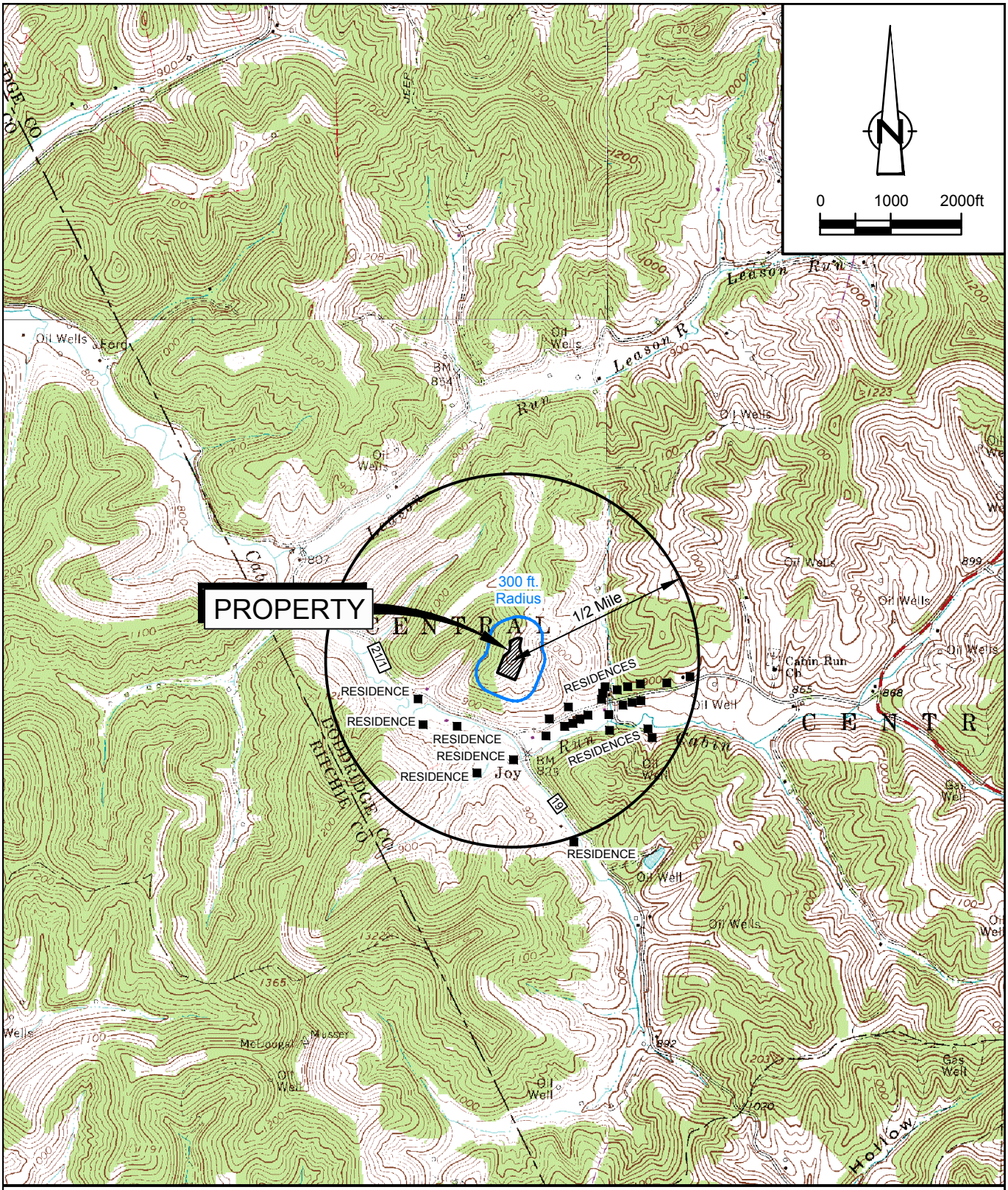
Attachment E

PLOT PLAN
STANLEY WELL PAD
ANTERO RESOURCES
Doddridge County, West Virginia

82715-00(206)GN-WA002 JUN 23/2015

Attachment F

Area Map



SOURCE: USGS QUADRANGLE MAP;
OXFORD, PENNSBORO, PULLMAN, AND WEST UNION, WEST VIRGINIA

SITE COORDINATES: LAT. 39.236867, LONG. -80.879461
SITE ELEVATION: 1095 ft AMSL

Attachment F

AREA MAP
STANLEY WELL PAD
ANTERO RESOURCES
Doddridge County, West Virginia

Attachment G

Emission Unit Data Sheets/G70-A Section Applicability Form

General Permit G70-A Registration
Section Applicability Form

General Permit G70-A was developed to allow qualified applicants to seek registration for a variety of sources. These sources include natural gas well affected facilities, storage tanks, natural gas-fired compressor engines (RICE), natural gas producing units, natural gas-fired in-line heaters, pneumatic controllers, heater treaters, tank truck loading, glycol dehydration units, completion combustion devices, flares, enclosed combustion devices, and vapor recovery systems. All registered facilities will be subject to Sections 1.0, 2.0, 3.0, and 4.0.

General Permit G70-A allows the registrant to choose which sections of the permit they are seeking registration under. Therefore, please mark which additional sections that you are applying for registration under. If the applicant is seeking registration under multiple sections, please select all that apply. Please keep in mind, that if this registration is approved, the issued registration will state which sections will apply to your affected facility.

Section 5	Natural Gas Well Affected Facility	☑
Section 6	Storage Vessels*	☑
Section 7	Gas Producing Units, In-Line Heaters, Heater Treaters, and Glycol Dehydration Reboilers	☑
Section 8	Pneumatic Controllers Affected Facility (NSPS, Subpart OOOO)	☐
Section 9	*Reserved*	☐
Section 10	Natural gas-fired Compressor Engine(s) (RICE) **	☑
Section 11	Tank Truck Loading Facility ***	☑
Section 12	Standards of Performance for Storage Vessel Affected Facilities (NSPS, Subpart OOOO)	☐
Section 13	Standards of Performance for Stationary Spark Ignition Internal Combustion Engines (NSPS, Subpart JJJJ)	☑
Section 14	Control Devices not subject to NSPS, Subpart OOOO	☑
Section 15	National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines (40CFR63, Subpart ZZZZ)	☑
Section 16	Glycol Dehydration Units	☐
Section 17	Dehydration Units With Exemption from NESHAP Standard, Subpart HH § 63.764(d) (40CFR63, Subpart HH)	☐
Section 18	Dehydration Units Subject to NESHAP Standard, Subpart HH and Not Located Within an UA/UC (40CFR63, Subpart HH)	☐
Section 19	Dehydration Units Subject to NESHAP Standard, Subpart HH and Located Within an UA/UC (40CFR63, Subpart HH)	☐

***** *Applicants that are subject to Section 6 may also be subject to Section 12 if the applicant is subject to the NSPS, Subpart OOOO control requirements or the applicable control device requirements of Section 14.*

****** *Applicants that are subject to Section 10 may also be subject to the applicable RICE requirements of Section 13 and/or Section 15.*

******* *Applicants that are subject to Section 11 may also be subject to control device requirements of Section 14.*

NATURAL GAS WELL AFFECTED FACILITY DATA SHEET

Complete this data sheet if you are the owner or operator of a gas well affected facility for which construction, modification, or reconstruction commenced after August 23, 2011. This form must be completed for natural gas well affected facilities regardless of when flowback operations occur (or have occurred).

Please provide the API number(s) for each NG well at this facility:	
47-017-06731-00	1 well not permitted
47-017-06732-00	
47-017-06737-00	
47-017-06736-00	
47-017-06735-00	
47-017-06733-00	
47-017-06734-00	

Note: This is the same API well number(s) provided in the well completion notification and as provided to the WVDEP, Office of Oil and Gas for the well permit. The API number may be provided on the application without the state code (047).

Every oil and gas well permitted in West Virginia since 1929 has been issued an API (American Petroleum Institute) number. This API is used by agencies to identify and track oil and gas wells.

The API number has the following format: 047-001-00001

Where,
047 = State code. The state code for WV is 047.
001 = County Code. County codes are odd numbers, beginning with 001 (Barbour) and continuing to 109 (Wyoming).
00001= Well number. Each well will have a unique well number.

Attachment G: Emission Units Data Sheet

(includes all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status)

Emission Unit ID[1]	Emission Point ID[2]	Emission Unit Description	Year Installed/ Modified	Design Capacity	Type[3] and Date of Change	Control Device[4]
H001, H002, H003, H004, H005, H006, H007, H008	EP-H001, EP-H002, EP-H003, EP-H004, EP-H005, EP-H006, EP-H007, EP-H008	Gas Production Unit Heaters	2016	1.5 MMBtu/hr (each)	New	N/A
F001	F001	Fugitives	2016	N/A	New	N/A
TANKCOND001-010	EP-EC001	Condensate Tank F/W/B	2016	400 bbl each	New	EC001, EC002
TANKPW001-002	EP-EC001	PW Tank F/W/B	2016	400 bbl each	New	EC001, EC002
L001	EP-L001	Loading (Condensate)	2016	200BBL capacity (each)	New	N/A
L002	EP-L002	Loading (Water)	2016	200BBL capacity (each)	New	N/A
HR001	EP-HR001	Haul Truck	2016	40 ton capacity	New	N/A
EC001, EC002	EP-EC001, EP-EC002	Enclosed Combustor	2016	90scf/min	New	EC001, EC002
PCV	EP-PCV	Pneumatic CV	2016	6.6 scf/day/PCV	New	N/A
ENG001	EP-ENG001	Compressor Engine	2016	24HP	New	N/A

1 For Emission Units (or Sources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.
2 For Emission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.
3 New, modification, removal.
4 For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

Attachment G: Storage Vessel Emission Unit Data Sheet (Condensate)

Provide the following information for each new or modified bulk liquid storage tank.

I. GENERAL INFORMATION (required)

1. Bulk Storage Area Name	CONDTANK	2. Tank Name	TANKCOND001-010
3. Emission Unit ID number	TANKCOND001-010	4. Emission Point ID number	EP-EC001, EP-EC002
5. Date Installed or Modified *(for existing tanks)*	2016	6. Type of change: New	
7A. Description of Tank Modification *(if applicable)* NA			
7B. Will more than one material be stored in this tank? *If so, a separate form must be completed for each material.* No			
7C. Provide any limitations on source operation affecting emissions. (production variation, etc.)			

II. TANK INFORMATION (required)

8. Design Capacity *(specify barrels or gallons).* Use the internal cross-sectional area multiplied by internal height. 400bbls			
9A. Tank Internal Diameter (ft.) 12		9B. Tank Internal Height (ft.) 20	
10A. Maximum Liquid Height (ft.) 18		10B. Average Liquid Height (ft.) 10	
11A. Maximum Vapor Space Height (ft.) 18		11B. Average Vapor Space Height (ft.) 10	
12. Nominal Capacity *(specify barrels or gallons)* . This is also known as "working volume." 400bbls			
13A. Maximum annual throughput (gal/yr)	12,264,000	13B. Maximum daily throughput (gal/day)	33,600
14. Number of tank turnovers per year	73	15. Maximum tank fill rate (gal/min)	168
16. Tank fill method: Splash Fill			
17. Is the tank system a variable vapor space system? No If yes, (A) What is the volume expansion capacity of the system (gal)? (B) What are the number of transfers into the system per year?			
18. Type of tank (check all that apply): X Fixed Roof X vertical horizontal X flat roof cone roof dome roof other (describe) External Floating Roof pontoon roof double deck roof Domed External (or Covered) Floating Roof Internal Floating Roof vertical column support self-supporting Variable Vapor Space lifter roof diaphragm Pressurized spherical cylindrical Underground Other (describe)			

III. TANK CONSTRUCTION AND OPERATION INFORMATION *(check which one applies)*

Refer to enclosed TANKS Summary Sheets

X Refer to the responses to items 19 – 26 in section VII

IV. SITE INFORMATION *(check which one applies)*

Refer to enclosed TANKS Summary Sheets

X Refer to the responses to items 27 – 33 in section VII

V. LIQUID INFORMATION *(check which one applies)*

Refer to enclosed TANKS Summary Sheets

X Refer to the responses to items 34 – 39 in section VII

Attachment G: Storage Vessel Emission Unit Data Sheet (Condensate)

Provide the following information for each new or modified bulk liquid storage tank.

VI. EMISSIONS AND CONTROL DEVICE DATA (required)

40. Emission Control Devices (check as many as apply):

Does Not Apply — Rupture Disc (psig)

Carbon Adsorption[1] — Inert Gas Blanket of _____

X Vent to Vapor Combustion Device[1] (vapor combustors, flares, thermal oxidizers) Condenser[1]

Conservation Vent (psig

Other[1] (describe) — Vacuum Setting — Pressure Setting Emergency Relief Valve (psig)

[1] Complete appropriate Air Pollution Control Device Sheet

41. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application).

Material Name and CAS No.	Flashing Loss		Breathing Loss		Working Loss		Total Emissions Loss		
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	
	Please see Tables 6 and 7								

1 EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)

Remember to attach emissions calculations, including TANKS Summary Sheets and other modeling summary sheets if applicable.

SECTION VII (required if did not provide TANKS Summary Sheets)

TANK CONSTRUCTION AND OPERATION INFORMATION		
19. Tank Shell Construction: Steel		
20A. Shell Color: Green	20B. Roof Color: Green	20C. Year Last Painted: 2016
21. Shell Condition (if metal and unlined): No Rust		
22A. Is the tank heated? No	22B. If yes, operating temperature:	22C. If yes, how is heat provided to tank?
23. Operating Pressure Range (psig): 0		
24. Is the tank a **Vertical Fixed Roof Tank**? Yes	24A. If yes, for dome roof provide radius (ft):	24B. If yes, for cone roof, provide slop (ft/ft):
25. Complete item 25 for **Floating Roof Tanks** Does not apply		
25A. Year Internal Floaters Installed:		
25B. Primary Seal Type *(check one):* Metallic (mechanical) shoe seal Liquid mounted resilient seal		
25C. Is the Floating Roof equipped with a secondary seal? Yes No		
25D. If yes, how is the secondary seal mounted? *(check one)* Shoe Rim Other (describe):		
25E. Is the floating roof equipped with a weather shield? Yes No		
25F. Describe deck fittings:		
26. Complete the following section for **Internal Floating Roof Tanks** Does not apply		
26A. Deck Type: Bolted Welded	26B. For bolted decks, provide deck construction:	
26C. Deck seam. Continuous sheet construction:		
26D. Deck seam length (ft.):	26E. Area of deck (ft2):	26F. For column supported	26G. For column supported

Attachment G: Storage Vessel Emission Unit Data Sheet (Condensate)

Provide the following information for each new or modified bulk liquid storage tank.

SITE INFORMATION:			
27. Provide the city and state on which the data in this section are based: West Union, WV			
28. Daily Avg. Ambient Temperature (°F): 51.7		29. Annual Avg. Maximum Temperature (°F): 63.8	
30. Annual Avg. Minimum Temperature (°F): 39.5		31. Avg. Wind Speed (mph): 4.8	
32. Annual Avg. Solar Insulation Factor (BTU/ft2-day): 1030.235999		33. Atmospheric Pressure (psia): 14.8	
LIQUID INFORMATION:			
34. Avg. daily temperature range of bulk liquid (°F): 51.7	34A. Minimum (°F): 39.5	34B. Maximum (°F): 103	
35. Avg. operating pressure range of tank (psig): 0	35A. Minimum (psig): 0	35B. Maximum (psig): 0	
36A. Minimum liquid surface temperature (°F): 39.5		36B. Corresponding vapor pressure (psia):	1.0758
37A. Avg. liquid surface temperature (°F): 51.7		37B. Corresponding vapor pressure (psia):	1.4176
38A. Maximum liquid surface temperature (°F): 103		38B. Corresponding vapor pressure (psia):	3.9666
39. Provide the following for each liquid or gas to be stored in the tank. Add additional pages if necessary.			
39A. Material name and composition:	Condensate		
39B. CAS number:	mix of HC		
39C. Liquid density (lb/gal):	5.93		
39D. Liquid molecular weight (lb/lb-mole):	108.7		
39E. Vapor molecular weight (lb/lb-mole):	44.20		
39F. Maximum true vapor pressure (psia):	1.8401		
39G. Max Reid vapor pressure (psi):	3.41000		
39H. Months Storage per year. From: To:	year round		

Attachment G: Storage Vessel Emission Unit Data Sheet (Produced Water)

Provide the following information for each new or modified bulk liquid storage tank.

I. GENERAL INFORMATION (required)

1. Bulk Storage Area Name PWTANK	2. Tank Name TANKPW001-002
3. Emission Unit ID number TANKPW001-002	4. Emission Point ID number EP-EC001, EP-EC002
5. Date Installed or Modified *(for existing tanks)* 2016	6. Type of change: New
7A. Description of Tank Modification *(if applicable)*	
7B. Will more than one material be stored in this tank? *If so, a separate form must be completed for each material.* No	
7C. Provide any limitations on source operation affecting emissions. (production variation, etc.)	

II. TANK INFORMATION (required)

8. Design Capacity *(specify barrels or gallons).* Use the internal cross-sectional area multiplied by internal height. 400bbls	
9A. Tank Internal Diameter (ft.) 12	9B. Tank Internal Height (ft.) 20
10A. Maximum Liquid Height (ft.) 18	10B. Average Liquid Height (ft.) 10
11A. Maximum Vapor Space Height (ft.) 18	11B. Average Vapor Space Height (ft.) 10
12. Nominal Capacity *(specify barrels or gallons)* . This is also known as "working volume." 400bbls	
13A. Maximum annual throughput (gal/yr) 73,584,000	13B. Maximum daily throughput (gal/day) 201,600
14. Number of tank turnovers per year 2190	15. Maximum tank fill rate (gal/min) 168
16. Tank fill method Splash Fill	
17. Is the tank system a variable vapor space system? No If yes, (A) What is the volume expansion capacity of the system (gal)? (B) What are the number of transfers into the system per year?	
18. Type of tank (check all that apply): X Fixed Roof X vertical horizontal X flat roof cone roof dome roof other (describe) External Floating Roof pontoon roof double deck roof Domed External (or Covered) Floating Roof Internal Floating Roof vertical column support self-supporting Variable Vapor Space lifter roof diaphragm Pressurized spherical cylindrical Underground Other (describe)	

III. TANK CONSTRUCTION AND OPERATION INFORMATION *(check which one applies)*

Refer to enclosed TANKS Summary Sheets

X Refer to the responses to items 19 – 26 in section VII

IV. SITE INFORMATION *(check which one applies)*

Refer to enclosed TANKS Summary Sheets

X Refer to the responses to items 27 – 33 in section VII

V. LIQUID INFORMATION *(check which one applies)*

Refer to enclosed TANKS Summary Sheets

X Refer to the responses to items 34 – 39 in section VII

Attachment G: Storage Vessel Emission Unit Data Sheet (Produced Water)

Provide the following information for each new or modified bulk liquid storage tank.

VI. EMISSIONS AND CONTROL DEVICE DATA (required)

40. Emission Control Devices (check as many as apply):

Does Not Apply — Rupture Disc (psig)

Carbon Adsorption[1] — Inert Gas Blanket of _____

X Vent to Vapor Combustion Device1 (vapor combustors, flares, thermal oxidizers) Condenser[1]

Conservation Vent (psig

Other[1] (describe) — Vacuum Setting — Pressure Setting Emergency Relief Valve (psig)

[1] Complete appropriate Air Pollution Control Device Sheet

41. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application).

Material Name and CAS No.	Flashing Loss		Breathing Loss		Working Loss		Total Emissions Loss		
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	
	Please see Tables 6 and 7								

1 EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)

Remember to attach emissions calculations, including TANKS Summary Sheets and other modeling summary sheets if applicable.

SECTION VII (required if did not provide TANKS Summary Sheets)

TANK CONSTRUCTION AND OPERATION INFORMATION		
19. Tank Shell Construction: Steel		
20A. Shell Color: Green	20B. Roof Color: Green	20C. Year Last Painted: 2016
21. Shell Condition (if metal and unlined): No Rust		
22A. Is the tank heated? No	22B. If yes, operating temperature:	22C. If yes, how is heat provided to tank?
23. Operating Pressure Range (psig): 0		
24. Is the tank a **Vertical Fixed Roof Tank**? Yes	24A. If yes, for dome roof provide radius (ft):	24B. If yes, for cone roof, provide slop (ft/ft):
25. Complete item 25 for **Floating Roof Tanks** Does not apply		
25A. Year Internal Floaters Installed:		
25B. Primary Seal Type *(check one):* Metallic (mechanical) shoe seal Liquid mounted resilient seal		
25C. Is the Floating Roof equipped with a secondary seal? Yes No		
25D. If yes, how is the secondary seal mounted? *(check one)* Shoe Rim Other (describe):		
25E. Is the floating roof equipped with a weather shield? Yes No		
25F. Describe deck fittings:		
26. Complete the following section for **Internal Floating Roof Tanks** Does not apply		
26A. Deck Type: Bolted Welded	26B. For bolted decks, provide deck construction:	
26C. Deck seam. Continuous sheet construction:		
26D. Deck seam length (ft.):	26E. Area of deck (ft2):	26F. For column supported	26G. For column supported

Attachment G: Storage Vessel Emission Unit Data Sheet (Produced Water)

Provide the following information for each new or modified bulk liquid storage tank.

SITE INFORMATION:			
27. Provide the city and state on which the data in this section are based: West Union, WV			
28. Daily Avg. Ambient Temperature (°F): 51.7		29. Annual Avg. Maximum Temperature (°F): 63.8	
30. Annual Avg. Minimum Temperature (°F): 39.5		31. Avg. Wind Speed (mph): 4.8	
32. Annual Avg. Solar Insulation Factor (BTU/ft2-day): 1030.235999		33. Atmospheric Pressure (psia): 14.8	
LIQUID INFORMATION:			
34. Avg. daily temperature range of bulk liquid (°F): 51.7	34A. Minimum (°F): 39.5	34B. Maximum (°F): 103	
35. Avg. operating pressure range of tank (psig): 0	35A. Minimum (psig): 0	35B. Maximum (psig): 0	
36A. Minimum liquid surface temperature (°F): 39.5		36B. Corresponding vapor pressure (psia):	0.1839
37A. Avg. liquid surface temperature (°F): 51.7		37B. Corresponding vapor pressure (psia):	0.2599
38A. Maximum liquid surface temperature (°F): 103		38B. Corresponding vapor pressure (psia):	0.9440
39. Provide the following for each liquid or gas to be stored in the tank. Add additional pages if necessary.			
39A. Material name and composition:	Produced Water		
39B. CAS number:	mix of HC and water		
39C. Liquid density (lb/gal):	8.33		
39D. Liquid molecular weight (lb/lb-mole):	18.0157		
39E. Vapor molecular weight (lb/lb-mole):	18.4251		
39F. Maximum true vapor pressure (psia):	0.4472		
39G. Max Reid vapor pressure (psi):	1.02416		
39H. Months Storage per year. From: To:	year round		

Attachment G: Natural Gas Fired Fuel Burning Units

Emission Data Sheet

Complete the information on this data for each Gas Producing Unit(s), Heater Treater(s), and in-line heater(s) at the production pad. Reboiler information should be entered on the Glycol Dehydration Emission Unit Data Sheet.

Emission Unit ID #[1]	Emission Point ID#[2]	Emission Unit Description (Manufacturer / Model #)	Year Installed/ Modified	Type[3] and Date of Change	Control Device[4]	Design Heat Input (mmBtu/hr)[5]	Fuel Heating Value (Btu/scf)[6]
H001	EP-H001	Gas Production Heaters	2016	New	--	1.50	1,247.06
H002	EP-H002	Gas Production Heaters	2016	New	--	1.50	1,247.06
H003	EP-H003	Gas Production Heaters	2016	New	--	1.50	1,247.06
H004	EP-H004	Gas Production Heaters	2016	New	--	1.50	1,247.06
H005	EP-H005	Gas Production Heaters	2016	New	--	1.50	1,247.06
H006	EP-H006	Gas Production Heaters	2016	New	--	1.50	1,247.06
H007	EP-H007	Gas Production Heaters	2016	New	--	1.50	1,247.06
H008	EP-H008	Gas Production Heaters	2016	New	--	1.50	1,247.06
ENG001	EP-ENG001	Engine (Kubota DG972-E2)	2016	New	--	--	1,247.06
EC001, EC002	EP-EC001, EP-EC002	Enclosed Combustor (Cimmaron 48", Model No. 700-TI-603-D-31C)	2016	New	EC001, EC002	6.6	1,247.06

1 Enter the appropriate Emission Unit (or Sources) identification numbers for each fuel burning unit located at the production pad. Gas Producing Unit Burners should be designated GPU-1, GPU-2, etc. Heater Treaters should be designated HT-1, HT-2, etc. Heaters or Line Heaters should be designated LH-1, LH-2, etc. For sources, use 1S, 2S, 3S…or other appropriate designation. Enter glycol dehydration unit Reboiler Vent data on the Glycol Dehydration Unit Data Sheet.

2 Enter the appropriate Emission Point identification numbers for each fuel burning unit located at the production pad. Gas Producing Unit Burners should be designated GPU-1, GPU-2, etc. Heater Treaters should be designated HT-1, HT-2, etc. Heaters or Line Heaters should be designated LH-1, LH-2, etc. For emission points, use 1E, 2E, 3E…or other appropriate designation.

3 New, modification, removal.

4 Complete appropriate air pollution control device sheet for any control device.

5 Enter design heat input capacity in mmBtu/hr.

6 Enter the fuel heating value in Btu/standard cubic foot.

Attachment G: Natural Gas-Fired Compressor Engine (RICE)

Emission Unit Data Sheet

Complete this section for any natural gas-fired reciprocating internal combustion engine.

Emission Unit (Source) ID No.		ENG001	
Emission Point ID No.		EP-ENG001	
Engine Manufacturer and Model		Engine (Kubota DG972-E2)	
Manufacturer's Rated bhp/rpm		24 HP @ 3600 rpm	
Source Status		NS	
Date Installed/Modified/Removed		2016	
Engine Manufactured/Reconstruction Date		2013	
Is this engine subject to 40CFR60, Subpart JJJJ?		Yes	
Is this a Certified Stationary Spark Ignition Engine according to 40CFR60, Subpart JJJJ? (Yes or No)		Yes	
Is this engine subject to 40CFR63, Subpart ZZZZ? (yes or no)		No	
Engine, Fuel and Combustion Data	Engine Type	RB4S	
	APCD Type	-	
	Fuel Type	RG	
	H2S (gr/100 scf)	0	
	Operating bhp/rpm	16.5 HP @ 2400 rpm	
	BSFC (Btu/bhp-hr)	9773	
	Fuel throughput (ft^3/hr)	193	
	Fuel throughput ($MMft^3$/yr)	1.6907	
	Operation (hrs/yr)	8760	
Reference	Potential Emissions	lbs/hr	tons/yr
MD	NO_X	0.3158	1.3831
MD	CO	5.6445	24.7228
AP	VOC	0.0071	0.0311
AP	SO_2	0.0001	0.0006
AP	PM_{10}	0.0024	0.0104
AP	Formaldehyde	0.0049	0.0215
MRR	Proposed Monitoring:	Monitor engine setting adjustments to ensure these are consistent with manufacturer's instructions.	
	Proposed Recordkeeping:	1) Maintain records of maintenance performed on engines. 2) Documentation from manufacturer that engine is certified to meet emission standards	
	Proposed Reporting:	N/A	

Attachment G: Tank Truck Loading

Emissions Unit Data Sheet

Furnish the following information for each new or modified bulk liquid transfer area or loading rack at the natural gas production pad.
This form is to be used for bulk liquid transfer operations to tank trucks.

1. Emission Unit ID: L001, L002	2. Emission Point ID: EP-L001, EP-L002	3. Year Installed/ Modified: 2016

4. Emission Unit Description: CONDENSATE AND PRODUCED WATER

5. Loading Area Data

5A. Number of pumps: 2	5B. Number of liquids loaded: 2	5C. Maximum number of tank trucks loading at one time: 2

6. Describe cleaning location, compounds and procedure for tank trucks: For hire tank trucks are used and are cleaned at the operator's dispatch terminal. These trucks are in dedicated service and cleaned only prior to repair or leak tests. Cleaning materials include water, steam, detergent, and solvents which are applied using hand held pressurized spray nozzles.

7. Are tank trucks pressure tested for leaks at this or any other location?
X Yes No
If YES, describe: Tank trucks are pressure tested for leaks at the location of the leak testing company. Trucks are tested using EPA Method 27-internal vapor valve test and issued certification that DOT requirements are met.

8. Projected Maximum Operating Schedule (for rack or transfer point as a whole):

Maximum	Jan. - Mar.	Apr. - June	July - Sept.	Oct. - Dec.
hours/day	12	12	12	12
days/week	7	7	7	7

9. Bulk Liquid Data *(add pages as necessary)*

Liquid Name		Condensate	Produced Water	
Max. daily throughput (1000 gal/day)		33.6	201.6	
Max. annual throughput (1000 gal/yr)		12,264.00	73,584.00	
Loading Method [1]		BF	BF	
Max. Fill Rate (gal/min)		168	168	
Average Fill Time (min/loading)		50	50	
Max. Bulk Liquid Temperature (^{o}F)		72.1	72.1	
True Vapor Pressure [2]		1.84	0.45	
Cargo Vessel Condition [3]		U	U	
Control Equipment or Method [4]		None	None	
Minimum collection efficiency (%)		0	0	
Minimum control efficiency (%)		0	0	
Maximum Emission Rate	Loading (lb/hr)	11.71	1.17	
	Annual (ton/yr)	7.12	4.26	
Estimation Method [5]		Promax	Promax	

Notes:

1 BF = Bottom Fill SP = Splash Fill SUB = Submerged Fill

2 At maximum bulk liquid temperature

3 B = Ballasted Vessel, C = Cleaned, U = Uncleaned (dedicated service), O = other (describe)

4 List as many as apply (complete and submit appropriate *Air Pollution Control Device Sheets as Attachment "H"*):
CA = Carbon Adsorption
VB = Dedicated Vapor Balance (closed system) ECD = Enclosed Combustion Device
F = Flare
TO = Thermal Oxidation or Incineration

5 EPA = EPA Emission Factor as stated in AP-42

10. **Proposed Monitoring, Recordkeeping, Reporting, and Testing**

MONITORING	RECORDKEEPING
1) Visual inspection to ensure that loading connections from storage tanks to trucks are leak-free.	1) Maintain records of condensate transferred from storage tanks. 2) Maintain records of produced water transferred from storage tanks.
REPORTING N/A	TESTING N/A

11. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty: N/A

Attachment H

Air Pollution Control Device Data Sheet

Attachment H: Air Pollution Control Device

Vapor Combustion Control Device Sheet

Complete this vapor combustion control device sheet for each enclosed combustion device, flare, thermal oxidizer, or completion combustion device that is located at the natural gas production pad for the purpose of thermally destructing waste gas to control emissions of regulated pollutants to the atmosphere.

IMPORTANT: READ THE INSTRUCTIONS ACCOMPANYING THIS FORM BEFORE COMPLETING.			
General Information			
1. Control Device ID#: EC001, EC002		2. Installation Date: New	
3. Maximum Rated Total Flow Capacity: scfh 131,000 scfd	4. Maximum Design Heat Input: 6.6 MMBtu/hr	5. Design Heat Content: 2300BTU/scf	
Control Device Information			
6. Select the type of vapor combustion control device being used: Enclosed Combustor			
7. Manufacturer: Model No. Cimmaron, Model No. 48" HV ECD		8. Hours of operation per year: 8760	
9. List the emission units whose emissions are controlled by this vapor combustion control device: (Emission Point ID#:)			
10. Emission Unit ID#	Emission Source Description:	Emission Unit ID#	Emission Source Description:
TANKCOND001-010	Condensate Tank		
TANKPW001-002	PW Tanks		
If this vapor combustor controls emissions from more than six emission units, please attach additional pages.			

11. Assist Type	12. Flare Height (ft)	13. Tip Diameter (ft)	14. Was the design per §60.18?
Steam - Air - Pressure - X Non -	25ft	3.33	Yes

Waste Gas Information			
15. Maximum waste gas flow rate (scfm):	16. Heat value of waste gas stream (BTU/ft3)	17. Temperature of the emissions stream (°F)	18. Exit Velocity of the emissions stream (ft/s)
55.18	2,106.02	900	1.06E-01
19. Provide an attachment with the characteristics of the waste gas stream to be burned.			

Pilot Information				
20. Type/Grade of pilot fuel:	21. Number of pilot lights:	22. Fuel flow rate to pilot flame per pilot (scf/hr):	23. Heat input per pilot (BTU/hr):	24. Will automatic re-ignition be used?
Natural Gas	1	12.6	12800	Yes
25. If automatic re-ignition will be used, describe the method: Based on a monitoring system				
26. Describe the method of controlling flame: Flame Rectification, a thermocouple equivalent				
27. Is pilot flame equipped with a monitor to detect the presence of the flame? Yes	28. If yes, what type? Thermocouple			

29. Pollutant(s) Controlled	30. % Capture Efficiency	31. Manufacturer's Guaranteed Control Efficiency (%)
F/W/B Emissions from TANKCOND	98	98
F/W/B Emissions from TANKPW	98	98

Attachment H: Air Pollution Control Device

Vapor Combustion Control Device Sheet

Complete this vapor combustion control device sheet for each enclosed combustion device, flare, thermal oxidizer, or completion combustion device that is located at the natural gas production pad for the purpose of thermally destructing waste gas to control emissions of regulated pollutants to the atmosphere.

32. Has the control device been tested by the manufacturer and certified? Yes, see spec sheet.

33. Describe all operating ranges and maintenance procedures required by the manufacturer to maintain warranty: See spec sheet for operating ranges.

MONITORING

1) Report any period when visible emissions exceeded 5 minutes during any two-hour period.
2) Monitor the presence of pilot flame at all times with the Flame rectification system, a thermocouple equivalent.
3) Monitor visible emissions from the vapor combustor.
4) Monitor throughput to the vapor combustor.

RECORDKEEPING

1) Record the times and duration of periods when the pilot flame was not present.
2) Records of throughput to the vapor combustor.
3) Records of vapor combustor malfunction or shutdown which resulted in excess emissions.
4) Records of vapor combustor inspection and maintenance activities conducted.

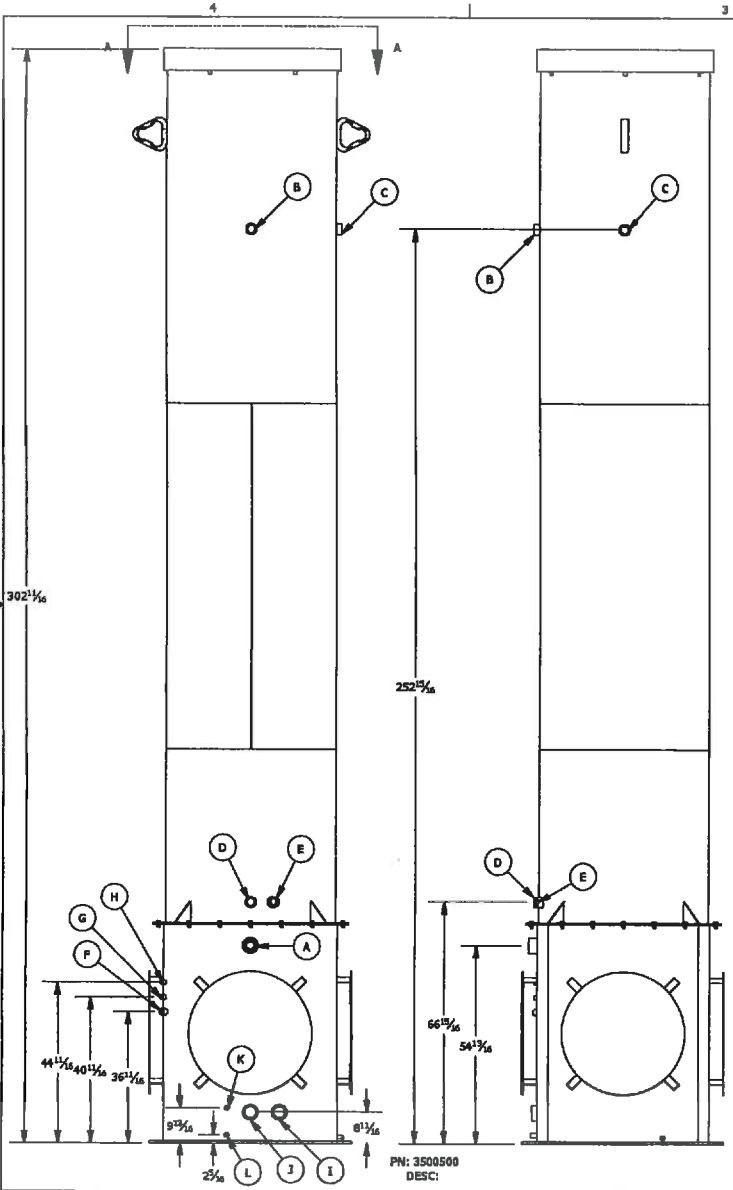
REPORTING

1) Report any period when visible emissions exceeded 5 minutes during any two-hour period.

34. Additional Information Attached? **YES**

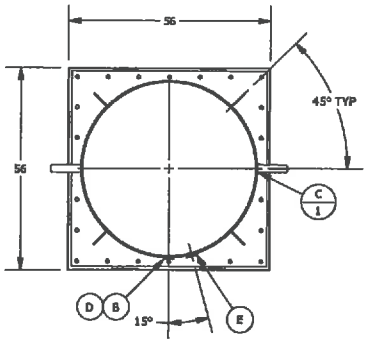
Please attach a copy of manufacturer's data sheet. Please attach a copy of manufacturer's drawing.
Please attach a copy of the manufacturer's performance testing.

If any of the requested information is not available, please contact the manufacturer.



48" DIA x 302 5/8" HEIGHT, 88 ORIFICES EMISSION CONTROL DEVICE

* >98% TVOC DRE, CERTIFIED USEPA 40 CFR 60, APPENDIX A, SOURCE EMMISIONS TEST METHODS REFERENCED. MEETS ALL EPA & CDPHE REGULATIONS.
* DESTROYS OIL/CONDENSATE PRODUCTION TANK VAPORS W/ NO VISIBLE FLAME.
* EXCELLENT OPACITY AND SMOKELESS OPERATION.
* RELIABLE AND CUSTOMIZABLE IGNITION.
* VERY LOW CAPITAL AND OPERATING COST.
* EASY TO OPERATE AND MAINTAIN.
* FIELD TESTED TO DESTROY UP TO 119.5 MDSCFD (131 MCFD) @ 10 oz/in^2; 2300 BTU/CF WASTE GAS (SG 1.45)
* STRUCTURE CERTIFIED FOR 90 MPH 3-SEC WIND GUST PER ASCE 7-05 & IBC 2006 STANDARDS. HIGHER WIND LOAD RATED STRUCTURES AVAILABLE.



VIEW A-A

PN: 3500500
DESC:

SCHEDULE OF NOZZLES				
MARK	QTY	DESCRIPTION	SERIES	SERVICE
A	1	3" HALF COUPLING	2000#	BURNER WASTE GAS IN
B	1	2" FULL COUPLING	3000#	FLOW TEST/AUTOMATION
C	1	2" FULL COUPLING	3000#	FLOW TEST/AUTOMATION
D	1	2" FULL COUPLING	3000#	SIGHT GLASS
E	1	2" FULL COUPLING	3000#	MANUAL LIGHTING
F	1	1" FULL COUPLING	3000#	PILOT GAS IN
G	1	1/2" FULL COUPLING	3000#	IGNITOR CABLE
H	1	1/2" FULL COUPLING	3000#	AUTOMATION
I	1	3" HALF COUPLING	3000#	DRIP TANK WASTE GAS IN
J	1	3" HALF COUPLING	3000#	DRIP TANK WASTE GAS OUT
K	1	1/2" FULL COUPLING	3000#	AUTOMATION
L	1	1/2" FULL COUPLING	3000#	LIQUID DRAIN

UNLESS OTHERWISE SPECIFIED

1. REMOVE ALL BURRS AND SHARP CORNERS.
2. COR. RAD .03
3. DO NOT SCALE DRAWING.
4. ALL DIMENSIONS ARE IN INCHES.
5. MACHINE FIN.
6. FABRICATION
   .X = ± 0.25
   .XX = ± 0.125
   .XXX = ± 0.06
   ANGLES ± 3°
7. MACHINE
   .X = ±0.030
   .XX = ±0.015
   .XXX = ±0.005
   ANGLES ±1/2°
   CONTRICITY WITHIN 0.010 TIR

APPROVED FOR A.S.M.E CODE, SECTION VIII DIV 1
_____ED,_____ ADDENDA BY_____ DATE_____

CIMARRON
Energy Inc.

TITLE:
48" HIGH VOLUME ECD

DATE:	WO No.:	SHEET: 1 OF 1

DRAWN BY: TDS | REV. | DRAW NO.: 3500500

Attachment I

Emission Calculations

Table 1

Facility Information
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

Oil and Gas Site General Information

Administrative Information	
Company Name	Antero Resources Corporation
Facility/Well Name	Stanley Well Pad
Nearest City/Town	West Union
API Number/SIC Code	1311
Latitude/Longitude	39.236867, -80.879461
County	Doddridge

Technical Information	
Max Condensate Site Throughput (bbl/day):	800
Max Produced Water Site Throughput (bbl/day):	4,800
Are there any sour gas streams at this site?	No
Is this site currently operational/producing?	No

Equipment/Processes at Site	
Equipment/Process Types	**How many for this site?**
Fugitives	8
IC Engines	1
Turbines	0
Diesel Engines	0
Gas Production Unit Heaters	8
Condensate Tanks	10
Produced Water Tanks	2
Miscellaneous Tanks	0
Loading Jobs	2
Glycol Units	0
Amine Units	0
Enclosed Combustors	2

Table 2

Uncontrolled/Controlled Emissions Summary
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

Emission Source	VOC		NO_X		CO_{2e}		CO		SO_2		$PM_{2.5}$		PM_{10}		Lead		Total HAPs		Benzene		Xylenes		Formaldehyde	
	(lbs/hr)	(ton/yr)	(lbs/hr)	(ton/yr)	(lbs/hr)	(ton/yr)	(lbs/hr)	(ton/yr)	(lbs/hr)	(ton/yr)	(lbs/hr)	(ton/yr)	(lbs/hr)	(ton/yr)	(lbs/hr)	(ton/yr)	(lbs/hr)	(ton/yr)	(lbs/hr)	(ton/yr)	(lbs/hr)	(ton/yr)	(lbs/hr)	(ton/yr)
UNCONTROLLED (Fugitives, Storage Tanks, Heater Treaters)																								
Fugitive Emissions (Component Count, PCV and Hauling)[1]	3.1338	13.7262			71.806	314.51							2.1058	5.2832			0.3035	1.3293	0.0052	0.0229	3.93E-02	1.72E-01		
Flashing, Working and Breathing (F/W/B) Losses[2]	253.04	1,108.3															9.555	41.850	0.3933	1.7225	0.2237	0.9797		
Engine Emissions[3]	0.0071	0.0311	0.3158	1.3831	27.78	121.66	5.6445	24.7228	0.0001	0.0006	0.0024	0.0104	0.0023	0.0100			0.0055	0.0241	0.0004	0.0017	0.0000	0.0002	0.0049	0.0215
Gas Production Unit Heater Emissions[4]	0.0529	0.2318	0.9623	4.2147	1,161.58	5,087.71	0.8083	3.5404	0.0058	0.0253	0.0731	0.3203	0.0731	0.3203	4.81E-06	2.11E-05	1.81E-02	7.93E-02	2.02E-05	8.85E-05			0.0007	0.0032
TOTALS:	**256.2370**	**1122.3179**	**1.2780**	**5.5978**	**1261.1602**	**5523.8815**	**6.4528**	**28.2632**	**0.0059**	**0.0259**	**0.0755**	**0.3307**	**2.1812**	**5.6135**	**4.81E-06**	**2.11E-05**	**9.8820**	**43.2833**	**0.3989**	**1.7471**	**0.2631**	**1.1523**	**0.0056**	**0.0247**
UNCONTROLLED (Truck Loading Emissions)																								
Truck Loading Emissions[5]	8.682	5.287			3.094	4.772											0.0248	0.0151	6.84E-04	4.25E-04	0.0019	0.0011		
CONTROLLED EMISSIONS																								
Enclosed Combustor Emissions (from F/W/B losses)[6]	5.0610	22.1672	0.3336	1.4611	1359.8315	5956.0619	0.2802	1.2273	1.51E-05	6.62E-05	0.0190	0.0833	0.0254	3.52E-05	1.67E-06	7.31E-06	0.1911	0.8372	7.87E-03	3.44E-02	0.0045	0.0196	1.89E-06	8.28E-06
Controlled Fugitive Emissions from Hauling													1.0529	2.6416										
TOTALS:	**5.0610**	**22.1672**	**0.3336**	**1.4611**	**1359.8315**	**5956.0619**	**0.2802**	**1.2273**	**1.51E-05**	**6.62E-05**	**0.0190**	**0.0833**	**1.0782**	**2.6416**	**1.67E-06**	**7.31E-06**	**0.1911**	**0.8372**	**0.0079**	**0.0344**	**0.0045**	**0.0196**	**1.89E-06**	**8.28E-06**
POTENTIAL TO EMIT[7]	**8.2549**	**41.4431**	**1.6116**	**7.0589**	**2620.9916**	**11484.7154**	**6.7330**	**29.4905**	**0.0059**	**0.0260**	**0.0945**	**0.4140**	**1.1536**	**2.9719**	**6.48E-06**	**2.84E-05**	**0.5183**	**2.2851**	**0.0135**	**0.0595**	**0.0439**	**0.1933**	**0.0056**	**0.0247**

Enter any notes here:	1 - See Tables 4 and 5 for fugitive emission calculations; Table 12 for PM emissions from hauling. 2 - See Tables 6 and 7 for tanks emission calculations 3 - See Table 13 for engine emissions 4 - See Table 9 for gas production unit heater emission calculations 5 - The maximum emission was calculated based on tank truck capacity of 200 barrels and actual fill rate of 50 minutes per tank truck. At a production rate of 800 barrels per day, VOC emissions would be 8.6819 pounds per hour when there are loading activities. Average hourly VOC emissions from truck loading is 1.207 pound per hour. 6 - See Table 10 and 11 for enclosed combustion emission calculations. 7 - The hourly potential to emit is the sum of emissions from gas production unit heaters, engine, storage tanks, fugitives and enclosed combustor. Does not include emissions from loading (see footnote 5). The total TPY PTE is the sum of all emissions. PM 10 TPY is the sum of uncontrolled hauling and other PM10 sources.

Table 3

Permits Summary

Stanley Well Pad

Doddridge, West Virginia

Antero Resources Corporation

Pollutant		Emissions			Threshold Exceeded?	
		Uncontrolled	Controlled	Threshold	Uncontrolled	Controlled
VOC	lbs/hr	256.2370	8.2549	6	**Yes**	**Yes**
	tons/yr	1127.6047	41.4431	10	**Yes**	**Yes**
NO_X	lbs/hr	1.2780	1.6116	6		
	tons/yr	5.5978	7.0589	10		
CO	lbs/hr	6.4528	6.7330	6	**Yes**	**Yes**
	tons/yr	28.2632	29.4905	10	**Yes**	**Yes**
SO_2	lbs/hr	0.0059	0.0059	6		
	tons/yr	0.0259	0.0260	10		
$PM_{2.5}$	lbs/hr	7.55E-02	9.45E-02	6		
	tons/yr	3.31E-01	4.14E-01	10		
PM_{10}	lbs/hr	2.1812	1.1536	6		
	tons/yr	5.6135	2.9719	10		
Lead	lbs/hr	4.81E-06	6.48E-06	6		
	tons/yr	2.11E-05	2.84E-05	10		
Total HAPs	lbs/hr	9.8820	0.5183	2	**Yes**	
	tons/yr	43.2983	2.2851	5	**Yes**	
Total TAPs	lbs/hr	0.4045	0.0191	1.14		
n-Hexane	lbs/hr	8.7519	0.4174			
	tons/yr	38.3456	1.8407			
Toluene	lbs/hr	0.3585	0.0232			
	tons/yr	1.5711	0.1024			
Ethylbenzene	lbs/hr	0.1040	0.0146			
	tons/yr	0.4558	0.0644			
Xylenes	lbs/hr	0.2631	0.0439			
	tons/yr	1.1534	0.1933			
Benzene	lbs/hr	0.3989	0.0135			
	tons/yr	1.7475	0.0595			

Enter any notes here:	1. Emissions are based on 98% Flare DRE operating 100% of the time.

Table 4

Fugitive Emissions
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

VOC Type:	Condensate VOC
Emission Type:	Steady State (continuous)

Gas Weight Fraction From Analysis:	VOC frac	0.191
	Benzene frac	0.000
	Toluene	0.000
	Ethylbenzene	0.000
	Xylenes	0.000
	n-Hexane	0.023
	Methane	0.603

Gas					
Number	Component	Pollutant	Emission Factor (kg/hr of THC per component)	kg/hr	lb/yr
400	Valves	Gas VOC	0.004500	0.34	6,624.61
		Non VOC	0.004500	1.46	28,064.99
472	Connectors	VOC	0.000200	0.02	347.42
		Non-VOC	0.000200	0.08	1,471.85
104	Flanges	VOC	0.000390	0.01	149.27
		Non-VOC	0.000390	0.03	632.40
			Total VOCs:	0.37	7,121.30
			Total THC:	1.93	37,290.55

Light Liquid Weight Fraction From Analysis:	VOC frac	0.974
	Benzene frac	0.002
	Toluene	0.007
	Ethylbenzene	0.006
	Xylenes	0.017
	n-hexane	0.053
	Methane	0.008

Light Liquid					
Number	Component	Pollutant	Emission Factor (kg/hr of THC per component)	kg/hr	lb/yr
416	Valves	Light Liquid VOC	0.002500	1.01	19,528.73
		Light Liquid Non-VOC		0.03	514.15
			Total VOC:	1.01	19,528.73
			Total THC:	1.04	20,042.88

Fugitive Total Emissions			
	Annual Emissions (lb/yr)	Annual Emissions (lb/hr)	Annual Emissions (tpy)
VOC	26,650.04	3.04	13.33
Ethylbenzene		0.01	0.06
Toluene		0.02	0.07
Xylenes		0.04	0.17
n-Hexane		0.22	0.96
TAPs (Benzene)		0.01	0.02
HAPs		0.29	1.28
CO_{2e}	565,717.91	64.58	282.86

Enter Notes Here:	Fugitive emissions based on an estimated component count Global Warming Potentials from EPA site <u>Reference to Emission factors used:</u> 1. Emission factors are for oil and gas production facilities (not refineries) come from the EPA's "Protocol for Equipment Leak Emission Estimates" November 1995, EPA 4531, R-95-017, Table 2-4. 2. Percent of speciated VOCs used in fugitive calculations are based on the total hydrocarbons, not of the total sample.

Table 5

Pneumatic Control Valve Emissions
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

Number of PCVs	32
Bleed Rate (scf/day/PCV)	6.6
Total Bleed Rate (scf/day)	211.2

Component	Mol%	Molecular Weight (lb/lb-mole)	Component Flow (scf/day)	Component Moles (lb-moles)	Component Emissions (lbs/day)	(lbs/hr)	(tons/year)
H2S	0	34.08	0	0.00	0.00	0.00	0.00
Nitrogen	0.4946	14.01	1.0445952	0.00	0.04	0.00	0.01
Carbon Dioxide	0.1467	44.01	0.3098304	0.00	0.04	0.00	0.01
Methane	77.6927	16.04	164.0869824	0.43	6.94	0.29	1.27
Ethane	14.1987	30.07	29.9876544	0.08	2.38	0.10	0.43
Propane	4.4938	44.1	9.4909056	0.03	1.10	0.05	0.20
Isobutane	0.5666	58.12	1.1966592	0.00	0.18	0.01	0.03
n-Butane	1.1838	58.12	2.5001856	0.01	0.38	0.02	0.07
Isopentane	0.3749	72.15	0.7917888	0.00	0.15	0.01	0.03
n-Pentane	0.2914	72.15	0.6154368	0.00	0.12	0.00	0.02
2-Methylpentane	0	86.18	0	0.00	0.00	0.00	0.00
3-Methylpentane	0	86.18	0	0.00	0.00	0.00	0.00
n-Hexane	0.5451	86.18	1.1512512	0.00	0.26	0.01	0.05
Methylcyclopentane	0	84.16	0	0.00	0.00	0.00	0.00
Benzene	0	78.11	0	0.00	0.00	0.00	0.00
2-Methylhexane	0	100.2	0	0.00	0.00	0.00	0.00
3-Methylhexane	0	100.2	0	0.00	0.00	0.00	0.00
Heptane	0	100.21	0	0.00	0.00	0.00	0.00
Methylcyclohexane	0	98.186	0	0.00	0.00	0.00	0.00
Toluene	0	92.14	0	0.00	0.00	0.00	0.00
Octane	0	114.23	0	0.00	0.00	0.00	0.00
Ethylbenzene	0	106.17	0	0.00	0.00	0.00	0.00
m & p-Xylene	0	106.16	0	0.00	0.00	0.00	0.00
o-Xylene	0	106.16	0	0.00	0.00	0.00	0.00
Nonane	0	128.2	0	0.00	0.00	0.00	0.00
C10+	0	174.28	0	0.00	0.00	0.00	0.00

	lb/hr	tpy
VOC Emissions	0.0916	0.4012
Benzene Emissions	0.0000	0.0000
Toluene Emissions	0.0000	0.0000
Ethylbenzene Emissions	0.0000	0.0000
Xylene Emissions	0.0000	0.0000
n-Hexane Emissions	0.0109	0.0477
HAPs Emissions	0.0109	0.0477
TAPs Emissions	0.0000	0.0000
CO_{2e} emissions	7.2262	31.6506

Enter any notes here:	1. PCV bleed rate obtained from the user manual for PCV http://issuu.com/rmcprocesscontrols/docs/mizer-pilot-operation--parts---installation-manual 2. Emissions per hour= Mol % x no. of PCV x bleed rate x MW / 379.48 / 24

Table 6

Uncontrolled Flashing Emissions
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

# Hours Operational	8760

	Condensate Tank Flashing Losses			Produced Water Tank Flashing Losses		
	Vapor Mass Fraction	Flashing Losses		Vapor Mass Fraction	Flashing Losses	
	wt%	lbs/hr	tpy	wt%	lbs/hr	tpy
Water	0.0950	0.2897	1.2689	2.5940	0.0000	0.0000
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0074	0.0224	0.0982	0.5024	0.1295	0.5674
Carbon Dioxide	0.1540	0.4694	2.0558	2.5439	0.6559	2.8727
Methane	3.3030	10.0699	44.1060	55.3792	14.2776	62.5357
Ethane	19.7050	60.0750	263.1287	22.3462	5.7612	25.2340
Propane	30.4702	92.8948	406.8791	11.1972	2.8868	12.6442
Isobutane	7.7155	23.5223	103.0278	0.6359	0.1639	0.7181
n-Butane	17.0657	52.0286	227.8851	2.6435	0.6815	2.9851
Isopentane	6.0892	18.5643	81.3117	0.5638	0.1454	0.6367
n-Pentane	6.2707	19.1175	83.7347	0.5503	0.1419	0.6214
2-Methylpentane	1.5994	4.8762	21.3578	0.0634	0.0163	0.0715
3-Methylpentane	0.9392	2.8633	12.5410	0.0983	0.0253	0.1110
n-Hexane	2.7709	8.4476	37.0006	0.0867	0.0223	0.0979
Methylcyclopentane	0.4057	1.2368	5.4170	0.1205	0.0311	0.1361
Benzene	0.1130	0.3444	1.5083	0.1851	0.0477	0.2091
2-Methylhexane	0.5442	1.6591	7.2669	0.0189	0.0049	0.0214
3-Methylhexane	0.4093	1.2478	5.4655	0.0148	0.0038	0.0167
Heptane	0.8284	2.5255	11.0617	0.0315	0.0081	0.0355
Methylcyclohexane	0.5919	1.8045	7.9035	0.1163	0.0300	0.1313
Toluene	0.0987	0.3008	1.3174	0.1521	0.0392	0.1718
Octane	0.6016	1.8342	8.0336	0.0135	0.0035	0.0153
Ethylbenzene	0.0262	0.0798	0.3496	0.0399	0.0103	0.0451
m & p-Xylene	0.0334	0.1019	0.4465	0.0505	0.0130	0.0570
o-Xylene	0.0306	0.0933	0.4087	0.0475	0.0122	0.0536
Nonane	0.1299	0.3959	1.7340	0.0045	0.0012	0.0051
C10+	0.0021	0.0064	0.0280	0.0000	0.0000	0.0000
Total VOCs	76.736	233.94	1,024.7	16.634	4.2886	18.7839
Total CO_{2e}		252.22	1,104.7		357.59	1,566.3
Total TAPs (Benzene)		0.3444	1.5083		0.0477	0.2091
Toluene		0.3008	1.3174		0.0392	0.1718
Ethylbenzene		0.0798	0.3496		0.0103	0.0451
Xylenes		0.1952	0.8552		0.0253	0.1106
n-Hexane		8.448	37.001		0.0223	0.0979
Total HAPs		9.368	41.031		0.1449	0.6345
Total	100.00	304.87	1,335.3	100.00	25.113	109.99

Enter any notes here:	Vapor mass fractions and Flashing losses from Promax output

Table 7

Uncontrolled Working and Breathing Losses

Stanley Well Pad

Doddridge, West Virginia

Antero Resources Corporation

Condensate Tank Information	
Number of Tanks	10
Maximum Working Losses (lbs/hr)	9.4873
Maximum Breathing Losses (lbs/hr)	10.4902

	Condensate Tank W/B Losses						
	Vapor Mass Fraction	Working Losses		Breathing Losses		Max W/B Losses	
	wt%	lbs/hr	tpy	lbs/hr	tpy	lbs/hr	tpy
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0003	0.0000	0.0001	0.0000	0.0001	0.0001	0.0003
Carbon Dioxide	0.1818	0.0172	0.0755	0.0191	0.0835	0.0363	0.1590
Methane	0.7253	0.0688	0.3014	0.0761	0.3332	0.1449	0.6346
Ethane	24.9627	2.3683	10.3730	2.6186	11.4697	4.9869	21.8427
Propane	32.6152	3.0943	13.5530	3.4214	14.9858	6.5157	28.5388
Isobutane	7.8278	0.7426	3.2528	0.8212	3.5967	1.5638	6.8494
n-Butane	17.0065	1.6134	7.0669	1.7840	7.8140	3.3975	14.8809
Isopentane	5.7989	0.5502	2.4097	0.6083	2.6644	1.1585	5.0741
n-Pentane	5.8731	0.5572	2.4405	0.6161	2.6985	1.1733	5.1391
2-Methylpentane	1.4784	0.1403	0.6144	0.1551	0.6793	0.2954	1.2937
3-Methylpentane	0.8636	0.0819	0.3589	0.0906	0.3968	0.1725	0.7557
n-Hexane	0.1733	0.0164	0.0720	0.0182	0.0796	0.0346	0.1516
Methylcyclopentane	0.3415	0.0324	0.1419	0.0358	0.1569	0.0682	0.2988
Benzene	0.0058	0.0006	0.0024	0.0006	0.0027	0.0012	0.0051
2-Methylhexane	0.0322	0.0031	0.0134	0.0034	0.0148	0.0064	0.0282
3-Methylhexane	0.3641	0.0345	0.1513	0.0382	0.1673	0.0727	0.3186
Heptane	0.6794	0.0645	0.2823	0.0713	0.3122	0.1357	0.5945
Methylcyclohexane	0.4814	0.0457	0.2001	0.0505	0.2212	0.0962	0.4213
Toluene	0.0109	0.0010	0.0045	0.0011	0.0050	0.0022	0.0096
Octane	0.4650	0.0441	0.1932	0.0488	0.2136	0.0929	0.4068
Ethylbenzene	0.0054	0.0005	0.0023	0.0006	0.0025	0.0011	0.0047
m & p-Xylene	0.0089	0.0008	0.0037	0.0009	0.0041	0.0018	0.0078
o-Xylene	0.0070	0.0007	0.0029	0.0007	0.0032	0.0014	0.0061
Nonane	0.0904	0.0086	0.0376	0.0095	0.0415	0.0181	0.0791
C10+	0.0010	0.0001	0.0004	0.0001	0.0005	0.0002	0.0009
Total VOCs	74.130	7.0329	30.804	7.7764	34.0607	14.8093	64.865
Total CO_{2e}		1.7375	7.6101	1.9212	8.4146	3.6586	16.025
Total TAPs (Benzene)		0.0006	0.0024	0.0006	0.0027	0.0012	0.0051
Toluene		0.0010	0.0045	0.0011	0.0050	0.0022	0.0096
Ethylbenzene		0.0005	0.0023	0.0006	0.0025	0.0011	0.0047
Xylenes		0.0015	0.0066	0.0017	0.0073	0.0032	0.0139
n-Hexane		0.0164	0.0720	0.0182	0.0796	0.0346	0.1516
Total HAPs		0.0201	0.0878	0.0222	0.0971	0.0422	0.1849
Total	100.00	9.4873	41.5542	10.4902	45.9473	19.9775	87.501

Table 7

Uncontrolled Working and Breathing Losses
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

Produced Water Tank Information	
Number of Tanks	2
Maximum Working Losses (lbs/hr)	0.2149
Maximum Breathing Losses (lbs/hr)	0.0083

	Produced Water Tank W/B Losses						
	Vapor Mass Fraction	Working Losses		Breathing Losses		Max W/B Losses	
	wt%	lbs/hr	tpy	lbs/hr	tpy	lbs/hr	tpy
H2S	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nitrogen	0.0102	0.0000	0.0001	0.0000	0.0000	0.0000	0.0001
Carbon Dioxide	3.4697	0.0075	0.0327	0.0003	0.0013	0.0077	0.0339
Methane	3.1154	0.0067	0.0293	0.0003	0.0011	0.0070	0.0305
Ethane	1.1599	0.0025	0.0109	0.0001	0.0004	0.0026	0.0113
Propane	0.1416	0.0003	0.0013	0.0000	0.0001	0.0003	0.0014
Isobutane	0.0010	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Butane	0.0063	0.0000	0.0001	0.0000	0.0000	0.0000	0.0001
Isopentane	0.0003	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Pentane	0.0002	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
2-Methylpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3-Methylpentane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Hexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Methylcyclopentane	0.0001	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Benzene	0.0002	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
2-Methylhexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3-Methylhexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Heptane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Methylcyclohexane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Toluene	0.0001	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Octane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Ethylbenzene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
m & p-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
o-Xylene	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Nonane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
C10+	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total VOCs	0.1500	0.0003	0.0014	0.0000	0.0001	0.0003	0.0015
Total CO_{2e}		0.1749	0.7659	0.0067	0.0295	0.1816	0.7954
Total TAPs (Benzene)		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Toluene		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Ethylbenzene		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Xylenes		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
n-Hexane		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total HAPs		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Total	100.00	0.2149	0.9414	0.0083	0.0362	0.2232	0.9777

Enter any notes here:	Vapor mass fractions, working losses and breathing losses from Promax output

Table 8

Loading Emissions
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

Annual Loading	Oil Truck Loading	Water Truck Loading
RVP	3.41	1.0242
Annual Average Temp (F)	63.8	72.1
S (saturation factor)	0.6	0.6
P (true vapor pressure)	1.84	0.45
M (MW of vapor)	44.20	18.43
Collection Efficiency (%)	0	0
Loading Loss (lb/10^3 gal)*	1.16	0.12
Maximum Throughput (gallons/hr)	10,080	10,080
Average Throughput (gallons/yr)	12,264,000	73,584,000
Loading Emissions (lbs/hr)	11.71	1.17
Loading Emissions (tpy)	7.12	4.26

	Condensate Tank Loading Losses			Produced Water Tank Loading Losses		
	Vapor Mass Fraction	Loading Losses		Vapor Mass Fraction	Loading Losses	
	wt%	lbs/hr	tpy	wt%	lbs/hr	tpy
H2S	0.0000	0.00	0.00	0.0000	0.00E+00	0.00E+00
Nitrogen	0.0003	0.00	0.00	0.0102	1.19E-04	4.34E-04
Carbon Dioxide	0.1818	0.02	0.01	3.4697	4.05E-02	1.48E-01
Methane	0.7253	0.08	0.05	3.1154	3.64E-02	1.33E-01
Ethane	24.9627	2.92	1.78	1.1599	1.35E-02	4.94E-02
Propane	32.6152	3.82	2.32	0.1416	1.65E-03	6.04E-03
Isobutane	7.8278	0.92	0.56	0.0010	1.18E-05	4.29E-05
n-Butane	17.0065	1.99	1.21	0.0063	7.36E-05	2.69E-04
Isopentane	5.7989	0.68	0.41	0.0003	3.93E-06	1.44E-05
n-Pentane	5.8731	0.69	0.42	0.0002	2.80E-06	1.02E-05
2-Methylpentane	1.4784	0.17	0.11	0.0000	6.15E-08	2.25E-07
3-Methylpentane	0.8636	0.10	0.06	0.0000	2.31E-07	8.44E-07
n-Hexane	0.1733	0.02	0.01	0.0000	3.26E-09	1.19E-08
Methylcyclopentane	0.3415	0.04	0.02	0.0001	6.10E-07	2.23E-06
Benzene	0.0058	0.00	0.00	0.0002	2.88E-06	1.05E-05
2-Methylhexane	0.0322	0.00	0.00	0.0000	3.01E-10	1.10E-09
3-Methylhexane	0.3641	0.04	0.03	0.0000	3.53E-09	1.29E-08
Heptane	0.6794	0.08	0.05	0.0000	5.51E-09	2.01E-08
Methylcyclohexane	0.4814	0.06	0.03	0.0000	1.26E-07	4.59E-07
Toluene	0.0109	0.00	0.00	0.0001	1.14E-06	4.16E-06
Octane	0.4650	0.05	0.03	0.0000	4.62E-10	1.69E-09
Ethylbenzene	0.0054	0.00	0.00	0.0000	1.68E-07	6.14E-07
m & p-Xylene	0.0089	0.00	0.00	0.0000	2.37E-07	8.66E-07
o-Xylene	0.0070	0.00	0.00	0.0000	2.33E-07	8.52E-07
Nonane	0.0904	0.01	0.01	0.0000	7.23E-11	2.64E-10
C10+	0.0010	0.00	0.00	0.0000	3.56E-17	1.30E-16
Total VOCs	74.1300	8.680	5.280	0.1500	1.75E-03	6.39E-03
Total CO_{2e}		2.144	1.3045		0.9500	3.4674
Total TAPs (Benzene)		0.0007	0.0004		0.0000	0.0000
Toluene		0.0013	0.0008		0.0000	0.0000
Ethylbenzene		0.0006	0.0004		0.0000	0.0000
Xylenes		0.0019	0.0011		0.0000	0.0000
n-Hexane		0.0203	0.0123		0.0000	0.0000
Total HAPs		0.0247	0.0151		0.0000	0.0000
Total	100.0000	11.7094	7.1232	100.0000	1.1677	4.2622

Enter any notes here

Vapor mass fractions and loading losses from Promax output
Using equation L_L = 12.46 SPM/T from AP-42, Chapter 5, Section 5.2-4
MW was obtained by Promax; RVP was taken from laboratory reports
Annual Average Temp (F) obtained from Charleston, WV (preset in Promax)
S (saturation factor) is based on submerged loading, dedicated service as it was most representative
True vapor pressure (TVP) equation from AP-42, Chapter 7, Figure 7.1-13b
Loading emissions are vented to the atmosphere.

Table 9

Gas Production Unit Heater Emissions
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

Number of Units	8
Heater Rating (MMBtu/hr)	1.50
Operating hours/year	8760
Fuel Heat Value (Btu/scf)	1,247

Pollutant	Emission Factors (lb/MMscf)	lb/hr	tpy
NOx	100	0.962	4.215
CO	84	0.808	3.540
CO_2	120,000	1154.716	5057.656
Lead	0.0005	4.81E-06	2.11E-05
N_2O	2.2	0.021	0.093
PM (Total)	7.6	0.073	0.320
SO_2	0.6	0.006	0.025
TOC	11	0.106	0.464
Methane	2.3	0.022	0.097
VOC	5.5	0.053	0.232
HAPS			
2-Methylnaphthalene	2.40E-05	2.31E-07	1.01E-06
Benzene	2.10E-03	2.02E-05	8.85E-05
Dichlorobenzene	1.20E-03	1.15E-05	5.06E-05
Fluoranthene	3.00E-06	2.89E-08	1.26E-07
Fluorene	2.80E-06	2.69E-08	1.18E-07
Formaldehyde	7.50E-02	7.22E-04	3.16E-03
Hexane	1.80E+00	1.73E-02	7.59E-02
Naphthalene	6.10E-04	5.87E-06	2.57E-05
Phenanathrene	1.70E-05	1.64E-07	7.17E-07
Toluene	3.40E-03	3.27E-05	1.43E-04

	lb/hr	tpy
TOTAL Uncontrolled VOC	0.053	0.232
TOTAL Uncontrolled HAPs	0.018	0.079
TOTAL Uncontrolled TAPs (Benzene)	0.000	0.000
TOTAL Uncontrolled TAPs (Formaldehyde)	0.001	0.003
TOTAL CO_{2e} Emissions	1,161.58	5,087.71

Enter any notes here:
All Emission Factors based off AP-42 Sec 1.4 Natural Gas Combustion

Table 10

Enclosed Combustor Emissions
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

General Information	
Unit Name:	EC001, EC002

Pollutant	Emission Factor (lb/MMscf)
NOx	100
CO	84
PM10	7.6
PM2.5	5.7
SO_2	0.6
CO_2	120,000
VOC	5.5
benzene	2.10E-03
Hexane	1.80E+00
Toluene	3.40E-03
Formaldehyde	7.50E-02
N_2O	2.20
Lead	5.00E-04

Constants	
Btu/MMBtu	1,000,000
scf/MMscf	1,000,000
lb/ton	2,000
H_2S molecular weight	34.08
SO_2 molecular weight	64.06
seconds/hour	3,600
inches/ft	12

Destruction Efficiency	
VOC percent destruction efficiency (%)	98
H_2S percent destruction efficiency (%)	98
No. of Enclosed Combustors	2

Enclosed Combustor operating hours	8760

Stream Information							
	1	2	3	4	5	6	Total
Stream Sent to Enclosed Combustor (Enter Name of Each Stream Here)	pilot(s)	added fuel stream(s)	Oil Tank Flash Emissions	Water Tank Flash Emissions	Oil Tank W/B Emissions	Water Tank W/B Emissions	-
Maximum Expected Hourly Volumetric Flow Rate of Stream (scf/hr)	25.2	--	2,617.32	517.22	171.51	4.60	3,335.84
Maximum Expected Annual Volumetric Flow Rate of Stream (scf/yr)	110,376.00	--	22,927,705.99	4,530,828.05	1,502,399.63	40,272.26	29,111,581.93
Heating Content (Btu/ft3)	1,247		2,314.06	1,095.87	2,314.06	1,095.87	2,106.02

Mass Flow Rates of the Vapors Sent to this Control Device, Hourly Basis (lb/hr)							
	1	2	3	4	5	6	Total
Stream Sent to Enclosed Combustor/Vapor Combustor	pilot(s)	added fuel stream(s)	Oil Tank Flash Emissions	Water Tank Flash Emissions	Oil Tank W/B Emissions	Water Tank W/B Emissions	-
H2S	-	-	0.000	0.000	0.000	0.000	0.000
Total VOC	-	-	233.945	4.289	14.809	0.000	253.04
Benzene	-	-	0.344	0.048	0.001	0.000	0.393
Toluene	-	-	0.301	0.039	0.002	0.000	0.342
Ethylbenzene	-	-	0.080	0.010	0.001	0.000	0.091
Xylenes	-	-	0.195	0.025	0.003	0.000	0.224
n-Hexane	-	-	8.448	0.022	0.035	0.000	8.505
HAPs	-	-	9.368	0.145	0.042	0.000	9.555
Total Mass Flow	-	-	304.871	25.113	19.978	0.223	350.185
Mass Flow Rates of the Vapors Sent to this Control Device, Annual Basis (tpy)							
H2S	-	-	0.000	0.000	0.000	0.000	0.000
Total VOC	-	-	1024.679	18.784	64.865	0.001	1108.329
Benzene	-	-	1.508	0.209	0.005	0.000	1.722
Toluene	-	-	1.317	0.172	0.010	0.000	1.499
Ethylbenzene	-	-	0.350	0.045	0.005	0.000	0.399
Xylenes	-	-	0.855	0.111	0.014	0.000	0.980
n-Hexane	-	-	37.001	0.098	0.152	0.000	37.250
HAP	-	-	41.031	0.634	0.185	0.000	41.850
Total Mass Flow	-	-	1335.336	109.994	87.501	0.978	1533.809

Table 10

Enclosed Combustor Emissions
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

Controlled Emissions							
Hourly (lb/hr)							
	1	2	3	4	5	6	Total
Stream Sent to Enclosed Combustor/Vapor Combustor	pilot(s)	added fuel stream(s)	Oil Tank Flash Emissions	Water Tank Flash Emissions	Oil Tank W/B Emissions	Water Tank W/B Emissions	-
NOx	0.003	-	0.262	0.052	0.017	0.000	0.33
CO	0.002	-	0.220	0.043	0.014	0.000	0.28
PM2.5	0.000	-	0.015	0.003	0.001	0.000	0.02
PM10	0.000	-	0.020	0.004	0.001	0.000	0.03
H2S	0.000	-	0.000	0.000	0.000	0.000	0.00
SO_2	0.000	-	0.000	0.000	0.000	0.000	0.00
CO_2	3.024	-	-	-	-	-	3.02
Total VOC	0.000	-	4.679	0.086	0.296	0.000	5.06
Benzene	0.000	-	0.007	0.001	0.000	0.000	0.01
Toluene	0.000	-	0.006	0.001	0.000	0.000	0.01
Ethylbenzene	0.000	-	0.002	0.000	0.000	0.000	0.00
Xylenes	0.000	-	0.004	0.001	0.000	0.000	0.00
n-Hexane	0.000	-	0.169	0.000	0.001	0.000	0.17
HAP	0.000	-	0.187	0.003	0.001	0.000	0.19
N_2O	0.000	-	0.006	0.001	0.000	0.000	0.01
Lead	0.000	-	0.000	0.000	0.000	0.000	0.00
Formaldehyde	0.000	-	-	-	-	-	0.00
Annual (tpy)							
	1	2	3	4	5	6	Total
Stream Sent to Enclosed Combustor/Vapor Combustor	pilot(s)	added fuel stream(s)	Oil Tank Flash Emissions	Water Tank Flash Emissions	Oil Tank W/B Emissions	Water Tank W/B Emissions	-
NOx	0.011	-	1.146	0.227	0.075	0.002	1.46
CO	0.009	-	0.963	0.190	0.063	0.002	1.23
PM2.5	0.001	-	0.065	0.013	0.004	0.000	0.08
PM10	0.001	-	0.087	0.017	0.006	0.000	0.11
H_2S	0.000	-	0.000	0.000	0.000	0.000	0.00
SO_2	0.000	-	0.000	0.000	0.000	0.000	0.00
CO_2	13.245	-	-	-	-	-	13.25
Total VOC	0.001	-	20.494	0.376	1.297	0.000	22.17
Benzene	0.000	-	0.030	0.004	0.000	0.000	0.03
Toluene	0.000	-	0.026	0.003	0.000	0.000	0.03
Ethylbenzene	0.000	-	0.007	0.001	0.000	0.000	0.01
Xylenes	0.000	-	0.017	0.002	0.000	0.000	0.02
n-Hexane	0.000	-	0.740	0.002	0.003	0.000	0.75
HAP	0.000	-	0.821	0.013	0.004	0.000	0.84
N_2O	0.000	-	0.025	0.005	0.002	0.000	0.03
Lead	0.000	-	0.000	0.000	0.000	0.000	0.00
Formaldehyde	0.000	-	-	-	-	-	0.00

Enclosed Combustor/Vapor Combustor Total Emissions		
	Hourly Emissions (lb/hr)	Annual Emissions (tpy)
Total VOC	5.06	22.17
NOx	3.34E-01	1.46E+00
CO	2.80E-01	1.23E+00
PM2.5	1.90E-02	8.33E-02
PM10	2.54E-02	1.11E-01
H_2S	8.04E-06	3.52E-05
SO_2	1.51E-05	6.62E-05
Benzene (TAPs)	7.87E-03	3.44E-02
Formaldehyde (TAPs)	1.89E-06	8.28E-06
HAPs	0.19	0.84
CO_2e	1359.83	5956.06
N_2O	7.34E-03	3.21E-02
Lead	1.67E-06	7.31E-06

Enter any notes here as needed
1. Emission Factors from AP-42 Tables 1.4-1, 1.4-2, and 1.4.3

Table 11

Enclosed Combustor GHG Emissions
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

Enclosed Combustor CO_2 and CH_4 Emissions

Components	Mole fraction of oil flash gas constituents[a]	Volume of oil flash gas sent to Enclosed Combustor *scf/year*	Mole fraction of water flash gas constituents[a]	Volume of water flash gas sent to Enclosed Combustor *scf/year*	Mole fraction of oil tank vapors constituents[a]	Volume of oil tank vapor sent to Enclosed Combustor *scf/year*	Mole fraction of water tank vapors constituents[a]	Volume of water tank vapors sent to Enclosed Combustor *scf/year*	Component volume of gas sent to Enclosed Combustor *scf/year*	Number of carbon atoms	Combustion Efficiency	Combusted CO_2 Volume[b] *scf/year*	Uncombusted CO_2 and CH_4 Volume[b] *scf/year*	Volume GHGs Emitted *scf/year*
CO_2	0.002	22,927,706	0.0506	4,530,828	0.0018	1,502,400	0.015	40,272	267,995	1	0	--	267,995	95,981,436
Methane	0.091	22,927,706	3.0210	4,530,828	0.0200	1,502,400	0.036	40,272	15,809,277	1	0.98	15,493,092	316,186	316,186
Ethane	0.290	22,927,706	0.6503	4,530,828	0.3670	1,502,400	0.007	40,272	10,148,694	2	0.98	19,891,441	--	
Propane	0.306	22,927,706	0.2222	4,530,828	0.3269	1,502,400	0.001	40,272	8,510,326	3	0.98	25,020,360	--	
i-Butane	0.059	22,927,706	0.0096	4,530,828	0.0595	1,502,400	0.000	40,272	1,480,148	4	0.98	5,802,181	--	
n-Butane	0.130	22,927,706	0.0398	4,530,828	0.1293	1,502,400	0.000	40,272	3,354,770	4	0.98	13,150,699	--	
Pentane	0.076	22,927,706	0.0135	4,530,828	0.0715	1,502,400	0.000	40,272	1,907,316	5	0.98	9,345,847	--	
Hexane	0.027	22,927,706	0.0025	4,530,828	0.0129	1,502,400	0.000	40,272	656,095	6	0.98	3,857,841	--	
Benzene	0.001	22,927,706	0.0021	4,530,828	0.0000	1,502,400	0.000	40,272	24,123	6	0.98	141,842	--	
Heptanes	0.010	22,927,706	0.0018	4,530,828	0.0065	1,502,400	0.000	40,272	247,480	7	0.98	1,697,714	--	
Toluene	0.000	22,927,706	0.0014	4,530,828	0.0001	1,502,400	0.000	40,272	17,492	7	0.98	119,996	--	
Octane	0.005	22,927,706	0.0011	4,530,828	0.0040	1,502,400	0.000	40,272	125,759	8	0.98	985,952	--	
Ethyl benzene	0.000	22,927,706	0.0003	4,530,828	0.0000	1,502,400	0.000	40,272	4,028	8	0.98	31,582	--	
Xylenes	0.000	22,927,706	0.0008	4,530,828	0.0001	1,502,400	0.000	40,272	9,881	8	0.98	77,465	--	
Nonane	0.000	22,927,706	0.0000	4,530,828	0.0003	1,502,400	0.000	40,272	10,888	9	0.98	96,030	--	
Decane plus	0.000	22,927,706	0.0000	4,530,828	0.0000	1,502,400	0.000	40,272	143	10	0.98	1,399	--	
											Subtotal	**95,713,441**	--	

Pollutant	Volume Emitted *scf/year*	Density of GHG[c] *lb/scf*	Conversion Factor *lb/ton*	GWF	Emissions[c] *lbs/hr*	Emissions[c] *(tons/yr)*
CO_2	95,981,436	0.12	2000	1	1270.58	5,565.15
CH_4	316,186	0.09	2000	25	3.36	14.71
				CO_2e Emissions	**1,354.5**	**5932.85**

GHG Emissions Summary

Notes

a Flashing/Working/Breathing Losses from ProMax output reports

b 40 CFR 98.233 (n)(4): Eqns: W-19, W-20 and W-21

c 40 CFR 98.233(v) Eqn W-36 - density at 60F and 14.7 psia

Table 12

Haul Road Emissions
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

	PM	PM10
Particle Size Multiplier (k)	0.8	0.36
Silt Content of Road Surface Material (s) (%)	5.1	5.1
Days per Year with Precipitation > 0.01 in (p)	150	150
Control Efficiency for Watering [1] (%)	50	50

Tanker Truck Trip Calculation	
Condensate Production (bbl/day)	800
PW Production (bbl/day)	4,800
Truck Capacity (bbl)	200

Pick Up Truck Trip Calculation	
No of Trips Per day	2
Trips Per Year	730

	# of Wheels	Mean Vehicle Weight (W) (tons)	Mean Vehicle Speed (S) (mph)	Miles Per Trip (miles)	Maximum Trips per Hour	Maximum Trips per Year	Vehicle Miles Travelled (miles/hr)	Vehicle Miles Travelled (miles/year)	PM (lbs/VMT)	PM10 (lbs/VMT)
Tanker Trucks Condensate	10	40	10	0.6000	1	1460	0.6000	876.0000	3.8175	1.7179
Tanker Trucks PW	10	40	10	0.6000	1	8760	0.6000	5256.0000	3.8175	1.7179
Pick Up Truck	4	3	10	0.2840	1	730	0.2840	207.3200	0.3467	0.1560

	Uncontrolled Emissions						Controlled Emissions					
	PM			PM10			PM			PM10		
	(lbs/hr)	(lbs/year)	(tpy)	(lbs/hr)	(lbs/year)	(tpy)	(lbs/hr)	(lbs/year)	(tpy)	(lbs/hr)	(lbs/year)	(tpy)
Tanker Trucks Condensate	2.2905	3344.1557	1.6721	1.0307	1504.8701	0.7524	1.1453	1672.0779	0.8360	0.5154	752.4350	0.3762
Tanker Trucks PW	2.2905	20064.9345	10.0325	1.0307	9029.2205	4.5146	1.1453	10032.4672	5.0162	0.5154	4514.6103	2.2573
Pick Up Truck	0.0985	71.8736	0.0359	0.0443	32.3431	0.0162	0.0492	35.9368	0.0180	0.0222	16.1716	0.0081
Total Emissions	4.6795	23,480.9639	11.7405	2.1058	10,566.4337	5.2832	2.3397	11,740.4819	5.8702	1.0529	5,283.2169	2.6416

Enter any notes here:	1 EPA, AP-42, Volume I, Section 13.2.2 Unpaved Roads (11/06); assume 2:1 moisture ratio Section 13.2.2 Unpaved Roads (11/06) Source: Attachment L, Fugitive Emissions from Unpaved Haul Roads, Rev 03/2007, West Virginia Department of Environmental Protection

Table 13

Engine Emissions
Stanley Well Pad
Doddridge, West Virginia
Antero Resources Corporation

Kubota DG972-E2

Power (hp)	24
Fuel consumption (lbs/BHP-hr) [1]	0.449
Heat Content of Fuel (Btu/scf)	1247.06
Density of NG (lb/scf)	0.056
Operating Hours/year	8760

Pollutant	Emission Factors (g/hp-hr)	Emission Factors (lb/MMBtu)	lb/hr	tpy
NOx[1]	5.97		0.3158	1.3831
CO[2]	106.7		5.6445	24.7228
CO_2		110.000	26.3967	115.62
$PM_{2.5}$		9.910E-03	0.0024	0.0104
PM_{10}		9.500E-03	0.0023	0.0100
PM (Total)		9.910E-03	0.0024	0.0104
SO_2		5.880E-04	0.0001	0.0006
TOC		0.358	0.0859	0.3763
Methane		0.230	0.0552	0.2417
VOC[3]		0.0296	0.0071	0.0311
HAPS				
Benzene		1.58E-03	3.79E-04	1.66E-03
Ethylbenzene		2.48E-05	5.95E-06	2.61E-05
Formaldehyde		2.05E-02	4.92E-03	2.15E-02
Naphthalene		9.71E-05	2.33E-05	1.02E-04
Toluene		5.58E-04	1.34E-04	5.86E-04
Xylene		1.95E-04	4.68E-05	2.05E-04

	lb/hr	tpy
TOTAL Uncontrolled VOC	0.007	0.031
TOTAL Uncontrolled NOx	0.316	1.383
TOTAL Uncontrolled HAPs	0.006	0.024
TOTAL Uncontrolled TAPs (Benzene)	0.000	0.002
TOTAL Uncontrolled TAPs (Formaldehyde)	0.005	0.022
TOTAL CO_{2e} Emissions	27.78	121.7

Enter Any Notes Here:

1. Emission factor used for the 24 HP engine's NOx is the 40 CFR 1054 standard indicated on the EPA's Certificate of Conformity. See Appendix P.

2. Emission factor for CO was the Certification CO level taken from EPA's Non-Road Small SI 2013 Certification issued by Office of Transportation and Air Quality, March 2014.

3. Emission factors for all other contaminants including VOCs were obtained from AP-42, Section 3.2 "Natural Gas-fired Reciprocating Engines", Table 3.2-3.

Bryan Research & Engineering, Inc.

ProMax® 3.2

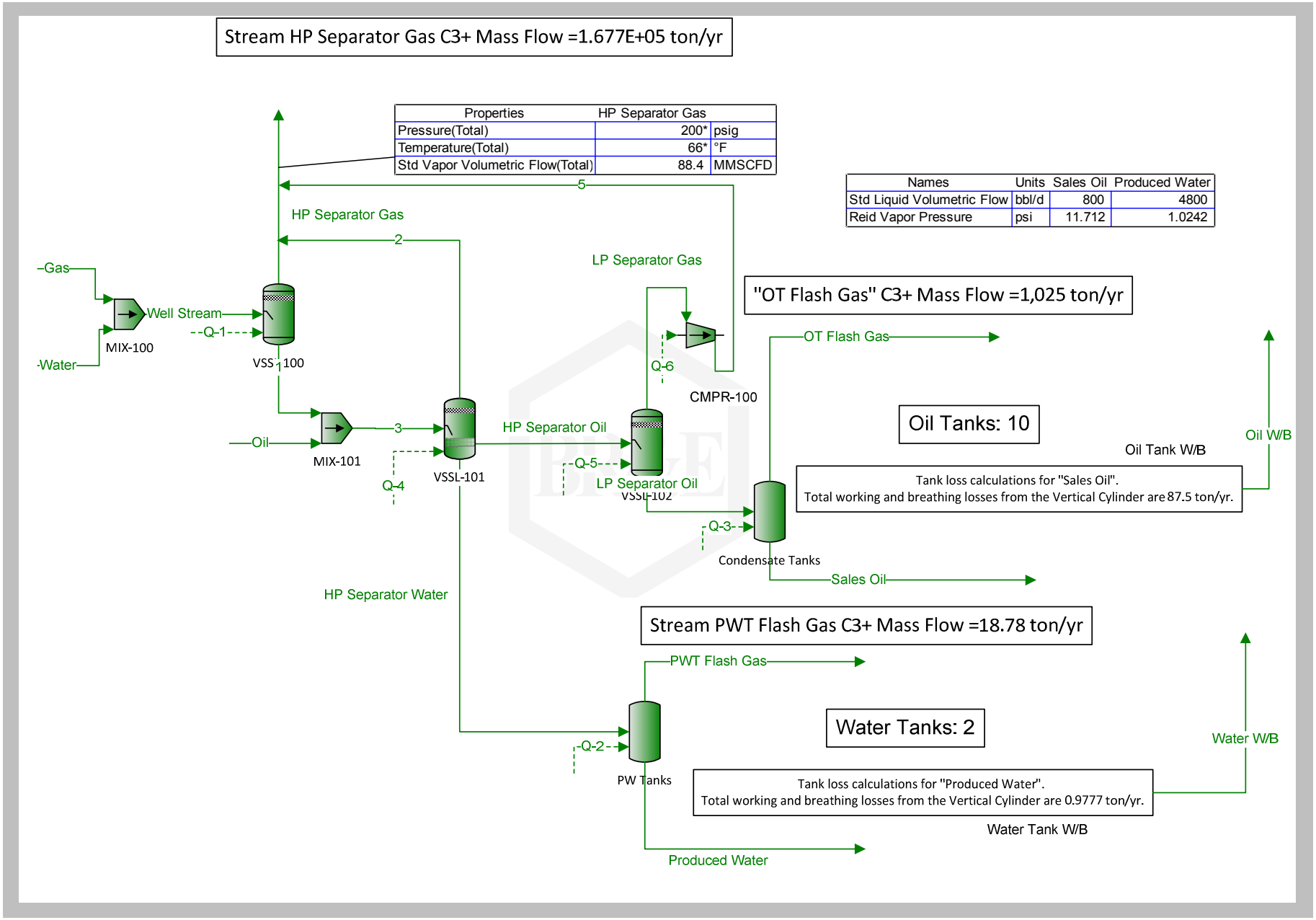
with

TSWEET® & PROSIM®

Simulation Report	
Client Name:	Antero Resources Corporation
Location:	West Virginia
Job:	Stanley Well Pad

Project Name:	PROMAX SCENARIO 3
File Name:	ProMax@V:\AirQuality\ANTERO RESOURCES\ProMax\Antero WV_Updated 2Ph Separator\PROMAX SCENARIO 3.PMX
ProMax Version:	3.2.13330.0

Report Created:	6/12/2015 10:32


Stream HP Separator Gas C3+ Mass Flow =1.677E+05 ton/yr
Properties | HP Separator Gas
Pressure(Total) | 200* | psig
Temperature(Total) | 66* | °F
Std Vapor Volumetric Flow(Total) | 88.4 | MMSCFD
Names | Units | Sales Oil | Produced Water
Std Liquid Volumetric Flow | bbl/d | 800 | 4800
Reid Vapor Pressure | psi | 11.712 | 1.0242
"OT Flash Gas" C3+ Mass Flow =1,025 ton/yr
Oil Tanks: 10
Water Tanks: 2
Stream PWT Flash Gas C3+ Mass Flow =18.78 ton/yr
Tank loss calculations for "Sales Oil".
Total working and breathing losses from the Vertical Cylinder are 87.5 ton/yr.
Tank loss calculations for "Produced Water".
Total working and breathing losses from the Vertical Cylinder are 0.9777 ton/yr.
Gas
Water
Well Stream
Oil
MIX-100
MIX-101
VSS 100
VSSL-101
VSSL-102
CMPR-100
Condensate Tanks
PW Tanks
HP Separator Gas
HP Separator Oil
HP Separator Water
LP Separator Gas
LP Separator Oil
OT Flash Gas
Sales Oil
PWT Flash Gas
Produced Water
Oil Tank W/B
Oil W/B
Water Tank W/B
Water W/B
Q-1
Q-2
Q-3
Q-4
Q-5
Q-6
2
3
5

Process Streams		Well Stream	HP Separator Gas	HP Separator Water	HP Separator Oil	OT Flash Gas	Sales Oil	Gas	Water	Oil	Produced Water	PWT Flash Gas	Oil W/B	Water W/B	1	3	LP Separator Oil
Phase: Total	Status	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved
Mole Fraction		%	%	%	%	%	%	%	%	%	%	%	%	%	%	%	%
Water		28.7041	0.156524	99.9661	0.0517839	0.233510	0.00486699	0	100	0	99.9967	3.02985	0.000118725	94.1901	99.9627	97.8661	0.0255382
H2S		0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Nitrogen		0.352671	0.493921	0.000123345	0.0164543	0.0116221	1.85250E-05	0.494658	0	0.0179998	4.42210E-06	0.377409	0.000455370	0.00669135	9.09774E-05	0.000466597	0.00106759
Carbon Dioxide		0.104603	0.146078	0.000972844	0.0357417	0.154871	0.00287906	0.146717	0	0.0309997	0.000589759	1.21632	0.182561	1.45262	0.00107601	0.00170363	0.0166204
Methane		55.3982	77.5806	0.0246369	4.91184	9.11491	0.0438867	77.7018	0	4.76595	0.00174859	72.6386	1.99841	3.57810	0.0279843	0.127358	0.863982
Ethane		10.1243	14.1780	0.00536606	5.72449	29.0118	0.861642	14.2004	0	5.72594	0.000438622	15.6378	36.6963	0.710738	0.00559480	0.125573	3.40665
Propane		3.20427	4.48718	0.00184921	6.53571	30.5911	3.39068	4.49433	0	6.54493	0.000165565	5.34325	32.6946	0.0591831	0.00194860	0.139181	5.84983
Isobutane		0.404010	0.565833	7.50256E-05	2.06276	5.87676	1.70532	0.566666	0	2.06698	2.48181E-06	0.230223	5.95316	0.000319269	7.82999E-05	0.0434295	2.08245
n-Butane		0.844100	1.18212	0.000324282	5.89758	12.9987	5.41519	1.18394	0	5.90894	2.27190E-05	0.957044	12.9337	0.00199737	0.000348886	0.124276	6.10080
Isopentane		0.267320	0.374384	5.44913E-05	3.76285	3.73637	4.06134	0.374944	0	3.76996	2.67515E-06	0.164443	3.55279	8.60034E-05	7.30268E-05	0.0791427	4.03196
n-Pentane		0.207781	0.291000	5.31537E-05	5.03533	3.84771	5.58289	0.291434	0	5.04595	2.58486E-06	0.160484	3.59826	6.12109E-05	5.44300E-05	0.105887	5.42602
2-Methylpentane		0	0	4.99297E-06	2.51940	0.821672	2.93319	0	0	2.52497	1.18622E-07	0.0154690	0.758355	1.12633E-06	0	0.0529588	2.74229
3-Methylpentane		0	0	8.06098E-06	1.64113	0.482477	1.91729	0	0	1.64498	4.99279E-07	0.0239978	0.442977	4.23634E-06	0	0.0345019	1.78757
n-Hexane		0.388680	0.544378	6.79802E-06	6.00456	1.42348	7.05779	0.545164	0	6.01594	1.29051E-07	0.0211643	0.0888805	5.96800E-08	3.58306E-05	0.126213	6.54840
Methylcyclopentane		0	0	1.13741E-05	0.921505	0.213396	1.08378	0	0	0.923991	1.88169E-06	0.0301263	0.179377	1.14368E-05	0	0.0193798	1.00509
Benzene		0	0	0.000170998	0.274434	0.0640181	0.322694	0	0	0.282997	0.000155332	0.0498717	0.00329177	5.81875E-05	0	0.00593558	0.299308
2-Methylhexane		0	0	1.27692E-06	2.37987	0.240437	2.83766	0	0	2.38498	2.57498E-08	0.00397064	0.0142108	4.73486E-09	0	0.0500225	2.60285
3-Methylhexane		0	0	1.00232E-06	1.87496	0.180833	2.23669	0	0	1.87898	2.11076E-08	0.00311392	0.160614	5.56530E-08	0	0.0394098	2.05082
Heptane		0	0	2.12665E-06	4.78171	0.365991	5.71602	0	0	4.79195	4.50293E-08	0.00660615	0.299701	8.66875E-08	0	0.100506	5.23233
Methylcyclohexane		0	0	8.88284E-06	3.39435	0.266867	4.05673	0	0	3.40197	1.02999E-06	0.0249223	0.216736	2.02048E-06	0	0.0713528	3.71409
Toluene		0	0	0.000100368	0.737743	0.0474013	0.883021	0	0	0.743993	8.94474E-05	0.0347472	0.00524329	1.95012E-05	0	0.0156045	0.807474
Octane		0	0	7.97318E-07	9.66836	0.233165	11.6204	0	0	9.68890	1.12198E-08	0.00249472	0.179922	6.37813E-09	0	0.203215	10.5909
Ethylbenzene		0	0	2.09259E-05	0.507941	0.0109172	0.610660	0	0	0.509995	1.84366E-05	0.00791821	0.00225470	2.49928E-06	0	0.0106966	0.556439
m-Xylene		0	0	2.72562E-05	0.774078	0.0139419	0.930953	0	0	0.776992	2.41118E-05	0.0100029	0.00370661	3.52471E-06	0	0.0162966	0.848047
o-Xylene		0	0	3.36330E-05	0.789747	0.0127638	0.949978	0	0	0.792992	3.06764E-05	0.00941353	0.00292518	3.46805E-06	0	0.0166322	0.865246
Nonane		0	0	2.38078E-07	5.64496	0.0448234	6.79601	0	0	5.65694	5.28319E-09	0.000738787	0.0311557	8.89240E-10	0	0.118649	6.18565
C10+		0	0	3.19828E-10	24.0507	0.000454420	28.9784	0	0	24.1018	9.98073E-13	1.01182E-06	0.000217289	2.74765E-16	0	0.505510	26.3586
Molar Flow		lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h
Water		3902.21	15.1924	3886.97	0.0432295	0.0160807	0.00337209	0	3902.21	0	3886.93	0.0371224	5.36578E-07	0.0114108	3887.02	3887.02	0.0194528
H2S		0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Nitrogen		47.9443	47.9407	0.00479600	0.0137362	0.000800360	1.28350E-05	47.9443	0	0.0149945	0.000171890	0.00462411	2.05804E-06	8.10634E-07	0.00353763	0.0185322	0.000813195
Carbon Dioxide		14.2204	14.1786	0.0378270	0.0298374	0.0106652	0.00199475	14.2204	0	0.0258239	0.0229243	0.0149027	0.000825084	0.000175980	0.0418404	0.0676644	0.0126600
Methane		7531.17	7530.09	0.957954	4.10043	0.627701	0.0304069	7531.17	0	3.97022	0.0679689	0.889985	0.00903181	0.000433474	1.08816	5.05838	0.658107
Ethane		1376.36	1376.14	0.208648	4.77884	1.99790	0.596988	1376.36	0	4.76993	0.0170495	0.191598	0.165849	8.61034E-05	0.217552	4.98748	2.59489
Propane		435.608	435.533	0.0719024	5.45605	2.10667	2.34923	435.608	0	5.45218	0.00643562	0.0654668	0.147763	7.16982E-06	0.0757707	5.52795	4.45590
Isobutane		54.9236	54.9206	0.00291721	1.72200	0.404705	1.18153	54.9236	0	1.72187	9.64695E-05	0.00282074	0.0269053	3.86783E-08	0.00304467	1.72492	1.58623
n-Butane		114.752	114.739	0.0126090	4.92333	0.895158	3.75191	114.752	0	4.92238	0.000883103	0.0117259	0.0584539	2.41974E-07	0.0135663	4.93594	4.64707
Isopentane		36.3411	36.3382	0.00211878	3.14125	0.257306	2.81389	36.3411	0	3.14052	0.000103985	0.00201479	0.0160568	1.04190E-08	0.00283962	3.14336	3.07120
n-Pentane		28.2470	28.2449	0.00206677	4.20352	0.264973	3.86810	28.2470	0	4.20347	0.000100475	0.00196629	0.0162623	7.41548E-09	0.00211649	4.20559	4.13307
2-Methylpentane		0	0	0.000194141	2.10321	0.0565847	2.03226	0	0	2.10340	4.61091E-06	0.000189530	0.00342739	1.36451E-10	0	2.10340	2.08884
3-Methylpentane		0	0	0.000313434	1.37002	0.0332259	1.32839	0	0	1.37034	1.94073E-05	0.000294027	0.00200203	5.13218E-10	0	1.37034	1.36162
n-Hexane		52.8395	52.8381	0.000264326	5.01264	0.0980283	4.88998	52.8395	0	5.01151	5.01628E-06	0.000259310	0.000401695	7.23002E-12	0.00139326	5.01290	4.98801
Methylcyclopentane		0	0	0.000442258	0.769278	0.0146955	0.750894	0	0	0.769720	7.31426E-05	0.000369115	0.000810692	1.38552E-09	0	0.769720	0.765589
Benzene		0	0	0.00064891	0.229099	0.00440862	0.223578	0	0	0.235748	0.00603787	0.000611040	1.48771E-05	7.04921E-09	0	0.235748	0.227987
2-Methylhexane		0	0	4.96502E-05	1.98673	0.0165577	1.96607	0	0	1.98678	1.00091E-06	4.86493E-05	6.42255E-05	5.73611E-13	0	1.98678	1.98263
3-Methylhexane		0	0	3.89729E-05	1.56523	0.0124531	1.54969	0	0	1.56526	8.20464E-07	3.81525E-05	0.000725892	6.74217E-12	0	1.56526	1.56214
Heptane		0	0	8.26904E-05	3.99180	0.0252041	3.96034	0	0	3.99188	1.75032E-06	8.09401E-05	0.00135450	1.05019E-11	0	3.99188	3.98554
Methylcyclohexane		0	0	0.000345391	2.83362	0.0183779	2.81070	0	0	2.83397	4.00363E-05	0.000305354	0.000979536	2.44774E-10	0	2.83397	2.82908
Toluene		0	0	0.00390261	0.615872	0.00326431	0.611800	0	0	0.619775	0.00347688	0.000425731	2.36970E-05	2.36251E-09	0	0.619775	0.615064
Octane		0	0	3.10020E-05	8.07120	0.0160569	8.05119	0	0	8.07123	4.36120E-07	3.05659E-05	0.000813158	7.72688E-13	0	8.07123	8.06725
Ethylbenzene		0	0	0.000813658	0.424032	0.000751814	0.423095	0	0	0.424846	0.000716642	9.70158E-05	1.01901E-05	3.02778E-10	0	0.424846	0.423847
m-Xylene		0	0	0.00105980	0.646205	0.000960109	0.645010	0	0	0.647265	0.000937242	0.000122558	1.67520E-05	4.27066E-10	0	0.647265	0.645970
o-Xylene		0	0	0.00130775	0.659285	0.000878981	0.658191	0	0	0.660593	0.00119241	0.000115337	1.32203E-05	4.20143E-10	0	0.660593	0.659070
Nonane		0	0	9.25716E-06	4.71244	0.00308678	4.70861	0	0	4.71245	2.05361E-07	9.05180E-06	0.000140808	1.07728E-13	0	4.71245	4.71169
C10+		0	0	1.24359E-08	20.0777	3.12937E-05	20.0777	0	0	20.0777	3.87957E-11	1.23971E-08	9.82038E-07	3.32869E-20	0	20.0777	20.0777
Mass Fraction		%	%	%	%	%	%	%	%	%	%	%	%	%	%	%	%
Water		25.7737	0.135025	99.9583	0.00856629	0.0950234	0.000708124	0	100	0	99.9942	2.59400	4.83874E-05	92.0949	99.9561	88.4772	0.00394482
H2S		0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Nitrogen		0.492411	0.662547	0.000191784	0.00423256	0.00735419	4.19114E-06	0.663391	0	0.00462148	6.87611E-06	0.502442	0.000288588	0.0101735	0.000141459	0.000655943	0.000256427
Carbon Dioxide		0.229448	0.307840	0.00237637	0.0144437	0.153957	0.00102331	0.309119	0	0.0125041	0.00144069	2.54392	0.181762	3.46966	0.00262842	0.00376254	0.00627166
Methane		44.2954	59.5960	0.0219373	0.723556	3.30299	0.00568607	59.6762	0	0.700758	0.00155707	55.3792	0.725278	3.11539	0.0249182	0.102531	0.118842
Ethane		15.1732	20.4140	0.00895571	1.58057	19.7050	0.209245	20.4417	0	1.57803	0.000732079	22.3462	24.9627	1.15989	0.00933758	0.189485	0.878299
Propane		7.04234	9.47464	0.00452591	2.64634	30.4702	1.20751	9.48766	0	2.64514	0.000405240	11.1972	32.6152	0.141639	0.00476924	0.307988	2.21174
Isobutane		1.17038	1.57479	0.000242034	1.10090	7.71550	0.800490	1.57677	0	1.10110	8.00679E-06	0.635914	7.82778	0.00100714	0.000252600	0.126673	1.03780
n-Butane		2.44528	3.29002	0.00104614	3.14755	17.0657	2.54193	3.29435	0	3.14774	7.32960E-05	2.64352	17.0065	0.00630071	0.00112553	0.362482	3.04036
Isopentane		0.961285	1.29342	0.000218213	2.49289	6.08923	2.36650	1.29507	0	2.49295	1.07134E-05	0.563835	5.79892	0.000336770	0.000292443	0.286548	2.49425
n-Pentane		0.747182	1.00534	0.000212857	3.33591	6.27068	3.25309	1.00663	0	3.33672	1.03517E-05	0.550263	5.87314	0.000239688	0.000217971	0.383380	3.35665
2-Methylpentane		0	0	2.38818E-05	1.99360	1.59943	2.04142	0	0	1.99429	5.67410E-07	0.0633511	1.47844	5.26790E-06	0	0.229023	2.02625
3-Methylpentane		0	0	3.85563E-05	1.29862	0.939167	1.33438	0	0	1.29925	2.38822E-06	0.0982794	0.863600	1.98136E-05	0	0.149205	1.32081
n-Hexane		1.66943	2.24635	3.25155E-05	4.75140	2.77088	4.91202	2.24910	0	4.75154	6.17293E-07	0.0866753	0.173276	2.79127E-07	0.000171383	0.545817	4.83854
Methylcyclopentane		0	0	5.31306E-05	0.712128	0.405669	0.736632	0	0	0.712719	8.79023E-06	0.120492	0.341521	5.22391E-05	0	0.0818484	0.725275
Benzene		0	0	0.000741368	0.196839	0.112954	0.203571	0	0	0.202603	0.000673484	0.185131	0.00581695	0.000246681	0	0.0232669	0.200461
2-Methylhexane		0	0	7.10172E-06	2.18971	0.544203	2.29639	0	0	2.19032	1.43218E-07	0.0189080	0.0322138	2.57497E-08	0	0.251536	2.23625
3-Methylhexane		0	0	5.57450E-06	1.72514	0.409296	1.81005	0	0	1.72562	1.17398E-07	0.0148283	0.364089	3.02659E-07	0	0.198170	1.76198
Heptane		0	0	1.18276E-05	4.39964	0.828381	4.62571	0	0	4.40085	2.50449E-07	0.0314581	0.679382	4.71435E-07	0	0.505392	4.49539
Methylcyclohexane		0	0	4.84091E-05	3.06030	0.591873	3.21687	0	0	3.06145	5.61345E-06	0.116291	0.481425	1.07670E-05	0	0.351576	3.12679

Toluene		0	0	0.000513289	0.624170	0.0986541	0.657082	0	0	0.628285	0.000457464	0.152149	0.0109293	9.75197E-05	0	0.0721521	0.637918
Octane		0	0	5.05511E-06	10.1411	0.601618	10.7202	0	0	10.1437	7.11388E-08	0.0135427	0.464952	3.95419E-08	0	1.16490	10.3730
Ethylbenzene		0	0	0.000123308	0.495167	0.0261803	0.523587	0	0	0.496243	0.000108645	0.0399500	0.00541525	1.44007E-05	0	0.0569884	0.506517
m-Xylene		0	0	0.000160610	0.754612	0.0334338	0.798210	0	0	0.756041	0.000142089	0.0504681	0.00890241	2.03093E-05	0	0.0868235	0.771964
o-Xylene		0	0	0.000198186	0.769887	0.0306086	0.814522	0	0	0.771610	0.000180773	0.0474943	0.00702558	1.99828E-05	0	0.0886114	0.787620
Nonane		0	0	1.69480E-06	6.64803	0.129856	7.03941	0	0	6.64973	3.76114E-08	0.00450300	0.0903983	6.18989E-09	0	0.763653	6.80229
C10+		0	0	3.63202E-09	45.1847	0.00210013	47.8837	0	0	45.1962	1.13348E-11	9.83822E-06	0.00100576	3.05110E-15	0	5.19032	46.2406
Mass Flow		**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**
Water		70299.4	273.696	70024.9	0.778791	0.289699	0.0607491	0	70299.4	0	70024.2	0.668771	9.66660E-06	0.205569	70025.7	70025.7	0.350448
H2S		0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Nitrogen		1343.08	1342.98	0.134352	0.384797	0.0224208	0.000359553	1343.08	0	0.420048	0.00481522	0.129537	5.76527E-05	2.27086E-05	0.0991009	0.519149	0.0227804
Carbon Dioxide		625.834	623.992	1.66475	1.31313	0.469371	0.0877882	625.834	0	1.13650	1.00889	0.655858	0.0363115	0.00774477	1.84138	2.97788	0.557159
Methane		120819	120801	15.3679	65.7810	10.0699	0.487801	120819	0	63.6921	1.09039	14.2776	0.144892	0.00695399	17.4568	81.1489	10.5577
Ethane		41385.7	41379.2	6.27384	143.695	60.0750	17.9508	41385.7	0	143.427	0.512663	5.76118	4.98692	0.00258905	6.54157	149.969	78.0259
Propane		19208.4	19205.1	3.17058	240.588	92.8948	103.591	19208.4	0	240.417	0.283783	2.88680	6.51571	0.000316158	3.34116	243.759	196.486
Isobutane		3192.28	3192.10	0.169555	100.087	23.5223	68.6731	3192.28	0	100.079	0.00560702	0.163948	1.56380	2.24807E-06	0.176963	100.256	92.1954
n-Butane		6669.65	6668.86	0.732865	286.155	52.0286	218.069	6669.65	0	286.099	0.0513279	0.681537	3.39747	1.40641E-05	0.788504	286.888	270.098
Isopentane		2621.96	2621.76	0.152867	226.637	18.5643	203.019	2621.96	0	226.585	0.00750238	0.145365	1.15848	7.51718E-07	0.204875	226.790	221.583
n-Pentane		2037.99	2037.83	0.149115	303.279	19.1175	279.079	2037.99	0	303.275	0.00724915	0.141866	1.17331	5.35018E-07	0.152702	303.428	298.196
2-Methylpentane		0	0	0.0167302	181.245	4.87621	175.131	0	0	181.261	0.000397347	0.0163328	0.295356	1.17587E-08	0	181.261	180.007
3-Methylpentane		0	0	0.0270103	118.062	2.86325	114.475	0	0	118.089	0.00167243	0.0253379	0.172526	4.42267E-08	0	118.089	117.338
n-Hexane		4553.46	4553.34	0.0227784	431.966	8.44762	421.396	4553.46	0	431.869	0.000432280	0.0223461	0.0346162	6.23050E-10	0.120065	431.989	429.844
Methylcyclopentane		0	0	0.0372202	64.7420	1.23677	63.1948	0	0	64.7792	0.00615565	0.0310645	0.0682274	1.16605E-07	0	64.7792	64.4316
Benzene		0	0	0.519359	17.8953	0.344366	17.4641	0	0	18.4147	0.471629	0.0477294	0.00116208	5.50627E-07	0	18.4147	17.8085
2-Methylhexane		0	0	0.00497504	199.074	1.65912	197.004	0	0	199.079	0.000100293	0.00487475	0.00643552	5.74769E-11	0	199.079	198.663
3-Methylhexane		0	0	0.00390516	156.839	1.24783	155.282	0	0	156.843	8.22121E-05	0.00382295	0.0727358	6.75578E-10	0	156.843	156.530
Heptane		0	0	0.00828574	399.986	2.52550	396.834	0	0	399.994	0.000175385	0.00811036	0.135724	1.05231E-09	0	399.994	399.359
Methylcyclohexane		0	0	0.0339125	278.222	1.80445	275.971	0	0	278.256	0.00393100	0.0299815	0.0961768	2.40334E-08	0	278.256	277.776
Toluene		0	0	0.359580	56.7455	0.300768	56.3703	0	0	57.1051	0.320354	0.0392262	0.00218341	2.17678E-07	0	57.1051	56.6711
Octane		0	0	0.00354131	921.961	1.83416	919.676	0	0	921.965	4.98173E-05	0.00349150	0.0928859	8.82630E-11	0	921.965	921.510
Ethylbenzene		0	0	0.0863820	45.0173	0.0798164	44.9179	0	0	45.1037	0.0760823	0.0102997	0.00108183	3.21445E-08	0	45.1037	44.9977
m-Xylene		0	0	0.112514	68.6043	0.101930	68.4774	0	0	68.7169	0.0995023	0.0130114	0.00177848	4.53331E-08	0	68.7169	68.5794
o-Xylene		0	0	0.138837	69.9930	0.0933170	69.8769	0	0	70.1319	0.126592	0.0122447	0.00140354	4.46044E-08	0	70.1319	69.9702
Nonane		0	0	0.00118728	604.395	0.395895	603.903	0	0	604.396	2.63386E-05	0.00116094	0.0180593	1.38167E-11	0	604.396	604.299
C10+		0	0	2.54437E-06	4107.90	0.00640269	4107.89	0	0	4107.90	7.93760E-09	2.53644E-06	0.000200925	6.81049E-18	0	4107.90	4107.90

Process Streams		**Well Stream**	**HP Separator Gas**	**HP Separator Water**	**HP Separator Oil**	**OT Flash Gas**	**Sales Oil**	**Gas**	**Water**	**Oil**	**Produced Water**	**PWT Flash Gas**	**Oil W/B**	**Water W/B**	**1**	**3**	**LP Separator Oil**
Phase: Total	**Status**	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved
Property	**Units**																
Temperature	°F	60.3	66.0	70.0	70.0	75.9	75.9	67.0	67.0	67.0	75.9	75.94	75.9425	75.9425	66	66.0894	70
Pressure	psig	200	200	200	200	0	0	300	200	300	0	0	8.81720	-14.2252	200	200	40
Mole Fraction Vapor	%	71.3764	100	0	0	100	0	100	0	0	0	100	100	100	0	0	0
Mole Fraction Light Liquid	%	28.6236	0	100	100	0	100	0	100	100	100	0	0	0	100	2.10145	100
Mole Fraction Heavy Liquid	%	0	0	0	0	0	0	0	0	0	0	0	0	0	0	97.8985	0
Molecular Weight	lb/lbmol	20.1	20.9	18.0	108.9	44.3	123.8	20.9	18.0	109.1	18.0	21.0422	44.2029	18.4251	18.0165	19.9270	116.628
Mass Density	lb/ft^3	1.1	0.8	62.3	45.0	0.1	45.8	1.3	62.3	45.2	62.2	0.0540011	0.185805	0.00150976	62.2960	59.6893	45.4833
Molar Flow	lbmol/h	13594.6	9706.1	3888.3	83.5	6.9	69.3	9692.4	3902.2	83.3	3887.1	1.22522	0.451950	0.0121146	3888.46	3971.77	76.1714
Mass Flow	lb/h	272756.3	202699.9	70054.1	9091.3	304.9	8578.9	202457.0	70299.4	9089.0	70028.3	25.7815	19.9775	0.223214	70056.4	79145.4	8883.75
Vapor Volumetric Flow	MCFH	238.3	240.4	1.1	0.2	2.6	0.2	159.5	1.1	0.2	1.1	0.477424	0.107519	0.147847	1.12457	1.32596	0.195319
Liquid Volumetric Flow	Mbbl/d	1018.7	1027.5	4.8	0.9	11.3	0.8	682.0	4.8	0.9	4.8	2.04079	0.459597	0.631985	4.80708	5.66791	0.834907
Std Vapor Volumetric Flow	MMSCFD	123.8	88.4	35.4	0.8	0.1	0.6	88.3	35.5	0.8	35.4	0.0111589	0.00411619	0.000110336	35.4147	36.1734	0.693741
Std Liquid Volumetric Flow	Mbbl/d	45.3	40.5	4.8	0.9	0.0	0.8	40.5	4.8	0.9	4.8	0.00502875	0.00281887	1.68735E-05	4.80556	5.68334	0.842324
Compressibility		0.674	0.943	0.011	0.091	0.983	0.007	0.916	0.011	0.135	0.001	0.996263	0.973171	0.999551	0.0110067	0.0127033	0.0246739
Specific Gravity			0.721	0.998	0.722	1.529	0.734	0.721	0.999	0.724	0.998	0.726531	1.52621	0.636170	0.998829	0.957035	0.729261
API Gravity				10.0	63.3		59.4		10.0	63.0	10.0				10.0494	16.1727	61.2683
Enthalpy	MMBtu/h	-814.6	-335.1	-478.2	-7.9	-0.3	-7.2	-334.4	-480.2	-7.9	-477.8	-0.0459476	-0.0207090	-0.00123358	-478.465	-486.382	-7.61278
Mass Enthalpy	Btu/lb	-2986.5	-1653.2	-6825.8	-870.8	-1043.3	-841.9	-1651.6	-6830.9	-871.0	-6822.3	-1782.20	-1036.62	-5526.45	-6829.71	-6145.42	-856.933
Mass Cp	Btu/(lb**F)	0.6	0.5	1.0	0.5	0.4	0.5	0.5	1.0	0.5	1.0	0.472150	0.407902	0.442480	0.983391	0.926432	0.486470
Ideal Gas CpCv Ratio		1.269	1.250	1.326	1.051	1.125	1.044	1.250	1.326	1.051	1.326	1.25095	1.12548	1.32218	1.32600	1.29284	1.04737
Dynamic Viscosity	cP		0.0	1.0	0.5	0.0	0.7	0.0	1.0	0.5	0.9	0.0106841	0.00837416	0.0102596	1.04779	0.970008	0.603026
Kinematic Viscosity	cSt		0.8	1.0	0.7	4.5	0.9	0.5	1.0	0.8	0.9	12.3513	2.81360	424.229	1.05001	1.00336	0.827681
Thermal Conductivity	Btu/(h*ft*°F)		0.0	0.3	0.1	0.0	0.1	0.0	0.3	0.1	0.3	0.0169920	0.0105206	0.0122137	0.344619	0.302802	0.0691577
Surface Tension	lbf/ft			0.005	0.001		0.002		0.005	0.001	0.005				0.00507040	0.00451710	0.00155152
Net I.G. Heating Value	Btu/ft^3	814.1	1140.1	0.4	5473.7	2314.1	6205.1	1141.9	0.0	5484.2	0.0	1095.87	2314.25	45.4956	0.409330	115.427	5853.31
Net Liquid Heating Value	Btu/lb	15080.0	20655.0	-1051.2	18903.6	19678.9	18845.6	20684.2	-1059.8	18904.8	-1058.8	19673.5	19710.4	-43.5288	-1050.70	1240.98	18874.2
Gross I.G. Heating Value	Btu/ft^3	911.9	1257.0	50.7	5877.5	2514.9	6656.5	1258.8	50.3	5888.7	50.4	1209.42	2515.16	97.6787	50.7427	173.189	6282.07
Gross Liquid Heating Value	Btu/lb	16930.0	22778.0	8.9	20309.5	21400.0	20227.8	22808.7	0.0	20310.4	0.9	21721.3	21435.1	1031.2	9.5	2340.8	20268.1

Process Streams		**Well Stream**	**HP Separator Gas**	**HP Separator Water**	**HP Separator Oil**	**OT Flash Gas**	**Sales Oil**	**Gas**	**Water**	**Oil**	**Produced Water**	**PWT Flash Gas**	**Oil W/B**	**Water W/B**	**1**	**3**	**LP Separator Oil**
Phase: Vapor	**Status**	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved
Mole Fraction		**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**
Water		0.128387	0.156524			0.233510	0.233510	0			3.02985	3.02985	0.000118725	94.1901	0.156524		0.325299
H2S		0	0			0	0	0			0	0	0	0	0		0
Nitrogen		0.494062	0.493921			0.0116221	0.0116221	0.494658			0.377409	0.377409	0.000455370	0.00669135	0.493921		0.176805
Carbon Dioxide		0.146090	0.146078			0.154871	0.154871	0.146717			1.21632	1.21632	0.182561	1.45262	0.146078		0.235012
Methane		77.6025	77.5806			9.11491	9.11491	77.7018			72.6386	72.6386	1.99841	3.57810	77.5806		47.0960
Ethane		14.1820	14.1780			29.0118	29.0118	14.2004			15.6378	15.6378	36.6963	0.710738	14.1780		29.8796
Propane		4.48840	4.48718			30.5911	30.5911	4.49433			5.34325	5.34325	32.6946	0.0591831	4.48718		13.6836

Isobutane		0.565994	0.565833			5.87676	5.87676	0.566666			0.230223	0.230223	5.95316	0.000319269	0.565833		1.85749
n-Butane		1.18245	1.18212			12.9987	12.9987	1.18394			0.957044	0.957044	12.9337	0.00199737	1.18212		3.77974
Isopentane		0.374489	0.374384			3.73637	3.73637	0.374944			0.164443	0.164443	3.55279	8.60034E-05	0.374384		0.958312
n-Pentane		0.291082	0.291000			3.84771	3.84771	0.291434			0.160484	0.160484	3.59826	6.12109E-05	0.291000		0.963818
2-Methylpentane		0	0			0.821672	0.821672	0			0.0154690	0.0154690	0.758355	1.12633E-06	0		0.196534
3-Methylpentane		0	0			0.482477	0.482477	0			0.0239978	0.0239978	0.442977	4.23634E-06	0		0.114985
n-Hexane		0.544534	0.544378			1.42348	1.42348	0.545164			0.0211643	0.0211643	0.0888805	5.96800E-08	0.544378		0.336947
Methylcyclopentane		0	0			0.213396	0.213396	0			0.0301263	0.0301263	0.179377	1.14368E-05	0		0.0504669
Benzene		0	0			0.0640181	0.0640181	0			0.0498717	0.0498717	0.00329177	5.81875E-05	0		0.0152082
2-Methylhexane		0	0			0.240437	0.240437	0			0.00397064	0.00397064	0.0142108	4.73486E-09	0		0.0560810
3-Methylhexane		0	0			0.180833	0.180833	0			0.00311392	0.00311392	0.160614	5.56530E-08	0		0.0421991
Heptane		0	0			0.365991	0.365991	0			0.00660615	0.00660615	0.299701	8.66875E-08	0		0.0855793
Methylcyclohexane		0	0			0.266867	0.266867	0			0.0249223	0.0249223	0.216736	2.02048E-06	0		0.0622117
Toluene		0	0			0.0474013	0.0474013	0			0.0347472	0.0347472	0.00524329	1.95012E-05	0		0.0110486
Octane		0	0			0.233165	0.233165	0			0.00249472	0.00249472	0.179922	6.37813E-09	0		0.0540869
Ethylbenzene		0	0			0.0109172	0.0109172	0			0.00791821	0.00791821	0.00225470	2.49928E-06	0		0.00252544
m-Xylene		0	0			0.0139419	0.0139419	0			0.0100029	0.0100029	0.00370661	3.52471E-06	0		0.00321761
o-Xylene		0	0			0.0127638	0.0127638	0			0.00941353	0.00941353	0.00292518	3.46805E-06	0		0.00294387
Nonane		0	0			0.0448234	0.0448234	0			0.000738787	0.000738787	0.0311557	8.89240E-10	0		0.0102543
C10+		0	0			0.000454420	0.000454420	0			1.01182E-06	1.01182E-06	0.000217289	0	0		0.000102967
Molar Flow		**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**	**lbmol/h**
Water		12.4579	15.1924			0.0160807	0	0			0	0.0371224	5.36578E-07	0.0114108	0		0
H2S		0	0			0	0	0			0	0	0	0	0		0
Nitrogen		47.9406	47.9407			0.000800360	0	47.9443			0	0.00462411	2.05804E-06	8.10634E-07	0		0
Carbon Dioxide		14.1756	14.1786			0.0106652	0	14.2204			0	0.0149027	0.000825084	0.000175980	0		0
Methane		7530.04	7530.09			0.627701	0	7531.17			0	0.889985	0.00903181	0.000433474	0		0
Ethane		1376.13	1376.14			1.99790	0	1376.36			0	0.191598	0.165849	8.61034E-05	0		0
Propane		435.525	435.533			2.10667	0	435.608			0	0.0654668	0.147763	7.16982E-06	0		0
Isobutane		54.9203	54.9206			0.404705	0	54.9236			0	0.00282074	0.0269053	3.86783E-08	0		0
n-Butane		114.738	114.739			0.895158	0	114.752			0	0.0117259	0.0584539	2.41974E-07	0		0
Isopentane		36.3380	36.3382			0.257306	0	36.3411			0	0.00201479	0.0160568	1.04190E-08	0		0
n-Pentane		28.2447	28.2449			0.264973	0	28.2470			0	0.00196629	0.0162623	7.41548E-09	0		0
2-Methylpentane		0	0			0.0565847	0	0			0	0.000189530	0.00342739	1.36451E-10	0		0
3-Methylpentane		0	0			0.0332259	0	0			0	0.000294027	0.00200203	5.13218E-10	0		0
n-Hexane		52.8380	52.8381			0.0980283	0	52.8395			0	0.000259310	0.000401695	7.23002E-12	0		0
Methylcyclopentane		0	0			0.0146955	0	0			0	0.000369115	0.000810692	1.38552E-09	0		0
Benzene		0	0			0.00440862	0	0			0	0.000611040	1.48771E-05	7.04921E-09	0		0
2-Methylhexane		0	0			0.0165577	0	0			0	4.86493E-05	6.42255E-05	5.73611E-13	0		0
3-Methylhexane		0	0			0.0124531	0	0			0	3.81525E-05	0.000725892	6.74217E-12	0		0
Heptane		0	0			0.0252041	0	0			0	8.09401E-05	0.00135450	1.05019E-11	0		0
Methylcyclohexane		0	0			0.0183779	0	0			0	0.000305354	0.000979536	2.44774E-10	0		0
Toluene		0	0			0.00326431	0	0			0	0.000425731	2.36970E-05	2.36251E-09	0		0
Octane		0	0			0.0160569	0	0			0	3.05659E-05	0.000813158	7.72688E-13	0		0
Ethylbenzene		0	0			0.000751814	0	0			0	9.70158E-05	1.01901E-05	3.02778E-10	0		0
m-Xylene		0	0			0.000960109	0	0			0	0.000122558	1.67520E-05	4.27006E-10	0		0
o-Xylene		0	0			0.000878981	0	0			0	0.000115337	1.32203E-05	4.20143E-10	0		0
Nonane		0	0			0.00308678	0	0			0	9.05180E-06	0.000140808	1.07728E-13	0		0
C10+		0	0			3.12937E-05	0	0			0	1.23971E-08	9.82038E-07	0	0		0
Mass Fraction		**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**
Water		0.110749	0.135025			0.0950234	0.0950234	0			2.59400	2.59400	4.83874E-05	92.0949	0.135025		0.206339
H2S		0	0			0	0	0			0	0	0	0	0		0
Nitrogen		0.662711	0.662547			0.00735419	0.00735419	0.663391			0.502442	0.502442	0.000288588	0.0101735	0.662547		0.174389
Carbon Dioxide		0.307853	0.307840			0.153957	0.153957	0.309119			2.54392	2.54392	0.181762	3.46966	0.307840		0.364162
Methane		59.6106	59.5960			3.30299	3.30299	59.6762			55.3792	55.3792	0.725278	3.11539	59.5960		26.6019
Ethane		20.4190	20.4140			19.7050	19.7050	20.4417			22.3462	22.3462	24.9627	1.15989	20.4140		31.6338
Propane		9.47685	9.47464			30.4702	30.4702	9.48766			11.1972	11.1972	32.6152	0.141639	9.47464		21.2448
Isobutane		1.57518	1.57479			7.71550	7.71550	1.57677			0.635914	0.635914	7.82778	0.00100714	1.57479		3.80125
n-Butane		3.29082	3.29002			17.0657	17.0657	3.29435			2.64352	2.64352	17.0065	0.00630071	3.29002		7.73503
Isopentane		1.29374	1.29342			6.08923	6.08923	1.29507			0.563835	0.563835	5.79892	0.000336770	1.29342		2.43441
n-Pentane		1.00559	1.00534			6.27068	6.27068	1.00663			0.550263	0.550263	5.87314	0.000239688	1.00534		2.44840
2-Methylpentane		0	0			1.59943	1.59943	0			0.0633511	0.0633511	1.47844	5.26790E-06	0		0.596318
3-Methylpentane		0	0			0.939167	0.939167	0			0.0982794	0.0982794	0.863600	1.98136E-05	0		0.348884
n-Hexane		2.24691	2.24635			2.77088	2.77088	2.24910			0.0866753	0.0866753	0.173276	2.79127E-07	2.24635		1.02236
Methylcyclopentane		0	0			0.405669	0.405669	0			0.120492	0.120492	0.341521	5.22391E-05	0		0.149543

Benzene		0	0			0.112954	0.112954	0			0.185131	0.185131	0.00581695	0.000246681	0		0.0418265
2-Methylhexane		0	0			0.544203	0.544203	0			0.0189080	0.0189080	0.0322138	2.57497E-08	0		0.197856
3-Methylhexane		0	0			0.409296	0.409296	0			0.0148283	0.0148283	0.364089	3.02659E-07	0		0.148880
Heptane		0	0			0.828381	0.828381	0			0.0314581	0.0314581	0.679382	4.71435E-07	0		0.301927
Methylcyclohexane		0	0			0.591873	0.591873	0			0.116291	0.116291	0.481425	1.07670E-05	0		0.215070
Toluene		0	0			0.0986541	0.0986541	0			0.152149	0.152149	0.0109293	9.75197E-05	0		0.0358431
Octane		0	0			0.601618	0.601618	0			0.0135427	0.0135427	0.464952	3.95419E-08	0		0.217532
Ethylbenzene		0	0			0.0261803	0.0261803	0			0.0399500	0.0399500	0.00541525	1.44007E-05	0		0.00944009
m-Xylene		0	0			0.0334338	0.0334338	0			0.0504681	0.0504681	0.00890241	2.03093E-05	0		0.0120274
o-Xylene		0	0			0.0306086	0.0306086	0			0.0474943	0.0474943	0.00702558	1.99828E-05	0		0.0110042
Nonane		0	0			0.129856	0.129856	0			0.00450300	0.00450300	0.0903983	6.18989E-09	0		0.0463062
C10+		0	0			0.00210013	0.00210013	0			9.83822E-06	9.83822E-06	0.00100576	0	0		0.000741756
Mass Flow		**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**
Water		224.432	273.696			0.289699	0	0			0	0.668771	9.66660E-06	0.205569	0		0
H2S		0	0			0	0	0			0	0	0	0	0		0
Nitrogen		1342.98	1342.98			0.0224208	0	1343.08			0	0.129537	5.76527E-05	2.27086E-05	0		0
Carbon Dioxide		623.862	623.992			0.469371	0	625.834			0	0.655858	0.0363115	0.00774477	0		0
Methane		120800	120801			10.0699	0	120819			0	14.2776	0.144892	0.00695399	0		0
Ethane		41378.8	41379.2			60.0750	0	41385.7			0	5.76118	4.98692	0.00258905	0		0
Propane		19204.7	19205.1			92.8948	0	19208.4			0	2.88680	6.51571	0.000316158	0		0
Isobutane		3192.09	3192.10			23.5223	0	3192.28			0	0.163948	1.56380	2.24807E-06	0		0
n-Butane		6668.80	6668.86			52.0286	0	6669.65			0	0.681537	3.39747	1.40641E-05	0		0
Isopentane		2621.74	2621.76			18.5643	0	2621.96			0	0.145365	1.15848	7.51718E-07	0		0
n-Pentane		2037.82	2037.83			19.1175	0	2037.99			0	0.141866	1.17331	5.35018E-07	0		0
2-Methylpentane		0	0			4.87621	0	0			0	0.0163328	0.295356	1.17587E-08	0		0
3-Methylpentane		0	0			2.86325	0	0			0	0.0253379	0.172526	4.42267E-08	0		0
n-Hexane		4553.33	4553.34			8.44762	0	4553.46			0	0.0223461	0.0346162	6.23050E-10	0		0
Methylcyclopentane		0	0			1.23677	0	0			0	0.0310645	0.0682274	1.16605E-07	0		0
Benzene		0	0			0.344366	0	0			0	0.0477294	0.00116208	5.50627E-07	0		0
2-Methylhexane		0	0			1.65912	0	0			0	0.00487475	0.00643552	5.74769E-11	0		0
3-Methylhexane		0	0			1.24783	0	0			0	0.00382295	0.0727358	6.75578E-10	0		0
Heptane		0	0			2.52550	0	0			0	0.00811036	0.135724	1.05231E-09	0		0
Methylcyclohexane		0	0			1.80445	0	0			0	0.0299815	0.0961768	2.40334E-08	0		0
Toluene		0	0			0.300768	0	0			0	0.0392262	0.00218341	2.17678E-07	0		0
Octane		0	0			1.83416	0	0			0	0.00349150	0.0928859	8.82630E-11	0		0
Ethylbenzene		0	0			0.0798164	0	0			0	0.0102997	0.00108183	3.21445E-08	0		0
m-Xylene		0	0			0.101930	0	0			0	0.0130114	0.00177848	4.53331E-08	0		0
o-Xylene		0	0			0.0933170	0	0			0	0.0122447	0.00140354	4.46044E-08	0		0
Nonane		0	0			0.395895	0	0			0	0.00116094	0.0180593	1.38167E-11	0		0
C10+		0	0			0.00640269	0	0			0	2.53644E-06	0.000200925	0	0		0

Process Streams		**Well Stream**	**HP Separator Gas**	**HP Separator Water**	**HP Separator Oil**	**OT Flash Gas**	**Sales Oil**	**Gas**	**Water**	**Oil**	**Produced Water**	**PWT Flash Gas**	**Oil W/B**	**Water W/B**	**1**	**3**	**LP Separator Oil**
Phase: Vapor	**Status**	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved
Property	**Units**																
Temperature	°F	60.3	66.0			75.9	75.9	67.0			75.9	75.94	75.9425	75.9425	66		70
Pressure	psig	200	200			0	0	300			0	0	8.81720	-14.2252	200		40
Mole Fraction Vapor	%	100	100			100	100	100			100	100	100	100	100		100
Mole Fraction Light Liquid	%	0	0			0	0	0			0	0	0	0	0		0
Mole Fraction Heavy Liquid	%	0	0			0	0	0			0	0	0	0	0		0
Molecular Weight	lb/lbmol	20.9	20.9			44.3	44.3	20.9			21.0	21.0422	44.2029	18.4251	20.8837		28.4016
Mass Density	lb/ft^3	0.9	0.8			0.1	0.1	1.3			0.1	0.0540011	0.185805	0.00150976	0.843230		0.280882
Molar Flow	lbmol/h	9703.3	9706.1			6.9	0.0	9692.4			0.0	1.22522	0.451950	0.0121146	0		0
Mass Flow	lb/h	202649.0	202699.9			304.9	0.0	202457.0			0.0	25.7815	19.9775	0.223214	0		0
Vapor Volumetric Flow	MCFH	237.2	240.4			2.6	0.0	159.5			0.0	0.477424	0.107519	0.147847	0		0
Liquid Volumetric Flow	Mbbl/d	1013.8	1027.5			11.3	0.0	682.0			0.0	2.04079	0.459597	0.631985	0		0
Std Vapor Volumetric Flow	MMSCFD	88.4	88.4			0.1	0.0	88.3			0.0	0.0111589	0.00411619	0.000110336	0		0
Std Liquid Volumetric Flow	Mbbl/d	40.5	40.5			0.0	0.0	40.5			0.0	0.00502875	0.00281887	1.68735E-05	0		0
Compressibility		0.940	0.943			0.983	0.983	0.916			0.996	0.996263	0.973171	0.999551	0.942556		0.972981
Specific Gravity		0.721	0.721			1.529	1.529	0.721			0.727	0.726531	1.52621	0.636170	0.721056		0.980629
API Gravity																	
Enthalpy	MMBtu/h	-335.4	-335.1			-0.3	0.0	-334.4			0.0	-0.0459476	-0.0207090	-0.00123358	0		0
Mass Enthalpy	Btu/lb	-1655.0	-1653.2			-1043.3	-1043.3	-1651.6			-1782.2	-1782.20	-1036.62	-5526.45	-1653.17		-1339.94
Mass Cp	Btu/(lb**F)	0.5	0.5			0.4	0.4	0.5			0.5	0.472150	0.407902	0.442480	0.504979		0.443559
Ideal Gas CpCv Ratio		1.252	1.250			1.125	1.125	1.250			1.251	1.25095	1.12548	1.32218	1.25012		1.19151

Dynamic Viscosity	cP	0.0	0.0			0.0	0.0	0.0			0.0	0.0106841	0.00837416	0.0102596	0.0106843		0.00967788
Kinematic Viscosity	cSt	0.8	0.8			4.5	4.5	0.5			12.4	12.3513	2.81360	424.229	0.791008		2.15098
Thermal Conductivity	Btu/(h*ft*°F)	0.0	0.0			0.0	0.0	0.0			0.0	0.0169920	0.0105206	0.0122137	0.0175999		0.0143978
Surface Tension	lbf/ft																
Net I.G. Heating Value	Btu/ft^3	1140.4	1140.1			2314.1	2314.1	1141.9			1095.9	1095.87	2314.25	45.4956	1140.12		1517.84
Net Liquid Heating Value	Btu/lb	20660.3	20655.0			19678.9	19678.9	20684.2			19673.5	19673.5	19710.4	-43.5288	20655.0		20163.5
Gross I.G. Heating Value	Btu/ft^3	1257.3	1257.0			2514.9	2514.9	1258.8			1209.4	1209.42	2515.16	97.6787	1256.95		1661.66
Gross Liquid Heating Value	Btu/lb	22783.6	22778.0			21400.0	21400.0	22808.7			21721.3	21721.3	21435.1	1031.2	22778.0		22085.1

Process Streams		Well Stream	HP Separator Gas	HP Separator Water	HP Separator Oil	OT Flash Gas	Sales Oil	Gas	Water	Oil	Produced Water	PWT Flash Gas	Oil W/B	Water W/B	1	3	LP Separator Oil
Phase: Light Liquid	**Status**	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved
Mole Fraction		%	%	%	%	%	%	%	%	%	%	%	%	%	%	%	%
Water		99.9609	99.9627	99.9661	0.0517839	0.00486699	0.00486699		100	0	99.9967	99.9967	3.55133E-06	100.0000	99.9627	0.0466800	0.0255382
H2S		0	0	0	0	0	0		0	0	0	0	0	0	0	0	0
Nitrogen		9.49020E-05	9.09774E-05	0.000123345	0.0164543	1.85250E-05	1.85250E-05		0	0.0179998	4.42210E-06	4.42210E-06	1.18304E-06	2.51118E-09	9.09774E-05	0.0163595	0.00106759
Carbon Dioxide		0.00115147	0.00107601	0.000972844	0.0357417	0.00287906	0.00287906		0	0.0309997	0.000589759	0.000589759	0.00511986	2.26825E-05	0.00107601	0.0354666	0.0166204
Methane		0.0291377	0.0279843	0.0246369	4.91184	0.0438867	0.0438867		0	4.76595	0.00174859	0.00174859	0.0158785	2.76748E-06	0.0279843	4.90085	0.863982
Ethane		0.00590427	0.00559480	0.00536606	5.72449	0.861642	0.861642		0	5.72594	0.000438622	0.000438622	1.77812	6.44255E-07	0.00559480	5.72481	3.40665
Propane		0.00214005	0.00194860	0.00184921	6.53571	3.39068	3.39068		0	6.54493	0.000165565	0.000165565	5.84268	5.95505E-08	0.00194860	6.53561	5.84983
Isobutane		8.46856E-05	7.82999E-05	7.50256E-05	2.06276	1.70532	1.70532		0	2.06698	2.48181E-06	2.48181E-06	2.73553	1.12235E-10	7.82999E-05	2.06316	2.08245
n-Butane		0.000372380	0.000348886	0.000324282	5.89758	5.41519	5.41519		0	5.90894	2.27190E-05	2.27190E-05	8.55964	1.54731E-09	0.000348886	5.89895	6.10080
Isopentane		7.97064E-05	7.30268E-05	5.44913E-05	3.76285	4.06134	4.06134		0	3.76996	2.67515E-06	2.67515E-06	6.09035	4.58851E-11	7.30268E-05	3.76358	4.03196
n-Pentane		5.82560E-05	5.44300E-05	5.31537E-05	5.03533	5.58289	5.58289		0	5.04595	2.58486E-06	2.58486E-06	8.21953	3.23329E-11	5.44300E-05	5.03635	5.42602
2-Methylpentane		0	0	4.99297E-06	2.51940	2.93319	2.93319		0	2.52497	1.18622E-07	1.18622E-07	4.25860	2.84258E-13	0	2.51988	2.74229
3-Methylpentane		0	0	8.06098E-06	1.64113	1.91729	1.91729		0	1.64498	4.99279E-07	4.99279E-07	2.76691	2.90089E-12	0	1.64145	1.78757
n-Hexane		3.82516E-05	3.58306E-05	6.79802E-06	6.00456	7.05779	7.05779		0	6.01594	1.29051E-07	1.29051E-07	0.692196	1.19906E-14	3.58306E-05	6.00570	6.54840
Methylcyclopentane		0	0	1.13741E-05	0.921505	1.08378	1.08378		0	0.923991	1.88169E-06	1.88169E-06	1.42335	2.34823E-11	0	0.921677	1.00509
Benzene		0	0	0.000170998	0.274434	0.322694	0.322694		0	0.282997	0.000155332	0.000155332	0.0254522	5.94681E-09	0	0.274558	0.299308
2-Methylhexane		0	0	1.27692E-06	2.37987	2.83766	2.83766		0	2.38498	2.57498E-08	2.57498E-08	0.257844	1.01570E-15	0	2.38032	2.60285
3-Methylhexane		0	0	1.00232E-06	1.87496	2.23669	2.23669		0	1.87898	2.11076E-08	2.11076E-08	3.05295	1.24759E-14	0	1.87531	2.05082
Heptane		0	0	2.12665E-06	4.78171	5.71602	5.71602		0	4.79195	4.50293E-08	4.50293E-08	7.16551	1.95658E-14	0	4.78261	5.23233
Methylcyclohexane		0	0	8.88284E-06	3.39435	4.05673	4.05673		0	3.40197	1.02999E-06	1.02999E-06	5.09273	2.75709E-12	0	3.39500	3.71409
Toluene		0	0	0.000100368	0.737743	0.883021	0.883021		0	0.743993	8.94474E-05	8.94474E-05	0.150080	1.65540E-09	0	0.737995	0.807474
Octane		0	0	7.97318E-07	9.66836	11.6204	11.6204		0	9.68890	1.12198E-08	1.12198E-08	13.6878	9.54306E-16	0	9.67017	10.5909
Ethylbenzene		0	0	2.09259E-05	0.507941	0.610660	0.610660		0	0.509995	1.84366E-05	1.84366E-05	0.193295	1.92908E-10	0	0.508051	0.556439
m-Xylene		0	0	2.72562E-05	0.774078	0.930953	0.930953		0	0.776992	2.41118E-05	2.41118E-05	0.378978	2.81836E-10	0	0.774255	0.848047
o-Xylene		0	0	3.36330E-05	0.789747	0.949978	0.949978		0	0.792992	3.06764E-05	3.06764E-05	0.333284	3.74821E-10	0	0.789941	0.865246
Nonane		0	0	2.38078E-07	5.64496	6.79601	6.79601		0	5.65694	5.28319E-09	5.28319E-09	7.27130	2.12703E-16	0	5.64602	6.18565
C10+		0	0	3.19828E-10	24.0507	28.9784	28.9784		0	24.1018	9.98073E-13	9.98073E-13	20.0028	0	0	24.0553	26.3586
Molar Flow		lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h
Water		3889.75	0	3886.97	0.0432295	0	0.00337209		3902.21	0	3886.93	0	0	0	3887.02	0.0389614	0.0194528
H2S		0	0	0	0	0	0		0	0	0	0	0	0	0	0	0
Nitrogen		0.00369289	0	0.00479600	0.0137362	0	1.28350E-05		0	0.0149945	0.000171890	0	0	0	0.00353763	0.0136544	0.000813195
Carbon Dioxide		0.0448068	0	0.0378270	0.0298374	0	0.00199475		0	0.0258239	0.0229243	0	0	0	0.0418404	0.0296022	0.0126600
Methane		1.13383	0	0.957954	4.10043	0	0.0304069		0	3.97022	0.0679689	0	0	0	1.08816	4.09049	0.658107
Ethane		0.229751	0	0.208648	4.77884	0	0.596988		0	4.76993	0.0170495	0	0	0	0.217552	4.77821	2.59489
Propane		0.0832752	0	0.0719024	5.45605	0	2.34923		0	5.45218	0.00643562	0	0	0	0.0757707	5.45494	4.45590
Isobutane		0.00329534	0	0.00291721	1.72200	0	1.18153		0	1.72187	9.64695E-05	0	0	0	0.00304467	1.72201	1.58623
n-Butane		0.0144903	0	0.0126090	4.92333	0	3.75191		0	4.92238	0.000883103	0	0	0	0.0135663	4.92356	4.64707
Isopentane		0.00310159	0	0.00211878	3.14125	0	2.81389		0	3.14052	0.000103985	0	0	0	0.00283962	3.14127	3.07120
n-Pentane		0.00226690	0	0.00206677	4.20352	0	3.86810		0	4.20347	0.000100475	0	0	0	0.00211649	4.20358	4.13307
2-Methylpentane		0	0	0.000194141	2.10321	0	2.03226		0	2.10340	4.61091E-06	0	0	0	0	2.10322	2.08884
3-Methylpentane		0	0	0.000313434	1.37002	0	1.32839		0	1.37034	1.94073E-05	0	0	0	0	1.37003	1.36162
n-Hexane		0.00148847	0	0.000264326	5.01264	0	4.88998		0	5.01151	5.01628E-06	0	0	0	0.00139326	5.01265	4.98801
Methylcyclopentane		0	0	0.000442258	0.769278	0	0.750894		0	0.769720	7.31426E-05	0	0	0	0	0.769277	0.765589
Benzene		0	0	0.00664891	0.229099	0	0.223578		0	0.235748	0.00603787	0	0	0	0	0.229160	0.227987
2-Methylhexane		0	0	4.96502E-05	1.98673	0	1.96607		0	1.98678	1.00091E-06	0	0	0	0	1.98673	1.98263
3-Methylhexane		0	0	3.89729E-05	1.56523	0	1.54969		0	1.56526	8.20464E-07	0	0	0	0	1.56523	1.56214
Heptane		0	0	8.26904E-05	3.99180	0	3.96034		0	3.99188	1.75032E-06	0	0	0	0	3.99180	3.98554
Methylcyclohexane		0	0	0.000345391	2.83362	0	2.81070		0	2.83397	4.00363E-05	0	0	0	0	2.83363	2.82908
Toluene		0	0	0.00390261	0.615872	0	0.611800		0	0.619775	0.00347688	0	0	0	0	0.615967	0.615064
Octane		0	0	3.10020E-05	8.07120	0	8.05119		0	8.07123	4.36120E-07	0	0	0	0	8.07120	8.06725
Ethylbenzene		0	0	0.000813658	0.424032	0	0.423095		0	0.424846	0.000716642	0	0	0	0	0.424044	0.423847
m-Xylene		0	0	0.00105980	0.646205	0	0.645010		0	0.647265	0.000937242	0	0	0	0	0.646231	0.645970

o-Xylene		0	0	0.00130775	0.659285	0	0.658191		0	0.660593	0.00119241	0	0	0	0	0.659323	0.659070
Nonane		0	0	9.25716E-06	4.71244	0	4.70861		0	4.71245	2.05361E-07	0	0	0	0	4.71244	4.71169
C10+		0	0	1.24359E-08	20.0777	0	20.0777		0	20.0777	3.87957E-11	0	0	0	0	20.0777	20.0777
Mass Fraction		**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**
Water		99.9538	99.9561	99.9583	0.00856629	0.000708124	0.000708124		100	0	99.9942	99.9942	5.79731E-07	99.9999	99.9561	0.00772077	0.00394482
H2S		0	0	0	0	0	0		0	0	0	0	0	0	0	0	0
Nitrogen		0.000147560	0.000141459	0.000191784	0.00423256	4.19114E-06	4.19114E-06		0	0.00462148	6.87611E-06	6.87611E-06	3.00304E-07	3.90484E-09	0.000141459	0.00420750	0.000256427
Carbon Dioxide		0.00281272	0.00262842	0.00237637	0.0144437	0.00102331	0.00102331		0	0.0125041	0.00144069	0.00144069	0.00204174	5.54111E-05	0.00262842	0.0143303	0.00627166
Methane		0.0259450	0.0249182	0.0219373	0.723556	0.00568607	0.00568607		0	0.700758	0.00155707	0.00155707	0.00230822	2.46442E-06	0.0249182	0.721824	0.118842
Ethane		0.00985403	0.00933758	0.00895571	1.58057	0.209245	0.209245		0	1.57803	0.000732079	0.000732079	0.484481	1.07532E-06	0.00933758	1.58041	0.878299
Propane		0.00523779	0.00476924	0.00452591	2.64634	1.20751	1.20751		0	2.64514	0.000405240	0.000405240	2.33455	1.45760E-07	0.00476924	2.64588	2.21174
Isobutane		0.000273199	0.000252600	0.000242034	1.10090	0.800490	0.800490		0	1.10110	8.00679E-06	8.00679E-06	1.44072	3.62101E-10	0.000252600	1.10094	1.03780
n-Butane		0.00120131	0.00112553	0.00104614	3.14755	2.54193	2.54193		0	3.14774	7.32960E-05	7.32960E-05	4.50809	4.99203E-09	0.00112553	3.14779	3.04036
Isopentane		0.000319191	0.000292443	0.000218213	2.49289	2.36650	2.36650		0	2.49295	1.07134E-05	1.07134E-05	3.98168	1.83764E-10	0.000292443	2.49298	2.49425
n-Pentane		0.000233291	0.000217971	0.000212857	3.33591	3.25309	3.25309		0	3.33672	1.03517E-05	1.03517E-05	5.37367	1.29489E-10	0.000217971	3.33606	3.35665
2-Methylpentane		0	0	2.38818E-05	1.99360	2.04142	2.04142		0	1.99429	5.67410E-07	5.67410E-07	3.32541	1.35974E-12	0	1.99366	2.02625
3-Methylpentane		0	0	3.85563E-05	1.29862	1.33438	1.33438		0	1.29925	2.38822E-06	2.38822E-06	2.16060	1.38763E-11	0	1.29867	1.32081
n-Hexane		0.000182962	0.000171383	3.25155E-05	4.75140	4.91202	4.91202		0	4.75154	6.17293E-07	6.17293E-07	0.540515	5.73563E-14	0.000171383	4.75155	4.83854
Methylcyclopentane		0	0	5.31306E-05	0.712128	0.736632	0.736632		0	0.712719	8.79023E-06	8.79023E-06	1.08545	1.09699E-10	0	0.712149	0.725275
Benzene		0	0	0.000741368	0.196839	0.203571	0.203571		0	0.202603	0.000673484	0.000673484	0.0180151	2.57845E-08	0	0.196897	0.200461
2-Methylhexane		0	0	7.10172E-06	2.18971	2.29639	2.29639		0	2.19032	1.43218E-07	1.43218E-07	0.234114	5.64936E-15	0	2.18978	2.23625
3-Methylhexane		0	0	5.57450E-06	1.72514	1.81005	1.81005		0	1.72562	1.17398E-07	1.17398E-07	2.77199	6.93916E-14	0	1.72519	1.76198
Heptane		0	0	1.18276E-05	4.39964	4.62571	4.62571		0	4.40085	2.50449E-07	2.50449E-07	6.50606	1.08826E-13	0	4.39977	4.49539
Methylcyclohexane		0	0	4.84091E-05	3.06030	3.21687	3.21687		0	3.06145	5.61345E-06	5.61345E-06	4.53102	1.50265E-11	0	3.06040	3.12679
Toluene		0	0	0.000513289	0.624170	0.657082	0.657082		0	0.628285	0.000457464	0.000457464	0.125302	8.46646E-09	0	0.624285	0.637918
Octane		0	0	5.05511E-06	10.1411	10.7202	10.7202		0	10.1437	7.11388E-08	7.11388E-08	14.1678	6.05092E-15	0	10.1414	10.3730
Ethylbenzene		0	0	0.000123308	0.495167	0.523587	0.523587		0	0.496243	0.000108645	0.000108645	0.185950	1.13681E-09	0	0.495197	0.506517
m-Xylene		0	0	0.000160610	0.754612	0.798210	0.798210		0	0.756041	0.000142089	0.000142089	0.364578	1.66088E-09	0	0.754665	0.771964
o-Xylene		0	0	0.000198186	0.769887	0.814522	0.814522		0	0.771610	0.000180773	0.000180773	0.320620	2.20884E-09	0	0.769954	0.787620
Nonane		0	0	1.69480E-06	6.64803	7.03941	7.03941		0	6.64973	3.76114E-08	3.76114E-08	8.45049	1.51428E-15	0	6.64823	6.80229
C10+		0	0	3.63202E-09	45.1847	47.8837	47.8837		0	45.1962	1.13348E-11	1.13348E-11	37.0845	0	0	45.1861	46.2406
Mass Flow		**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**
Water		70074.9	0	70024.9	0.778791	0	0.0607491		70299.4	0	70024.2	0	0	0	70025.7	0.701901	0.350448
H2S		0	0	0	0	0	0		0	0	0	0	0	0	0	0	0
Nitrogen		0.103450	0	0.134352	0.384797	0	0.000359553		0	0.420048	0.00481522	0	0	0	0.0991009	0.382507	0.0227804
Carbon Dioxide		1.97193	0	1.66475	1.31313	0	0.0877882		0	1.13650	1.00889	0	0	0	1.84138	1.30278	0.557159
Methane		18.1894	0	15.3679	65.7810	0	0.487801		0	63.6921	1.09039	0	0	0	17.4568	65.6215	10.5577
Ethane		6.90840	0	6.27384	143.695	0	17.9508		0	143.427	0.512663	0	0	0	6.54157	143.676	78.0259
Propane		3.67207	0	3.17058	240.588	0	103.591		0	240.417	0.283783	0	0	0	3.34116	240.539	196.486
Isobutane		0.191533	0	0.169555	100.087	0	68.6731		0	100.079	0.00560702	0	0	0	0.176963	100.087	92.1954
n-Butane		0.842208	0	0.732865	286.155	0	218.069		0	286.099	0.0513279	0	0	0	0.788504	286.168	270.098
Isopentane		0.223776	0	0.152867	226.637	0	203.019		0	226.585	0.00750238	0	0	0	0.204875	226.639	221.583
n-Pentane		0.163554	0	0.149115	303.279	0	279.079		0	303.275	0.00724915	0	0	0	0.152702	303.283	298.196
2-Methylpentane		0	0	0.0167302	181.245	0	175.131		0	181.261	0.000397347	0	0	0	0	181.245	180.007
3-Methylpentane		0	0	0.0270103	118.062	0	114.475		0	118.089	0.00167243	0	0	0	0	118.063	117.338
n-Hexane		0.128270	0	0.0227784	431.966	0	421.396		0	431.869	0.000432280	0	0	0	0.120065	431.967	429.844
Methylcyclopentane		0	0	0.0372202	64.7420	0	63.1948		0	64.7792	0.00615565	0	0	0	0	64.7419	64.4316
Benzene		0	0	0.519359	17.8953	0	17.4641		0	18.4147	0.471629	0	0	0	0	17.9001	17.8085
2-Methylhexane		0	0	0.00497504	199.074	0	197.004		0	199.079	0.000100293	0	0	0	0	199.074	198.663
3-Methylhexane		0	0	0.00390516	156.839	0	155.282		0	156.843	8.22121E-05	0	0	0	0	156.839	156.530
Heptane		0	0	0.00828574	399.986	0	396.834		0	399.994	0.000175385	0	0	0	0	399.986	399.359
Methylcyclohexane		0	0	0.0339125	278.222	0	275.971		0	278.256	0.00393100	0	0	0	0	278.223	277.776
Toluene		0	0	0.359580	56.7455	0	56.3703		0	57.1051	0.320354	0	0	0	0	56.7542	56.6711
Octane		0	0	0.00354131	921.961	0	919.676		0	921.965	4.98173E-05	0	0	0	0	921.962	921.510
Ethylbenzene		0	0	0.0863820	45.0173	0	44.9179		0	45.1037	0.0760823	0	0	0	0	45.0187	44.9977
m-Xylene		0	0	0.112514	68.6043	0	68.4774		0	68.7169	0.0995023	0	0	0	0	68.6072	68.5794
o-Xylene		0	0	0.138837	69.9930	0	69.8769		0	70.1319	0.126592	0	0	0	0	69.9971	69.9702
Nonane		0	0	0.00118728	604.395	0	603.903		0	604.396	2.63386E-05	0	0	0	0	604.395	604.299
C10+		0	0	2.54437E-06	4107.90	0	4107.89		0	4107.90	7.93760E-09	0	0	0	0	4107.90	4107.90

Process Streams		**Well Stream**	**HP Separator Gas**	**HP Separator Water**	**HP Separator Oil**	**OT Flash Gas**	**Sales Oil**	**Gas**	**Water**	**Oil**	**Produced Water**	**PWT Flash Gas**	**Oil W/B**	**Water W/B**	**1**	**3**	**LP Separator Oil**
Phase: Light Liquid	**Status**	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved
Property	**Units**																
Temperature	°F	60.3	66.0	70.0	70.0	75.9	75.9		67.0	67.0	75.9	75.94	75.9425	75.9425	66	66.0894	70

Pressure	psig	200	200	200	200	0	0	200	300	0	0	8.81720	-14.2252	200	200	40
Mole Fraction Vapor	%	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Mole Fraction Light Liquid	%	100	100	100	100	100	100	100	100	100	100	100	100	100	100	100
Mole Fraction Heavy Liquid	%	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
Molecular Weight	lb/lbmol	18.0	18.0	18.0	108.9	123.8	123.8	18.0	109.1	18.0	18.0157	110.358	18.0153	18.0165	108.921	116.628
Mass Density	lb/ft^3	62.3	62.3	62.3	45.0	45.8	45.8	62.3	45.2	62.2	62.2171	44.4786	62.2179	62.2960	45.1281	45.4833
Molar Flow	lbmol/h	3891.3	0.0	3888.3	83.5	0.0	69.3	3902.2	83.3	3887.1	0	0	0	3888.46	83.4649	76.1714
Mass Flow	lb/h	70107.3	0.0	70054.1	9091.3	0.0	8578.9	70299.4	9089.0	70028.3	0	0	0	70056.4	9091.07	8883.75
Vapor Volumetric Flow	MCFH	1.1	0.0	1.1	0.2	0.0	0.2	1.1	0.2	1.1	0	0	0	1.12457	0.201451	0.195319
Liquid Volumetric Flow	Mbbl/d	4.8	0.0	4.8	0.9	0.0	0.8	4.8	0.9	4.8	0	0	0	4.80708	0.861117	0.834907
Std Vapor Volumetric Flow	MMSCFD	35.4	0.0	35.4	0.8	0.0	0.6	35.5	0.8	35.4	0	0	0	35.4147	0.760167	0.693741
Std Liquid Volumetric Flow	Mbbl/d	4.8	0.0	4.8	0.9	0.0	0.8	4.8	0.9	4.8	0	0	0	4.80556	0.878259	0.842324
Compressibility		0.011	0.011	0.011	0.091	0.007	0.007	0.011	0.135	0.001	0.000740333	0.0101496	2.37153E-05	0.0110067	0.0918411	0.0246739
Specific Gravity		1.000	0.999	0.998	0.722	0.734	0.734	0.999	0.724	0.998	0.997564	0.713153	0.997577	0.998829	0.723565	0.729261
API Gravity		10.1	10.0	10.0	63.3	59.4	59.4	10.0	63.0	10.0	10.0153	64.7846	10.0135	10.0494	63.2491	61.2683
Enthalpy	MMBtu/h	-479.2	0.0	-478.2	-7.9	0.0	-7.2	-480.2	-7.9	-477.8	0	0	0	-478.465	-7.93357	-7.61278
Mass Enthalpy	Btu/lb	-6835.2	-6829.7	-6825.8	-870.8	-841.9	-841.9	-6830.9	-871.0	-6822.3	-6822.34	-888.613	-6822.66	-6829.71	-872.677	-856.933
Mass Cp	Btu/(lb*°F)	1.0	1.0	1.0	0.5	0.5	0.5	1.0	0.5	1.0	0.982731	0.494366	0.982746	0.983391	0.487817	0.486470
Ideal Gas CpCv Ratio		1.326	1.326	1.326	1.051	1.044	1.044	1.326	1.051	1.326	1.32555	1.04937	1.32556	1.32600	1.05104	1.04737
Dynamic Viscosity	cP	1.1	1.0	1.0	0.5	0.7	0.7	1.0	0.5	0.9	0.924432	0.512471	0.924434	1.04779	0.540870	0.603026
Kinematic Viscosity	cSt	1.1	1.1	1.0	0.7	0.9	0.9	1.0	0.8	0.9	0.927566	0.719278	0.927556	1.05001	0.748213	0.827681
Thermal Conductivity	Btu/(h*ft*°F)	0.3	0.3	0.3	0.1	0.1	0.1	0.3	0.1	0.3	0.349779	0.0684433	0.349835	0.344619	0.0688948	0.0691577
Surface Tension	lbf/ft	0.005	0.005	0.005	0.001	0.002	0.002	0.005	0.001	0.005	0.00499710	0.00147181	0.00499737	0.00507040	0.00143115	0.00155152
Net I.G. Heating Value	Btu/ft^3	0.4	0.4	0.4	5473.7	6205.1	6205.1	0.0	5484.2	0.0	0.0409897	5559.45	3.73571E-05	0.409330	5474.62	5853.31
Net Liquid Heating Value	Btu/lb	-1050.2	-1050.7	-1051.2	18903.6	18845.6	18845.6	-1059.8	18904.8	-1058.8	-1058.84	18949.3	-1059.76	-1050.70	18903.8	18874.2
Gross I.G. Heating Value	Btu/ft^3	50.8	50.7	50.7	5877.5	6656.5	6656.5	50.3	5888.7	50.4	50.3528	5974.93	50.3100	50.7427	5878.49	6282.07
Gross Liquid Heating Value	Btu/lb	10.0	9.5	8.9	20309.5	20227.8	20227.8	0.0	20310.4	0.9	0.930057	20377.1	0.000825555	9.48135	20309.7	20268.1

Process Streams		Well Stream	HP Separator Gas	HP Separator Water	HP Separator Oil	OT Flash Gas	Sales Oil	Gas	Water	Oil	Produced Water	PWT Flash Gas	Oil W/B	Water W/B	1	3	LP Separator Oil
Phase: Heavy Liquid	Status	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved
Mole Fraction		%	%	%	%	%	%	%	%	%	%	%	%	%	%	%	%
Water					99.9661											99.9659	
H2S					0											0	
Nitrogen					0.000123345											0.000125446	
Carbon Dioxide					0.000972844											0.000978889	
Methane					0.0246369											0.0248925	
Ethane					0.00536606											0.00538224	
Propane					0.00184921											0.00187777	
Isobutane					7.50256E-05											7.46803E-05	
n-Butane					0.000324282											0.000318584	
Isopentane					5.44913E-05											5.38236E-05	
n-Pentane					5.31537E-05											5.16053E-05	
2-Methylpentane					4.99297E-06											4.77877E-06	
3-Methylpentane					8.06098E-06											7.79338E-06	
n-Hexane					6.79802E-06											6.49815E-06	
Methylcyclopentane					1.13741E-05											1.14021E-05	
Benzene					0.000170998											0.000169430	
2-Methylhexane					1.27692E-06											1.26913E-06	
3-Methylhexane					1.00232E-06											9.93998E-07	
Heptane					2.12665E-06											2.17128E-06	
Methylcyclohexane					8.88284E-06											8.64437E-06	
Toluene					0.000100368											9.79261E-05	
Octane					7.97318E-07											7.55697E-07	
Ethylbenzene					2.09259E-05											2.06033E-05	
m-Xylene					2.72562E-05											2.65736E-05	
o-Xylene					3.36330E-05											3.26560E-05	
Nonane					2.38078E-07											2.25535E-07	
C10+					3.19828E-10											2.92527E-10	
Molar Flow		lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h
Water					0											3886.98	
H2S					0											0	
Nitrogen					0											0.00487774	
Carbon Dioxide					0											0.0380622	
Methane					0											0.967895	

Ethane					0											0.209278	
Propane					0											0.0730135	
Isobutane					0											0.00290380	
n-Butane					0											0.0123875	
Isopentane					0											0.00209282	
n-Pentane					0											0.00200657	
2-Methylpentane					0											0.000185813	
3-Methylpentane					0											0.000303030	
n-Hexane					0											0.000252668	
Methylcyclopentane					0											0.00443349	
Benzene					0											0.00658794	
2-Methylhexane					0											4.93476E-05	
3-Methylhexane					0											3.86497E-05	
Heptane					0											8.44259E-05	
Methylcyclohexane					0											0.000336119	
Toluene					0											0.00380767	
Octane					0											2.93838E-05	
Ethylbenzene					0											0.000801120	
m-Xylene					0											0.00103326	
o-Xylene					0											0.00126977	
Nonane					0											8.76949E-06	
C10+					0											1.13743E-08	
Mass Fraction		**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**	**%**
Water					99.9583											99.9581	
H2S					0											0	
Nitrogen					0.000191784											0.000195051	
Carbon Dioxide					0.00237637											0.00239114	
Methane					0.0219373											0.0221648	
Ethane					0.00895571											0.00898272	
Propane					0.00452591											0.00459583	
Isobutane					0.000242034											0.000240920	
n-Butane					0.00104614											0.00102776	
Isopentane					0.000218213											0.000215539	
n-Pentane					0.000212857											0.000206656	
2-Methylpentane					2.38818E-05											2.28573E-05	
3-Methylpentane					3.85563E-05											3.72764E-05	
n-Hexane					3.25155E-05											3.10812E-05	
Methylcyclopentane					5.31306E-05											5.32615E-05	
Benzene					0.000741368											0.000734567	
2-Methylhexane					7.10172E-06											7.05841E-06	
3-Methylhexane					5.57450E-06											5.52824E-06	
Heptane					1.18276E-05											1.20758E-05	
Methylcyclohexane					4.84091E-05											4.71095E-05	
Toluene					0.000513289											0.000500800	
Octane					5.05511E-06											4.79123E-06	
Ethylbenzene					0.000123308											0.000121407	
m-Xylene					0.000160610											0.000156587	
o-Xylene					0.000198186											0.000192429	
Nonane					1.69480E-06											1.60551E-06	
C10+					3.63202E-09											3.32197E-09	
Mass Flow		**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**	**lb/h**
Water					0											70025.0	
H2S					0											0	
Nitrogen					0											0.136642	
Carbon Dioxide					0											1.67510	
Methane					0											15.5274	
Ethane					0											6.29279	
Propane					0											3.21958	
Isobutane					0											0.168775	
n-Butane					0											0.719989	
Isopentane					0											0.150995	
n-Pentane					0											0.144772	
2-Methylpentane					0											0.0160125	
3-Methylpentane					0											0.0261138	

n-Hexane					0											0.0217737	
Methylcyclopentane					0											0.0373120	
Benzene					0											0.514596	
2-Methylhexane					0											0.00494473	
3-Methylhexane					0											0.00387277	
Heptane					0											0.00845964	
Methylcyclohexane					0											0.0330022	
Toluene					0											0.350832	
Octane					0											0.00335647	
Ethylbenzene					0											0.0850509	
m-Xylene					0											0.109696	
o-Xylene					0											0.134805	
Nonane					0											0.00112473	
C10+					0											2.32719E-06	

Process Streams		Well Stream	HP Separator Gas	HP Separator Water	HP Separator Oil	OT Flash Gas	Sales Oil	Gas	Water	Oil	Produced Water	PWT Flash Gas	Oil W/B	Water W/B	1	3	LP Separator Oil
Phase: Heavy Liquid	Status	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved	Solved
Property	Units																
Temperature	°F				70.0											66.0894	
Pressure	psig				200											200	
Mole Fraction Vapor	%				0											0	
Mole Fraction Light Liquid	%				0											0	
Mole Fraction Heavy Liquid	%				100											100	
Molecular Weight	lb/lbmol				18.0											18.0167	
Mass Density	lb/ft^3				62.3											62.2979	
Molar Flow	lbmol/h				0.0											3888.30	
Mass Flow	lb/h				0.0											70054.4	
Vapor Volumetric Flow	MCFH				0.0											1.12451	
Liquid Volumetric Flow	Mbbl/d				0.0											4.80679	
Std Vapor Volumetric Flow	MMSCFD				0.0											35.4132	
Std Liquid Volumetric Flow	Mbbl/d				0.0											4.80508	
Compressibility					0.011											0.0110046	
Specific Gravity					0.998											0.998860	
API Gravity					10.0											10.0432	
Enthalpy	MMBtu/h				0.0											-478.448	
Mass Enthalpy	Btu/lb				-6825.8											-6829.67	
Mass Cp	Btu/(lb*°F)				1.0											0.983352	
Ideal Gas CpCv Ratio					1.326											1.32600	
Dynamic Viscosity	cP				1.0											1.04689	
Kinematic Viscosity	cSt				1.0											1.04907	
Thermal Conductivity	Btu/(h*ft*°F)				0.3											0.344705	
Surface Tension	lbf/ft				0.005											0.00506994	
Net I.G. Heating Value	Btu/ft^3				0.4											0.388970	
Net Liquid Heating Value	Btu/lb				-1051.2											-1051.15	
Gross I.G. Heating Value	Btu/ft^3				50.7											50.7208	
Gross Liquid Heating Value	Btu/lb				8.9											9.0	

September 26, 2013

FESCO, Ltd.
1100 FESCO Avenue- Alice, Texas 78332

For: Antero Resources Appalachian Corp.
1625 17th Street
Denver, Colorado 80202

Sample: Prunty No. 1H (Lockhart Heirs Pad)
Separator Hydrocarbon Liquid
Sampled @ 200 psig & 66 oF

Date Sampled: 09/05/13 Job Number: 35453.002

CHROMATOGRAPH EXTENDED ANALYSIS- GPA 2186-M

COMPONENT	MOL%	LIQ VOL%	WT%
Nitrogen	0.018	0.004	0.005
Carbon Dioxide	0.031	0.011	0.013
Methane	4.766	1.667	0.703
Ethane	5.726	3.161	1.584
Propane	6.545	3.722	2.654
Isobutane	2.067	1.396	1.105
n-Butane	5.909	3.845	3.159
2,2 Dimethylpropane	0.174	0.138	0.116
Isopentane	3.770	2.846	2.502
n-Pentane	4.872	3.645	3.233
2,2 Dimethylbutane	0.188	0.162	0.149
Cyclopentane	0.000	0.000	0.000
2,3 Dimethylbutane	0.408	0.345	0.323
2 Methylpentane	2.525	2.163	2.001
3 Methylpentane	1.645	1.386	1.304
n-Hexane	4.430	3.760	3.511
Heptanes Plus	56.925	71.749	77.639
Totals:	100.000	100.000	100.000

Characteristics of Heptanes Plus:

Specific Gravity	0.7695	(Water-1)
°API Gravity	52.38	@ 60°F
Molecular Weight	148.3	
Vapor Volume	16.47	CF/Gal
Weight	6.41	Lbs/Gal

Characteristics of Total Sample:

Specific Gravity	0.7111	(Water=1)
°API Gravity	67.48	@ 60°F
Molecular Weight	108.7	
Vapor Volume	20.76	CF/Gal
Weight	5.93	Lbs/Gal

Base Conditions: 14.850 PSI & 60 oF

Certified: FESCO, Ltd. - Alice, Texas

Analyst: XG
Processor: JCdjv
Cylinder ID: W-1106

David Dannhaus 361-661-7015

TANKS DATA INPUT REPORT

COMPONENT	Mol%	LiqVol%	Wt%
Carbon Dioxide	0.031	0.011	0.013
Nitrogen	0.018	0.004	0.005
Methane	4.766	1.667	0.703
Ethane	5.726	3.161	1.584
Propane	6.545	3.722	2.654
Isobutane	2.067	1.396	1.105
n-Butane	6.083	3.983	3.274
Isopentane	3.770	2.846	2.502
n-Pentane	4.872	3.645	3.233
Other C-6's	4.766	4.057	3.778
Heptanes	10.970	9.986	9.818
Octanes	13.091	12.723	13.001
Nonanes	5.657	6.431	6.603
Decanes Plus	24.100	40.280	45.352
Benzene	0.283	0.163	0.203
Toluene	0.744	0.514	0.630
E-Benzene	0.510	0.406	0.498
Xylenes	1.570	1.245	1.533
n-Hexane	4.430	3.760	3.511
2,2,4 Trimethylpentane	0.000	0.000	0.000
Totals:	100.000	100.000	100.000

Characteristics of Total Sample:

Specific Gravity	0.7111	(Water-1)
°API Gravity	67.48	@ 60°F
Molecular Weight	108.7	
Vapor Volume	20.76	CF/Gal
Weight	5.93	Lbs/Gal

Characteristics of Decanes (C10) Plus:

Specific Gravity	0.8007	(Water-1)
Molecular Weight	204.6	

Characteristics of Atmospheric Sample:

°API Gravity	59.13	@ 60°F
Reid Vapor Pressure (ASTM D-5191)	3.41	psi

QUALITY CONTROL CHECK			
	Sampling Conditions	Test Samples	
Cylinder Number	------	W-1106*	W-1020
Pressure, PSIG	200	176	173
Temperature, °F	66	70	70

* Sample used for analysis

TOTAL EXTENDED REPORT

COMPONENT	Mol%	LiqVol%	Wt%
Nitrogen	0.018	0.004	0.005
Carbon Dioxide	0.031	0.011	0.013
Methane	4.766	1.667	0.703
Ethane	5.726	3.161	1.584
Propane	6.545	3.722	2.654
Isobutane	2.067	1.396	1.105
n-Butane	5.909	3.845	3.159
2,2 Dimethylpropane	0.174	0.138	0.116
Isopentane	3.770	2.846	2.502
n-Pentane	4.872	3.645	3.233
2,2 Dimethylbutane	0.188	0.162	0.149
Cyclopentane	0.000	0.000	0.000
2,3 Dimethylbutane	0.408	0.345	0.323
2 Methylpentane	2.525	2.163	2.001
3 Methylpentane	1.645	1.386	1.304
n-Hexane	4.430	3.760	3.511
Methylcyclopentane	0.924	0.675	0.715
Benzene	0.283	0.163	0.203
Cyclohexane	0.990	0.695	0.766
2-Methylhexane	2.385	2.288	2.198
3-Methylhexane	1.879	1.780	1.732
2,2,4 Trimethylpentane	0.000	0.000	0.000
Other C-7's	0.950	0.888	0.867
n-Heptane	3.842	3.658	3.540
Methylcyclohexane	3.402	2.823	3.072
Toluene	0.744	0.514	0.630
Other C-8's	6.777	6.822	6.870
n-Octane	2.912	3.079	3.059
E-Benzene	0.510	0.406	0.498
M & P Xylenes	0.777	0.622	0.758
0-Xylene	0.793	0.623	0.775
Other C-9's	3.760	4.227	4.366
n-Nonane	1.897	2.203	2.238
Other C-1O's	3.702	4.574	4.810
n-decane	1.350	1.710	1.766
Undecanes(11)	3.614	4.581	4.885
Dodecanes(12)	2.655	3.636	3.932
Tridecanes(13)	2.209	3.243	3.555
Tetradecanes(14)	1.728	2.718	3.020
Pentadecanes(15)	1.331	2.242	2.521
Hexadecanes(16)	1.068	1.923	2.181
Heptadecanes(17)	0.926	1.763	2.018
Octadecanes(18)	0.821	1.647	1.896
Nonadecanes(19)	0.691	1.442	1.670
Eicosanes(20)	0.601	1.304	1.519
Heneicosanes(21)	0.459	1.048	1.228
Docosanes(22)	0.372	0.884	1.042
Tricosanes(23)	0.349	0.862	1.021
Tetracosanes(24)	0.313	0.800	0.952
Pentacosanes(25)	0.261	0.693	0.829
Hexacosanes(26)	0.243	0.668	0.803
Heptacosanes(27)	0.193	0.550	0.664
Octacosanes(28)	0.192	0.565	0.684
Nonacosanes(29)	0.157	0.479	0.582
Triacontanes(30)	0.150	0.470	0.574
Hentriacontanes Plus(31+)	0.717	2.481	3.199
Total	100.000	100.000	100.000

October 7, 2013

FESCO, Ltd.
1100 Fesco Avenue- Alice, Texas 78332

For: Antero Resources Appalachian Corp.
1625 17th Street
Denver, Colorado 80202

Date Sampled: 09/05/13

Date Analyzed: 09/13/13

Job Number: J35434

Sample: Prunty No. 1H (Lockhart Heirs Pad)

FLASH LIBERATION OF SEPARATOR WATER		
	Separator	Stock Tank
Pressure, psig	200	0
Temperature, "F	66	70
Gas Water Ratio (1)	------	1.55
Gas Specific Gravity (2)	------	0.922

(1) - Scf of water saturated vapor per barrel of stock tank water
(2)- Air= 1.000
(3) - Separator volume / Stock tank volume
Analyst: O. A.

Piston No. : WF-133*

Base Conditions: 14.85 PSI & 60 "F

Certified: FESCO, Ltd. Alice, Texas

David Dannhaus 361-661-7015

September 18, 2013

FESCO, Ltd.
1100 Fesco Ave. · Alice, Texas 78332

For: Antero Resources Appalachian Corp.
1625 17th Street
Denver, Colorado 80202

Sample: Prunty No. 1H (Lockhart Heirs Pad)
Gas Liberated from Separator Water
From 200 psig & 66 oF to 0 psig & 70 oF

Date Sampled: 09/05/13 Job Number: 35453.001

CHROMATOGRAPH EXTENDED ANALYSIS SUMMATION REPORT

COMPONENT	MOL%	GPM
Hydrogen Sulfide*	< 0.001	
Nitrogen	0.000	
Carbon Dioxide	1.891	
Methane	63.614	
Ethane	17.120	4.615
Propane	7.633	2.119
Isobutane	1.356	0.447
n-Butane	3.304	1.050
2-2 Dimethylpropane	0.064	0.025
Isopentane	1.192	0.439
n-Pentane	1.225	0.448
Hexanes	1.136	0.472
Heptanes Plus	1.465	0.652
Totals	100.000	10.266

Computed Real Characteristics Of Heptanes Plus:

Specific Gravity	3.602	(Air=1)
Molecular Weight	103.68	
Gross Heating Value	5501	BTU/CF

Computed Real Characteristics Of Total Sample:

Specific Gravity	0.922	(Air=1)
Compressibility (Z)	0.9937	
Molecular Weight	26.54	
Gross Heating Value		
Dry Basis	1548	BTU/CF
Saturated Basis	1522	BTU/CF

*Hydrogen Sulfide tested in laboratory by: Stained Tube Method (GPA 2377)
Results: <0.013 Gr/100 CF, <0.2 PPMV or <0.001 Mol%

Base Conditions: 14.850 PSI & 60 Deg F

Certified: FESCO, Ltd. Alice, Texas

Analyst: MR
Processor: ANB
Cylinder ID: WF# 13 S

David Dannhaus 361-661-7015

CHROMATOGRAPH EXTENDED ANALYSIS
TOTAL REPORT

COMPONENT	MOL%	GPM	WT%
Hydrogen Sulfide*	< 0.001		< 0.001
Nitrogen	0.000		0.000
Carbon Dioxide	1.891		3.135
Methane	63.614		38.445
Ethane	17.120	4.615	19.393
Propane	7.633	2.119	12.680
lsobutane	1.356	0.447	2.969
n-Butane	3.304	1.050	7.234
2,2 Dimethylpropane	0.064	0.025	0.174
lsopentane	1.192	0.439	3.240
n-Pentane	1.225	0.448	3.330
2,2 Dimethylbutane	0.035	0.015	0.114
Cyclopentane	0.019	0.008	0.050
2,3 Dimethylbutane	0.060	0.025	0.195
2 Methylpentane	0.334	0.140	1.084
3 Methylpentane	0.207	0.085	0.672
n-Hexane	0.481	0.199	1.562
Methylcyclopentane	0.071	0.025	0.225
Benzene	0.042	0.012	0.124
Cyclohexane	0.089	0.031	0.282
2-Methylhexane	0.113	0.053	0.427
3-Methylhexane	0.108	0.050	0.408
2,2,4 Trimethylpentane	0.000	0.000	0.000
Other C?'s	0.121	0.053	0.452
n-Heptane	0.183	0.085	0.691
Methylcyclohexane	0.161	0.065	0.596
Toluene	0.057	0.019	0.198
Other C8's	0.217	0.102	0.901
n-Octane	0.070	0.036	0.301
Ethylbenzene	0.003	0.001	0.012
M & P Xylenes	0.031	0.012	0.124
0-Xylene	0.005	0.002	0.020
Other C9's	0.099	0.051	0.471
n-Nonane	0.033	0.019	0.159
Other C10's	0.044	0.026	0.234
n-Decane	0.010	0.006	0.054
Undecanes (11)	0.008	0.005	0.044
Totals	100.000	10.266	100.000

Computed Real Characteristics Of Total Sample:

Specific Gravity----------	0.922	(Air-1)
Compressibility (Z) ----------	0.9937	
Molecular Weight----------	26.54	

Gross Heating Value

Dry Basis ----------	1548	BTU/CF
Saturated Basis ----------	1522	BTU/CF

Antero Resources
Prunty Unit 1H - Lockhart Heirs Pad

Tag Name	Value	Units	Timestamp
Accumulated Gas Flow	560999.8	MCF	10/16/2013 16:11:13
Casing Pressure	450.96	PSIA	10/16/2013 17:05:05
Current Day Gas Flow	2287.78	MCF	10/16/2013 16:11:13
Differential Pressure	57.03	inH2O	10/16/2013 16:11:13
Flow Rate	7454.35	MCF Per Day	10/16/2013 16:11:13
Pressure	108.81	PSIA	10/16/2013 16:11:13
Previous Day Energy	9462.83	MBTU	10/16/2013 16:11:15
Previous Day Gas Flow	7588.11	MCF	10/16/2013 16:11:15
Temperature	60.11	F	10/16/2013 16:11:13
Tubing Pressure	748.58	PSIA	10/16/2013 17:05:05
Daily AP	63.93	PSIA	10/16/2013 09:00:00
Daily DP	111.06	inH2O	10/16/2013 09:00:00
Daily Energy	9462.83	MBTU	10/16/2013 09:00:00
Daily Flow	7588.11	MCF	10/16/2013 09:00:00
Daily Tf	59.56	F	10/16/2013 09:00:00
Hourly AP	110.1	PSIA	10/16/2013 10:00:00
Hourly DP	61.64	Inches	10/16/2013 10:00:00
Hourly Energy	399.7	MBTU	10/16/2013 10:00:00
Hourly Flow Time	3600	Seconds	10/16/2013 10:00:00
Hourly Tf	61.1	F	10/16/2013 10:00:00
Hourly Volume	320.5	MCF	10/16/2013 10:00:00
Argon	0	%	10/16/2013 16:11:25
BTU	1247.06	BTU	10/16/2013 16:11:13
C02	0.1467	%	10/16/2013 16:11:25
Carbon Monoxide	0	%	10/16/2013 16:11:25
Decane	0	%	10/16/2013 16:11:25
Ethane	14.1987	%	10/16/2013 16:11:25
Helium	0	%	10/16/2013 16:11:25
Heptane	0	%	10/16/2013 16:11:25
Hexane	0.5451	%	10/16/2013 16:11:25
Hydrogen	0	%	10/16/2013 16:11:25
Hydrogen Sulfide	0	%	10/16/2013 16:11:25
Iso-Butane	0.5666	%	10/16/2013 16:11:25
Iso-Pentane	0.3749	%	10/16/2013 16:11:25
Methane	77.6927	%	10/16/2013 16:11:25
N2	0.4946	%	10/16/2013 16:11:25
N-Butane	1.1838	%	10/16/2013 16:11:25
Nonane	0	%	10/16/2013 16:11:25
N-Pentane	0.2914	%	10/16/2013 16:11:25
Octane	0	%	10/16/2013 16:11:25
Oxygen	0.0117	%	10/16/2013 16:11:25
Plate Size	3.75	Inches	10/16/2013 16:11:20
Propane	4.4938	%	10/16/2013 16:11:25
SPG	0.7248		10/16/2013 16:11:13
Water	0	%	10/16/2013 16:11:25

Attachment J

Class I Legal Advertisement

Attachment J

Air Quality Permit Notice
Notice of Application
Stanley Well Pad
Antero Resources Corporation
Doddridge, West Virginia

Notice is given that Antero Resources Corporation has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a General Permit Registration for an Oil and Natural Gas facility located at 0.20 mile south from the intersection of Taylor Drain Rte. 19 and Cabin Run Rte. 21/1. in Doddridge, West Virginia.

The latitude and longitude coordinates are: 39.236867 degrees N and -80.879461 degrees W

The applicant estimates the potential to discharge the following Regulated Air Pollutants will be:

Pollutants	TOTALS (tpy):
VOC	41.4430
NO_X	7.0589
CO_{2e}	11484.7000
CO	29.4905
SO_2	0.0260
$PM_{2.5}$	0.4140
PM_{10}	2.9719
Lead	2.84E-05
Total HAPs	2.2851
Benzene	0.0595
Formaldehyde	0.0247
Xylenes	0.1933

Startup of operation is planned to begin in May 2016. Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1227, during normal business hours.
Dated this the____, 2015

By: Antero Resources Corporation
Barry Schatz
Senior Environmental & Regulatory Manager
1615 Wynkoop Street
Denver, CO 80202

Attachment K

Electronic Submittal

Attachment K

Electronic Submittal
Stanley Well Pad
Antero Resources Corporation
Doddridge West Virginia

No electronic submission was made.

Attachment L

General Permit Registration Application Fee

Conestoga-Rovers & Associates, Inc.

▼ PLEASE DETACH AND RETAIN FOR YOUR RECORDS ▼

INVOICE NUMBER	DATE		VOUCHER NO.	AMOUNT
Account Number:		40WVDEPAQ	407684	
CR60215	6/2/2015	400953358		1,500.00
		TOTAL:		1,500.00

THIS DOCUMENT IS PROTECTED BY A MICRO-PRINT SIGNATURE LINE, FLUORESCENT PAPER FIBERS, A WATERMARKED BACKER, AND IS REACTIVE TO CHEMICAL ALTERATION

Conestoga-Rovers & Associates, Inc.
2055 NIAGARA FALLS BLVD, SUITE 3
NIAGARA FALLS, NY 14304

M&T BANK
MANUFACTURERS AND TRADERS TRUST COMPANY
Commercial Banking
Main Office, Ithaca, NY 14850
50-7063-2213

6/2/2015 NO. 407684

PAY **********1,500 DOLLARS AND **********00 CENTS $ **********1,500.00

TO THE ORDER OF
WV Dept. of Environmental Protectio
Division Air Quality
601 57th Street SE
Charleston,, WV 25304 US

Conestoga-Rovers & Associates, Inc.

AUTHORIZED SIGNATURES

WARNING: THIS DOCUMENT IS VOID IF ACCOUNT NUMBER DOES NOT APPEAR ON THE REVERSE SIDE IN RED

⑈407684⑈ ⑆221370632⑆6 1000000 18910⑈

Attachment M

Siting Criteria Waiver

Attachment M

Siting Waiver
Stanley Well Pad
Antero Resources Corporation
Doddridge County, West Virginia

A Siting Waiver form is not required because there are no occupied dwelling structures within 300 feet of Stanley Well Pad.

Attachment N

Material Safety Data Sheet

Attachment N

Description of Material Safety Data Sheets (MSDS)
Stanley Well Pad
Antero Resources Corporation
Doddridge County, West Virginia

Three generic Material Safety Data Sheets (MSDS), and analysis of the condensate and produced water of a similar well with the same formation are provided. Antero Resources Corporation has developed its own MSDS for these materials.

1. Natural Gas: The MSDS for natural gas reflects pipeline quality odorized gas. This is essentially the same as the material delivered to the metering and downstream gathering lines from the Antero well pad.
2. Condensate: Condensate is the hydrocarbon liquid that has been separated from raw natural gas through the well pad gas production unit. The liquid is often characterized as having a gasoline-like odor and consistency.
3. Produced Water: Produced water is primarily groundwater with residual trace hydrocarbons that has been withdrawn from the ground during the gas extraction process and then separated from the natural gas and condensate in the gas production units.

SAFETY DATA SHEET

Material Name: Dry Field Natural Gas **US GHS**

SYNONYMS: **CNG, Natural Gas, Methane.**

* * * Section 1 – PRODUCT AND COMPANY IDENTIFICATION * * *

PRODUCT NAME: **Dry Field Natural Gas**
PRODUCT CODES: **CAS Reg. No. 68410-63-9**

EMERGENCY PHONE: **(800) 878-1373**
AFTER HOURS: **(800) 878-1373**

PRODUCER: **Antero Resources**
ADDRESS: **1615 Wynkoop Street**
Denver, Colorado 80202

CHEMTREC PHONE: **(800) 424-9300**

* * * Section 2 – HAZARDS IDENTIFICATION * * *

GHS Classification:

Flammable Gas – Category 1.
Gases Under Pressure – Gas.
Specific Target Organ Systemic Toxicity (STOT) – Single Exposure Category 2.

GHS LABEL ELEMENTS

Symbol(s)

Signal Word

Danger

Hazard Statements

Extremely flammable gas.
Contains gas under pressure, may explode if heated.
May cause damage to central nervous and respiratory systems.

Precautionary Statements

Prevention

Keep away from heat/sparks/open flames/hot surfaces. No smoking.
Do not breathe fume/gas/mist/vapors/spray.
Wash thoroughly after handling.
Do not eat, drink or smoke when using this product.

Response

Leaking gas fire: Do not extinguish, unless leak can be stopped safely. Eliminate all ignition sources if safe to do so.
If exposed to gas, or concerned about possible exposure: Call a POISON CENTER or doctor/physician.

Storage

Protect from sunlight. Store in a well-ventilated place.
Store in a secure area.

Disposal

Dispose of contents/containers in accordance with local/regional/national/international regulations.

* * * Section 3 – COMPOSITION / INFORMATION ON INGREDIENTS * * *

CAS #	Component	Percent
74-82-8	Methane	95.01
78-84-0	Ethane	3.99
74-98-6	Propane	0.32
106-97-8	Butanes	0.07
109-66-0	Pentanes	0.02
110-54-3	Hexanes	0.01
7727-37-9	Nitrogen	0.35
124-38-9	Carbon Dioxide	0.19
7782-44-7	Oxygen	0.03

Because natural gas is a natural product, composition can vary greatly.

* * * Section 4 – FIRST AID MEASURES * * *

First Aid: Eyes

In case of freeze burn, cover eyes to protect from light. Flush eyes with running water for at least fifteen (15) minutes. Following flushing, seek medical attention.

First Aid: Skin

Remove contaminated clothing. In case of blistering, frostbite or freeze burns, seek immediate medical attention.

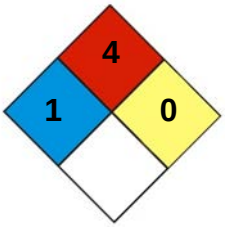
First Aid: Ingestion

Risk of ingestion is extremely low. However, if oral exposure occurs, seek immediate medical assistance.

First Aid: Inhalation

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

* * * Section 5 – FIRE FIGHTING MEASURES * * *



NFPA 704 Hazard Class

Health: **1** Flammability: **4** Instability: **0** (0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

General Fire Hazards

See Section 9 for Flammability Properties.
Forms a flammable mixture with air. If released, the resulting vapors will disperse with the prevailing wind. If a source of ignition is present where the vapor exists at a 5 – 15% concentration in air, the vapor will burn along the flame front toward the source of the fuel.

Hazardous Combustion Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

Extinguishing Media

Any extinguisher suitable for Class B fires, dry chemical, fire fighting foam, CO2, and other gaseous agents. However, fire should not be extinguished unless flow of gas can be immediately stopped.

Unsuitable Extinguishing Media

None.

Fire Fighting Equipment / Instructions

Gas fires should not be extinguished unless flow of gas can be immediately stopped. Shut off gas source and allow gas to burn out. If spill or leak has not ignited, determine

if water spray may assist in dispersing gas or vapor to protect personnel attempting to stop leak. Use water to cool equipment, surfaces and piping exposed to fire and excessive heat. For large fire, the use of unmanned hose holders or monitor nozzles may be advantageous to further minimize personnel exposure. Isolate area, particularly around piping. Let the fire burn unless leak can be stopped. Concentrate fire-fighting efforts on objects / materials ignited by the initial fire. Withdraw immediately in the event of a rising sound from a venting safety device.

Firefighting activities that may result in potential exposure to high heat, smoke or toxic by-products of combustion should require NIOSH-approved pressure-demand self-contained breathing apparatus with full facepiece and full protective clothing.

* * * Section 6 – ACCIDENTAL RELEASE MEASURES * * *

Recovery and Neutralization

Stop the source of the release, if safe to do so.

Materials and Methods for Clean-Up

Consider the use of water spray to disperse gas vapors. Do not use water spray to direct gas vapors toward sewer or drainage systems. Isolate the area until gas has dispersed. Ventilate and gas test area before entering.

Emergency Measures

Evacuate nonessential personnel and secure all ignition sources. No road flares, smoking or flames in hazard area. Consider wind direction. Stay upwind and uphill, if possible. Vapor cloud may be white, but color will dissipate as cloud disperses. Fire and explosion hazard is still present.

Personal Precautions and Protective Equipment

Cooling effect of expanding gas from leak may present frostbite / freeze burn hazard. Wear flame retardant (FR) clothing around un-ignited leak. Wear fire protective clothing around an active fire.

Environmental Precautions

Do not flush gas vapors toward sewer or drainage systems.

Prevention of Secondary Hazards

None.

* * * Section 7 – HANDLING AND STORAGE * * *

Handling Procedures

Keep away from flame, sparks and excessive temperatures. Bond and ground containers. Use only in well ventilated areas.

Storage Procedures

Natural gas will be contained in the pipeline. Keep away from flame, sparks, excessive temperatures and open flames. Empty pipeline segments may contain explosive residues from natural gas liquids. Do not cut, heat, weld or expose containers to sources of ignition sections of pipeline unless the sections have been purged of natural gas residues.

Incompatibilities

Keep away from strong oxidizers, ignition sources and heat.

* * * Section 8 – EXPOSURE CONTROLS / PERSONAL PROTECTION * * *

Component Exposure Limits

Methane (74-82-8)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Ethane (74-84-0)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Propane (74-98-6)

ACGIH: 2500 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Butane (106-97-8)

ACGIH: 800 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Pentanes (109-66-0)

ACGIH: 600 ppm TWA (listed under Pentane, all isomers)

Hexanes (110-54-3)

ACGIH: 50 ppm TWA (listed under n-Hexane)

Nitrogen (7727-37-9)

Simple Asphyxiant

Carbon Dioxide (124-38-9)

ACGIH: 5000 ppm TWA (listed under Carbon Dioxide)

Oxygen (7782-44-7)

N/A – Necessary for life

Engineering Measures

Use adequate ventilation to keep gas and vapor concentrations of this product below occupational exposure and flammability limits, particularly in confined spaces. Use explosion-proof equipment and lighting in classified / controlled areas.

Personal Protective Equipment: Respiratory

Use a NIOSH approved positive-pressure, supplied air respirator with escape bottle or self-contained breathing apparatus (SCBA) for gas concentrations above occupational exposure limits, for potential for uncontrolled release, if exposure levels are not known, or in an oxygen-deficient atmosphere. CAUTION: Flammability limits (i.e., explosion hazard should be considered when assessing the need to expose personnel to concentrations requiring respiratory protection.

Personal Protective Equipment: Hands

Use cold-impervious, insulating flame-retardant (FR) gloves where contact with pressurized gas may occur.

Personal Protective Equipment: Eyes

Where there is a possibility of pressurized gas contact, wear splash-proof safety goggles and faceshield.

Personal Protective Equipment: Skin and Body

Where contact with pressurized gas may occur, wear flame-retardant (FR) and a faceshield.

* * * Section 9 – PHYSICAL AND CHEMICAL PROPERTIES * * *

Appearance:	Colorless	**Odor:**	Odorless to slight petroleum odor
Physical State:	Gas	**pH:**	ND
Vapor Pressure:	40 atm @ -187°F (-86°C)	**Vapor Density:**	0.6
Boiling Point:	-259°F (-162°C)	**Melting Point:**	ND
Solubility (H2O):	3.5%	**Specific Gravity:**	0.4 @ -263°F (-164°C)

Evaporation Rate:	ND	**VOC:**	ND
Octanol / H2O Coeff.:	ND	**Flash Point:**	Flammable Gas
Flash Point Method:	N/A		
Lower Flammability Limit: (LFL):	3.8 – 6.5	**Upper Flammability Limit: (UFL):**	13-17
Auto Ignition:	900-1170°F (482-632°C)	**Burning Rate:**	ND

* * * Section 10 – CHEMICAL STABILITY & REACTIVITY INFORMATION * * *

Chemical Stability

This is a stable material.

Hazardous Reaction Potential

Will not occur.

Conditions to Avoid

Keep away from strong oxidizers, ignition sources and heat.

Hazardous Decomposition Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

* * * Section 11 – TOXICOLOGICAL INFORMATION * * *

Acute Toxicity

A: General Product Information

Methane and ethane, the main components of natural gas, are considered practically inert in terms of physiological effects. At high concentrations these materials act as simple asphyxiants and may cause death due to lack of oxygen.

B. Component Analysis – LD50/LC50

Methane (74-82-8)

Inhalation LC50 Mouse 326 g/m3 2h

Ethane (74-84-0)

Inhalation LC50 Rat 658 mg/l 4h

Propane (74-98-6)

Inhalation LC50 Rat 658 mg/l 4h

Butanes (106-97-8)
Inhalation LC50 Rat 658 g/m3 4h

Pentanes (109-66-0)
Inhalation LD50 Rat 364 g/m3 4h

Hexanes (110-54-3)
Inhalation LC50 Rat > 20 mg/l 4h

Nitrogen (7727-37-9)
Simple Asphyxiant

Carbon Dioxide (124-38-9)
Inhalation LC50 Human 100,000 ppm 1minute

Oxygen (7782-44-7)
N/A – Necessary for life

Potential Health Effects: Skin Corrosion Property / Stimulativeness
This product is not reported to have any skin sensitization effects.

Generative Cell Mutagenicity
This product is not reported to have any mutagenic effects.

Carcinogenicity

A: General Product Information
This product is not reported to have any carcinogenic effects.

B: Component Carcinogenicity
None of this product's components are listed by ACGIH, IARC, OSHA, NIOSH, or NTP.

Reproductive Toxicity
This product is not reported to have any reproductive toxicity effects.

Specified Target Organ General Toxicity: Single Exposure
This product may cause damage to the heart.

Specified Target Organ General Toxicity: Repeated Exposure
This product is not reported to have any specific target organ repeat effects.

Aspiration Respiratory Organs Hazard
This product is not reported to have any aspiration hazard effects.

* * * Section 12 – ECOLOGICAL INFORMATION * * *

Ecotoxicity

A: General Product Information

Keep gas and vapors out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

B: Component Analysis – Ecotoxicity – Aquatic Toxicity

No ecotoxicity data are available for this product's components.

Persistance / Degradability

No information available.

Bioaccumulation

No information available.

Mobility in Soil

No information available.

* * * Section 13 – DISPOSAL CONSIDERATIONS * * *

Waste Disposal Instructions

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

Disposal of Contaminated Containers or Packaging

Dispose of contents / container in accordance with local / regional / national / international regulations.

* * * Section 14 – TRANSPORTATION INFORMATION * * *

DOT Information

Shipping Name: Natural Gas, Compressed

UN #: 1971 **Hazard Class:** 2.1

Placard:

* * * Section 15 – REGULATORY INFORMATION * * *

Regulatory Information

Component Analysis

None of this products components are listed under SARA Section 302 (40 CFR 355 Appendix A.
n-hexane is listed under SARA Section 313 (40 CFR 372.65). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

n-hexane is listed under CERCLA (40 CFR 302.4). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

SARA Section 311/312 – Hazard Classes

Acute Health	Chronic Health	Fire	Sudden Release of Pressure	Reactive
---	---	X	X	---

SARA Section 313 – Supplier Notification

This product contains one chemical (n-Hexane) that is subject to the reporting requirements of section 313 of the Emergency Planning and Community Right-to-know act (EPCRA) of 1986 and of 40 CFR 372. However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

State Regulations

Component Analysis – State

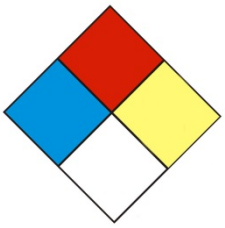
The following components appear on one or more of the following state hazardous substances lists:

Component	CAS	CA	MA	MN	NJ	PA	RI
Methane	74-82-8	No	No	Yes	Yes	Yes	No
Ethane	78-84-0	No	No	Yes	Yes	Yes	No
Propane	74-98-6	No	No	Yes	Yes	Yes	Yes
Butane	106-97-8	Yes	No	Yes	Yes	Yes	Yes
Pentanes	109-66-0	Yes	No	Yes	Yes	Yes	Yes
Hexanes	110-54-3	Yes	Yes	Yes	Yes	Yes	Yes
Nitrogen	7727-37-9	No	No	No	No	No	No
Carbon Dioxide	124-38-9	Yes	No	Yes	Yes	Yes	Yes
Oxygen	7782-44-7	No	No	No	No	No	No

* * * Section 16 – OTHER INFORMATION * * *

NFPA® Hazard Rating

Health	1
Fire	4
Reactivity	0



HMIS® Hazard Rating

Health	1	Moderate
Fire	4	Severe
Physical	0	Minimal
		* Chronic

Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act: ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

Literature References

None

Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: January 30, 2014

Date of Last Revision: March 4, 2014

End of Sheet

SAFETY DATA SHEET

Material Name: Natural Gas Condensate **US GHS**

SYNONYMS: **Drips; Condensate; Field Condensate; Gas Well Condensate; High Pressure Inlet Liquids; Lease Condensate; Natural Gas Liquids; Pipeline Liquids**

* * * Section 1 – PRODUCT AND COMPANY IDENTIFICATION * * *

PRODUCT NAME: **Natural Gas Condensate**
PRODUCT CODES: **64741-47-5**

EMERGENCY PHONE: **(800) 878-1373**
AFTER HOURS: **(800) 878-1373**

PRODUCER: **Antero Resources**
ADDRESS: **1615 Wynkoop Street**
Denver, Colorado 80202

CHEMTREC PHONE: **(800) 424-9300**

* * * Section 2 – HAZARDS IDENTIFICATION * * *

GHS Classification:

Flammable Liquids – Category 2.
Acute Toxicity Inhalation – Category 3
Germ Cell Mutagenicity – Category 1B
Carcinogenicity – Category 1A
Specific Target Organ Systemic Toxicity (STOT) – Single Exposure Category 3
Specific Target Organ Systemic Toxicity (STOT) – Repeat Exposure Category 1
Aspiration Toxicity – Category 1
Toxic to the Aquatic Environment Acute – Category 3

GHS LABEL ELEMENTS

Symbol(s)

Signal Word

Danger

Hazard Statements

Highly flammable liquid and vapor.
Toxic if inhaled.
May cause genetic defects.
May cause cancer.
May cause respiratory irritation.
May cause drowsiness or dizziness.
May cause damage to organs (liver, kidneys, blood, nervous system, and skin) through prolonged or repeated exposure.
May be fatal if swallowed and enters airways.
Harmful to aquatic life.

Precautionary Statements

Prevention

Keep away from heat/sparks/open flames/hot surfaces. No smoking.
Keep container tightly closed.
Ground/bond container and receiving equipment.
Use explosion-proof electrical/ventilating/lighting equipment.
Use only non-sparking tools.
Take precautionary measures against static discharge.
Wear protective gloves/protective clothing/eye protection/face protection.
Do not breathe gas/mist/vapors/spray.
Do not handle until all safety precautions have been read and understood.
Wash thoroughly after handling.
Do not eat, drink or smoke when using this product.
Use only outdoors or in a well-ventilated area.
Avoid release to the environment.

Response

If on SKIN (or hair): Wash with plenty of soap and water. Remove / Take off all contaminated clothing immediately. Rinse skin with water/shower.
If INHALED: Remove victim to fresh air and keep comfortable for breathing. Call a poison center/doctor if the victim feels unwell.
If SWALLOWED: Immediately call a poison center or doctor / physician. Do not Induce vomiting.
If exposed or concerned: Get medical advice/attention.
In case of fire: Use water spray, fog or fire-fighting foam.

Storage

Store in a well-ventilated place. Keep cool.
Store in a secure area.

Disposal

Dispose of contents/containers in accordance with local/regional/national/international regulations.

* * * Section 3 – COMPOSITION / INFORMATION ON INGREDIENTS * * *

CAS #	Component	Percent
111-65-9	Octanes	25 - 95
142-82-5	Heptanes	25 - 95
110-54-3	Hexanes as n-Hexane	25 - 95
109-66-0	Pentanes as n-Pentane	5 - 70
106-97-8	N-butane	0 - 45
74-98-6	Propane	0 - 15
78-84-0	Ethane	0 - 5
71-43-2	Benzene	< 1
108-88-3	Toluene	< 1
1330-20-7	m-,o-,p-Xylene	< 1

Because natural gas condensate is a natural product, composition can vary greatly.

* * * Section 4 – FIRST AID MEASURES * * *

First Aid: Eyes

Flush eyes with clean running water for at least fifteen (15) minutes. Following flushing, seek medical attention.

First Aid: Skin

Remove contaminated clothing. Wash contaminated areas thoroughly with soap and water or waterless hand cleanser. Obtain medical attention if irritation or redness develops. Wash contaminated clothing before reuse.

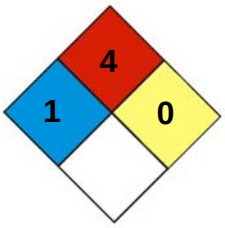
First Aid: Ingestion (swallowing)

DO NOT INDUCE VOMITING. Do not give liquids. Obtain immediate medical attention. If spontaneous vomiting occurs, lean the victim forward to reduce the risk of aspiration. Monitor for breathing difficulties. Small amounts of material which enter the mouth should be rinsed out until the taste is dissipated.

First Aid: Inhalation (breathing)

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

* * * Section 5 – FIRE FIGHTING MEASURES * * *



NFPA 704 Hazard Class

Health: 1 **Flammability:** 4 **Instability:** 0 (0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

General Fire Hazards

See Section 9 for Flammability Properties.
Extremely flammable. Vapors may be ignited rapidly when exposed to heat, spark, open flame, or other source of ignition (e.g., static electricity, pilot lights, mechanical / electrical equipment, and electronic devices such as cell phones, computers, calculators, and pagers which have not been certified as intrinsically safe). Flammable vapors can burn in the open or explode in confined spaces. Vapors are heavier than air, and may travel distances to an ignition source and flash back. Runoff to sewer systems may cause fire or explosion.

Hazardous Combustion Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

Extinguishing Media

SMALL FIRES: Any extinguisher suitable for Class B fires, dry chemical, firefighting foam, water spray, carbon dioxide (CO_2), or other gaseous extinguishing agents. Use caution when applying CO2 in confined spaces.

LARGE FIRES: Water spray, fog or fire-fighting foam. Water may be ineffective for fighting the fire, but may be used to cool fire-exposed containers.

Unsuitable Extinguishing Media

None

Fire Fighting Equipment / Instructions

Small fires in the beginning stage may typically be extinguished using handheld portable fire extinguishers and other firefighting equipment. Isolate area around container involved in fire. Cool tanks, shells, and containers exposed to fire and excessive heat with water. For massive fires the use of unmanned hose holders or monitor nozzles may be advantageous to minimize personnel exposure. Major fires may require withdrawal, allowing the tank to burn. Large storage tank fires typically require specially trained personnel and equipment to extinguish the fire, often including the need for properly applied firefighting foam.

Firefighting activities that may result in potential exposure to high heat, smoke or toxic by-products of combustion should require NIOSH/MSHA- approved pressure-demand self-contained breathing apparatus with full face piece and full protective clothing.

* * * Section 6 – ACCIDENTAL RELEASE MEASURES * * *

Recovery and Neutralization

Contain and stop the source of the spill, if safe to do so.

Materials and Methods for Clean-Up

Notify relevant authorities in accordance with all applicable regulations. Immediate cleanup of any spill is recommended. Dike far ahead of spill for later recovery or disposal. Absorb spill with inert material such as sand or vermiculite, and place in suitable container for disposal. If spilled on water remove with appropriate methods (e.g. skimming, booms or absorbents). In case of soil contamination, remove contaminated soil for remediation or disposal, in accordance with local regulations.

Recommended measures are based on the most likely spillage scenarios for this material; however local conditions and regulations may influence or limit the choice of appropriate actions to be taken.

Emergency Measures

Evacuate nonessential personnel and secure all ignition sources. No road flares, smoking or flames in hazard area. Consider wind direction. Stay upwind and uphill, if possible. Vapor cloud may be white, but color will dissipate as cloud disperses. Fire and explosion hazard is still present.

Personal Precautions and Protective Equipment

Response and clean-up crews must be properly trained and must utilize proper protective equipment (see Section 8). Extremely flammable. Spillages of liquid product will create a fire hazard and may form an explosive atmosphere. Keep all sources of

ignition and hot metal surfaces away from spill/release if safe to do so.

The use of explosion-proof electrical equipment is recommended. Stay upwind and away from spill/release. Avoid direct contact with material. For large spillages, notify persons downwind of the spill/release, isolate immediate hazard area and keep unauthorized personnel out. Wear appropriate protective equipment, including respiratory protection, as conditions warrant (see Section 8). See Sections 2 and 7 for additional information on hazards and precautionary measures.

Environmental Precautions

Protect bodies of water by diking, absorbents, or absorbent boom, if possible. Do not flush down sewer or drainage systems, unless system is designed and permitted to handle such material. The use of firefighting foam may be useful in certain situations to reduce vapors. If spill occurs on water notify appropriate authorities and advise shipping of any hazard. Spills into or upon navigable waters, the contiguous zone, or adjoining shorelines that cause a sheen or discoloration on the surface of the water, may require notification of the National Response Center (phone number 800-424-8802).

Prevention of Secondary Hazards

None

* * * Section 7 – HANDLING AND STORAGE * * *

Handling Procedures

Keep away from flame, sparks and excessive temperatures. Bond and ground containers. Use non-sparking tools. Use only outdoors or in well ventilated areas. Wear protective gloves / clothing and eye / face protection. Wash thoroughly after handling. Use good personal hygiene practices and wear appropriate personal protective equipment (see section 8).

Storage Procedures

Store only in approved containers. Bond and ground containers. Keep away from flame, sparks, excessive temperatures and open flames. Keep containers closed and clearly labeled. Empty product containers or vessels may contain explosive vapors. Do not pressurize, cut, heat, weld or expose containers to sources of ignition.

Store in a well-ventilated area. This storage area should comply with NFPA 30 "Flammable and Combustible Liquid Code". Avoid storage near incompatible materials. The cleaning of tanks previously containing this product should follow API Recommended Practice (RP) 2013 "Cleaning Mobile Tanks In Flammable and Combustible Liquid Service" and API RP 2015 "Cleaning Petroleum Storage Tanks."

Incompatibilities

Keep away from strong oxidizers, ignition sources and heat.

* * * Section 8 – EXPOSURE CONTROLS / PERSONAL PROTECTION * * *

Component Exposure Limits

Octanes (111-65-9)

ACGIH: 300 ppm TWA (listed under Octane, all isomers)

Heptanes (142-82-5)

ACGIH: 400 ppm TWA (listed under n-Heptane)

n-Hexane (110-54-3)

ACGIH: 20 ppm TWA (listed under n-Hexane)

n-Pentane (109-66-0)

ACGIH: 600 ppm TWA (listed under Pentane, all isomers)

n-Butane (106-97-8)

ACGIH: 600 ppm TWA (listed under n-Butane)

Propane (74-98-6)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases C1-C4)

Ethane (74-84-0)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases C1-C4)

Benzene (71-43-2)

ACGIH: 0.5 ppm (TWA); NIOSH: 0.1 ppm (TWA); OSHA 1 ppm (TWA)

Toluene (108-88-3)

ACGIH: 20 ppm TWA (listed under Toluene)

m-, o-, p-Xylene (1330-20-7)

ACGIH: 100 ppm TWA (listed under Xylene o, m & p isomers)

Engineering Measures

Use adequate ventilation to keep vapor concentrations of this product below occupational exposure and flammability limits, particularly in confined spaces. Use explosion-proof equipment and lighting in classified / controlled areas.

Personal Protective Equipment: Respiratory

Use a NIOSH-approved positive-pressure, supplied air respirator with escape bottle or self-contained breathing apparatus (SCBA) for gas concentrations above occupational exposure limits, for potential for uncontrolled release, if exposure levels are not known, or in an oxygen-deficient atmosphere (oxygen content less than 19.5 percent). A respiratory program that meets or is equivalent to OSHA 29 CFR 1910.134 and ANSI Z88.2 should be followed whenever workplace conditions warrant the use of a respirator.

If benzene concentrations equal or exceed applicable exposure limits, OSHA requirements for personal protective equipment, exposure monitoring, and training may apply (29 CFR 1910.1028 – Benzene).

CAUTION: Flammability limits (i.e., explosion hazard should be considered when assessing the need to expose personnel to concentrations requiring respiratory protection.

Personal Protective Equipment: Hands

Gloves constructed of nitrile or neoprene are recommended.

Personal Protective Equipment: Eyes

Safety glasses or goggles are recommended where there is a possibility of splashing or spraying. Eye protection that meets or exceeds ANSI Z.87.1 is recommended. Depending on conditions of use, a face shield may be necessary.

Personal Protective Equipment: Skin and Body

Chemical protective clothing such as of E.I. DuPont TyChem®, Saranex® or equivalent recommended based on degree of exposure. Note: The resistance of specific material may vary from product to product as well as with degree of exposure. Consult manufacturer specifications for further information.

Hygiene Measures

Emergency eye wash capability should be available in the near proximity to operations presenting a potential splash exposure. Use good personal hygiene practices. Avoid repeated and/or prolonged skin exposure. Wash hands before eating, drinking, smoking, or using toilet facilities. Do not use as a cleaning solvent on the skin. Do not use gasoline or solvents (naphtha, kerosene, etc.) for washing this product from

exposed skin areas. Waterless hand cleaners are effective. Promptly remove contaminated clothing and launder before reuse. Use care when laundering to prevent the formation of flammable vapors which could ignite via washer or dryer. Consider the need to discard contaminated leather shoes and gloves.

* * * Section 9 – PHYSICAL AND CHEMICAL PROPERTIES * * *

Appearance:	Colorless to straw yellow	**Odor:**	Aromatic, Gasoline;
Physical State:	Liquid	**pH:**	ND
Vapor Pressure:	110 – 200 psia (Reid VP) @ 100°F/37.8°C	**Vapor Density (air = 1):**	> 1
Boiling Point:	Approx. 85 - 437°F (39 – 200°C)	**Melting Point:**	ND
Solubility (H2O):	Insoluble to slightly soluble	**Specific Gravity:**	AP 0.62-0.76 (varies)
Evaporation Rate:	High	**VOC:**	ND
Octanol / H2O Coeff.:	ND	**Flash Point:**	-40°F -40°C
Flash Point Method:	Tag Closed Cup (TCC)		
Lower Flammability Limit: (LFL):	ND (NFPA Gasoline 1.4)	**Upper Flammability Limit: (UFL):**	ND (NFPA Gasoline 7.6)
Auto Ignition:	AP 480°F (250°C)	**Burning Rate:**	ND

* * * Section 10 – CHEMICAL STABILITY & REACTIVITY INFORMATION * * *

Chemical Stability

This is a stable material.

Hazardous Reaction Potential

Will not occur.

Conditions to Avoid

Keep away from ignition sources and high temperatures.

Hazardous Decomposition Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

* * * Section 11 – TOXICOLOGICAL INFORMATION * * *

Acute Toxicity

A: General Product Information

Harmful if swallowed.

B. Component Analysis – LD50/LC50

Octanes (111-65-9)
Inhalation LC50 rat = 118,000 mg/m3 / 4H

Heptanes (142-82-5)
Inhalation LC50 rat = 103,000 mg/m3 / 4H

Hexanes as n-Hexane (110-53-3)
Inhalation LC50 rat = 48,000 ppm / 4H

Pentanes as n-Pentane (109-66-0)
Inhalation LC50 rat = 364,000 mg/m3 / 4H

Butanes as n-Butane (106-97-8)
Inhalation LC50 rat 658,000 mg/l / 4H

Propane (74-98-6)
Inhalation LC50 Rat > 800,000 ppm / 0.25H

Ethane (74-84-0)
Inhalation LC50 Rat 658,000 mg/l / 4H

Benzene (71-43-2)
Inhalation LC50 Rat 44,700 mg/m3 /

Toluene (108-88-3)
Inhalation LD50 Rat 12/5 mg/l / 4H

m-, o-, p-Xylene (1330-20-7)
Inhalation LC50 Rat 5000 ppm / 4H

Potential Health Effects: Skin Corrosion Property / Stimulativeness

May cause skin irritation with prolonged or repeated contact. Liquid may be absorbed through the skin in toxic amounts if large areas of skin are exposed repeatedly.

Potential Health Effects: Eye Critical Damage / Stimulativeness

Contact with eyes may cause moderate irritation.

Potential Health Effects: Ingestion (swallowing)

Ingestion may cause gastrointestinal disturbances, including irritation, nausea, vomiting and diarrhea, and central nervous system (brain) effects similar to alcohol intoxication. In severe cases, tremors, convulsions, loss of consciousness, coma, respiratory arrest, and death may occur.

Potential Health Effects: Inhalation (breathing)

Excessive exposure may cause irritations to the nose, throat, lungs and respiratory tract. Central nervous system (brain) effects may include headache, dizziness, loss of balance and coordination, unconsciousness, coma, respiratory failure, and death.

Respiratory Organs Sensitization / Skin Sensitization

This product is not reported to have any skin sensitization effects.

Generative Cell Mutagenicity

May cause genetic defects. Some crude oils and crude oil fractions have been positive in mutagenicity studies.

Carcinogenicity

A: General Product Information

May cause cancer.

This product contains benzene, although at very low concentrations. Human health studies indicate that prolonged and/or repeated overexposure to benzene may cause damage to the blood-forming system (particularly bone marrow), and serious blood disorders such as aplastic anemia and leukemia. Benzene is listed as a human carcinogen by the NTP, IARC, OSHA and ACGIH.

Exposure to light hydrocarbons in the same boiling range as this product have been associated in animal studies with effects to the central nervous system, peripheral nervous system, liver, and kidneys. The significance of these animal models to predict similar human response is uncertain. Observing good work practices and personal hygiene procedures (Sections 7 and 8) can minimize potential risks to humans.

B: Component Carcinogenicity

Benzene (71-43-2)

ACGIH:	A1 - Confirmed Human Carcinogen
OSHA:	5 ppm STEL (Cancer hazard, Flammable, See 29 CFR 1910.1028, 15 min); 0.5 ppm Action Level; 1 ppm TWA
NIOSH:	potential occupational carcinogen
NTP:	Known Human Carcinogen (Select Carcinogen)

IARC: Monograph 100F [in preparation]; Supplement 7 [1987]; Monograph 29 [1982] (Group 1 (carcinogenic to humans))

Reproductive Toxicity

This product is not reported to have any reproductive toxicity effects.

Specified Target Organ General Toxicity: Single Exposure

This product is not reported to have any specific target organ general toxicity single exposure effects.

Specified Target Organ General Toxicity: Repeated Exposure

May cause damage to organs (liver, kidneys, blood, nervous system and skin) through prolonged or repeated exposure.

Aspiration Respiratory Organs Hazard

The major health threat of ingestion occurs from the danger of aspiration (breathing) of liquid drops into the lungs, particularly from vomiting. Aspiration may result in chemical pneumonia (fluid in the lungs), severe lung damage, respiratory failure and even death.

* * * Section 12 – ECOLOGICAL INFORMATION * * *

Ecotoxicity

A: General Product Information

Keep out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

B: Component Analysis – Ecotoxicity – Aquatic Toxicity

Benzene (71-43-2)

Test and Species	Conditions
96 Hr LC50 Pimephales promelas	10.7-14.7 mg/L [flow-through]
96 Hr LC50 Oncorhynchus mykiss	5.3 mg/L [flow-through]
96 Hr LC50 Lepomis macrochirus	22.49 mg/L [static]
96 Hr LC50 Poecilia reticulata	28.6 mg/L [static]
96 Hr LC50 Pimephales promelas	22330-41160 µg/L [static]
96 Hr LC50 Lepomis macrochirus	70000-142000 µg/L [static]
72 Hr EC50 Pseudokirchneriella subcapitata	29 mg/L
48 Hr EC50 Daphnia magna	8.76 - 15.6 mg/L [static]
48 Hr EC50 Daphnia magna	10 mg/L

Natural Gas condensates (68919-39-1)

Test and Species	Conditions
96 Hr LC50 Alburnus alburnus	119 mg/L [static]
96 Hr LC50 Cyprinodon variegatus	82 mg/L [static]
72 Hr EC50 Pseudokirchneriella subcapitata	56 mg/L
24 Hr EC50 Daphnia magna	170 mg/L

Persistence / Degradability

No information available

Bioaccumulation

No information available

Mobility in Soil

No information available

* * * Section 13 – DISPOSAL CONSIDERATIONS * * *

Waste Disposal Instructions

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

Disposal of Contaminated Containers or Packaging

Recover or recycle if possible. It is the responsibility of the generator to determine the toxicity and physical properties of the material generated so as to properly classify the waste and ensure disposal methods comply with applicable regulations.
This material, if discarded should be fully characterized for ignitability (D001), reactivity (D003) and benzene (D018) prior to disposal (40 CFR261). Use which results in chemical or physical change or contamination may subject it to regulation as a hazardous waste. Along with properly characterizing all waste materials, consult state and local regulations regarding the proper disposal of this material. Do not dispose of by draining onto the ground. This will result in soil and groundwater contamination. Waste arising from spillage or tank cleaning should be disposed of in accordance with applicable regulations.

Container contents should be completely used and containers should be emptied prior to discard. Container rinsate could be considered a RCRA hazardous waste and must be disposed of with care and in full compliance with federal, state and local regulations. Larger empty containers, such as drums, should be returned to the distributor or to a qualified drum reconditioner. To assure proper disposal of smaller empty containers, consult with state and local regulations and disposal authorities.

* * * Section 14 – TRANSPORTATION INFORMATION * * *

DOT Information

Shipping Name: Petroleum Products, n.o.s. (condensate)

UN #: 1268 **Hazard Class:** 3

Additional Info.: Dependent on the product's properties, the shipper may also elect to classify as Gasoline UN1203 or Petroleum Crude Oil UN1267 - reference 49 CFR 172.101 for further description (e.g., packing group determination).

Placard:

* * * Section 15 – REGULATORY INFORMATION * * *

Regulatory Information

Component Analysis

This material contains one or more of the following chemicals required to be identified under SARA Section 302 (40 CFR 355 Appendix A), SARA Section 313 (40 CFR 372.65) and/or CERCLA (40 CFR 302.4).

Benzene (71-43-2)

SARA 313: 0.1% de minimis concentration

CERCLA: 10 lb final RQ (received an adjusted RQ of 10 lbs based on potential carcinogenicity in an August 14, 1989 final rule); 4.54 kg final RQ (received an adjusted RQ of 10 lbs based on potential carcinogenicity in an August 14, 1989 final rule)

SARA Section 311/312 – Hazard Classes

Acute Health	Chronic Health	Fire	Sudden Release of Pressure	Reactive
X	X	X	--	--

SARA SECTION 313 – SUPPLIER NOTIFICATION

This product contains the following toxic chemicals subject to the reporting requirements of section 313 of the Emergency Planning and Community Right-To-Know Act (EPCRA) of 1986 and of 40 CFR 372:

INGREDIENT NAME (CAS NUMBER)	CONCENTRATION PERCENT BY WEIGHT
Benzene (71-43-2)	<0.1 to 2

Canadian Regulatory Information

DSL/NDSL Inventory	This product has been classified in accordance with the hazard criteria of the Controlled Products Regulations (CPR) and the SDS contains all the information required by the Regulations.
Workplace Hazardous Materials Information System	B2 - Flammable Liquid D1A – Material Causing Immediate and Serious Toxic Effects - Very Toxic Material D2A: Material Causing Other Toxic Effects Very Toxic D2B - Material Causing Other Toxic Effects - Toxic Material

European Union Regulatory Information

Labeling	Product is dangerous as defined by the European Union Dangerous Substances / Preparations Directives. Contains: Low Boiling Point Naphtha
Symbol	**F+** Extremely Flammable **T** Toxic **N** Dangerous for the Environment
Risk Phrases	R12-45-38-65-67-51/53 Extremely flammable. May cause cancer. Irritating to skin. Harmful: may cause lung damage if swallowed. Vapors may cause drowsiness and dizziness. Toxic to aquatic organisms, may cause long-term adverse effects in the aquatic environment.
Safety Phrases	S16-53-45-2-23-24-29-43-62 Keep away from sources of ignition – No smoking. Avoid exposure – obtain special instructions before use. In case of accident or if you feel unwell, seek medical advice immediately (show the label where possible). Keep out of reach of children. Do not breathe vapor. Avoid contact with skin. Do not empty into drains. In case of fire use foam/dry powder/CO2. If swallowed, do not induce vomiting: seek medical advice immediately and show this container or label.

State Regulations

Component Analysis – State

The following components appear on one or more of the following state hazardous substances lists

Component	CAS	CA	MA	MN	NJ	PA	RI
Octanes	111-65-9	Yes	No	Yes	Yes	Yes	Yes
Heptanes	142-82-5	Yes	No	Yes	Yes	Yes	Yes
n-Hexane	110-54-3	Yes	Yes	Yes	Yes	Yes	Yes
n-Pentane	109-66-0	Yes	No	Yes	Yes	Yes	Yes
n-Butane	106-97-8	Yes	No	Yes	Yes	Yes	Yes
Propane	74-98-6	No	No	Yes	Yes	Yes	Yes
Ethane	78-84-0	No	No	Yes	Yes	Yes	No
Benzene	71-43-2	Yes	Yes	Yes	Yes	Yes	Yes
Toluene	108-88-3	Yes	Yes	Yes	Yes	Yes	Yes
m-, o-, p-Xylene	1330-20-7	Yes	Yes	Yes	Yes	Yes	Yes

The following statement(s) are provided under the California Safe Drinking Water and Toxic Enforcement Act of 1986 (Proposition 65):

WARNING! This product contains a chemical known to the state of California to cause cancer.

WARNING! This product contains a chemical known to the state of California to cause Reproductive / developmental effects.

Component Analysis – WHMIS IDL

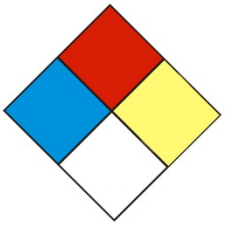
The following components are identified under the Canadian Hazardous Products Act Ingredient Disclosure List:

Component	CAS #	Minimum Concentration
Benzene	71-43-2	0.1%

* * * Section 16 – OTHER INFORMATION * * *

NFPA® Hazard Rating

Health 1
Fire 4
Reactivity 0



HMIS® Hazard Rating

Health	1	Slight
Fire	4	Severe
Physical	0	Minimal
		* Chronic

Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act: ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

Literature References

None

Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: January 29, 2014

Date of Last Revision: March 4, 2014

End of Sheet

SAFETY DATA SHEET

Material Name: Produced Water **US GHS**

SYNONYMS: **Produced Brine Water, Brine, Brine Water, Formation Water**

* * * Section 1 – PRODUCT AND COMPANY IDENTIFICATION * * *

PRODUCT NAME: **Produced Water**
PRODUCT CODES: **Mixture**

EMERGENCY PHONE: **(800) 878-1373**
AFTER HOURS: **(800) 878-1373**

PRODUCER: **Antero Resources**
ADDRESS: **1615 Wynkoop Street**
Denver, Colorado 80202

CHEMTREC PHONE: **(800) 424-9300**

* * * Section 2 – HAZARDS IDENTIFICATION * * *

GHS Classification:

Eye Irritant – Category 2A.

GHS LABEL ELEMENTS
Symbol(s)

Signal Word

Warning

Hazard Statements

Causes serious eye irritation

Precautionary Statements

Prevention

Wear protective gloves/protective clothing/eye protection/face protection.

Response

If on SKIN (or hair): Rinse skin with water / shower. Remove / Take off all contaminated clothing immediately.

If in EYES: Rinse cautiously with water for at least fifteen (15) minutes. Remove Contact Lenses, if present and easy to do. Continue rinsing.

If EYE irritation persists, get medical advice / attention.

Storage
Store in a secure area.

Disposal
Dispose of contents/containers in accordance with regulations.

* * * Section 3 – COMPOSITION / INFORMATION ON INGREDIENTS * * *

CAS #	Component	Percent
7732-18-5	Water	80
7647-14-5	Sodium Chloride	20

Because brine water is a natural product, composition can vary greatly.

* * * Section 4 – FIRST AID MEASURES * * *

First Aid: Eyes
Flush eyes with clean running water for at least fifteen (15) minutes. If irritation or redness develops from exposure, following flushing, seek medical attention.

First Aid: Skin
First aid is not required, normally. However, it is a good practice to wash any chemical from the skin.

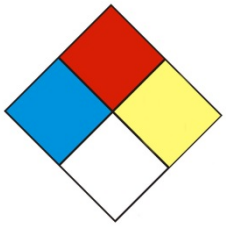
First Aid: Ingestion (Swallowing)
First aid is not required, normally. If spontaneous vomiting occurs, lean the victim forward to reduce the risk of aspiration. Monitor for breathing difficulties. If symptoms develop, seek medical attention.

First Aid: Inhalation (Breathing)
Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

Most important symptoms and effects

None known or anticipated.

* * * Section 5 – FIRE FIGHTING MEASURES * * *



NFPA 704 Hazard Class

Health: 1 Flammability: 0 Instability: 0 (0=Minimal, 1=Slight, 2=Moderate, 3=Serious, 4=Severe)

General Fire Hazards

No fire hazards are expected.

General Fire Hazards

No unusual fire or explosion hazards are expected. If container is not properly cooled, it can rupture in the heat of a fire.

Extinguishing Media

The material is non-flammable. Use extinguishing agent suitable for the type of surrounding fire.

Unsuitable Extinguishing Media

None

Fire Fighting Equipment / Instructions

Small fires in the beginning stage may typically be extinguished using handheld portable fire extinguishers and other firefighting equipment. Isolate area around container involved in fire and keep unauthorized personnel out. Stop spill/release if it can be done safely. Move undamaged containers from the immediate hazard area if it can be done safely. Cool equipment exposed to fire with water, if it can be done safely.

Hazardous Combustion Products

None Anticipated. See Section 9 for Flammable Properties including Flash Point and Flammable (Explosive) Limits

* * * Section 6 – ACCIDENTAL RELEASE MEASURES * * *

Recovery and Neutralization

Contain and stop the source of the spill, if safe to do so.

Materials and Methods for Clean-Up

Notify relevant authorities in accordance with all applicable regulations. Immediate cleanup of any spill is recommended. Dike far ahead of spill for later recovery or disposal. Absorb spill with inert material such as sand or vermiculite, and place in suitable container for disposal. If spilled on water remove with appropriate methods (e.g. skimming, booms or absorbents). In case of soil contamination, remove contaminated soil for remediation or disposal, in accordance with local regulations.

Recommended measures are based on the most likely spillage scenarios of this material. However, local conditions and regulations may influence or limit the choice of appropriate actions to be taken. See Section 13 for information on appropriate disposal.

Emergency Measures

The material is not considered hazardous. Nevertheless, evacuate nonessential personnel and secure the area. Stay upwind and uphill, if possible.

Personal Precautions and Protective Equipment

Stay upwind and away from the spill/release. Avoid direct contact with the material. For large spillages, notify persons downstream of the spill/release. Isolate the immediate hazard area and keep unauthorized personnel out. Response and clean-up crews must be properly trained and must utilize proper protective equipment (see Section 8).

Environmental Precautions

Protect bodies of water by diking or absorbents, if possible. Do not flush down sewer or drainage systems. Use water sparingly to minimize environmental contamination and reduce disposal requirements. If a spill occurs on water, notify appropriate authorities and advise shipping of any hazard.

Prevention of Secondary Hazards

None

* * * Section 7 – HANDLING AND STORAGE * * *

Handling Procedures

Wash thoroughly after handling. Use good personal hygiene practices and wear appropriate personal protective equipment (see section 8).

Do not enter confined spaces such as tanks or pits without following proper entry procedures such as ASTM D-4276 and 29 CFR 1910.146. Do not wear contaminated clothing or shoes.

Storage Procedures

Keep container(s) tightly closed and properly labeled. Use and store this material in cool, dry, well ventilated areas. Store only in approved containers. Keep away from any incompatible material (see Section 10). Protect container(s) against physical damage.

Incompatibilities

Keep away from excessive heat to prevent rupture of container.

* * * Section 8 – EXPOSURE CONTROLS / PERSONAL PROTECTION * * *

Component Exposure Limits

Water (7732-18-5)

ACGIH: Not listed

Sodium Chloride (7647-14-5)

ACGIH: Not listed

Engineering Measures

If current ventilation practices are not adequate to maintain airborne concentrations below the established exposure limits, additional engineering controls may be required.

Personal Protective Equipment: Respiratory

Emergencies or conditions that could result in significant airborne exposures may require the use of NIOSH approved respiratory protection. An industrial hygienist or other appropriate health and safety professional should be consulted for specific guidance under these situations.

A respiratory protection program that meets or is equivalent to OSHA 29 CFR

1910.134 and ANSI Z88.2 should be followed whenever workplace conditions warrant a respirator's use.

Personal Protective Equipment: Skin and Hands

The use of skin protection is not normally required; however, good industrial hygiene practice suggests the use of gloves or other appropriate skin protection whenever working with chemicals.

Personal Protective Equipment: Eyes

Safety glasses or goggles that meet or exceed ANSI Z-87.1 are recommended where there is a possibility of splashing or spraying.

Hygiene Measures

Emergency eye wash capability should be available in the near proximity to operations presenting a potential splash exposure. Use good personal hygiene practices. Avoid repeated and/or prolonged skin exposure. Wash hands before eating, drinking, smoking, or using toilet facilities. Promptly remove contaminated clothing and launder before reuse.

* * * Section 9 – PHYSICAL AND CHEMICAL PROPERTIES * * *

Appearance:	Clear to Brown	**Odor:**	Salty
Physical State:	Liquid	**pH:**	ND
Vapor Pressure:	< 0.36 psia @ 70°F / 21.1°C	**Vapor Density:**	> 1
Boiling Point:	212°F / 100°C	**Melting Point:**	2.4°F / -16.5°C
Solubility (H2O):	Complete	**Specific Gravity:**	1.1 @ 68°F / 20°C
Evaporation Rate:	Variable	**VOC:**	ND
Octanol / H2O Coeff.:	ND	**Flash Point:**	ND
Flash Point Method:	ND		
Lower Flammability Limit: (LFL):	ND	**Upper Flammability Limit: (UFL):**	ND
Auto Ignition:	ND	**Burning Rate:**	ND

* * * Section 10 – CHEMICAL STABILITY & REACTIVITY INFORMATION * * *

Chemical Stability

This is a stable material.

Hazardous Reaction Potential

Will react with alkali and alkaline metals to form flammable hydrogen gas.

Conditions to Avoid

Avoid contact with alkali metals (lithium, sodium, potassium), alkaline metals (beryllium, magnesium, calcium, strontium, and barium), and metallic hydrides like lithium aluminum hydride.

Hazardous Decomposition Products

Not anticipated under normal conditions of use.

Hazardous Polymerization

Not known to occur.

* * * Section 11 – TOXICOLOGICAL INFORMATION * * *

Acute Toxicity

A: General Product Information

Unlikely to be harmful.

B. Component Analysis – D50/LC50

Water (7732-18-5)

Oral LD50 Rat 90 g/kg

Sodium Chloride (7647-14-5)

Oral LD50 Rat 3 g/kg

Potential Health Effects: Skin Corrosion Property / Stimulativeness

May cause skin irritation with prolonged or repeated contact. Not expected to be a skin sensitizer.

Potential Health Effects: Eye Critical Damage / Stimulativeness

Contact with eyes may cause moderate irritation.

Potential Health Effects: Ingestion

Ingestion may result in nausea, vomiting, diarrhea, abdominal cramps, and dehydration (thirst).

Potential Health Effects: Inhalation

No information available on the mixture. However, none of the components have been classified for respiratory sensitization (or are below the concentration threshold for classification).

Generative Cell Mutagenicity

Not expected to cause genetic effects.

Carcinogenicity

General Product Information

Not expected to cause cancer. This substance is not listed as a carcinogen by IARC, NTP or OSHA.

Reproductive Toxicity

This product is not reported to have any reproductive toxicity effects.

Specified Target Organ General Toxicity: Single Exposure

This product is not reported to have any specific target organ general toxicity single exposure effects.

Specified Target Organ General Toxicity: Repeated Exposure

This product is not reported to have any specific target organ general toxicity multiple exposure effects.

Aspiration Respiratory Organs Hazard

The major health threat of ingestion occurs from the danger of aspiration (breathing) of liquid drops into the lungs, particularly from vomiting. Aspiration may result in chemical pneumonia (fluid in the lungs), severe lung damage, respiratory failure and even death.

* * * Section 12 – ECOLOGICAL INFORMATION * * *

Ecotoxicity

A: General Product Information

Keep out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

Persistence / Degradability

No information available

Bioaccumulation

No information available

Mobility in Soil

No information available

* * * Section 13 – DISPOSAL CONSIDERATIONS * * *

Waste Disposal Instructions

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

Disposal of Contaminated Containers or Packaging

Recover or recycle if possible. It is the responsibility of the generator to determine the toxicity and physical properties of the material generated so as to properly classify the waste and ensure disposal methods comply with applicable regulations.

This material, if discarded as produced, is not a RCRA "listed" hazardous waste, and is not believed to exhibit characteristics of hazardous waste. Consult state and local regulations regarding the proper disposal of this material. Do not dispose of brine water by draining onto the ground. This will result in soil and groundwater contamination. Waste arising from spillage or tank cleaning should be disposed of in accordance with applicable regulations.

Container contents should be completely used and containers should be emptied prior to discard. Container rinsate should not be considered a RCRA hazardous waste but must be disposed of with care and in full compliance with federal, state and local regulations. Larger empty containers, such as drums, should be returned to the distributor or to a qualified drum reconditioner. To assure proper disposal of smaller empty containers, consult with state and local regulations and disposal authorities.

* * * Section 14 – TRANSPORTATION INFORMATION * * *

DOT Information

Shipping Description: Not Regulated

UN #: Not Regulated

* * * Section 15 – REGULATORY INFORMATION * * *

CERCLA/SARA – Section 302 Extremely Hazardous Substances and TPQs (in pounds):
This material does not contain any chemicals subject to the reporting requirements of SARA 302 and 40 CFR 372,

CERCLA/SARA – Section 313 and 40 CFR 372):
This material does not contain any chemicals subject to the reporting requirements of SARA 313 and 40 CFR 372.

EPA (CERCLA) Reportable Quantity (in pounds):
This material does not contain any chemicals with CERCLA Reportable Quantities.

State Regulations

Component Analysis

The following components appear on one or more of the following state hazardous substances list.

California Proposition 65:
This material does not contain any chemicals that are known to the State of California to cause cancer, birth defects or other reproductive harm at concentrations that trigger the warning requirements of California Proposition 65.

National Chemical Inventories:
All components are either listed on the US TSCA Inventory, or are not regulated under TSCA.

U.S. Export control classification Number: EAR99.

* * * Section 16 – OTHER INFORMATION * * *

NFPA® Hazard Rating

Health	1
Fire	0
Reactivity	0

HMIS® Hazard Rating

Health	1	Slight
Fire	0	Minimal
Physical	0	Minimal

Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act: ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

Literature References

None

Other Information

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Date of Preparation: January 28, 2014

Date of Last Revision: March 4, 2014

End of Sheet

Attachment O

Emissions Summary Sheet

Attachment O: G70-A Emissions Summary Sheet

Emission Points Data Summary Sheet

Table 1: Emissions Data												
Emission Point ID No. *(Must match Emission Units Table & Plot Plan)*	Emission Point Type[1]	Emission Unit Vented Through This Point *(Must match Emission Units Table & Plot Plan)*		Air Pollution Control Device *(Must match Emission Units Table & Plot Plan)*		All Regulated Pollutants - Chemical Name/CAS[3] *(Speciate VOCs & HAPS)*	Maximum Potential Uncontrolled Emissions [4]		Maximum Potential Controlled Emissions [5]		Emission Form or Phase *(At exit conditions, Solid, Liquid or Gas/Vapor)*	Est. Method Used [6]
		ID No.	Source	ID No.	Device Type		lb/hr	ton/yr	lb/hr	ton/yr		
EP-H001, EP-H002, EP-H003, EP-H004, EP-H005, EP-H006, EP-H007, EP-H008	Vertical Stack	H001, H002, H003, H004, H005, H006, H007, H008	Gas Production Heaters	N/A		CO (630080)	0.8083	3.5404	0.8083	3.5404	Gas/Vapor /Solid (for PM)	MB AP-42
						NOx (10102439)	0.9623	4.2147	0.9623	4.2147		
						Pb (7439-92-1)	4.81E-06	2.11E-05	4.81E-06	2.11E-05		
						CO2 Equivalent N2O (10024972), CO2 (124389), CH4 (74828)	1161.5778	5087.7107	1161.5778	5087.7107		
						SO2 (7446095)	5.77E-03	0.0253	5.77E-03	0.0253		
						PM, PM10, PM2.5	0.0731	0.3203	0.0731	0.3203		
						Benzene (71432)	2.02E-05	8.85E-05	2.02E-05	8.85E-05		
						Toluene (108883)	3.27E-05	1.43E-04	3.27E-05	1.43E-04		
						Hexane (110543)	0.0173	0.0759	0.0173	0.0759		
						Formaldehyde (50000)	7.22E-04	3.16E-03	7.22E-04	3.16E-03		
						2-Methylnaphthalene (91576)	2.31E-07	1.01E-06	2.31E-07	1.01E-06		
						Dichlorobenzene (95501)	1.15E-05	5.06E-05	1.15E-05	5.06E-05		
						Fluoranthene (206440)	2.89E-08	1.26E-07	2.89E-08	1.26E-07		
						Fluorene (86737)	2.69E-08	1.18E-07	2.69E-08	1.18E-07		
						Naphthalene (91203)	5.87E-06	2.57E-05	5.87E-06	2.57E-05		
						Phenanathrene (85018)	1.64E-07	7.17E-07	1.64E-07	7.17E-07		
						Total VOCs	0.0529	0.2318	0.0529	0.2318		
F001	n/a	F001	Fugitives	N/A		Benzene (71432)	5.22E-03	0.0229	5.22E-03	0.0229	Gas/Vapor	MB
						Toluene (108883)	1.62E-02	0.0709	1.62E-02	0.0709		
						Ethyl benzene (100414)	0.0128	0.0560	0.0128	0.0560		
						Hexane (110543)	0.2191	0.9596	0.2191	0.9596		
						o,m,p-xylenes (95476,108383,106423)	0.0393	0.1723	0.0393	0.1723		
						CO2 Equivalent CO2 (124389)), CH4	64.5797	282.8590	64.5797	282.8590		
						VOCs	3.0422	13.3250	3.0422	13.3250		
						TAPs (benzene)	5.22E-03	0.0229	5.22E-03	0.0229		

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Emission Point ID No. *(Must match Emission Units Table & Plot Plan)*	Emission Point Type[1]	Emission Unit Vented Through This Point *(Must match Emission Units Table & Plot Plan)*		Air Pollution Control Device *(Must match Emission Units Table & Plot Plan)*		All Regulated Pollutants - Chemical Name/CAS[3] *(Speciate VOCs & HAPS)*	Maximum Potential Uncontrolled Emissions [4]		Maximum Potential Controlled Emissions [5]		Emission Form or Phase *(At exit conditions, Solid, Liquid or Gas/Vapor)*	Est. Method Used [6]
		ID No.	Source	ID No.	Device Type		lb/hr	ton/yr	lb/hr	ton/yr		
EP-L001, EP-L002	n/a	L001, L002	Loading (Condensate), Loading (Water)	N/A		VOCs	8.6819	5.2868	8.6819	5.2868	Gas/Vapor	MB
						toluene (108883)	1.28E-03	7.83E-04	1.28E-03	7.83E-04		
						ethyl benzene (100414)	6.34E-04	3.86E-04	6.34E-04	3.86E-04		
						hexane (110543)	0.0203	0.0123	0.0203	0.0123		
						o,m,p-xylenes (95476,108383,106423)	1.87E-03	1.14E-03	1.87E-03	1.14E-03		
						CO2 Equivalent CO2 (124389), CH4	3.0944	4.7720	3.0944	4.7720		
						benzene (71432)	6.84E-04	4.25E-04	6.84E-04	4.25E-04		
						TAPs (benzene)	6.84E-04	4.25E-04	6.84E-04	4.25E-04		
EP-HR001	n/a	HR001	Haul Truck	N/A		PM, PM10, PM2.5	4.6795	11.7405	2.3397	5.8702	Solid	MB
EP-EC001, EP-EC002	n/a	TANKCOND001-010, TANKPW001-002, EC001, EC002	Condensate Tank F/W/B, PW Tank F/W/B, Enclosed Combustor	N/A	Enclosed Combustor	CO (630080)	0.00E+00	0.00E+00	0.2802	1.2273	Gas/Vapor/ Solid (for PM)	MB
						NOx (10102439)	0.00E+00	0.00E+00	0.3336	1.4611		
						Pb (7439-92-1)	0.00E+00	0.00E+00	1.67E-06	7.31E-06		
						CO2 Equivalent N2O (10024972), CO2 (124389), CH4	0.00E+00	0.0000	1359.8315	5956.0619		
						SO2 (7446095)	0.00E+00	0.00E+00	1.51E-05	6.62E-05		
						PM, PM10, PM2.5	0.00E+00	0.00E+00	0.0254	3.52E-05		
						Benzene (71432)	0.3933	1.7225	7.87E-03	0.0344		
						Toluene (108883)	0.3422	1.4987	6.84E-03	0.0300		
						ethyl benzene (100414)	0.0912	8.4558	1.82E-03	0.1691		
						hexane (110543)	8.5046	37.2501	0.1701	0.7450		
						o,m,p-xylenes (95476,108383,106423)	0.2237	0.9797	4.47E-03	0.0196		
						Formaldehyde (50000)	0.00E+00	0.00E+00	1.89E-06	8.28E-06		
						VOCs	253.0431	1108.3288	5.0610	22.1672		
EP-PCV	valve	PCV	Pneumatic CV	N/A		hexane (110543)	1.09E-02	0.0477	1.09E-02	0.0477	Gas/Vapor	MB
						CO2 Equivalent CO2 (124389)), CH4	7.2262	31.6506	7.2262	31.6506		
						VOCs	0.0916	0.4012	0.0916	0.4012		

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		ID No.	Source	ID No.	Device Type		lb/hr	ton/yr	lb/hr	ton/yr		
EP-ENG001	Vertical Stack	ENG001	Compressor Engine	N/A		CO (630080)	5.6445	24.7228	5.6445	24.7228	Gas/Vapor/ Solid (for PM)	MB
						NOx (10102439)	0.3158	1.3831	0.3158	1.3831		
						CO2 Equivalent N2O (10024972), CO2 (124389), CH4 (74828)	27.7765	121.6612	27.7765	121.6612		
						SO2 (7446095)	1.41E-04	6.18E-04	1.41E-04	6.18E-04		
						PM, PM10, PM2.5	2.28E-03	0.0100	2.28E-03	0.0100		
						TAPs Benzene (71432)	3.79E-04	1.66E-03	3.79E-04	1.66E-03		
						Toluene (108883)	1.34E-04	5.86E-04	1.34E-04	5.86E-04		
						TAPs Formaldehyde (50000)	4.92E-03	0.0215	4.92E-03	0.0215		
						Naphthalene (91203)	2.33E-05	1.02E-04	2.33E-05	1.02E-04		
						o,m,p-xylenes (95476,108383,106423)	4.68E-05	2.05E-04	4.68E-05	2.05E-04		
						Total VOCs	7.10E-03	0.0311	7.10E-03	0.0311		

Attachment C/O: G70-A Emissions Summary Sheet

Fugitive Emissions Data Summary Sheet

FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants Chemical Name/CAS [1]	Maximum Potential Uncontrolled Emissions [2]		Maximum Potential Controlled Emissions [3]		Est. Method Used [4]
		lb/hr	ton/yr	lb/hr	ton/yr	
Haul Road/Road Dust Emissions Paved Haul Roads	n/a					
Unpaved Haul Roads	PM, PM10, PM2.5	4.6795	11.7405	2.3397	5.8702	MB
Loading/Unloading Operations	VOCs	8.6819	5.2868	8.6819	5.2868	MB
	toluene (108883)	1.28E-03	7.83E-04	1.28E-03	7.83E-04	
	ethyl benzene (100414)	6.34E-04	3.86E-04	6.34E-04	3.86E-04	
	hexane (110543)	0.0203	0.0123	0.0203	0.0123	
	o,m,p-xylenes (95476,108383,106423)	1.87E-03	1.14E-03	1.87E-03	1.14E-03	
	CO2 Equivalent CO2 (124389), CH4	3.0944	4.7720	3.0944	4.7720	
	benzene (71432)	6.84E-04	4.25E-04	6.84E-04	4.25E-04	
	TAPs (benzene)	6.84E-04	4.25E-04	6.84E-04	4.25E-04	
Equipment Leaks (Components)	Benzene (71432)	Does not apply	0.0229	Does not apply	0.0229	MB
	Toluene (108883)		0.0709		0.0709	
	Ethyl benzene (100414)		0.0560		0.0560	
	Hexane (110543)		0.9596		0.9596	
	o,m,p-xylenes (95476,108383,106423)		0.1723		0.1723	
	CO2 Equivalent CO2 (124389)), CH4		282.8590		282.8590	
	VOCs		13.3250		13.3250	
	TAPs (benzene)		0.0229		0.0229	
Equipment Leaks (PCVs)	hexane (110543)	0.0109	0.0477	0.0109	0.0477	MB
	CO2 Equivalent CO2 (124389)), CH4	7.2262	31.6506	7.2262	31.6506	
	VOCs	0.0916	0.4012	0.0916	0.4012	

[1] List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS_2, VOCs, H_2S, Inorganics, Lead, Organics, O_3, NO, NO_2, SO_2, SO_3, all applicable Greenhouse Gases (including CO_2 and methane), etc. DO NOT LIST H_2, H_2O, N_2, O_2, and Noble Gases.

[2] Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

[3] Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

[4] Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

Attachment P

Other Supporting Documentation
(Engine EPA's Certificate of Conformity and Technical Information)

UNITED STATES ENVIRONMENTAL PROTECTION AGENCY
2013 MODEL YEAR
CERTIFICATE OF CONFORMITY
WITH THE CLEAN AIR ACT OF 1990

OFFICE OF TRANSPORTATION AND AIR QUALITY
ANN ARBOR, MICHIGAN 48105

Certificate Issued To: **Kubota Corporation**
(U.S. Manufacturer or Importer)

Certificate Number: DKBXS.9622HP-002

Effective Date: 11/20/2012

Expiration Date: 12/31/2013

Byron J. Bunker, Division Director
Compliance Division

Issue Date: 11/20/2012

Revision Date: N/A

Manufacturer: Kubota Corporation
Engine Family: DKBXS.9622HP
Certificate Number: DKBXS.9622HP-002
Useful Life : 1000 Hours / 5 Years
Engine Class : Nonhandheld-Class II
Fuel : Natural Gas (CNG/LNG)
Emission Standards : NMHC + NOx (g/kW-hr) : 8
CO (g/kW-hr) : 610

Pursuant to Section 213 of the Clean Air Act (42 U.S.C. section 7547), 40 CFR Part 1054, 40 CFR Part 1068 and 40 CFR Part 60 (stationary only and combined stationary and mobile), and subject to the terms and conditions prescribed in those provisions, this certificate of conformity is hereby issued for the following small nonroad engine family, more fully described in the documentation required by 40 CFR Part 1054 and produced in the stated model year.

This certificate of conformity covers only those new small nonroad engines which conform in all material respects to the design specifications that applied to those engines described in the documentation required by 40 CFR Part 1054 and which are produced during the model year stated on this certificate of the said manufacturer, as defined in 40 CFR Part 1054. This certificate of conformity does not cover small nonroad engines imported prior to the effective date of the certificate.

It is a term of this certificate that the manufacturer shall consent to all inspections described in 40 CFR 1068.20 and 1068, Subpart E and authorized in a warrant or court order. Failure to comply with the requirements of such a warrant or court order may lead to revocation or suspension of this certificate for reasons specified in 40 CFR Part 1054. It is also a term of this certificate that this certificate may be revoked or suspended or rendered void *ab initio* for other reasons specified in 40 CFR Part 1054, 40 CFR Part 1068.

This certificate does not cover small nonroad engines sold, offered for sale, or introduced, or delivered for introduction, into commerce in the U.S. prior to the effective date of the certificate.

TECHNICAL INFORMATION

DG972-SAEH-S1

NATURAL GAS FUEL ENGINE

July, 2006

KUBOTA Corporation

CONTENTS

Specifications and dimensions are subject to change without prior notice.

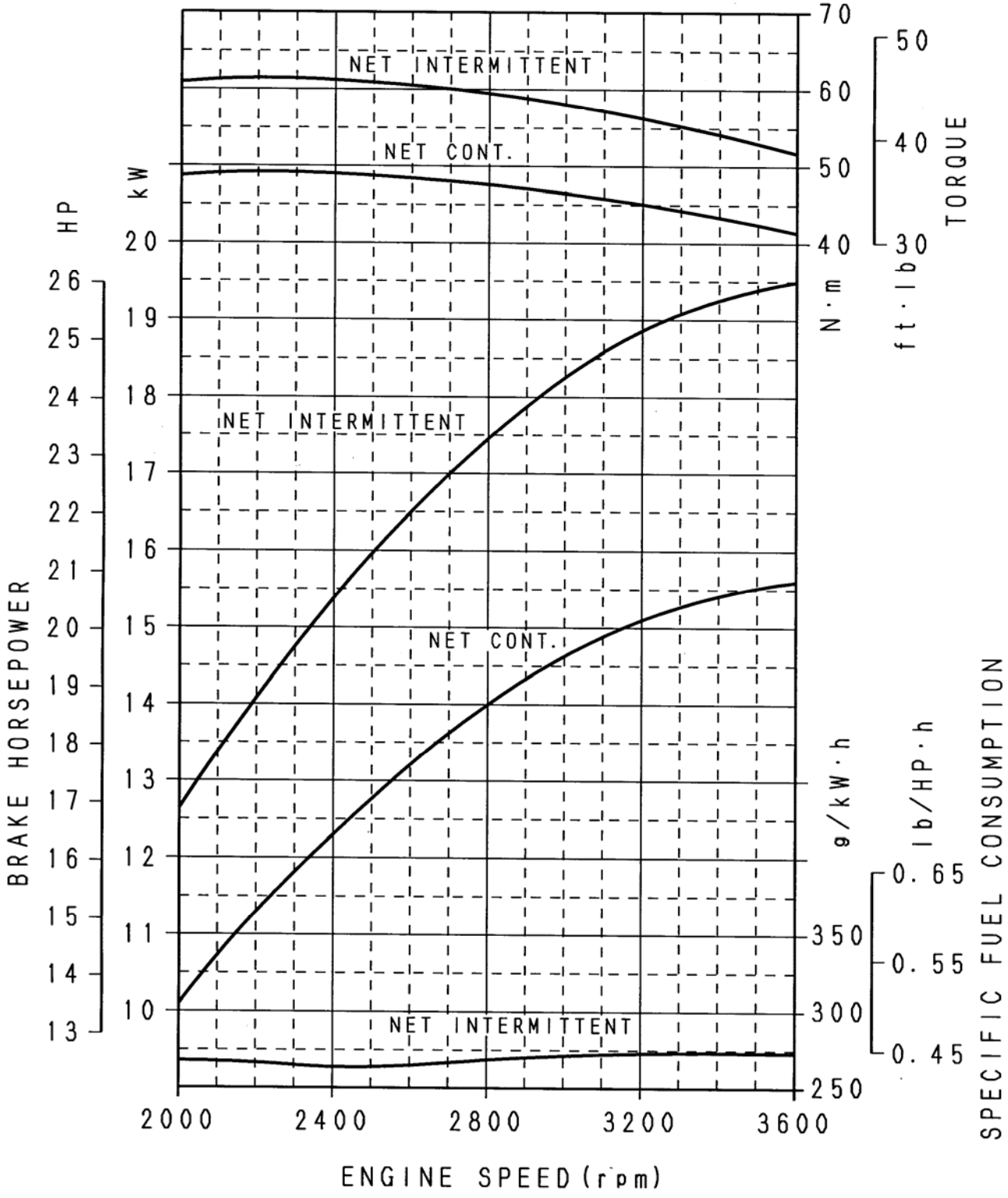
1. GENERAL SPECIFICATIONS

ITEM	UNIT	SPECIFICATIONS
Engine model		DG972-SAEH-S1
Type		Vertical, In line, 4cycle Natural Gas engine
Cooling system		Water cooling with water pump
Number of cylinders		3
Cylinder bore	mm(in)	74.5 (2.93)
Stroke	mm(in)	73.6 (2.90)
Total displacement	L(cu. in)	0.962 (58.7)
High idle	rpm	3850
Low idle	rpm	1500
Horsepower	kW(HP)	19.5(26.1)
Max. torque (SAE J1349)	Nm(ft-lb) /rpm	61.2 (45.2)/2400
Compression ratio		9.2
Firing order		1-2-3
Ignition timing		B.T.D.C.15˚/1000rpm B.T.D.C.28˚/3600rpm
Ignition system		Distributor-less Solid State type
Fuel		Natural Gas only
Direction of rotation		Counter-clockwise from flywheel side
Starting system		Electric starting with cell starter
Starter output	V-kW	12-1.0
Alternator output	V-W	12-480 (Standard)
Lubricating system		Forced lubricating by trochoid pump
Lubricating oil		Quality better than SH class
Lube. oil capacity	L(US gal)	3.4 (0.90)
Coolant capacity	L(US gal)	1.22 (0.32)
Governor type		Centrifugal flyweight mechanical type governor
Dimensions (LxBxH)	mm(in)	526x415x503 (20.7x16.3x19.8)
Dry weight	kg(lb)	Approx. 95.4(210)
Application		Stationary only

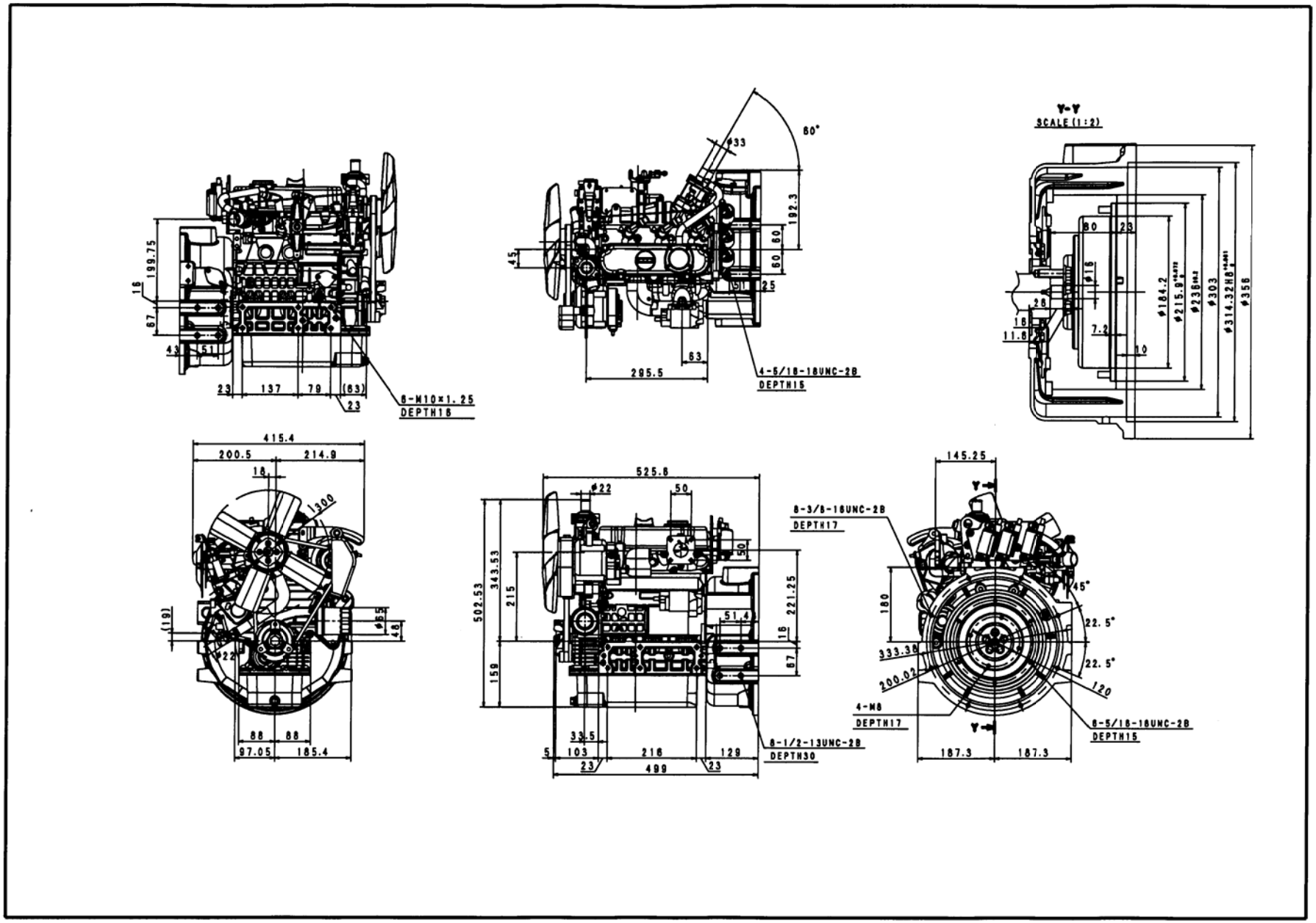
2. PERFORMANCE CURVES

DG972 PERFORMANCE CURVES

Higher calorific value : 11000kcal/m^3 (1236BTU/ft^3)



3. DIMENSIONS



4. TECHNICAL DATA

ITEM		SPECIFICATIONS
Engine model		DG972-SAEH-S1
Brake horse power		See attached sheet 4-1)
Top Clearance		1.35 to 1.65mm (0.05315 to 0.06496in)
Compression pressure		1.32MPa (192psi)
Fuel consumption		See attached sheet 4-2)
Lube. oil consumption		Max.0.67g/kWh (0.5g/HPh) at rated load
Lube. oil pressure		at idling speed: more than 69kPa (more than 9.95psi)
		at rated speed: 196 to 441kPa (28.44 to 63.99psi)
Noise level		See attached sheet 4-3)
Combustion air requirements		See attached sheet (Refer to 25deg.C and 1000hPa) 4-4)
Cooling air requirements		
Combustion and cooling air requirements		
Exhaust gas volume		See attached sheet (Refer to 25deg.C and 1000hPa) 4-5)
Cold starting limits		-15deg.C (5deg.F)
Heat rejection		See attached sheet 4-6)
Angles of tilt	Front or Rear down	30° (Less than 10min. continuous operation)
		20° (Continuous operation)
	Left or Right side down	30° (Less than 10min. continuous operation)
		20° (Continuous operation)
Valve timing		[Inlet valve] Open: TDC –20° Close: BDT +45°
		[Exhaust valve] Open: BDC –50° Close: TDC +15°
Cooling fan data		See attached sheet 4-7)
Center of gravity		See attached sheet 4-8)
Unbalanced forces of engines		See attached sheet 4-9)
Mass elastic system		See attached sheet 4-10)
Thermostat specifications		Opening temperature: 71±1.5deg.C (159.8±2.7deg.F)
		Fully opened temperature: 85deg.C (185deg.F) [at Thermostat lift:8mm (0.31in)]

4-1) BRAKE HORSE POWER

SAE J1349

Engine speed	rpm	2000	2400	2800	3200	3600
Net intermittent	kW	12.6	15.4	17.4	18.9	19.5
	HP	16.9	20.6	23.3	25.3	26.1
	PS	17.1	20.9	23.7	25.7	26.5
Net continuous	kW	10.1	12.3	13.9	15.1	15.6
	HP	13.5	16.5	18.7	20.3	20.9
	PS	13.7	16.8	18.9	20.6	21.2

Note

1. Conversion rates 1kW=1.35962PS=1.34048HP
   1PS=0.7355kW=0.985925HP
   1HP=0.7457kW=1.01428PS
2. Fuel detail Japanese standard gas
   higher calorific value : 11000kcal/m^3 (1236BTU/ft^3)
   supply pressure : 0.98 – 2.45kPa (7.35 – 18.38mmHg)

4-2) FUEL CONSUMPTION

Specific at net intermittent (SAE J1349)

Engine speed	rpm	2000	2400	2800	3200	3600
Brake horse power	kW	12.6	15.4	17.4	18.9	19.5
	HP	16.9	20.6	23.3	25.3	26.1
	PS	17.1	20.9	23.7	25.7	26.5
Fuel consumption	g/kWh	269	264	269	273	273
	g/HPh	200	197	200	204	204
	g/PSh	198	194	198	201	201
	lb/HPh	0.442	0.434	0.442	0.449	0.449

Note

1. Conversion rates 1kW=1.35962PS=1.34048HP 1kg=2.20462lb (1g=0.00220462lb)
   1PS=0.7355kW=0.985925HP 1lb=0.45359kg
   1HP=0.7457kW=1.01428PS
2. Fuel detail Japanese standard gas
   higher calorific value : 11000kcal/m^3 (1236BTU/ft^3)
   supply pressure : 0.98 – 2.45kPa (7.35 – 18.38mmHg)

4-3) NOISE LEVEL

Load × rpm	Unit	Sound pressure at 1m(3.3ft)
0/4 × 3850	dB(A)	90.0
4/4 × 3850 15.6kW (20.9HP)	dB(A)	92.0
0/4 × 1500	dB(A)	72.0

These data show the average noise level at four points.

Note

1. Measurement conditions : With radiator, cooling fan, air cleaner and muffler.

4-4) AIR REQUIREMENTS

1. Combustion air requirements (Refer to 25deg.C and 1000hPa)

rpm	2000	2400	2800	3200	3600
L/sec	12.35	14.81	17.28	19.75	22.22
m^3/h	44.44	53.33	62.22	71.11	80.00
in^3/sec	753	904	1055	1205	1356
ft^3/min	26.13	31.35	36.58	41.80	47.03

Combustion air requirements calculating formula

$Q_1=Vh \bullet N \bullet C \bullet \eta \bullet 10^{-3}$

Q_1: Amount of intake air (m^3/min)
Vh: Total displacement (L)
N: Engine speed (rpm)
C: Coefficient=0.5
η: Intake efficiency
Natural Gas: 0.77

2. Cooling air requirements (Refer to 25deg.C and 1000hPa)

rpm	2000	2400	2800	3200	3600
L/sec	571.2	737.2	824.7	833.9	764.7
m^3/h	2056	2654	2969	3002	2753
in^3/sec	34859	44984	50327	50888	46667
ft^3/min	1210.2	1561.8	1747.3	1766.7	1620.2

Above data is decided by following conditions.

1. Using the standard radiator.
2. Engine is run as open unit.

3. Combustion and cooling air requirements (Refer to 25deg.C and 1000hPa)

rpm	2000	2400	2800	3200	3600
L/sec	583.5	752.0	842.0	853.7	786.9
m^3/h	2100.4	2707.3	3031.2	3073.1	2833.0
in^3/sec	35612	45888	51382	52093	48023
ft^3/min	1236.3	1593.2	1783.9	1808.5	1667.2

Note

1. Cooling fan and fan pulley specifications(Cooling fan Part No. 15881-74112)

Item	
Fan diameter	300mm (11.81in)
No. of blade and type of shape	4, S type
Diameter of fan driving pulley	100mm (3.94in)
Diameter of fan pulley	84mm (3.31in)

2. Conversion rates

$1L=61.0237in^3=0.035315ft^3$
$1ft^3=28.3168L$
$1L/sec=3.6m^3/h=2.1189ft^3/min$

4-5) EXHAUST GAS VOLUME

Refer to 25deg.C and 1000hPa

rpm	2000	2400	2800	3200	3600
L/sec	35.46	42.55	49.65	56.74	63.83
m^3/h	127.67	153.19	178.73	204.26	229.80
in^3/sec	2164	2597	3030	3462	3895
ft^3/min	75.05	90.06	105.07	120.08	135.09

Note

1. Conversion rates $1L=61.0237in^3=0.035315ft^3$
   $1ft^3=28.3168L$
   $1L/sec=3.6m^3/h=127.133ft^3/hr$

4-6) HEAT REJECTION TO COOLING WATER

1. Specific at net intermittent (SAE J1349)

Engine speed	rpm	2000	2400	2800	3200	3600
Brake horse power	kW	12.6	15.4	17.4	18.9	19.5
	HP	16.9	20.6	23.3	25.3	26.1
	PS	17.1	20.9	23.7	25.7	26.5
Fuel consumption	g/kWh	269	264	269	273	273
	g/HPh	200	197	200	204	204
	g/PSh	198	194	198	201	201
	lb/HPh	0.442	0.434	0.442	0.449	0.449
Heat rejection to cooling water	MJ/h	29.05	31.52	38.79	45.13	51.82
	kcal/h	6940	7529	9267	10781	12379
	BTU/h	12491	13551	16679	19404	22281

Note

Heat rejection to cooling water calculating formula

Ho=Hu•Ne•be•i

Ho: Heat rejection to cooling water

Hu: Fuel low calorific value

Japanese standard gas; 49.4MJ/kg, 11800kcal/h, 212391BTU/lb

Ne: Brake horse power

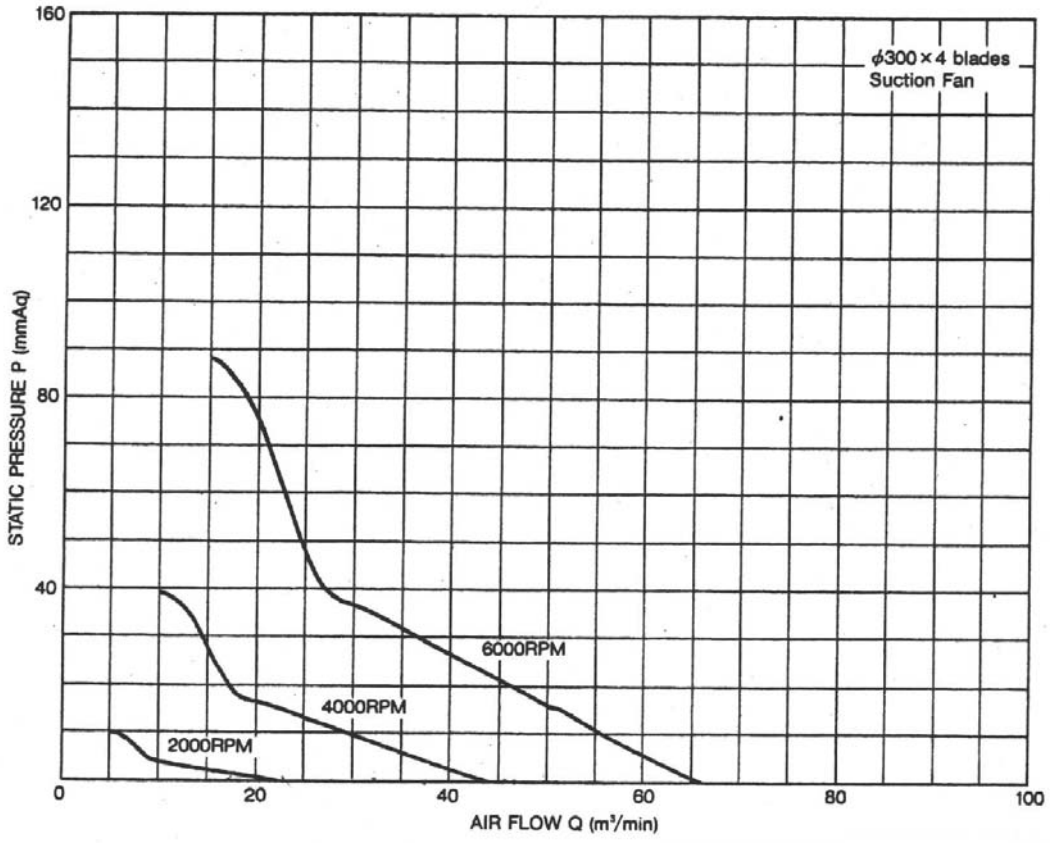
Be: Specific fuel consumption

i: Dispersion ratio to cooling water

4-7) COOLING FAN DATA

1. Performance curves <P-Q>

- Part No. 15881-74110 (Applicable for DG972)



4-8) CENTER OF GRAVITY

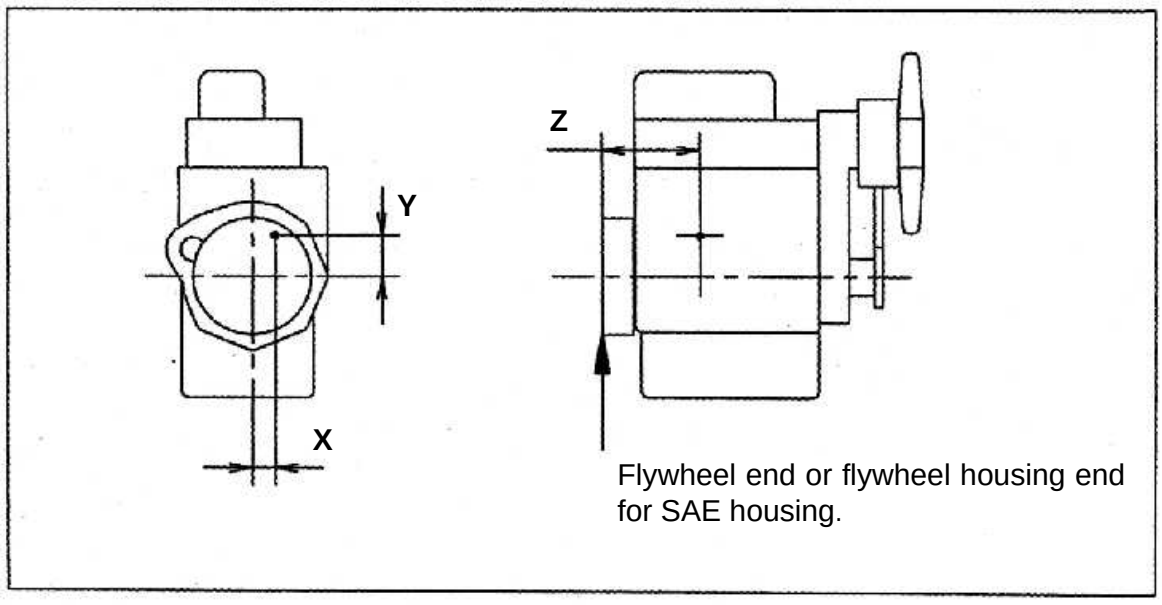
1. With standard flywheel and rear-end plate

Model	Dry weight kg (lb)	Center of gravity		
		X mm (in)	Y mm (in)	Z mm (in)
WG/DF972	72.0 (159)	-25.5 (-1.00)	73.3 (2.89)	179.5 (7.07)

2. With SAE flywheel and flywheel housing

Model	Dry weight kg (lb)	Center of gravity		
		X mm (in)	Y mm (in)	Z mm (in)
DG972 -SAEH-S1	95.4 (210)	-10.0 (0.39)	28.0 (1.10)	207.0 (8.15)

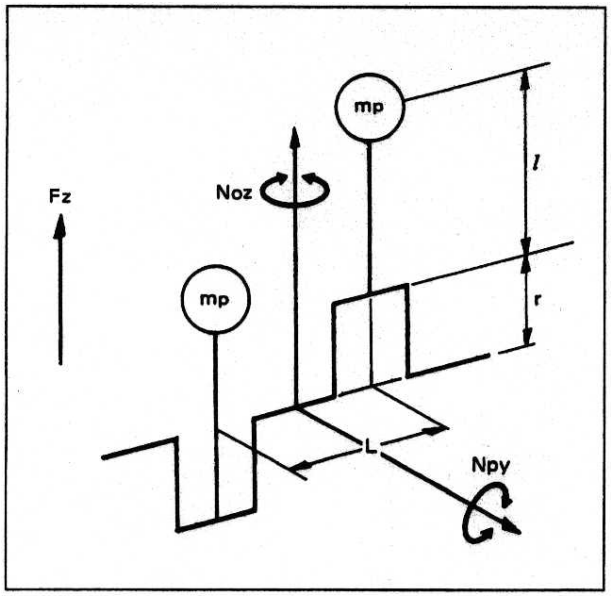
Note
Cooling water and lubricating oil weight is not included in above engine weight.



Flywheel end or flywheel housing end for SAE housing.

4-9) UNBALANCED FORCES OF ENGINES

1. Base data



FZ: Unbalanced inertia force
Npy, Noz: Unbalanced inertia couple
mp: Reciprocating mass
r: Crank radius
l: Center distance of connecting rod
L: Cylinder distance
ω: Angular velocity

ω=2πn/60	n: Engine speed(rpm)

l=0.098m r=0.0368m L=0.080m	Cylinder bore (mm)	mp (kg)
	74.5	0.37/9.80665

2. Unbalanced inertia force and couple

($x\omega^2$)

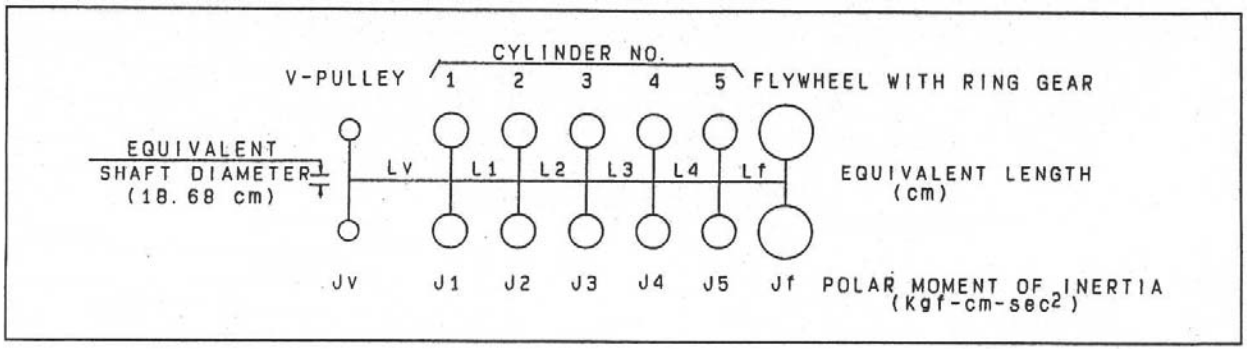
Model	No. of Cylinder	Cylinder Bore	Order	Fz	Npy	Noz
WG/DF/DG 972	3	74.5mm	1	0	0.000096	0.000096
			2	0	0.000072	0

▼An example of calculation

Calculation condition	ω^2	Fz, Npy, Noz		
			Order	Calculation
Engine model DG972 Engine speed 3600(rpm)	$[2 \times \pi \times 3600/60]^2$ =142122	Fz	1	0
			2	0
		Npy	1	0.000096 × 142122=13.6kg
			2	0.000072 × 142122=10.2kg
		Noz	1	0.000096 × 142122=13.6kg
			2	0

4-10) MASS ELASTIC SYSTEM

Equivalent torsional vibration data



MODEL	EQUIVALENT LENGTH (cm)				POLAR MOMENT OF INERTIA (kgfcm-sec^2)				
	LV	L1	L2	Lf	JV	J1	J2	J3	Jf
DG972 -SAEH-S1	35082	4528	4528	2824	0.013	0.026	0.026	0.026	1.281

Note: Flywheel E8052-25110, V-Pulley 16861-74280

5. FUEL SYSTEM AND FUEL DIAGRAM

- **All fuel connections added to this engine must be installed by qualified personnel utilizing recognized procedures and standards.**
- **These non-KUBOTA installed parts, such as hoses, shutoff solenoid valve should be approved for Natural gas use.**
- **An approved, listed fuel filter and shutoff solenoid valve must be installed between the gas tank and Kubota regulator.**
- **Two fuel cut solenoids must be installed in series before the regulator on the fuel supply line for safety (backup) purpose.**

1. Tightening torque and leak check

1) The joint must be installed to the gas entrance of the regulator by screw with O-ring. Screw is tightened to the specified torque using a driver, and leak check must be performed as shown in the below table.
2) The connector on the gas mixer may be mounted on any position since it is not sealed. The lock nut may be loosened using a wrench. The connector may be changed to any specified angle. The lock nut should be tightened to the specified torque using a wrench as shown in the below table.

[TIGHTENING TORQUE AND LEAK CHECK]

			Tightening torque			Leak check pressure
	Qty.	Size	Nm	kgfm	ft-lb	
SCREW	2	M4	1.9 to 2.9	0.2 to 0.3	1.5 to 2.2	Soap solution or its equivalent
LOCK NUT	1	M16 × 1	19.6 to 39.2	2.0 to 4.0	14.5 to 28.9	

2. Setting of the regulator

1) Install the regulator in **UPRIGHT** position, it must be installed within 4G vibration level. If not, it may not supply necessary fuel to the engine.
2) **DO NOT** connect any extension hose to the air vent pipe of the regulator. This may cause an improper supply of fuel to the engine.

3. Caution for FUEL SYSTEM

The standard engine is equipped with ϕ6.6 jet for the fuel calorific gas value of 11000kcal/m^3 (1236BTU/ft^3).
When the engine is operated with the different calorific gas, it is necessary to select the correct jet of the mixer.
In that case, refer to the manual **[Adjustment for Natural Gas Engine DG972]**.

Japanese standard gas higher calorific value : 11000kcal/m^3 (1236BTU/ft^3)
supply pressure : 0.98 – 2.45kPa (7.35 – 18.38mmHg)

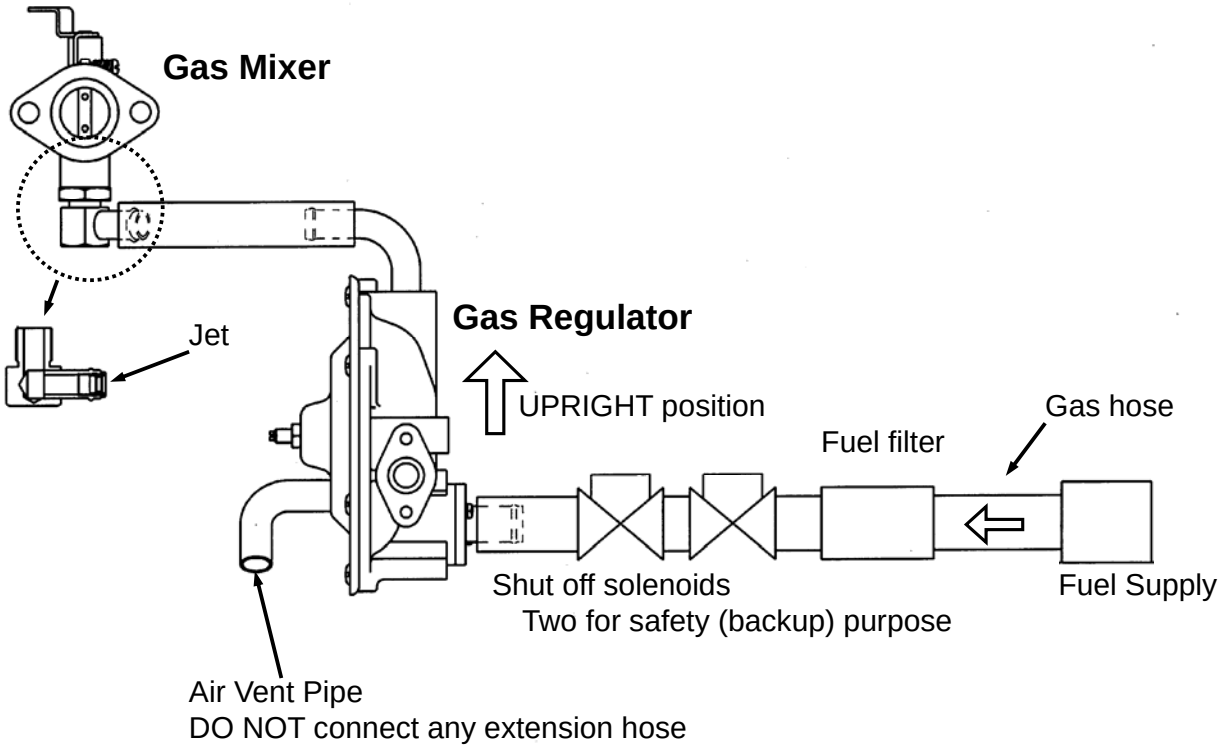
Equipments Vacuum Meter : Not KUBOTA supplied
Adjustable Jet : Service Tool

4. Application Check Item

The items as shown below must be managed for all engines, and these items must be informed to KUBOTA with Application Check results.
Refer to the attached sheet **[Application Check Sheet for DG972]**.

1) The diameter of the jet (with the intake vacuum curve)
2) The calorific value of the gas
3) The supply pressure of gas
4) The serial number of the engine

5. Fuel diagram



NATURAL GAS ENGINE

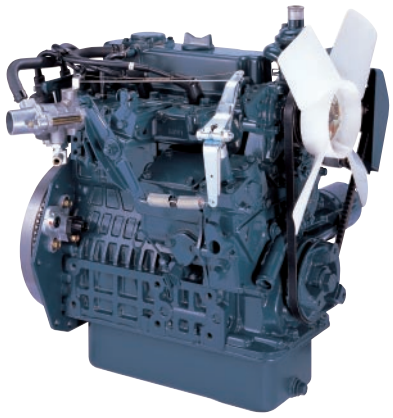
KUBOTA DG SERIES (3-cylinder)

DG972-E2

2 EPA Tier

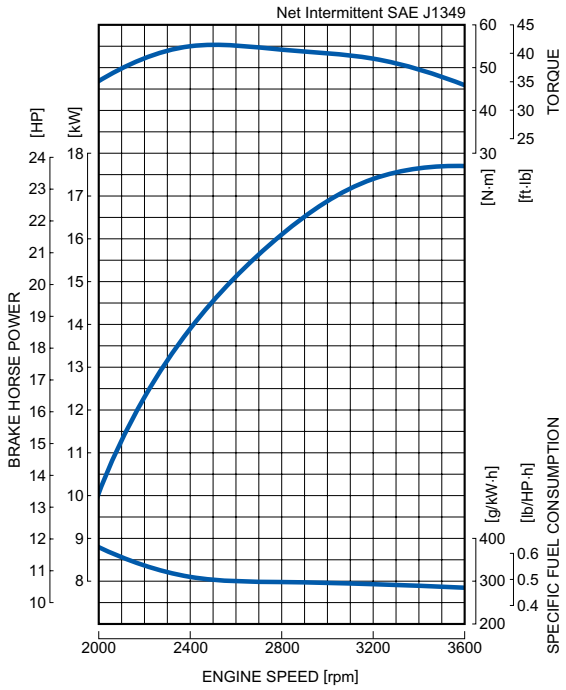
RATED POWER

17.6kW@3600rpm



Photograph may show non-standard equipment.

PERFORMANCE CURVE



FEATURES and BENEFITS

New Engine Series

- The Kubota DG Series offers a new solution to the increasing needs for natural gas engine. The diesel engine based Kubota DG Series gives users the same foot-print, reliability and durability of D902, WG972, and DF972 acknowledged as the world's top quality small industrial engines.
- Kubota offers SAE Flywheel Housing and Rear End Plate specifications for the DG972 engine. These options offer users flexible Power Take Off (PTO) choices.
- The Kubota DG Series is designed to endure use outdoors under severe environment. This series is equipped with a bypass breather tube to avoid freezing below zero.

Emission

- Kubota DG Series complies with EPA Tier 2 Emissions Regulations. EPA regulation is one of the most stringent emissions regulations in the world.

Best Fuel System

- Specialized for Natural Gas use, the DG972 engine eliminated the carburetor, regulator and a fuel filter parts, which are only necessary for Gasoline or LPG use. Also, Kubota adopts the best jet set and the ignition timing that provides the best engine performance in severe conditions.

Ease maintenance cost and time

- Mechanical governor system will contribute to lower maintenance cost and prevents users from having to deal with complicated electric maintenance. Moreover, water resistant spark plug caps are adopted for outdoor use.

DG972-E2

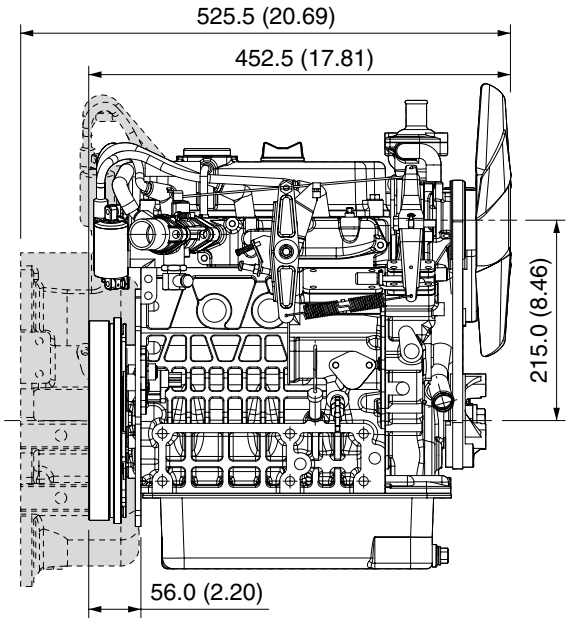
KUBOTA DG SERIES

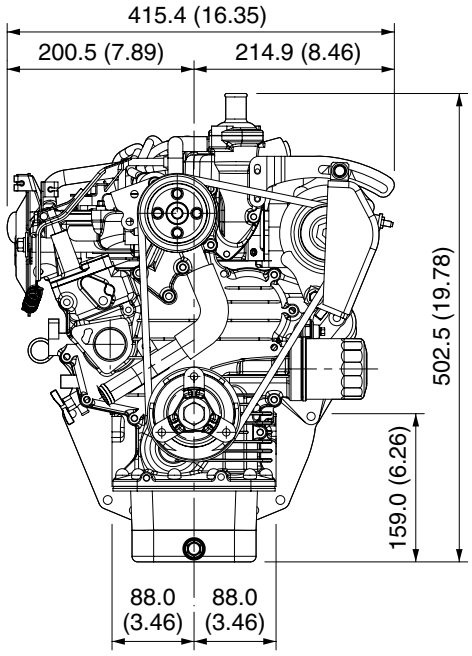
GENERAL SPECIFICATION

Model		DG972-E2
Emission Regulation		Tier 2
Type		Vertical 4-cycle Liquid Cooled Natural Gas
Number of Cylinders		3
Bore	mm (in)	74.5 (2.93)
Stroke	mm (in)	73.6 (2.9)
Displacement	L (cu.in)	0.962 (58.70)
Fuel		Natural Gas
Intake System		Naturally Aspirated
Maximum Speed	rpm	3600
Output: Net Intermittent	kW	17.6
	hp	23.6
	ps	23.9
Direction of Rotation		Counterclockwise Viewed on Flywheel
Oil Pan Capacity	L (gal)	3.7 (0.98)
Starter Capacity	V-kW	12-1.0
Alternator Capacity	V-A	12-40
Length	mm (in)	525.5 (20.69)*1 / 452.5 (17.81)*2
Width	mm (in)	415.4 (16.35)
Height (1)	mm (in)	502.5 (19.78)
Height (2)	mm (in)	159.0 (6.26)
Dry Weight	kg (lb)	72.0 (158.7)*1 / 95.4 (210.3)*2

*Specification is subject to change without notice.
*Output: Net Intermittent SAE J1349
*Dry weight is according to Kubota's standard specification.
When specification varies, the weight will vary accordingly.
*1 with SAE Flywheel and Housing
*2 with Rear End Plate

DIMENSIONS





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