



January 26, 2016

Mr. Jerry Williams, P.E.
WV Department of Environmental Protection
Division of Air Quality
601 57th Street, SE
Charleston, WV 25304

**RE: Antero Midstream LLC – Monroe Compressor Station
West Virginia Department of Environmental Protection, Division of Air Quality,
45CSR13 Air Permit Modification R13-3184A**

Dear Mr. Williams,

On behalf of Antero Midstream LLC, please find attached the 45CSR13 Air Permit Modification for permit number R13-3184A for the Monroe Compressor Station (Facility ID 095-00037) located in Tyler County, West Virginia. A summary of the modifications in this application include:

1. Updating compressor engine emissions to reflect catalyst data based on a new catalyst design from the manufacturer,
2. The installation of two new compressor engines and associated blowdown events,
3. Eliminating the compressor fuel use limit and synthetic minor status,
4. Increasing the dehydrator throughput to 72.5 MMscfd per dehydrator, and
5. Modifying the dehydrator flash tank control efficiency based on new standardized guidance from WVDEP.

Additionally, Antero is requesting to modify the permit language for the recordkeeping of the hours of operation for the generators based on suggestion from a WVDEP inspector. Condition 5.1.3. Maximum Yearly Operation Limit should read:

The two (2) 600 kW natural gas fired microturbine generators, Capstone C600 (GEN1, GEN2) are comprised of six (6) 200 kW individual generators and engines. The maximum combined yearly hours of operation for the six (6) individual hour meters on the six (6) 200 kW natural gas fired microturbine generators enclosed within the two Capstone C600 (GEN1, GEN2) shall not exceed 27,780 hours per year. Compliance with the Maximum Yearly Operation Limitation shall be determined using a twelve month rolling total. A twelve month rolling total shall mean the sum of the six (6) meters of the hours of operation at any given time during the previous twelve consecutive calendar months.

This request does not alter emissions or currently permitted operating hours and is strictly to streamline recordkeeping of the operational hours of the generators (GEN1 and GEN2).

Enclosed are one hardcopy and two CDs containing the entire permit application including the application form and required attachments. Per 45CSR22, a \$4,500 application fee is also

enclosed, which covers the base 45CSR13 \$1,000 application fee, an additional \$1,000 for NSPS requirements, and an additional \$2,500 for Hazardous Air Pollutant requirements.

A copy of the Air Quality Permit Notice for the advertisement is included as Attachment P. As the Notice is being submitted simultaneously with the application, the official affidavit of publication will be submitted to the Division of Air Quality separately once it is completed.

Please call if you have any questions or if I can be of further assistance. I can be reached at (719)632-3593 or by email at msteyskal@kleinfelder.com.

Sincerely,
KLEINFELDER



Michele Steyskal
Air Quality Specialist

Enclosures: Monroe Compressor Station R13-3184A Air Permit Modification

Antero Midstream LLC

Monroe Compressor Station

**NSR Permit Application R13-3184A Modification
West Virginia Department of Environmental Protection
Division of Air Quality
45CSR13**

Tyler County, West Virginia

January 2016

Prepared by:



**1801 California Street, Suite 1100
Denver, CO 80202
(303) 237-6601
Fax (303) 237-6602
www.kleinfelder.com**

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WEST VIRGINIA DEPARTMENT OF ENVIRONMENTAL PROTECTION
DIVISION OF AIR QUALITY

601 57th Street, SE
Charleston, WV 25304
(304) 926-0475
www.dep.wv.gov/daq

**APPLICATION FOR NSR PERMIT
AND
TITLE V PERMIT REVISION
(OPTIONAL)**

PLEASE CHECK ALL THAT APPLY TO **NSR (45CSR13)** (IF KNOWN):

- CONSTRUCTION MODIFICATION RELOCATION
 CLASS I ADMINISTRATIVE UPDATE TEMPORARY
 CLASS II ADMINISTRATIVE UPDATE AFTER-THE-FACT

PLEASE CHECK TYPE OF **45CSR30 (TITLE V)** REVISION (IF ANY):

- ADMINISTRATIVE AMENDMENT MINOR MODIFICATION
 SIGNIFICANT MODIFICATION

IF ANY BOX ABOVE IS CHECKED, INCLUDE TITLE V REVISION INFORMATION AS **ATTACHMENT S** TO THIS APPLICATION

FOR TITLE V FACILITIES ONLY: Please refer to "Title V Revision Guidance" in order to determine your Title V Revision options (Appendix A, "Title V Permit Revision Flowchart") and ability to operate with the changes requested in this Permit Application.

Section I. General

1. Name of applicant (as registered with the WV Secretary of State's Office): Antero Midstream LLC		2. Federal Employer ID No. (FEIN): 46-5517375	
3. Name of facility (if different from above): Monroe Compressor Station		4. The applicant is the: <input type="checkbox"/> OWNER <input type="checkbox"/> OPERATOR <input checked="" type="checkbox"/> BOTH	
5A. Applicant's mailing address: 1615 Wynkoop Street Denver, CO 80202		5B. Facility's present physical address: Conaway Run Road Alma, WV 26320	
6. West Virginia Business Registration. Is the applicant a resident of the State of West Virginia? <input type="checkbox"/> YES <input checked="" type="checkbox"/> NO <ul style="list-style-type: none"> - If YES, provide a copy of the Certificate of Incorporation/Organization/Limited Partnership (one page) including any name change amendments or other Business Registration Certificate as Attachment A. - If NO, provide a copy of the Certificate of Authority/Authority of L.L.C./Registration (one page) including any name change amendments or other Business Certificate as Attachment A. 			
7. If applicant is a subsidiary corporation, please provide the name of parent corporation:			
8. Does the applicant own, lease, have an option to buy or otherwise have control of the <i>proposed site</i> ? <input checked="" type="checkbox"/> YES <input type="checkbox"/> NO <ul style="list-style-type: none"> - If YES, please explain: Antero Resources Corporation owns the land for the site - If NO, you are not eligible for a permit for this source. 			
9. Type of plant or facility (stationary source) to be constructed, modified, relocated, administratively updated or temporarily permitted (e.g., coal preparation plant, primary crusher, etc.): Natural Gas Compressor Station		10. North American Industry Classification System (NAICS) code for the facility: 221210	
11A. DAQ Plant ID No. (for existing facilities only): 095-00037		11B. List all current 45CSR13 and 45CSR30 (Title V) permit numbers associated with this process (for existing facilities only): R13-3184A	

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

<p>12A.</p> <ul style="list-style-type: none"> For Modifications, Administrative Updates or Temporary permits at an existing facility, please provide directions to the <i>present location</i> of the facility from the nearest state road; For Construction or Relocation permits, please provide directions to the <i>proposed new site location</i> from the nearest state road. Include a MAP as Attachment B. <p>From Alma, WV, on WV-18 turn west onto Conaway Run Road (Co Rd 48). After 1.6 miles, turn right onto facility entrance.</p>		
<p>12.B. New site address (if applicable):</p> <p>Conaway Run Road Alma, WV 26320</p>	<p>12C. Nearest city or town:</p> <p>Alma</p>	<p>12D. County:</p> <p>Tyler</p>
<p>12.E. UTM Northing (KM): 4363.467</p>	<p>12F. UTM Easting (KM): 511.720</p>	<p>12G. UTM Zone: 17</p>
<p>13. Briefly describe the proposed change(s) at the facility: The reduction efficiencies for the engine catalysts have been updated based on new catalyst information. Two new compressor engines have been added. The dehydrator throughput has been increased to 72.5 MMscfd per dehydrator. Lastly, the fuel limit for the compressors has been removed so the facility is no longer a synthetic minor.</p>		
<p>14A. Provide the date of anticipated installation or change: Upon Permit Issuance</p> <ul style="list-style-type: none"> If this is an After-The-Fact permit application, provide the date upon which the proposed change did happen: / / 	<p>14B. Date of anticipated Start-Up if a permit is granted: <p style="text-align: right;">April 1, 2016</p></p>	
<p>14C. Provide a Schedule of the planned Installation of/Change to and Start-Up of each of the units proposed in this permit application as Attachment C (if more than one unit is involved).</p>		
<p>15. Provide maximum projected Operating Schedule of activity/activities outlined in this application:</p> <p style="text-align: center;">Hours Per Day 24 Days Per Week 7 Weeks Per Year 52</p>		
<p>16. Is demolition or physical renovation at an existing facility involved? <input type="checkbox"/> YES <input checked="" type="checkbox"/> NO</p>		
<p>17. Risk Management Plans. If this facility is subject to 112(r) of the 1990 CAAA, or will become subject due to proposed changes (for applicability help see www.epa.gov/ceppo), submit your Risk Management Plan (RMP) to U. S. EPA Region III.</p>		
<p>18. Regulatory Discussion. List all Federal and State air pollution control regulations that you believe are applicable to the proposed process (<i>if known</i>). A list of possible applicable requirements is also included in Attachment S of this application (Title V Permit Revision Information). Discuss applicability and proposed demonstration(s) of compliance (<i>if known</i>). Provide this information as Attachment D.</p>		
<p>Section II. Additional attachments and supporting documents.</p>		
<p>19. Include a check payable to WVDEP – Division of Air Quality with the appropriate application fee (per 45CSR22 and 45CSR13).</p>		
<p>20. Include a Table of Contents as the first page of your application package.</p>		
<p>21. Provide a Plot Plan, e.g. scaled map(s) and/or sketch(es) showing the location of the property on which the stationary source(s) is or is to be located as Attachment E (Refer to Plot Plan Guidance) .</p> <ul style="list-style-type: none"> Indicate the location of the nearest occupied structure (e.g. church, school, business, residence). 		
<p>22. Provide a Detailed Process Flow Diagram(s) showing each proposed or modified emissions unit, emission point and control device as Attachment F.</p>		
<p>23. Provide a Process Description as Attachment G.</p> <ul style="list-style-type: none"> Also describe and quantify to the extent possible all changes made to the facility since the last permit review (if applicable). 		
<p>All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.</p>		

24. Provide **Material Safety Data Sheets (MSDS)** for all materials processed, used or produced as **Attachment H**.
 – For chemical processes, provide a MSDS for each compound emitted to the air.

25. Fill out the **Emission Units Table** and provide it as **Attachment I**.

26. Fill out the **Emission Points Data Summary Sheet (Table 1 and Table 2)** and provide it as **Attachment J**.

27. Fill out the **Fugitive Emissions Data Summary Sheet** and provide it as **Attachment K**.

28. Check all applicable **Emissions Unit Data Sheets** listed below:

<input type="checkbox"/> Bulk Liquid Transfer Operations	<input type="checkbox"/> Haul Road Emissions	<input type="checkbox"/> Quarry
<input checked="" type="checkbox"/> Chemical Processes	<input type="checkbox"/> Hot Mix Asphalt Plant	<input type="checkbox"/> Solid Materials Sizing, Handling and Storage Facilities
<input type="checkbox"/> Concrete Batch Plant	<input type="checkbox"/> Incinerator	<input type="checkbox"/> Storage Tanks
<input type="checkbox"/> Grey Iron and Steel Foundry	<input type="checkbox"/> Indirect Heat Exchanger	
<input checked="" type="checkbox"/> General Emission Unit, specify: Engines, Dehydrator		

Fill out and provide the **Emissions Unit Data Sheet(s)** as **Attachment L**.

29. Check all applicable **Air Pollution Control Device Sheets** listed below:

<input type="checkbox"/> Absorption Systems	<input type="checkbox"/> Baghouse	<input type="checkbox"/> Flare
<input type="checkbox"/> Adsorption Systems	<input type="checkbox"/> Condenser	<input type="checkbox"/> Mechanical Collector
<input type="checkbox"/> Afterburner	<input type="checkbox"/> Electrostatic Precipitator	<input type="checkbox"/> Wet Collecting System
<input checked="" type="checkbox"/> Other Collectors, specify : Catalysts		

Fill out and provide the **Air Pollution Control Device Sheet(s)** as **Attachment M**.

30. Provide all **Supporting Emissions Calculations** as **Attachment N**, or attach the calculations directly to the forms listed in Items 28 through 31.

31. **Monitoring, Recordkeeping, Reporting and Testing Plans.** Attach proposed monitoring, recordkeeping, reporting and testing plans in order to demonstrate compliance with the proposed emissions limits and operating parameters in this permit application. Provide this information as **Attachment O**.
 ➤ Please be aware that all permits must be practically enforceable whether or not the applicant chooses to propose such measures. Additionally, the DAQ may not be able to accept all measures proposed by the applicant. If none of these plans are proposed by the applicant, DAQ will develop such plans and include them in the permit.

32. **Public Notice.** At the time that the application is submitted, place a **Class I Legal Advertisement** in a newspaper of general circulation in the area where the source is or will be located (See 45CSR§13-8.3 through 45CSR§13-8.5 and **Example Legal Advertisement** for details). Please submit the **Affidavit of Publication** as **Attachment P** immediately upon receipt.

33. **Business Confidentiality Claims.** Does this application include confidential information (per 45CSR31)?
 YES NO
 ➤ If **YES**, identify each segment of information on each page that is submitted as confidential and provide justification for each segment claimed confidential, including the criteria under 45CSR§31-4.1, and in accordance with the DAQ's "**Precautionary Notice – Claims of Confidentiality**" guidance found in the **General Instructions** as **Attachment Q**.

Section III. Certification of Information

34. **Authority/Delegation of Authority.** Only required when someone other than the responsible official signs the application. Check applicable **Authority Form** below:

<input type="checkbox"/> Authority of Corporation or Other Business Entity	<input type="checkbox"/> Authority of Partnership
<input type="checkbox"/> Authority of Governmental Agency	<input type="checkbox"/> Authority of Limited Partnership

Submit completed and signed **Authority Form** as **Attachment R**.

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

35A. **Certification of Information.** To certify this permit application, a Responsible Official (per 45CSR§13-2.22 and 45CSR§30-2.28) or Authorized Representative shall check the appropriate box and sign below.

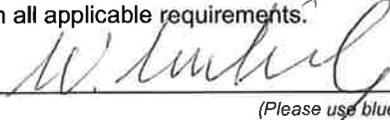
Certification of Truth, Accuracy, and Completeness

I, the undersigned **Responsible Official** / **Authorized Representative**, hereby certify that all information contained in this application and any supporting documents appended hereto, is true, accurate, and complete based on information and belief after reasonable inquiry I further agree to assume responsibility for the construction, modification and/or relocation and operation of the stationary source described herein in accordance with this application and any amendments thereto, as well as the Department of Environmental Protection, Division of Air Quality permit issued in accordance with this application, along with all applicable rules and regulations of the West Virginia Division of Air Quality and W.Va. Code § 22-5-1 et seq. (State Air Pollution Control Act). If the business or agency changes its Responsible Official or Authorized Representative, the Director of the Division of Air Quality will be notified in writing within 30 days of the official change.

Compliance Certification

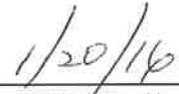
Except for requirements identified in the Title V Application for which compliance is not achieved, I, the undersigned hereby certify that, based on information and belief formed after reasonable inquiry, all air contaminant sources identified in this application are in compliance with all applicable requirements.

SIGNATURE _____



(Please use blue ink)

DATE: _____



(Please use blue ink)

35B. Printed name of signee: Ward McNeilly

35C. Title: Vice President, Reserves Planning and Midstream

35D. E-mail: wmcneilly@anteroresources.com

35E. Phone: (303)357-6822

35F. FAX: (303)357-7315

36A. Printed name of contact person (if different from above): Barry Schatz

36B. Title: Senior Environmental and Regulatory Manager

36C. E-mail: bschatz@anteroresources.com

36D. Phone: (303) 357-7276

36E. FAX: (303)357-7315

PLEASE CHECK ALL APPLICABLE ATTACHMENTS INCLUDED WITH THIS PERMIT APPLICATION:

- | | |
|--|--|
| <input checked="" type="checkbox"/> Attachment A: Business Certificate | <input checked="" type="checkbox"/> Attachment K: Fugitive Emissions Data Summary Sheet |
| <input checked="" type="checkbox"/> Attachment B: Map(s) | <input checked="" type="checkbox"/> Attachment L: Emissions Unit Data Sheet(s) |
| <input checked="" type="checkbox"/> Attachment C: Installation and Start Up Schedule | <input checked="" type="checkbox"/> Attachment M: Air Pollution Control Device Sheet(s) |
| <input checked="" type="checkbox"/> Attachment D: Regulatory Discussion | <input checked="" type="checkbox"/> Attachment N: Supporting Emissions Calculations |
| <input checked="" type="checkbox"/> Attachment E: Plot Plan | <input checked="" type="checkbox"/> Attachment O: Monitoring/Recordkeeping/Reporting/Testing Plans |
| <input checked="" type="checkbox"/> Attachment F: Detailed Process Flow Diagram(s) | <input checked="" type="checkbox"/> Attachment P: Public Notice |
| <input checked="" type="checkbox"/> Attachment G: Process Description | <input type="checkbox"/> Attachment Q: Business Confidential Claims |
| <input checked="" type="checkbox"/> Attachment H: Material Safety Data Sheets (MSDS) | <input checked="" type="checkbox"/> Attachment R: Authority Forms |
| <input checked="" type="checkbox"/> Attachment I: Emission Units Table | <input type="checkbox"/> Attachment S: Title V Permit Revision Information |
| <input checked="" type="checkbox"/> Attachment J: Emission Points Data Summary Sheet | <input checked="" type="checkbox"/> Application Fee |

Please mail an original and three (3) copies of the complete permit application with the signature(s) to the DAQ, Permitting Section, at the address listed on the first page of this application. Please DO NOT fax permit applications.

FOR AGENCY USE ONLY – IF THIS IS A TITLE V SOURCE:

- Forward 1 copy of the application to the Title V Permitting Group and:
- For Title V Administrative Amendments:
 - NSR permit writer should notify Title V permit writer of draft permit,
- For Title V Minor Modifications:
 - Title V permit writer should send appropriate notification to EPA and affected states within 5 days of receipt,
 - NSR permit writer should notify Title V permit writer of draft permit.
- For Title V Significant Modifications processed in parallel with NSR Permit revision:
 - NSR permit writer should notify a Title V permit writer of draft permit,
 - Public notice should reference both 45CSR13 and Title V permits,
 - EPA has 45 day review period of a draft permit.

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

Discussion of Nearby Facilities

Monroe Compressor Station – Closest Antero Midstream Facilities

1. Common Control: Only those facilities that are owned and managed by Antero were included in the aggregation discussion. This includes Antero Resources Corporation production facilities in addition to the Antero Midstream LLC midstream facilities.

2. SIC Code: The Monroe Compressor Station will operate under SIC code 4923 (natural gas distribution). The closest facility owned by Antero Midstream LLC with this SIC code is the Underwood Compressor station which is 0.93 miles northwest of the Facility. All Antero Resources Corporation production facilities operate under the SIC code of 1311 (crude petroleum and natural gas extraction). The closest facility operated by Antero Resources Corporation with the SIC code of 1311 is the Dale Pad 0.78 miles to the north.

3. Contiguous or Adjacent: The land between the Monroe Compressor Station and its nearest facility operating under SIC code 4923 is not owned or managed by Antero Midstream LLC or Antero Resources Corporation. Therefore, the two facilities are not contiguous or adjacent.

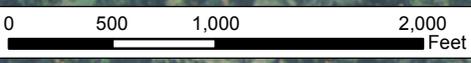
Based on this three-pronged evaluation, although the Monroe Compressor Station and Underwood Compressor Station do belong to the same major industrial group, they should not be aggregated because they are not contiguous or adjacent.

The Monroe Compressor Station and Dale Pad should not be aggregated because they do not belong to the same major industrial group and do not directly rely on each other nor are they contiguous or adjacent.



Service Layer Credits: Source: Esri, DigitalGlobe, GeoEye, Earthstar Geographics, CNES/Airbus DS, USDA, USGS, AEX, Getmapping, Aerognd, IGN, IGP, swisstopo, and the GIS User Community

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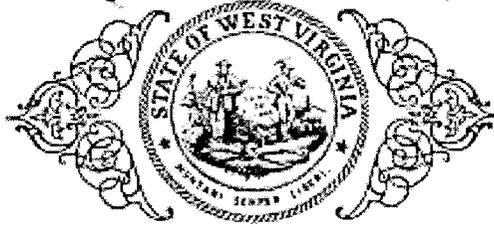
Legend

- Receptor
- ▲ Monroe Compressor Station
- Existing Road

 KLEINFELDER <i>Bright People. Right Solutions.</i> www.kleinfelder.com	PROJECT NO. 20163815.001A	Antero Midstream LLC	FIGURE
	DRAWN: 1/20/2016		
	DRAWN BY: B. McDavid	Monroe Compressor Station Tyler County, West Virginia	
	CHECKED BY: M. Steyskal		
FILE NAME: Monroe_ClosestReceptor.mxd			

**Attachment A.
Business Certificate**

State of West Virginia



Certificate

LAB

I, Natalie E. Tennant, Secretary of State of the State of West Virginia, hereby certify that

ANTERO MIDSTREAM LLC

Control Number: 9A5E1

a limited liability company, organized under the laws of the State of Delaware has filed its "Application for Certificate of Authority" in my office according to the provisions of West Virginia Code §31B-10-1002. I hereby declare the organization to be registered as a foreign limited liability company from its effective date of April 29, 2014, until a certificate of cancellation is filed with our office.

Therefore, I hereby issue this

CERTIFICATE OF AUTHORITY OF A FOREIGN LIMITED LIABILITY COMPANY

to the limited liability company authorizing it to transact business in West Virginia



Given under my hand and the Great Seal of the State of West Virginia on this day of April 29, 2014

Natalie E. Tennant

Secretary of State

FILED

APR 29 2014

IN THE OFFICE OF
WV SECRETARY OF STATE

Submitted by:
CT Corporation Rep-Terry Stamper
Terry.Stamper@wolterskluwer.com
304-776-1152

1152

Natafie E. Tennant
Secretary of State
1900 Kanawha Blvd E
Bldg 1, Suite 157-K
Charleston, WV 25305



Penney Barker, Manager
Corporations Division
Tel: (304)558-8000
Fax: (304)558-8381
Website: www.wvsos.com
E-mail: business@wvsos.com

WV APPLICATION FOR
CERTIFICATE OF AUTHORITY OF
LIMITED LIABILITY COMPANY

FILE ONE ORIGINAL.
(Two if you want a filed
stamped copy returned to you)
FEE: \$150

Office Hours: Monday - Friday
8:30 a.m. - 5:00 p.m. ET

Control # CAE1

1. The name of the company as registered in its home state is: Antero Midstream LLC

and the state or country of organization is: Delaware

CHECK HERE to indicate you have obtained and submitted with this application a **CERTIFICATE OF EXISTENCE (GOOD STANDING)**, dated during the current tax year, from your home state of original incorporation as required to process your application. The certificate may be obtained by contacting the Secretary of State's Office in the home state of original incorporation.

2. The name to be used in West Virginia will be: Home State name as listed above, if available in WV (If name is not available, check DBA Name box below and follow special instructions in Section 2. attached.)
 DBA name _____
(See special instructions in Section 2. Regarding the Letter of Resolution attached to this application.)

3. The company will be a: [See instructions for limitations on professions which may form P.L.L.C. in WV. All members must have WV professional license. In most cases, a Letter of Authorization/Approval from the appropriate State Licensing Board is required to process the application.]
 regular L.L.C.
 Professional L.L.C. for the profession of _____

4. The street address of the principal office is: No. & Street: 1625 17th Street, Suite 300
City/State/Zip: Denver, Colorado 80202
and the mailing address (if different) is: Street/Box: _____
City/State/Zip: _____

5. The address of the designated office of the company in WV, if any, will be: No. & Street: 5400 D Big Tyler Road
City/State/Zip: Charleston, West Virginia 25313

6. Agent of Process: Properly designated person to whom notice of legal process may be sent, if any: Name: C T Corporation System
Address: 5400 D Big Tyler Road
City/State/Zip: Charleston, West Virginia 25313

RECEIVED

APR 29 2014

7. E-mail address where business correspondence may be received: jgiannaula@anteroresources.com

8. Website address of the business, if any: N/A

9. The company is: an at-will company, for an indefinite period
 a term company, for the term of _____ years,
 which will expire on _____.

10. The company is: member-managed. [List the names and addresses of all members.]
 manager-managed. [List the names and addresses of all managers.]

List the Name(s) and Address(es) of the Member(s)/Manager(s) of the company (attach additional pages if necessary).

Name	Street Address	City, State, Zip
Antero Resources Corporation	1625 17th Street, Suite 300	Denver, Colorado 80202

11. All or specified members of a limited liability company are liable in their capacity as members for all or specified debts, obligations or liabilities of the company. No--All debts, obligations and liabilities are those of the company.
 Yes--Those persons who are liable in their capacity as members for all debts, obligations or liability of the company have consented in writing to the adoption of the provision or to be bound by the provision.

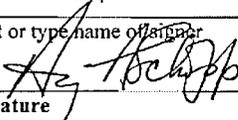
12. The purpose for which this limited liability company is formed are as follows:
 (Describe the type(s) of business activity which will be conducted, for example, "real estate," "construction of residential and commercial buildings," "commercial printing," "professional practice of architecture.")
Midstream oil and gas operating company

13. Is the business a Scrap Metal Dealer?
 Yes [If "Yes," you must complete the Scrap Metal Dealer Registration Form (Form SMD-1) and proceed to question 14.]
 No [Proceed to question 14.]

14. The number of pages attached and included in this application is: 3

15. The requested effective date is: the date & time of filing in the Secretary of State's Office
 [Requested date may not be earlier than filing nor later than 90 days after filing in our office.]
 the following date _____ and time _____

16. Contact and Signature Information* (See below Important Legal Notice Regarding Signature):

a.	Alvyn A. Schopp	(313) 357-7310
	_____	_____
	Contact Name	Phone Number
b.	Alvyn A. Schopp	Chief Administrative Officer and Regional Vice President
	_____	_____
	Print or type name of signer	Title / Capacity of Signer
c.		April 28, 2014
	_____	_____
	Signature	Date

***Important Legal Notice Regarding Signature:** Per West Virginia Code §31B-2-209. Liability for false statement in filed record. If a record authorized or required to be filed under this chapter contains a false statement, one who suffers loss by reliance on the statement may recover damages for the loss from a person who signed the record or caused another to sign it on the person's behalf and knew the statement to be false at the time the record was signed.

Delaware

PAGE 1

The First State

I, JEFFREY W. BULLOCK, SECRETARY OF STATE OF THE STATE OF DELAWARE, DO HEREBY CERTIFY "ANTERO MIDSTREAM LLC" IS DULY FORMED UNDER THE LAWS OF THE STATE OF DELAWARE AND IS IN GOOD STANDING AND HAS A LEGAL EXISTENCE SO FAR AS THE RECORDS OF THIS OFFICE SHOW, AS OF THE TWENTY-NINTH DAY OF APRIL, A.D. 2014.

AND I DO HEREBY FURTHER CERTIFY THAT THE ANNUAL TAXES HAVE NOT BEEN ASSESSED TO DATE.

5466900 8300

140532521

You may verify this certificate online
at corp.delaware.gov/authver.shtml




Jeffrey W. Bullock, Secretary of State
AUTHENTICATION: 1328067

DATE: 04-29-14

**Attachment B.
Area Map**



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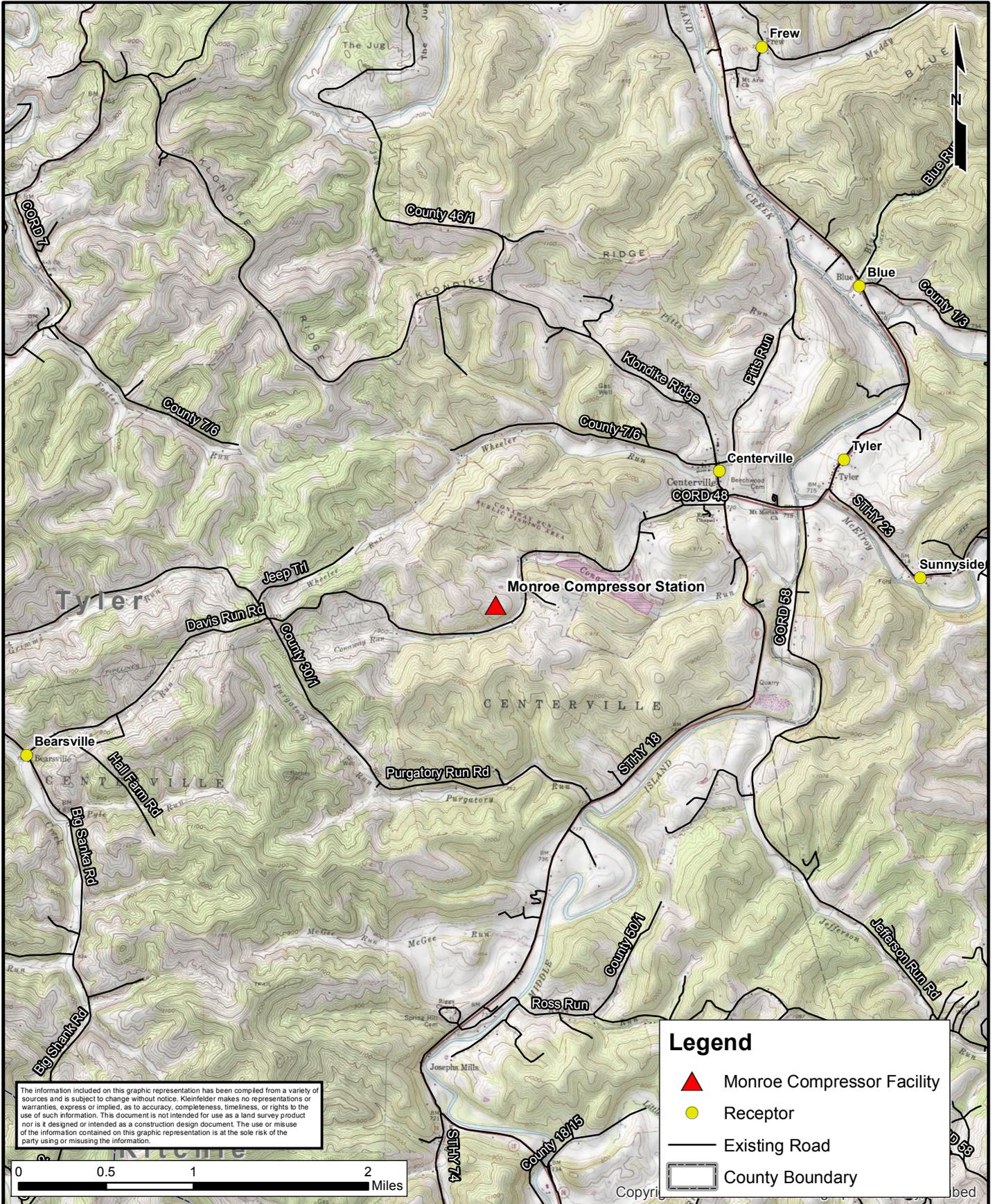


Source: Esri, DigitalGlobe, CNES/Airbus DS, USDA, swisstopo, and the GIS User Community

Legend

- Monroe Compressor Facility
- Receptor
- Existing Road
- County Boundary

<p>KLEINFELDER Bright People. Right Solutions. www.kleinfelder.com</p>	PROJECT NO. 139193/1	Antero Midstream LLC	FIGURE
	DRAWN: 10/21/2014		
	DRAWN BY: A.Leonard	Monroe Compressor Station Tyler County, West Virginia	
	CHECKED BY: K.Meszaros		
FILE NAME: MonroeCompressor_Receptor.mxd			



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Legend

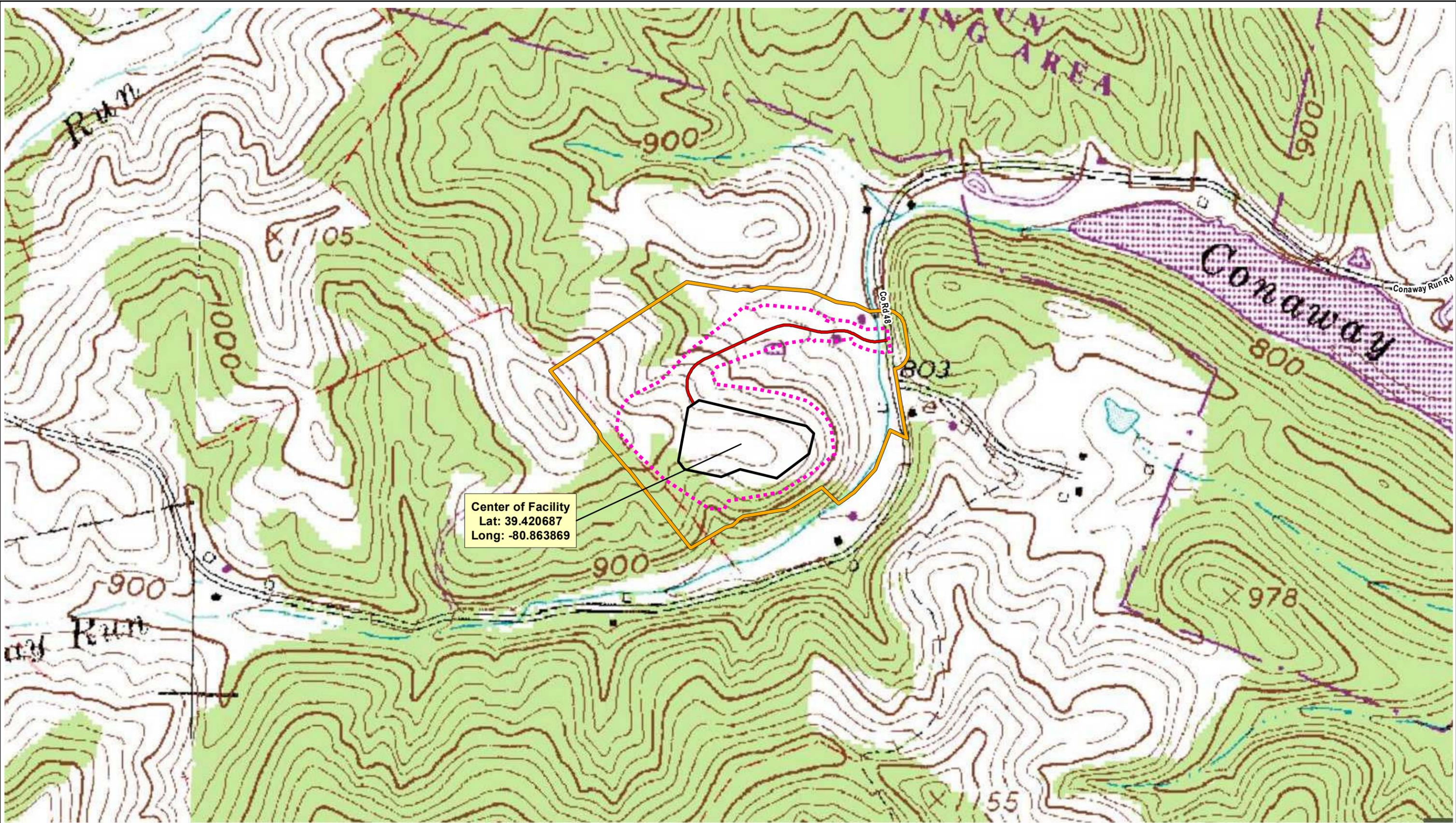
- ▲ Monroe Compressor Facility
- Receptor
- Existing Road
- ▭ County Boundary

PROJECT NO.	139193/1
DRAWN:	10/21/2014
DRAWN BY:	A. Leonard
CHECKED BY:	K. Meszaros
FILE NAME:	MonroeCompressor_Topo_v3.mxd

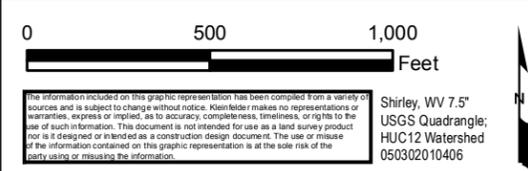
Antero Midstream LLC

Monroe Compressor Station
Tyler County, West Virginia

FIGURE



Center of Facility
 Lat: 39.420687
 Long: -80.863869



- Legend**
- ⋯ Limit of Disturbance (19.70 ac)
 - AOI (45.82 ac)
 - Proposed Access Road (0.26 mi)
 - Proposed Compressor Facility



PROJECT NO.	00137885.000A
DRAWN:	3/6/2014
DRAWN BY:	GHB
CHECKED BY:	TV
FILE NAME:	MonroeCF_WDSIR_Map1.mxd

Project Location Map

Monroe Compressor Facility
Antero Resources Corporation
Tyler County, WV

FIGURE
1

**Attachment C.
Installation and Startup Schedule**

Monroe Compressor Station – Installation and Startup Schedule

The Monroe Compressor Station is an existing facility located in Tyler County, WV, approximately 2.0 miles west of Alma, WV. Equipment is currently installed and operating per permit R13-3184A. The proposed equipment is scheduled to be installed and operational around April 1, 2016.

**Attachment D.
Regulatory Discussion**

Monroe Compressor Station – Regulatory Discussion

Federal Regulations

40 CFR Part 60 – Standards of Performance for New Stationary Sources

- I. *Subpart Kb - Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984.*

Applicability: Subpart Kb applies to volatile organic liquid storage tanks with a capacity greater than or equal to 75 m³ (§60.110b(a)). Since all storage tanks at the Monroe Compressor Station are 64 m³, Subpart Kb does not apply.

- II. *Subpart GG - Standards of Performance for Stationary Gas Turbines*

Applicability: Subpart GG applies to all stationary gas turbines with a heat input at peak load equal to or greater than 10 million BTU per hour based on the lower heating value of the fuel (§60.330(a)). Since the microturbine generators at the Monroe Compressor Station have a heat input rating less than 10 million Btu per hour, Subpart GG does not apply.

- III. *Subpart KKK - Standards of Performance for Equipment Leaks of VOC from Onshore Natural Gas Processing Plants for Which Construction, Reconstruction, or Modification Commenced After January 20, 1984, and on or Before August 23, 2011.*

Applicability: Subpart KKK applies to facilities built or modified before August 23, 2011, so Subpart KKK will not apply as the Monroe Compressor Station was constructed in 2014.

- IV. *Subpart LLL - Standards of Performance for SO₂ Emissions from Onshore Natural Gas Processing for Which Construction, Reconstruction, or Modification Commenced After January 20, 1984, and on or Before August 23, 2011.*

Applicability: Subpart LLL applies to facilities built or modified before August 23, 2011, so Subpart LLL will not apply as the Monroe Compressor Station was constructed in 2014.

- V. *Subpart JJJJ - Standards of Performance for Stationary Spark Ignition Internal Combustion Engines*

Applicability: Subpart JJJJ applies to rich burn engines that were ordered after June 12, 2006 and manufactured on or after July 1, 2007 for engines with maximum power greater than or equal to 500 hp (§60.4230(a)(4)(i)). Thus, Subpart JJJJ applies to the Monroe Compressor Station as the compressor engines were ordered after June 12, 2006 and manufactured after July 1, 2007.

VI. *Subpart KKKK - Standards of Performance for Stationary Combustion Turbines*

Applicability: Subpart KKKK applies to all stationary combustion turbines with a heat input at peak load equal to or greater than 10 million BTU per hour based on the higher heating value of the fuel (§60.4305(a)). Since the microturbine generators at the Monroe Compressor Station have a heat input rating less than 10 million Btu per hour, Subpart KKKK does not apply.

VII. *Subpart OOOO - Standards of Performance for Crude Oil and Natural Gas Production, Transmission, and Distribution*

Applicability: Subpart OOOO applies to reciprocating compressor facilities that were constructed, modified, or reconstructed after August 23, 2011 (§60.5365(c)). Additionally, Subpart OOOO applies to storage vessel affected facilities with individual tank emissions greater than 6 tons per year (§60.5365(e)). Thus, Subpart OOOO applies to the Monroe Compressor Station as it was constructed after August 23, 2011 and has reciprocating compressors and a settling tank with uncontrolled VOC potential to emit greater than six (6) tons per year. The pneumatic controllers installed at Monroe Compressor Station are air-actuated and therefore exempt from the requirements of this subpart.

40 CFR Part 61 – National Emission Standards for Hazardous Air Pollutants

I. *Subpart V – National Emission Standard for Equipment Leaks (Fugitive Emission Sources)*

Applicability: Subpart V applies to components such as compressors, valves, and pumps that are intended to operate in volatile hazardous air pollutant (VHAP) service (§61.240(a)). VHAP service means that a component contains or contacts a fluid that is at least 10 percent by weight a VHAP. Subpart V does not apply to the Monroe Compressor Station because none of the components have fluid (natural gas, water, or condensate) that is over 10 percent by weight of any VHAP.

40 CFR Part 63 – National Emission Standards for Hazardous Air Pollutants for Source Categories

I. *Subpart HH – National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities*

Applicability: Subpart HH applies to oil and natural gas production facilities that are a major or area source of HAP emissions, and that process, upgrade, or store hydrocarbon liquids or natural gas prior to the transmission and storage source category (§63.760(a)). Subpart HH does apply to the Monroe Compressor Station, and because it is an area source of HAP emissions, the two (2) TEG dehydrators are applicable sources under Subpart HH (§63.760(b)(2)). However, actual benzene emissions from

the dehydrators at the Monroe Compressor Station are less than 1 ton per year, so both dehydrators are exempt from all requirements except recordkeeping (§63.764(e)(1)(ii)).

II. Subpart HHH – National Emission Standards for Hazardous Air Pollutants from Natural Gas Transmission and Storage Facilities

Applicability: Subpart HHH applies to natural gas transmission and storage facilities that are a major source of HAP emissions (§63.1270(a)). Subpart HHH does not apply to the Monroe Compressor Station as it is not a major source of HAP emissions. Further, the Monroe Compressor Station is prior to the gas transmission and storage phase.

III. Subpart EEEE – National Emission Standards for Hazardous Air Pollutants: Organic Liquids Distribution (Non-Gasoline)

Applicability: Subpart EEEE applies to organic liquids distribution operations that are located at major source of HAP emissions (§63.2334(a)). Subpart EEEE does not apply to the Monroe Compressor Station as it is not a major source of HAP emissions.

IV. Subpart YYYY – National Emission Standards for Hazardous Air Pollutants for Stationary Combustion Turbines

Applicability: Subpart YYYY applies to stationary combustion turbines located at major sources of HAP emissions (§63.6085(a)). Since the Monroe Compressor Station is not a major source of HAP emissions, Subpart YYYY does not apply.

V. Subpart ZZZZ - National Emission Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines

Applicability: Subpart ZZZZ applies to stationary RICE at a major or area source of HAP emissions (§63.6585). Subpart ZZZZ applies to the Monroe Compressor Station as the compressor engines are new RICE. The engines will meet Subpart ZZZZ by meeting 40 CFR Part 60, Subpart JJJJ as the Monroe Compressor Station is an area source of HAP emissions (§63.6590(c)(1)).

VI. Subpart DDDDD – National Emission Standards for Hazardous Air Pollutants for Industrial, Commercial, and Institutional Boilers and Process Heaters

Applicability: Subpart DDDDD applies to process heaters at a major source of HAP emissions (§63.7485). Subpart DDDDD does not apply to the Monroe Compressor Station as it is not a major source of HAP emissions.

West Virginia State Regulations

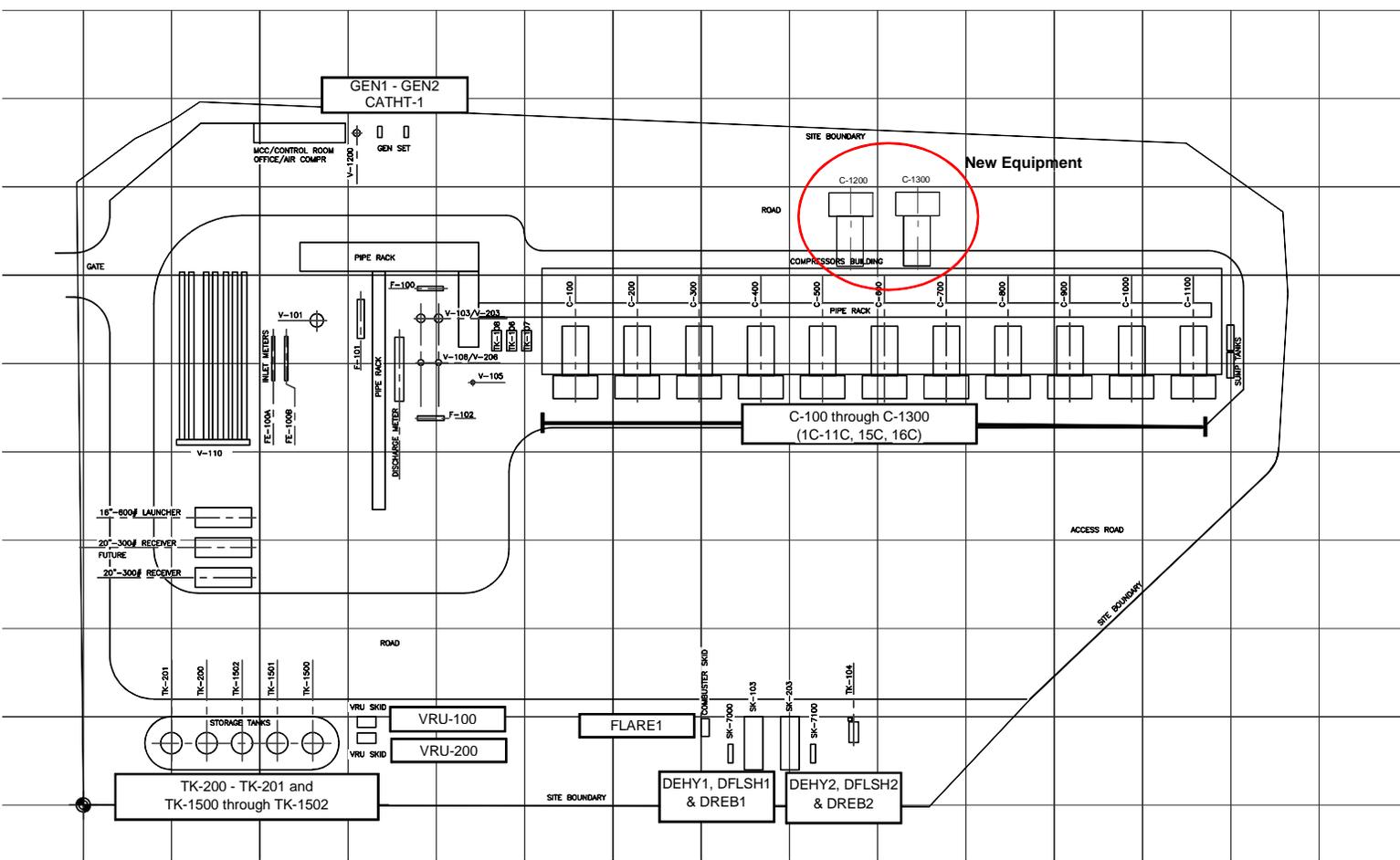
Title 45 Legislative Rule – Division of Environmental Protection, Office of Air Quality

The following Title 45 Legislative Rules will be applicable to the Monroe Compressor Station:

- I. *45CSR2 – To Prevent and Control Particulate Air Pollution from Combustion of Fuel in Indirect Heat Exchangers*
- II. *45CSR2A – Testing, Monitoring, Recordkeeping and Reporting Requirements Under 45CSR2*
- III. *45CSR4 – To Prevent and Control the Discharge of Air Pollutants into the Open Air Which Causes or Contributes to an Objectionable Odor or Odors*
- IV. *45CSR6 – Control of Air Pollution from Combustion of Refuse*
- V. *45CSR8 – Ambient Air Quality Standards*
- VI. *45CSR11 – Prevention of Air Pollution Emergency Episodes*
- VII. *45CSR13 – Permits for Construction, Modification, Relocation and Operation of Stationary Sources of Air Pollutants, Notification Requirements, Administrative Updates, Temporary Permits, General Permits, and Procedures for Evaluation*
- VIII. *45CSR16 – Standards of Performance for New Stationary Sources Pursuant to 40 CFR, Part 60*
- IX. *45CSR20 – Good Engineering Practice as Applicable to Stack Heights*
- X. *45CSR22 – Air Quality Management Fee Program*
- XI. *45CSR27 – To Prevent and Control the Emissions of Toxic Air Pollutants*
- XII. *45CSR33 – Acid Rain Provisions and Permits*
- XIII. *45CSR34 – Emission Standards for Hazardous Air Pollutants for Source Categories Pursuant to 40 CFR, Part 63*
- XIV. *45CSR38 – Provisions for Determination of Compliance with Air Quality Management Rules*
- XV. *45CSR42 – Greenhouse Gas Emissions Inventory*

**Attachment E.
Plot Plan**

10.116'



EQUIPMENT	DESCRIPTION
C-100	COMPRESSOR SKID JGK/4
C-200	COMPRESSOR SKID JGK/4
C-300	COMPRESSOR SKID JGK/4
C-400	COMPRESSOR SKID JGK/4
C-500	COMPRESSOR SKID JGK/4
C-600	COMPRESSOR SKID JGK/4
C-700	COMPRESSOR SKID JGK/4
C-800	COMPRESSOR SKID JGK/4
C-900	COMPRESSOR SKID JGK/4
C-1000	COMPRESSOR SKID JGK/4
C-1100	COMPRESSOR SKID JGK/4
F-100	INLET COALESCING FILTER SEPARATOR
F-101	DISCHARGE COALESCING FILTER SEPARATOR
F-102	DISCHARGE COALESCING FILTER SEPARATOR
FE-100A	INLET METER
FE-100B	INLET METER
L-1	DISCHARGE METER
PR-100	PIG LAUNCHER
PR-200	PIG RECEIVER FUTURE
SK-103	DEHY SKID
SK-203	DEHY SKID
SK-7000	BTEX SKID
SK-7100	BTEX SKID
TK-104	TED MAKE UP TANK
TK-109	COOLANT STORAGE TANK
TK-107	ENGINE LUBE OIL TANK
TK-108	COMPRESSOR LUBE OIL TANK
TK-200	CONDENSATE TANK
TK-201	CONDENSATE TANK
TK-1500	PRODUCED WATER TANK
TK-1501	PRODUCED WATER TANK
TK-1502	WATER/ORGANIC SETTLING TANK
V-101	INLET SCRUBBER
V-103	DEHY TOWER
V-105	FUEL GAS SCRUBBER
V-108	DISCHARGE VERTICAL SCRUBBER
V-110	INLET SLAG CATCHER
V-203	DEHY TOWER
V-206	DISCHARGE VERTICAL SCRUBBER
V-1200	STARTING AIR VOLUME BOTTLE

REFERENCE DRAWINGS	No	REVISIONS	BY	CHKD	PM	DATE

ARCO RESOURCES APPALACHIAN CORP.

 WEST VIRGINIA

 MONROE COMPRESSOR STATION

 PLOT PLAN

PLOT NUMBER 13MONROECS	DRAWING NUMBER MON-PP-4100	SCALE 1" = 30'-0"	REVISION
---------------------------	-------------------------------	----------------------	--------------

ISSUED FOR PERMIT 1/30/14

**Attachment F.
Process Flow Diagram**

**Attachment G.
Process Description**

Monroe Compressor Station – Process Description

The Monroe Compressor Station is located in Tyler County, West Virginia. Gas from surrounding pipelines enters the facility through one (1) receiver and associated slug catcher. From there, the gas is metered and routed through a scrubber and filter separator. Any produced liquids from the scrubber or separator are sent to the 400 barrel settling tank (TK-1502). Gas from the filter separator is sent to one (1) of thirteen (13) 1680 hp Waukesha compressor engines (C-100 – C-1300). The thirteen (13) compressor engines are controlled with NSCR catalysts and air-fuel ratio controllers (1C – 11C, 15C, 16C). Produced fluids are routed to the settling tank and gas going to one of the two (2) TEG dehydrators.

Each TEG dehydrator (DEHY1 – DEHY2) contains a flash gas tank and 1.5 MMBtu/hr reboiler. Each dehydrator has a design rate of 72.5 MMscf/day. Within the dehydrator unit, vent gas from the flash gas tank (DFLSH1 – DFLSH2) is routed to the reboiler (DREB1 – DREB2) and used as fuel. In the case where the flash tank gas cannot be used by the reboiler due to excess gas or the reboiler being offline, the gas will be sent to the VRUs (VRU-100 and VRU-200) via the storage tanks (TK-1500 – TK-1502, TK-200 – TK-201) and thus controlled by 98%. Emissions from each reboiler are routed to the atmosphere. The dehydrator still vents (DEHY1 – DEHY2) are controlled by a flare with at least 98% control efficiency (FLARE1). Produced fluids from the dehydrator are routed to the settling tank. The dry gas from the dehydration process is either routed to a fuel gas scrubber, metered, and routed to the compressors as fuel gas or metered and sent to plant discharge.

All produced fluids enter one (1) 400 barrel settling tank (TK-1502) where the fluids settle out as either condensate or produced water. The produced water goes to two (2) 400 barrel produced water tanks (TK-1500 – TK-1501) and the condensate goes to two (2) 400 barrel condensate tanks (TK-200 – TK-201). Flashing only occurs at the settling tank as the fluids stabilize in the settling tank before going to the other storage tanks. All five (5) tanks are connected to a vapor recovery unit (VRU-100) where tank vapors are collected and recycled back into the gas system right before the initial filter scrubber. A second vapor recovery unit (VRU-200) is also connected to the tank as a backup unit. The produced fluids are trucked out via tanker trucks as needed (LDOUT1). The anticipated production is 150 barrels per day of condensate and 45 barrels per day of produced water.

Two (2) natural gas microturbine generators, each rated at 600 kWe, supply power to the facility (GEN1 – GEN2). Each 600 kWe generator is actually comprised of three smaller units, each rated at 200 kWe. All generators (six 200 kWe) are wired together and operation between individual 200 kWe engines will rotate based on functionality of engines. No more than 600 kWe will be operational at any given time, except when units are being switched. Each individual engine will continuously record hours of operation and will be used interchangeably. A small 24,000 Btu/hr catalytic heater (CATHT-1) is used to heat fuel to power the generators.

There are also small storage tanks (1,000 to 2,000 gallons) located at the facility. Their ID number, description, and exact size are listed in the table below.

Fugitive emissions from component leaks and emissions from venting or blowdown events also occur.

Tag Number	Description	Gallons
TK-300	Compressor Skid Oily Water Tank	1,000
TK-301	Used Oil Tank	1,000
TK-104	TEG Make-Up Tank	1,000
TK-106	Compressor Coolant Tank	2,000
TK-107	Engine Lube Oil Tank	2,000
TK-108	Compressor Lube Oil Tank	2,000

Attachment H.
Material Safety Data Sheets



SAFETY DATA SHEET

Material Name: Produced Water

US GHS

SYNONYMS: Produced Brine Water, Brine, Brine Water, Formation Water

***** Section 1 – PRODUCT AND COMPANY IDENTIFICATION *****

PRODUCT NAME:	Produced Water	EMERGENCY PHONE:	(800) 878-1373
PRODUCT CODES:	Mixture	AFTER HOURS:	(800) 878-1373
PRODUCER:	Antero Resources		
ADDRESS:	1615 Wynkoop Street Denver, Colorado 80202	CHEMTREC PHONE:	(800) 424-9300

***** Section 2 – HAZARDS IDENTIFICATION *****

GHS Classification:
Eye Irritant – Category 2A.

GHS LABEL ELEMENTS
Symbol(s)



Signal Word
Warning

Hazard Statements
Causes serious eye irritation

Precautionary Statements
Prevention
Wear protective gloves/protective clothing/eye protection/face protection.

Response
If on SKIN (or hair): Rinse skin with water / shower. Remove / Take off all contaminated clothing immediately.

SAFETY DATA SHEET

Material Name: Produced Water

US GHS

If in EYES: Rinse cautiously with water for at least fifteen (15) minutes. Remove Contact Lenses, if present and easy to do. Continue rinsing.

If EYE irritation persists, get medical advice / attention.

Storage

Store in a secure area.

Disposal

Dispose of contents/containers in accordance with regulations.

***** Section 3 – COMPOSITION / INFORMATION ON INGREDIENTS *****

CAS #	Component	Percent
7732-18-5	Water	80
7647-14-5	Sodium Chloride	20

Because brine water is a natural product, composition can vary greatly.

***** Section 4 – FIRST AID MEASURES *****

First Aid: Eyes

Flush eyes with clean running water for at least fifteen (15) minutes. If irritation or redness develops from exposure, following flushing, seek medical attention.

First Aid: Skin

First aid is not required, normally. However, it is a good practice to wash any chemical from the skin.

First Aid: Ingestion (Swallowing)

First aid is not required, normally. If spontaneous vomiting occurs, lean the victim forward to reduce the risk of aspiration. Monitor for breathing difficulties. If symptoms develop, seek medical attention.

First Aid: Inhalation (Breathing)

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

SAFETY DATA SHEET

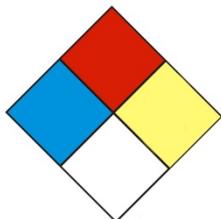
Material Name: Produced Water

US GHS

Most important symptoms and effects

None known or anticipated.

*** Section 5 – FIRE FIGHTING MEASURES ***



NFPA 704 Hazard Class

Health: 1 Flammability: 0 Instability: 0 (0=Minimal, 1=Slight, 2=Moderate, 3=Serious, 4=Severe)

General Fire Hazards

No fire hazards are expected.

General Fire Hazards

No unusual fire or explosion hazards are expected. If container is not properly cooled, it can rupture in the heat of a fire.

Extinguishing Media

The material is non-flammable. Use extinguishing agent suitable for the type of surrounding fire.

Unsuitable Extinguishing Media

None

Fire Fighting Equipment / Instructions

Small fires in the beginning stage may typically be extinguished using handheld portable fire extinguishers and other firefighting equipment. Isolate area around container involved in fire and keep unauthorized personnel out. Stop spill/release if it can be done safely. Move undamaged containers from the immediate hazard area if it can be done safely. Cool equipment exposed to fire with water, if it can be done safely.

Hazardous Combustion Products

None Anticipated. See Section 9 for Flammable Properties including Flash Point and Flammable (Explosive) Limits

SAFETY DATA SHEET

Material Name: Produced Water

US GHS

*** Section 6 – ACCIDENTAL RELEASE MEASURES ***
--

Recovery and Neutralization

Contain and stop the source of the spill, if safe to do so.

Materials and Methods for Clean-Up

Notify relevant authorities in accordance with all applicable regulations. Immediate cleanup of any spill is recommended. Dike far ahead of spill for later recovery or disposal. Absorb spill with inert material such as sand or vermiculite, and place in suitable container for disposal. If spilled on water remove with appropriate methods (e.g. skimming, booms or absorbents). In case of soil contamination, remove contaminated soil for remediation or disposal, in accordance with local regulations.

Recommended measures are based on the most likely spillage scenarios of this material. However, local conditions and regulations may influence or limit the choice of appropriate actions to be taken. See Section 13 for information on appropriate disposal.

Emergency Measures

The material is not considered hazardous. Nevertheless, evacuate nonessential personnel and secure the area. Stay upwind and uphill, if possible.

Personal Precautions and Protective Equipment

Stay upwind and away from the spill/release. Avoid direct contact with the material. For large spillages, notify persons downstream of the spill/release. Isolate the immediate hazard area and keep unauthorized personnel out. Response and clean-up crews must be properly trained and must utilize proper protective equipment (see Section 8).

Environmental Precautions

Protect bodies of water by diking or absorbents, if possible. Do not flush down sewer or drainage systems. Use water sparingly to minimize environmental contamination and reduce disposal requirements. If a spill occurs on water, notify appropriate authorities and advise shipping of any hazard.

Prevention of Secondary Hazards

None

SAFETY DATA SHEET

Material Name: Produced Water

US GHS

*** Section 7 – HANDLING AND STORAGE ***

Handling Procedures

Wash thoroughly after handling. Use good personal hygiene practices and wear appropriate personal protective equipment (see section 8).

Do not enter confined spaces such as tanks or pits without following proper entry procedures such as ASTM D-4276 and 29 CFR 1910.146. Do not wear contaminated clothing or shoes.

Storage Procedures

Keep container(s) tightly closed and properly labeled. Use and store this material in cool, dry, well ventilated areas. Store only in approved containers. Keep away from any incompatible material (see Section 10). Protect container(s) against physical damage.

Incompatibilities

Keep away from excessive heat to prevent rupture of container.

*** Section 8 – EXPOSURE CONTROLS / PERSONAL PROTECTION ***

Component Exposure Limits

Water (7732-18-5)

ACGIH: Not listed

Sodium Chloride (7647-14-5)

ACGIH: Not listed

Engineering Measures

If current ventilation practices are not adequate to maintain airborne concentrations below the established exposure limits, additional engineering controls may be required.

Personal Protective Equipment: Respiratory

Emergencies or conditions that could result in significant airborne exposures may require the use of NIOSH approved respiratory protection. An industrial hygienist or other appropriate health and safety professional should be consulted for specific guidance under these situations.

A respiratory protection program that meets or is equivalent to OSHA 29 CFR

SAFETY DATA SHEET

Material Name: Produced Water

US GHS

1910.134 and ANSI Z88.2 should be followed whenever workplace conditions warrant a respirator's use.

Personal Protective Equipment: Skin and Hands

The use of skin protection is not normally required; however, good industrial hygiene practice suggests the use of gloves or other appropriate skin protection whenever working with chemicals.

Personal Protective Equipment: Eyes

Safety glasses or goggles that meet or exceed ANSI Z-87.1 are recommended where there is a possibility of splashing or spraying.

Hygiene Measures

Emergency eye wash capability should be available in the near proximity to operations presenting a potential splash exposure. Use good personal hygiene practices. Avoid repeated and/or prolonged skin exposure. Wash hands before eating, drinking, smoking, or using toilet facilities. Promptly remove contaminated clothing and launder before reuse.

*** Section 9 – PHYSICAL AND CHEMICAL PROPERTIES ***

Appearance:	Clear to Brown	Odor:	Salty
Physical State:	Liquid	pH:	ND
Vapor Pressure:	< 0.36 psia @ 70°F / 21.1°C	Vapor Density:	> 1
Boiling Point:	212°F / 100°C	Melting Point:	2.4°F / -16.5°C
Solubility (H2O):	Complete	Specific Gravity:	1.1 @ 68°F / 20°C
Evaporation Rate:	Variable	VOC:	ND
Octanol / H2O Coeff.:	ND	Flash Point:	ND
Flash Point Method:	ND	Upper Flammability Limit:	ND
Lower Flammability Limit: (LFL):	ND	(UFL):	
Auto Ignition:	ND	Burning Rate:	ND

SAFETY DATA SHEET

Material Name: Produced Water

US GHS

*** Section 10 – CHEMICAL STABILITY & REACTIVITY INFORMATION ***

Chemical Stability

This is a stable material.

Hazardous Reaction Potential

Will react with alkali and alkaline metals to form flammable hydrogen gas.

Conditions to Avoid

Avoid contact with alkali metals (lithium, sodium, potassium), alkaline metals (beryllium, magnesium, calcium, strontium, and barium), and metallic hydrides like lithium aluminum hydride.

Hazardous Decomposition Products

Not anticipated under normal conditions of use.

Hazardous Polymerization

Not known to occur.

*** Section 11 – TOXICOLOGICAL INFORMATION ***

Acute Toxicity

A: General Product Information

Unlikely to be harmful.

B. Component Analysis – D50/LC50

Water (7732-18-5)

Oral LD50 Rat 90 g/kg

Sodium Chloride (7647-14-5)

Oral LD50 Rat 3 g/kg

Potential Health Effects: Skin Corrosion Property / Stimulativeness

May cause skin irritation with prolonged or repeated contact. Not expected to be a skin sensitizer.

Potential Health Effects: Eye Critical Damage / Stimulativeness

Contact with eyes may cause moderate irritation.

SAFETY DATA SHEET

Material Name: Produced Water

US GHS

Potential Health Effects: Ingestion

Ingestion may result in nausea, vomiting, diarrhea, abdominal cramps, and dehydration (thirst).

Potential Health Effects: Inhalation

No information available on the mixture. However, none of the components have been classified for respiratory sensitization (or are below the concentration threshold for classification).

Generative Cell Mutagenicity

Not expected to cause genetic effects.

Carcinogenicity

General Product Information

Not expected to cause cancer. This substance is not listed as a carcinogen by IARC, NTP or OSHA.

Reproductive Toxicity

This product is not reported to have any reproductive toxicity effects.

Specified Target Organ General Toxicity: Single Exposure

This product is not reported to have any specific target organ general toxicity single exposure effects.

Specified Target Organ General Toxicity: Repeated Exposure

This product is not reported to have any specific target organ general toxicity multiple exposure effects.

Aspiration Respiratory Organs Hazard

The major health threat of ingestion occurs from the danger of aspiration (breathing) of liquid drops into the lungs, particularly from vomiting. Aspiration may result in chemical pneumonia (fluid in the lungs), severe lung damage, respiratory failure and even death.

*** Section 12 – ECOLOGICAL INFORMATION ***
--

Ecotoxicity

A: General Product Information

Keep out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

SAFETY DATA SHEET

Material Name: Produced Water

US GHS

Persistence / Degradability

No information available

Bioaccumulation

No information available

Mobility in Soil

No information available

*** Section 13 – DISPOSAL CONSIDERATIONS ***

Waste Disposal Instructions

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

Disposal of Contaminated Containers or Packaging

Recover or recycle if possible. It is the responsibility of the generator to determine the toxicity and physical properties of the material generated so as to properly classify the waste and ensure disposal methods comply with applicable regulations.

This material, if discarded as produced, is not a RCRA "listed" hazardous waste, and is not believed to exhibit characteristics of hazardous waste. Consult state and local regulations regarding the proper disposal of this material. Do not dispose of brine water by draining onto the ground. This will result in soil and groundwater contamination. Waste arising from spillage or tank cleaning should be disposed of in accordance with applicable regulations.

Container contents should be completely used and containers should be emptied prior to discard. Container rinsate should not be considered a RCRA hazardous waste but must be disposed of with care and in full compliance with federal, state and local regulations. Larger empty containers, such as drums, should be returned to the distributor or to a qualified drum reconditioner. To assure proper disposal of smaller empty containers, consult with state and local regulations and disposal authorities.

*** Section 14 – TRANSPORTATION INFORMATION ***

DOT Information

Shipping Description: Not Regulated

UN #: Not Regulated

SAFETY DATA SHEET

Material Name: Produced Water

US GHS

*** Section 15 – REGULATORY INFORMATION ***

CERCLA/SARA – Section 302 Extremely Hazardous Substances and TPQs (in pounds):

This material does not contain any chemicals subject to the reporting requirements of SARA 302 and 40 CFR 372,

CERCLA/SARA – Section 313 and 40 CFR 372):

This material does not contain any chemicals subject to the reporting requirements of SARA 313 and 40 CFR 372.

EPA (CERCLA) Reportable Quantity (in pounds):

This material does not contain any chemicals with CERCLA Reportable Quantities.

State Regulations

Component Analysis

The following components appear on one or more of the following state hazardous substances list.

California Proposition 65:

This material does not contain any chemicals that are known to the State of California to cause cancer, birth defects or other reproductive harm at concentrations that trigger the warning requirements of California Proposition 65.

National Chemical Inventories:

All components are either listed on the US TSCA Inventory, or are not regulated under TSCA.

U.S. Export control classification Number: EAR99.

*** Section 16 – OTHER INFORMATION ***

NFPA® Hazard Rating

Health	1
Fire	0
Reactivity	0

HMIS® Hazard Rating

Health	1	Slight
Fire	0	Minimal
Physical	0	Minimal

SAFETY DATA SHEET

Material Name: Produced Water

US GHS

Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act; ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

Literature References

None

Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: January 28, 2014

Date of Last Revision: March 4, 2014

End of Sheet

Material Name: Natural Gas Condensate

US GHS

SYNONYMS: Drips; Condensate; Field Condensate; Gas Well Condensate; High Pressure Inlet Liquids; Lease Condensate; Natural Gas Liquids; Pipeline Liquids

*** Section 1 – PRODUCT AND COMPANY IDENTIFICATION ***

PRODUCT NAME: Natural Gas Condensate EMERGENCY PHONE: (800) 878-1373

PRODUCT CODES: 64741-47-5 AFTER HOURS: (800) 878-1373

PRODUCER: Antero Resources

ADDRESS: 1615 Wynkoop Street CHEMTREC PHONE: (800) 424-9300

Denver, Colorado 80202

*** Section 2 – HAZARDS IDENTIFICATION ***

GHS Classification:

- Flammable Liquids – Category 2.
- Acute Toxicity Inhalation – Category 3
- Germ Cell Mutagenicity – Category 1B
- Carcinogenicity – Category 1A
- Specific Target Organ Systemic Toxicity (STOT) – Single Exposure Category 3
- Specific Target Organ Systemic Toxicity (STOT) – Repeat Exposure Category 1
- Aspiration Toxicity – Category 1
- Toxic to the Aquatic Environment Acute – Category 3

GHS LABEL ELEMENTS

Symbol(s)



Signal Word

Danger

SAFETY DATA SHEET

Material Name: Natural Gas Condensate

US GHS

Hazard Statements

Highly flammable liquid and vapor.

Toxic if inhaled.

May cause genetic defects.

May cause cancer.

May cause respiratory irritation.

May cause drowsiness or dizziness.

May cause damage to organs (liver, kidneys, blood, nervous system, and skin) through prolonged or repeated exposure.

May be fatal if swallowed and enters airways.

Harmful to aquatic life.

Precautionary Statements

Prevention

Keep away from heat/sparks/open flames/hot surfaces. No smoking.

Keep container tightly closed.

Ground/bond container and receiving equipment.

Use explosion-proof electrical/ventilating/lighting equipment.

Use only non-sparking tools.

Take precautionary measures against static discharge.

Wear protective gloves/protective clothing/eye protection/face protection.

Do not breathe gas/mist/vapors/spray.

Do not handle until all safety precautions have been read and understood.

Wash thoroughly after handling.

Do not eat, drink or smoke when using this product.

Use only outdoors or in a well-ventilated area.

Avoid release to the environment.

Response

If on SKIN (or hair): Wash with plenty of soap and water. Remove / Take off all contaminated clothing immediately. Rinse skin with water/shower.

If INHALED: Remove victim to fresh air and keep comfortable for breathing. Call a poison center/doctor if the victim feels unwell.

If SWALLOWED: Immediately call a poison center or doctor / physician. Do not induce vomiting.

If exposed or concerned: Get medical advice/attention.

In case of fire: Use water spray, fog or fire-fighting foam.

Storage

Store in a well-ventilated place. Keep cool.

Store in a secure area.

SAFETY DATA SHEET

Material Name: Natural Gas Condensate

US GHS

Disposal

Dispose of contents/containers in accordance with local/regional/national/international regulations.

*** Section 3 – COMPOSITION / INFORMATION ON INGREDIENTS ***

CAS #	Component	Percent
111-65-9	Octanes	25 - 95
142-82-5	Heptanes	25 - 95
110-54-3	Hexanes as n-Hexane	25 - 95
109-66-0	Pentanes as n-Pentane	5 - 70
106-97-8	N-butane	0 - 45
74-98-6	Propane	0 - 15
78-84-0	Ethane	0 - 5
71-43-2	Benzene	< 1
108-88-3	Toluene	< 1
1330-20-7	m-,o-,p-Xylene	< 1

Because natural gas condensate is a natural product, composition can vary greatly.

*** Section 4 – FIRST AID MEASURES ***

First Aid: Eyes

Flush eyes with clean running water for at least fifteen (15) minutes. Following flushing, seek medical attention.

First Aid: Skin

Remove contaminated clothing. Wash contaminated areas thoroughly with soap and water or waterless hand cleanser. Obtain medical attention if irritation or redness develops. Wash contaminated clothing before reuse.

First Aid: Ingestion (swallowing)

DO NOT INDUCE VOMITING. Do not give liquids. Obtain immediate medical attention. If spontaneous vomiting occurs, lean the victim forward to reduce the risk of aspiration. Monitor for breathing difficulties. Small amounts of material which enter the mouth should be rinsed out until the taste is dissipated.

SAFETY DATA SHEET

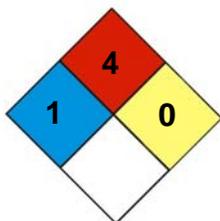
Material Name: Natural Gas Condensate

US GHS

First Aid: Inhalation (breathing)

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

*** Section 5 – FIRE FIGHTING MEASURES ***



NFPA 704 Hazard Class

Health: 1 Flammability: 4 Instability: 0 (0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

General Fire Hazards

See Section 9 for Flammability Properties.

Extremely flammable. Vapors may be ignited rapidly when exposed to heat, spark, open flame, or other source of ignition (e.g., static electricity, pilot lights, mechanical / electrical equipment, and electronic devices such as cell phones, computers, calculators, and pagers which have not been certified as intrinsically safe). Flammable vapors can burn in the open or explode in confined spaces. Vapors are heavier than air, and may travel distances to an ignition source and flash back. Runoff to sewer systems may cause fire or explosion.

Hazardous Combustion Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

Extinguishing Media

SMALL FIRES: Any extinguisher suitable for Class B fires, dry chemical, firefighting foam, water spray, carbon dioxide (CO₂), or other gaseous extinguishing agents. Use caution when applying CO₂ in confined spaces.

LARGE FIRES: Water spray, fog or fire-fighting foam. Water may be ineffective for fighting the fire, but may be used to cool fire-exposed containers.

Unsuitable Extinguishing Media

None

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Fire Fighting Equipment / Instructions

Small fires in the beginning stage may typically be extinguished using handheld portable fire extinguishers and other firefighting equipment. Isolate area around container involved in fire. Cool tanks, shells, and containers exposed to fire and excessive heat with water. For massive fires the use of unmanned hose holders or monitor nozzles may be advantageous to minimize personnel exposure. Major fires may require withdrawal, allowing the tank to burn. Large storage tank fires typically require specially trained personnel and equipment to extinguish the fire, often including the need for properly applied firefighting foam.

Firefighting activities that may result in potential exposure to high heat, smoke or toxic by-products of combustion should require NIOSH/MSHA- approved pressure-demand self-contained breathing apparatus with full face piece and full protective clothing.

* * * Section 6 – ACCIDENTAL RELEASE MEASURES * * *

Recovery and Neutralization

Contain and stop the source of the spill, if safe to do so.

Materials and Methods for Clean-Up

Notify relevant authorities in accordance with all applicable regulations. Immediate cleanup of any spill is recommended. Dike far ahead of spill for later recovery or disposal. Absorb spill with inert material such as sand or vermiculite, and place in suitable container for disposal. If spilled on water remove with appropriate methods (e.g. skimming, booms or absorbents). In case of soil contamination, remove contaminated soil for remediation or disposal, in accordance with local regulations.

Recommended measures are based on the most likely spillage scenarios for this material; however local conditions and regulations may influence or limit the choice of appropriate actions to be taken.

Emergency Measures

Evacuate nonessential personnel and secure all ignition sources. No road flares, smoking or flames in hazard area. Consider wind direction. Stay upwind and uphill, if possible. Vapor cloud may be white, but color will dissipate as cloud disperses. Fire and explosion hazard is still present.

Personal Precautions and Protective Equipment

Response and clean-up crews must be properly trained and must utilize proper protective equipment (see Section 8). Extremely flammable. Spillages of liquid product will create a fire hazard and may form an explosive atmosphere. Keep all sources of

SAFETY DATA SHEET

Material Name: Natural Gas Condensate

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ignition and hot metal surfaces away from spill/release if safe to do so.

The use of explosion-proof electrical equipment is recommended. Stay upwind and away from spill/release. Avoid direct contact with material. For large spillages, notify persons downwind of the spill/release, isolate immediate hazard area and keep unauthorized personnel out. Wear appropriate protective equipment, including respiratory protection, as conditions warrant (see Section 8). See Sections 2 and 7 for additional information on hazards and precautionary measures.

Environmental Precautions

Protect bodies of water by diking, absorbents, or absorbent boom, if possible. Do not flush down sewer or drainage systems, unless system is designed and permitted to handle such material. The use of firefighting foam may be useful in certain situations to reduce vapors. If spill occurs on water notify appropriate authorities and advise shipping of any hazard. Spills into or upon navigable waters, the contiguous zone, or adjoining shorelines that cause a sheen or discoloration on the surface of the water, may require notification of the National Response Center (phone number 800-424-8802).

Prevention of Secondary Hazards

None

*** Section 7 – HANDLING AND STORAGE ***

Handling Procedures

Keep away from flame, sparks and excessive temperatures. Bond and ground containers. Use non-sparking tools. Use only outdoors or in well ventilated areas. Wear protective gloves / clothing and eye / face protection. Wash thoroughly after handling. Use good personal hygiene practices and wear appropriate personal protective equipment (see section 8).

Storage Procedures

Store only in approved containers. Bond and ground containers. Keep away from flame, sparks, excessive temperatures and open flames. Keep containers closed and clearly labeled. Empty product containers or vessels may contain explosive vapors. Do not pressurize, cut, heat, weld or expose containers to sources of ignition.

Store in a well-ventilated area. This storage area should comply with NFPA 30 "Flammable and Combustible Liquid Code". Avoid storage near incompatible materials. The cleaning of tanks previously containing this product should follow API Recommended Practice (RP) 2013 "Cleaning Mobile Tanks In Flammable and Combustible Liquid Service" and API RP 2015 "Cleaning Petroleum Storage Tanks."

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Incompatibilities

Keep away from strong oxidizers, ignition sources and heat.

*** Section 8 – EXPOSURE CONTROLS / PERSONAL PROTECTION ***

Component Exposure Limits

Octanes (111-65-9)

ACGIH: 300 ppm TWA (listed under Octane, all isomers)

Heptanes (142-82-5)

ACGIH: 400 ppm TWA (listed under n-Heptane)

n-Hexane (110-54-3)

ACGIH: 20 ppm TWA (listed under n-Hexane)

n-Pentane (109-66-0)

ACGIH: 600 ppm TWA (listed under Pentane, all isomers)

n-Butane (106-97-8)

ACGIH: 600 ppm TWA (listed under n-Butane)

Propane (74-98-6)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases C1-C4)

Ethane (74-84-0)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases C1-C4)

Benzene (71-43-2)

ACGIH: 0.5 ppm (TWA); NIOSH: 0.1 ppm (TWA); OSHA 1 ppm (TWA)

Toluene (108-88-3)

ACGIH: 20 ppm TWA (listed under Toluene)

m-, o-, p-Xylene (1330-20-7)

ACGIH: 100 ppm TWA (listed under Xylene o, m & p isomers)

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Engineering Measures

Use adequate ventilation to keep vapor concentrations of this product below occupational exposure and flammability limits, particularly in confined spaces. Use explosion-proof equipment and lighting in classified / controlled areas.

Personal Protective Equipment: Respiratory

Use a NIOSH-approved positive-pressure, supplied air respirator with escape bottle or self-contained breathing apparatus (SCBA) for gas concentrations above occupational exposure limits, for potential for uncontrolled release, if exposure levels are not known, or in an oxygen-deficient atmosphere (oxygen content less than 19.5 percent). A respiratory program that meets or is equivalent to OSHA 29 CFR 1910.134 and ANSI Z88.2 should be followed whenever workplace conditions warrant the use of a respirator.

If benzene concentrations equal or exceed applicable exposure limits, OSHA requirements for personal protective equipment, exposure monitoring, and training may apply (29 CFR 1910.1028 – Benzene).

CAUTION: Flammability limits (i.e., explosion hazard should be considered when assessing the need to expose personnel to concentrations requiring respiratory protection.

Personal Protective Equipment: Hands

Gloves constructed of nitrile or neoprene are recommended.

Personal Protective Equipment: Eyes

Safety glasses or goggles are recommended where there is a possibility of splashing or spraying. Eye protection that meets or exceeds ANSI Z.87.1 is recommended. Depending on conditions of use, a face shield may be necessary.

Personal Protective Equipment: Skin and Body

Chemical protective clothing such as of E.I. DuPont TyChem®, Saranex® or equivalent recommended based on degree of exposure. Note: The resistance of specific material may vary from product to product as well as with degree of exposure. Consult manufacturer specifications for further information.

Hygiene Measures

Emergency eye wash capability should be available in the near proximity to operations presenting a potential splash exposure. Use good personal hygiene practices. Avoid repeated and/or prolonged skin exposure. Wash hands before eating, drinking, smoking, or using toilet facilities. Do not use as a cleaning solvent on the skin. Do not use gasoline or solvents (naphtha, kerosene, etc.) for washing this product from

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exposed skin areas. Waterless hand cleaners are effective. Promptly remove contaminated clothing and launder before reuse. Use care when laundering to prevent the formation of flammable vapors which could ignite via washer or dryer. Consider the need to discard contaminated leather shoes and gloves.

*** Section 9 – PHYSICAL AND CHEMICAL PROPERTIES ***

Appearance:	Colorless to straw yellow	Odor:	Aromatic, Gasoline;
Physical State:	Liquid	pH:	ND
Vapor Pressure:	110 – 200 psia (Reid VP) @ 100°F/37.8°C	Vapor Density (air = 1):	> 1
Boiling Point:	Approx. 85 - 437°F (39 – 200°C)	Melting Point:	ND
Solubility (H2O):	Insoluble to slightly soluble	Specific Gravity:	AP 0.62-0.76 (varies)
Evaporation Rate:	High	VOC:	ND
Octanol / H2O Coeff.:	ND	Flash Point:	-40°F -40°C
Flash Point Method:	Tag Closed Cup (TCC)	Upper Flammability Limit:	ND (NFPA Gasoline 7.6)
Lower Flammability Limit:	ND (NFPA Gasoline 1.4)	(UFL):	
(LFL):		Burning Rate:	ND
Auto Ignition:	AP 480°F (250°C)		

*** Section 10 – CHEMICAL STABILITY & REACTIVITY INFORMATION ***

Chemical Stability

This is a stable material.

Hazardous Reaction Potential

Will not occur.

Conditions to Avoid

Keep away from ignition sources and high temperatures.

Hazardous Decomposition Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

SAFETY DATA SHEET

Material Name: Natural Gas Condensate

US GHS

*** Section 11 – TOXICOLOGICAL INFORMATION ***
--

Acute Toxicity

A: General Product Information

Harmful if swallowed.

B. Component Analysis – LD50/LC50

Octanes (111-65-9)

Inhalation LC50 rat = 118,000 mg/m³ / 4H

Heptanes (142-82-5)

Inhalation LC50 rat = 103,000 mg/m³ / 4H

Hexanes as n-Hexane (110-53-3)

Inhalation LC50 rat = 48,000 ppm / 4H

Pentanes as n-Pentane (109-66-0)

Inhalation LC50 rat = 364,000 mg/m³ / 4H

Butanes as n-Butane (106-97-8)

Inhalation LC50 rat 658,000 mg/l / 4H

Propane (74-98-6)

Inhalation LC50 Rat > 800,000 ppm / 0.25H

Ethane (74-84-0)

Inhalation LC50 Rat 658,000 mg/l / 4H

Benzene (71-43-2)

Inhalation LC50 Rat 44,700 mg/m³ /

Toluene (108-88-3)

Inhalation LD50 Rat 12/5 mg/l / 4H

m-, o-, p-Xylene (1330-20-7)

Inhalation LC50 Rat 5000 ppm / 4H

Potential Health Effects: Skin Corrosion Property / Stimulativeness

May cause skin irritation with prolonged or repeated contact. Liquid may be absorbed through the skin in toxic amounts if large areas of skin are exposed repeatedly.

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Potential Health Effects: Eye Critical Damage / Stimulativeness

Contact with eyes may cause moderate irritation.

Potential Health Effects: Ingestion (swallowing)

Ingestion may cause gastrointestinal disturbances, including irritation, nausea, vomiting and diarrhea, and central nervous system (brain) effects similar to alcohol intoxication. In severe cases, tremors, convulsions, loss of consciousness, coma, respiratory arrest, and death may occur.

Potential Health Effects: Inhalation (breathing)

Excessive exposure may cause irritations to the nose, throat, lungs and respiratory tract. Central nervous system (brain) effects may include headache, dizziness, loss of balance and coordination, unconsciousness, coma, respiratory failure, and death.

Respiratory Organs Sensitization / Skin Sensitization

This product is not reported to have any skin sensitization effects.

Generative Cell Mutagenicity

May cause genetic defects. Some crude oils and crude oil fractions have been positive in mutagenicity studies.

Carcinogenicity

A: General Product Information

May cause cancer.

This product contains benzene, although at very low concentrations. Human health studies indicate that prolonged and/or repeated overexposure to benzene may cause damage to the blood-forming system (particularly bone marrow), and serious blood disorders such as aplastic anemia and leukemia. Benzene is listed as a human carcinogen by the NTP, IARC, OSHA and ACGIH.

Exposure to light hydrocarbons in the same boiling range as this product have been associated in animal studies with effects to the central nervous system, peripheral nervous system, liver, and kidneys. The significance of these animal models to predict similar human response is uncertain. Observing good work practices and personal hygiene procedures (Sections 7 and 8) can minimize potential risks to humans.

B: Component Carcinogenicity

Benzene (71-43-2)

ACGIH:	A1 - Confirmed Human Carcinogen
OSHA:	5 ppm STEL (Cancer hazard, Flammable, See 29 CFR 1910.1028, 15 min); 0.5 ppm Action Level; 1 ppm TWA
NIOSH:	potential occupational carcinogen
NTP:	Known Human Carcinogen (Select Carcinogen)

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IARC: Monograph 100F [in preparation]; Supplement 7 [1987]; Monograph 29 [1982] (Group 1 (carcinogenic to humans))

Reproductive Toxicity

This product is not reported to have any reproductive toxicity effects.

Specified Target Organ General Toxicity: Single Exposure

This product is not reported to have any specific target organ general toxicity single exposure effects.

Specified Target Organ General Toxicity: Repeated Exposure

May cause damage to organs (liver, kidneys, blood, nervous system and skin) through prolonged or repeated exposure.

Aspiration Respiratory Organs Hazard

The major health threat of ingestion occurs from the danger of aspiration (breathing) of liquid drops into the lungs, particularly from vomiting. Aspiration may result in chemical pneumonia (fluid in the lungs), severe lung damage, respiratory failure and even death.

*** Section 12 – ECOLOGICAL INFORMATION ***

Ecotoxicity

A: General Product Information

Keep out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

B: Component Analysis – Ecotoxicity – Aquatic Toxicity

Benzene (71-43-2)

Test and Species	Conditions
96 Hr LC50 Pimephales promelas	10.7-14.7 mg/L [flow-through]
96 Hr LC50 Oncorhynchus mykiss	5.3 mg/L [flow-through]
96 Hr LC50 Lepomis macrochirus	22.49 mg/L [static]
96 Hr LC50 Poecilia reticulata	28.6 mg/L [static]
96 Hr LC50 Pimephales promelas	22330-41160 µg/L [static]
96 Hr LC50 Lepomis macrochirus	70000-142000 µg/L [static]
72 Hr EC50 Pseudokirchneriella subcapitata	29 mg/L
48 Hr EC50 Daphnia magna	8.76 - 15.6 mg/L [static]
48 Hr EC50 Daphnia magna	10 mg/L

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Natural Gas condensates (68919-39-1)

Test and Species	Conditions
96 Hr LC50 Alburnus alburnus	119 mg/L [static]
96 Hr LC50 Cyprinodon variegatus	82 mg/L [static]
72 Hr EC50 Pseudokirchneriella subcapitata	56 mg/L
24 Hr EC50 Daphnia magna	170 mg/L

Persistence / Degradability

No information available

Bioaccumulation

No information available

Mobility in Soil

No information available

*** Section 13 – DISPOSAL CONSIDERATIONS ***

Waste Disposal Instructions

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

Disposal of Contaminated Containers or Packaging

Recover or recycle if possible. It is the responsibility of the generator to determine the toxicity and physical properties of the material generated so as to properly classify the waste and ensure disposal methods comply with applicable regulations.

This material, if discarded should be fully characterized for ignitability (D001), reactivity (D003) and benzene (D018) prior to disposal (40 CFR261). Use which results in chemical or physical change or contamination may subject it to regulation as a hazardous waste. Along with properly characterizing all waste materials, consult state and local regulations regarding the proper disposal of this material. Do not dispose of by draining onto the ground. This will result in soil and groundwater contamination. Waste arising from spillage or tank cleaning should be disposed of in accordance with applicable regulations.

Container contents should be completely used and containers should be emptied prior to discard. Container rinsate could be considered a RCRA hazardous waste and must be disposed of with care and in full compliance with federal, state and local regulations. Larger empty containers, such as drums, should be returned to the distributor or to a qualified drum reconditioner. To assure proper disposal of smaller empty containers, consult with state and local regulations and disposal authorities.

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*** Section 14 – TRANSPORTATION INFORMATION ***

DOT Information

Shipping Name: Petroleum Products, n.o.s. (condensate)

UN #: 1268 **Hazard Class:** 3

Additional Info.: Dependent on the product's properties, the shipper may also elect to classify as Gasoline UN1203 or Petroleum Crude Oil UN1267 - reference 49 CFR 172.101 for further description (e.g., packing group determination).

Placard:



*** Section 15 – REGULATORY INFORMATION ***

Regulatory Information

Component Analysis

This material contains one or more of the following chemicals required to be identified under SARA Section 302 (40 CFR 355 Appendix A), SARA Section 313 (40 CFR 372.65) and/or CERCLA (40 CFR 302.4).

Benzene (71-43-2)

SARA 313: 0.1% de minimis concentration

CERCLA: 10 lb final RQ (received an adjusted RQ of 10 lbs based on potential carcinogenicity in an August 14, 1989 final rule); 4.54 kg final RQ (received an adjusted RQ of 10 lbs based on potential carcinogenicity in an August 14, 1989 final rule)

SARA Section 311/312 – Hazard Classes

<u>Acute Health</u>	<u>Chronic Health</u>	<u>Fire</u>	<u>Sudden Release of Pressure</u>	<u>Reactive</u>
X	X	X	--	--

SARA SECTION 313 – SUPPLIER NOTIFICATION

This product contains the following toxic chemicals subject to the reporting requirements of section 313 of the Emergency Planning and Community Right-To-Know Act (EPCRA) of 1986 and of 40 CFR 372:

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INGREDIENT NAME (CAS NUMBER)	CONCENTRATION PERCENT BY WEIGHT
Benzene (71-43-2)	<0.1 to 2

Canadian Regulatory Information

DSL/NDSL Inventory	This product has been classified in accordance with the hazard criteria of the Controlled Products Regulations (CPR) and the SDS contains all the information required by the Regulations.
Workplace Hazardous Materials Information System	B2 - Flammable Liquid D1A – Material Causing Immediate and Serious Toxic Effects - Very Toxic Material D2A: Material Causing Other Toxic Effects Very Toxic D2B - Material Causing Other Toxic Effects - Toxic Material

European Union Regulatory Information

Labeling	Product is dangerous as defined by the European Union Dangerous Substances / Preparations Directives. Contains: Low Boiling Point Naphtha
Symbol	F+ Extremely Flammable T Toxic N Dangerous for the Environment
Risk Phrases	R12-45-38-65-67-51/53 Extremely flammable. May cause cancer. Irritating to skin. Harmful: may cause lung damage if swallowed. Vapors may cause drowsiness and dizziness. Toxic to aquatic organisms, may cause long-term adverse effects in the aquatic environment.
Safety Phrases	S16-53-45-2-23-24-29-43-62 Keep away from sources of ignition – No smoking. Avoid exposure – obtain special instructions before use. In case of accident or if you feel unwell, seek medical advice immediately (show the label where possible). Keep out of reach of children. Do not breathe vapor. Avoid contact with skin. Do not empty into drains. In case of fire use foam/dry powder/CO2. If swallowed, do not induce vomiting: seek medical advice immediately and show this container or label.

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Material Name: Natural Gas Condensate

US GHS

State Regulations

Component Analysis – State

The following components appear on one or more of the following state hazardous substances lists

Component	CAS	CA	MA	MN	NJ	PA	RI
Octanes	111-65-9	Yes	No	Yes	Yes	Yes	Yes
Heptanes	142-82-5	Yes	No	Yes	Yes	Yes	Yes
n-Hexane	110-54-3	Yes	Yes	Yes	Yes	Yes	Yes
n-Pentane	109-66-0	Yes	No	Yes	Yes	Yes	Yes
n-Butane	106-97-8	Yes	No	Yes	Yes	Yes	Yes
Propane	74-98-6	No	No	Yes	Yes	Yes	Yes
Ethane	78-84-0	No	No	Yes	Yes	Yes	No
Benzene	71-43-2	Yes	Yes	Yes	Yes	Yes	Yes
Toluene	108-88-3	Yes	Yes	Yes	Yes	Yes	Yes
m-, o-, p-Xylene	1330-20-7	Yes	Yes	Yes	Yes	Yes	Yes

The following statement(s) are provided under the California Safe Drinking Water and Toxic Enforcement Act of 1986 (Proposition 65):

WARNING! This product contains a chemical known to the state of California to cause cancer.

WARNING! This product contains a chemical known to the state of California to cause Reproductive / developmental effects.

Component Analysis – WHMIS IDL

The following components are identified under the Canadian Hazardous Products Act

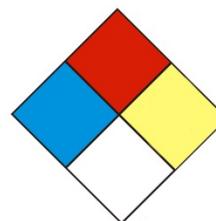
Ingredient Disclosure List:

Component	CAS #	Minimum Concentration
Benzene	71-43-2	0.1%

* * * Section 16 – OTHER INFORMATION * * *

NFPA® Hazard Rating

Health 1
Fire 4
Reactivity 0



HMIS® Hazard Rating

Health 1 Slight
Fire 4 Severe
Physical 0 Minimal
* Chronic

SAFETY DATA SHEET

Material Name: Natural Gas Condensate

US GHS

Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act; ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

Literature References

None

Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: January 29, 2014

Date of Last Revision: March 4, 2014

End of Sheet

Material Name: Wet Field Natural Gas

SYNONYMS: CNG, Natural Gas, Methane.

***** Section 1 – PRODUCT AND COMPANY IDENTIFICATION *****

PRODUCT NAME: Wet Field Natural Gas **EMERGENCY PHONE:** (800) 878-1373

PRODUCT CODES: CAS Reg. No. 68410-63-9 **AFTER HOURS:** (800) 878-1373

PRODUCER: Antero Resources

ADDRESS: 1615 Wynkoop Street **CHEMTREC PHONE:** (800) 424-9300

Denver, Colorado 80202

***** Section 2 – HAZARDS IDENTIFICATION *****

GHS Classification:

Flammable Gas – Category 1.

Gases Under Pressure – Gas.

Specific Target Organ Systemic Toxicity (STOT) – Single Exposure Category 2.

GHS LABEL ELEMENTS

Symbol(s)



Signal Word

Danger

Hazard Statements

Extremely flammable gas.

Contains gas under pressure, may explode if heated.

May cause damage to central nervous and respiratory systems.

Precautionary Statements

Prevention

Keep away from heat/sparks/open flames/hot surfaces. No smoking.

Do not breathe fume/gas/mist/vapors/spray.

Wash thoroughly after handling.

Do not eat, drink or smoke when using this product.

SAFETY DATA SHEET

Material Name: Wet Field Natural Gas

Response

Leaking gas fire: Do not extinguish, unless leak can be stopped safely. Eliminate all ignition sources if safe to do so.

If exposed to gas, or concerned about possible exposure: Call a POISON CENTER or doctor/physician.

Storage

Protect from sunlight. Store in a well-ventilated place.

Store in a secure area.

Disposal

Dispose of contents/containers in accordance with local/regional/national/international regulations.

*** Section 3 – COMPOSITION / INFORMATION ON INGREDIENTS ***

CAS #	Component	Percent
74-82-8	Methane	72 - 97
78-84-0	Ethane	2.2 - 14
74-98-6	Propane	0.0 – 8.0
106-97-8	Butanes	0.0 – 3.5
109-66-0	Pentanes	0.0 – 1.4
110-54-3	Hexanes	0.0 – 0.5
7727-37-9	Nitrogen	< 0.4
124-38-9	Carbon Dioxide	< 0.2
7782-44-7	Oxygen	< 0.04

Because natural gas is a natural product, composition can vary greatly.

*** Section 4 – FIRST AID MEASURES ***

First Aid: Eyes

In case of freeze burn, cover eyes to protect from light. Flush eyes with running water for at least fifteen (15) minutes. Following flushing, seek medical attention.

First Aid: Skin

Remove contaminated clothing. In case of blistering, frostbite or freeze burns, seek immediate medical attention.

SAFETY DATA SHEET

Material Name: Wet Field Natural Gas

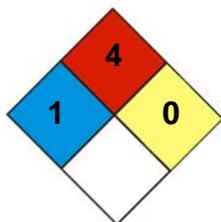
First Aid: Ingestion

Risk of ingestion is extremely low. However, if oral exposure occurs, seek immediate medical assistance.

First Aid: Inhalation

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

***** Section 5 – FIRE FIGHTING MEASURES *****



NFPA 704 Hazard Class

Health: **1** Flammability: **4** Instability: **0** (0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

General Fire Hazards

See Section 9 for Flammability Properties.

Forms a flammable mixture with air. If released, the resulting vapors will disperse with the prevailing wind. If a source of ignition is present where the vapor exists at a 5 – 15% concentration in air, the vapor will burn along the flame front toward the source of the fuel.

Hazardous Combustion Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

Extinguishing Media

Any extinguisher suitable for Class B fires, dry chemical, firefighting foam, CO₂, and other gaseous agents. However, fire should not be extinguished unless flow of gas can be immediately stopped.

Unsuitable Extinguishing Media

None.

Fire Fighting Equipment / Instructions

Gas fires should not be extinguished unless flow of gas can be immediately stopped. Shut off gas source and allow gas to burn out. If spill or leak has not ignited, determine

SAFETY DATA SHEET

Material Name: Wet Field Natural Gas

if water spray may assist in dispersing gas or vapor to protect personnel attempting to stop leak. Use water to cool equipment, surfaces and piping exposed to fire and excessive heat. For large fire, the use of unmanned hose holders or monitor nozzles may be advantageous to further minimize personnel exposure. Isolate area, particularly around piping. Let the fire burn unless leak can be stopped. Concentrate fire-fighting efforts on objects / materials ignited by the initial fire. Withdraw immediately in the event of a rising sound from a venting safety device.

Firefighting activities that may result in potential exposure to high heat, smoke or toxic by-products of combustion should require NIOSH-approved pressure-demand self-contained breathing apparatus with full facepiece and full protective clothing.

*** Section 6 – ACCIDENTAL RELEASE MEASURES ***

Recovery and Neutralization

Stop the source of the release, if safe to do so.

Materials and Methods for Clean-Up

Consider the use of water spray to disperse gas vapors. Do not use water spray to direct gas vapors toward sewer or drainage systems. Isolate the area until gas has dispersed. Ventilate and gas test area before entering.

Emergency Measures

Evacuate nonessential personnel and secure all ignition sources. No road flares, smoking or flames in hazard area. Consider wind direction. Stay upwind and uphill, if possible. Vapor cloud may be white, but color will dissipate as cloud disperses. Fire and explosion hazard is still present.

Personal Precautions and Protective Equipment

Cooling effect of expanding gas from leak may present frostbite / freeze burn hazard. Wear flame retardant (FR) clothing around un-ignited leak. Wear fire protective clothing around an active fire.

Environmental Precautions

Do not flush gas vapors toward sewer or drainage systems.

Prevention of Secondary Hazards

None.

SAFETY DATA SHEET

Material Name: Wet Field Natural Gas

*** Section 7 – HANDLING AND STORAGE ***

Handling Procedures

Keep away from flame, sparks and excessive temperatures. Bond and ground containers. Use only in well ventilated areas.

Storage Procedures

Natural gas will be contained in the pipeline. Keep away from flame, sparks, excessive temperatures and open flames. Empty pipeline segments may contain explosive residues from natural gas liquids. Do not cut, heat, weld or expose containers to sources of ignition sections of pipeline unless the sections have been purged of natural gas residues.

Incompatibilities

Keep away from strong oxidizers, ignition sources and heat.

*** Section 8 – EXPOSURE CONTROLS / PERSONAL PROTECTION ***

Component Exposure Limits

Methane (74-82-8)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Ethane (74-84-0)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Propane (74-98-6)

ACGIH: 2500 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Butane (106-97-8)

ACGIH: 800 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Pentanes (109-66-0)

ACGIH: 600 ppm TWA (listed under Pentane, all isomers)

Hexanes (110-54-3)

ACGIH: 50 ppm TWA (listed under n-Hexane)

SAFETY DATA SHEET

Material Name: Wet Field Natural Gas

Nitrogen (7727-37-9)

Simple Asphyxiant

Carbon Dioxide (124-38-9)

ACGIH: 5000 ppm TWA (listed under Carbon Dioxide)

Oxygen (7782-44-7)

N/A – Necessary for life

Engineering Measures

Use adequate ventilation to keep gas and vapor concentrations of this product below occupational exposure and flammability limits, particularly in confined spaces. Use explosion-proof equipment and lighting in classified / controlled areas.

Personal Protective Equipment: Respiratory

Use a NIOSH approved positive-pressure, supplied air respirator with escape bottle or self-contained breathing apparatus (SCBA) for gas concentrations above occupational exposure limits, for potential for uncontrolled release, if exposure levels are not known, or in an oxygen-deficient atmosphere. CAUTION: Flammability limits (i.e., explosion hazard should be considered when assessing the need to expose personnel to concentrations requiring respiratory protection.

Personal Protective Equipment: Hands

Use cold-impervious, insulating flame-retardant (FR) gloves where contact with pressurized gas may occur.

Personal Protective Equipment: Eyes

Where there is a possibility of pressurized gas contact, wear splash-proof safety goggles and faceshield.

Personal Protective Equipment: Skin and Body

Where contact with pressurized gas may occur, wear flame-retardant (FR) and a faceshield.

***** Section 9 – PHYSICAL AND CHEMICAL PROPERTIES *****

Appearance: Colorless	Odor: Odorless to slight petroleum odor
Physical State: Gas	pH: ND
Vapor Pressure: 40 atm @ -187°F (-86°C)	Vapor Density: 0.6
Boiling Point: -259°F (-162°C)	Melting Point: ND
Solubility (H2O): 3.5%	Specific Gravity: 0.4 @ -263°F (-164°C)

SAFETY DATA SHEET

Material Name: Wet Field Natural Gas

Evaporation Rate: ND	VOC: ND
Octanol / H₂O Coeff.: ND	Flash Point: Flammable Gas
Flash Point Method: N/A	
Lower Flammability Limit: 3.8 – 6.5	Upper Flammability Limit: 13-17
(LFL):	(UFL):
Auto Ignition: 900-1170°F (482-632°C)	Burning Rate: ND

*** Section 10 – CHEMICAL STABILITY & REACTIVITY INFORMATION ***

Chemical Stability

This is a stable material.

Hazardous Reaction Potential

Will not occur.

Conditions to Avoid

Keep away from strong oxidizers, ignition sources and heat.

Hazardous Decomposition Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

*** Section 11 – TOXICOLOGICAL INFORMATION ***

Acute Toxicity

A: General Product Information

Methane and ethane, the main components of natural gas, are considered practically inert in terms of physiological effects. At high concentrations these materials act as simple asphyxiants and may cause death due to lack of oxygen.

B. Component Analysis – LD50/LC50

Methane (74-82-8)

Inhalation LC50 Mouse 326 g/m³ 2h

Ethane (74-84-0)

Inhalation LC50 Rat 658 mg/l 4h

Propane (74-98-6)

Inhalation LC50 Rat 658 mg/l 4h

SAFETY DATA SHEET

Material Name: Wet Field Natural Gas

Butanes (106-97-8)

Inhalation LC50 Rat 658 g/m³ 4h

Pentanes (109-66-0)

Inhalation LD50 Rat 364 g/m³ 4h

Hexanes (110-54-3)

Inhalation LC50 Rat > 20 mg/l 4h

Nitrogen (7727-37-9)

Simple Asphyxiant

Carbon Dioxide (124-38-9)

Inhalation LC50 Human 100,000 ppm 1minute

Oxygen (7782-44-7)

N/A – Necessary for life

Potential Health Effects: Skin Corrosion Property / Stimulativeness

This product is not reported to have any skin sensitization effects.

Generative Cell Mutagenicity

This product is not reported to have any mutagenic effects.

Carcinogenicity

A: General Product Information

This product is not reported to have any carcinogenic effects.

B: Component Carcinogenicity

None of this product's components are listed by ACGIH, IARC, OSHA, NIOSH, or NTP.

Reproductive Toxicity

This product is not reported to have any reproductive toxicity effects.

Specified Target Organ General Toxicity: Single Exposure

This product may cause damage to the heart.

Specified Target Organ General Toxicity: Repeated Exposure

This product is not reported to have any specific target organ repeat effects.

Aspiration Respiratory Organs Hazard

This product is not reported to have any aspiration hazard effects.

SAFETY DATA SHEET

Material Name: Wet Field Natural Gas

*** Section 12 – ECOLOGICAL INFORMATION ***

Ecotoxicity

A: General Product Information

Keep gas and vapors out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

B: Component Analysis – Ecotoxicity – Aquatic Toxicity

No ecotoxicity data are available for this product's components.

Persistence / Degradability

No information available.

Bioaccumulation

No information available.

Mobility in Soil

No information available.

*** Section 13 – DISPOSAL CONSIDERATIONS ***

Waste Disposal Instructions

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

Disposal of Contaminated Containers or Packaging

Dispose of contents / container in accordance with local / regional / national / international regulations.

*** Section 14 – TRANSPORTATION INFORMATION ***

DOT Information

Shipping Name: Natural Gas, Compressed

UN #: 1971 **Hazard Class:** 2.1

Placard:



SAFETY DATA SHEET

Material Name: Wet Field Natural Gas

***** Section 15 – REGULATORY INFORMATION *****

Regulatory Information

Component Analysis

None of this products components are listed under SARA Section 302 (40 CFR 355 Appendix A).

n-hexane is listed under SARA Section 313 (40 CFR 372.65). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

n-hexane is listed under CERCLA (40 CFR 302.4). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

SARA Section 311/312 – Hazard Classes

<u>Acute Health</u>	<u>Chronic Health</u>	<u>Fire</u>	<u>Sudden Release of Pressure</u>	<u>Reactive</u>
---	---	X	X	---

SARA Section 313 – Supplier Notification

This product contains one chemical (n-Hexane) that is subject to the reporting requirements of section 313 of the Emergency Planning and Community Right-to-know act (EPCRA) of 1986 and of 40 CFR 372. However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

State Regulations

Component Analysis – State

The following components appear on one or more of the following state hazardous substances lists:

Component	CAS	CA	MA	MN	NJ	PA	RI
Methane	74-82-8	No	No	Yes	Yes	Yes	No
Ethane	78-84-0	No	No	Yes	Yes	Yes	No
Propane	74-98-6	No	No	Yes	Yes	Yes	Yes
Butane	106-97-8	Yes	No	Yes	Yes	Yes	Yes
Pentanes	109-66-0	Yes	No	Yes	Yes	Yes	Yes
Hexanes	110-54-3	Yes	Yes	Yes	Yes	Yes	Yes
Nitrogen	7727-37-9	No	No	No	No	No	No
Carbon Dioxide	124-38-9	Yes	No	Yes	Yes	Yes	Yes
Oxygen	7782-44-7	No	No	No	No	No	No

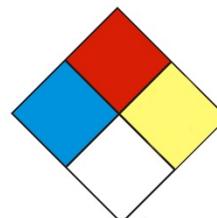
SAFETY DATA SHEET

Material Name: Wet Field Natural Gas

*** Section 16 – OTHER INFORMATION ***
--

NFPA® Hazard Rating

Health	1
Fire	4
Reactivity	0



HMIS® Hazard Rating

Health	1	Moderate
Fire	4	Severe
Physical	0	Minimal

* Chronic

Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act; ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

Literature References

None

Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: February 7, 2014

Date of Last Revision: March 4,, 2014

End of Sheet

Material Name: Dry Field Natural Gas

US GHS

SYNONYMS: CNG, Natural Gas, Methane.

*** Section 1 – PRODUCT AND COMPANY IDENTIFICATION ***

PRODUCT NAME: Dry Field Natural Gas EMERGENCY PHONE: (800) 878-1373

PRODUCT CODES: CAS Reg. No. 68410-63-9 AFTER HOURS: (800) 878-1373

PRODUCER: Antero Resources

ADDRESS: 1615 Wynkoop Street CHEMTREC PHONE: (800) 424-9300
Denver, Colorado 80202

*** Section 2 – HAZARDS IDENTIFICATION ***

GHS Classification:

Flammable Gas – Category 1.

Gases Under Pressure – Gas.

Specific Target Organ Systemic Toxicity (STOT) – Single Exposure Category 2.

GHS LABEL ELEMENTS

Symbol(s)



Signal Word

Danger

Hazard Statements

Extremely flammable gas.

Contains gas under pressure, may explode if heated.

May cause damage to central nervous and respiratory systems.

Precautionary Statements

Prevention

Keep away from heat/sparks/open flames/hot surfaces. No smoking.

Do not breathe fume/gas/mist/vapors/spray.

Wash thoroughly after handling.

Do not eat, drink or smoke when using this product.

SAFETY DATA SHEET

Material Name: Dry Field Natural Gas

US GHS

Response

Leaking gas fire: Do not extinguish, unless leak can be stopped safely. Eliminate all ignition sources if safe to do so.

If exposed to gas, or concerned about possible exposure: Call a POISON CENTER or doctor/physician.

Storage

Protect from sunlight. Store in a well-ventilated place.

Store in a secure area.

Disposal

Dispose of contents/containers in accordance with local/regional/national/international regulations.

*** Section 3 – COMPOSITION / INFORMATION ON INGREDIENTS ***

CAS #	Component	Percent
74-82-8	Methane	95.01
78-84-0	Ethane	3.99
74-98-6	Propane	0.32
106-97-8	Butanes	0.07
109-66-0	Pentanes	0.02
110-54-3	Hexanes	0.01
7727-37-9	Nitrogen	0.35
124-38-9	Carbon Dioxide	0.19
7782-44-7	Oxygen	0.03

Because natural gas is a natural product, composition can vary greatly.

*** Section 4 – FIRST AID MEASURES ***

First Aid: Eyes

In case of freeze burn, cover eyes to protect from light. Flush eyes with running water for at least fifteen (15) minutes. Following flushing, seek medical attention.

First Aid: Skin

Remove contaminated clothing. In case of blistering, frostbite or freeze burns, seek immediate medical attention.

SAFETY DATA SHEET

Material Name: Dry Field Natural Gas

US GHS

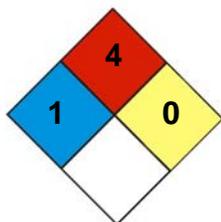
First Aid: Ingestion

Risk of ingestion is extremely low. However, if oral exposure occurs, seek immediate medical assistance.

First Aid: Inhalation

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

***** Section 5 – FIRE FIGHTING MEASURES *****



NFPA 704 Hazard Class

Health: **1** Flammability: **4** Instability: **0** (0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

General Fire Hazards

See Section 9 for Flammability Properties.

Forms a flammable mixture with air. If released, the resulting vapors will disperse with the prevailing wind. If a source of ignition is present where the vapor exists at a 5 – 15% concentration in air, the vapor will burn along the flame front toward the source of the fuel.

Hazardous Combustion Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

Extinguishing Media

Any extinguisher suitable for Class B fires, dry chemical, fire fighting foam, CO₂, and other gaseous agents. However, fire should not be extinguished unless flow of gas can be immediately stopped.

Unsuitable Extinguishing Media

None.

Fire Fighting Equipment / Instructions

Gas fires should not be extinguished unless flow of gas can be immediately stopped. Shut off gas source and allow gas to burn out. If spill or leak has not ignited, determine

SAFETY DATA SHEET

Material Name: Dry Field Natural Gas

US GHS

if water spray may assist in dispersing gas or vapor to protect personnel attempting to stop leak. Use water to cool equipment, surfaces and piping exposed to fire and excessive heat. For large fire, the use of unmanned hose holders or monitor nozzles may be advantageous to further minimize personnel exposure. Isolate area, particularly around piping. Let the fire burn unless leak can be stopped. Concentrate fire-fighting efforts on objects / materials ignited by the initial fire. Withdraw immediately in the event of a rising sound from a venting safety device.

Firefighting activities that may result in potential exposure to high heat, smoke or toxic by-products of combustion should require NIOSH-approved pressure-demand self-contained breathing apparatus with full facepiece and full protective clothing.

*** Section 6 – ACCIDENTAL RELEASE MEASURES ***

Recovery and Neutralization

Stop the source of the release, if safe to do so.

Materials and Methods for Clean-Up

Consider the use of water spray to disperse gas vapors. Do not use water spray to direct gas vapors toward sewer or drainage systems. Isolate the area until gas has dispersed. Ventilate and gas test area before entering.

Emergency Measures

Evacuate nonessential personnel and secure all ignition sources. No road flares, smoking or flames in hazard area. Consider wind direction. Stay upwind and uphill, if possible. Vapor cloud may be white, but color will dissipate as cloud disperses. Fire and explosion hazard is still present.

Personal Precautions and Protective Equipment

Cooling effect of expanding gas from leak may present frostbite / freeze burn hazard. Wear flame retardant (FR) clothing around un-ignited leak. Wear fire protective clothing around an active fire.

Environmental Precautions

Do not flush gas vapors toward sewer or drainage systems.

Prevention of Secondary Hazards

None.

SAFETY DATA SHEET

Material Name: Dry Field Natural Gas

US GHS

*** Section 7 – HANDLING AND STORAGE ***

Handling Procedures

Keep away from flame, sparks and excessive temperatures. Bond and ground containers. Use only in well ventilated areas.

Storage Procedures

Natural gas will be contained in the pipeline. Keep away from flame, sparks, excessive temperatures and open flames. Empty pipeline segments may contain explosive residues from natural gas liquids. Do not cut, heat, weld or expose containers to sources of ignition sections of pipeline unless the sections have been purged of natural gas residues.

Incompatibilities

Keep away from strong oxidizers, ignition sources and heat.

*** Section 8 – EXPOSURE CONTROLS / PERSONAL PROTECTION ***

Component Exposure Limits

Methane (74-82-8)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Ethane (74-84-0)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Propane (74-98-6)

ACGIH: 2500 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Butane (106-97-8)

ACGIH: 800 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Pentanes (109-66-0)

ACGIH: 600 ppm TWA (listed under Pentane, all isomers)

Hexanes (110-54-3)

ACGIH: 50 ppm TWA (listed under n-Hexane)

SAFETY DATA SHEET

Material Name: Dry Field Natural Gas

US GHS

Nitrogen (7727-37-9)

Simple Asphyxiant

Carbon Dioxide (124-38-9)

ACGIH: 5000 ppm TWA (listed under Carbon Dioxide)

Oxygen (7782-44-7)

N/A – Necessary for life

Engineering Measures

Use adequate ventilation to keep gas and vapor concentrations of this product below occupational exposure and flammability limits, particularly in confined spaces. Use explosion-proof equipment and lighting in classified / controlled areas.

Personal Protective Equipment: Respiratory

Use a NIOSH approved positive-pressure, supplied air respirator with escape bottle or self-contained breathing apparatus (SCBA) for gas concentrations above occupational exposure limits, for potential for uncontrolled release, if exposure levels are not known, or in an oxygen-deficient atmosphere. CAUTION: Flammability limits (i.e., explosion hazard should be considered when assessing the need to expose personnel to concentrations requiring respiratory protection.

Personal Protective Equipment: Hands

Use cold-impervious, insulating flame-retardant (FR) gloves where contact with pressurized gas may occur.

Personal Protective Equipment: Eyes

Where there is a possibility of pressurized gas contact, wear splash-proof safety goggles and faceshield.

Personal Protective Equipment: Skin and Body

Where contact with pressurized gas may occur, wear flame-retardant (FR) and a faceshield.

***** Section 9 – PHYSICAL AND CHEMICAL PROPERTIES *****

Appearance: Colorless	Odor: Odorless to slight petroleum odor
Physical State: Gas	pH: ND
Vapor Pressure: 40 atm @ -187°F (-86°C)	Vapor Density: 0.6
Boiling Point: -259°F (-162°C)	Melting Point: ND
Solubility (H2O): 3.5%	Specific Gravity: 0.4 @ -263°F (-164°C)

SAFETY DATA SHEET

Material Name: Dry Field Natural Gas

US GHS

Evaporation Rate:	ND	VOC:	ND
Octanol / H ₂ O Coeff.:	ND	Flash Point:	Flammable Gas
Flash Point Method:	N/A		
Lower Flammability Limit:	3.8 – 6.5	Upper Flammability Limit:	13-17
(LFL):		(UFL):	
Auto Ignition:	900-1170°F (482-632°C)	Burning Rate:	ND

*** Section 10 – CHEMICAL STABILITY & REACTIVITY INFORMATION ***

Chemical Stability

This is a stable material.

Hazardous Reaction Potential

Will not occur.

Conditions to Avoid

Keep away from strong oxidizers, ignition sources and heat.

Hazardous Decomposition Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

*** Section 11 – TOXICOLOGICAL INFORMATION ***

Acute Toxicity

A: General Product Information

Methane and ethane, the main components of natural gas, are considered practically inert in terms of physiological effects. At high concentrations these materials act as simple asphyxiants and may cause death due to lack of oxygen.

B. Component Analysis – LD50/LC50

Methane (74-82-8)

Inhalation LC50 Mouse 326 g/m³ 2h

Ethane (74-84-0)

Inhalation LC50 Rat 658 mg/l 4h

Propane (74-98-6)

Inhalation LC50 Rat 658 mg/l 4h

SAFETY DATA SHEET

Material Name: Dry Field Natural Gas

US GHS

Butanes (106-97-8)

Inhalation LC50 Rat 658 g/m³ 4h

Pentanes (109-66-0)

Inhalation LD50 Rat 364 g/m³ 4h

Hexanes (110-54-3)

Inhalation LC50 Rat > 20 mg/l 4h

Nitrogen (7727-37-9)

Simple Asphyxiant

Carbon Dioxide (124-38-9)

Inhalation LC50 Human 100,000 ppm 1 minute

Oxygen (7782-44-7)

N/A – Necessary for life

Potential Health Effects: Skin Corrosion Property / Stimulativeness

This product is not reported to have any skin sensitization effects.

Generative Cell Mutagenicity

This product is not reported to have any mutagenic effects.

Carcinogenicity

A: General Product Information

This product is not reported to have any carcinogenic effects.

B: Component Carcinogenicity

None of this product's components are listed by ACGIH, IARC, OSHA, NIOSH, or NTP.

Reproductive Toxicity

This product is not reported to have any reproductive toxicity effects.

Specified Target Organ General Toxicity: Single Exposure

This product may cause damage to the heart.

Specified Target Organ General Toxicity: Repeated Exposure

This product is not reported to have any specific target organ repeat effects.

Aspiration Respiratory Organs Hazard

This product is not reported to have any aspiration hazard effects.

SAFETY DATA SHEET

Material Name: Dry Field Natural Gas

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*** Section 12 – ECOLOGICAL INFORMATION ***

Ecotoxicity

A: General Product Information

Keep gas and vapors out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

B: Component Analysis – Ecotoxicity – Aquatic Toxicity

No ecotoxicity data are available for this product's components.

Persistence / Degradability

No information available.

Bioaccumulation

No information available.

Mobility in Soil

No information available.

*** Section 13 – DISPOSAL CONSIDERATIONS ***

Waste Disposal Instructions

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

Disposal of Contaminated Containers or Packaging

Dispose of contents / container in accordance with local / regional / national / international regulations.

*** Section 14 – TRANSPORTATION INFORMATION ***

DOT Information

Shipping Name: Natural Gas, Compressed

UN #: 1971 **Hazard Class:** 2.1

Placard:



SAFETY DATA SHEET

Material Name: Dry Field Natural Gas

US GHS

*** Section 15 – REGULATORY INFORMATION ***

Regulatory Information

Component Analysis

None of this products components are listed under SARA Section 302 (40 CFR 355 Appendix A).

n-hexane is listed under SARA Section 313 (40 CFR 372.65). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

n-hexane is listed under CERCLA (40 CFR 302.4). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

SARA Section 311/312 – Hazard Classes

<u>Acute Health</u>	<u>Chronic Health</u>	<u>Fire</u>	<u>Sudden Release of Pressure</u>	<u>Reactive</u>
---	---	X	X	---

SARA Section 313 – Supplier Notification

This product contains one chemical (n-Hexane) that is subject to the reporting requirements of section 313 of the Emergency Planning and Community Right-to-know act (EPCRA) of 1986 and of 40 CFR 372. However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

State Regulations

Component Analysis – State

The following components appear on one or more of the following state hazardous substances lists:

Component	CAS	CA	MA	MN	NJ	PA	RI
Methane	74-82-8	No	No	Yes	Yes	Yes	No
Ethane	78-84-0	No	No	Yes	Yes	Yes	No
Propane	74-98-6	No	No	Yes	Yes	Yes	Yes
Butane	106-97-8	Yes	No	Yes	Yes	Yes	Yes
Pentanes	109-66-0	Yes	No	Yes	Yes	Yes	Yes
Hexanes	110-54-3	Yes	Yes	Yes	Yes	Yes	Yes
Nitrogen	7727-37-9	No	No	No	No	No	No
Carbon Dioxide	124-38-9	Yes	No	Yes	Yes	Yes	Yes
Oxygen	7782-44-7	No	No	No	No	No	No

SAFETY DATA SHEET

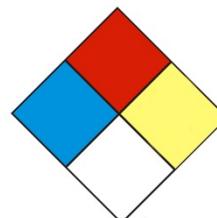
Material Name: Dry Field Natural Gas

US GHS

*** Section 16 – OTHER INFORMATION ***

NFPA® Hazard Rating

Health 1
Fire 4
Reactivity 0



HMIS® Hazard Rating

Health 1 Moderate
Fire 4 Severe
Physical 0 Minimal
* Chronic

Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act; ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

Literature References

None

Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: January 30, 2014

Date of Last Revision: March 4, 2014

End of Sheet

**Attachment I.
Emission Units Table**

Attachment I
Emission Units Table
(includes all emission units and air pollution control devices
that will be part of this permit application review, regardless of permitting status)

Emission Unit ID ¹	Emission Point ID ²	Emission Unit Description	Year Installed/ Modified	Design Capacity	Type ³ and Date of Change	Control Device ⁴
C-100	1E	Compressor Engine #1	2014	1,680 hp	Modified	NSCR (1C)
C-200	2E	Compressor Engine #2	2014	1,680 hp	Modified	NSCR (2C)
C-300	3E	Compressor Engine #3	2014	1,680 hp	Modified	NSCR (3C)
C-400	4E	Compressor Engine #4	2014	1,680 hp	Modified	NSCR (4C)
C-500	5E	Compressor Engine #5	2014	1,680 hp	Modified	NSCR (5C)
C-600	6E	Compressor Engine #6	2014	1,680 hp	Modified	NSCR (6C)
C-700	7E	Compressor Engine #7	2014	1,680 hp	Modified	NSCR (7C)
C-800	8E	Compressor Engine #8	2014	1,680 hp	Modified	NSCR (8C)
C-900	9E	Compressor Engine #9	2014	1,680 hp	Modified	NSCR (9C)
C-1000	10E	Compressor Engine #10	2014	1,680 hp	Modified	NSCR(10C)
C-1100	11E	Compressor Engine #11	2014	1,680 hp	Modified	NSCR(11C)
GEN1	12E	Microturbine Generator #1	2014	600 kWe	NA	None
GEN2	13E	Microturbine Generator #2	2014	600 kWe	NA	None
DEHY1	14E	Dehydrator Still Vent #1	2014	72.5 MMscfd	Modified	FLARE1 (12C)
DFLSH1	15E	Dehydrator Flash Tank #1	2014	72.5 MMscfd	Modified	98% control
DREB1	16E	Dehydrator Reboiler #1	2014	1.5 mmbtu/hr	Modified	None
DEHY2	17E	Dehydrator Still Vent #2	2014	72.5 MMscfd	Modified	FLARE1 (12C)
DFLSH2	18E	Dehydrator Flash Tank #2	2014	72.5 MMscfd	Modified	98% control
DREB2	19E	Dehydrator Reboiler #2	2014	1.5 mmbtu/hr	Modified	None
TK-1502	20E	Settling Tank 1	2014	400 barrel	NA	VRU-100 & 200 (13C & 14C)
TK-200	21E	Condensate Tank 1	2014	400 barrel	NA	VRU-100 & 200 (13C & 14C)
TK-201	22E	Condensate Tank 2	2014	400 barrel	NA	VRU-100 & 200 (13C & 14C)
TK-1500	23E	Produced Water Tank 1	2014	400 barrel	NA	VRU-100 & 200 (13C & 14C)

TK-1501	24E	Produced Water Tank 2	2014	400 barrel	NA	VRU-100 & 200 (13C & 14C)
CATHT1	27E	Catalytic Heater for Generator Fuel	2014	0.024 MMBtu/hr	NA	None
----	----	NSCR Catalyst for Compressor #1	2014	----	Modified	1C
----	----	NSCR Catalyst for Compressor #2	2014	----	Modified	2C
----	----	NSCR Catalyst for Compressor #3	2014	----	Modified	3C
----	----	NSCR Catalyst for Compressor #4	2014	----	Modified	4C
----	----	NSCR Catalyst for Compressor #5	2014	----	Modified	5C
----	----	NSCR Catalyst for Compressor #6	2014	----	Modified	6C
----	----	NSCR Catalyst for Compressor #7	2014	----	Modified	7C
----	----	NSCR Catalyst for Compressor #8	2014	----	Modified	8C
----	----	NSCR Catalyst for Compressor #9	2014	----	Modified	9C
----	----	NSCR Catalyst for Compressor #10	2014	----	Modified	10C
----	----	NSCR Catalyst for Compressor #11	2014	----	Modified	11C
FLARE1	26E	Flare Combustion Device 1	2014	4.8 MMBtu/hr	NA	12C
VRU-100	----	Vapor Recovery Unit 1	2014	----	NA	13C
VRU-200	----	Vapor Recovery Unit 2	2014	----	NA	14C
C-1200	28E	Compressor Engine #12	2016	1,680 hp	New	NSCR (15C)
C-1300	29E	Compressor Engine #13	2016	1,680 hp	New	NSCR (16C)
----	----	NSCR Catalyst for Compressor #12	2016	----	New	15C
----	----	NSCR Catalyst for Compressor #13	2016	----	New	16C

¹ For Emission Units (or Sources) use the following numbering system: 1S, 2S, 3S,... or other appropriate designation.

² For Emission Points use the following numbering system: 1E, 2E, 3E, ... or other appropriate designation.

³ New, modification, removal

⁴ For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

Attachment J.
Emission Point Data Summary Sheet

**Attachment J
EMISSION POINTS DATA SUMMARY SHEET**

Table 1: Emissions Data															
Emission Point ID No. <i>(Must match Emission Units Table & Plot Plan)</i>	Emission Point Type ¹	Emission Unit Vented Through This Point <i>(Must match Emission Units Table & Plot Plan)</i>		Air Pollution Control Device <i>(Must match Emission Units Table & Plot Plan)</i>		Vent Time for Emission Unit <i>(chemical processes only)</i>		All Regulated Pollutants - Chemical Name/CAS ³ <i>(Speciate VOCs & HAPS)</i>	Maximum Potential Uncontrolled Emissions ⁴		Maximum Potential Controlled Emissions ⁵		Emission Form or Phase <i>(At exit conditions, Solid, Liquid or Gas/Vapor)</i>	Est. Method Used ⁶	Emission Concentration ⁷ <i>(ppmv or mg/m⁴)</i>
		ID No.	Source	ID No.	Device Type	Short Term ²	Max (hr/yr)		lb/hr	ton/yr	lb/hr	ton/yr			
1E	Upward Vertical Stack	C-100	Compressor engine 1	1C	NSCR catalyst	C	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
								CO	47.04	206.02	1.18	5.15			
								VOC	1.70	7.46	0.27	1.19			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2080	9109	1993	8731			
2E	Upward Vertical Stack	C-200	Compressor engine 2	2C	NSCR catalyst	C	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
								CO	47.04	206.02	1.18	5.15			
								VOC	1.70	7.46	0.27	1.19			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2080	9109	1993	8731			
3E	Upward Vertical Stack	C-300	Compressor engine 3	3C	NSCR catalyst	C	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
								CO	47.04	206.02	1.18	5.15			
								VOC	1.70	7.46	0.27	1.19			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2080	9109	1993	8731			

4E	Upward Vertical Stack	C-400	Compressor engine 4	4C	NSCR catalyst	C	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.74 47.04 1.70 0.27 0.008 0.35 0.19 2080	222.24 206.02 7.46 1.18 0.036 1.54 0.81 9109	1.27 1.18 0.27 0.27 0.008 0.18 0.019 1993	5.56 5.15 1.19 1.18 0.036 0.81 0.081 8731	Gas/Vapor	EE	
5E	Upward Vertical Stack	C-500	Compressor engine 5	5C	NSCR catalyst	C	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.74 47.04 1.70 0.27 0.008 0.35 0.19 2080	222.24 206.02 7.46 1.18 0.036 1.54 0.81 9109	1.27 1.18 0.27 0.27 0.008 0.18 0.019 1993	5.56 5.15 1.19 1.18 0.036 0.81 0.081 8731	Gas/Vapor	EE	
6E	Upward Vertical Stack	C-600	Compressor engine 6	6C	NSCR catalyst	C	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.74 47.04 1.70 0.27 0.008 0.35 0.19 2080	222.24 206.02 7.46 1.18 0.036 1.54 0.81 9109	1.27 1.18 0.27 0.27 0.008 0.18 0.019 1993	5.56 5.15 1.19 1.18 0.036 0.81 0.081 8731	Gas/Vapor	EE	
7E	Upward Vertical Stack	C-700	Compressor engine 7	7C	NSCR catalyst	C	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.74 47.04 1.70 0.27 0.008 0.35 0.19 2080	222.24 206.02 7.46 1.18 0.036 1.54 0.81 9109	1.27 1.18 0.27 0.27 0.008 0.18 0.019 1993	5.56 5.15 1.19 1.18 0.036 0.81 0.081 8731	Gas/Vapor	EE	

8E	Upward Vertical Stack	C-800	Compressor engine 8	8C	NSCR catalyst	C	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
								CO	47.04	206.02	1.18	5.15			
								VOC	1.70	7.46	0.27	1.19			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2080	9109	1993	8731			
9E	Upward Vertical Stack	C-900	Compressor engine 9	9C	NSCR catalyst	C	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
								CO	47.04	206.02	1.18	5.15			
								VOC	1.70	7.46	0.27	1.19			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2080	9109	1993	8731			
10E	Upward Vertical Stack	C-1000	Compressor engine 10	10C	NSCR catalyst	C	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
								CO	47.04	206.02	1.18	5.15			
								VOC	1.70	7.46	0.27	1.19			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2080	9109	1993	8731			
11E	Upward Vertical Stack	C-1100	Compressor engine 11	11C	NSCR catalyst	C	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
								CO	47.04	206.02	1.18	5.15			
								VOC	1.70	7.46	0.27	1.19			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2080	9109	1993	8731			

12E-13E	Upward Vertical Stack	GEN1 & GEN2	Microturbine Generators	----	----	C	9,260	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	0.24 0.66 0.06 0.04 0.02 0.006 0.004 799	1.11 3.06 0.28 0.19 0.10 0.03 0.02 3698	0.24 0.66 0.06 0.28 0.10 0.006 0.004 799	1.11 3.06 0.28 0.19 0.10 0.03 0.02 3698	Gas/Vapor	EE	
14E	Upward Vertical Stack	DEHY1	Dehydrator Still Vent 1	12C	Flare-98% Control	C	8,760	VOC Total HAPs Benzene Toluene Xylenes n-Hexane CO2e	15.71 6.40 1.58 2.45 2.00 0.37 447	68.82 28.02 6.92 10.72 8.77 1.61 1958	0.31 0.13 0.031 0.14 0.049 0.040 0.007 9.5	1.37 0.56 0.14 0.21 0.17 0.032 41.5	Gas/Vapor	EE	
15E	Used for fuel in 16E	DFLSH1	Dehydrator Flash Gas 1	Used for Fuel in 16E	98% Control Backup	C	8,760	VOC Total HAPs Benzene Toluene Xylenes n-Hexane CO2e	45.03 2.35 0.39 0.46 0.18 1.32 1798	197.25 10.30 1.72 2.01 0.78 5.79 7874	0.90 0.047 0.008 0.009 0.004 0.026 39.3	3.94 0.21 0.034 0.040 0.016 0.12 172	Gas/Vapor	EE	
16E	Upward Vertical Stack	DREB1	Dehydrator Reboiler 1	---	----	C	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	0.18 0.15 0.010 0.014 0.001 0.004 0.0001 176.1	0.81 0.68 0.044 0.061 0.005 0.015 0.0006 771	0.18 0.15 0.010 0.014 0.001 0.004 0.0001 176.1	0.81 0.68 0.044 0.061 0.005 0.015 0.0006 771	Gas/Vapor	EE	

17E	Upward Vertical Stack	DEHY2	Dehydrator Still Vent 2	12C	Flare-98% Control	C	8,760	VOC Total HAPs Benzene Toluene Xylenes n-Hexane CO2e	15.71 6.40 1.58 2.45 2.00 0.37 447	68.82 28.02 6.92 10.72 8.77 1.61 1958	0.31 0.13 0.031 0.049 0.040 0.007 9.5	1.37 0.56 0.14 0.21 0.17 0.032 41.5	Gas/Vapor	EE	
18E	Used for fuel in 19E	DFLSH2	Dehydrator Flash Gas 2	Used for Fuel in 19E	98% Control Backup	C	8,760	VOC Total HAPs Benzene Toluene Xylenes n-Hexane CO2e	45.03 2.35 0.39 0.46 0.18 1.32 1798	197.25 10.30 1.72 2.01 0.78 5.79 7874	0.90 0.047 0.008 0.009 0.004 0.026 39.3	3.94 0.21 0.034 0.040 0.016 0.12 172	Gas/Vapor	EE	
19E	Upward Vertical Stack	DREB2	Dehydrator Reboiler 2	---	----	C	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	0.18 0.15 0.010 0.014 0.001 0.004 0.0001 176.1	0.81 0.68 0.044 0.061 0.005 0.015 0.0006 771	0.18 0.15 0.010 0.014 0.001 0.004 0.0001 176.1	0.81 0.68 0.044 0.061 0.005 0.015 0.0006 771	Gas/Vapor	EE	
20E	Upward Vertical Stack	TK-1502	Settler Tank	13C	VRU-98% control	C	8,760	VOC Total HAPs CO2e	72.24 1.03 516	316.39 4.52 2260	1.44 0.02 10.32	6.33 0.09 45.20	Gas/Vapor	EE	
21E	Upward Vertical Stack	TK-200	Condensate Tank 1	13C	VRU-98% control	C	8,760	VOC Total HAPs CO2e	1.21 0.02 8.62	5.29 0.08 37.77	0.02 0.0003 0.17	0.11 0.002 0.76	Gas/Vapor	EE	
22E	Upward Vertical Stack	TK-201	Condensate Tank 2	13C	VRU-98% control	C	8,760	VOC Total HAPs CO2e	1.21 0.02 8.62	5.29 0.08 37.77	0.02 0.0003 0.17	0.11 0.002 0.76	Gas/Vapor	EE	

23E	Upward Vertical Stack	TK-1500	Produced Water Tank 1	13C	VRU-98% control	C	8,760	VOC Total HAPs CO2e	0.08 0.0011 0.55	0.34 0.005 2.42	0.0016 2.2E-5 0.011	0.007 0.0001 0.05	Gas/Vapor	EE	
24E	Upward Vertical Stack	TK-1501	Produced Water Tank 2	13C	VRU-98% control	C	8,760	VOC Total HAPs CO2e	0.08 0.0011 0.55	0.34 0.005 2.42	0.0016 2.2E-5 0.011	0.007 0.0001 0.05	Gas/Vapor	EE	
26E	Upward Vertical Stack	FLARE 1	Flare combustion device 1	---	---	C	8,760	NOx CO VOC PM10 Total HAPs CO2e	--- --- --- --- --- ---	--- --- --- --- --- ---	0.33 1.78 0.0001 0.0001 3.4E-5 563	1.44 7.79 0.0004 0.0006 0.0002 2465	Gas/Vapor	EE	
27E	Upward Vertical Stack	CATHT 1	Catalytic Heater for Generator Fuel	---	---	C	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	0.0029 0.0025 1.6 E-4 2.2 E-4 1.8 E-5 6 E-5 2 E-6 2.82	0.013 0.011 7.1 E-4 0.001 7.7 E-5 2.4 E-4 1 E-5 12	0.0029 0.0025 1.6 E-4 2.2 E-4 1.8 E-5 6 E-5 2 E-6 2.82	0.013 0.011 7.1 E-4 0.001 7.7 E-5 2.4 E-4 1 E-5 12	Gas/Vapor	EE	
28E	Upward Vertical Stack	C-1200	Compressor engine 12	15C	NSCR catalyst	C	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.74 47.04 1.70 0.27 0.008 0.35 0.19 2080	222.24 206.02 7.46 1.18 0.036 1.54 0.81 9109	1.27 1.18 0.27 0.27 0.008 0.18 0.019 1993	5.56 5.15 1.19 1.18 0.036 0.81 0.081 8731	Gas/Vapor	EE	

29E	Upward Vertical Stack	C-1300	Com-pressor engine 13	16C	NSCR catalyst	C	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
								CO	47.04	206.02	1.18	5.15			
								VOC	1.70	7.46	0.27	1.19			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2080	9109	1993	8731			

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit emissions are not typically considered to be fugitive and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugitive emission activities.

¹ Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.

² Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (ie., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).

³ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. **LIST** Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. **DO NOT LIST** H₂, H₂O, N₂, O₂, and Noble Gases.

⁴ Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁵ Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁶ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

⁷ Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmv) are used. If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m³) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO₂, use units of ppmv (See 45CSR10).

**Attachment J
EMISSION POINTS DATA SUMMARY SHEET**

Table 2: Release Parameter Data								
Emission Point ID No.	Inner Diameter (ft.)	Exit Gas			Emission Point Elevation (ft)		UTM Coordinates (km)	
		Temp. (°F)	Volumetric Flow ¹ (acfm) <i>at operating conditions</i>	Velocity (fps)	Ground Level (<i>Height above mean sea level</i>)	Stack Height ²	Northing	Easting
1E/1C	1.1	1224	8858	112	956	25	4363.536	511.678
2E/2C	1.1	1224	8858	112	956	25	4363.529	511.688
3E/3C	1.1	1224	8858	112	956	25	4363.522	511.697
4E/4C	1.1	1224	8858	112	956	25	4363.515	511.707
5E/5C	1.1	1224	8858	112	956	25	4363.508	511.716
6E/6C	1.1	1224	8858	112	956	25	4363.500	511.726
7E/7C	1.1	1224	8858	112	956	25	4363.493	511.735
8E/8C	1.1	1224	8858	112	956	25	4363.486	511.745
9E/9C	1.1	1224	8858	112	956	25	4363.581	511.754
10E/10C	1.1	1224	8858	112	956	25	4363.574	511.764
11E/11C	1.1	1224	8858	112	956	25	4363.464	511.773
12E	NA	535	3.99 kg/s mass flow	TBD	956	10	4363.564	511.639
13E	NA	535	3.99 kg/s mass flow	TBD	956	10	4363.581	511.626
14E/12C/26E	5	1400	TBD	TBD	956	15	4363.442	511.659
15E	Combusted in 16E		TBD	TBD	956	TBD	4363.442	511.659
16E	TBD		TBD	TBD	956	TBD	4363.442	511.659
17E/12C/26E	5	1400	TBD	TBD	956	15	4363.426	511.684
18E	Combusted in 19E		N/A	N/A	956	N/A	4363.426	511.684
19E	TBD	TBD	N/A	N/A	956	N/A	4363.426	511.684
20E-25E/13C-14C	Emissions captured in closed loop system with VRU				956	N/A	4363.466	511.568
27E	TBD	TBD	TBD	TBD	956	TBD	4363.569	511.646

28E/15C	1.1	1224	8858	112	956	25	4363.489	511.753
29E/16C	1.1	1224	8858	112	956	25	4363.487	511.765

¹ Give at operating conditions. Include inerts.

² Release height of emissions above ground level.

Attachment K.
Fugitive Emissions Data Summary Sheet

Attachment K

FUGITIVE EMISSIONS DATA SUMMARY SHEET

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not typically considered to be fugitive, and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET.

Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS
1.) Will there be haul road activities? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No <input checked="" type="checkbox"/> If YES, then complete the HAUL ROAD EMISSIONS UNIT DATA SHEET.
2.) Will there be Storage Piles? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No <input type="checkbox"/> If YES, complete Table 1 of the NONMETALLIC MINERALS PROCESSING EMISSIONS UNIT DATA SHEET.
3.) Will there be Liquid Loading/Unloading Operations? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No <input checked="" type="checkbox"/> If YES, complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET.
4.) Will there be emissions of air pollutants from Wastewater Treatment Evaporation? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No <input type="checkbox"/> If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
5.) Will there be Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, open-ended valves, sampling connections, flanges, agitators, cooling towers, etc.)? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No <input checked="" type="checkbox"/> If YES, complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS UNIT DATA SHEET.
6.) Will there be General Clean-up VOC Operations? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No <input type="checkbox"/> If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
7.) Will there be any other activities that generate fugitive emissions? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No <input checked="" type="checkbox"/> If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form.
If you answered "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions Summary."

FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants - Chemical Name/CAS ¹	Maximum Potential Uncontrolled Emissions ²		Maximum Potential Controlled Emissions ³		Est. Method Used ⁴
		lb/hr	ton/yr	lb/hr	ton/yr	
Haul Road/Road Dust Emissions Paved Haul Roads						EE
Unpaved Haul Roads	PM-10 PM-2.5	0.05 0.005	0.22 0.02	0.05 0.005	0.22 0.02	EE
Storage Pile Emissions						
Loading/Unloading Operations	VOCs Total HAPs CO2e	77.14 1.10 551	8.11 0.12 57.91	77.14 1.10 551	8.11 0.12 57.91	EE
Wastewater Treatment Evaporation & Operations						
Equipment Leaks	VOCs Total HAPs CO2e	1.79 0.0045 32.06	7.84 0.020 140	1.79 0.0045 32.06	7.84 0.020 140	EE
General Clean-up VOC Emissions						
Other – Venting Episodes	VOCs Total HAPs CO2e	Does not apply	10.73 0.027 773	Does not apply	10.73 0.027 773	EE

¹ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. DO NOT LIST H₂, H₂O, N₂, O₂, and Noble Gases.

² Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

³ Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁴ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

**Attachment L.
Emission Unit Data Sheets**

Compressor Engines

NATURAL GAS COMPRESSOR/GENERATOR ENGINE DATA SHEET

Source Identification Number ¹		1E		2E		3E	
Engine Manufacturer and Model		Waukesha, 7044 GSI		Waukesha, 7044 GSI		Waukesha, 7044 GSI	
Manufacturer's Rated bhp/rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm	
Source Status ²		MS		MS		MS	
Date Installed/Modified/Removed ³		April 2016		April 2016		April 2016	
Engine Manufactured/Reconstruction Date ⁴		Late 2013/Early 2014		Late 2013/Early 2014		Late 2013/Early 2014	
Is this a Certified Stationary Spark Ignition Engine according to 40CFR60 Subpart JJJJ? (Yes or No) ⁵		No		No		No	
Engine, Fuel and Combustion Data	Engine Type ⁶	RB4S		RB4S		RB4S	
	APCD Type ⁷	NSCR		NSCR		NSCR	
	Fuel Type ⁸	PQ		PQ		PQ	
	H ₂ S (gr/100 scf)	0		0		0	
	Operating bhp/rpm	1680 bhp/1200 rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm	
	BSFC (Btu/bhp-hr)	8,272		8,272		8,272	
	Fuel throughput (ft ³ /hr)	12,120		12,120		12,120	
	Fuel throughput (MMft ³ /yr)	106.17		106.17		106.17	
	Operation (hrs/yr)	8,760		8,760		8,760	
Reference ⁹	Potential Emissions ¹⁰	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	NO _x	1.27	5.56	1.27	5.56	1.27	5.56
MD	CO	1.18	5.15	1.18	5.15	1.18	5.15
MD	VOC	0.27	1.19	0.27	1.19	0.27	1.19
AP	SO ₂	0.0082	0.036	0.0082	0.036	0.0082	0.036
AP	PM ₁₀	0.27	1.18	0.27	1.18	0.27	1.18
MD	Formaldehyde	0.019	0.081	0.019	0.081	0.019	0.081
MD	CO _{2e}	1993	8731	1993	8731	1993	8731

Source Identification Number ¹		4E		5E		6E	
Engine Manufacturer and Model		Waukesha, 7044 GSI		Waukesha, 7044 GSI		Waukesha, 7044 GSI	
Manufacturer's Rated bhp/rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm	
Source Status ²		MS		MS		MS	
Date Installed/Modified/Removed ³		April 2016		April 2016		April 2016	
Engine Manufactured/Reconstruction Date ⁴		Late 2013/Early 2014		Late 2013/Early 2014		Late 2013/Early 2014	
Is this a Certified Stationary Spark Ignition Engine according to 40CFR60 Subpart JJJJ? (Yes or No) ⁵		No		No		No	
Engine, Fuel and Combustion Data	Engine Type ⁶	RB4S		RB4S		RB4S	
	APCD Type ⁷	NSCR		NSCR		NSCR	
	Fuel Type ⁸	PQ		PQ		PQ	
	H ₂ S (gr/100 scf)	0		0		0	
	Operating bhp/rpm	1680 bhp/1200 rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm	
	BSFC (Btu/bhp-hr)	8,272		8,272		8,272	
	Fuel throughput (ft ³ /hr)	12,120		12,120		12,120	
	Fuel throughput (MMft ³ /yr)	106.17		106.17		106.17	
	Operation (hrs/yr)	8,760		8,760		8,760	
Reference ⁹	Potential Emissions ¹⁰	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	NO _x	1.27	5.56	1.27	5.56	1.27	5.56
MD	CO	1.18	5.15	1.18	5.15	1.18	5.15
MD	VOC	0.27	1.19	0.27	1.19	0.27	1.19
AP	SO ₂	0.0082	0.036	0.0082	0.036	0.0082	0.036
AP	PM ₁₀	0.27	1.18	0.27	1.18	0.27	1.18
MD	Formaldehyde	0.019	0.081	0.019	0.081	0.019	0.081
MD	CO _{2e}	1993	8731	1993	8731	1993	8731

Source Identification Number ¹		7E		8E		9E	
Engine Manufacturer and Model		Waukesha, 7044 GSI		Waukesha, 7044 GSI		Waukesha, 7044 GSI	
Manufacturer's Rated bhp/rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm	
Source Status ²		MS		MS		MS	
Date Installed/Modified/Removed ³		April 2016		April 2016		April 2016	
Engine Manufactured/Reconstruction Date ⁴		Late 2013/Early 2014		Late 2013/Early 2014		Late 2013/Early 2014	
Is this a Certified Stationary Spark Ignition Engine according to 40CFR60 Subpart JJJJ? (Yes or No) ⁵		No		No		No	
Engine, Fuel and Combustion Data	Engine Type ⁶	RB4S		RB4S		RB4S	
	APCD Type ⁷	NSCR		NSCR		NSCR	
	Fuel Type ⁸	PQ		PQ		PQ	
	H ₂ S (gr/100 scf)	0		0		0	
	Operating bhp/rpm	1680 bhp/1200 rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm	
	BSFC (Btu/bhp-hr)	8,272		8,272		8,272	
	Fuel throughput (ft ³ /hr)	12,120		12,120		12,120	
	Fuel throughput (MMft ³ /yr)	106.17		106.17		106.17	
	Operation (hrs/yr)	8,760		8,760		8,760	
Reference ⁹	Potential Emissions ¹⁰	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	NO _x	1.27	5.56	1.27	5.56	1.27	5.56
MD	CO	1.18	5.15	1.18	5.15	1.18	5.15
MD	VOC	0.27	1.19	0.27	1.19	0.27	1.19
AP	SO ₂	0.0082	0.036	0.0082	0.036	0.0082	0.036
AP	PM ₁₀	0.27	1.18	0.27	1.18	0.27	1.18
MD	Formaldehyde	0.019	0.081	0.019	0.081	0.019	0.081
MD	CO _{2e}	1993	8731	1993	8731	1993	8731

Source Identification Number ¹		10E		11E		28E	
Engine Manufacturer and Model		Waukesha, 7044 GSI		Waukesha, 7044 GSI		Waukesha, 7044 GSI	
Manufacturer's Rated bhp/rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm	
Source Status ²		MS		MS		NS	
Date Installed/Modified/Removed ³		April 2016		April 2016		April 2016	
Engine Manufactured/Reconstruction Date ⁴		Late 2013/Early 2014		Late 2013/Early 2014		TBD	
Is this a Certified Stationary Spark Ignition Engine according to 40CFR60 Subpart JJJJ? (Yes or No) ⁵		No		No		No	
Engine, Fuel and Combustion Data	Engine Type ⁶	RB4S		RB4S		RB4S	
	APCD Type ⁷	NSCR		NSCR		NSCR	
	Fuel Type ⁸	PQ		PQ		PQ	
	H ₂ S (gr/100 scf)	0		0		0	
	Operating bhp/rpm	1680 bhp/1200 rpm		1680 bhp/1200 rpm		1680 bhp/1200 rpm	
	BSFC (Btu/bhp-hr)	8,272		8,272		8,272	
	Fuel throughput (ft ³ /hr)	12,120		12,120		12,120	
	Fuel throughput (MMft ³ /yr)	106.17		106.17		106.17	
	Operation (hrs/yr)	8,760		8,760		8,760	
Reference ⁹	Potential Emissions ¹⁰	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	NO _x	1.27	5.56	1.27	5.56	1.27	5.56
MD	CO	1.18	5.15	1.18	5.15	1.18	5.15
MD	VOC	0.27	1.19	0.27	1.19	0.27	1.19
AP	SO ₂	0.0082	0.036	0.0082	0.036	0.0082	0.036
AP	PM ₁₀	0.27	1.18	0.27	1.18	0.27	1.18
MD	Formaldehyde	0.019	0.081	0.019	0.081	0.019	0.081
MD	CO _{2e}	1993	8731	1993	8731	1993	8731

Source Identification Number ¹		29E					
Engine Manufacturer and Model		Waukesha, 7044 GSI					
Manufacturer's Rated bhp/rpm		1680 bhp/1200 rpm					
Source Status ²		NS					
Date Installed/Modified/Removed ³		April 2016					
Engine Manufactured/Reconstruction Date ⁴		TBD					
Is this a Certified Stationary Spark Ignition Engine according to 40CFR60 Subpart JJJJ? (Yes or No) ⁵		No					
Engine, Fuel and Combustion Data	Engine Type ⁶	RB4S					
	APCD Type ⁷	NSCR					
	Fuel Type ⁸	PQ					
	H ₂ S (gr/100 scf)	0					
	Operating bhp/rpm	1680 bhp/1200 rpm					
	BSFC (Btu/bhp-hr)	8,272					
	Fuel throughput (ft ³ /hr)	12,120					
	Fuel throughput (MMft ³ /yr)	106.17					
	Operation (hrs/yr)	8,760					
Reference ⁹	Potential Emissions ¹⁰	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	NO _x	1.27	5.56				
MD	CO	1.18	5.15				
MD	VOC	0.27	1.19				
AP	SO ₂	0.0082	0.036				
AP	PM ₁₀	0.27	1.18				
MD	Formaldehyde	0.019	0.081				
MD	CO _{2e}	1993	8731				

1. Enter the appropriate Source Identification Number for each natural gas-fueled reciprocating internal combustion compressor/generator engine located at the compressor station. Multiple compressor engines should be designated CE-1, CE-2, CE-3 etc. Generator engines should be designated GE-1, GE-2, GE-3 etc. If more than three (3) engines exist, please use additional sheets.
2. Enter the Source Status using the following codes:

NS	Construction of New Source (installation)	ES	Existing Source
MS	Modification of Existing Source	RS	Removal of Source
3. Enter the date (or anticipated date) of the engine's installation (construction of source), modification or removal.

4. Enter the date that the engine was manufactured, modified or reconstructed.
5. Is the engine a certified stationary spark ignition internal combustion engine according to 40CFR60 Subpart JJJJ. If so, the engine and control device must be operated and maintained in accordance with the manufacturer's emission-related written instructions. You must keep records of conducted maintenance to demonstrate compliance, but no performance testing is required. If the certified engine is not operated and maintained in accordance with the manufacturer's emission-related written instructions, the engine will be considered a non-certified engine and you must demonstrate compliance according to 40CFR§60.4243a(2)(i) through (iii), as appropriate.

Provide a manufacturer's data sheet for all engines being registered.

6. Enter the Engine Type designation(s) using the following codes:

LB2S Lean Burn Two Stroke	RB4S Rich Burn Four Stroke
LB4S Lean Burn Four Stroke	
7. Enter the Air Pollution Control Device (APCD) type designation(s) using the following codes:

A/F Air/Fuel Ratio	IR Ignition Retard
HEIS High Energy Ignition System	SIPC Screw-in Precombustion Chambers
PSC Prestratified Charge	LEC Low Emission Combustion
NSCR Rich Burn & Non-Selective Catalytic Reduction	SCR Lean Burn & Selective Catalytic Reduction
8. Enter the Fuel Type using the following codes:

PQ Pipeline Quality Natural Gas	RG Raw Natural Gas
---------------------------------	--------------------
9. Enter the Potential Emissions Data Reference designation using the following codes. Attach all referenced data to this *Compressor/Generator Data Sheet(s)*.

MD Manufacturer's Data	AP AP-42
GR GRI-HAPCalc™	OT Other
10. Enter each engine's Potential to Emit (PTE) for the listed regulated pollutants in pounds per hour and tons per year. PTE shall be calculated at manufacturer's rated brake horsepower and may reflect reduction efficiencies of listed Air Pollution Control Devices. Emergency generator engines may use 500 hours of operation when calculating PTE. PTE data from this data sheet shall be incorporated in the *Emissions Summary Sheet*.



Monroe Compressor Station - Tyler County, WV

VHP - L7044GSI

Kleinfelder Kaitlin Meszaros 719-632-3593 kmeszaros@kleinfelder.com

Gas Compression - Continuous

ENGINE SPEED (rpm):	1200	COOLING SYSTEM:	JW, IC + OC
DISPLACEMENT (in3):	7040	INTERCOOLER WATER INLET (°F):	130
COMPRESSION RATIO:	8:1	JACKET WATER OUTLET (°F):	180
IGNITION SYSTEM:	ESM	JACKET WATER CAPACITY (gal):	100
EXHAUST MANIFOLD:	Water Cooled	AUXILIARY WATER CAPACITY (gal):	11
COMBUSTION:	Rich Burn, Turbocharged	LUBE OIL CAPACITY (gal):	190
ENGINE DRY WEIGHT (lbs):	21000	MAX. EXHAUST BACKPRESSURE (in. H2O):	18
AIR/FUEL RATIO SETTING:	0.38% CO	MAX. AIR INLET RESTRICTION (in. H2O):	15
ENGINE SOUND LEVEL (dBA)	104	EXHAUST SOUND LEVEL (dBA)	111

SITE CONDITIONS:

FUEL:		ALTITUDE (ft):	956
FUEL PRESSURE RANGE (psig):	30 - 60	MAXIMUM INLET AIR TEMPERATURE (°F):	100
FUEL HHV (BTU/ft3):	1,271.5	FUEL WKI:	60.2
FUEL LHV (BTU/ft3):	1,149.5		

SITE SPECIFIC TECHNICAL DATA

POWER RATING	UNITS	MAX RATING AT 100 °F AIR TEMP	SITE RATING AT MAXIMUM INLET AIR TEMPERATURE OF 100 °F		
			100%	75%	50%
CONTINUOUS ENGINE POWER	BHP	1680	1680	1260	843
OVERLOAD	% 2/24 hr	2	2	-	-
MECHANICAL EFFICIENCY (LHV)	%	30.8	30.8	29.4	28.6
CONTINUOUS POWER AT FLYWHEEL	BHP	1680	1680	1260	843

based on no auxiliary engine driven equipment

FUEL CONSUMPTION

FUEL CONSUMPTION (LHV)	BTU/BHP-hr	8272	8272	8653	8900
FUEL CONSUMPTION (HHV)	BTU/BHP-hr	9151	9151	9572	9845
FUEL FLOW	SCFM	202	202	158	109

based on fuel analysis LHV

HEAT REJECTION

JACKET WATER (JW)	BTU/hr x 1000	4152	4152	3414	2512
LUBE OIL (OC)	BTU/hr x 1000	571	571	520	431
INTERCOOLER (IC)	BTU/hr x 1000	268	268	185	92
EXHAUST	BTU/hr x 1000	4196	4195	3139	1925
RADIATION	BTU/hr x 1000	706	706	651	541

EMISSIONS

NOx (NO + NO2)	g/bhp-hr	13.7	13.7	14.8	16.5
CO	g/bhp-hr	12.7	12.7	12.6	11.4
THC	g/bhp-hr	2.3	2.3	2.2	1.8
NMHC	g/bhp-hr	0.96	0.96	0.92	0.75
NM, NEHC	g/bhp-hr	0.46	0.46	0.43	0.35
CH4	g/bhp-hr	1.33	1.33	1.26	1.03
CO2	g/bhp-hr	528	528	553	568
CO2e	g/bhp-hr	556	556	579	590
CH2O	g/bhp-hr	0.05	0.05	0.05	0.05

AIR INTAKE / EXHAUST GAS

INDUCTION AIR FLOW	SCFM	2545	2545	1997	1373
EXHAUST GAS MASS FLOW	lb/hr	11835	11835	9285	6387
EXHAUST GAS FLOW	ACFM	8858	8858	6759	4355
EXHAUST TEMPERATURE	°F	1224	1224	1178	1074

at exhaust temp, 14.5 psia

HEAT EXCHANGER SIZING

TOTAL JACKET WATER CIRCUIT (JW)	BTU/hr x 1000	4709
TOTAL AUXILIARY WATER CIRCUIT (IC + OC)	BTU/hr x 1000	951

COOLING SYSTEM WITH ENGINE MOUNTED WATER PUMPS

JACKET WATER PUMP MIN. DESIGN FLOW	GPM	450
JACKET WATER PUMP MAX. EXTERNAL RESTRICTION	psig	16
AUX WATER PUMP MIN. DESIGN FLOW	GPM	79
AUX WATER PUMP MAX. EXTERNAL RESTRICTION	psig	44



Monroe Compressor Station - Tyler County, WV

Kleinfelder Kaitlin Meszaros 719-632-3593 kmeszaros@kleinfelder.com

VHP - L7044GSI

Gas Compression - Continuous

FUEL COMPOSITION

HYDROCARBONS:

		<u>Mole or Volume %</u>
Methane	CH4	75.007
Ethane	C2H6	15.315
Propane	C3H8	4.9896
Iso-Butane	I-C4H10	0.5963
Normal Butane	N-C4H10	1.3659
Iso-Pentane	I-C5H12	0.3416
Normal Pentane	N-C5H12	0.3862
Hexane	C6H14	0.3125
Heptane	C7H16	0
Ethene	C2H4	0
Propene	C3H6	0

SUM HYDROCARBONS 98.314

NON-HYDROCARBONS:

Nitrogen	N2	1.2734
Oxygen	O2	0.2744
Helium	He	0
Carbon Dioxide	CO2	0.1384
Carbon Monoxide	CO	0
Hydrogen	H2	0
Water Vapor	H2O	0

TOTAL FUEL 100

FUEL:

FUEL PRESSURE RANGE (psig):	30 - 60
FUEL WKI:	60.2
FUEL SLHV (BTU/ft3):	1129.46
FUEL SLHV (MJ/Nm3):	44.41
FUEL LHV (BTU/ft3):	1149.46
FUEL LHV (MJ/Nm3):	45.20
FUEL HHV (BTU/ft3):	1271.53
FUEL HHV (MJ/Nm3):	50.00
FUEL DENSITY (SG):	0.73

Standard Conditions per ASTM D3588-91 [60°F and 14.696psia] and ISO 6976:1996-02-01[25, V(0;101.325)].
 Based on the fuel composition, supply pressure and temperature, liquid hydrocarbons may be present in the fuel. No liquid hydrocarbons are allowed in the fuel. The fuel must not contain any liquid water.
 Waukesha recommends both of the following:
 1) Dew point of the fuel gas to be at least 20°F (11°C) below the measured temperature of the gas at the inlet of the engine fuel regulator.
 2) A fuel filter separator to be used on all fuels except commercial quality natural gas.
 Refer to the 'Fuel and Lubrication' section of 'Technical Data' or contact the Waukesha Application Engineering Department for additional information on fuels, or LHV and WKI* calculations.
 * Trademark of General Electric Company

FUEL CONTAMINANTS

Total Sulfur Compounds	0 % volume	Total Sulfur Compounds	0 µg/BTU
Total Halogen as Chloride	0 % volume	Total Halogen as Chloride	0 µg/BTU
Total Ammonia	0 % volume	Total Ammonia	0 µg/BTU
<u>Siloxanes</u>		Total Siloxanes (as Si)	0 µg/BTU
Tetramethyl silane	0 % volume		
Trimethyl silanol	0 % volume		
Hexamethyldisiloxane (L2)	0 % volume		
Hexamethylcyclotrisiloxane (D3)	0 % volume		
Octamethyltrisiloxane (L3)	0 % volume		
Octamethylcyclotetrasiloxane (D4)	0 % volume		
Decamethyltetrasiloxane (L4)	0 % volume		
Decamethylcyclopentasiloxane (D5)	0 % volume		
Dodecamethylpentasiloxane (L5)	0 % volume		
Dodecamethylcyclohexasiloxane (D6)	0 % volume		
Others	0 % volume		

Calculated fuel contaminant analysis will depend on the entered fuel composition and selected engine model.

No water or hydrocarbon condensates are allowed in the engine. Requires liquids removal.



Monroe Compressor Station - Tyler County, WV

Kleinfelder Kaitlin Meszaros 719-632-3593 kmeszaros@kleinfelder.com

VHP - L7044GSI

Gas Compression - Continuous

NOTES

1. All data is based on engines with standard configurations unless noted otherwise.
2. Power rating is adjusted for fuel, site altitude, and site air inlet temperature, in accordance with ISO 3046/1 with tolerance of $\pm 3\%$.
3. Fuel consumption is presented in accordance with ISO 3046/1 with a tolerance of $-0 / +5\%$ at maximum rating. Fuel flow calculation based on fuel LHV and fuel consumption with a tolerance of $-0/+5\%$. For sizing piping and fuel equipment, it is recommended to include the 5% tolerance.
4. Heat rejection tolerances are $\pm 30\%$ for radiation, and $\pm 8\%$ for jacket water, lube oil, intercooler, and exhaust energy.
5. Emission levels are given at engine exhaust outlet flange prior to any after treatment. Values are based on a new engine operating at indicated site conditions, and adjusted to the specified timing and air/fuel ratio at rated load. Emissions are at an absolute humidity of 75 grains H₂O/lb (10.71 g H₂O/kg) of dry air. Emission levels may vary subject to instrumentation, measurement, ambient conditions, fuel quality, and engine variation. Engine may require adjustment on-site to meet emission values, which may affect engine performance and heat output. NO_x, CO, THC, and NMHC emission levels are listed as a not to exceed limit, all other emission levels are estimated. CO₂ emissions based on EPA Federal Register/Vol. 74, No. 209/Friday, October 30, 2009 Rules and Regulations 56398, 56399 (3) Tier 3 Calculation Methodology, Equation C-5.
6. Air flow is based on undried air with a tolerance of $\pm 7\%$.
7. Exhaust temperature given at engine exhaust outlet flange with a tolerance of $\pm 75^{\circ}\text{F}$ (42°C).
8. Exhaust gas mass flow value is based on a "wet basis" with a tolerance of $\pm 7\%$.
9. Inlet air restrictions based on full rated engine load. Exhaust backpressure based on 158 PSI BMEP and 1200 RPM. Refer to the engine specification section of Waukesha's standard technical data for more information.
10. Cooling circuit capacity, lube oil capacity, and engine dry weight values are typical.
11. Fuel must conform to Waukesha's "Gaseous Fuel Specification" S7884-7 or most current version. Fuel may require treatment to meet current fuel specification.
12. Heat exchanger sizing values given as the maximum heat rejection of the circuit, with applied tolerances and an additional 5% reserve factor.
13. Fuel volume flow calculation in english units is based on 100% relative humidity of the fuel gas at standard conditions of 60°F and 14.696 psia (29.92 inches of mercury; 101.325 kPa).
14. Fuel volume flow calculation in metric units is based on 100% relative humidity of the fuel gas at a combustion temperature of 25°C and metering conditions of 0°C and 101.325 kPa (14.696 psia; 29.92 inches of mercury). This is expressed as [25, V(0;101.325)].
15. Engine sound data taken with the microphone at 1 m (3.3 ft) from the side of the engine at the approximate front-to-back centerline. Microphone height was at intake manifold level. Engine sound pressure data may be different at front, back and opposite side locations. Exhaust sound data taken with microphone 1 meter (3.3 ft) away and 1 meter (3.3 ft) to the side of the exhaust outlet.
16. Due to variation between test conditions and final site conditions, such as exhaust configuration and background sound level, sound pressure levels under site conditions may be different than those tabulated above.
17. Cooling system design flow is based on minimum allowable cooling system flow. Cooling system maximum external restriction is defined as the allowable restriction at the minimum cooling system flow. Refer to technical data sheets S-5136-34 and S-6543-36 (or latest version) for more information.
18. Continuous Power Rating: The highest load and speed that can be applied 24 hours per day, seven days per week, 365 days per year except for normal maintenance at indicated ambient reference conditions and fuel. It is permissible to operate the engine at the indicated overload power, for two hours in every 24 hour period.

REQUIRED OPTION CODES

Dehydrators

West Virginia Department of Environmental Protection

DIVISION OF AIR QUALITY : (304) 926-0475
 WEB PAGE: <http://www.wvdep.org>

Division of Air Quality

40 CFR Part 63; Subpart HH & HHH Registration Form

Complete this form for any oil and natural gas production or natural gas transmission and storage facility that uses an affected unit under HH/HHH, whether subject or not.

Section A: Facility Description			
Affected facility actual annual average natural gas throughput (scf/day):	145,000,000 (72,500,000 per dehy)		
Affected facility actual annual average hydrocarbon liquid throughput: (bbl/day):	195		
The affected facility processes, upgrades, or stores hydrocarbon liquids prior to custody transfer.	<input checked="" type="radio"/> Yes	No	
The affected facility processes, upgrades, or stores natural gas prior to the point at which natural gas (NG) enters the NG transmission and storage source category or is delivered to the end user.	<input checked="" type="radio"/> Yes	No	
The affected facility is: <input checked="" type="checkbox"/> prior to a NG processing plant <input type="checkbox"/> a NG processing plant <input type="checkbox"/> prior to the point of custody transfer and there is no NG processing plant			
The affected facility transports or stores natural gas prior to entering the pipeline to a local distribution company or to a final end user (if there is no local distribution company).	<input checked="" type="radio"/> Yes	No	
The affected facility exclusively processes, stores, or transfers black oil.	Yes	<input checked="" type="radio"/> No	
Initial producing gas-to-oil ratio (GOR): _____scf/bbl	API gravity: _____degrees		
Section B: Dehydration Unit (if applicable) ¹			
Description: Monroe Compressor Station Dehydrators (DEHY1 and DEHY2)			
Date of Installation: Modified 2016	Annual Operating Hours: 8,760	Burner rating (MMbtu/hr): 1.5	
Exhaust Stack Height (ft): TBD	Stack Diameter (ft): TBD	Stack Temp. (°F): 212	
Glycol Type:	<input checked="" type="checkbox"/> TEG <input type="checkbox"/> EG <input type="checkbox"/> Other:		
Glycol Pump Type:	<input type="checkbox"/> Electric <input checked="" type="checkbox"/> Gas	If gas, what is the volume ratio? <u>0.032</u> ACFM/gpm	
Condenser installed?	<input checked="" type="checkbox"/> Yes <input type="checkbox"/> No	Exit Temp. 145 °F	Condenser Pressure <u>0</u> psig
Incinerator/flare installed?	<input checked="" type="checkbox"/> Yes <input type="checkbox"/> No	Destruction Eff. <u>98</u> %	
Other controls installed?	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	Describe:	
Wet Gas ² : (Upstream of Contact Tower)	Gas Temp.: <u>120</u> °F	Gas Pressure <u>1,000</u> psig	Saturated Gas? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No If no, water content _____ lb/MMSCF
Dry Gas: (Downstream of Contact Tower)	Gas Flowrate(MMSCFD) Actual _____ Design <u>72.5</u>	Water Content <u>7.0</u> lb/MMSCF	
Lean Glycol:	Circulation rate (gpm) Actual ³ _____ Maximum ⁴ <u>7.5</u>	Pump make/model: Kimray 45015PV	
Glycol Flash Tank (if applicable):	Temp.: <u>190</u> °F	Pressure <u>35</u> psig	Vented? Yes <input type="checkbox"/> No <input checked="" type="checkbox"/> If no, describe vapor control: Vent gas used in reboiler as fuel or sent to VRU system
Stripping Gas (if applicable):	Source of gas: Dry gas, if used	Rate <u>9</u> scfm	

Please attach the following required dehydration unit information:

1. System map indicating the chain of custody information. See Page 43 of this document for an example of a gas flow schematic. It is not intended that the applicant provide this level of detail for all sources. The level of detail that is necessary is to establish where the custody transfer points are located. This can be accomplished by submitting a process flow diagram indicating custody transfer points and the natural gas flow. However, the DAQ reserves the right to request more detailed information in order to make the necessary decisions.
2. Extended gas analysis from the Wet Gas Stream including mole percents of C₁-C₈, benzene, ethylbenzene, toluene, xylene and n-Hexane, using Gas Processors Association (GPA) 2286 (or similar). A sample should be taken from the inlet gas line, downstream from any inlet separator, and using a manifold to remove entrained liquids from the sample and a probe to collect the sample from the center of the gas line. GPA standard 2166 reference method or a modified version of EPA Method TO-14, (or similar) should be used.
3. GRI-GLYCalc Ver. 3.0 aggregate report based on maximum Lean Glycol circulation rate and maximum throughput.
4. Detailed calculations of gas or hydrocarbon flow rate.

Section C: Facility NESHAPS Subpart HH/HHH status

	<input checked="" type="checkbox"/> Subject to Subpart HH - applies, but is exempt through < 1 tpy benzene exemption	
Affected facility status:	<input type="checkbox"/> Subject to Subpart HHH	
(choose only one)	<input checked="" type="checkbox"/> Not Subject	<input checked="" type="checkbox"/> < 10/25 TPY
	because:	<input type="checkbox"/> Affected facility exclusively handles black oil
		<input type="checkbox"/> The facility wide actual annual average NG throughput is < 650 thousand scf/day and facility wide actual annual average hydrocarbon liquid is < 250 bpd
		<input type="checkbox"/> No affected source is present

NATURAL GAS GLYCOL DEHYDRATION UNIT DATA SHEET

General Glycol Dehydration Unit Data		Manufacturer and Model		Exterran, 72.5 MMscfd	
		Max Dry Gas Flow Rate (MMscf/day)		72.5	
		Design Heat Input (MMBtu/hr)		1.5	
		Design Type (DEG or TEG)		TEG	
		Source Status ²		MS	
		Date Installed/Modified/Removed ³		April 2016	
		Regenerator Still Vent APCD ⁴		FL	
		Fuel HV (Btu/scf)		1,149	
		H ₂ S Content (gr/100 scf)		0	
		Operation (hrs/yr)		8,760	
Source ID # ¹	Vent	Reference ⁵	Potential Emissions ⁶	lbs/hr	tons/yr
16E	Reboiler Vent	AP	NO _x	0.18	0.81
		AP	CO	0.15	0.68
		AP	VOC	0.010	0.044
		AP	SO ₂	0.0011	0.0048
		AP	PM ₁₀	0.014	0.061
14E	Glycol Regenerator Still Vent	GRI-GLYCalc TM	VOC	0.31	1.37
		GRI-GLYCalc TM	Benzene	0.031	0.14
		GRI-GLYCalc TM	Ethylbenzene	0.00	0.00
		GRI-GLYCalc TM	Toluene	0.049	0.21
		GRI-GLYCalc TM	Xylenes	0.040	0.17
		GRI-GLYCalc TM	n-Hexane	0.0074	0.032
15E	Flash Gas Tank Vent	GRI-GLYCalc TM	VOC	0.90	3.94
		GRI-GLYCalc TM	Benzene	0.0079	0.034
		GRI-GLYCalc TM	Ethylbenzene	0.00	0.00
		GRI-GLYCalc TM	Toluene	0.0092	0.040
		GRI-GLYCalc TM	Xylenes	0.0036	0.016
		GRI-GLYCalc TM	n-Hexane	0.026	0.12

General Glycol Dehydration Unit Data		Manufacturer and Model		Exterran, 72.5 MMscfd	
		Max Dry Gas Flow Rate (mmscf/day)		72.5	
		Design Heat Input (mmBtu/hr)		1.5	
		Design Type (DEG or TEG)		TEG	
		Source Status ²		MS	
		Date Installed/Modified/Removed ³		April 2016	
		Regenerator Still Vent APCD ⁴		FL	
		Fuel HV (Btu/scf)		1,149	
		H ₂ S Content (gr/100 scf)		0	
		Operation (hrs/yr)		8,760	
Source ID # ¹	Vent	Reference ⁵	Potential Emissions ⁶	lbs/hr	tons/yr
19E	Reboiler Vent	AP	NO _x	0.18	0.81
		AP	CO	0.15	0.68
		AP	VOC	0.010	0.044
		AP	SO ₂	0.0011	0.0048
		AP	PM ₁₀	0.014	0.061
17E	Glycol Regenerator Still Vent	GRI-GLYCalc™	VOC	0.31	1.37
		GRI-GLYCalc™	Benzene	0.031	0.14
		GRI-GLYCalc™	Ethylbenzene	0.00	0.00
		GRI-GLYCalc™	Toluene	0.049	0.21
		GRI-GLYCalc™	Xylenes	0.040	0.17
		GRI-GLYCalc™	n-Hexane	0.0074	0.032
18E	Flash Gas Tank Vent	GRI-GLYCalc™	VOC	0.90	3.94
		GRI-GLYCalc™	Benzene	0.0079	0.034
		GRI-GLYCalc™	Ethylbenzene	0.00	0.00
		GRI-GLYCalc™	Toluene	0.0092	0.040
		GRI-GLYCalc™	Xylenes	0.0036	0.016
		GRI-GLYCalc™	n-Hexane	0.026	0.12

1. Enter the appropriate Source Identification Numbers for the glycol dehydration unit Reboiler Vent and glycol Regenerator Still Vent. The glycol dehydration unit Reboiler Vent and glycol Regenerator Still Vent should be designated RBV-1 and RSV-1, respectively. If the compressor station incorporates multiple glycol dehydration units, a *Glycol Dehydration Unit Data Sheet* shall be completed for each, using Source Identification #s RBV-2 and RSV-2, RBV-3 and RSV-3, etc.

2. Enter the Source Status using the following codes:

NS Construction of New Source
MS Modification of Existing Source

ES Existing Source
RS Removal of Source

3. Enter the date (or anticipated date) of the glycol dehydration unit's installation (construction of source), modification or removal.
4. Enter the Air Pollution Control Device (APCD) type designation using the following codes:

NA	None	CD	Condenser
FL	Flare	CC	Condenser/Combustion Combination
TO	Thermal Oxidizer		
5. Enter the Potential Emissions Data Reference designation using the following codes:

MD	Manufacturer's Data	AP	AP-42	
GR	GRI-GLYCalc™	OT	Other _____	(please list)
6. Enter the Reboiler Vent and glycol Regenerator Still Vent Potential to Emit (PTE) for the listed regulated pollutants in lbs per hour and tons per year. The glycol Regenerator Still Vent potential emissions may be determined using the most recent version of the thermodynamic software model GRI-GLYCalc™ (Radian International LLC & Gas Research Institute). Attach all referenced Potential Emissions Data (or calculations) and the GRI-GLYCalc *Aggregate Calculations Report* to this *Glycol Dehydration Unit Data Sheet(s)*. This PTE data shall be incorporated in the *Emissions Summary Sheet*.

Include a copy of the GRI-GLYCalc™ analysis. This includes a printout of the aggregate calculations report, which shall include emissions reports, equipment reports, and stream reports.

***An explanation of input parameters and examples, when using GRI-GLYCalc™ is available on our website.**

Bulk Loading and Fugitives

Attachment L
EMISSIONS UNIT DATA SHEET
CHEMICAL PROCESS

For chemical processes please fill out this sheet and all supplementary forms (see below) that apply. Please check all supplementary forms that have been completed.

- Emergency Vent Summary Sheet*
- Leak Sources Data Sheet*
- Toxicology Data Sheet*
- Reactor Data Sheet*
- Distillation Column Data Sheet*

1. Chemical process area name and equipment ID number (as shown in *Equipment List Form*)
Piping for Entire Facility. Piping not contained in equipment form.

2. Standard Industrial Classification Codes (SICs) for process(es)
4923

3. List raw materials and attach MSDSs
Wet Natural Gas

4. List Products and Maximum Production and attach MSDSs

Description and CAS Number	Maximum Hourly (lb/hr)	Maximum Annual (ton/year)
Dry Natural Gas	6.04 MMscf/hour	52,925 MMscf/year
Condensate	6.25 barrels/hour	54,750 barrels/year
Produced Water	1.88 barrels/hour	16,425 barrels/year

5. Complete the *Emergency Vent Summary Sheet* for all emergency relief devices.

6. Complete the *Leak Source Data Sheet* and describe below or attach to application the leak detection or maintenance program to minimize fugitive emissions. Include detection instruments, calibration gases or methods, planned inspection frequency, and record-keeping, and similar pertinent information. If subject to a rule requirement (e.g. 40CFR60, Subpart VV), please list those here.

Leak Detection Plan in place. Not subject to any federal regulations

7. Clearly describe below or attach to application Accident Procedures to be followed in the event of an accidental spill or release.

Will reference developed and approved Spill Prevention, Control and Countermeasure (SPCC) plan.

8A. Complete the *Toxicology Data Sheet* or attach to application a toxicology report (an up-to-date material safety data sheets (MSDS) may be used) outlining the currently known acute and chronic health effects of each compound or chemical entity emitted to the air. If these compounds have already been listed in Item 3, then a duplicate MSDS sheet is not required. Include data such as the OSHA time weighted average (TWA) or mutagenicity, teratogenicity, irritation, and other known or suspected effects should be addressed. Indicate where these are unknown, and provide references.

8B. Describe any health effects testing or epidemiological studies on these compounds that are being or may be conducted by the company or required under TSCA, RCRA or other federal regulations. Discuss the persistence in the environment of any emission (e.g. pesticides, etc.).

9. **Waste Products** - Waste products status: (If source is subject to RCRA or 45CSR25, please contact the Hazardous Waste Section of WVDEP, OAQ at (304) 926-3647.)

9A. Types and amounts of wastes to be disposed:

9B. Method of disposal and location of waste disposal facilities:

Carrier:

Phone:

9C. Check here if approved USEPA/State Hazardous Waste Landfill will be used

10. Maximum and Projected Typical Operating Schedule for process or project as a whole (circle appropriate units).

circle units:	(hrs/day) (hr/batch)	(days), (batches/day), (batches/week)	(days/yr), (weeks/year)
10A. Maximum	24	7	52
10B. Typical	24	7	52

11. Complete a *Reactor Data Sheet* for each reactor in this chemical process.

12. Complete a *Distillation Column Data Sheet* for each distillation column in this chemical process.

13. Proposed Monitoring, Recordkeeping, Reporting, and Testing

Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

MONITORING

RECORDKEEPING

See Attachment O

See Attachment O

REPORTING

TESTING

See Attachment O

See Attachment O

MONITORING. Please list and describe the process parameters and ranges that are proposed to be monitored in order to demonstrate compliance with the operation of this process equipment operation or air pollution control device.

RECORDKEEPING. Please describe the proposed recordkeeping that will accompany the monitoring.

REPORTING. Please describe the proposed frequency of reporting of the recordkeeping.

TESTING. Please describe any proposed emissions testing for this process equipment or air pollution control device.

14. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty

LEAK SOURCE DATA SHEET

Source Category	Pollutant	Number of Source Components ¹	Number of Components Monitored by Frequency ²	Average Time to Repair (days) ³	Estimated Annual Emission Rate (lb/yr) ⁴
Pumps ⁵	light liquid VOC ^{6,7}				
	heavy liquid VOC ⁸				
	Non-VOC ⁹				
Valves ¹⁰	Gas VOC	773	TBD	1	13,514 – EE
	Light Liquid VOC				
	Heavy Liquid VOC				
	Non-VOC				
Safety Relief Valves ¹¹	Gas VOC				
	Non VOC				
Open-ended Lines ¹²	VOC				
	Non-VOC				
Sampling Connections ¹³	VOC				
	Non-VOC				
Compressors	VOC	39	TBD	1	1,333– EE
	Non-VOC				
Flanges	VOC	548	TBD	1	830 – EE
	Non-VOC				
Other	VOC				
	Non-VOC				

^{1 - 13} See notes on the following page.

Attachment L
EMISSIONS UNIT DATA SHEET
GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on *Equipment List Form*): Fugitive so no number assigned

<p>1. Name or type and model of proposed affected source:</p> <p>Fugitive emissions from venting episodes such as plant shutdowns and compressor start ups/shut downs.</p>
<p>2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.</p>
<p>3. Name(s) and maximum amount of proposed process material(s) charged per hour:</p>
<p>4. Name(s) and maximum amount of proposed material(s) produced per hour:</p> <ul style="list-style-type: none">- compressor blowdown - 0.055 tons VOC per event, 3.96 tons CO₂e per event- compressor startup - 0.006 tons VOC per event, 0.42 tons CO₂e per event- plant shutdown - 0.55 tons VOC per event, 39.64 tons CO₂e per event-pigging venting - 0.005 tons VOC per event, 0.40 tons CO₂e per event
<p>5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:</p> <p>none</p>

* The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

6. Combustion Data (if applicable):					
(a) Type and amount in appropriate units of fuel(s) to be burned:					
(b) Chemical analysis of proposed fuel(s), excluding coal, including maximum percent sulfur and ash:					
(c) Theoretical combustion air requirement (ACF/unit of fuel):					
@		°F and		psia.	
(d) Percent excess air:					
(e) Type and BTU/hr of burners and all other firing equipment planned to be used:					
(f) If coal is proposed as a source of fuel, identify supplier and seams and give sizing of the coal as it will be fired:					
(g) Proposed maximum design heat input:					$\times 10^6$ BTU/hr.
7. Projected operating schedule:					
Hours/Day	not a regular schedule	Days/Week	not a regular schedule	Weeks/Year	not a regular schedule

8. Projected amount of pollutants that would be emitted from this affected source if no control devices were used:

		@	venting events are uncontrolled	°F and	psia
a.	NO _x			lb/hr	grains/ACF
b.	SO ₂			lb/hr	grains/ACF
c.	CO			lb/hr	grains/ACF
d.	PM ₁₀			lb/hr	grains/ACF
e.	Hydrocarbons			lb/hr	grains/ACF
f.	VOCs			lb/hr	grains/ACF
g.	Pb			lb/hr	grains/ACF
h.	Specify other(s)			lb/hr	grains/ACF
				lb/hr	grains/ACF
				lb/hr	grains/ACF
				lb/hr	grains/ACF
				lb/hr	grains/ACF

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

(2) Complete the Emission Points Data Sheet.

9. Proposed Monitoring, Recordkeeping, Reporting, and Testing
Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

MONITORING
See Attachment O

RECORDKEEPING
See Attachment O

REPORTING
See Attachment O

TESTING
See Attachment O

MONITORING. PLEASE LIST AND DESCRIBE THE PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OPERATION OF THIS PROCESS EQUIPMENT OPERATION/AIR POLLUTION CONTROL DEVICE.

RECORDKEEPING. PLEASE DESCRIBE THE PROPOSED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.

REPORTING. PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORDKEEPING.

TESTING. PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR POLLUTION CONTROL DEVICE.

10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty
N/A

Attachment M.
Air Pollution Control Device Sheets

NSCR Catalysts

Attachment M
Air Pollution Control Device Sheet
(OTHER COLLECTORS)

Control Device ID No. (must match Emission Units Table): 1C-11C, 15C, 16C

Equipment Information

1. Manufacturer: EMIT Technologies Model No. R-3615-T	2. Control Device Name: 1C-11C, 15C, 16C – Catalyst for C-100-C-1300 Type: NSCR Catalyst
3. Provide diagram(s) of unit describing capture system with duct arrangement and size of duct, air volume, capacity, horsepower of movers. If applicable, state hood face velocity and hood collection efficiency.	
4. On a separate sheet(s) supply all data and calculations used in selecting or designing this collection device.	
5. Provide a scale diagram of the control device showing internal construction.	
6. Submit a schematic and diagram with dimensions and flow rates.	
7. Guaranteed minimum collection efficiency for each pollutant collected: N/A – no capture of pollutants	
8. Attached efficiency curve and/or other efficiency information.	
9. Design inlet volume: 8,858 ACFM	10. Capacity:
11. Indicate the liquid flow rate and describe equipment provided to measure pressure drop and flow rate, if any. N/A	
12. Attach any additional data including auxiliary equipment and operation details to thoroughly evaluate the control equipment.	
13. Description of method of handling the collected material(s) for reuse or disposal. Replace Catalyst elements when necessary	

Gas Stream Characteristics

14. Are halogenated organics present?	<input type="checkbox"/> Yes	<input checked="" type="checkbox"/> No	
Are particulates present?	<input checked="" type="checkbox"/> Yes	<input type="checkbox"/> No	
Are metals present?	<input type="checkbox"/> Yes	<input checked="" type="checkbox"/> No	
15. Inlet Emission stream parameters:	Maximum	Typical	
Pressure (mmHg):	Not specified		
Heat Content (BTU/scf):	1,400	1,149	
Oxygen Content (%):	Not specified		
Moisture Content (%):	Not specified		
Relative Humidity (%):	Not specified		

27. Describe any air pollution control device inlet and outlet gas conditioning processes (e.g., gas cooling, gas reheating, gas humidification): None

28. Describe the collection material disposal system: Catalyst elements can be cleaned and/or replaced; materials are not disposed on site.

29. Have you included **Other Collectores Control Device** in the Emissions Points Data Summary Sheet? yes

30. **Proposed Monitoring, Recordkeeping, Reporting, and Testing**
Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

MONITORING: **See Attachment O**

RECORDKEEPING: **See Attachment O**

REPORTING: **See Attachment O**

TESTING: **See Attachment O**

MONITORING: Please list and describe the process parameters and ranges that are proposed to be monitored in order to demonstrate compliance with the operation of this process equipment or air control device.
RECORDKEEPING: Please describe the proposed recordkeeping that will accompany the monitoring.
REPORTING: Please describe any proposed emissions testing for this process equipment on air pollution control device.
TESTING: Please describe any proposed emissions testing for this process equipment on air pollution control device.

31. Manufacturer's Guaranteed Control Efficiency for each air pollutant.
NOx: 97.5%, CO: 97.5%, VOC: 84%, HCHO: 90%, CH4: 70%
Due to variable load conditions, the catalyst efficiency may vary. The catalyst efficiencies listed above are typical based on expected operating conditions.

32. Manufacturer's Guaranteed Control Efficiency for each air pollutant.

33. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty. Inlet temperature range is 750 F – 1250 F. Engine must be operated between 50 – 100 % load. A/F ratio controller must be set properly with fuel heating value of around 1400 Btu/scf. Engine lube oil shall contain less than 0.5 wt% sulfated ash. Catalyst must not be exposed to the following: antimony, arsenic, chromium, copper, iron, lead, lithium, magnesium, mercury, nickel, phosphorous, potassium, silicon, sodium, sulfur, tin, zinc.



2585 Heartland Dr.
Sheridan, WY 82801
Office: | Direct: +1 (307) 675.5081
riames@emittechnologies.com

Prepared For:
Clayton Brown
ANTERO RESOURCES

QUOTE: QUO-17302-L3Z6

INFORMATION PROVIDED BY WAUKESHA

Engine: L7044GSI
Horsepower: 1680
RPM: 1200
Compression Ratio: 8.0
Exhaust Flow Rate: 8820 CFM
Exhaust Temperature: 1226 °F
Reference: N/A
Fuel: Natural Gas
Annual Operating Hours: 8760

Uncontrolled Emissions

	<u>g/bhp-hr</u>	<u>Lb/Hr</u>	<u>Tons/Year</u>
NOx:	13.50	50.00	219.00
CO:	12.50	46.30	202.78
THC:	2.30	8.52	37.31
NMHC	0.90	3.33	14.60
NMNEHC:	0.48	1.78	7.79
HCHO:	0.05	0.19	0.81
O2:	0.30 %		

POST CATALYST EMISSIONS

	<u>% Reduction</u>
NOx:	>97.5%
CO:	>97.5%
VOC:	>84.0%
HCHO:	>90.0%
CH4:	>70.0%

CONTROL EQUIPMENT

Catalyst Element

Model: RT-3615-T
Catalyst Type: NSCR, Standard Precious Group Metals
Substrate Type: BRAZED
Manufacturer: EMIT Technologies, Inc
Element Quantity: 6
Element Size: Rectangle 36" x 15" x 3.5"



2585 Heartland Dr.
Sheridan, WY 82801
Office: | Direct: +1 (307) 675.5081
riames@emittechnologies.com

WARRANTY

EMIT Technologies, Inc. warrants that the goods supplied will be free from defects in workmanship by EMIT Technologies, Inc. for a period of two (2) years from date of shipment. EMIT Technologies, Inc. will not be responsible for any defects which result from improper use, neglect, failure to properly maintain or which are attributable to defects, errors or omissions in any drawings, specifications, plans or descriptions, whether written or oral, supplied to EMIT Technologies, Inc. by Buyer.

Catalyst performance using an EMIT Air/Fuel ratio controller is dependent upon properly defined set-points, variable with engine and fuel gas composition. Air/fuel ratio controller performance is guaranteed, but not limited, to fuel gas with a HHV content of 1400 BTU/SCF.

Catalyst performance will be guaranteed for a period of 1 year from installation, or 8760 operating hours, whichever comes first. The catalyst shall be operated with an automatic air/fuel ratio controller. The performance guarantee shall not cover the effects of excessive ash masking due to operation at low load, improper engine maintenance, or inappropriate lubrication oil. The performance guarantee shall not cover the effects of continuous engine misfires (cylinder or ignition) exposing the catalyst to excessive exothermic reaction temperatures. In most cases, excluding thermal deactivation, catalyst performance is redeemable by means of proper washing (refer to EMIT Catalyst/Silencer Housing Manual for element wash information, or contact a local EMIT Sales representative).

The exhaust temperature operating range at the converter inlet is a minimum of 600°F for oxidation catalyst and 750 °F for NSCR catalyst, and a maximum of 1250°F.

If a properly functioning, high temperature shut down switch is not installed, thermal deactivation of catalyst at sustained temperatures above 1250 °F is not covered. If excessive exposure to over oxygenation of NSCR catalyst occurs due to improperly functioning or non-existent Air/Fuel ratio control, then deactivation of catalyst is not warranted.

The catalyst conversion efficiencies (% reduction) will be guaranteed for engine loads of 50 to 100 percent. Standard Oxidation Catalyst conversion efficiencies (% reduction) will be guaranteed for fuel gas containing less than 1.5% mole fraction of non-methane, non-ethane hydrocarbons. Applications where fuel gas exceeds this level will require a Premium Oxidation Catalyst to maintain guaranteed VOC conversion efficiencies.

Engine lubrication oil shall contain less than 0.5 wt% Sulfated Ash with a maximum allowable specific oil consumption of 0.7 g/bhp-hr. The catalyst shall be limited to a maximum ash loading of 0.022 lb/ft³. Phosphorous and zinc additives are limited to 0.03 wt%. New or Reconstructed engines must operate for a minimum of 50 hours prior to catalyst installation, otherwise the warranty is void.

The catalyst must not be exposed to the following know poisoning agents, including: antimony, arsenic, chromium, copper, iron, lead, lithium, magnesium, mercury, nickel, phosphorous, potassium, silicon, sodium, sulfur, tin, and zinc. Total poison concentrations in the fuel gas must be limited to 0.25 ppm or less for catalyst to function properly.

Shipment - Promised shipping dates are approximate lead times from the point of manufacture and are not guaranteed. EMIT Technologies, Inc. will not be liable for any loss, damage or delay in manufacture or delivery resulting from any cause beyond its control including, but not limited to a period equal to the time lost by reason of that delay. All products will be crated as per best practice to prevent any damage during shipment. Unless otherwise specified, Buyer will pay for any special packing and shipping requirements. Acceptance of goods by common carrier constitutes delivery to Buyer. EMIT Technologies, Inc. shall not be responsible for goods damaged or lost in transit.

Terms: Credit is extended to purchaser for net 30 time period. If payment is not received in the net 30 timeframe, interest on the unpaid balance will accrue at a rate of 1.5% per month from the invoice date.

Order Cancellation Terms: Upon cancellation of an order once a Purchase Order has occurred, the customer will pay a 25% restocking fee for Catalyst Housings, Catalyst Elements, and Air/Fuel Ratio Controllers; 50% restocking fee for Cooler Top Solutions Exhaust System Accessories, and other Custom Built Products; 100% of all associated shipping costs incurred by EMIT; 100% of all project expenses incurred by EMIT for Field Services.

**Attachment N.
Supporting Emissions Calculations**

Emission Calculations

EMISSIONS SUMMARY TOTAL

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Facility Location:	Tyler County, West Virginia

UNCONTROLLED POTENTIAL EMISSION SUMMARY

Source	NOx		CO		VOC		SO ₂		PM-10		HAPs		Formaldehyde		CO ₂ e tpy
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	
<u>Engines</u>															
Compressor Engine 1	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 2	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 3	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 4	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 5	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 6	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 7	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 8	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 9	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 10	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 11	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 12	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
Compressor Engine 13	50.74	222.24	47.04	206.02	1.70	7.46	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,109
<u>Turbines</u>															
Microturbine Generators	0.24	1.11	0.66	3.06	0.060	0.28	0.021	0.10	0.041	0.19	0.0063	0.029	0.0044	0.020	3,698
Catalytic Heater for Generator Fuel	0.0029	0.013	0.0025	0.011	0.00016	0.00071	0.000018	0.000077	0.00022	0.0010	0.000055	0.00024	0.0000022	0.000010	12
<u>Dehydrator</u>															
TEG Dehydrator 1	---	---	---	---	60.75	266.07	---	---	---	---	8.75	38.32	---	---	9,832
TEG Dehydrator 2	---	---	---	---	60.75	266.07	---	---	---	---	8.75	38.32	---	---	9,832
Reboiler 1	0.18	0.81	0.15	0.68	0.010	0.044	0.0011	0.0048	0.014	0.061	0.0035	0.015	0.00014	0.00060	771
Reboiler 2	0.18	0.81	0.15	0.68	0.010	0.044	0.0011	0.0048	0.014	0.061	0.0035	0.015	0.00014	0.00060	771
<u>Combustors</u>															
Flare and Pilot	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---
<u>Hydrocarbon Loading</u>															
Truck Loadout	---	---	---	---	77.14	8.11	---	---	---	---	1.10	0.12	---	---	57.91
<u>Fugitive Emissions</u>															
Component Leak Emissions	---	---	---	---	1.79	7.84	---	---	---	---	0.0045	0.020	---	---	140
Venting Emissions	---	---	---	---	---	10.73	---	---	---	---	---	0.027	---	---	773
Fugitive Dust Emissions	---	---	---	---	---	---	---	---	0.051	0.22	---	---	---	---	---
<u>Storage Tanks</u>															
Produced Water Tanks	---	---	---	---	0.15	0.68	---	---	---	---	0.0022	0.010	---	---	4.85
Settler Tank	---	---	---	---	72.24	316.39	---	---	---	---	1.03	4.52	---	---	2,260
Condensate Tanks	---	---	---	---	2.41	10.58	---	---	---	---	0.034	0.15	---	---	76
Total Facility PTE =	660.24	2,891.91	612.45	2,682.71	297.46	983.84	0.13	0.57	3.63	15.90	24.23	101.56	2.41	10.57	146,645

EMISSIONS SUMMARY TOTAL

Company:	Antero Midstream LLC	
Facility Name:	Monroe Compressor Station	
Facility Location:	Tyler County, West Virginia	

CONTROLLED POTENTIAL EMISSION SUMMARY

Source	NOx		CO		VOC		SO ₂		PM-10		HAPs		Formaldehyde		CO ₂ e tpy
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	
<u>Engines</u>															
Compressor Engine 1	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 2	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 3	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 4	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 5	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 6	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 7	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 8	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 9	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 10	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 11	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 12	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
Compressor Engine 13	1.27	5.56	1.18	5.15	0.27	1.19	0.0082	0.036	0.27	1.18	0.18	0.81	0.019	0.081	8,731
<u>Turbines</u>															
Microturbine Generators	0.24	1.11	0.66	3.06	0.060	0.28	0.021	0.10	0.041	0.19	0.0063	0.029	0.0044	0.020	3,698
Catalytic Heater for Generator Fuel	0.0029	0.013	0.0025	0.011	0.00016	0.00071	0.000018	0.000077	0.00022	0.0010	0.000055	0.00024	0.0000022	0.000010	12
<u>Dehydrator</u>															
TEG Dehydrator 1	---	---	---	---	1.21	5.32	---	---	---	---	0.17	0.76	---	---	214
TEG Dehydrator 2	---	---	---	---	1.21	5.32	---	---	---	---	0.17	0.76	---	---	214
Reboiler 1	0.18	0.81	0.15	0.68	0.010	0.044	0.0011	0.0048	0.014	0.061	0.0035	0.015	0.00014	0.00060	771
Reboiler 2	0.18	0.81	0.15	0.68	0.010	0.044	0.0011	0.0048	0.014	0.061	0.0035	0.015	0.00014	0.00060	771
<u>Combustion</u>															
Flare and Pilot	0.33	1.44	1.78	7.79	0.00010	0.00045	0.000011	0.000049	0.00014	0.00062	0.000035	0.00015	---	---	2,465
<u>Hydrocarbon Loading</u>															
Truck Loadout	---	---	---	---	77.14	8.11	---	---	---	---	0.022	0.0023	---	---	1.16
<u>Fugitive Emissions</u>															
Component Leak Emissions	---	---	---	---	1.79	7.84	---	---	---	---	0.0045	0.020	---	---	140
Venting Emissions	---	---	---	---	---	10.73	---	---	---	---	---	0.027	---	---	773
Fugitive Dust Emissions	---	---	---	---	---	---	---	---	0.051	0.22	---	---	---	---	---
<u>Storage Tanks</u>															
Produced Water Tanks	---	---	---	---	0.0031	0.014	---	---	---	---	0.000044	0.00019	---	---	0.10
Settler Tank	---	---	---	---	1.44	6.33	---	---	---	---	0.021	0.090	---	---	45.20
Condensate Tanks	---	---	---	---	0.048	0.21	---	---	---	---	0.00069	0.0030	---	---	1.51
Total Facility PTE =	17.43	76.40	18.04	79.16	86.48	59.75	0.13	0.57	3.63	15.90	2.75	12.26	0.25	1.08	122,615

Compressor Engine Emission Calculations

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Compressor Engines

Source Information-Per Engine

Emission Unit ID:	C-100 - C-1300	
Engine Make/Model	Waukesha 7044 GSI	
Service	Compression	
Controls - Y or N / Type	Y	NSCR/AFRC
Site Horsepower Rating ¹	1,680	hp
Fuel Consumption (BSFC) ¹	8,272	Btu/(hp-hr)
Heat Rating ²	13.90	MMBtu/hr
Fuel Consumption ^{2,3}	106.17	MMscf/yr
Fuel Consumption ¹	12,120	scf/hr
Fuel Heating Value	1,149	Btu/scf
Operating Hours	8,760	hrs/yr

Notes:

1. Values from Waukesha specification sheet
2. Calculated values
3. Annual fuel consumption is 100% of maximum fuel consumption at 100% load.

Potential Emissions per Engine

Pollutant	Uncontrolled					Controlled					Source of Emissions Factors
	Emission Factor (lb/MMBtu)	(g/bhp-hr)	Estimated Emissions ²			Emission Factor (lb/MMBtu)	(g/bhp-hr)	Estimated Emissions ²			
			(lb/hr)	(lb/yr)	(tpy)			(lb/hr)	(lb/yr)	(tpy)	
NOx ^{1,4}	---	13.7	50.74	---	222.24	---	0.34	1.27	---	5.56	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled
CO ^{1,4}	---	12.7	47.04	---	206.02	---	0.32	1.18	---	5.15	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled
VOC ^{1,4}	---	0.46	1.70	---	7.46	---	0.074	0.27	---	1.19	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled
SO ₂	5.88E-04	---	0.0082	---	0.036	5.88E-04	---	0.0082	---	0.03579	AP-42, Chapter 3.2, Table 3.2-3
PM _{2.5} /PM ₁₀	1.94E-02	---	0.27	---	1.18	1.94E-02	---	0.27	---	1.18	AP-42, Chapter 3.2, Table 3.2-3
Total PM	1.94E-02	---	0.27	---	1.18	1.94E-02	---	0.27	---	1.18	AP-42, Chapter 3.2, Table 3.2-3
1,1,2,2-Tetrachloroethane	2.53E-05	---	0.00035	3.08	0.0015	2.53E-05	---	0.00035	3.08	0.0015	AP-42, Chapter 3.2, Table 3.2-3
1,3-Butadiene	6.63E-04	---	0.0092	80.71	0.040	6.63E-04	---	0.0092	80.71	0.040	AP-42, Chapter 3.2, Table 3.2-3
Acetaldehyde	2.79E-03	---	0.039	339.65	0.17	2.79E-03	---	0.039	339.65	0.17	AP-42, Chapter 3.2, Table 3.2-3
Acrolein	2.63E-03	---	0.037	320.17	0.16	2.63E-03	---	0.037	320.17	0.16	AP-42, Chapter 3.2, Table 3.2-3
Benzene	1.58E-03	---	0.022	192.35	0.10	1.58E-03	---	0.022	192.35	0.10	AP-42, Chapter 3.2, Table 3.2-3
Ethylbenzene	2.48E-05	---	0.00034	3.02	0.0015	2.48E-05	---	0.00034	3.02	0.0015	AP-42, Chapter 3.2, Table 3.2-3
Formaldehyde ^{1,4}	---	0.05	0.19	1,622	0.81	---	0.005	0.019	162.22	0.081	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled
Methanol	3.06E-03	---	0.043	372.52	0.19	3.06E-03	---	0.043	372.52	0.19	AP-42, Chapter 3.2, Table 3.2-3
Methylene Chloride	4.12E-05	---	0.00057	5.02	0.0025	4.12E-05	---	0.00057	5.02	0.0025	AP-42, Chapter 3.2, Table 3.2-3
PAH	1.41E-04	---	0.0020	17.16	0.0086	1.41E-04	---	0.0020	17.16	0.0086	AP-42, Chapter 3.2, Table 3.2-3
Toluene	5.58E-04	---	0.0078	67.93	0.034	5.58E-04	---	0.0078	67.93	0.034	AP-42, Chapter 3.2, Table 3.2-3
Xylenes	1.95E-04	---	0.0027	23.74	0.012	1.95E-04	---	0.0027	23.74	0.012	AP-42, Chapter 3.2, Table 3.2-3
Other HAPs ²	2.10E-04	---	0.0029	25.54	0.013	2.10E-04	---	0.0029	25.54	0.013	AP-42, Chapter 3.2, Table 3.2-3
Total HAPs			0.35	3,073	1.54			0.18	1,613	0.81	
Pollutant	Emission Factor (kg/MMBtu)	(g/bhp-hr)	Estimated Emissions ²			Emission Factor (kg/MMBtu)	(g/bhp-hr)	Estimated Emissions ²			Source of Emissions Factors
			(lb/hr)	(lb/yr)	(tpy)			(lb/hr)	(lb/yr)	(tpy)	
CO ₂ ¹	---	528	1,956	---	8,566	---	528	1,956	---	8,566	Manufacturer's Specs
CH ₄ ^{1,4}	---	1.33	4.93	---	22	---	0.40	1.48	---	6.5	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled
N ₂ O	0.0001	---	0.003	---	0.013	0.0001	---	0.003	---	0.013	40 CFR Part 98, Subpart C, Table C-2
CO ₂ e ²	---	---	2,080	---	9,109	---	---	1,993	---	8,731	40 CFR Part 98, Subpart A, Table A-1, effective January 2014

Notes:

4. Due to variable load conditions, the catalyst efficiency may vary. The catalyst efficiencies used in the emissions are typical based on expected operating conditions. The catalyst specification sheet shows typical destruction efficiencies that were used in the calculations. The emission factors shown on the catalyst specification sheet are not site specific, so those will vary; however the efficiencies will be the same.

Example Calculations

lb/hr = (g/bhp-hr) * (hp) * (1 lb/453.6 g) or (lb/MMBtu) * (MMBtu/hr)

tpy = (MMscf/yr) * (Btu/scf) * (10⁶ Btu/MMBtu) * (g/bhp-hr) / (Btu/bhp-hr) * (1 lb/453.59 g) * (1 ton/2000 lb) or (MMscf/yr) * (Btu/scf) * (lb/MMBtu) * (1 ton/2000 lb)

Microturbine Generator Emission Calculations

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Microturbine Generators

Source Information

Emission Unit ID:	GEN1 - GEN2	
Make/Model	Capstone C600 Standard	
Microturbine Rating	600	kWe
Net Heat Rate	10,300	Btu/kWhe
Heat Input ¹	6.18	MMBtu/hr
Operating Hours ⁴	9,260	hrs/yr

Notes:

- 1) Calculated
- 2) The C600 is sold as three (3) C200 units in operation together. Thus emission factors for the C600 are the same as the C200 (just three times the kWe). There will be two C600 units (six C200 units on location).
- 3) No more than 600 kWe will be operational at one time, except when C200 units are being switched. All units are wired together and operation between individual C200 units will rotate based on functionality of units (e.g., during repairs).
- 4) Annual operation for 600 kW will be for a maximum of 8,760 hours. It is expected that no more than 500 hours of back up power will be utilized during repairs or during unit switches. Each C200 has an hour meter, so it will be known how much each C200 unit is operating and will be used interchangeably.

Potential Emissions

Pollutant	Uncontrolled					Controlled					Source of Emissions Factors
	Emission Factor		Estimated Emissions ¹			Emission Factor		Estimated Emissions ¹			
	(lb/MMBtu)	(lb/MWhe)	(lb/hr)	(lb/yr)	(tpy)	(lb/MMBtu)	(lb/MWhe)	(lb/hr)	(lb/yr)	(tpy)	
NOx	---	0.40	0.24	---	1.11	---	0.40	0.24	---	1.11	Manufacturer Specifications
CO	---	1.10	0.66	---	3.06	---	1.10	0.66	---	3.06	Manufacturer Specifications
VOC	---	0.10	0.060	---	0.28	---	0.10	0.060	---	0.28	Manufacturer Specifications
SO ₂	3.40E-03	---	0.021	---	0.10	3.40E-03	---	0.021	---	0.10	AP-42, Chapter 3.1, Table 3.1-2a
PM _{2.5} /PM ₁₀	6.60E-03	---	0.041	---	0.19	6.60E-03	---	0.041	---	0.19	AP-42, Chapter 3.1, Table 3.1-2a
1,3-Butadiene	4.30E-07	---	2.66E-06	0.02	0.00001	4.30E-07	---	2.66E-06	0.025	0.00001	AP-42, Chapter 3.1, Table 3.1-3
Acetaldehyde	4.00E-05	---	2.47E-04	2.29	0.001	4.00E-05	---	2.47E-04	2.29	0.001	AP-42, Chapter 3.1, Table 3.1-3
Acrolein	6.40E-06	---	3.96E-05	0.37	0.0002	6.40E-06	---	3.96E-05	0.37	0.0002	AP-42, Chapter 3.1, Table 3.1-3
Benzene	1.20E-05	---	7.42E-05	0.69	0.0003	1.20E-05	---	7.42E-05	0.69	0.0003	AP-42, Chapter 3.1, Table 3.1-3
Ethylbenzene	3.20E-05	---	1.98E-04	1.83	0.0009	3.20E-05	---	1.98E-04	1.83	0.0009	AP-42, Chapter 3.1, Table 3.1-3
Formaldehyde	7.10E-04	---	4.39E-03	40.63	0.02	7.10E-04	---	4.39E-03	40.63	0.02	AP-42, Chapter 3.1, Table 3.1-3
Naphthalene	1.30E-06	---	8.03E-06	0.07	0.00004	1.30E-06	---	8.03E-06	0.074	0.00004	AP-42, Chapter 3.1, Table 3.1-3
PAH	2.20E-06	---	1.36E-05	0.13	0.00006	2.20E-06	---	1.36E-05	0.13	0.00006	AP-42, Chapter 3.1, Table 3.1-3
Propylene Oxide	2.90E-05	---	1.79E-04	1.66	0.0008	2.90E-05	---	1.79E-04	1.66	0.0008	AP-42, Chapter 3.1, Table 3.1-3
Toluene	1.30E-04	---	8.03E-04	7.44	0.004	1.30E-04	---	8.03E-04	7.44	0.004	AP-42, Chapter 3.1, Table 3.1-3
Xylenes	6.40E-05	---	3.96E-04	3.66	0.002	6.40E-05	---	3.96E-04	3.66	0.002	AP-42, Chapter 3.1, Table 3.1-3
Total HAPS			0.006	58.79	0.03			0.006	58.79	0.03	
Pollutant	Emission Factor		Estimated Emissions ¹			Emission Factor		Estimated Emissions ¹			Source of Emissions Factors
	(kg/MMBtu)	(lb/MWhe)	(lb/hr)		(tpy)	(kg/MMBtu)	(lb/MWhe)	(lb/hr)		(tpy)	
CO ₂	---	1,330	798	---	3,695	---	1,330	798	---	3,695	Manufacturer Specifications
CH ₄	0.001	---	0.01	---	0.06	0.001	---	0.01	---	0.06	40 CFR Part 98, Subpart C, Table C-2
N ₂ O	0.0001	---	0.001	---	0.006	0.0001	---	0.001	---	0.006	40 CFR Part 98, Subpart C, Table C-2
CO ₂ e	---	---	799	---	3,698	---	---	799	---	3,698	40 CFR Part 98, Subpart A, Table A-1, effective January 2014

Example Calculations

lb/hr = (lb/Mwhe) * kWe * (1 MWe/1000 kWe) or (lb/MMBtu) * (MMBtu/hr) or (kg/MMBtu) * (MMBtu/hr) * (2.21 lb/kg)

tpy = (lb/hr) * (hr/yr) * (ton/2000 lb)

Natural Gas Fueled Catalytic Heater Emissions

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Location:	Tyler County, West Virginia
Source Description:	Catalytic Heater for Generator Fuel

Source Information

Emission Unit ID:	CATHT1	
Source Description:	Generator Fuel Heater	
Hours of Operation	8,760	hr/yr
Design Heat Rate	0.024	MMBtu/hr
Heater Efficiency	80%	
Fuel Heat Value	1,020	Btu/scf
Fuel Use	0.26	MMscf/yr

Emission Calculations per Heater

Pollutant	Emission Factor (lb/MMscf)	Emissions (lb/hr)	Emissions (tpy)	Emission Factor Source
NO _x	100	0.0029	0.013	AP-42 Ch. 1.4 Table 1.4-1
CO	84	0.0025	0.011	AP-42 Ch. 1.4 Table 1.4-1
VOC	5.5	0.00016	0.00071	AP-42 Ch. 1.4 Table 1.4-2
PM ₁₀	7.6	0.00022	0.0010	AP-42 Ch. 1.4 Table 1.4-2
SO ₂	0.6	0.000018	0.000077	AP-42 Ch. 1.4 Table 1.4-2
Formaldehyde	0.075	0.0000022	0.000010	AP-42 Ch. 1.4 Table 1.4-3
Total HAPs (including HCHO) ¹	1.9	0.000055	0.00024	AP-42 Ch. 1.4 Table 1.4-3
Pollutant	Emission Factor (kg/MMBtu)	Emissions (lb/hr)	Emissions (tpy)	Emission Factor Source
Carbon Dioxide	53.06	2.81	12	40 CFR Part 98, Subpart C, Table C-1
Methane	0.001	0.0001	0.00023	40 CFR Part 98, Subpart C, Table C-2
Nitrous Oxide	0.0001	0.00001	0.000023	40 CFR Part 98, Subpart C, Table C-2
CO ₂ e	----	2.82	12	40 CFR Part 98, Subpart A, Table A-1

1. Only those HAP pollutants above detection thresholds were included.

Sample Calculations:

$$\text{Fuel Consumption (MMscf/yr)} = \frac{\text{Heater Size (MMBtu/hr)} * \text{Hours of Operation (hrs/yr)}}{\text{Fuel Heat Value (Btu/scf)} * \text{Heater Efficiency}}$$

$$\text{Emissions (tons/yr)} = \frac{\text{Emission Factor (lbs/MMscf)} * \text{Fuel Consumption (MMscf/yr)}}{2,000 \text{ (lbs/ton)}}$$

Dehydrator Emissions

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Dehydrator Units

Potential Emissions per Dehydrator

Pollutant	Emission Unit ID: DEHY1/DEHY2 Dehydrator Still Vent		Emission Unit ID: DFLSH1/DFLSH2 Flash Tank Gas	
	(lb/hr)	(tpy)	(lb/hr)	(tpy)
Uncontrolled Emissions ¹				
VOC	15.71	68.82	45.03	197.25
Total HAPs	6.40	28.02	2.35	10.30
Benzene	1.58	6.92	0.39	1.72
Toluene	2.45	10.72	0.46	2.01
Xylenes	2.00	8.77	0.18	0.78
n-Hexane	0.37	1.61	1.32	5.79
Methane	17.86	78.24	71.77	314.34
Carbon Dioxide	0.55	2.39	3.44	15.07
CO ₂ e	447	1,958	1,798	7,874
Controlled Emissions ^{2,3}				
VOC	0.31	1.37	0.90	3.94
Total HAPs	0.13	0.56	0.047	0.21
Benzene	0.031	0.14	0.0079	0.034
Toluene	0.049	0.21	0.0092	0.040
Xylenes	0.040	0.17	0.0036	0.016
n-Hexane	0.0074	0.032	0.026	0.12
Methane	0.36	1.56	1.44	6.29
Carbon Dioxide	0.55	2.39	3.44	15.07
CO ₂ e	9.5	41.5	39.3	172

Pollutant	Unit ID: DEHY + DFLSH Dehydrator Emission Totals	
	(lb/hr)	(tpy)
Uncontrolled Emissions ¹		
VOC	60.75	266.07
Total HAPs	8.75	38.32
Benzene	1.97	8.64
Toluene	2.91	12.73
Xylenes	2.18	9.55
n-Hexane	1.69	7.40
Methane	89.63	392.58
Carbon Dioxide	3.99	17.46
CO ₂ e	2,245	9,832
Controlled Emissions ^{2,3}		
VOC	1.21	5.32
Total HAPs	0.17	0.76
Benzene	0.039	0.17
Toluene	0.058	0.25
Xylenes	0.043	0.19
n-Hexane	0.034	0.15
Methane	1.79	7.85
Carbon Dioxide	3.99	17.46
CO ₂ e	48.8	213.7

¹Output from GRI-GLYCalc 4.0 for both the still vent and flash tank gas emissions

²Controlled emissions assume that the glycol still vent is equipped with a condenser and is controlled by a combustor with 98% control efficiency.

³Flash tank gas is used in the reboiler as the primary fuel source. However, in the case that gas cannot be used in the reboiler, the gas is sent to the primary/backup VRU system via the storage tanks for 98% control.

Natural Gas Fueled Dehydrator Reboiler Emissions

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Location:	Tyler County, West Virginia
Source Description:	Dehydrator Reboilers

Source Information

Emission Unit ID:	DREB1 - DREB2	
Source Description:	Dehydrator Reboiler	
Hours of Operation	8,760	hr/yr
Design Heat Rate	1.5	MMBtu/hr
Heater Efficiency	0.8	
Fuel Heat Value	1,020	Btu/scf
Fuel Use	16.1	MMscf/yr

Emission Calculations per Reboiler

Pollutant	Emission Factor (lb/MMscf)	Emissions (lb/hr)	Emissions (tpy)	Emission Factor Source
NO _x	100	0.18	0.81	AP-42 Ch. 1.4 Table 1.4-1
CO	84	0.15	0.68	AP-42 Ch. 1.4 Table 1.4-1
VOC	5.5	0.010	0.044	AP-42 Ch. 1.4 Table 1.4-2
PM ₁₀	7.6	0.014	0.061	AP-42 Ch. 1.4 Table 1.4-2
SO ₂	0.6	0.0011	0.0048	AP-42 Ch. 1.4 Table 1.4-2
Formaldehyde	0.075	0.00014	0.00060	AP-42 Ch. 1.4 Table 1.4-3
Total HAPs (including HCHO)	1.9	0.0035	0.015	AP-42 Ch. 1.4 Table 1.4-3
Pollutant	Emission Factor (kg/MMBtu)	Emissions (lb/hr)	Emissions (tpy)	Emission Factor Source
Carbon Dioxide	53.06	175.89	770	40 CFR Part 98, Subpart C, Table C-1
Methane	0.001	0.0033	0.015	40 CFR Part 98, Subpart C, Table C-2
Nitrous Oxide	0.0001	0.00033	0.0015	40 CFR Part 98, Subpart C, Table C-2
CO ₂ e	----	176.1	771	40 CFR Part 98, Subpart A, Table A-1

Sample Calculations:

$$\text{Fuel Consumption (MMscf/yr)} = \frac{\text{Heater Size (MMBtu/hr)} * \text{Hours of Operation (hrs/yr)}}{\text{Fuel Heat Value (Btu/scf)} * \text{Heater Efficiency}}$$

$$\text{Emissions (tons/yr)} = \frac{\text{Emission Factor (lbs/MMscf)} * \text{Fuel Consumption (MMscf/yr)}}{2,000 \text{ (lbs/ton)}}$$

Flare Emissions

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Flare for Dehydrator Still Vent Gas
Emission Unit ID:	FLARE1

Combusted Gas Emissions

Flare Heat Input :	4.80	MMBtu/hr
Vent Gas to Flare Rate:	4,176	scf/hr
Gas Heating Value:	1,149	Btu/scf
Hours of Operation:	8,760	hr/yr

Pollutant	Emission Factor ¹ (lb/MMBtu)	Emissions (lbs/hr)	Emissions (tons/yr)
Particulate Matter (PM/PM ₁₀ /PM _{2.5})	N/A - Smokeless Design		
Nitrogen Oxides (NO _x)	0.068	0.33	1.43
Carbon Monoxide (CO)	0.37	1.78	7.78

¹ Emission Factors from Table 13.5-1 of AP-42 Section 13.5 (Sept 1991)

Pilot Emissions

Pilot Heating Value:	1,149	Btu/scf
Hours of Operation:	8,760	hr/yr
Total Pilot Natural Gas Usage:	1.64E-05	MMscf/hr

Pollutant	Emission Factor (lb/MMscf)	Emissions (lbs/hr)	Emissions (tons/yr)
Particulate Matter (PM/PM ₁₀ /PM _{2.5}) ²	7.6	1.40E-04	6.15E-04
Nitrogen Oxides (NO _x)	100	1.85E-03	8.09E-03
Sulfur Dioxide (SO ₂) ²	0.6	1.11E-05	4.86E-05
Carbon Monoxide (CO) ²	84	1.55E-03	6.80E-03
Volatile Organic Compounds (VOC) ²	5.5	1.02E-04	4.45E-04
Total HAPs ^{2,3}	1.88	3.47E-05	1.52E-04

² Emission Factors from AP-42 Tables 1.4-1, 1.4-2, 1.4-3, and 1.4-4 (7/98).

³ Sum of Emissions Factors published for pollutants classified as "HAPS" under AP-42 Table 1.4-3.

Total Flare Emissions

Pollutant	Total Potential Emission Rate (tons/year)
Particulate Matter (PM/PM ₁₀ /PM _{2.5})	6.15E-04
Nitrogen Oxides (NO _x)	1.44
Sulfur Dioxide (SO ₂)	4.86E-05
Carbon Monoxide (CO)	7.79
Volatile Organic Compounds (VOC)	4.45E-04
Total HAPs	1.52E-04

Greenhouse Gas Emissions

Pollutant	Emission Factor (kg/MMBtu)	Emissions (lb/hr)	Emissions (tpy)	Emission Factor Source
Carbon Dioxide	53.06	562.86	2,465	40 CFR Part 98, Subpart C, Table C-1
Methane	0.001	0.01	0.05	40 CFR Part 98, Subpart C, Table C-2
Nitrogen Dioxide	0.0001	0.001	0.005	40 CFR Part 98, Subpart C, Table C-2
CO _{2e}	----	562.86	2,465	40 CFR Part 98, Subpart A, Table A-1

Storage Tank Flashing Emissions Calculated by Vasquez-Beggs Correlation

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Settling Tank
Emission Unit ID:	TK-1502

Calculation Parameters

Parameter	Settling Tank Value
Oil Gravity (API) ¹	38
Production Rate (bbl/day) ²	195
Separator Pressure (psig) ³	300
Separator Temperature (F) ⁴	120
Atmospheric Pressure (psia)	14.70
Mole wt. of Flash Gas ⁵	60.0
Gas Spec. Gravity @ separator conditions ⁵	0.9
VOC % of Flash Gas ⁵	70
Methane % of Flash Gas ⁵	20
Total HAP % of Flash Gas ⁵	1

Vasquez - Beggs Correlation Constants

Constant	API < 30	API > 30
C1	0.0362	0.0178
C2	1.0937	1.1870
C3	25.724	23.9310

Notes:

1. Anticipated API gravity based on similar compressor stations
2. Estimated production of condensate and produced water entering the settling tank. Flashing will only occur in the settling tank as the fluids will settle and stabilize in the settling tank at atmospheric pressure.
3. Most of the produced fluids will come into the settling tank at lower pressure than 300 psig; however, some equipment is at higher pressure, so 300 psig was used.
4. Typical design temperature of facility.
5. Typical/upper end bound values for the parameters.

Calculations Results

Parameter	Settling Tank Value	
	Uncontrolled	Controlled ⁶
Calculated Gas Specific gravity @ 100 psig	1.01	---
Calculated Solution Gas Ratio (scf/bbl)	78.57	---
Calculated Rate of Flash Loss (scf/day)	15322	---
Calculated THC Emissions (tons/yr)	442.09	8.84
Calculated CH₄ Emissions (tons/yr)	88.42	1.77
Calculated CO₂e Emissions (tons/yr)	2,210.5	44.21
Calculated VOC Emissions (tons/yr)	309.46	6.19
Calculated HAP Emissions (tons/yr)	4.42	0.09

Notes:

6. Tanks are controlled by a VRU with assumed 98% capture efficiency; but will likely be higher as vapors are recycled back into the system
- Gas Spec. Grav. @ 100 psig = Gas Spec. Grav. @ Sep. Cond. * [1.0+5.912E-5 * Oil Grav. * Sep. Temp. * log[(Sep. Press.+ Atmos. Press.)/114.7]]
- Gas Ratio(scf/bbl) = C1 * Gas Spec. Grav. @ 100 psig * Separator Press.^C2 * Exp[C3 * Oil Gravity/(Separator Temp. +460)]
- Flash Losses(scf/day) = Solution Gas Ratio(scf/bbl) * Oil Production Rate(bbl/day)
- THC Emissions(ton/yr) = Flash Losses(scf/day) * Mole Wt. of Flash Gas(lb/lb-mole) * 365 days/yr / [379.5 scf/lb-mol * 2000 lb/ton]
- CH₄ Emissions (tons/yr) = THC Emissions (tons/yr) * Methane % / 100
- VOC Emissions (tons/yr) = THC Emissions (tons/yr) * VOC % / 100
- HAP Emissions (tons/yr) = THC Emissions (tons/yr) * HAP % / 100

Storage Tank Working and Breathing Emissions

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Condensate, Settling, and Produced Water Tanks
Emission Unit ID:	TK-1500, TK-1501, TK-1502, TK-200, TK-201

TANK DESCRIPTION	Uncontrolled VOC Emissions ¹ (tons/yr)	Uncontrolled CH ₄ Emissions ³ (tons/yr)	Uncontrolled CO ₂ e Emissions (tons/yr)	Uncontrolled HAP Emissions ⁴ (tons/yr)
400 bbl Hydrocarbon Storage Tank (TK-200)	5.29	1.51	37.77	0.076
400 bbl Hydrocarbon Storage Tank (TK-201)	5.29	1.51	37.77	0.076
400 bbl Settling Tank (TK-1502)	6.93	1.98	49.48	0.10
400 bbl Produced Water Storage Tank ² (TK-1500)	0.34	0.097	2.42	0.0048
400 bbl Produced Water Storage Tank ² (TK-1501)	0.34	0.097	2.42	0.0048
TOTAL	18.18	5.19	129.86	0.26

TANK DESCRIPTION	Controlled VOC Emissions ⁵ (tons/yr)	Controlled CH ₄ Emissions ⁵ (tons/yr)	Controlled CO ₂ e Emissions ⁵ (tons/yr)	Controlled HAP Emissions ⁵ (tons/yr)
400 bbl Hydrocarbon Storage Tank (TK-200)	0.11	0.030	0.76	0.0015
400 bbl Hydrocarbon Storage Tank (TK-201)	0.11	0.030	0.76	0.0015
400 bbl Settling Tank (TK-1502)	0.14	0.040	0.99	0.0020
400 bbl Produced Water Storage Tank ² (TK-1500)	0.0068	0.0019	0.048	0.00010
400 bbl Produced Water Storage Tank ² (TK-1501)	0.0068	0.0019	0.048	0.00010
TOTAL	0.36	0.10	2.60	0.005

Notes:

1. Tanks 4.0.9d used to calculate standing, working, and breathing (S,W,B) emissions
2. Produced water assumed to have no more than 10% hydrocarbon liquid
3. Methane emissions estimated assuming 70% VOC and 20% CH₄ in tank vent gas
4. HAP emissions estimated assuming 1% HAPs in the tank vent gas
5. Tanks are controlled by a VRU with assumed 98% capture efficiency; but will likely be higher as vapors are recycled back into the system.

Truck Loading Emissions

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Production Liquids Truck Loadout
Emission Unit ID:	LDOUT1

AP - 42, Chapter 5.2 $L_L = 12.46 \times S \times P \times M / T$

L_L = Loading Loss Emission Factor (lbs VOC/1000 gal loaded)

S = Saturation Factor

P = True Vapor Pressure of the Loaded Liquid (psia)

M = Vapor Molecular Weight of the Loaded Liquid (lbs/lbmol)

T = Temperature of Loaded Liquid (°R)

$$\text{VOC Emissions (tpy)} = \frac{L_L (\text{lbs VOC}/1000 \text{ gal}) * 42 \text{ gal}/\text{bbl} * 365 \text{ days}/\text{year} * \text{production (bbl}/\text{day})}{1000 \text{ gal} * 2000 \text{ lbs}/\text{ton}}$$

Source	S ¹	P (psia) ²	M ³	T (°F) ⁴	T (°R)	L _L (lb/1000 gal)	Production (bbl/day)	Uncontrolled		
								VOC (tpy)	HAP ⁶ (tpy)	CO ₂ e ⁷ (tpy)
Condensate	0.6	8.2	60	60	519.67	7.05	150	8.10	0.12	57.86
Produced Water ⁵	0.6	0.37	36	60	519.67	0.19	45	0.0066	0.00009	0.047

- Notes:
1. Saturation factor from AP-42, Table 5.2-1 (Submerged loading (bottom loading): dedicated normal service)
 2. True vapor pressure is estimated from AP-42, Table 7.1-2 assuming an average daily temperature of 60 deg F and an RVP of 15.
 3. Molecular weight liquid vapor is estimated from AP-42, Table 7.1-2 assuming an RVP of 15.
 4. Temperature based on the annual average temperature for Elkins, West Virginia.
 5. Produced water assumed to have no more than 10% hydrocarbon liquid
 6. HAP emissions estimated from % HAP/%VOC from condensate vent gas
 7. CO₂e emissions estimated from % CH₄/%VOC from condensate vent gas

Assume 1 truck loaded per hour, 260 bbl truck, for short term emissions

Source	S ¹	P (psia) ²	M ³	T (°F) ⁴	T (°R)	L _L (lb/1000 gal)	Loading bbl/hr	Uncontrolled		
								VOC (lb/hr)	HAP ⁶ (lb/hr)	CO ₂ e ⁷ (lb/hr)
Condensate	0.6	8.2	60	60	519.67	7.05	260	76.93	1.10	549.5
Produced Water ⁵	0.6	0.37	36	60	519.67	0.19	260	0.21	0.0030	1.50

Component Fugitive Emissions

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Fugitive Emissions - Component Leaks

VOC Fugitive Emissions						
Equipment Type and Service	Number of Units ¹	Hours of Operation (hours/yr)	THC Emission Factor ² (kg/hr-unit)	VOC Weight Fraction ²	THC Emissions (tpy)	VOC Emissions (tpy)
Flanges - Gas Service	548	8,760	3.90E-04	0.20	2.07	0.42
Valves - Gas Service	773	8,760	4.50E-03	0.20	33.67	6.76
Compressor Seals Gas Service	39	8,760	8.80E-03	0.20	3.32	0.67
Total Emissions (tons/yr)					39.06	7.84

HAPs Fugitive Emissions								
Equipment Type and Service	Benzene Weight Fraction ³	Benzene Emissions (tpy)	Toluene Weight Fraction ²	Toluene Emissions (tpy)	Ethylbenzene Weight Fraction ²	Ethylbenzene Emissions (tpy)	Xylene Weight Fraction ²	Xylene Emissions (tpy)
Flanges - Gas Service	0.00018	0.00038	0.00022	0.00046	---	---	0.00010	0.00021
Valves - Gas Service	0.00018	0.0062	0.00022	0.0075	---	---	0.00010	0.0034
Compressor Seals Gas Service	0.00018	0.00061	0.00022	0.00074	---	---	0.00010	0.00034
Total Emissions (tons/yr)		0.0072		0.0086		---		0.0040

1) Component counts from Engineering Lists.

2) API average emission factors are for oil and gas production operations - Table 2.4, EPA Protocol for Equipment Leak Emission Estimates - 1995.

GHG Fugitive Emissions								
Equipment Type	Number of Units ¹	Hours of Operation (hours/yr)	Emission Factor ² (scf/hr-unit)	CH ₄ Concentration ³	CO ₂ Concentration ³	CH ₄ Emissions (tpy)	CO ₂ Emissions (tpy)	CO ₂ e Emissions (tpy)
Flanges	548	8,760	0.003	0.98	0.011	0.27	0.008	6.75
Valves	773	8,760	0.027	0.98	0.011	3.42	0.11	85.67
Compressor Seals	39	8,760	0.300	0.98	0.011	1.92	0.06	48.03
Total Emissions (tons/yr)						5.61	0.17	140.44

1) Component counts from Engineering Lists.

2) Emission factors from 40 CFR Part 98 Subpart W, Table W1-A; Gas service where available, else light crude service

3) CH₄ and CO₂ concentrations as defined in 40 CFR Part 98.233(r)

Fugitive Emissions From Venting Episodes

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Fugitive Emissions-Venting Episodes

VOC Venting Emissions						
Type of Event ¹	Number Of Events (event/yr)	Amount Vented per Event (scf/event)	Molecular Weight of Vented Gas (lb/lb-mol)	Total Emissions (ton/yr)	VOC Weight Fraction ⁴	VOC Emissions (ton/yr)
Compressor Blowdown ²	156	10,000	21.32	43.82	0.20	8.58
Compressor Startup ³	156	1,050	21.32	4.60	0.20	0.90
Plant Shutdown	2	100,000	21.32	5.62	0.20	1.10
Pigging Venting	26	1,000	21.32	0.73	0.20	0.14
Total Emissions (tons/yr)						10.73

HAPs Venting Emissions								
Type of Event ¹	Benzene Weight Fraction ⁴	Benzene Emissions (tpy)	Toluene Weight Fraction ⁴	Toluene Emissions (tpy)	Ethylbenzene Weight Fraction ⁴	Ethylbenzene Emissions (tpy)	Xylene Weight Fraction ⁴	Xylene Emissions (tpy)
Compressor Blowdown ²	0.00018	0.0080	0.00022	0.0095	---	---	0.00010	0.0044
Compressor Startup ³	0.00018	0.00084	0.00022	0.0010	---	---	0.00010	0.00046
Plant Shutdown	0.00018	0.0010	0.00022	0.0012	---	---	0.00010	0.00056
Pigging Venting	0.00018	0.00013	0.00022	0.00016	---	---	0.00010	0.000073
Total Emissions (tons/yr)		0.010		0.012		---		0.0055

GHG Venting Emissions								
Type of Event ¹	Number Of Events (event/yr)	Amount Vented per Event (scf/event)	Molecular Weight of Vented Gas (lb/lb-mol)	CH ₄ Weight Fraction ⁴	CO ₂ Weight Fraction ⁴	CH ₄ Emissions (ton/yr)	CO ₂ Emissions (ton/yr)	CO ₂ e Emissions (tpy)
Compressor Blowdown ²	156	10,000	21.32	0.56	0.0029	24.73	0.13	618.34
Compressor Startup ³	156	1,050	21.32	0.56	0.0029	2.60	0.013	64.93
Plant Shutdown	2	100,000	21.32	0.56	0.0029	3.17	0.016	79.27
Pigging Venting	26	1,000	21.32	0.56	0.0029	0.41	0.0021	10.31
Total Emissions (tons/yr)						30.91	0.16	772.85

- 1) Estimated number of events and venting per event from engineering based on other facilities
- 2) Total number of compressor blowdowns based on 12 blowdowns per compressor.
- 3) Total number of compressor startups based on 12 starts per compressor.
- 4) Weight Fraction is from a gas analysis that will be typical for the facility

Fugitive Dust Emissions

Company:	Antero Midstream LLC
Facility Name:	Monroe Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Fugitive Dust Emissions

Gravel Access Road	Loaded Truck Weight ¹	Trips per year ²	Trips per day ²	Distance per round trip (truck in and out) ³		VMT per year ⁴
	tons			feet	miles	miles
Condensate Tank Truck	40.00	365	1.0	2,746	0.52	190
Produced Water Tank Truck	40.00	365	1.0	2,746	0.52	190

Equation Parameter	PM-10/PM2.5	PM-Total
E , annual size-specific emission factor for PM ₁₀ & PM _{2.5} (upaved industrial roads) extrapolated for natural mitigation ⁶	see table below	see table below
k , Particle size multiplier for particle size range (PM ₁₀), (lb/VMT) (Source: AP-42 Table 13.2.2-2)	1.5	4.9
k , Particle size multiplier for particle size range (PM _{2.5}), (lb/VMT) (Source: AP-42 Table 13.2.2-2)	0.15	
s , surface material silt content, (%) (Source: AP-42 Table 13.2.2-1)	4.8	4.8
W , mean weight (tons) of the vehicles traveling the road	40.00	40.00
a , constant for PM ₁₀ and PM _{2.5} on industrial roads (Source: AP-42 Table 13.2.2-2)	0.9	0.7
b , constant for PM ₁₀ and PM _{2.5} on industrial roads (Source: AP-42 Table 13.2.2-2)	0.45	0.45
P , number of "wet" days with at least 0.254 mm (0.01 in) of precipitation during the averaging period, based on AP-42 Figure 13.2.2-1.	160	160

$$E = \left[k \left(\frac{s}{12} \right)^a \times \left(\frac{W}{3} \right)^b \right] \times (365 - P/365)$$

Source of Equation: AP-42 Section 13.2.2

PM₁₀ Emissions

Emission Factor (lb/VMT)	Vehicle miles traveled (VMT/yr) ⁴	Annual Uncontrolled PM ₁₀ Emissions (tpy)
1.18	379.60	0.22

PM_{2.5} Emissions (tons/yr)

Emission Factor (lb/VMT)	Vehicle miles traveled (VMT/yr) ⁴	Annual Uncontrolled PM _{2.5} Emissions (tpy)
0.118	379.60	0.022

PM- Total Emissions (tons/yr)

Emission Factor (lb/VMT)	Vehicle miles traveled (VMT/yr) ⁴	Annual Uncontrolled PM-Total Emissions (tpy)
4.65	379.60	0.88

Table Notes:

1. Loaded truck weight is based on typical weight limit for highway vehicles.
2. Based on production, it's assumed a maximum of one condensate truck (200 bbl truck) and one produced water truck (200 bbl truck) will be onsite per day.
3. Distance per round trip is based on the proposed site layout. The one way distance is measured as 0.26 miles for the gravel access road.
4. VMT/yr = Trips/yr x Roundtrip Distance
5. Hourly emissions determined from tons per year calculation using 2,000 lb/ton and 8,760 hours per year.

Facility Gas Analysis

	Blanche 1H MOL %	MW	Component Weight lb/lb-mol	Wt. Fraction
Methane	75.007	16.04	12.03	0.564
Ethane	15.315	30.07	4.61	0.216
Propane	4.990	44.10	2.20	0.103
i-Butane	0.596	58.12	0.35	0.016
n-Butane	1.366	58.12	0.79	0.037
i-Pentane	0.342	72.15	0.25	0.012
n-Pentane	0.386	72.15	0.28	0.013
Hexanes +	0.201	106.72	0.21	0.010
n-Hexane	0.100	86.18	0.09	0.004
Benzene	0.005	78.11	0.00	0.0002
Toluene	0.005	92.14	0.00	0.0002
Ethylbenzene	---	106.17	---	---
Xylenes	0.002	106.16	0.00	0.0001
Nitrogen	1.273	28.01	0.36	0.017
Carbon Dioxide	0.138	44.01	0.06	0.003
Oxygen	0.274	32.00	0.09	0.004
Totals	100.00		21.32	1.00

Heating Value (Btu/scf) 1,149.46
Molecular weight 21.32

VOC weight fraction 0.1959
Methane weight fraction 0.5644
THC weight fraction 0.9763
VOC of THC wt fraction 0.2007
CH4 of THC wt fraction 0.5781
Benzene of THC wt fraction 0.0002
Toluene of THC wt fraction 0.0002
E-benzene of THC wt fraction ---
Xylene of THC wt fraction 0.0001
n-Hexane of THC wt fraction 0.0041

GlyCalc

GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES

Case Name: Monroe Compressor Station

File Name: W:\20163815 Antero WV 2016 Comp Air Mods\2.0 Technical Information\Monroe CS\Attachment N\Gly Calc Monroe CS.ddf

Date: January 19, 2016

DESCRIPTION:

Description: Kimray 45015PV pump
72.5 MMscfd

Annual Hours of Operation: 8760.0 hours/yr

WET GAS:

Temperature: 120.00 deg. F
Pressure: 1000.00 psig
Wet Gas Water Content: Saturated

Component	Conc. (vol %)
Carbon Dioxide	0.4128
Nitrogen	1.2734
Methane	75.0069
Ethane	15.3148
Propane	4.9896
Isobutane	0.5963
n-Butane	1.3659
Isopentane	0.3416
n-Pentane	0.3862
n-Hexane	0.1000
Other Hexanes	0.2005
Benzene	0.0050
Toluene	0.0050
Xylenes	0.0020

DRY GAS:

Flow Rate: 72.5 MMSCF/day
Water Content: 7.0 lbs. H2O/MMSCF

LEAN GLYCOL:

Glycol Type: TEG
Water Content: 1.5 wt% H2O
Recirculation Ratio: 2.5 gal/lb H2O

PUMP:

Glycol Pump Type: Gas Injection
Gas Injection Pump Volume Ratio: 0.032 acfm gas/gpm glycol

FLASH TANK:

Flash Control: Combustion device
Flash Control Efficiency: 98.00 %
Temperature: 190.0 deg. F
Pressure: 35.0 psig

STRIPPING GAS:

Source of Gas: Dry Gas
Gas Flow Rate: 9.000 scfm

REGENERATOR OVERHEADS CONTROL DEVICE:

Control Device: Condenser
Temperature: 145.0 deg. F
Pressure: 14.7 psia

Control Device: Combustion Device
Destruction Efficiency: 98.0 %
Excess Oxygen: 0.0 %
Ambient Air Temperature: 0.0 deg. F

GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: Monroe Compressor Station

File Name: W:\20163815 Antero WV 2016 Comp Air Mods\2.0 Technical Information\Monroe CS\Attachment N\Gly Calc Monroe CS.ddf

Date: January 19, 2016

DESCRIPTION:

Description: Kimray 45015PV pump
72.5 MMscfd

Annual Hours of Operation: 8760.0 hours/yr

EMISSIONS REPORTS:

CONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.3572	8.573	1.5646
Ethane	0.1528	3.667	0.6692
Propane	0.0885	2.123	0.3875
Isobutane	0.0157	0.378	0.0689
n-Butane	0.0415	0.996	0.1817
Isopentane	0.0126	0.301	0.0550
n-Pentane	0.0164	0.394	0.0719
n-Hexane	0.0074	0.177	0.0323
Other Hexanes	0.0116	0.279	0.0510
Benzene	0.0313	0.752	0.1372
Toluene	0.0486	1.167	0.2131
Xylenes	0.0398	0.955	0.1744
Total Emissions	0.8235	19.764	3.6068
Total Hydrocarbon Emissions	0.8235	19.764	3.6068
Total VOC Emissions	0.3135	7.523	1.3730
Total HAP Emissions	0.1272	3.052	0.5570
Total BTEX Emissions	0.1198	2.875	0.5247

UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	17.8629	428.710	78.2395
Ethane	7.6407	183.376	33.4661
Propane	4.4244	106.186	19.3790
Isobutane	0.7868	18.884	3.4463
n-Butane	2.0746	49.791	9.0869
Isopentane	0.6280	15.071	2.7504
n-Pentane	0.8209	19.702	3.5956
n-Hexane	0.3685	8.844	1.6140
Other Hexanes	0.5818	13.964	2.5484
Benzene	1.5788	37.891	6.9151
Toluene	2.4469	58.726	10.7174
Xylenes	2.0024	48.058	8.7705
Total Emissions	41.2167	989.202	180.5293

Total Hydrocarbon Emissions	41.2167	989.202	180.5293
Total VOC Emissions	15.7132	377.116	68.8237
Total HAP Emissions	6.3966	153.518	28.0171
Total BTEX Emissions	6.0281	144.674	26.4030

FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	1.4354	34.449	6.2869
Ethane	0.7507	18.016	3.2879
Propane	0.4185	10.045	1.8332
Isobutane	0.0726	1.743	0.3182
n-Butane	0.1898	4.555	0.8313
Isopentane	0.0553	1.327	0.2422
n-Pentane	0.0709	1.702	0.3107
n-Hexane	0.0264	0.634	0.1157
Other Hexanes	0.0465	1.115	0.2035
Benzene	0.0079	0.189	0.0345
Toluene	0.0092	0.221	0.0402
Xylenes	0.0036	0.085	0.0156
Total Emissions	3.0867	74.081	13.5197
Total Hydrocarbon Emissions	3.0867	74.081	13.5197
Total VOC Emissions	0.9007	21.616	3.9450
Total HAP Emissions	0.0470	1.129	0.2060
Total BTEX Emissions	0.0206	0.495	0.0903

FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Methane	71.7681	1722.434	314.3442
Ethane	37.5327	900.785	164.3932
Propane	20.9267	502.241	91.6590
Isobutane	3.6319	87.166	15.9077
n-Butane	9.4893	227.743	41.5631
Isopentane	2.7649	66.357	12.1101
n-Pentane	3.5469	85.125	15.5353
n-Hexane	1.3209	31.703	5.7857
Other Hexanes	2.3226	55.743	10.1732
Benzene	0.3935	9.444	1.7235
Toluene	0.4594	11.025	2.0121
Xylenes	0.1778	4.268	0.7788
Total Emissions	154.3347	3704.033	675.9860
Total Hydrocarbon Emissions	154.3347	3704.033	675.9860
Total VOC Emissions	45.0339	1080.814	197.2486
Total HAP Emissions	2.3516	56.439	10.3002
Total BTEX Emissions	1.0307	24.737	4.5144

EQUIPMENT REPORTS:

CONDENSER AND COMBUSTION DEVICE

Condenser Outlet Temperature: 145.00 deg. F
 Condenser Pressure: 14.70 psia
 Condenser Duty: 1.89e-001 MM BTU/hr
 Produced Water: 18.93 bbls/day
 Ambient Temperature: 0.00 deg. F
 Excess Oxygen: 0.00 %
 Combustion Efficiency: 98.00 %
 Supplemental Fuel Requirement: 1.89e-001 MM BTU/hr

Component	Emitted	Destroyed
Methane	2.00%	98.00%
Ethane	2.00%	98.00%
Propane	2.00%	98.00%
Isobutane	2.00%	98.00%
n-Butane	2.00%	98.00%
Isopentane	2.00%	98.00%
n-Pentane	2.00%	98.00%
n-Hexane	2.00%	98.00%
Other Hexanes	2.00%	98.00%
Benzene	1.98%	98.02%
Toluene	1.99%	98.01%
Xylenes	1.99%	98.01%

ABSORBER

Calculated Absorber Stages: 1.44
 Specified Dry Gas Dew Point: 7.00 lbs. H2O/MMSCF
 Temperature: 120.0 deg. F
 Pressure: 1000.0 psig
 Dry Gas Flow Rate: 72.5000 MMSCF/day
 Glycol Losses with Dry Gas: 3.8865 lb/hr
 Wet Gas Water Content: Saturated
 Calculated Wet Gas Water Content: 102.10 lbs. H2O/MMSCF
 Specified Lean Glycol Recirc. Ratio: 2.50 gal/lb H2O

Component	Remaining in Dry Gas	Absorbed in Glycol
Water	6.84%	93.16%
Carbon Dioxide	99.80%	0.20%
Nitrogen	99.98%	0.02%
Methane	99.98%	0.02%
Ethane	99.95%	0.05%
Propane	99.93%	0.07%
Isobutane	99.92%	0.08%
n-Butane	99.89%	0.11%
Isopentane	99.90%	0.10%
n-Pentane	99.88%	0.12%
n-Hexane	99.83%	0.17%
Other Hexanes	99.86%	0.14%
Benzene	93.73%	6.27%
Toluene	92.15%	7.85%
Xylenes	87.17%	12.83%

FLASH TANK

Flash Control: Combustion device
 Flash Control Efficiency: 98.00 %
 Flash Temperature: 190.0 deg. F

Flash Pressure: 35.0 psig

Component	Left in Glycol	Removed in Flash Gas
Water	99.13%	0.87%
Carbon Dioxide	7.73%	92.27%
Nitrogen	0.98%	99.02%
Methane	1.02%	98.98%
Ethane	2.82%	97.18%
Propane	5.83%	94.17%
Isobutane	7.49%	92.51%
n-Butane	9.06%	90.94%
Isopentane	9.41%	90.59%
n-Pentane	11.00%	89.00%
n-Hexane	16.02%	83.98%
Other Hexanes	13.26%	86.74%
Benzene	80.99%	19.01%
Toluene	85.41%	14.59%
Xylenes	92.89%	7.11%

REGENERATOR

Regenerator Stripping Gas:
 Dry Product Gas Stripping Gas Flow Rate: 9.0000 scfm

Component	Remaining in Glycol	Distilled Overhead
Water	26.20%	73.80%
Carbon Dioxide	0.00%	100.00%
Nitrogen	0.00%	100.00%
Methane	0.00%	100.00%
Ethane	0.00%	100.00%
Propane	0.00%	100.00%
Isobutane	0.00%	100.00%
n-Butane	0.00%	100.00%
Isopentane	3.33%	96.67%
n-Pentane	3.08%	96.92%
n-Hexane	2.33%	97.67%
Other Hexanes	5.29%	94.71%
Benzene	6.12%	93.88%
Toluene	9.20%	90.80%
Xylenes	13.89%	86.11%

STREAM REPORTS:

WET GAS STREAM

Temperature: 120.00 deg. F
 Pressure: 1014.70 psia
 Flow Rate: 3.03e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	2.15e-001	3.09e+002

Carbon Dioxide	4.12e-001	1.45e+003
Nitrogen	1.27e+000	2.84e+003
Methane	7.48e+001	9.58e+004
Ethane	1.53e+001	3.67e+004
Propane	4.98e+000	1.75e+004
Isobutane	5.95e-001	2.76e+003
n-Butane	1.36e+000	6.32e+003
Isopentane	3.41e-001	1.96e+003
n-Pentane	3.85e-001	2.22e+003
n-Hexane	9.98e-002	6.86e+002
Other Hexanes	2.00e-001	1.38e+003
Benzene	4.99e-003	3.11e+001
Toluene	4.99e-003	3.67e+001
Xylenes	2.00e-003	1.69e+001
-----	-----	-----
Total Components	100.00	1.70e+005

DRY GAS STREAM

Temperature: 120.00 deg. F
 Pressure: 1014.70 psia
 Flow Rate: 3.02e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
-----	-----	-----
Water	1.47e-002	2.11e+001
Carbon Dioxide	4.12e-001	1.44e+003
Nitrogen	1.27e+000	2.84e+003
Methane	7.50e+001	9.58e+004
Ethane	1.53e+001	3.67e+004
Propane	4.99e+000	1.75e+004
Isobutane	5.96e-001	2.76e+003
n-Butane	1.36e+000	6.32e+003
Isopentane	3.41e-001	1.96e+003
n-Pentane	3.86e-001	2.22e+003
n-Hexane	9.98e-002	6.85e+002
Other Hexanes	2.00e-001	1.37e+003
Benzene	4.69e-003	2.92e+001
Toluene	4.61e-003	3.38e+001
Xylenes	1.74e-003	1.47e+001
-----	-----	-----
Total Components	100.00	1.70e+005

LEAN GLYCOL STREAM

Temperature: 120.00 deg. F
 Flow Rate: 1.20e+001 gpm

Component	Conc. (wt%)	Loading (lb/hr)
-----	-----	-----
TEG	9.85e+001	6.64e+003
Water	1.50e+000	1.01e+002
Carbon Dioxide	4.28e-012	2.88e-010
Nitrogen	8.56e-013	5.77e-011
Methane	8.42e-018	5.67e-016
Ethane	1.21e-007	8.18e-006
Propane	7.28e-009	4.90e-007
Isobutane	1.03e-009	6.97e-008
n-Butane	2.49e-009	1.68e-007
Isopentane	1.42e-004	9.56e-003

n-Pentane	2.00e-004	1.35e-002
n-Hexane	8.71e-005	5.87e-003
Other Hexanes	2.79e-004	1.88e-002
Benzene	1.52e-003	1.03e-001
Toluene	3.67e-003	2.47e-001
Xylenes	4.79e-003	3.23e-001

Total Components	100.00	6.74e+003

RICH GLYCOL AND PUMP GAS STREAM

Temperature: 120.00 deg. F
 Pressure: 1014.70 psia
 Flow Rate: 1.29e+001 gpm
 NOTE: Stream has more than one phase.

Component	Conc. (wt%)	Loading (lb/hr)
TEG	9.22e+001	6.63e+003
Water	5.41e+000	3.89e+002
Carbon Dioxide	5.18e-002	3.72e+000
Nitrogen	3.09e-002	2.23e+000
Methane	1.01e+000	7.25e+001
Ethane	5.37e-001	3.86e+001
Propane	3.09e-001	2.22e+001
Isobutane	5.46e-002	3.93e+000
n-Butane	1.45e-001	1.04e+001
Isopentane	4.24e-002	3.05e+000
n-Pentane	5.54e-002	3.98e+000
n-Hexane	2.19e-002	1.57e+000
Other Hexanes	3.72e-002	2.68e+000
Benzene	2.88e-002	2.07e+000
Toluene	4.38e-002	3.15e+000
Xylenes	3.48e-002	2.50e+000

Total Components	100.00	7.19e+003

FLASH TANK OFF GAS STREAM

Temperature: 190.00 deg. F
 Pressure: 49.70 psia
 Flow Rate: 2.62e+003 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	2.71e+000	3.37e+000
Carbon Dioxide	1.13e+000	3.44e+000
Nitrogen	1.14e+000	2.20e+000
Methane	6.48e+001	7.18e+001
Ethane	1.81e+001	3.75e+001
Propane	6.87e+000	2.09e+001
Isobutane	9.05e-001	3.63e+000
n-Butane	2.36e+000	9.49e+000
Isopentane	5.55e-001	2.76e+000
n-Pentane	7.12e-001	3.55e+000
n-Hexane	2.22e-001	1.32e+000
Other Hexanes	3.90e-001	2.32e+000
Benzene	7.29e-002	3.94e-001

Toluene	7.22e-002	4.59e-001
Xylenes	2.42e-002	1.78e-001

Total Components	100.00	1.63e+002

FLASH TANK GLYCOL STREAM

Temperature: 190.00 deg. F
Flow Rate: 1.25e+001 gpm

Component	Conc. (wt%)	Loading (lb/hr)

TEG	9.43e+001	6.63e+003
Water	5.49e+000	3.86e+002
Carbon Dioxide	4.09e-003	2.88e-001
Nitrogen	3.09e-004	2.17e-002
Methane	1.05e-002	7.41e-001
Ethane	1.55e-002	1.09e+000
Propane	1.84e-002	1.29e+000
Isobutane	4.18e-003	2.94e-001
n-Butane	1.35e-002	9.46e-001
Isopentane	4.08e-003	2.87e-001
n-Pentane	6.23e-003	4.38e-001
n-Hexane	3.58e-003	2.52e-001
Other Hexanes	5.05e-003	3.55e-001
Benzene	2.38e-002	1.68e+000
Toluene	3.82e-002	2.69e+000
Xylenes	3.30e-002	2.32e+000

Total Components	100.00	7.03e+003

FLASH GAS EMISSIONS

Flow Rate: 1.01e+004 scfh
Control Method: Combustion Device
Control Efficiency: 98.00

Component	Conc. (vol%)	Loading (lb/hr)

Water	6.18e+001	2.96e+002
Carbon Dioxide	3.74e+001	4.38e+002
Nitrogen	2.96e-001	2.20e+000
Methane	3.36e-001	1.44e+000
Ethane	9.39e-002	7.51e-001
Propane	3.57e-002	4.19e-001
Isobutane	4.70e-003	7.26e-002
n-Butane	1.23e-002	1.90e-001
Isopentane	2.88e-003	5.53e-002
n-Pentane	3.70e-003	7.09e-002
n-Hexane	1.15e-003	2.64e-002
Other Hexanes	2.03e-003	4.65e-002
Benzene	3.79e-004	7.87e-003
Toluene	3.75e-004	9.19e-003
Xylenes	1.26e-004	3.56e-003

Total Components	100.00	7.39e+002

REGENERATOR OVERHEADS STREAM

 Temperature: 212.00 deg. F
 Pressure: 14.70 psia
 Flow Rate: 6.63e+003 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	9.06e+001	2.85e+002
Carbon Dioxide	7.10e-002	5.46e-001
Nitrogen	1.08e-001	5.29e-001
Methane	6.38e+000	1.79e+001
Ethane	1.46e+000	7.64e+000
Propane	5.75e-001	4.42e+000
Isobutane	7.75e-002	7.87e-001
n-Butane	2.04e-001	2.07e+000
Isopentane	4.98e-002	6.28e-001
n-Pentane	6.52e-002	8.21e-001
n-Hexane	2.45e-002	3.69e-001
Other Hexanes	3.87e-002	5.82e-001
Benzene	1.16e-001	1.58e+000
Toluene	1.52e-001	2.45e+000
Xylenes	1.08e-001	2.00e+000
Total Components	100.00	3.27e+002

CONDENSER PRODUCED WATER STREAM

 Temperature: 145.00 deg. F
 Flow Rate: 5.52e-001 gpm

Component	Conc. (wt%)	Loading (lb/hr)	(ppm)
Water	1.00e+002	2.76e+002	999841.
Carbon Dioxide	4.08e-004	1.13e-003	4.
Nitrogen	1.22e-005	3.37e-005	0.
Methane	7.49e-004	2.07e-003	7.
Ethane	3.48e-004	9.63e-004	3.
Propane	2.41e-004	6.65e-004	2.
Isobutane	2.27e-005	6.28e-005	0.
n-Butane	7.73e-005	2.14e-004	1.
Isopentane	1.60e-005	4.41e-005	0.
n-Pentane	2.21e-005	6.10e-005	0.
n-Hexane	7.86e-006	2.17e-005	0.
Other Hexanes	1.02e-005	2.81e-005	0.
Benzene	4.35e-003	1.20e-002	43.
Toluene	5.33e-003	1.47e-002	53.
Xylenes	4.28e-003	1.18e-002	43.
Total Components	100.00	2.76e+002	1000000.

CONDENSER RECOVERED OIL STREAM

 Temperature: 145.00 deg. F

The calculated flow rate is less than 0.000001 #mol/hr.
 The stream flow rate and composition are not reported.

CONDENSER VENT STREAM

Temperature: 145.00 deg. F
 Pressure: 14.70 psia
 Flow Rate: 8.05e+002 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	2.25e+001	8.59e+000
Carbon Dioxide	5.83e-001	5.45e-001
Nitrogen	8.91e-001	5.29e-001
Methane	5.25e+001	1.79e+001
Ethane	1.20e+001	7.64e+000
Propane	4.73e+000	4.42e+000
Isobutane	6.38e-001	7.87e-001
n-Butane	1.68e+000	2.07e+000
Isopentane	4.10e-001	6.28e-001
n-Pentane	5.36e-001	8.21e-001
n-Hexane	2.02e-001	3.68e-001
Other Hexanes	3.18e-001	5.82e-001
Benzene	9.46e-001	1.57e+000
Toluene	1.24e+000	2.43e+000
Xylenes	8.84e-001	1.99e+000
Total Components	100.00	5.08e+001

COMBUSTION DEVICE OFF GAS STREAM

Temperature: 1000.00 deg. F
 Pressure: 14.70 psia
 Flow Rate: 1.22e+001 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Methane	6.90e+001	3.57e-001
Ethane	1.57e+001	1.53e-001
Propane	6.22e+000	8.85e-002
Isobutane	8.39e-001	1.57e-002
n-Butane	2.21e+000	4.15e-002
Isopentane	5.39e-001	1.26e-002
n-Pentane	7.05e-001	1.64e-002
n-Hexane	2.65e-001	7.37e-003
Other Hexanes	4.18e-001	1.16e-002
Benzene	1.24e+000	3.13e-002
Toluene	1.64e+000	4.86e-002
Xylenes	1.16e+000	3.98e-002
Total Components	100.00	8.23e-001

Attachment O.
Monitoring, Recordkeeping, Reporting, and Testing Plans

Monitoring, Recordkeeping, Reporting, and Testing Plans

The following is a summary of the methods to comply with the requirements of West Virginia Division of Air Quality (WVDAQ) 45CSR13 rules and regulations for the Monroe Compressor Station, including federal and state regulatory requirements.

1. Summary of Key Operational Throughput Limits

- a. Maximum wet gas throughput into each Dehy: 72.5 MMscf/day or 26,463 MMscf/year.
- b. Maximum liquids loaded out: 2,989,350 gallons per year.
- c. Maximum fuel use of all compressor engines is 1,380 MMscf/year

2. Operational Requirements

- a. Compressor engines will operate with the catalytic converter in place at all times and will be fueled by natural gas only.
- b. Catalysts installed on all compressor engines will be operated per manufacturer instructions.
- c. Replace reciprocating compressor rod packing within 36 months of last packing/startup or within 26,000 operating hours, whichever comes first.
- d. Microturbines must be fueled by natural gas only.
- e. Operate each Dehy Reboiler at no more than 1.5 MMBtu/hr and fuel only by natural gas or off-gases from the Dehydrator flash tanks.
- f. No fuel-burning unit of any kind will have opacity greater than 10 percent based on a six minute block average observation.
- g. The Dehy Flare capacity will not exceed 4.80 MMBtu/hr, will achieve 98 percent destruction efficiency, will operate at all times that gas is vented to it, will have a flame present at all times, and will have no visible emissions other than for periods not to exceed a total of 5 minutes during any 2 consecutive hours.
- h. The flare will be operated per manufacturer instructions.
- i. Produced water, Condensate, and Settling storage tanks potential emissions shall be routed to the VRU with recovery greater than 98 percent at all times.
- j. Storage tanks must be covered and routed to a closed vent system with no detectable emissions.
- k. Liquid loadout trucks must use the submerged-fill method.
- l. Dehydrator still vents must be controlled by the flare.
- m. Dehydrator flash tank vent gas is to be used in the reboiler as fuel or routed to the VRU system.

3. Monitoring

- a. Non-certified engines must be stack tested within 1 year of startup and every 8,760 hours of operation thereafter.
- b. Monitor catalyst inlet temperature.

- c. Monitor compressor run time or track number of months since compressor rod repacking.
- d. Monitor daily, monthly, and rolling 12-month average wet gas throughput for the Dehy.
- e. Conduct an initial Method 22 observation of the Reboiler exhaust and flare for a minimum of 2 hours.
- f. Monthly conduct Method 22 observations of the Reboiler exhaust and flare for a minimum of 10 minutes each.
- g. Monthly conduct olfactory, visual, and auditory inspections of the tanks closed vent and control system (flare) for leaks or defects that could result in emissions. Repair leaks as soon as practicable (no later than 5 days for first attempt).
- h. Continuously monitor presence of flare flame.
- i. Monitor monthly and rolling twelve-month average amount of liquids loaded out.

4. Recordkeeping

- a. Keep records on-site for a minimum of 2 years, and in company records (on or off-site) for a minimum of 5 years.
- b. Keep records of inspection, observations, preventive maintenance, malfunctions, and shutdowns of all onsite equipment.
- c. Keep records of the date, time, duration of each time that a flame is not present at the flare and startup, shutdown, malfunctions of the flare.
- d. Keep records of engine maintenance and engine run time.
- e. Keep records of catalyst inlet temperature.
- f. Keep records of the actual annual average natural gas throughput in the dehy.

5. Notifications and Reports

- a. Notify WVDAQ within 30 calendar days of startup.
- b. Upon startup, file a Certificate to Operate (CTO) application and pay fees to WVDAQ for the period from startup to the following June 30 and then annually renew the CTO and pay fees. Maintain CTO on-site.
- c. File an annual report of compliance with 40 CFR 60 Subpart OOOO for the compressors and storage tanks (for settling tank only) within 90 days after one year of operation (i.e., within 90 days after 12 months after initial startup).
- d. For stack testing, file protocol at least 30 days prior to test and notify WVDAQ and EPA of the test at least 15 days prior to test. Report results within 60 days of test.
- e. If operations are suspended for 60 days or more, notify WVDAQ within 2 weeks after the 60th day.

**Attachment P.
Public Notice**

AIR QUALITY PERMIT NOTICE
Notice of Application – Monroe Compressor Station

Notice is given that Antero Midstream LLC has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a modification to the existing 45CSR13 Construction Permit R13-3184A for a Natural Gas Compressor Station located north of Conaway Run Road (Co Rd 48) near Alma, in Tyler County, West Virginia. The latitude and longitude coordinates are: 39.4206N, 80.8638W.

The applicant estimates the increased potential to discharge of the following Regulated Air Pollutants will be: Sulfur Dioxide (SO₂) - 0.11 tpy; Particulate Matter less than 10 µm (PM₁₀) - 3.64 tpy; Particulate Matter less than 2.5 µm (PM_{2.5}) - 3.63 tpy; Benzene – 0.27 tpy; Toluene – 0.09 tpy; Ethylbenzene – 0.005 tpy; Xylenes – 0.07 tpy; and Carbon Dioxide equivalent (CO_{2e}) - 26,636 tpy.

The applicant estimates the decreased potential to discharge of the following Regulated Air Pollutants will be: Nitrogen Oxides (NO_x) - 16.00 tons per year (tpy); Carbon Monoxide (CO) - 14.83 tpy; Volatile Organic Compounds (VOC) - 28.09 tpy; and Formaldehyde: 0.87 tpy.

Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1250, during normal business hours.

Dated the 27th day of January 2016.

By: Antero Midstream LLC
Barry Schatz
Midstream Environmental Supervisor
1615 Wynkoop Street
Denver, CO 80202

Attachment R.
Authority/Delegation of Authority

Attachment R
AUTHORITY OF CORPORATION
OR OTHER BUSINESS ENTITY (DOMESTIC OR FOREIGN)

TO: The West Virginia Department of Environmental Protection,
Division of Air Quality

DATE: August 5, 2015

ATTN.: Director

Corporation's / other business entity's Federal Employer I.D. Number 46-5517375

The undersigned hereby files with the West Virginia Department of Environmental Protection, Division of Air Quality, a permit application and hereby certifies that the said name is a trade name which is used in the conduct of an incorporated business or other business entity.

Further, the corporation or the business entity certifies as follows:

(1) Luz Slauter and Barry Schatz (is/are) the authorized representative(s) and in that capacity may represent the interest of the corporation or the business entity and may obligate and legally bind the corporation or the business entity.

(2) The corporation or the business entity is authorized to do business in the State of West Virginia.

(3) If the corporation or the business entity changes its authorized representative(s), the corporation or the business entity shall notify the Director of the West Virginia Department of Environmental Protection, Division of Air Quality, immediately upon such change.


Ward McNeilly, Vice President - Vice President Reserves Planning & Midstream

President or Other Authorized Officer
(Vice President, Secretary, Treasurer or other official in charge of a principal business function of the corporation or the business entity)

(If not the President, then the corporation or the business entity must submit certified minutes or bylaws stating legal authority of other authorized officer to bind the corporation or the business entity).

Secretary

Antero Midstream LLC
Name of Corporation or business entity