

February 15, 2016

Mr. Roy Kees, P.E. WV Department of Environmental Protection Division of Air Quality 601 57th Street, SE Charleston, WV 25304

RE: Antero Midstream LLC – Underwood Compressor Station West Virginia Department of Environmental Protection, Division of Air Quality, 45CSR13 Air Permit Modification, R13-3281

Dear Mr. Kees,

On behalf of Antero Midstream LLC, please find attached the 45CSR13 Air Permit Modification for permit number R13-3281 for the Underwood Compressor Station (Facility ID 095-00065) located in Tyler County, West Virginia. A summary of the modifications in this application include:

1. Updating compressor engine emissions to reflect catalyst data based on a new catalyst design from the manufacturer,

2. The installation of two new compressor engines and associated blowdown events,

3. Eliminating the compressor fuel use limit and synthetic minor status,

4. Increasing the dehydrator throughput to 88 MMscfd per dehydrator, and

5. Modifying the dehydrator flash tank control efficiency based on new standardized guidance from WVDEP.

Enclosed are one hardcopy and two CDs containing the entire permit application including the application form and required attachments. Per 45CSR22, a \$4,500 application fee is also enclosed, which covers the base 45CSR13 \$1,000 application fee, an additional \$1,000 for NSPS requirements, and an additional \$2,500 for Hazardous Air Pollutant requirements.

A copy of the Air Quality Permit Notice for the advertisement is included as Attachment P. As the Notice is being submitted simultaneously with the application, the official affidavit of publication will be submitted to the Division of Air Quality separately once it is completed.

Please call if you have any questions or if I can be of further assistance. I can be reached at (719)632-3593 or by email at <u>msteyskal@kleinfelder.com</u>.

Sincerely, **KLEINFELDER**

Michele Stephel

Michele Steyskal Air Quality Specialist

Enclosures: Underwood Compressor Station R13-3281 Air Permit Modification

20163815/DEN16O34563 © 2016 Kleinfelder Page 1 of 1

February 15, 2016

Antero Midstream LLC

Underwood Compressor Station

NSR Permit Application West Virginia Department of Environmental Protection Division of Air Quality 45CSR13

Tyler County, West Virginia

February 2016

Prepared by:

KLEINFELDER Bright People. Right Solutions.

1801 California Street, Suite 1100 Denver, CO 80202 (303) 237-6601 Fax (303) 237-6602 <u>www.kleinfelder.com</u>

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WEST VIRGINIA DEPARTMENT OF ENVIRONMENTAL PROTECTION DIVISION OF AIR QUALITY 601 57 th Street, SE Charleston, WV 25304 (304) 926-0475 WWW.dep.wv.gov/dag		LICATION FOR NSR PERMIT AND TLE V PERMIT REVISION (OPTIONAL)	
PLEASE CHECK ALL THAT APPLY TO NSR (45CSR13) (IF KNC CONSTRUCTION MODIFICATION RELOCATION CLASS I ADMINISTRATIVE UPDATE TEMPORARY		TYPE OF 45CSR30 (TITLE V) REVISION (IF ANY): TIVE AMENDMENT Iminor modification MODIFICATION DVE IS CHECKED, INCLUDE TITLE V REVISION	
CLASS II ADMINISTRATIVE UPDATE AFTER-THE-FA	INFORMATION A Revision Guidance" in or	AS ATTACHMENT S TO THIS APPLICATION	
Sect	ion I. General		
1. Name of applicant (as registered with the WV Secretary Antero Midstream LLC	of State's Office):	2. Federal Employer ID No. (FEIN): 46-5517375	
 Name of facility (<i>if different from above</i>): Underwood Compressor Station 		4. The applicant is the:	
5A. Applicant's mailing address: 1615 Wynkoop Street Denver, CO 80202	5B. Facility's pres Wheelers Run Road Centerville, WV 263		
 6. West Virginia Business Registration. Is the applicant a resident of the State of West Virginia? YES NO If YES, provide a copy of the Certificate of Incorporation/Organization/Limited Partnership (one page) including any name change amendments or other Business Registration Certificate as Attachment A. If NO, provide a copy of the Certificate of Authority/Authority of L.L.C./Registration (one page) including any name change amendments or other Business Certificate as Attachment A. 			
7. If applicant is a subsidiary corporation, please provide th	e name of parent corpo	pration:	
 8. Does the applicant own, lease, have an option to buy or otherwise have control of the <i>proposed site</i>? XES NO If YES, please explain: Antero Midstream LLC owns the land for the proposed site If NO, you are not eligible for a permit for this source. 			
 9. Type of plant or facility (stationary source) to be constructed, modified, relocated, administratively updated or temporarily permitted (e.g., coal preparation plant, primary classification System (NAICS) code for the facility: 221210 			
11A. DAQ Plant ID No. (for existing facilities only): 095 – 00065		SR13 and 45CSR30 (Title V) permit numbers s process (for existing facilities only):	
I All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone			

12A.

 For Modifications, Administrative Updates or Temporary permits at an existing facility, please provide directions to the present location of the facility from the nearest state road; 					
- For Construction or Relocation permits , please provide directions to the proposed new site location from the nearest state					
road. Include a MAP as Attachment B.					
From Centerville, WV, head west on Wheelers Run Road	d for approximately 1.6 miles. Turn left i	nto the facility driveway.			
12.B. New site address (if applicable):	12C. Nearest city or town:	12D. County:			
Wheelers Run Road	Centerville	Tyler			
Centerville, WV 26320					
12.E. UTM Northing (KM): 4364.783	12F. UTM Easting (KM): 511.052	12G. UTM Zone: 17			
13. Briefly describe the proposed change(s) at the facilit	y:				
The reduction efficiencies for the engine catalysts have a engines have been added. The dehydrator throughput h the compressors has been removed so the facility is no l	as been increased to 88 MMscfd per de				
 14A. Provide the date of anticipated installation or change If this is an After-The-Fact permit application, providence of the providence of the permit application of the per	-	14B. Date of anticipated Start-Up if a permit is granted: June 2016			
14C. Provide a Schedule of the planned Installation of/ application as Attachment C (if more than one uni					
15. Provide maximum projected Operating Schedule o Hours Per Day 24 Days Per Week 7	·	ation:			
16. Is demolition or physical renovation at an existing fa	cility involved? 🗌 YES 🛛 🕅 NO				
17. Risk Management Plans. If this facility is subject to	112(r) of the 1990 CAAA, or will becom	ne subject due to proposed			
changes (for applicability help see www.epa.gov/cepp	oo), submit your Risk Management Pla	n (RMP) to U. S. EPA Region III.			
18. Regulatory Discussion. List all Federal and State air pollution control regulations that you believe are applicable to the					
proposed process (if known). A list of possible applicable requirements is also included in Attachment S of this application					
(Title V Permit Revision Information). Discuss applicability and proposed demonstration(s) of compliance (if known). Provide this					
information as Attachment D.					
Section II. Additional att	achments and supporting d	ocuments.			
19. Include a check payable to WVDEP – Division of Air Quality with the appropriate application fee (per 45CSR22 and					
45CSR13).					
20. Include a Table of Contents as the first page of your application package.					
 Provide a Plot Plan, e.g. scaled map(s) and/or sketch(es) showing the location of the property on which the stationary source(s) is or is to be located as Attachment E (Refer to Plot Plan Guidance). 					
 Indicate the location of the nearest occupied structure (e.g. church, school, business, residence). 					
22. Provide a Detailed Process Flow Diagram(s) showing each proposed or modified emissions unit, emission point and control device as Attachment F.					
23. Provide a Process Description as Attachment G.					
 Also describe and quantify to the extent possible all changes made to the facility since the last permit review (if applicable). 					
All of the required forms and additional information can be	All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.				

24. Provide Material Safety Data Sheets (MSDS) for all materials processed, used or produced as Attachment H.				
 For chemical processes, provide a MSDS for each compound emitted to the air. 				
25. Fill out the Emission Units Table and provide it as Attachment I.				
26. Fill out the Emission Points Data Summary Sheet (Table 1 and Table 2) and provide it as Attachment J.				
27. Fill out the Fugitive Emissions Data Summary Sheet and provide it as Attachment K.				
28. Check all applicable Emissions Un	it Data Sheets listed below:			
Bulk Liquid Transfer Operations	Haul Road Emissions	Quarry		
Chemical Processes	Hot Mix Asphalt Plant	Solid Materials Sizing, Handling and Storage		
Concrete Batch Plant	Incinerator	Facilities		
Grey Iron and Steel Foundry	Indirect Heat Exchanger	. 🔲 Storage Tanks		
General Emission Unit, specify: Engi	nes, Dehydrator			
Fill out and provide the Emissions Unit	Data Sheet(s) as Attachment	L.		
29. Check all applicable Air Pollution C	Control Device Sheets listed b	elow:		
Absorption Systems	Baghouse	Flare		
Adsorption Systems	Condenser	Mechanical Collector		
Afterburner	Electrostatic Precip	itator Wet Collecting System		
Other Collectors, specify: Catalysts				
Fill out and provide the Air Pollution Co	ntrol Device Sheet(s) as Atta	chment M.		
30. Provide all Supporting Emissions Items 28 through 31.	Calculations as Attachment N	I , or attach the calculations directly to the forms listed in		
testing plans in order to demonstrate	 Monitoring, Recordkeeping, Reporting and Testing Plans. Attach proposed monitoring, recordkeeping, reporting and testing plans in order to demonstrate compliance with the proposed emissions limits and operating parameters in this permit application. Provide this information as Attachment O. 			
 Please be aware that all permits must be practically enforceable whether or not the applicant chooses to propose such measures. Additionally, the DAQ may not be able to accept all measures proposed by the applicant. If none of these plans are proposed by the applicant, DAQ will develop such plans and include them in the permit. 				
32. Public Notice. At the time that the application is submitted, place a Class I Legal Advertisement in a newspaper of general				
circulation in the area where the source is or will be located (See 45CSR§13-8.3 through 45CSR§13-8.5 and Example Legal				
Advertisement for details). Please submit the Affidavit of Publication as Attachment P immediately upon receipt.				
33. Business Confidentiality Claims. Does this application include confidential information (per 45CSR31)?				
If YES, identify each segment of information on each page that is submitted as confidential and provide justification for each segment claimed confidential, including the criteria under 45CSR§31-4.1, and in accordance with the DAQ's "Precautionary Notice – Claims of Confidentiality" guidance found in the General Instructions as Attachment Q.				
Section III. Certification of Information				
34. Authority/Delegation of Authority. Only required when someone other than the responsible official signs the application. Check applicable Authority Form below:				
Authority of Corporation or Other Bus	iness Entity	Authority of Partnership		
Authority of Governmental Agency		Authority of Limited Partnership		
Submit completed and signed Authority Form as Attachment R. All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.				

35A. Certification of Information. To certify this permit application, a Responsible Official (per 45CSR§13-2.22 and 45CSR§30-2.28) or Authorized Representative shall check the appropriate box and sign below.

Certification of Truth, Accuracy, and Completeness

I, the undersigned 🖾 **Responsible Official** / 🛄 **Authorized Representative**, hereby certify that all information contained in this application and any supporting documents appended hereto, is true, accurate, and complete based on information and belief after reasonable inquiry I further agree to assume responsibility for the construction, modification and/or relocation and operation of the stationary source described herein in accordance with this application and any amendments thereto, as well as the Department of Environmental Protection, Division of Air Quality permit issued in accordance with this application, along with all applicable rules and regulations of the West Virginia Division of Air Quality and W.Va. Code § 22-5-1 et seq. (State Air Pollution Control Act). If the business or agency changes its Responsible Official or Authorized Representative, the Director of the Division of Air Quality will be notified in writing within 30 days of the official change.

Compliance Certification

Except for requirements identified in the Title V Application for which compliance is not achieved, I, the undersigned hereby certify that, based on information and belief formed after reasonable inquiry, all air contaminant sources identified in this application are in compliance with all applicable requirements.

SIGNATURE W UNVIL		DATE:	2/10/16	
-	(Please use blue ink)		(Please use blue ink)	
35B. Printed na	ame of signee: Ward McNeilly	35C. Title: Vice Pr	resident, Reserves Planning and	

		Midstream
35D. E-mail: wmcneilly@anteroresources.com	36E. Phone: (303) 357-6822	36F. FAX: (303)357-7315
36A. Printed name of contact person (if differe	nt from above): Barry Schatz	36B. Title: Senior Environmental and Regulatory Manager
36C. E-mail: <u>bschatz@anteroresources.com</u>	36D. Phone: (303) 357-7276	36E. FAX: (303)357-7315

PLEASE CHECK ALL APPLICABLE ATTACHMENTS INCLUDED WITH THIS PERMIT APPLICATION:				
 Attachment A: Business Certificate Attachment B: Map(s) Attachment C: Installation and Start Up Schedule Attachment D: Regulatory Discussion Attachment E: Plot Plan Attachment F: Detailed Process Flow Diagram(s) Attachment G: Process Description Attachment H: Material Safety Data Sheets (MSDS) Attachment I: Emission Units Table Attachment J: Emission Points Data Summary Sheet 	 Attachment K: Fugitive Emissions Data Summary Sheet Attachment L: Emissions Unit Data Sheet(s) Attachment M: Air Pollution Control Device Sheet(s) Attachment N: Supporting Emissions Calculations Attachment O: Monitoring/Recordkeeping/Reporting/Testing Plans Attachment P: Public Notice Attachment Q: Business Confidential Claims Attachment R: Authority Forms Attachment S: Title V Permit Revision Information Application Fee 			
	permit application with the signature(s) to the DAQ, Permitting Section, at the sapplication. Please DO NOT fax permit applications.			
FOR AGENCY USE ONLY - IF THIS IS A TITLE V SOURCE:				
□ Forward 1 copy of the application to the Title V Permitting Group and:				
For Title V Administrative Amendments:				
NSR permit writer should notify Title V permit writ	er of draft permit,			
For Title V Minor Modifications:				

Title V permit writer should send appropriate notification to EPA and affected states within 5 days of receipt,

☐ NSR permit writer should notify Title V permit writer of draft permit.
 ☐ For Title V Significant Modifications processed in parallel with NSR Permit revision:

NSR permit writer should notify a Title V permit writer of draft permit,

- □ Public notice should reference both 45CSR13 and Title V permits,
- EPA has 45 day review period of a draft permit.

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

Discussion of Nearby Facilities

Underwood Compressor Station – Closest Antero Facilities

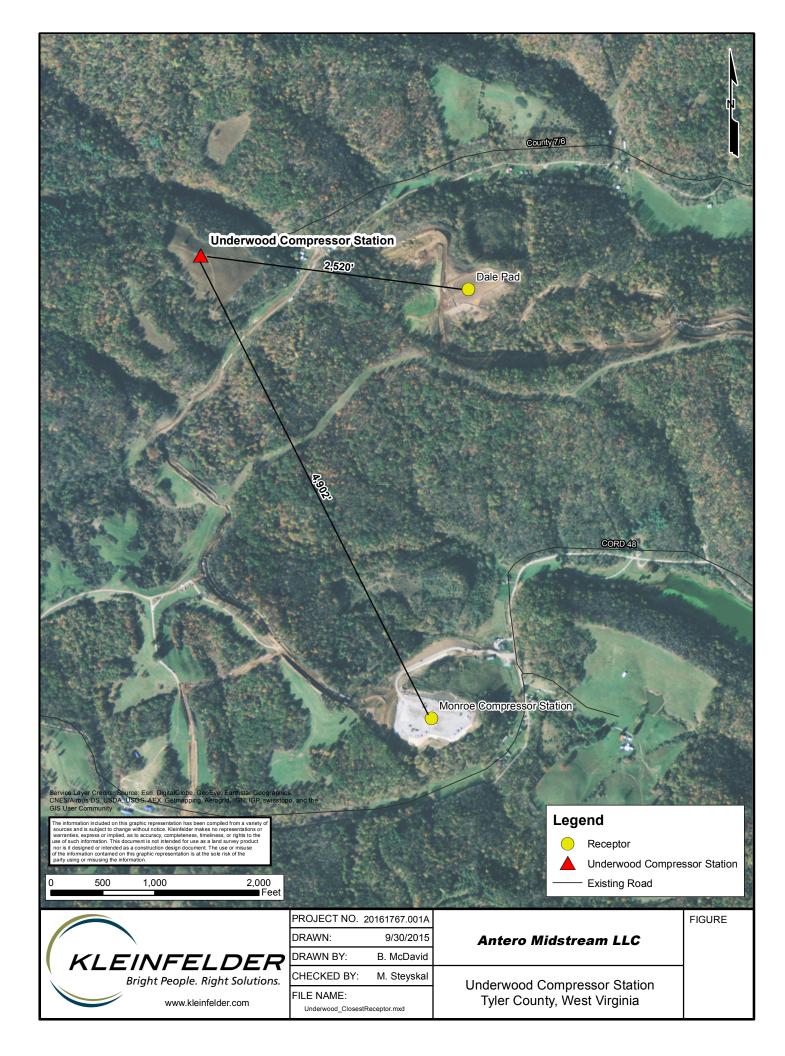
1. Common Control: Only those facilities that are owned and managed by Antero were included in the aggregation discussion. This includes Antero Resources Corporation production facilities in addition to the Antero Midstream LLC midstream facilities.

2. SIC Code: The Underwood Compressor Station will operate under SIC code 4923 (natural gas distribution). The closest facility owned by Antero Midstream LLC with this SIC code is the Monroe Compressor station which is 4,902 feet southeast of the Facility. All Antero Resources Corporation production facilities operate under the SIC code of 1311 (crude petroleum and natural gas extraction). The closest facility operated by Antero Resources Corporation with the SIC code of 1311 is the Dale Pad 2,520 feet to the east.

3. Contiguous or Adjacent: The land between the Underwood Compressor Station and its nearest facility operating under SIC code 4923 is not owned or managed by Antero Midstream LLC or Antero Resources Corporation. Therefore, the two facilities are not contiguous or adjacent. Secondly, although most of the Underwood Compressor Station land parcel border is not adjacent to any parcels operated by Antero, a small portion of the Underwood Compressor Station land parcel is adjacent to the land parcel for the Dale Pad facility operating under 1311. The actual pad locations for the Underwood Compressor Station and the Dale Pad are 2,520 feet apart and thus not contiguous.

Based on this three-pronged evaluation, although the Underwood Compressor Station and Monroe Compressor Station do belong to the same major industrial group, they should not be aggregated because they are not contiguous or adjacent.

Although a small portion of their land parcel borders are adjacent, the Underwood Compressor Station and Dale Pad should not be aggregated because they do not belong to the same major industrial group and do not directly rely on each other nor are they contiguous.



Attachment A. Business Certificate



I, Natalie E. Tennant, Secretary of State of the State of West Virginia, hereby certify that

ANTERO MIDSTREAM LLC

Control Number: 9A5E1

a limited liability company, organized under the laws of the State of Delaware

has filed its "Application for Certificate of Authority" in my office according to the provisions of West Virginia Code §31B-10-1002. I hereby declare the organization to be registered as a foreign limited liability company from its effective date of April 29, 2014, until a certificate of cancellation is filed with our office.

Therefore, I hereby issue this

CERTIFICATE OF AUTHORITY OF A FOREIGN LIMITED LIABILITY COMPANY

to the limited liability company authorizing it to transact business in West Virginia



Given under my hand and the Great Seal of the State of West Virginia on this day of April 29, 2014

talil & Your

Secretary of State

	APR 292014 IN THE OFFICE WV SECRETARY OF			Submitted by: CT Corporation Rep-Terry Terry.Stamper@wolterski 304-776-1152
Sec 190 Bidj Cha FIL (Tw star	LE ONE ORIGINAL CERTIFI	APPLICATIO CATE OF AUT D LIABILITY	HORITY OF	Penney Barker, Manager Corporations Division Tel: (304)558-8000 Fax: (304)558-8381 Website: <u>www.wwsos.com</u> E-mail: <u>business@wwsos.com</u> Office Hours: Monday – Friday 8:30 a.m. – 5:00 p.m. ET Control #
1.	The name of the company as registered home state is:	d in its	Midstream LLC	
	I UNEX NERE IO MUICALE YOU HAVE OF	btained and submit	ted with this app	lication a CERTIFICATE OF
	EXISTENCE (GOOD STANDING), di incorporation as required to process ye Secretary of State's Office in the home The name to be used in West Virginia [The name must contain one of the required t as limited liability company" or abbreviations so "LLC" or "PLLC". See instructions for complet acceptable terms and requirements for use of tra	ated during the cor our application. The estate of original in will be: Hou terms such (If uch as for e list of de name.] DBA (SL L	rent tax year, fro e certificate may corporation. ne State name as name is not availabilitow special instruc- to special instruc- to special instruction etter of Resolution	lication a <u>CERTIFICATE OF</u> m your home state of original be obtained by contacting the listed above, if available in WV e. check DBA Name box below and tions in Section 2. attached.) is in Section 2. Regarding the attached to this application.)
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3 . 4.	 EXISTENCE (GOOD STANDING), di incorporation as required to process ye Secretary of State's Office in the home. The name to be used in West Virginia [The name must contain one of the required t as limited liability company" or abbreviations st "LLC" or "PLLC". See instructions for complet acceptable terms and requirements for use of transformer to the company will be at [See instructions for on professions which may form P.L.L.C. in WV. A must have WV professional license. In most cases, Authorization/Approval from the appropriate S Licensing Board is required to process the applica. The street address of the principal officies: 	ated during the cur our application. The estate of original in events such (If uch as free list of DB/ (Second Contents) (Second Contents) ide name.] DB/ (Second Contents) (Second Contents) is a Letter of If itate the content of City/State/ Street/Rox; City/State/	rent tax year, fro e certificate may corporation. ne State name as name is not availabi- illow special instruc- to special instruction egular L.L.C. rofessional L.L.C rofessional L.L.C tip:	m your home state of original be obtained by contacting the listed above, if available in WV le. check DBA Name box below and tions in Section 2. attached.) is in Section 2. Regarding the attached to this application.) . for the profession of

WV045 - 09/04/2013 Wolters Kluwe: Online

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APPLICATION FOR CERTIFICATE OF AUTHORITY OF LIMITED LIABILITY COMPANY Page 2

7.	E-mail address where business correspondence may be received:
8.	Website address of the business, if any:
9.	The company is: an at-will company, for an indefinite period a term company, for the term of years, which will expire on
10.	The company is: member-managed. [List the names and addresses of all members.] manager-managed. [List the names and addresses of all managers.]
	List the Name(s) and Address(es) of the Member(s)/Manager(s) of the company (attach additional pages if necessary).
	Name Street Address City, State, Zip
	Antero Resources Corporation 1625 17th Street, Suite 300 Denver, Colorado 80202
11.	All or specified members of a limited liability company are liable in their capacity as members for all or specified debts, obligations or liabilities of the company. Yes- Those persons who are liable in their capacity as members for all debts, obligations or liability of the company have consented in writing to the adoption of the provision or to be bound by the provision.
12.	The purpose for which this limited liability company is formed are as follows: (Describe the type(s) of business activity which will be conducted, for example, "real estate." "construction of residentia and commercial buildings," "commercial printing," "professional practice of architecture.")
	Midstream oil and gas operating company
13.	Is the business a Scrap Metal Dealer?
	Yes [If "Yes," you must complete the Scrap Metal Dealer Registration Form (Form SMD-1) and proceed to question 14.].
	No [Proceed to question 14.]

14. The number of pages attached and included in this application is: ______

Form LLF+1

Issued by the Office of the Secretary of State

Revised 8/13

WV045 - 09/04/2013 Wolters Kluwer Online

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APPLICATION FOR CERTIFICATE OF AUTHORITY OF LIMITED LIABILITY COMPANY Page 3

15. The requested effective date is:	the date & time of filing in	the Secretary of State's Office
[Requested date <u>may not be earlier than</u> <u>filing nor later than 90 days after filing</u> <u>in our office.</u>]	the following date	and time

16. Contact and Signature Information* (See below Important Legal Notice Regarding Signature):

a.	Alvyn A. Schopp	(313) 357-7310
	Contact Name	Phone Number
ь.	Alvyn A. Schopp	Chief Administrative Officer and Regional Vice President
0.	Print or type name offait ar	Title / Capacity of Signer
c.	Hz-Tochopp	April 28, 2014
	Signature /	Date

*Important Legal Notice Regarding Signature: Per West Virginia Code §31B-2-209. Liability for false statement in filed record. If a record authorized or required to be filed under this chapter contains a false statement, one who suffers loss by reliance on the statement may recover damages for the loss from a person who signed the record or caused another to sign it on the person's behalf and knew the statement to be false at the time the record was signed.

Form LLF-1

Issued by the Office of the Secretary of State

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Revised 8/13

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Delaware

PAGE 1

The First State

I, JEFFREY W. BULLOCK, SECRETARY OF STATE OF THE STATE OF DELAWARE, DO HEREBY CERTIFY "ANTERO MIDSTREAM LLC" IS DULY FORMED UNDER THE LAWS OF THE STATE OF DELAWARE AND IS IN GOOD STANDING AND HAS A LEGAL EXISTENCE SO FAR AS THE RECORDS OF THIS OFFICE SHOW, AS OF THE TWENTY-NINTH DAY OF APRIL, A.D. 2014.

AND I DO HEREBY FURTHER CERTIFY THAT THE ANNUAL TAXES HAVE NOT BEEN ASSESSED TO DATE.



5466900 8300

140532521 You may verify this certificate online at corp.delaware.gov/authver.shtml

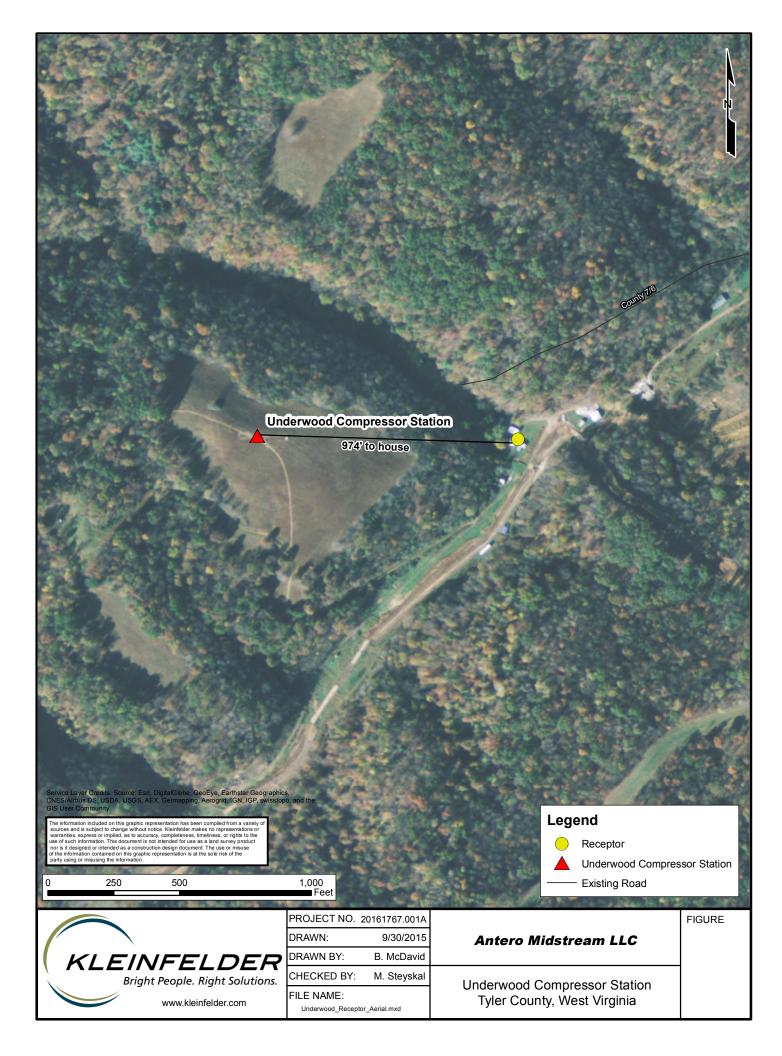
••••

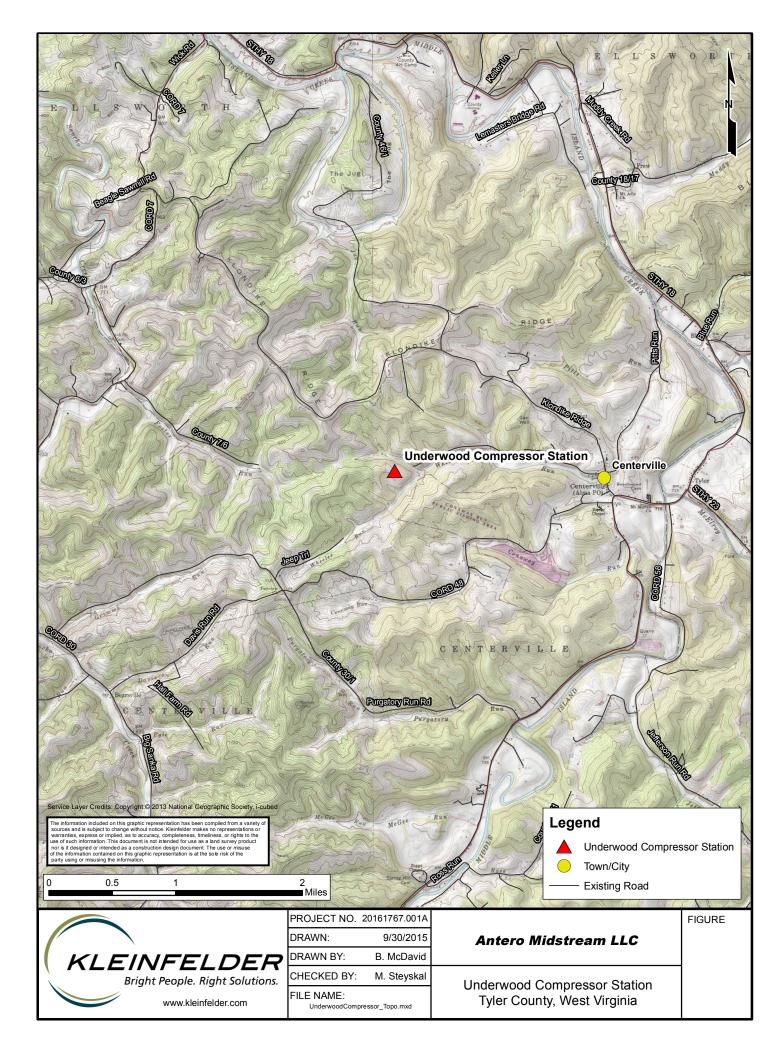
Jeffrey W. Bullock, Secretary of State

AUTHENTICATION: 1328067

DATE: 04-29-14

Attachment B. Area Map





Attachment C. Installation and Startup Schedule

Underwood Compressor Station – Installation and Startup Schedule

The Underwood Compressor Station will be a new facility located in Tyler County, WV, approximately 1.7 miles west of Centerville, WV. Existing equipment will be installed and operated per permit R13-3281. The proposed equipment is scheduled to be installed and operational around June 1, 2016 with construction starting in April 2016.

Attachment D. Regulatory Discussion

Underwood Compressor Station – Regulatory Discussion

Federal Regulations

40 CFR Part 60 – Standards of Performance for New Stationary Sources

I. Subpart Kb - Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, 1984.

<u>Applicability:</u> Subpart Kb applies to volatile organic liquid storage tanks with a capacity greater than or equal to 75 m³ (§60.110b(a)). Storage vessels with a design capacity less than 1,589.874 m3 do not apply to this subpart if they are used store condensate prior to custody transfer. The condensate and produced water storage tanks at the Underwood Compressor Station are 64 m³. The settler tank is 79 m³, but stores condensate prior to custody transfer. Therefore, Subpart Kb does not apply to the Underwood Compressor Station.

II. Subpart GG - Standards of Performance for Stationary Gas Turbines

<u>Applicability:</u> Subpart GG applies to all stationary gas turbines with a heat input at peak load equal to or greater than 10 million BTU per hour based on the lower heating value of the fuel (§60.330(a)). Since the microturbine generators at the Underwood Compressor Station have a heat input rating less than 10 million Btu per hour, Subpart GG does not apply.

III. Subpart KKK - Standards of Performance for Equipment Leaks of VOC from Onshore Natural Gas Processing Plants for Which Construction, Reconstruction, or Modification Commenced After January 20, 1984, and on or Before August 23, 2011.

<u>Applicability:</u> Subpart KKK applies to facilities built or modified before August 23, 2011, so Subpart KKK will not apply as the Underwood Compressor Station was constructed after August 23, 2011.

IV. Subpart LLL - Standards of Performance for SO₂ Emissions from Onshore Natural Gas Processing for Which Construction, Reconstruction, or Modification Commenced After January 20, 1984, and on or Before August 23, 2011.

<u>Applicability:</u> Subpart LLL applies to facilities built or modified before August 23, 2011, so Subpart LLL will not apply as the Underwood Compressor Station was constructed after August 23, 2011.

V. Subpart JJJJ - Standards of Performance for Stationary Spark Ignition Internal Combustion Engines

<u>Applicability:</u> Subpart JJJJ applies to rich burn engines that were ordered after June 12, 2006 and manufactured on or after July 1, 2007 for engines with maximum power

greater than or equal to 500 hp (§60.4230(a)(4)(i)). Thus, Subpart JJJJ applies to the Underwood Compressor Station as the compressor engines will be installed in 2016 and are new engines manufactured after July 1, 2007.

VI. Subpart KKKK - Standards of Performance for Stationary Combustion Turbines

<u>Applicability:</u> Subpart KKKK applies to all stationary combustion turbines with a heat input at peak load equal to or greater than 10 million BTU per hour based on the higher heating value of the fuel (§60.4305(a)). Since the microturbine generators at the Underwood Compressor Station have a heat input rating less than 10 million Btu per hour, Subpart KKKK does not apply.

VII. Subpart OOOO - Standards of Performance for Crude Oil and Natural Gas Production, Transmission, and Distribution

<u>Applicability:</u> Subpart OOOO applies to reciprocating compressor facilities that were constructed, modified, or reconstructed after August 23, 2011 (§60.5365(c)). Additionally, Subpart OOOO applies to storage vessel affected facilities with individual tank emissions greater than 6 tons per year (§60.5365(e)). Thus, Subpart OOOO applies to the Underwood Compressor Station as it was constructed after August 23, 2011 and has reciprocating compressors and a settler tank that has controlled VOC potential to emit greater than six (6) tons per year. The pneumatic controllers installed at Underwood Compressor Station are air-actuated and therefore exempt from the requirements of this subpart.

40 CFR Part 61 – National Emission Standards for Hazardous Air Pollutants

I. Subpart V – National Emission Standard for Equipment Leaks (Fugitive Emission Sources)

<u>Applicability:</u> Subpart V applies to components such as compressors, valves, and pumps that are intended to operate in volatile hazardous air pollutant (VHAP) service (§61.240(a)). VHAP service means that a component contains or contacts a fluid that is at least 10 percent by weight a VHAP. Subpart V does not apply to the Underwood Compressor Station because none of the components have fluid (natural gas, water, or condensate) that is over 10 percent by weight of any VHAP.

40 CFR Part 63 – National Emission Standards for Hazardous Air Pollutants for Source Categories

I. Subpart HH – National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities

<u>Applicability:</u> Subpart HH applies to oil and natural gas production facilities that are a major or area source of HAP emissions, and that process, upgrade, or store hydrocarbon liquids or natural gas prior to the transmission and storage source category

(§63.760(a)). Subpart HH does apply to the Underwood Compressor Station, and because it is an area source of HAP emissions, the two (2) TEG dehydrators are applicable sources under Subpart HH (§63.760(b)(2)). However, actual benzene emissions from the dehydrators at the Underwood Compressor Station are less than 1 ton per year, so both dehydrators are exempt from all requirements except recordkeeping (§63.764(e)(1)(ii)).

II. Subpart HHH – National Emission Standards for Hazardous Air Pollutants from Natural Gas Transmission and Storage Facilities

<u>Applicability:</u> Subpart HHH applies to natural gas transmission and storage facilities that are a major source of HAP emissions (§63.1270(a)). Subpart HHH does not apply to the Underwood Compressor Station as it is not a major source of HAP emissions. Further, the Underwood Compressor Station is prior to the gas transmission and storage phase.

III. Subpart EEEE – National Emission Standards for Hazardous Air Pollutants: Organic Liquids Distribution (Non-Gasoline)

<u>Applicability:</u> Subpart EEEE applies to organic liquids distribution operations that are located at major source of HAP emissions (§63.2334(a)). Subpart EEEE does not apply to the Underwood Compressor Station as it is not a major source of HAP emissions.

IV. Subpart YYYY – National Emission Standards for Hazardous Air Pollutants for Stationary Combustion Turbines

<u>Applicability:</u> Subpart YYYY applies to stationary combustion turbines located at major sources of HAP emissions (§63.6085(a)). Since the Underwood Compressor Station is not a major source of HAP emissions, Subpart YYYY does not apply.

V. Subpart ZZZZ - National Emission Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines

<u>Applicability:</u> Subpart ZZZZ applies to stationary RICE at a major or area source of HAP emissions (§63.6585). Subpart ZZZZ applies to the Underwood Compressor Station as the compressor engines are new RICE. The engines will meet Subpart ZZZZ by meeting 40 CFR Part 60, Subpart JJJJ as the Underwood Compressor Station is an area source of HAP emissions (§63.6590(c)(1)).

VI. Subpart DDDDD – National Emission Standards for Hazardous Air Pollutants for Industrial, Commercial, and Institutional Boilers and Process Heaters

<u>Applicability:</u> Subpart DDDDD applies to process heaters at a major source of HAP emissions (§63.7485). Subpart DDDDD does not apply to the Underwood Compressor Station as it is not a major source of HAP emissions.

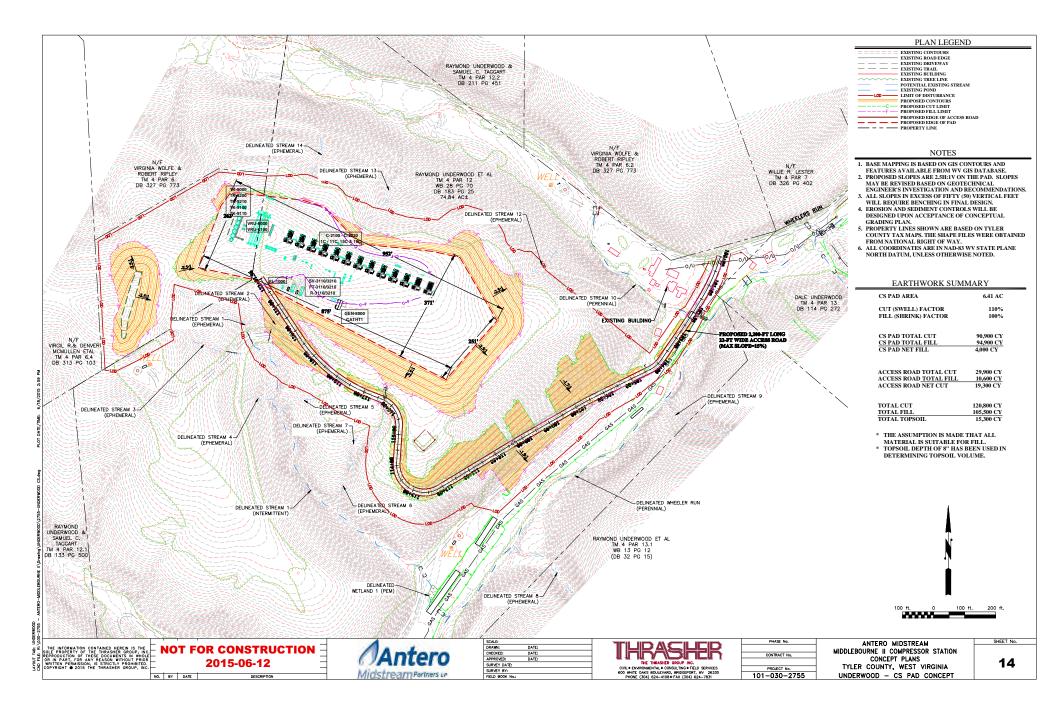
West Virginia State Regulations

Title 45 Legislative Rule – Division of Environmental Protection, Office of Air Quality

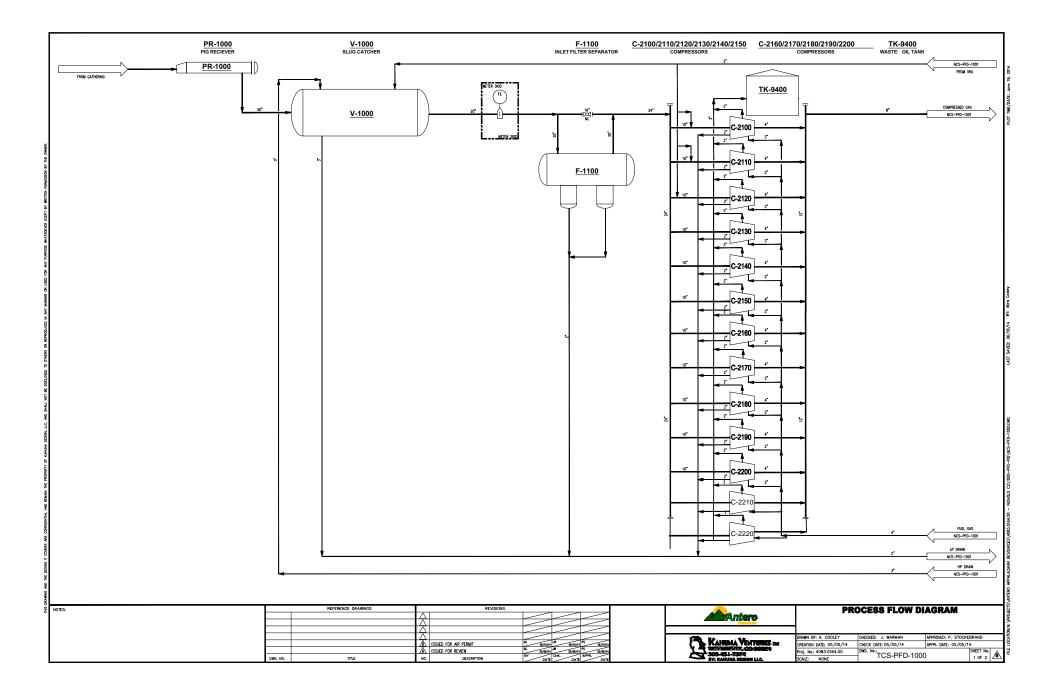
The following Title 45 Legislative Rules will be applicable to the Underwood Compressor Station:

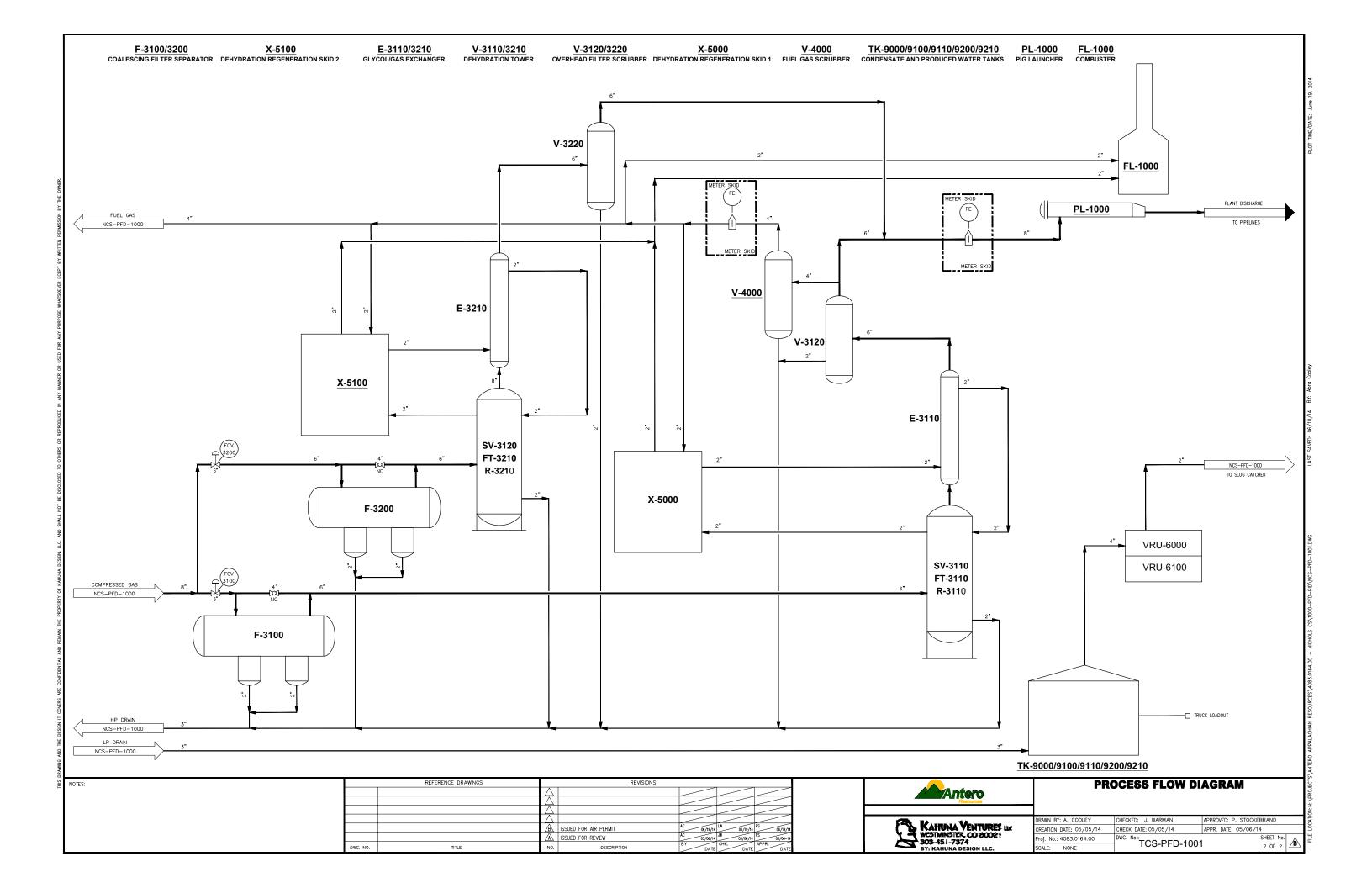
- I. 45CSR2 To Prevent and Control Particulate Air Pollution from Combustion of Fuel in Indirect Heat Exchangers
- II. 45CSR2A Testing, Monitoring, Recordkeeping and Reporting Requirements Under 45CSR2
- III. 45CSR4 To Prevent and Control the Discharge of Air Pollutants into the Open Air Which Causes or Contributes to an Objectionable Odor or Odors
- IV. 45CSR6 Control of Air Pollution from Combustion of Refuse
- V. 45CSR8 Ambient Air Quality Standards
- VI. 45CSR11 Prevention of Air Pollution Emergency Episodes
- VII. 45CSR13 Permits for Construction, Modification, Relocation and Operation of Stationary Sources of Air Pollutants, Notification Requirements, Administrative Updates, Temporary Permits, General Permits, and Procedures for Evaluation
- VIII. 45CSR16 Standards of Performance for New Stationary Sources Pursuant to 40 CFR, Part 60
- IX. 45CSR20 Good Engineering Practice as Applicable to Stack Heights
- X. 45CSR22 Air Quality Management Fee Program
- XI. 45CSR27 To Prevent and Control the Emissions of Toxic Air Pollutants
- XII. 45CSR33 Acid Rain Provisions and Permits
- XIII. 45CSR34 Emission Standards for Hazardous Air Pollutants for Source Categories Pursuant to 40 CFR, Part 63
- XIV. 45CSR38 Provisions for Determination of Compliance with Air Quality Management Rules
- XV. 45CSR42 Greenhouse Gas Emissions Inventory

Attachment E. Plot Plan



Attachment F. Process Flow Diagram





Attachment G. Process Description

Underwood Compressor Station – Process Description

The existing Underwood Compressor Station is located in Tyler County, West Virginia. Gas from surrounding pipelines enters the facility through one (1) receiver and associated slug catcher. From there, the gas is metered and routed through a filter separator. Any produced liquids from the scrubber or separator are sent to the 500 barrel settling tank (TK-9000). Gas from the filter separator is sent to one (1) of thirteen (13) 1680 hp compressor engines (C-2100 – C-2220). The thirteen (13) compressor engines are controlled with NSCR catalysts and airfuel ratio controllers (1C – 11C, 15C & 16C). Produced fluids are routed to the settling tank and high pressure gas is sent to one of the two (2) TEG dehydrators.

Each TEG dehydrator contains a flash gas tank (FT-3110 & FT-3210) and 1.5 MMBtu/hr reboiler (R-3110 & R-3210). Each dehydrator has a design rate of 88 MMscf/day. Within the dehydrator unit, vent gas from the flash gas tank (FT-3110 & FT-3210) is routed to the reboiler (R-3110 & R-3210) and used as fuel. In the case where the flash tank gas cannot be used by the reboiler due to excess gas or the reboiler being offline, the gas will be sent to the VRUs (VRU-6000 and VRU-6100) via the storage tanks (TK-9000 –TK-9210) and thus controlled by 98%. Combustion emissions from each reboiler are routed to the atmosphere. The dehydrator still vents (SV-3110 & SV-3210) are controlled by a flare with at least 98% control efficiency (FL-1000). Produced fluids from the dehydrator are routed to the settling tank. The dry gas from the dehydration process is either routed to a fuel gas scrubber, metered, and routed to the compressors as fuel gas or metered and sent to the high pressure facility discharge pipeline.

All produced fluids enter one (1) 500 barrel settling tank (TK-9000) where the fluids settle out as either condensate or produced water. The produced water goes to two (2) 400 barrel produced water tanks (TK-9200 – TK-9210) and the condensate goes to two (2) 400 barrel condensate tanks (TK-9100 – TK-9110). Flashing only occurs at the settling tank as the fluids stabilize in the settling tank before going to the other storage tanks. All five (5) tanks are connected to a primary vapor recovery unit (VRU-6000) where tank vapors are collected and recycled back into the gas system right before the initial filter scrubber. A second vapor recovery unit (VRU-6100) is used as back-up to the primary vapor recovery unit. The produced fluids are trucked out via tanker trucks as needed (LDOUT1). The loading emissions are uncontrolled. The anticipated production is 150 barrels per day of condensate and 45 barrels per day of produced water.

One (1) 600 kWe microturbine generator is used at the facility. The Capstone C600 unit is comprised of three (3) 200 kWe units that can be operated individually. Likely, all three units will not be operating 8,760 hours per year; however, emissions were calculated as such for maximum flexibility. The fuel line for the generators will be heated by a small catalytic heater (CATHT1) with a burner rating of 24 Btu/hr.

Fugitive emissions from component leaks and emissions from venting or blowdown events will also occur.

There will also be small storage tanks located at the facility. Their ID number, description, and exact size are listed in the table below.

Tag Number	Description	Gallons
TK-9300 & TK-9320	Compressor Skid Oily Water Tanks	1,000 each
TK-9310 & TK-9330	Used Oil Tank	500 each
TK-9410	TEG Make-Up Tank	1,000
TK-9420	Compressor Coolant Tank	2,000
TK-9430	Engine Lube Oil Tank	2,000
TK-9440	Compressor Lube Oil Tank	2,000
TK-9400	Compressor Waste Oil Tank	4,200

Attachment H. Material Safety Data Sheets

Material Safety Data Sheet (TRIETHYLENE GLYCOL (TEG))

JMN Specialties, Inc.

1100 Victory Drive Westwego, LA 70094 (504) 341-3749 ISO 9001 Registered HMIS HEALTH:.....2 HMIS FLAMMABILITY:.....1 HMIS REACTIVITY:.....0 PERSONAL PROTECTION:C

SECTION 1 – IDENTIFICATION OF CHEMICAL PRODUCT

PRODUCT NAME:TRIETHYLENE GLYCOL (TEG)**EFFECTIVE DATE:**October 1, 2007**CHEMICAL FAMILY:**Glycol**FORMULA:** $C_6H_{14}O_4$ **CAS NUMBER:**112-27-6

SECTION 2 – COMPOSITION / INFORMATION ON INGREDIENTS

HAZARDOUS INGREDIENT	PERCENT	CAS NUMBER	PEL
TRIETHYLENE GLYCOL	> 99	112-27-6	None Established by ACGIH
			or OSHA.

The criteria for listing components in the composition section are as follows: Carcinogens are listed when present at 0.1% or greater; components which are otherwise hazardous according to OSHA are listed when present at 1.0% or greater. Non-hazardous components may be listed at 3.0% or greater if not proprietary in nature. This is not intended to be complete compositional disclosure. Refer to section 14 for applicable states right to know and other regulatory information.

SECTION 3 – HAZARDS IDENTIFICATION

EMERGENCY OVERVIEW			
APPEARANCE / ODOR:	Clear Liquid / Mild Odor		
SHORT TERM EXPOSURE:	Inhalation: No adverse health effects expected from inhalation.		
	Ingestion: No adverse effects expected. Skin Contact: Prolonged		
	exposure may cause skin irritation. Eye Contact: Splashing in eye		
	causes irritation with transitory disturbances of corneal epithelium.		
	However, these effects diminish and no permanent injury is expected.		
	Vapors are non-irritating. Chronic Exposure: Possible skin irritation.		
	Aggravation of Pre-existing Conditions: No information found.		
OSHA REGULATED:	. No		
LISTED CARCINOGEN:	. NTP: No IARC MONOGRAPHS: No		

POTENTIAL HEALTH EFFECTS

INHALATION:	Unlikely
INGESTION:	Irritant
SKIN (DERMAL):	Slight Irritant After Prolonged Contact

OVER EXPOSURE EFFECTS: Inhalation: No adverse health effects expected from inhalation. Ingestion: No adverse effects expected. Skin Contact: Prolonged exposure may cause skin irritation. Eye Contact: Splashing in eye causes irritation with transitory disturbances of corneal epithelium. However, these effects diminish and no permanent injury is expected. Vapors are non-irritating. Chronic Exposure: Possible skin irritation. Aggravation of Pre-existing Conditions: No information found.

SECTION 4 – FIRST AID MEASURES

FIRST AID:	SKIN CONTACT: Remove contaminated clothing and shoes immediately. Wash affected area with soap or mild detergent and large amounts of water until no evidence of chemical remains (at least 15-20 minutes). Get medical attention immediately. EYE CONTACT: Flush eyes immediately with large amounts of water or normal saline solution, occasionally lifting upper and lower lids until no evidence of chemical remains (at least 15-20 minutes). Get medical attention immediately. INGESTION: Give large amounts of fresh water or milk immediately. Do not give anything by mouth if person is unconscious or otherwise unable to swallow. If vomiting occurs, keep head below hips to prevent aspiration. Treat symptomatically and supportively. Seek medical attention immediately. INHALATION: Remove from exposure area to fresh air immediately. If breathing has stopped, perform artificial resuscitation. Keep person warm and at rest. Treat symptomatically and supportively. Seek medical attention immediately. Qualified medical personnel should consider
NOTE TO PHYSICIAN:	administering oxygen. • Ethylene Glycol (EG) and diethylene glycol (DEG) intoxication may initially produce behavioral changes, drowsiness, vomiting, diarrhea, thirst, and convulsions. EG and DEG are nephrotoxic. End stages of poisoning may include renal damage or failure with acidosis. Supportive measures, supplemented with hemodialysis if indicated, may limit the progression and severity of toxic effects. Primary toxic effects of EG when swallowed are kidney damage and metabolic acidosis. This product may contain trace amounts of Ethylene Glycol (EG) or Diethylene Glycol (DEG).

SECTION 5 - FIRE FIGHTING MEASURES

FLASHPOINT:	.350°F
EXTINGUISHING MEDIA:	Water fog or spray, Foam, Dry Powder, Carbon Dioxide (CO ₂).
DECOMPOSITION	
PRODUCTS:	. From fire; Smoke, Carbon dioxide, & Carbon Monoxide
LOWER FLAME LIMIT:	. < 0.9
HIGHER FLAME LIMIT:	.>9
UNUSUAL FIRE AND	
EXPLOSION HAZARDS:	• Toxic levels of carbon monoxide, carbon dioxide, irritation aldehydes and ketones may be formed on burning. Heating in air may produce
	irritating aldehydes, acids, and ketones.
FIRE FIGHTING	inflating aldenytes, actos, and ketolies.

EOUIPMENT:	Fire fighters and others exposed to products of combustion should wear
-	self-contained breathing apparatus. Equipment should be thoroughly
	decontaminated after use.

SECTION 6 – ACCIDENTAL RELEASE MEASURES

CHEMTEL EMERGENCY NUMBER (24 Hour):	. 1-800-255-3924
SPILL:	. Ventilate area of leak or spill. Wear appropriate personal protective
	equipment as specified in Section 8. Isolate hazard area. Keep
	unnecessary and unprotected personnel from entering. Contain and
	recover liquid when possible. Collect liquid in an appropriate container
	or absorb with an inert material (e. g., vermiculite, dry sand, earth), and
	place in a chemical waste container. Do not use combustible materials,
	such as saw dust. Do not flush to sewer!
RCRA STATUS:	. None

SECTION 7 – HANDLING AND STORAGE

HANDLE IN ACCORDANCE WITH GOOD INDUSTRIAL HYGIENE AND SAFETY PRACTICES. THESE PRACTICES INCLUDE AVOIDING UNNECESSARY EXPOSURE AND PROMPT REMOVAL OF MATERIAL FROM EYES, SKIN, AND CLOTHING.

HANDLING AND STORAGE: .. No special storage requirements. Do not store above 120°F. PRECAUTIONARY

MEASURES: Provide fresh air ventilation during and after application. Close container after each use. Avoid prolonged or repeated contact with skin. Avoid contact with skin, eyes, and clothing. After handling this product, wash hands before eating, drinking, or smoking. If needed, take first aid action shown in Section 4.

SECTION 8 – EXPOSURE CONTROL / PERSONAL PROTECTION

GENERAL CONSIDERATIONS:

Consider the potential hazards of this material (see section 3), applicable exposure limits, job activities, and other substances in the work place when designing engineering controls and selecting personal protective equipment.

EYE PROTECTION:	• Chemical safety goggles meeting the specifications of OSHA 29CFR 1910.133 / ANSI Standard Z87.1 should be worn whenever there is the possibility of splashing or other contact with the eyes. Wear safety glasses meeting the specifications of OSHA 29CFR 1910.133 / ANSI Standard Z87.1 where no contact with the eye is anticipated.
RESPIRATORY PROTECTION:	• Not normally needed. Use NIOSH approved vapor respirator if exposure is unknown or exceeds permissible limits. A respiratory protection program that meets OSHA's 29 CFR 1910.134 or ANSI Z88.2 requirements must be followed whenever workplace conditions warrant respirator use.

Use NIOSH / MSHA approved respiratory protection equipment when airborne exposure limits are exceeded (see below). Consult the respirator manufacturer to determine appropriate type of

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A system of local and/or general exhaust is recommended to keep employee exposures below the Airborne Exposure Limits. Local exhaust ventilation is generally preferred because it can control the emissions of the contaminant at its source, preventing dispersion of it into the general work area. Please refer to the ACGIH document, *Industrial Ventilation, A Manual of Recommended Practices*, most recent edition, for details.

MECHANICAL EXHAUST: Desired in closed places LOCAL EXHAUST: Recommended

VENTILATION:

VENTILATION NOTES: Provide natural or mechanical ventilation to control exposure levels below Airborne exposure limits (see below). The use of local mechanical exhaust ventilation is preferred at sources of air contamination such as open process equipment. Consult NFPA Standard 91 for design of exhaust systems.

THRESHOLD LIMIT VALUE: None Established

PROTECTIVE EQUIPMENT:... HMIS PERSONAL PROTECTION: C: Safety Glasses, Gloves, Apron The user should read and understand all instructions and limitations supplied with the equipment since protection is usually provided for a limited time or under certain circumstances.

SECTION 9 - PHYSICAL AND CHEMICAL PROPERTIES

SECTION 10 – STABILITY AND REACTIVITY

STABILITY:StableHAZARDOUSWill Not OccurPOLYMERIZATION AVOID:Will Not OccurPOLYMERIZATION AVOID:Explosive decomposition may occur if combined with strong acids or
strong bases and subjected to elevated temperatures. Therefore, avoid
strong acids and strong bases at elevated temperatures. Avoid
contamination with strong oxidizing agentsand materials reactive with
hydroxyl compounds. Avoid burning or heating in air. This may
produce irritating aldehydes, acids, and ketones.CONDITIONS TO AVOID:Excessive heat. Will ignite in air at 700°F

SECTION 11 – TOXICOLOGICAL INFORMATION

EYE EFFECTS:

The eye irritation hazard is based on data from information supplied by raw material(s) supplier(s). **SKIN EFFECTS:**

The skin irritation hazard is based on data from information supplied by raw material(s) supplier(s). **ACUTE ORAL EFFECTS:**

The acute oral toxicity is based on data from information supplied by raw material(s) supplier(s). **ACUTE INHALATION EFFECTS:**

The acute respiratory toxicity is based on data from information supplied by raw material(s) supplier(s).

SECTION 12 – ECOLOGICAL INFORMATION

Data from laboratory studies and from scientific literature is noted below if available.

SECTION 13 DISPOSAL CONSIDERATIONS

WASTE DISPOSAL: Treatment, storage, transportation and disposal must be in accordance with Federal, State/Provincial and Local Regulations. Regulations may vary in different locations. Characterization and compliance with applicable laws are the responsibility solely of the generator. Whatever cannot be saved for recovery or recycling should be managed in an appropriate and approved waste disposal facility. Processing, use or contamination of this product may change the waste management options. State and local disposal regulations may differ from federal disposal regulations. Dispose of container and unused contents in accordance with federal, state and local requirements.

SECTION 14- TRANSPORTATION INFORMATION

The data provided in this section is for information only. The description shown may not apply to all shipping situations. Consult 49CFR, or appropriate regulations to properly classify your shipment for transportation.

SECTION 15 - REGULATORY INFORMATION

EPA CHRONIC: No EPA IGNITABILITY: No EPA REACTIVITY: No **EPA SUDDEN RELEASE** OF PRESSURE: No CERCLA RQ VALUE: None SARA TPO: None SARA RQ:..... None EPA HAZARD WASTE #:..... None CLEAN AIR: NA CLEAN WATER:..... NA SARA SECTION 313:..... No NFPA FLAMMABILITY:.....1 NFPA REACTIVITY:0 **DEA Chemical Trafficking Act:..** No TSCA STATUS: All ingredients in this product are on the TSCA Inventory List.

SECTION 16 - ADDITIONAL INFORMATION

FOOT NOTES: NA - NOT APPLICABLE ND - NO DATA AVAILABLE > = GREATER THAN < = LESS THAN

Prepared according to the OSHA Hazard Communication Standard (29 CFR 1910.1200) and the ANSI MSDS Standard (Z400.1) by the Company Health and Risk Assessment Unit, PO Box 1519, Gretna, LA 70054-1519.

REVISION STATEMENT: Changes have been made throughout this Material Safety Data Sheet. Please read the entire document.

DISCLAIMER:

Although the information and recommendations set forth herein (hereinafter "Information") are presented in good faith and believed to be correct as of the date hereof, the Company makes no representations as to the completeness or accuracy thereof. Information is supplied upon the condition that the persons receiving this MSDS will make their own determination as to its suitability for their intended purposes prior to use. Since the product is within the exclusive control of the user, it is the user's obligation to determine the conditions of safe use of this product. Such conditions should comply with all Federal Regulations concerning the Product. It must be recognized that the physical and chemical properties of any product may not be fully understood and that new, possibly hazardous products may arise from reactions between chemicals. The information given in this data sheet is based on our present knowledge and shall not constitute a guarantee for any specific product features and shall not establish a legally valid contractual relationship. NO REPRESENTATIONS OR WARRANTIES, EITHER EXPRESS OR IMPLIED. OF MERCHANTABILITY, FITNESS FOR A PARTICULAR PURPOSE OR OF ANY OTHER NATURE ARE MADE HEREUNDER WITH RESPECT TO INFORMATION OR THE PRODUCT TO WHICH INFORMATION REFERS.



Material Name: Produced Water

US GHS

SYNONYMS: Produced Brine Water, Brine, Brine Water, Formation Water

* * * Section 1 – PRODUCT AND COMPANY IDENTIFICATION * * *

PRODUCT NAME:	Produced Water	EMERGENCY PHONE:	(800) 878-1373
PRODUCT CODES:	Mixture	AFTER HOURS:	(800) 878-1373
ADDRESS: 16	ntero Resources 15 Wynkoop Street enver, Colorado 80202	CHEMTREC PHONE:	(800) 424-9300

* * * Section 2 – HAZARDS IDENTIFICATION * * *

GHS Classification:

Eye Irritant – Category 2A.

GHS LABEL ELEMENTS Symbol(s)



Signal Word Warning

Hazard Statements

Causes serious eye irritation

Precautionary Statements

Prevention

Wear protective gloves/protective clothing/eye protection/face protection.

Response

If on SKIN (or hair): Rinse skin with water / shower. Remove / Take off all contaminated clothing immediately.

Material Name: Produced Water

If in EYES: Rinse cautiously with water for at least fifteen (15) minutes. Remove Contact Lenses, if present and easy to do. Continue rinsing.

If EYE irritation persists, get medical advice / attention.

Storage

Store in a secure area.

Disposal

Dispose of contents/containers in accordance with regulations.

* * * Section 3 – COMPOSITION / INFORMATION ON INGREDIENTS * * *

CAS #	Component	Percent
7732-18-5	Water	80
7647-14-5	Sodium Chloride	20

Because brine water is a natural product, composition can vary greatly.

* * * Section 4 – FIRST AID MEASURES * * *

First Aid: Eyes

Flush eyes with clean running water for at least fifteen (15) minutes. If irritation or redness develops from exposure, following flushing, seek medical attention.

First Aid: Skin

First aid is not required, normally. However, it is a good practice to wash any chemical from the skin.

First Aid: Ingestion (Swallowing)

First aid is not required, normally. If spontaneous vomiting occurs, lean the victim forward to reduce the risk of aspiration. Monitor for breathing difficulties. If symptoms develop, seek medical attention.

First Aid: Inhalation (Breathing)

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

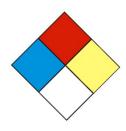
Material Name: Produced Water

US GHS

Most important symptoms and effects

None known or anticipated.

* * * Section 5 – FIRE FIGHTING MEASURES * * *



NFPA 704 Hazard Class

Health: 1 Flammability: 0 Instability: 0 (0=Minimal, 1=Slight, 2=Moderate, 3=Serious, 4=Severe)

General Fire Hazards

No fire hazards are expected.

General Fire Hazards

No unusual fire or explosion hazards are expected. If container is not properly cooled, it can rupture in the heat of a fire.

Extinguishing Media

The material is non-flammable. Use extinguishing agent suitable for the type of surrounding fire.

Unsuitable Extinguishing Media

None

Fire Fighting Equipment / Instructions

Small fires in the beginning stage may typically be extinguished using handheld portable fire extinguishers and other firefighting equipment. Isolate area around container involved in fire and keep unauthorized personnel out. Stop spill/release if it can be done safely. Move undamaged containers from the immediate hazard area if it can be done safely. Cool equipment exposed to fire with water, if it can be done safely.

Hazardous Combustion Products

None Anticipated. See Section 9 for Flammable Properties including Flash Point and Flammable (Explosive) Limits

Material Name: Produced Water

* * * Section 6 – ACCIDENTAL RELEASE MEASURES * * *

Recovery and Neutralization

Contain and stop the source of the spill, if safe to do so.

Materials and Methods for Clean-Up

Notify relevant authorities in accordance with all applicable regulations. Immediate cleanup of any spill is recommended. Dike far ahead of spill for later recovery or disposal. Absorb spill with inert material such as sand or vermiculite, and place in suitable container for disposal. If spilled on water remove with appropriate methods (e.g. skimming, booms or absorbents). In case of soil contamination, remove contaminated soil for remediation or disposal, in accordance with local regulations.

Recommended measures are based on the most likely spillage scenarios of this material. However, local conditions and regulations may influence or limit the choice of appropriate actions to be taken. See Section 13 for information on appropriate disposal.

Emergency Measures

The material is not considered hazardous. Nevertheless, evacuate nonessential personnel and secure the area. Stay upwind and uphill, if possible.

Personal Precautions and Protective Equipment

Stay upwind and away from the spill/release. Avoid direct contact with the material. For large spillages, notify persons downstream of the spill/release. Isolate the immediate hazard area and keep unauthorized personnel out. Response and clean-up crews must be properly trained and must utilize proper protective equipment (see Section 8).

Environmental Precautions

Protect bodies of water by diking or absorbents, if possible. Do not flush down sewer or drainage systems. Use water sparingly to minimize environmental contamination and reduce disposal requirements. If a spill occurs on water, notify appropriate authorities and advise shipping of any hazard.

Prevention of Secondary Hazards

None

Material Name: Produced Water

* * * Section 7 – HANDLING AND STORAGE * * *

Handling Procedures

Wash thoroughly after handling. Use good personal hygiene practices and wear appropriate personal protective equipment (see section 8).

Do not enter confined spaces such as tanks or pits without following proper entry procedures such as ASTM D-4276 and 29 CFR 1910.146. Do not wear contaminated clothing or shoes.

Storage Procedures

Keep container(s) tightly closed and properly labeled. Use and store this material in cool, dry, well ventilated areas. Store only in approved containers. Keep away from any incompatible material (see Section 10). Protect container(s) against physical damage.

Incompatibilities

Keep away from excessive heat to prevent rupture of container.

* * * Section 8 – EXPOSURE CONTROLS / PERSONAL PROTECTION * * *

Component Exposure Limits

Water (7732-18-5) ACGIH: Not listed

Sodium Chloride (7647-14-5)

ACGIH: Not listed

Engineering Measures

If current ventilation practices are not adequate to maintain airborne concentrations below the established exposure limits, additional engineering controls may be required.

Personal Protective Equipment: Respiratory

Emergencies or conditions that could result in significant airborne exposures may require the use of NIOSH approved respiratory protection. An industrial hygienist or other appropriate health and safety professional should be consulted for specific guidance under these situations.

A respiratory protection program that meets or is equivalent to OSHA 29 CFR

Material Name: Produced Water

1910.134 and ANSI Z88.2 should be followed whenever workplace conditions warrant a respirator's use.

Personal Protective Equipment: Skin and Hands

The use of skin protection is not normally required; however, good industrial hygiene practice suggests the use of gloves or other appropriate skin protection whenever working with chemicals.

Personal Protective Equipment: Eyes

Safety glasses or goggles that meet or exceed ANSI Z-87.1 are recommended where there is a possibility of splashing or spraying.

Hygiene Measures

Emergency eye wash capability should be available in the near proximity to operations presenting a potential splash exposure. Use good personal hygiene practices. Avoid repeated and/or prolonged skin exposure. Wash hands before eating, drinking, smoking, or using toilet facilities. Promptly remove contaminated clothing and launder before reuse.

* * * Section 9 – PHYSICAL AND CHEMICAL PROPERTIES * * *			
Appearance:	Clear to Brown	Odor:	Salty
Physical State:	Liquid	pH:	ND
Vapor Pressure:	< 0.36 psia @ 70°F / 21.1°C	Vapor Density:	> 1
Boiling Point:	212°F / 100°C	Melting Point:	2.4°F / -16.5°C
Solubility (H2O):	Complete	Specific Gravity:	1.1 @ 68°F / 20°C
Evaporation Rate:	Variable	VOC:	ND
Octanol / H2O Coeff.:	ND	Flash Point:	ND
Flash Point Method:	ND		
Lower Flammability Limit:	ND	Upper Flammability Limit:	ND
(LFL):		(UFL):	
Auto Ignition:	ND	Burning Rate:	ND

Material Name: Produced Water

*** Section 10 – CHEMICAL STABILITY & REACTIVITY INFORMATION ***

Chemical Stability

This is a stable material.

Hazardous Reaction Potential

Will react with alkali and alkaline metals to form flammable hydrogen gas.

Conditions to Avoid

Avoid contact with alkali metals (lithium, sodium, potassium), alkaline metals (beryllium, magnesium, calcium, strontium, and barium), and metallic hydrides like lithium aluminum hydride.

Hazardous Decomposition Products

Not anticipated under normal conditions of use.

Hazardous Polymerization

Not known to occur.

*** Section 11 - TOXICOLOGICAL INFORMATION ***

Acute Toxicity

A: General Product Information

Unlikely to be harmful.

B. Component Analysis – D50/LC50

Water (7732-18-5) Oral LD50 Rat 90 g/kg

Sodium Chloride (7647-14-5)

Oral LD50 Rat 3 g/kg

Potential Health Effects: Skin Corrosion Property / Stimulativeness

May cause skin irritation with prolonged or repeated contact. Not expected to be a skin sensitizer.

Potential Health Effects: Eye Critical Damage / Stimulativeness

Contact with eyes may cause moderate irritation.

Material Name: Produced Water

Potential Health Effects: Ingestion

Ingestion may result in nausea, vomiting, diarrhea, abdominal cramps, and dehydration (thirst).

Potential Health Effects: Inhalation

No information available on the mixture. However, none of the components have been classified for respiratory sensitization (or are below the concentration threshold for classification).

Generative Cell Mutagenicity

Not expected to cause genetic effects.

Carcinogenicity

General Product Information

Not expected to cause cancer. This substance is not listed as a carcinogen by IARC, NTP or OSHA.

Reproductive Toxicity

This product is not reported to have any reproductive toxicity effects.

Specified Target Organ General Toxicity: Single Exposure

This product is not reported to have any specific target organ general toxicity single exposure effects.

Specified Target Organ General Toxicity: Repeated Exposure

This product is not reported to have any specific target organ general toxicity multiple exposure effects.

Aspiration Respiratory Organs Hazard

The major health threat of ingestion occurs from the danger of aspiration (breathing) of liquid drops into the lungs, particularly from vomiting. Aspiration may result in chemical pneumonia (fluid in the lungs), severe lung damage, respiratory failure and even death.

* * * Section 12 - ECOLOGICAL INFORMATION * * *

Ecotoxicity

A: General Product Information

Keep out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

Material Name: Produced Water

US GHS

Persistence / Degradability

No information available

Bioaccumulation

No information available

Mobility in Soil

No information available

* * * Section 13 – DISPOSAL CONSIDERATIONS * * *

Waste Disposal Instructions

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

Disposal of Contaminated Containers or Packaging

Recover or recycle if possible. It is the responsibility of the generator to determine the toxicity and physical properties of the material generated so as to properly classify the waste and ensure disposal methods comply with applicable regulations.

This material, if discarded as produced, is not a RCRA "listed" hazardous waste, and is not believed to exhibit characteristics of hazardous waste. Consult state and local regulations regarding the proper disposal of this material. Do not dispose of brine water by draining onto the ground. This will result in soil and groundwater contamination. Waste arising from spillage or tank cleaning should be disposed of in accordance with applicable regulations.

Container contents should be completely used and containers should be emptied prior to discard. Container rinsate should not be considered a RCRA hazardous waste but must be disposed of with care and in full compliance with federal, state and local regulations. Larger empty containers, such as drums, should be returned to the distributor or to a qualified drum reconditioner. To assure proper disposal of smaller empty containers, consult with state and local regulations and disposal authorities.

* * * Section 14 – TRANSPORTATION INFORMATION * * *

DOT Information Shipping Description: Not Regulated UN #: Not Regulated

Material Name: Produced Water

*** Section 15 – REGULATORY INFORMATION ***

CERCLA/SARA – Section 302 Extremely Hazardous Substances and TPQs (in pounds):

This material does not contain any chemicals subject to the reporting requirements of SARA 302 and 40 CFR 372,

CERCLA/SARA – Section 313 and 40 CFR 372):

This material does not contain any chemicals subject to the reporting requirements of SARA 313 and 40 CFR 372.

EPA (CERCLA) Reportable Quantity (in pounds):

This material does not contain any chemicals with CERCLA Reportable Quantities.

State Regulations

Component Analysis

The following components appear on one or more of the following state hazardous substances list.

California Proposition 65:

This material does not contain any chemicals that are known to the State of California to cause cancer, birth defects or other reproductive harm at concentrations that trigger the warning requirements of California Proposition 65.

National Chemical Inventories:

All components are either listed on the US TSCA Inventory, or are not regulated under TSCA.

U.S. Export control classification Number: EAR99.

* * * Section 16 – OTHER INFORMATION * * *

NFPA® Hazard Rating

	Health Fire Reactivit	0	
HMIS® Hazard Rating	Fire	0	Slight Minimal Minimal

Material Name: Produced Water

Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act: ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

Literature References

None

Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: January 28, 2014

Date of Last Revision: March 4, 2014

End of Sheet



Material Name: Natural Gas Condensate

US GHS

SYNONYMS: Drips; Condensate; Field Condensate; Gas Well Condensate; High Pressure Inlet Liquids; Lease Condensate; Natural Gas Liquids; Pipeline Liquids

* * * Section 1 – PRODUCT AND COMPANY IDENTIFICATION * * *

PRODUCT NAM		EMERGENCY PHONE: AFTER HOURS:	(800) 878-1373 (800) 878-1373
ADDRESS:	Antero Resources 1615 Wynkoop Street Denver, Colorado 80202	CHEMTREC PHONE:	(800) 424-9300

* * * Section 2 – HAZARDS IDENTIFICATION * * *

GHS Classification:

Flammable Liquids – Category 2. Acute Toxicity Inhalation – Category 3 Germ Cell Mutagenicity – Category 1B Carcinogenicity – Category 1A Specific Target Organ Systemic Toxicity (STOT) – Single Exposure Category 3 Specific Target Organ Systemic Toxicity (STOT) – Repeat Exposure Category 1 Aspiration Toxicity – Category 1 Toxic to the Aquatic Environment Acute – Category 3

GHS LABEL ELEMENTS



Signal Word Danger

Material Name: Natural Gas Condensate

US GHS

Hazard Statements

Highly flammable liquid and vapor.
Toxic if inhaled.
May cause genetic defects.
May cause cancer.
May cause respiratory irritation.
May cause drowsiness or dizziness.
May cause damage to organs (liver, kidneys, blood, nervous system, and skin) through prolonged or repeated exposure.
May be fatal if swallowed and enters airways.
Harmful to aquatic life.

Precautionary Statements

Prevention

Keep away from heat/sparks/open flames/hot surfaces. No smoking. Keep container tightly closed.

Ground/bond container and receiving equipment.

Use explosion-proof electrical/ventilating/lighting equipment.

Use only non-sparking tools.

Take precautionary measures against static discharge.

Wear protective gloves/protective clothing/eye protection/face protection.

Do not breathe gas/mist/vapors/spray.

Do not handle until all safety precautions have been read and understood. Wash thoroughly after handling.

Do not eat, drink or smoke when using this product.

Use only outdoors or in a well-ventilated area.

Avoid release to the environment.

Response

If on SKIN (or hair): Wash with plenty of soap and water. Remove / Take off all contaminated clothing immediately. Rinse skin with water/shower.

If INHALED: Remove victim to fresh air and keep comfortable for breathing. Call a poison center/doctor if the victim feels unwell.

If SWALLOWED: Immediately call a poison center or doctor / physician. Do not Induce vomiting.

If exposed or concerned: Get medical advice/attention.

In case of fire: Use water spray, fog or fire-fighting foam.

Storage

Store in a well-ventilated place. Keep cool. Store in a secure area.

Material Name: Natural Gas Condensate

Disposal

Dispose of contents/containers in accordance with local/regional/national/international regulations.

CAS #	Component	Percent
111-65-9	Octanes	25 - 95
142-82-5	Heptanes	25 - 95
110-54-3	Hexanes as n-Hexane	25 - 95
109-66-0	Pentanes as n-Pentane	5 - 70
106-97-8	N-butane	0 - 45
74-98-6	Propane	0 - 15
78-84-0	Ethane	0 - 5
71-43-2	Benzene	< 1
108-88-3	Toluene	< 1
1330-20-7	m-,o-,p-Xylene	< 1

Because natural gas condensate is a natural product, composition can vary greatly.

* * * Section 4 – FIRST AID MEASURES * * *

First Aid: Eyes

Flush eyes with clean running water for at least fifteen (15) minutes. Following flushing, seek medical attention.

First Aid: Skin

Remove contaminated clothing. Wash contaminated areas thoroughly with soap and water or waterless hand cleanser. Obtain medical attention if irritation or redness develops. Wash contaminated clothing before reuse.

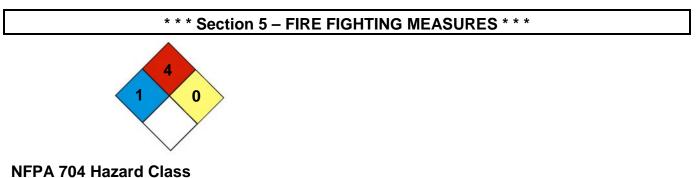
First Aid: Ingestion (swallowing)

DO NOT INDUCE VOMITING. Do not give liquids. Obtain immediate medical attention. If spontaneous vomiting occurs, lean the victim forward to reduce the risk of aspiration. Monitor for breathing difficulties. Small amounts of material which enter the mouth should be rinsed out until the taste is dissipated.

Material Name: Natural Gas Condensate

First Aid: Inhalation (breathing)

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.



Health: 1 Flammability: 4 Instability: 0 (0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

General Fire Hazards

See Section 9 for Flammability Properties.

Extremely flammable. Vapors may be ignited rapidly when exposed to heat, spark, open flame, or other source of ignition (e.g., static electricity, pilot lights, mechanical / electrical equipment, and electronic devices such as cell phones, computers, calculators, and pagers which have not been certified as intrinsically safe). Flammable vapors can burn in the open or explode in confined spaces. Vapors are heavier than air, and may travel distances to an ignition source and flash back. Runoff to sewer systems may cause fire or explosion.

Hazardous Combustion Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

Extinguishing Media

SMALL FIRES: Any extinguisher suitable for Class B fires, dry chemical, firefighting foam, water spray, carbon dioxide (CO_2), or other gaseous extinguishing agents. Use caution when applying CO2 in confined spaces.

LARGE FIRES: Water spray, fog or fire-fighting foam. Water may be ineffective for fighting the fire, but may be used to cool fire-exposed containers.

Unsuitable Extinguishing Media

None

Material Name: Natural Gas Condensate

US GHS

Fire Fighting Equipment / Instructions

Small fires in the beginning stage may typically be extinguished using handheld portable fire extinguishers and other firefighting equipment. Isolate area around container involved in fire. Cool tanks, shells, and containers exposed to fire and excessive heat with water. For massive fires the use of unmanned hose holders or monitor nozzles may be advantageous to minimize personnel exposure. Major fires may require withdrawal, allowing the tank to burn. Large storage tank fires typically require specially trained personnel and equipment to extinguish the fire, often including the need for properly applied firefighting foam.

Firefighting activities that may result in potential exposure to high heat, smoke or toxic by-products of combustion should require NIOSH/MSHA- approved pressure-demand self-contained breathing apparatus with full face piece and full protective clothing.

* * * Section 6 – ACCIDENTAL RELEASE MEASURES * * *

Recovery and Neutralization

Contain and stop the source of the spill, if safe to do so.

Materials and Methods for Clean-Up

Notify relevant authorities in accordance with all applicable regulations. Immediate cleanup of any spill is recommended. Dike far ahead of spill for later recovery or disposal. Absorb spill with inert material such as sand or vermiculite, and place in suitable container for disposal. If spilled on water remove with appropriate methods (e.g. skimming, booms or absorbents). In case of soil contamination, remove contaminated soil for remediation or disposal, in accordance with local regulations.

Recommended measures are based on the most likely spillage scenarios for this material; however local conditions and regulations may influence or limit the choice of appropriate actions to be taken.

Emergency Measures

Evacuate nonessential personnel and secure all ignition sources. No road flares, smoking or flames in hazard area. Consider wind direction. Stay upwind and uphill, if possible. Vapor cloud may be white, but color will dissipate as cloud disperses. Fire and explosion hazard is still present.

Personal Precautions and Protective Equipment

Response and clean-up crews must be properly trained and must utilize proper protective equipment (see Section 8). Extremely flammable. Spillages of liquid product will create a fire hazard and may form an explosive atmosphere. Keep all sources of

Page 5 of 17

Material Name: Natural Gas Condensate

ignition and hot metal surfaces away from spill/release if safe to do so.

The use of explosion-proof electrical equipment is recommended. Stay upwind and away from spill/release. Avoid direct contact with material. For large spillages, notify persons downwind of the spill/release, isolate immediate hazard area and keep unauthorized personnel out. Wear appropriate protective equipment, including respiratory protection, as conditions warrant (see Section 8). See Sections 2 and 7 for additional information on hazards and precautionary measures.

Environmental Precautions

Protect bodies of water by diking, absorbents, or absorbent boom, if possible. Do not flush down sewer or drainage systems, unless system is designed and permitted to handle such material. The use of firefighting foam may be useful in certain situations to reduce vapors. If spill occurs on water notify appropriate authorities and advise shipping of any hazard. Spills into or upon navigable waters, the contiguous zone, or adjoining shorelines that cause a sheen or discoloration on the surface of the water, may require notification of the National Response Center (phone number 800-424-8802).

Prevention of Secondary Hazards

None

* * * Section 7 – HANDLING AND STORAGE * * *

Handling Procedures

Keep away from flame, sparks and excessive temperatures. Bond and ground containers. Use non-sparking tools. Use only outdoors or in well ventilated areas. Wear protective gloves / clothing and eye / face protection. Wash thoroughly after handling. Use good personal hygiene practices and wear appropriate personal protective equipment (see section 8).

Storage Procedures

Store only in approved containers. Bond and ground containers. Keep away from flame, sparks, excessive temperatures and open flames. Keep containers closed and clearly labeled. Empty product containers or vessels may contain explosive vapors. Do not pressurize, cut, heat, weld or expose containers to sources of ignition.

Store in a well-ventilated area. This storage area should comply with NFPA 30 "Flammable and Combustible Liquid Code". Avoid storage near incompatible materials. The cleaning of tanks previously containing this product should follow API Recommended Practice (RP) 2013 "Cleaning Mobile Tanks In Flammable and Combustible Liquid Service" and API RP 2015 "Cleaning Petroleum Storage Tanks."

Material Name: Natural Gas Condensate

Incompatibilities

Keep away from strong oxidizers, ignition sources and heat.

* * * Section 8 – EXPOSURE CONTROLS / PERSONAL PROTECTION * * *

Component Exposure Limits

Octanes (111-65-9)

ACGIH: 300 ppm TWA (listed under Octane, all isomers)

Heptanes (142-82-5)

ACGIH: 400 ppm TWA (listed under n-Heptane)

n-Hexane (110-54-3)

ACGIH: 20 ppm TWA (listed under n-Hexane)

n-Pentane (109-66-0)

ACGIH: 600 ppm TWA (listed under Pentane, all isomers)

n-Butane (106-97-8)

ACGIH: 600 ppm TWA (listed under n-Butane)

Propane (74-98-6)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases C1-C4)

Ethane (74-84-0)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases C1-C4)

Benzene (71-43-2)

ACGIH: 0.5 ppm (TWA); NIOSH: 0.1 ppm (TWA); OSHA 1 ppm (TWA)

Toluene (108-88-3)

ACGIH: 20 ppm TWA (listed under Toluene)

m-, o-, p-Xylene (1330-20-7)

ACGIH: 100 ppm TWA (listed under Xylene o, m & p isomers)

Material Name: Natural Gas Condensate

Engineering Measures

Use adequate ventilation to keep vapor concentrations of this product below occupational exposure and flammability limits, particularly in confined spaces. Use explosion-proof equipment and lighting in classified / controlled areas.

Personal Protective Equipment: Respiratory

Use a NIOSH-approved positive-pressure, supplied air respirator with escape bottle or self-contained breathing apparatus (SCBA) for gas concentrations above occupational exposure limits, for potential for uncontrolled release, if exposure levels are not known, or in an oxygen-deficient atmosphere (oxygen content less than 19.5 percent). A respiratory program that meets or is equivalent to OSHA 29 CFR 1910.134 and ANSI Z88.2 should be followed whenever workplace conditions warrant the use of a respirator.

If benzene concentrations equal or exceed applicable exposure limits, OSHA requirements for personal protective equipment, exposure monitoring, and training may apply (29 CFR 1910.1028 – Benzene).

CAUTION: Flammability limits (i.e., explosion hazard should be considered when assessing the need to expose personnel to concentrations requiring respiratory protection.

Personal Protective Equipment: Hands

Gloves constructed of nitrile or neoprene are recommended.

Personal Protective Equipment: Eyes

Safety glasses or goggles are recommended where there is a possibility of splashing or spraying. Eye protection that meets or exceeds ANSI Z.87.1 is recommended. Depending on conditions of use, a face shield may be necessary.

Personal Protective Equipment: Skin and Body

Chemical protective clothing such as of E.I. DuPont TyChem®, Saranex® or equivalent recommended based on degree of exposure. Note: The resistance of specific material may vary from product to product as well as with degree of exposure. Consult manufacturer specifications for further information.

Hygiene Measures

Emergency eye wash capability should be available in the near proximity to operations presenting a potential splash exposure. Use good personal hygiene practices. Avoid repeated and/or prolonged skin exposure. Wash hands before eating, drinking, smoking, or using toilet facilities. Do not use as a cleaning solvent on the skin. Do not use gasoline or solvents (naphtha, kerosene, etc.) for washing this product from

Material Name: Natural Gas Condensate

* * * Section 9 – PHYSICAL AND CHEMICAL PROPERTIES * * *

Appearance: Physical State: Vapor Pressure:	Colorless to straw yellow Liquid 110 – 200 psia (Reid VP) @ 100°F/37.8°C	Odor: pH: Vapor Density (air = 1):	Aromatic, Gasoline; ND > 1
Boiling Point:	Approx. 85 - 437°F (39 – 200°C)	Melting Point:	ND
Solubility (H2O):	Insoluble to slightly soluble	Specific Gravity:	AP 0.62-0.76 (varies)
Evaporation Rate:	High	VOC:	ND
Octanol / H2O Coeff.:	ND	Flash Point:	-40°F -40°C
Flash Point Method:	Tag Closed Cup (TCC)		
Lower Flammability Limit: (LFL):	ND (NFPA Gasoline 1.4)	Upper Flammability Limit: (UFL):	ND (NFPA Gasoline 7.6)
Auto Ignition:	AP 480°F (250°C)	Burning Rate:	ND

* * * Section 10 - CHEMICAL STABILITY & REACTIVITY INFORMATION * * *

Chemical Stability

This is a stable material.

Hazardous Reaction Potential

Will not occur.

Conditions to Avoid

Keep away from ignition sources and high temperatures.

Hazardous Decomposition Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

Material Name: Natural Gas Condensate

US GHS

*** Section 11 – TOXICOLOGICAL INFORMATION ***

Acute Toxicity

- A: General Product Information Harmful if swallowed.
- B. Component Analysis LD50/LC50 Octanes (111-65-9) Inhalation LC50 rat = 118,000 mg/m3 / 4H

Heptanes (142-82-5) Inhalation LC50 rat = 103,000 mg/m3 / 4H

Hexanes as n-Hexane (110-53-3) Inhalation LC50 rat = 48,000 ppm / 4H

Pentanes as n-Pentane (109-66-0)

Inhalation LC50 rat = 364,000 mg/m3 / 4H

Butanes as n-Butane (106-97-8)

Inhalation LC50 rat 658,000 mg/l / 4H

Propane (74-98-6) Inhalation LC50 Rat > 800,000 ppm / 0.25H

Ethane (74-84-0) Inhalation LC50 Rat 658,000 mg/l / 4H

Benzene (71-43-2) Inhalation LC50 Rat 44,700 mg/m3 /

Toluene (108-88-3) Inhalation LD50 Rat 12/5 mg/l / 4H

m-, o-, p-Xylene (1330-20-7) Inhalation LC50 Rat 5000 ppm / 4H

Potential Health Effects: Skin Corrosion Property / Stimulativeness

May cause skin irritation with prolonged or repeated contact. Liquid may be absorbed through the skin in toxic amounts if large areas of skin are exposed repeatedly.

Material Name: Natural Gas Condensate

Potential Health Effects: Eye Critical Damage / Stimulativeness

Contact with eyes may cause moderate irritation.

Potential Health Effects: Ingestion (swallowing)

Ingestion may cause gastrointestinal disturbances, including irritation, nausea, vomiting and diarrhea, and central nervous system (brain) effects similar to alcohol intoxication. In severe cases, tremors, convulsions, loss of consciousness, coma, respiratory arrest, and death may occur.

Potential Health Effects: Inhalation (breathing)

Excessive exposure may cause irritations to the nose, throat, lungs and respiratory tract. Central nervous system (brain) effects may include headache, dizziness, loss of balance and coordination, unconsciousness, coma, respiratory failure, and death.

Respiratory Organs Sensitization / Skin Sensitization

This product is not reported to have any skin sensitization effects.

Generative Cell Mutagenicity

May cause genetic defects. Some crude oils and crude oil fractions have been positive in mutagenicity studies.

Carcinogenicity

A: General Product Information

May cause cancer.

This product contains benzene, although at very low concentrations. Human health studies indicate that prolonged and/or repeated overexposure to benzene may cause damage to the blood-forming system (particularly bone marrow), and serious blood disorders such as aplastic anemia and leukemia. Benzene is listed as a human carcinogen by the NTP, IARC, OSHA and ACGIH.

Exposure to light hydrocarbons in the same boiling range as this product have been associated in animal studies with effects to the central nervous system, peripheral nervous system, liver, and kidneys. The significance of these animal models to predict similar human response is uncertain. Observing good work practices and personal hygiene procedures (Sections 7 and 8) can minimize potential risks to humans.

B: Component Carcinogenicity

Benzene (71-43-2)

ACGIH:	A1 - Confirmed Human Carcinogen
OSHA:	5 ppm STEL (Cancer hazard, Flammable, See 29 CFR 1910.1028,
	15 min); 0.5 ppm Action Level; 1 ppm TWA
NIOSH:	potential occupational carcinogen
NTP:	Known Human Carcinogen (Select Carcinogen)
• · -	

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Material Name: Natural Gas Condensate

US GHS

IARC: Monograph 100F [in preparation]; Supplement 7 [1987]; Monograph 29 [1982] (Group 1 (carcinogenic to humans))

Reproductive Toxicity

This product is not reported to have any reproductive toxicity effects.

Specified Target Organ General Toxicity: Single Exposure

This product is not reported to have any specific target organ general toxicity single exposure effects.

Specified Target Organ General Toxicity: Repeated Exposure

May cause damage to organs (liver, kidneys, blood, nervous system and skin) through prolonged or repeated exposure.

Aspiration Respiratory Organs Hazard

The major health threat of ingestion occurs from the danger of aspiration (breathing) of liquid drops into the lungs, particularly from vomiting. Aspiration may result in chemical pneumonia (fluid in the lungs), severe lung damage, respiratory failure and even death.

* * * Section 12 - ECOLOGICAL INFORMATION * * *

Ecotoxicity

A: General Product Information

Keep out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

B: Component Analysis – Ecotoxicity – Aquatic Toxicity Benzene (71-43-2)

Test and Species Conditions 96 Hr LC50 Pimephales promelas 10.7-14.7 mg/L [flow-through] 96 Hr LC50 Oncorhynchus mykiss 5.3 mg/L [flow-through] 96 Hr LC50 Lepomis macrochirus 22.49 mg/L [static] 96 Hr LC50 Poecilia reticulata 28.6 mg/L [static] 22330-41160 µg/L [static] 96 Hr LC50 Pimephales promelas 70000-142000 µg/L [static] 96 Hr LC50 Lepomis macrochirus 72 Hr EC50 Pseudokirchneriella subcapitata 29 mg/L 8.76 - 15.6 mg/L [static] 48 Hr EC50 Daphnia magna 48 Hr EC50 Daphnia magna 10 mg/L

Conditions

119 mg/L [static]

82 mg/L [static]

56 mg/L

170 mg/L

Material Name: Natural Gas Condensate

Natural Gas condensates (68919-39-1)

Test and Species

96 Hr LC50 Alburnus alburnus
96 Hr LC50 Cyprinodon variegatus
72 Hr EC50 Pseudokirchneriella subcapitata
24 Hr EC50 Daphnia magna

Persistence / Degradability

No information available

Bioaccumulation

No information available

Mobility in Soil

No information available

* * * Section 13 - DISPOSAL CONSIDERATIONS * * *

Waste Disposal Instructions

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

Disposal of Contaminated Containers or Packaging

Recover or recycle if possible. It is the responsibility of the generator to determine the toxicity and physical properties of the material generated so as to properly classify the waste and ensure disposal methods comply with applicable regulations. This material, if discarded should be fully characterized for ignitability (D001), reactivity (D003) and benzene (D018) prior to disposal (40 CFR261). Use which results in chemical or physical change or contamination may subject it to regulation as a hazardous waste. Along with properly characterizing all waste materials, consult state and local regulations regarding the proper disposal of this material. Do not dispose of by draining onto the ground. This will result in soil and groundwater contamination. Waste arising from spillage or tank cleaning should be disposed of in accordance with applicable regulations.

Container contents should be completely used and containers should be emptied prior to discard. Container rinsate could be considered a RCRA hazardous waste and must be disposed of with care and in full compliance with federal, state and local regulations. Larger empty containers, such as drums, should be returned to the distributor or to a qualified drum reconditioner. To assure proper disposal of smaller empty containers, consult with state and local regulations and disposal authorities.

US GHS

Material Name: Natural Gas Condensate

* * * Section 14 - TRANSPORTATION INFORMATION * * *

DOT Information

Shipping Name: Petroleum Products, n.o.s. (condensate)

UN #: 1268 Hazard Class: 3

Additional Info.: Dependent on the product's properties, the shipper may also elect to classify as Gasoline UN1203 or Petroleum Crude Oil UN1267 - reference 49 CFR 172.101 for further description (e.g., packing group determination).

Placard:



* * * Section 15 - REGULATORY INFORMATION * * *

Regulatory Information

Component Analysis

This material contains one or more of the following chemicals required to be identified under SARA Section 302 (40 CFR 355 Appendix A), SARA Section 313 (40 CFR 372.65) and/or CERCLA (40 CFR 302.4).

Benzene (71-43-2)

SARA 313: 0.1% de minimis concentration

CERCLA: 10 lb final RQ (received an adjusted RQ of 10 lbs based on potential carcinogenicity in an August 14, 1989 final rule); 4.54 kg final RQ (received an adjusted RQ of 10 lbs based on potential carcinogenicity in an August 14, 1989 final rule)

SARA Section 311/312 – Hazard Classes

Acute Health	Chronic Health	<u>Fire</u>	Sudden Release of Pressure	Reactive
Х	Х	Х		

SARA SECTION 313 – SUPPLIER NOTIFICATION

This product contains the following toxic chemicals subject to the reporting requirements of section 313 of the Emergency Planning and Community Right-To-Know Act (EPCRA) of 1986 and of 40 CFR 372:

Material Name: Natural Gas Condensate

US GHS

INGREDIENT NAME (CAS NUMBER)

CONCENTRATION PERCENT BY WEIGHT

Benzene (71-43-2) <0.1 to 2

Canadian Regulatory Information

DSL/NDSL Inventory	This product has been classified in accordance with the hazard criteria of the Controlled Products Regulations (CPR) and the SDS contains all the information required by the Regulations.
Workplace Hazardous Materials Information System	 B2 - Flammable Liquid D1A – Material Causing Immediate and Serious Toxic Effects - Very Toxic Material D2A: Material Causing Other Toxic Effects Very Toxic D2B - Material Causing Other Toxic Effects - Toxic Material

European Union Regulatory Information

Labeling	Product is dangerous as defined by the European Union Dangerous Substances / Preparations Directives. Contains: Low Boiling Point Naphtha
Symbol	 F+ Extremely Flammable T Toxic N Dangerous for the Environment
Risk Phrases	R12-45-38-65-67-51/53 Extremely flammable. May cause cancer. Irritating to skin. Harmful: may cause lung damage if swallowed. Vapors may cause drowsiness and dizziness. Toxic to aquatic organisms, may cause long-term adverse effects in the aquatic environment.
Safety Phrases	S16-53-45-2-23-24-29-43-62 Keep away from sources of ignition – No smoking. Avoid exposure – obtain special instructions before use. In case of accident or if you feel unwell, seek medical advice immediately (show the label where possible). Keep out of reach of children. Do not breathe vapor. Avoid contact with skin. Do not empty into drains. In case of fire use foam/dry powder/CO2. If swallowed, do not induce vomiting: seek medical advice immediately and show this container or label.

Material Name: Natural Gas Condensate

State Regulations

Component Analysis – State

The following components appear on one or more of the following state hazardous substances lists

Component	CAS	СА	MA	MN	NJ	ΡΑ	RI
Octanes	111-65-9	Yes	No	Yes	Yes	Yes	Yes
Heptanes	142-82-5	Yes	No	Yes	Yes	Yes	Yes
n-Hexane	110-54-3	Yes	Yes	Yes	Yes	Yes	Yes
n-Pentane	109-66-0	Yes	No	Yes	Yes	Yes	Yes
n-Butane	106-97-8	Yes	No	Yes	Yes	Yes	Yes
Propane	74-98-6	No	No	Yes	Yes	Yes	Yes
Ethane	78-84-0	No	No	Yes	Yes	Yes	No
Benzene	71-43-2	Yes	Yes	Yes	Yes	Yes	Yes
Toluene	108-88-3	Yes	Yes	Yes	Yes	Yes	Yes
m-, o-, p-Xylene	1330-20-7	Yes	Yes	Yes	Yes	Yes	Yes

The following statement(s) are provided under the California Safe Drinking Water and Toxic Enforcement Act of 1986 (Proposition 65):

WARNING! This product contains a chemical known to the state of California to cause cancer.

WARNING! This product contains a chemical known to the state of California to cause Reproductive / developmental effects.

Component Analysis – WHMIS IDL

The following components are identified under the Canadian Hazardous Products Act

Ingredient Disclosure List:

Component	CAS #	Minimum Concentration
Benzene	71-43-2	0.1%

* * * Section 16 – OTHER INFORMATION * * *					
NFPA® Hazard Rating	Health 1 Fire 4 Reactivity 0				
HMIS® Hazard Rating	Health 1 Slight Fire 4 Severe Physical 0 Minimal * Chronic				

Material Name: Natural Gas Condensate

Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act: ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

Literature References

None

Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: January 29, 2014

Date of Last Revision: March 4, 2014

End of Sheet



Material Name: Wet Field Natural Gas

SYNONYMS: CNG, Natural Gas, Methane.

* * * Section 1 – PRODUCT AND COMPANY IDENTIFICATION * * *

PRODUCT NAM		Wet Field Natural Gas CAS Reg. No. 68410-63-9	EMERGENCY PHONE: AFTER HOURS:	(800) 878-1373 (800) 878-1373
PRODUCER: ADDRESS:	16 ⁻	tero Resources I5 Wynkoop Street nver, Colorado 80202	CHEMTREC PHONE:	(800) 424-9300

* * * Section 2 – HAZARDS IDENTIFICATION * * *

GHS Classification:

Flammable Gas – Category 1.

Gases Under Pressure – Gas.

Specific Target Organ Systemic Toxicity (STOT) – Single Exposure Category 2.

GHS LABEL ELEMENTS

Symbol(s)



Signal Word

Danger

Hazard Statements

Extremely flammable gas.

Contains gas under pressure, may explode if heated.

May cause damage to central nervous and respiratory systems.

Precautionary Statements

Prevention

Keep away from heat/sparks/open flames/hot surfaces. No smoking.

Do not breathe fume/gas/mist/vapors/spray.

Wash thoroughly after handling.

Do not eat, drink or smoke when using this product.

Material Name: Wet Field Natural Gas

Response

Leaking gas fire: Do not extinguish, unless leak can be stopped safely. Eliminate all ignition sources if safe to do so.

If exposed to gas, or concerned about possible exposure: Call a POISON CENTER or doctor/physician.

Storage

Protect from sunlight. Store in a well-ventilated place. Store in a secure area.

Disposal

Dispose of contents/containers in accordance with local/regional/national/international regulations.

* * * Section 3 – COMPOSITION	INFORMATION ON INGREDIENTS * * *

CAS #	Component	Percent
74-82-8	Methane	72 - 97
78-84-0	Ethane	2.2 - 14
74-98-6	Propane	0.0 - 8.0
106-97-8	Butanes	0.0 - 3.5
109-66-0	Pentanes	0.0 - 1.4
110-54-3	Hexanes	0.0 - 0.5
7727-37-9	Nitrogen	< 0.4
124-38-9	Carbon Dioxide	< 0.2
7782-44-7	Oxygen	< 0.04

Because natural gas is a natural product, composition can vary greatly.

* * * Section 4 – FIRST AID MEASURES * * *

First Aid: Eyes

In case of freeze burn, cover eyes to protect from light. Flush eyes with running water for at least fifteen (15) minutes. Following flushing, seek medical attention.

First Aid: Skin

Remove contaminated clothing. In case of blistering, frostbite or freeze burns, seek immediate medical attention.

Material Name: Wet Field Natural Gas

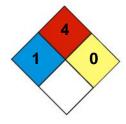
First Aid: Ingestion

Risk of ingestion is extremely low. However, if oral exposure occurs, seek immediate medical assistance.

First Aid: Inhalation

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

* * * Section 5 – FIRE FIGHTING MEASURES * * *



NFPA 704 Hazard Class

Health: **1** Flammability: **4** Instability: **0** (0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

General Fire Hazards

See Section 9 for Flammability Properties.

Forms a flammable mixture with air. If released, the resulting vapors will disperse with the prevailing wind. If a source of ignition is present where the vapor exists at a 5 - 15% concentration in air, the vapor will burn along the flame front toward the source of the fuel.

Hazardous Combustion Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

Extinguishing Media

Any extinguisher suitable for Class B fires, dry chemical, firefighting foam, CO2, and other gaseous agents. However, fire should not be extinguished unless flow of gas can be immediately stopped.

Unsuitable Extinguishing Media

None.

Fire Fighting Equipment / Instructions

Gas fires should not be extinguished unless flow of gas can be immediately stopped. Shut off gas source and allow gas to burn out. If spill or leak has not ignited, determine

Material Name: Wet Field Natural Gas

if water spray may assist in dispersing gas or vapor to protect personnel attempting to stop leak. Use water to cool equipment, surfaces and piping exposed to fire and excessive heat. For large fire, the use of unmanned hose holders or monitor nozzles may be advantageous to further minimize personnel exposure. Isolate area, particularly around piping. Let the fire burn unless leak can be stopped. Concentrate fire-fighting efforts on objects / materials ignited by the initial fire. Withdraw immediately in the event of a rising sound from a venting safety device.

Firefighting activities that may result in potential exposure to high heat, smoke or toxic by-products of combustion should require NIOSH-approved pressure-demand self-contained breathing apparatus with full facepiece and full protective clothing.

* * * Section 6 – ACCIDENTAL RELEASE MEASURES * * *

Recovery and Neutralization

Stop the source of the release, if safe to do so.

Materials and Methods for Clean-Up

Consider the use of water spray to disperse gas vapors. Do not use water spray to direct gas vapors toward sewer or drainage systems. Isolate the area until gas has dispersed. Ventilate and gas test area before entering.

Emergency Measures

Evacuate nonessential personnel and secure all ignition sources. No road flares, smoking or flames in hazard area. Consider wind direction. Stay upwind and uphill, if possible. Vapor cloud may be white, but color will dissipate as cloud disperses. Fire and explosion hazard is still present.

Personal Precautions and Protective Equipment

Cooling effect of expanding gas from leak may present frostbite / freeze burn hazard. Wear flame retardant (FR) clothing around un-ignited leak. Wear fire protective clothing around an active fire.

Environmental Precautions

Do not flush gas vapors toward sewer or drainage systems.

Prevention of Secondary Hazards

None.

Material Name: Wet Field Natural Gas

* * * Section 7 – HANDLING AND STORAGE * * *

Handling Procedures

Keep away from flame, sparks and excessive temperatures. Bond and ground containers. Use only in well ventilated areas.

Storage Procedures

Natural gas will be contained in the pipeline. Keep away from flame, sparks, excessive temperatures and open flames. Empty pipeline segments may contain explosive residues from natural gas liquids. Do not cut, heat, weld or expose containers to sources of ignition sections of pipeline unless the sections have been purged of natural gas residues.

Incompatibilities

Keep away from strong oxidizers, ignition sources and heat.

*** Section 8 – EXPOSURE CONTROLS / PERSONAL PROTECTION ***

Component Exposure Limits

Methane (74-82-8)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Ethane (74-84-0)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Propane (74-98-6)

ACGIH: 2500 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Butane (106-97-8)

ACGIH: 800 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Pentanes (109-66-0)

ACGIH: 600 ppm TWA (listed under Pentane, all isomers)

Hexanes (110-54-3)

ACGIH: 50 ppm TWA (listed under n-Hexane)

Material Name: Wet Field Natural Gas

Nitrogen (7727-37-9)

Simple Asphyxiant

Carbon Dioxide (124-38-9)

ACGIH: 5000 ppm TWA (listed under Carbon Dioxide)

Oxygen (7782-44-7)

N/A – Necessary for life

Engineering Measures

Use adequate ventilation to keep gas and vapor concentrations of this product below occupational exposure and flammability limits, particularly in confined spaces. Use explosion-proof equipment and lighting in classified / controlled areas.

Personal Protective Equipment: Respiratory

Use a NIOSH approved positive-pressure, supplied air respirator with escape bottle or self-contained breathing apparatus (SCBA) for gas concentrations above occupational exposure limits, for potential for uncontrolled release, if exposure levels are not known, or in an oxygen-deficient atmosphere. CAUTION: Flammability limits (i.e., explosion hazard should be considered when assessing the need to expose personnel to concentrations requiring respiratory protection.

Personal Protective Equipment: Hands

Use cold-impervious, insulating flame-retardant (FR) gloves where contact with pressurized gas may occur.

Personal Protective Equipment: Eyes

Where there is a possibility of pressurized gas contact, wear splash-proof safety goggles and faceshield.

Personal Protective Equipment: Skin and Body

Where contact with pressurized gas may occur, wear flame-retardant (FR) and a faceshield.

Appearance:	Colorless	Odor:	Odorless to slight petroleum odor
Physical State:	Gas	pH:	ND
Vapor Pressure:	40 atm @ -187°F (-86°C)	Vapor Density:	0.6
Boiling Point:	-259°F (-162°C)	Melting Point:	ND
Solubility (H2O):	3.5%	Specific Gravity:	0.4 @ -263°F (-164°C)

*** Section 9 – PHYSICAL AND CHEMICAL PROPERTIES ***

Material Name: Wet Field Natural Gas

Evaporation Rate: ND Octanol / H2O Coeff.: ND Flash Point Method: N/A Lower Flammability Limit: 3.8 – 6.5 (LFL): Auto Ignition: 900-1170°F (482-632°C) VOC: ND Flash Point: Flammable Gas

Upper Flammability Limit: 13-17 (UFL): Burning Rate: ND

* * * Section 10 – CHEMICAL STABILITY & REACTIVITY INFORMATION * * *

Chemical Stability

This is a stable material.

Hazardous Reaction Potential

Will not occur.

Conditions to Avoid

Keep away from strong oxidizers, ignition sources and heat.

Hazardous Decomposition Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

* * * Section 11 - TOXICOLOGICAL INFORMATION * * *

Acute Toxicity

A: General Product Information

Methane and ethane, the main components of natural gas, are considered practically inert in terms of physiological effects. At high concentrations these materials act as simple asphyxiants and may cause death due to lack of oxygen.

B. Component Analysis – LD50/LC50

Methane (74-82-8)

Inhalation LC50 Mouse 326 g/m3 2h

Ethane (74-84-0)

Inhalation LC50 Rat 658 mg/l 4h

Propane (74-98-6)

Inhalation LC50 Rat 658 mg/l 4h

Material Name: Wet Field Natural Gas

Butanes (106-97-8) Inhalation LC50 Rat 658 g/m3 4h

Pentanes (109-66-0) Inhalation LD50 Rat 364 g/m3 4h

Hexanes (110-54-3) Inhalation LC50 Rat > 20 mg/l 4h

Nitrogen (7727-37-9) Simple Asphyxiant

Carbon Dioxide (124-38-9) Inhalation LC50 Human 100,000 ppm 1minute

Oxygen (7782-44-7) N/A – Necessary for life

Potential Health Effects: Skin Corrosion Property / Stimulativeness

This product is not reported to have any skin sensitization effects.

Generative Cell Mutagenicity

This product is not reported to have any mutagenic effects.

Carcinogenicity

A: General Product Information

This product is not reported to have any carcinogenic effects.

B: Component Carcinogenicity

None of this product's components are listed by ACGIH, IARC, OSHA, NIOSH, or NTP.

Reproductive Toxicity

This product is not reported to have any reproductive toxicity effects.

Specified Target Organ General Toxicity: Single Exposure

This product may cause damage to the heart.

Specified Target Organ General Toxicity: Repeated Exposure

This product is not reported to have any specific target organ repeat effects.

Aspiration Respiratory Organs Hazard

This product is not reported to have any aspiration hazard effects.

Page 8 of 11

Material Name: Wet Field Natural Gas

*** Section 12 - ECOLOGICAL INFORMATION ***

Ecotoxicity

A: General Product Information

Keep gas and vapors out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

B: Component Analysis – Ecotoxicity – Aquatic Toxicity

No ecotoxicity data are available for this product's components.

Persistance / Degradability

No information available.

Bioaccumulation

No information available.

Mobility in Soil

No information available.

* * * Section 13 - DISPOSAL CONSIDERATIONS * * *

Waste Disposal Instructions

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

Disposal of Contaminated Containers or Packaging

Dispose of contents / container in accordance with local / regional / national / international regulations.

* * * Section 14 – TRANSPORTATION INFORMATION * * *

DOT Information

Shipping Name: Natural Gas, Compressed UN #: 1971 Hazard Class: 2.1

Placard:



Material Name: Wet Field Natural Gas

* * * Section 15 – REGULATORY INFORMATION * * *

Regulatory Information Component Analysis

None of this products components are listed under SARA Section 302 (40 CFR 355 Appendix A.

n-hexane is listed under SARA Section 313 (40 CFR 372.65). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

n-hexane is listed under CERCLA (40 CFR 302.4). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

SARA Section 311/312 – Hazard Classes

Acute Health	Chronic Health	<u>Fire</u>	Sudden Release of Pressure	Reactive
		Х	Х	

SARA Section 313 – Supplier Notification

This product contains one chemical (n-Hexane) that is subject to the reporting requirements of section 313 of the Emergency Planning and Community Right-to-know act (EPCRA) of 1986 and of 40 CFR 372. However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

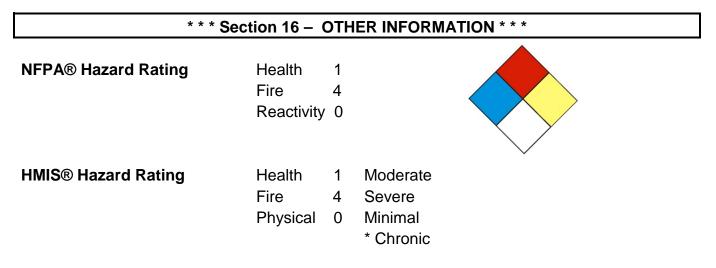
State Regulations

Component Analysis – State

The following components appear on one or more of the following state hazardous substances lists:

Component	CAS	CA	MA	MN	NJ	РА	RI
Methane	74-82-8	No	No	Yes	Yes	Yes	No
Ethane	78-84-0	No	No	Yes	Yes	Yes	No
Propane	74-98-6	No	No	Yes	Yes	Yes	Yes
Butane	106-97-8	Yes	No	Yes	Yes	Yes	Yes
Pentanes	109-66-0	Yes	No	Yes	Yes	Yes	Yes
Hexanes	110-54-3	Yes	Yes	Yes	Yes	Yes	Yes
Nitrogen	7727-37-9	No	No	No	No	No	No
Carbon Dioxide	124-38-9	Yes	No	Yes	Yes	Yes	Yes
Oxygen	7782-44-7	No	No	No	No	No	No

Material Name: Wet Field Natural Gas



Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act: ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

Literature References

None

Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: February 7, 2014

Date of Last Revision: March 4,, 2014



Material Name: Dry Field Natural Gas

US GHS

SYNONYMS: CNG, Natural Gas, Methane.

* * * Section 1 – PRODUCT AND COMPANY IDENTIFICATION * * *

PRODUCT NAM		Dry Field Natural Gas CAS Reg. No. 68410-63-9	EMERGENCY PHONE: AFTER HOURS:	(800) 878-1373 (800) 878-1373
PRODUCER: ADDRESS:	16′	tero Resources I5 Wynkoop Street nver, Colorado 80202	CHEMTREC PHONE:	(800) 424-9300

* * * Section 2 – HAZARDS IDENTIFICATION * * *

GHS Classification:

Flammable Gas – Category 1.

Gases Under Pressure – Gas.

Specific Target Organ Systemic Toxicity (STOT) – Single Exposure Category 2.

GHS LABEL ELEMENTS

Symbol(s)



Signal Word

Danger

Hazard Statements

Extremely flammable gas.

Contains gas under pressure, may explode if heated.

May cause damage to central nervous and respiratory systems.

Precautionary Statements

Prevention

Keep away from heat/sparks/open flames/hot surfaces. No smoking.

Do not breathe fume/gas/mist/vapors/spray.

Wash thoroughly after handling.

Do not eat, drink or smoke when using this product.

Material Name: Dry Field Natural Gas

Response

Leaking gas fire: Do not extinguish, unless leak can be stopped safely. Eliminate all ignition sources if safe to do so.

If exposed to gas, or concerned about possible exposure: Call a POISON CENTER or doctor/physician.

Storage

Protect from sunlight. Store in a well-ventilated place. Store in a secure area.

Disposal

Dispose of contents/containers in accordance with local/regional/national/international regulations.

* * * Section 3 – COMPOSITION / INFORMATION ON INGREDIENTS * * *
--

CAS #	Component	Percent
74-82-8	Methane	95.01
78-84-0	Ethane	3.99
74-98-6	Propane	0.32
106-97-8	Butanes	0.07
109-66-0	Pentanes	0.02
110-54-3	Hexanes	0.01
7727-37-9	Nitrogen	0.35
124-38-9	Carbon Dioxide	0.19
7782-44-7	Oxygen	0.03

Because natural gas is a natural product, composition can vary greatly.

* * * Section 4 – FIRST AID MEASURES * * *

First Aid: Eyes

In case of freeze burn, cover eyes to protect from light. Flush eyes with running water for at least fifteen (15) minutes. Following flushing, seek medical attention.

First Aid: Skin

Remove contaminated clothing. In case of blistering, frostbite or freeze burns, seek immediate medical attention.

Material Name: Dry Field Natural Gas

First Aid: Ingestion

Risk of ingestion is extremely low. However, if oral exposure occurs, seek immediate medical assistance.

First Aid: Inhalation

Remove person to fresh air. If person is not breathing, provide artificial respiration. If necessary, provide additional oxygen once breathing is restored if trained to do so. Seek medical attention immediately.

* * * Section 5 – FIRE FIGHTING MEASURES * * *



NFPA 704 Hazard Class

Health: **1** Flammability: **4** Instability: **0** (0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

General Fire Hazards

See Section 9 for Flammability Properties.

Forms a flammable mixture with air. If released, the resulting vapors will disperse with the prevailing wind. If a source of ignition is present where the vapor exists at a 5 - 15% concentration in air, the vapor will burn along the flame front toward the source of the fuel.

Hazardous Combustion Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

Extinguishing Media

Any extinguisher suitable for Class B fires, dry chemical, fire fighting foam, CO2, and other gaseous agents. However, fire should not be extinguished unless flow of gas can be immediately stopped.

Unsuitable Extinguishing Media

None.

Fire Fighting Equipment / Instructions

Gas fires should not be extinguished unless flow of gas can be immediately stopped. Shut off gas source and allow gas to burn out. If spill or leak has not ignited, determine

Material Name: Dry Field Natural Gas

if water spray may assist in dispersing gas or vapor to protect personnel attempting to stop leak. Use water to cool equipment, surfaces and piping exposed to fire and excessive heat. For large fire, the use of unmanned hose holders or monitor nozzles may be advantageous to further minimize personnel exposure. Isolate area, particularly around piping. Let the fire burn unless leak can be stopped. Concentrate fire-fighting efforts on objects / materials ignited by the initial fire. Withdraw immediately in the event of a rising sound from a venting safety device.

Firefighting activities that may result in potential exposure to high heat, smoke or toxic by-products of combustion should require NIOSH-approved pressure-demand self-contained breathing apparatus with full facepiece and full protective clothing.

* * * Section 6 – ACCIDENTAL RELEASE MEASURES * * *

Recovery and Neutralization

Stop the source of the release, if safe to do so.

Materials and Methods for Clean-Up

Consider the use of water spray to disperse gas vapors. Do not use water spray to direct gas vapors toward sewer or drainage systems. Isolate the area until gas has dispersed. Ventilate and gas test area before entering.

Emergency Measures

Evacuate nonessential personnel and secure all ignition sources. No road flares, smoking or flames in hazard area. Consider wind direction. Stay upwind and uphill, if possible. Vapor cloud may be white, but color will dissipate as cloud disperses. Fire and explosion hazard is still present.

Personal Precautions and Protective Equipment

Cooling effect of expanding gas from leak may present frostbite / freeze burn hazard. Wear flame retardant (FR) clothing around un-ignited leak. Wear fire protective clothing around an active fire.

Environmental Precautions

Do not flush gas vapors toward sewer or drainage systems.

Prevention of Secondary Hazards

None.

Material Name: Dry Field Natural Gas

* * * Section 7 – HANDLING AND STORAGE * * *

Handling Procedures

Keep away from flame, sparks and excessive temperatures. Bond and ground containers. Use only in well ventilated areas.

Storage Procedures

Natural gas will be contained in the pipeline. Keep away from flame, sparks, excessive temperatures and open flames. Empty pipeline segments may contain explosive residues from natural gas liquids. Do not cut, heat, weld or expose containers to sources of ignition sections of pipeline unless the sections have been purged of natural gas residues.

Incompatibilities

Keep away from strong oxidizers, ignition sources and heat.

* * * Section 8 – EXPOSURE CONTROLS / PERSONAL PROTECTION * * *

Component Exposure Limits

Methane (74-82-8)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Ethane (74-84-0)

ACGIH: 1000 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Propane (74-98-6)

ACGIH: 2500 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Butane (106-97-8)

ACGIH: 800 ppm TWA (listed under Aliphatic hydrocarbon gases : Alkane C1-4)

Pentanes (109-66-0)

ACGIH: 600 ppm TWA (listed under Pentane, all isomers)

Hexanes (110-54-3)

ACGIH: 50 ppm TWA (listed under n-Hexane)

Material Name: Dry Field Natural Gas

US GHS

Nitrogen (7727-37-9)

Simple Asphyxiant

Carbon Dioxide (124-38-9)

ACGIH: 5000 ppm TWA (listed under Carbon Dioxide)

Oxygen (7782-44-7)

N/A – Necessary for life

Engineering Measures

Use adequate ventilation to keep gas and vapor concentrations of this product below occupational exposure and flammability limits, particularly in confined spaces. Use explosion-proof equipment and lighting in classified / controlled areas.

Personal Protective Equipment: Respiratory

Use a NIOSH approved positive-pressure, supplied air respirator with escape bottle or self-contained breathing apparatus (SCBA) for gas concentrations above occupational exposure limits, for potential for uncontrolled release, if exposure levels are not known, or in an oxygen-deficient atmosphere. CAUTION: Flammability limits (i.e., explosion hazard should be considered when assessing the need to expose personnel to concentrations requiring respiratory protection.

Personal Protective Equipment: Hands

Use cold-impervious, insulating flame-retardant (FR) gloves where contact with pressurized gas may occur.

Personal Protective Equipment: Eyes

Where there is a possibility of pressurized gas contact, wear splash-proof safety goggles and faceshield.

Personal Protective Equipment: Skin and Body

Where contact with pressurized gas may occur, wear flame-retardant (FR) and a faceshield.

Appearance:	Colorless	Odor:	Odorless to slight petroleum odor
Physical State:	Gas	pH:	ND
Vapor Pressure:	40 atm @ -187°F (-86°C)	Vapor Density:	0.6
Boiling Point:	-259°F (-162°C)	Melting Point:	ND
Solubility (H2O):	3.5%	Specific Gravity:	0.4 @ -263°F (-164°C)

* * * Section 9 – PHYSICAL AND CHEMICAL PROPERTIES * * *

Material Name: Dry Field Natural Gas

Evaporation Rate: ND Octanol / H2O Coeff.: ND Flash Point Method: N/A Lower Flammability Limit: 3.8 – 6.5 (LFL): Auto Ignition: 900-1170°F (482-632°C) VOC: ND Flash Point: Flammable Gas

Upper Flammability Limit: 13-17 (UFL): Burning Rate: ND

* * * Section 10 – CHEMICAL STABILITY & REACTIVITY INFORMATION * * *

Chemical Stability

This is a stable material.

Hazardous Reaction Potential

Will not occur.

Conditions to Avoid

Keep away from strong oxidizers, ignition sources and heat.

Hazardous Decomposition Products

Carbon monoxide, carbon dioxide and non-combusted hydrocarbons (smoke).

*** Section 11 – TOXICOLOGICAL INFORMATION ***

Acute Toxicity

A: General Product Information

Methane and ethane, the main components of natural gas, are considered practically inert in terms of physiological effects. At high concentrations these materials act as simple asphyxiants and may cause death due to lack of oxygen.

B. Component Analysis – LD50/LC50

Methane (74-82-8)

Inhalation LC50 Mouse 326 g/m3 2h

Ethane (74-84-0)

Inhalation LC50 Rat 658 mg/l 4h

Propane (74-98-6)

Inhalation LC50 Rat 658 mg/l 4h

Material Name: Dry Field Natural Gas

Butanes (106-97-8) Inhalation LC50 Rat 658 g/m3 4h

Pentanes (109-66-0) Inhalation LD50 Rat 364 g/m3 4h

Hexanes (110-54-3) Inhalation LC50 Rat > 20 mg/l 4h

Nitrogen (7727-37-9) Simple Asphyxiant

Carbon Dioxide (124-38-9) Inhalation LC50 Human 100,000 ppm 1minute

Oxygen (7782-44-7) N/A – Necessary for life

Potential Health Effects: Skin Corrosion Property / Stimulativeness

This product is not reported to have any skin sensitization effects.

Generative Cell Mutagenicity

This product is not reported to have any mutagenic effects.

Carcinogenicity

A: General Product Information

This product is not reported to have any carcinogenic effects.

B: Component Carcinogenicity

None of this product's components are listed by ACGIH, IARC, OSHA, NIOSH, or NTP.

Reproductive Toxicity

This product is not reported to have any reproductive toxicity effects.

Specified Target Organ General Toxicity: Single Exposure

This product may cause damage to the heart.

Specified Target Organ General Toxicity: Repeated Exposure

This product is not reported to have any specific target organ repeat effects.

Aspiration Respiratory Organs Hazard

This product is not reported to have any aspiration hazard effects.

Page 8 of 11

Material Name: Dry Field Natural Gas

*** Section 12 - ECOLOGICAL INFORMATION ***

Ecotoxicity

A: General Product Information

Keep gas and vapors out of sewers, drainage areas, and waterways. Report spills and releases, as applicable under Federal and State regulations.

B: Component Analysis – Ecotoxicity – Aquatic Toxicity

No ecotoxicity data are available for this product's components.

Persistance / Degradability

No information available.

Bioaccumulation

No information available.

Mobility in Soil

No information available.

*** Section 13 - DISPOSAL CONSIDERATIONS ***

Waste Disposal Instructions

See Section 7 for Handling Procedures. See Section 8 for Personal Protective Equipment Recommendations.

Disposal of Contaminated Containers or Packaging

Dispose of contents / container in accordance with local / regional / national / international regulations.

* * * Section 14 – TRANSPORTATION INFORMATION * * *

DOT Information

Shipping Name: Natural Gas, Compressed UN #: 1971 Hazard Class: 2.1

Placard:



Material Name: Dry Field Natural Gas

*** Section 15 – REGULATORY INFORMATION ***

Regulatory Information Component Analysis

None of this products components are listed under SARA Section 302 (40 CFR 355 Appendix A.

n-hexane is listed under SARA Section 313 (40 CFR 372.65). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

n-hexane is listed under CERCLA (40 CFR 302.4). However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

SARA Section 311/312 – Hazard Classes

Acute Health	Chronic Health	<u>Fire</u>	Sudden Release of Pressure	Reactive
		Х	Х	

SARA Section 313 – Supplier Notification

This product contains one chemical (n-Hexane) that is subject to the reporting requirements of section 313 of the Emergency Planning and Community Right-to-know act (EPCRA) of 1986 and of 40 CFR 372. However the concentration of this component is approximately 0.01 % in compressed natural gas and is therefore far under the reporting threshold for the chemical.

State Regulations

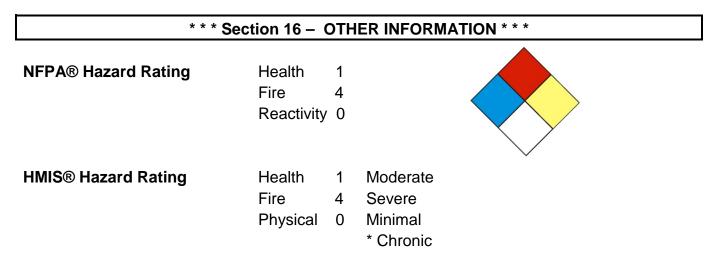
Component Analysis – State

The following components appear on one or more of the following state hazardous substances lists:

Component	CAS	CA	MA	MN	NJ	PA	RI
Methane	74-82-8	No	No	Yes	Yes	Yes	No
Ethane	78-84-0	No	No	Yes	Yes	Yes	No
Propane	74-98-6	No	No	Yes	Yes	Yes	Yes
Butane	106-97-8	Yes	No	Yes	Yes	Yes	Yes
Pentanes	109-66-0	Yes	No	Yes	Yes	Yes	Yes
Hexanes	110-54-3	Yes	Yes	Yes	Yes	Yes	Yes
Nitrogen	7727-37-9	No	No	No	No	No	No
Carbon Dioxide	124-38-9	Yes	No	Yes	Yes	Yes	Yes
Oxygen	7782-44-7	No	No	No	No	No	No

Material Name: Dry Field Natural Gas

US GHS



Key/Legend

EPA = Environmental Protection Agency; TSCA = Toxic Substance Control Act: ACGIH = American Conference of Governmental Industrial Hygienists; IARC = International Agency for Research on Cancer; NIOSH = National Institute for Occupational Safety and Health; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; NJTSR = New Jersey Trade Secret Registry.

Literature References

None

Other Information

The information presented herein has been compiled from sources considered to be dependable, and is accurate and reliable to the best of our knowledge and belief, but is not guaranteed to be so. Since conditions of use are beyond our control, we make no warranties, expressed or implied, except those that may be contained in our written contract of sale or acknowledgment.

Vendor assumes no responsibility for injury to vendee or third persons proximately caused by the material if reasonable safety procedures are not adhered to as stipulated in the data sheet. Additionally, vendor assumes no responsibility for injury to vendee or third persons proximately caused by abnormal use of the material, even if reasonable safety procedures are followed. Furthermore, vendee assumes the risk in their use of the material.

Date of Preparation: January 30, 2014

Date of Last Revision: March 4, 2014

Attachment I. Emission Units Table

Attachment I

Emission Units Table

(includes all emission units and air pollution control devices

that will be part of this permit application review, regardless of permitting status)

EmissionEmissionUnit ID1Point ID2		Emission Unit Description	Year Installed/ Modified	Design Capacity	Type ³ and of Char		Control Device ⁴	
C-2100	100 1E Compressor Engine #1		2016	1,680 hp	Modified	NSCR (1C)		
C-2110	2E	Compressor Engine #2	2016	1,680 hp	Modified	NSCR	(2C)	
C-2120	3E	Compressor Engine #3	2016	1,680 hp	Modified	NSCR	(3C)	
C-2130	4E	Compressor Engine #4	2016	1,680 hp	Modified	NSCR	(4C)	
C-2140	5E	Compressor Engine #5	2016	1,680 hp	Modified	NSCR	(5C)	
C-2150	6E	Compressor Engine #6	2016	1,680 hp	Modified	NSCR	(6C)	
C-2160	7E	Compressor Engine #7	2016	1,680 hp	Modified	NSCR	(7C)	
C-2170	8E	Compressor Engine #8	2016	1,680 hp	Modified	NSCR	(8C)	
C-2180	9E	Compressor Engine #9	2016	1,680 hp	Modified	NSCR	(9C)	
C-2190	10E	Compressor Engine #10	2016	1,680 hp	Modified	NSCR	(10C)	
C-2200	11E	Compressor Engine #11	2016	1,680 hp	Modified	NSCR	(11C)	
G-8000	12E	Microturbine Generator #1	2016	600 kWe	N/A	None		
SV-3110	13E	Dehydrator Still Vent #1	2016	88 MMscfd	Modified	FL-100	00 (12C)	
FT-3110	14E	Dehydrator Flash Tank #1	2016	88 MMscfd	Modified	R-3110) (15E)	
R-3110	15E	Dehydrator Reboiler #1	2016	1.5 mmbtu/hr	Modified	None		
SV-3210	16E	Dehydrator Still Vent #2	2016	88 MMscfd	Modified	FL-100	00 (12C)	
FT-3210	17E	Dehydrator Flash Tank #2	2016	88 MMscfd	Modified	R-3210) (18E)	
R-3210	18E	Dehydrator Reboiler #2	2016	1.5 mmbtu/hr	Modified	None		
TK-9000	19E	Settling Tank 1	2016	500 barrel	N/A		5000 & VRU (13C & 14C)	
TK-9200	20E	Condensate Tank 1	2016	400 barrel	N/A	VRU-6	000 & VRU 13C & 14C)	
TK-9210	0 21E Condensate Tank 2		2016	400 barrel	N/A	VRU-6000 & VRU- 6100 (13C & 14C)		
TK-9100	22E	Produced Water Tank 1	2016	400 barrel			VRU-6000 & VRU- 6100 (13C & 14C)	
TK-9110	23E	Produced Water Tank 2	2016	400 barrel	N/A		5000 & VRU 13C & 14C)	

CATHT1 24E		Catalytic Heater for Generator Fuel	2016	0.024 MMBtu/hr	N/A	None	
	NSCR Catalyst for Compressor #1		2016		Modified	1C	
		NSCR Catalyst for Compressor #2	2016		Modified	2C	
		NSCR Catalyst for Compressor #3	2016		Modified	3C	
		NSCR Catalyst for Compressor #4	2016		Modified	4C	
		NSCR Catalyst for Compressor #5	2016		Modified	5C	
		NSCR Catalyst for Compressor #6	2016		Modified	6C	
		NSCR Catalyst for Compressor #7	2016		Modified	7C	
		NSCR Catalyst for Compressor #8	2016		Modified	8C	
		NSCR Catalyst for Compressor #9	2016		Modified	9C	
		NSCR Catalyst for Compressor #10	2016		Modified	10C	
		NSCR Catalyst for Compressor #11	2016		Modified	11C	
FL-1000	25E	Flare Combustion Device 1	2016	9.21 MMBtu/hr	N/A	12C	
VRU-6000		Vapor Recovery Unit 1	2016	TBD	N/A	13C	
VRU-6100		Vapor Recovery Unit 2	2016	TBD	N/A	14C	
C-2210	26E	Compressor Engine #12	2016	1,680 hp	New	NSCR(15C)	
C-2220	27E	Compressor Engine #13	2016	1,680 hp	New	NSCR(16C)	
		NSCR Catalyst for Compressor #12	2016		New	15C	
		NSCR Catalyst for Compressor #13	2016		New	16C	
LDOUT1	28E	Tanker Truck Loading	2016	195 bbl/day	N/A	none	

¹ For Emission Units (or <u>Sources</u>) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.
 ² For <u>E</u>mission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.
 ³ New, modification, removal
 ⁴ For <u>C</u>ontrol Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

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Attachment J. Emission Point Data Summary Sheet

Attachment J EMISSION POINTS DATA SUMMARY SHEET

							Table '	1: Emissions [Data						
Emission Point ID No. (Must match Emission Units Table & Plot Plan)	Emission Point Type ¹	Vented		Vented Control Device Through This Point (Must match (Must match Emission Units Table & Plot Plan)		Vent Time for Emission Unit (chemical processes only)		All Regulated Pollutants - Chemical Name/CAS ³ (Speciate VOCs & HAPS)	- Potential Uncontrolled ³³ Emissions ⁴		Potential Potential Jncontrolled Controlled		Emission Form or Phase (At exit conditions, Solid, Liquid	Est. Method Used ⁶	Emission Concentration ⁷ (ppmv or mg/m ⁴)
		ID No.	Source	ID No.	Device Type	Short Term ²	Max (hr/yr)		lb/hr	ton/yr	lb/hr	ton/yr	or Gas/Vapor)		
1E	Upward Vertical Stack	C-2100	Com- pressor engine 1	1C	NSCR catalyst	С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.74 47.04 1.74 0.27 0.008 0.35 0.19 2081	222.24 206.02 7.62 1.18 0.036 1.54 0.81 9113	1.27 1.18 0.28 0.27 0.008 0.18 0.019 1996	5.56 5.15 1.22 1.18 0.036 0.81 0.081 8744	Gas/Vapor	EE	
2E	Upward Vertical Stack	C-2110	Com- pressor engine 2	2C	NSCR catalyst	С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.74 47.04 1.74 0.27 0.008 0.35 0.19 2081	222.24 206.02 7.62 1.18 0.036 1.54 0.81 9113	1.27 1.18 0.28 0.27 0.008 0.18 0.019 1996	5.56 5.15 1.22 1.18 0.036 0.81 0.081 8744	Gas/Vapor	EE	
3E	Upward Vertical Stack	C-2120	Com- pressor engine 3	3C	NSCR catalyst	С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.74 47.04 1.74 0.27 0.008 0.35 0.19 2081	222.24 206.02 7.62 1.18 0.036 1.54 0.81 9113	1.27 1.18 0.28 0.27 0.008 0.18 0.019 1996	5.56 5.15 1.22 1.18 0.036 0.81 0.081 8744	Gas/Vapor	EE	

			1											I I	
4E	Upward Vertical	C-2130	Com- pressor	4C	NSCR catalyst	C	8,760	NOx CO	50.74 47.04	222.24 206.02	1.27 1.18	5.56 5.15	Gas/Vapor	EE	
	Stack		engine 4		,			VOC	1.74	7.62	0.28	1.22			
								PM10	0.27	1.18	0.28	1.18			
								SO2	0.27	0.036	0.27	0.036			
								Total HAPs	0.35	1.54	0.000	0.81			
								Formaldehyde		0.81	0.10	0.081			
								CO2e	2081	9113	1996	8744			
5E	Upward Vertical	C-2140	Com- pressor	5C	NSCR catalyst	С	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
	Stack		engine 5		Catalyst			CO	47.04	206.02	1.18	5.15			
	Stuck							VOC	1.74	7.62	0.28	1.22			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde		0.81	0.019	0.081			
	_							CO2e	2081	9113	1996	8744			
6E	Upward	C-2150	Com-	6C	NSCR	С	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
	Vertical		pressor engine 6		catalyst			CO	47.04	206.02	1.18	5.15			
	Stack		_					VOC	1.74	7.62	0.28	1.22			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2081	9113	1996	8744			
7E	Upward	C-2160	Com-	7C	NSCR	С	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
	Vertical		pressor engine 7		catalyst	-		CO	47.04	206.02	1.18	5.15	1		
	Stack		engine /					VOC	1.74	7.62	0.28	1.22			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2081	9113	1996	8744			
								•							

0.5	TT 1	0.2170	Com-	0.0	NGCD	a	0.7.0	NO	50 74	222.24	1.07		C N	D D	
8E	Upward Vertical	C-2170	pressor	8C	NSCR catalyst	C	8,760	NOx CO	50.74	222.24	1.27	5.56 5.15	Gas/Vapor	EE	
	Stack		engine 8		cataryst			VOC	47.04	206.02	1.18				
								PM10	1.74	7.62	0.28	1.22			
								SO2	0.27	1.18 0.036	0.27 0.008	1.18 0.036			
								Total HAPs	0.008 0.35	0.036 1.54	0.008	0.030			
								Formaldehyde		0.81	0.18	0.81			
								CO2e	2081	9113	0.019 1996	8744			
										-					
9E	Upward	C-2180	Com- pressor	9C	NSCR	С	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
	Vertical Stack		engine 9		catalyst			СО	47.04	206.02	1.18	5.15			
	Stack							VOC	1.74	7.62	0.28	1.22			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde		0.81	0.019	0.081			
								CO2e	2081	9113	1996	8744			
10E	Upward	C-2190	Com-	10C	NSCR	С	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
	Vertical		pressor engine		catalyst			CO	47.04	206.02	1.18	5.15			
	Stack		10					VOC	1.74	7.62	0.28	1.22			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2081	9113	1996	8744			
11E	Upward	C-2200	Com-	11C	NSCR	С	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
	Vertical		pressor		catalyst	-	-,	CO	47.04	206.02	1.18	5.15	1		
	Stack		engine 11					VOC	1.74	7.62	0.28	1.22			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2081	9113	1996	8744			

12E	Upward Vertical Stack	G8000	Microtu rbine Genera tor			С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	0.24 0.66 0.06 0.04 0.02 0.006 0.004 799	1.05 2.89 0.26 0.18 0.09 0.03 0.02 3499	0.24 0.66 0.06 0.04 0.02 0.006 0.004 799	1.05 2.89 0.26 0.18 0.09 0.03 0.02 3499	Gas/Vapor	EE	
13E	Upward Vertical Stack	SV- 3110	Dehydr ator Still Vent 1	12C	Flare- 98% Control	С	8,760	VOC Total HAPs Benzene Toluene Ethylbenzene Xylenes n-Hexane CO2e	15.90 7.18 0.26 1.17 1.03 4.47 0.24 436	69.65 31.43 1.16 5.13 4.51 19.59 1.04 1910	See 25E emissi ons		Gas/Vapor	EE	
14E	Used for fuel in 15E	FT-3110	Dehydr ator Flash Gas 1	Used for Fuel in 15E	95% Combu stion	С	8,760	VOC Total HAPs Benzene Toluene Ethylbenzene Xylenes n-Hexane CO2e	32.28 0.68 0.022 0.056 0.026 0.069 0.50 1367	141.39 2.96 0.095 0.24 0.11 0.30 2.21 5988	See 15E emissi ons		Gas/Vapor	EE	
15E	Upward Vertical Stack	R-3110	Dehydr ator Reboile r 1			С	8,760	NOx CO VOC PM10 SO2 Total HAPs CO2e	0.18 0.15 0.01 0.01 0.001 0.004 176.1	0.81 0.68 0.04 0.06 0.005 0.015 771	0.18 0.15 0.66 0.01 0.001 0.017 204.1	0.81 0.68 2.87 0.06 0.005 0.074 895	Gas/Vapor	EE	

16E	Upward Vertical Stack	SV- 3210	Dehydr ator Still Vent 2	12C	Flare- 98% Control	С	8,760	VOC Total HAPs Benzene Toluene Ethylbenzene Xylenes n-Hexane CO2e	15.90 7.18 0.26 1.17 1.03 4.47 0.24 436	69.65 31.43 1.16 5.13 4.51 19.59 1.04 1910	See 25E emissi ons		Gas/Vapor	EE	
17E	Used for fuel in 18E	FT-3210	Dehydr ator Flash Gas 2	Used for Fuel in 18E	95% Combu stion	С	8,760	VOC Total HAPs Benzene Toluene Ethylbenzene Xylenes n-Hexane CO2e	32.28 0.68 0.022 0.056 0.026 0.069 0.50 1367	141.39 2.96 0.095 0.24 0.11 0.30 2.21 5988	See 18E emissi ons		Gas/Vapor	EE	
18E	Upward Vertical Stack	R-3210	Dehydr ator Reboile r 2			С	8,760	NOx CO VOC PM10 SO2 Total HAPs CO2e	0.18 0.15 0.01 0.01 0.001 0.004 176.1	0.81 0.68 0.04 0.06 0.005 0.015 771	0.18 0.15 0.66 0.01 0.001 0.017 204.1	0.81 0.68 2.87 0.06 0.005 0.074 895	Gas/Vapor	EE	
19E	Upward Vertical Stack	TK- 9000	Settler Tank	13C	VRU- 98% capture	С	8,760	VOC Total HAPs CO2e	128.9 3.94 325.8	564.6 17.25 1427	2.58 0.079 6.62	11.29 0.35 29	Gas/Vapor	EE	
20E	Upward Vertical Stack	TK- 9200	Conden sate Tank 1	13C	VRU- 98% capture	С	8,760	VOC Total HAPs CO2e		6.82 0.017 2.01	0.032 7.8e-5 0.011	0.14 3.4e-4 0.047	Gas/Vapor	EE	
21E	Upward Vertical Stack	TK- 9210	Conden sate Tank 2	13C	VRU- 98% capture	С	8,760	VOC Total HAPs CO2e	1.56 0.004 0.046	6.82 0.017 2.01	0.032 7.8e-5 0.011	0.14 3.4e-4 0.047	Gas/Vapor	EE	

22E	Upward Vertical Stack	TK- 9100	Produc ed Water Tank 1	13C	VRU- 98% capture	С	8,760	VOC Total HAPs CO2e	8.7e-5 3.4e-8 0.002		1.8e-6 6.9e-10 7.5e-5	7.7e-6 3.0e-9 3.3e-4	Gas/Vapor	EE	
23E	Upward Vertical Stack	ТК- 9110	Produc ed Water Tank 2	13C	VRU- 98% capture	С	8,760	VOC Total HAPs CO2e	8.7e-5 3.4e-8 0.002		1.8e-6 6.9e-10 7.5e-5	7.7e-6 3.0e-9 3.3e-4	Gas/Vapor	EE	
24E	Upward Vertical Stack	CATHT 1	Catalyti c Heater for Genera tor Fuel			С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	0.0029 0.0025 1.6 E-4 2.2 E-4 1.8 E-5 6 E-5 2 E-6 2.82	0.013 0.011 7.1 E-4 0.001 7.7 E-5 2.4 E-4 1 E-5 12	0.0029 0.0025 1.6 E-4 2.2 E-4 1.8 E-5 6 E-5 2 E-6 2.82	0.013 0.011 7.1 E-4 0.001 7.7 E-5 2.4 E-4 1 E-5 12	Gas/Vapor	EE	
25E	Upward Vertical Stack	FL- 1000	Flare combu stion device 1			С	8,760	NOx CO VOC Benzene Toluene Ethylbenzene Xylene n-Hexane Total HAPs CO2e	 	 	0.63 2.86 0.64 0.011 0.047 0.041 0.18 0.010 0.29 1101	2.75 12.51 2.79 0.046 0.21 0.18 0.78 0.042 1.26 4822	Gas/Vapor	EE	
26E	Upward Vertical Stack	C-2210	Com- pressor engine 12	15C	NSCR catalyst	С	8,760	NOx CO VOC PM10 SO2 Total HAPs Formaldehyde CO2e	50.74 47.04 1.74 0.27 0.008 0.35 0.19 2081	222.24 206.02 7.62 1.18 0.036 1.54 0.81 9113	1.27 1.18 0.28 0.27 0.008 0.18 0.019 1996	5.56 5.15 1.22 1.18 0.036 0.81 0.081 8744	Gas/Vapor	EE	

27E	Upward	C-2220	Com-	16C		С	8,760	NOx	50.74	222.24	1.27	5.56	Gas/Vapor	EE	
	Vertical		pressor engine		catalyst			CO	47.04	206.02	1.18	5.15			
	Stack		13					VOC	1.74	7.62	0.28	1.22			
								PM10	0.27	1.18	0.27	1.18			
								SO2	0.008	0.036	0.008	0.036			
								Total HAPs	0.35	1.54	0.18	0.81			
								Formaldehyde	0.19	0.81	0.019	0.081			
								CO2e	2081	9113	1996	8744			

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit emissions are not typically considered to be fugitive and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugitive emission activities.

¹ Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.

² Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (ie., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).

³ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. **LIST** Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. **DO NOT LIST** H₂O, N₂O, O₂, and Noble Gases.

⁴ Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁵ Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁶ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

⁷ Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmv) are used. If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m³) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO₂, use units of ppmv (See 45CSR10).

Attachment J EMISSION POINTS DATA SUMMARY SHEET

			Table 2: Re	lease Paramete	er Data			
Emission	Inner		Exit Gas		Emission Point Ele	evation (ft)	UTM Coordinates	s (km)
Point ID No.	Diameter (ft.)	Temp. (°F)	Volumetric Flow ¹ (acfm) at operating conditions	Velocity (fps)	Ground Level (Height above mean sea level)	Stack Height ²	Northing	Easting
1E/1C	1.1	1223	8813	155	980	TBD	4,364.863	510.979
2E/2C	1.1	1223	8813	155	980	TBD	4,364.858	510.991
3E/3C	1.1	1223	8813	155	980	TBD	4,364.854	511.002
4E/4C	1.1	1223	8813	155	980	TBD	4,364.851	511.013
5E/5C	1.1	1223	8813	155	980	TBD	4,364.848	511.025
6E/6C	1.1	1223	8813	155	980	TBD	4,364.843	511.036
7E/7C	1.1	1223	8813	155	980	TBD	4,364.839	511.048
8E/8C	1.1	1223	8813	155	980	TBD	4,364.834	511.059
9E/9C	1.1	1223	8813	155	980	TBD	4,364.829	511.071
10E/10C	1.1	1223	8813	155	980	TBD	4,364.825	511.082
11E/11C	1.1	1223	8813	155	980	TBD	4,364.820	511.093
12E	0.5	535	4.0 kg/s mass flow	·	980	~11	4364.802	511.026
15E	0.75	350	530	20	980	~18	4364.801	510.984
18E	0.75	350	530	20	980	~18	4364.814	510.993
24E	0.5	225	47	4	980	~10	4364.802	511.026
25E	3	1030	2545	6	980	20	4364.819	510.975
26E/15C	1.1	1223	8813	155	980	TBD	4,364.816	511.104
27E/16C	1.1	1223	8813	155	980	TBD	4,364.812	511.115
Note: Points 13E a			4E and 17E are grouped into 15	E and 18E respective	ly. Points 19E-23E are sen	t to the VRUs in a closed	loop.	

¹ Give at operating conditions. Include inerts. ² Release height of emissions above ground level.

Attachment K. Fugitive Emissions Data Summary Sheet

Attachment K

FUGITIVE EMISSIONS DATA SUMMARY SHEET

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not typically considered to be fugitive, and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET.

Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

	APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS
1.)	Will there be haul road activities?
	Yes No
	If YES, then complete the HAUL ROAD EMISSIONS UNIT DATA SHEET.
2.)	Will there be Storage Piles?
	□ Yes
	☐ If YES, complete Table 1 of the NONMETALLIC MINERALS PROCESSING EMISSIONS UNIT DATA SHEET.
3.)	Will there be Liquid Loading/Unloading Operations?
	⊠ Yes □ No
	If YES, complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET.
4.)	Will there be emissions of air pollutants from Wastewater Treatment Evaporation?
	□ Yes
	If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
5.)	Will there be Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, open-ended valves, sampling connections, flanges, agitators, cooling towers, etc.)?
	⊠ Yes □ No
	If YES, complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS UNIT DATA SHEET.
6.)	Will there be General Clean-up VOC Operations?
	□ Yes
	If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
7.)	Will there be any other activities that generate fugitive emissions?
	🖾 Yes 🗌 No
	If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form.
	ou answered "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions nmary."

FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants ⁻ Chemical Name/CAS ¹	Maximum Uncontrolled		Maximum Po Controlled Em		Est. Method
	Chemical Name/CAS	lb/hr	ton/yr	lb/hr	ton/yr	Used ⁴
Haul Road/Road Dust Emissions Paved Haul Roads						
Unpaved Haul Roads	PM-10 PM-2.5	0.15 0.015	0.67 0.067	0.15 0.015	0.67 0.067	EE
Storage Pile Emissions						
Loading/Unloading Operations	VOCs Total HAPs CO2e	52.65 0.13 30.7	7.94 0.02 3.03	52.65 0.13 30.7	7.94 0.02 3.03	EE
Wastewater Treatment Evaporation & Operations						
Equipment Leaks	VOCs Total HAPs CO2e	1.03 0.020 24.36	4.53 0.087 107	1.03 0.020 24.36	4.53 0.087 107	EE
General Clean-up VOC Emissions						
Other – Venting Episodes	VOCs Total HAPs CO2e	Does not apply	11.46 0.19 778	Does not apply	11.46 0.19 778	EE

¹ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. DO NOT LIST H₂, H₂O, N₂, O₂, and Noble Gases.

² Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

³ Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁴ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

Attachment L. Emission Unit Data Sheets **Compressor Engines**

Source Identification Number ¹		1E		2	ЕE	3E		
Engine Manufacturer and Model		Waukesha, 7044 GSI		Waukesha, 7044 GSI		Waukesha, 7044 GSI		
Manufactu	Manufacturer's Rated bhp/rpm		o/1200 rpm	1680 bhp	/1200 rpm	1680 bhp/1200 rpm		
So	purce Status ²	Ν	/IS	Ν	1S	Ν	1S	
Date Installe	d/Modified/Removed ³	June	2016	June	2016	June	2016	
Engine Manufact	tured/Reconstruction Date4	T	BD	T	BD	TI	BD	
	l Stationary Spark Ignition to 40CFR60 Subpart JJJJ?	1	No	Γ	ło	Ν	lo	
	Engine Type ⁶	RI	B4S	RI	34S	RF	34S	
	APCD Type ⁷	NS	SCR	NS	SCR	NS	CR	
	Fuel Type ⁸	F	²Q	F	PQ	PQ		
Engine, Fuel and	H ₂ S (gr/100 scf)		0		0		0	
Combustion Data	Operating bhp/rpm	1674 bhp/1200 rpm		1674 bhp/1200 rpm		1674 bhp/1200 rpm		
Data	BSFC (Btu/bhp-hr)	8,267		8,267		8,267		
	Fuel throughput (ft ³ /hr)	11,820		11,820		11,820		
	Fuel throughput (MMft ³ /yr)	103.54		103.54		103.54		
	Operation (hrs/yr)	8,	760	8,760		8,760		
Reference9	Potential Emissions ¹⁰	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr	
MD	NOx	1.27	5.56	1.27	5.56	1.27	5.56	
MD	СО	1.18	5.15	1.18	5.15	1.18	5.15	
MD	VOC	0.28	1.22	0.28	1.22	0.28	1.22	
AP	SO_2	0.0082	0.036	0.0082	0.036	0.0082	0.036	
AP	PM_{10}	0.27	1.18	0.27	1.18	0.27	1.18	
MD	Formaldehyde	0.019	0.081	0.019	0.081	0.019	0.081	
MD	CO2e	1,996	8,744	1,996	8,744	1,996	8,744	

NATURAL GAS COMPRESSOR/GENERATOR ENGINE DATA SHEET

Source Ide	ntification Number ¹	4	4E 5E		Е	6	Έ
Engine Mar	Engine Manufacturer and Model		Waukesha, 7044 GSI		Waukesha, 7044 GSI		, 7044 GSI
Manufactu	Manufacturer's Rated bhp/rpm		1680 bhp/1200 rpm		/1200 rpm	1680 bhp/1200 rpm	
So	urce Status ²	Ν	AS	Ν	IS	Ν	1S
Date Installe	d/Modified/Removed ³	June	2016	June	2016	June	2016
Engine Manufact	ured/Reconstruction Date4	T	BD	TI	3D	TI	3D
Is this a Certified Stationary Spark Ignition Engine according to 40CFR60 Subpart JJJJ? (Yes or No) ⁵		Ν	No	Ν	lo	Ν	lo
	Engine Type ⁶	RI	34S	RE	84S	RE	34S
	APCD Type ⁷	NS	SCR	NS	CR	NS	CR
	Fuel Type ⁸	F	°Q	Р	Q	Р	Q
Engine, Fuel and	H ₂ S (gr/100 scf)		0)	0	
Combustion Data	Operating bhp/rpm	1674 bhp/1200 rpm		1674 bhp/1200 rpm		1674 bhp/1200 rpm	
Data	BSFC (Btu/bhp-hr)	8,267		8,267		8,267	
	Fuel throughput (ft ³ /hr)	11,820		11,820		11,820	
	Fuel throughput (MMft ³ /yr)	103.54		103.54		103.54	
	Operation (hrs/yr)	8,	760	8,760		8,7	760
Reference ⁹	Potential Emissions ¹⁰	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	NO _X	1.27	5.56	1.27	5.56	1.27	5.56
MD	СО	1.18	5.15	1.18	5.15	1.18	5.15
MD	VOC	0.28	1.22	0.28	1.22	0.28	1.22
AP	SO_2	0.0082	0.036	0.0082	0.036	0.0082	0.036
AP	PM_{10}	0.27	1.18	0.27	1.18	0.27	1.18
MD	Formaldehyde	0.019	0.081	0.019	0.081	0.019	0.081
MD	CO2e	1,996	8,744	1,996	8,744	1,996	8,744

Source Ide	ntification Number ¹	7	7E 8E		E	9	Έ
Engine Mar	Engine Manufacturer and Model		Waukesha, 7044 GSI		Waukesha, 7044 GSI		, 7044 GSI
Manufactu	Manufacturer's Rated bhp/rpm		1680 bhp/1200 rpm		/1200 rpm	1680 bhp/1200 rpm	
So	urce Status ²	Ν	4S	Ν	IS	Ν	1S
Date Installe	d/Modified/Removed ³	June	2016	June	2016	June	2016
Engine Manufact	ured/Reconstruction Date4	T	BD	TI	3D	TI	3D
Is this a Certified Stationary Spark Ignition Engine according to 40CFR60 Subpart JJJJ? (Yes or No) ⁵		Ν	No	Ν	lo	Ν	ło
	Engine Type ⁶	RI	34S	RI	34S	RE	34S
	APCD Type ⁷	NS	SCR	NS	CR	NS	CR
	Fuel Type ⁸	F	YQ	P	Q	Р	'Q
Engine, Fuel and	H ₂ S (gr/100 scf)		0		0	0	
Combustion Data	Operating bhp/rpm	1674 bhp/1200 rpm		1674 bhp/1200 rpm		1674 bhp/1200 rpm	
Data	BSFC (Btu/bhp-hr)	8,267		8,267		8,267	
	Fuel throughput (ft ³ /hr)	11,820		11,820		11,820	
	Fuel throughput (MMft ³ /yr)	103.54		103.54		103.54	
	Operation (hrs/yr)	8,	760	8,760		8,760	
Reference ⁹	Potential Emissions ¹⁰	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	NO _X	1.27	5.56	1.27	5.56	1.27	5.56
MD	СО	1.18	5.15	1.18	5.15	1.18	5.15
MD	VOC	0.28	1.22	0.28	1.22	0.28	1.22
AP	SO_2	0.0082	0.036	0.0082	0.036	0.0082	0.036
AP	PM_{10}	0.27	1.18	0.27	1.18	0.27	1.18
MD	Formaldehyde	0.019	0.081	0.019	0.081	0.019	0.081
MD	CO2e	1,996	8,744	1,996	8,744	1,996	8,744

Source Ide	entification Number ¹	-1 10E		11E		26E	
Engine Mar	Engine Manufacturer and Model		Waukesha, 7044 GSI		Waukesha, 7044 GSI		, 7044 GSI
Manufacturer's Rated bhp/rpm		1680 bhp	/1200 rpm	1680 bhp	/1200 rpm	1680 bhp/1200 rpm	
So	purce Status ²	Ν	1S	Ν	1S	Ν	IS
Date Installe	d/Modified/Removed ³	June	2016	June	2016	June	2016
Engine Manufact	ured/Reconstruction Date4	TI	BD	TI	3D	TI	3D
Is this a Certified Stationary Spark Ignition Engine according to 40CFR60 Subpart JJJJ? (Yes or No) ⁵		Ν	ło	Ν	ło	Ν	lo
	Engine Type ⁶	RI	34S	RI	34S	RE	34S
	APCD Type ⁷	NS	SCR	NS	CR	NS	CR
	Fuel Type ⁸	P	PQ	P	Q	PQ 0	
Engine, Fuel and	H ₂ S (gr/100 scf)		0		0		
Combustion Data	Operating bhp/rpm	1674 bhp/1200 rpm		1674 bhp/1200 rpm		1674 bhp/1200 rpm	
Data	BSFC (Btu/bhp-hr)	8,267		8,267		8,267	
	Fuel throughput (ft ³ /hr)	11,820		11,820		11,820	
	Fuel throughput (MMft ³ /yr)	103.54		103.54		103.54	
	Operation (hrs/yr)	8,7	760	8,760		8,760	
Reference ⁹	Potential Emissions ¹⁰	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	NOx	1.27	5.56	1.27	5.56	1.27	5.56
MD	СО	1.18	5.15	1.18	5.15	1.18	5.15
MD	VOC	0.28	1.22	0.28	1.22	0.28	1.22
AP	SO ₂	0.0082	0.036	0.0082	0.036	0.0082	0.036
AP	PM10	0.27	1.18	0.27	1.18	0.27	1.18
MD	Formaldehyde	0.019	0.081	0.019	0.081	0.019	0.081
MD	CO2e	1,996	8,744	1,996	8,744	1,996	8,744

Source Ide	ntification Number ¹	2	7E				
Engine Mar	nufacturer and Model	Waukesha, 7044 GSI					
Manufactu	rer's Rated bhp/rpm	1680 bhp	/1200 rpm				
So	urce Status ²	Ν	٧S				
Date Installe	d/Modified/Removed ³	June	2016				
	ured/Reconstruction Date4	T	BD				
Is this a Certified Engine according (Yes or No) ⁵	Stationary Spark Ignition to 40CFR60 Subpart JJJJ?	ľ	No				
	Engine Type ⁶	RI	B4S				
	APCD Type ⁷	NS	SCR				
. .	Fuel Type ⁸	F	PQ				
Engine, Fuel and	H ₂ S (gr/100 scf)		0				
Combustion Data	Operating bhp/rpm	1674 bhp/1200 rpm					
Data	BSFC (Btu/bhp-hr)	8,267					
	Fuel throughput (ft ³ /hr)	11,820					
	Fuel throughput (MMft ³ /yr)	10	3.54				
	Operation (hrs/yr)	8,	760				
Reference ⁹	Potential Emissions ¹⁰	lbs/hr	tons/yr	lbs/hr	tons/yr	lbs/hr	tons/yr
MD	NO _X	1.27	5.56				
MD	СО	1.18	5.15				
MD	VOC	0.28	1.22				
AP	SO_2	0.0082	0.036				
AP	PM10	0.27	1.18				
MD	Formaldehyde	0.019	0.081				
MD	CO2e	1,996	8,744				

1. Enter the appropriate Source Identification Number for each natural gas-fueled reciprocating internal combustion compressor/generator engine located at the compressor station. Multiple compressor engines should be designated CE-1, CE-2, CE-3 etc. Generator engines should be designated GE-1, GE-2, GE-3 etc. If more than three (3) engines exist, please use additional sheets.

- 2. Enter the Source Status using the following codes:
 - NS Construction of New Source (installation)
- ES **Existing Source**
- MS Modification of Existing Source
- RS Removal of Source
- 3. Enter the date (or anticipated date) of the engine's installation (construction of source), modification or removal.

- 4. Enter the date that the engine was manufactured, modified or reconstructed.
- 5. Is the engine a certified stationary spark ignition internal combustion engine according to 40CFR60 Subpart JJJJ. If so, the engine and control device must be operated and maintained in accordance with the manufacturer's emission-related written instructions. You must keep records of conducted maintenance to demonstrate compliance, but no performance testing is required. If the certified engine is not operated and maintained in accordance with the manufacturer's emission-related written instructions, the engine will be considered a non-certified engine and you must demonstrate compliance according to 40CFR§60.4243a(2)(i) through (iii), as appropriate.

Provide a manufacturer's data sheet for all engines being registered.

6. Enter the Engine Type designation(s) using the following codes:

7.

8.

	LB2S	Lean Burn Two Stroke	RB4S	Ri	ich Burn Four Stroke
	LB4S	Lean Burn Four Stroke			
	Enter the A	Air Pollution Control Device (APCD) type designation	on(s) usi	ng	the following codes:
	A/F	Air/Fuel Ratio	IR		Ignition Retard
	HEIS	High Energy Ignition System	SIF	PC	Screw-in Precombustion Chambers
	PSC	Prestratified Charge	LE	С	Low Emission Combustion
	NSCR	Rich Burn & Non-Selective Catalytic Reduction	SC	R	Lean Burn & Selective Catalytic Reduction
•	Enter the F	Fuel Type using the following codes:			
	PQ	Pipeline Quality Natural Gas	RG	ć	Raw Natural Gas
		• • •			
	Enter the	Potential Emissions Data Reference designation u	sing the	a fo	allowing codes. Attach all referenced data to

9. Enter the Potential Emissions Data Reference designation using the following codes. Attach all referenced data to this *Compressor/Generator Data Sheet(s)*.

MD	Manufacturer's Data	AP	AP-42	
GR	GRI-HAPCalc [™]	OT	Other	(please list)

10. Enter each engine's Potential to Emit (PTE) for the listed regulated pollutants in pounds per hour and tons per year. PTE shall be calculated at manufacturer's rated brake horsepower and may reflect reduction efficiencies of listed Air Pollution Control Devices. Emergency generator engines may use 500 hours of operation when calculating PTE. PTE data from this data sheet shall be incorporated in the *Emissions Summary Sheet*.



Underwood Compressor Station - Tyler County, West Virginia

			Gas Compression
ENGINE SPEED (rpm):	1200	NOx SELECTION (g/bhp-hr):	Customer Catalyst
DISPLACEMENT (in3):	7040	COOLING SYSTEM:	JW, IC + OC
COMPRESSION RATIO:	8:1	INTERCOOLER WATER INLET (°F):	130
IGNITION SYSTEM:	ESM	JACKET WATER OUTLET (°F):	180
EXHAUST MANIFOLD:	Water Cooled	JACKET WATER CAPACITY (gal):	100
COMBUSTION:	Rich Burn, Turbocharged	AUXILIARY WATER CAPACITY (gal):	11
ENGINE DRY WEIGHT (lbs):	24250	LUBE OIL CAPACITY (gal):	190
AIR/FUEL RATIO SETTING:	0.38% CO	MAX. EXHAUST BACKPRESSURE (in. H2O):	18
ENGINE SOUND LEVEL (dBA)	104	MAX. AIR INLET RESTRICTION (in. H2O):	15
		EXHAUST SOUND LEVEL (dBA)	111

SITE CONDITIONS:			
FUEL:	Commercial Quality Natural Gas	ALTITUDE (ft):	980
FUEL PRESSURE RANGE (psig):	30 - 60	MAXIMUM INLET AIR TEMPERATURE (°F):	100
FUEL HHV (BTU/ft3):	1,295.7	FUEL WKI:	58.9
FUEL LHV (BTU/ft3):	1,171.3		

SITE SPECIFIC TECHNICAL DATA		MAX RATING AT 100 °F		IG AT MAXIMUN PERATURE OF 1	
POWER RATING	UNITS	AIR TEMP	100%	75%	50%
CONTINUOUS ENGINE POWER	BHP	1674	1674	1260	843
OVERLOAD	% 2/24 hr	0	0	-	-
MECHANICAL EFFICIENCY (LHV)	%	30.8	30.8	29.3	28.6
CONTINUOUS POWER AT FLYWHEEL	BHP	1674	1674	1260	843
based on no auxiliary engine driven equipment					
FUEL CONSUMPTION					
FUEL CONSUMPTION (LHV)	BTU/BHP-hr	8267	8267	8686	8896
FUEL CONSUMPTION (HHV)	BTU/BHP-hr	9145	9145	9609	9841
FUEL FLOW based on fuel analysis LHV	SCFM	197	197	156	107
HEAT REJECTION					
JACKET WATER (JW)	BTU/hr x 1000	4131	4131	3428	2505
LUBE OIL (OC)	BTU/hr x 1000	570	570	521	430
INTERCOOLER (IC)	BTU/hr x 1000	266	266	185	92
EXHAUST	BTU/hr x 1000	4173	4173	3160	1928
RADIATION	BTU/hr x 1000	705	705	655	543
EMISSIONS (ENGINE OUT):					
NOx (NO + NO2)	g/bhp-hr	13.7	13.7	14.9	16.5
CO	g/bhp-hr	12.7	12.7	12.7	11.4
THC	g/bhp-hr	2.3	2.3	2.3	2.3
NMHC NM, NEHC	g/bhp-hr g/bhp-hr	0.98 0.47	0.98 0.47	0.94 0.45	0.76 0.37
CO2	g/bhp-hr	529	529	556	569
CO2e	g/bhp-hr	561	561	587	505 594
CH2O	g/bhp-hr	0.05	0.05	0.05	0.05
CH4	g/bhp-hr	1.30	1.30	1.25	1.01
	- · ·				
AIR INTAKE / EXHAUST GAS					
	SCFM	2534	2534	2004	1373
EXHAUST GAS MASS FLOW	lb/hr	11782	11782	9320	6384
EXHAUST GAS FLOW at exhaust temp, 14.5 psia EXHAUST TEMPERATURE	ACFM °F	8813 1223	8813 1223	6797 1181	4358 1076
	Г	1223	1223	1101	1076
HEAT EXCHANGER SIZING					
	BTU/hr x 1000	4685			
TOTAL AUXILIARY WATER CIRCUIT (IC + OC)	BTU/hr x 1000	947			
COOLING SYSTEM WITH ENGINE MOUNTED WATER PUMPS					
JACKET WATER PUMP MIN. DESIGN FLOW	GPM	450			
JACKET WATER PUMP MAX. EXTERNAL RESTRICTION	psig	16			
AUX WATER PUMP MIN. DESIGN FLOW	GPM	79			

44

psig

All data provided per the conditions listed in the notes section on page three. Data Generated by EngCalc Program Version 3.5.1 Dresser Inc. 10/8/2015 3:54 PM

AUX WATER PUMP MAX. EXTERNAL RESTRICTION

Underwood Compressor Station - Tyler County, West Virginia



FUEL COMPOSITION

HYDROCARBONS:		<u>/olume %</u>		FUEL:		Quality Natural Gas
Methane	CH4	75.469		FUEL PRESSURE F	₹ANGE (psig):	30 - 60
Ethane	C2H6	15.543		FUEL WKI:		58.9
Propane	C3H8	5.177				
Iso-Butane	I-C4H10	0.676		FUEL SLHV (BTU/ft	,	1150.92
Normal Butane	N-C4H10	1.475		FUEL SLHV (MJ/Nn	า3):	45.26
Iso-Pentane	I-C5H12	0.348				
Normal Pentane	N-C5H12	0.358		FUEL LHV (BTU/ft3)	,	1171.30
Hexane	C6H14	0.415		FUEL LHV (MJ/Nm3	3):	46.06
Heptane	C7H16	0				
Ethene	C2H4	0		FUEL HHV (BTU/ft3	·):	1295.69
Propene	C3H6	0		FUEL HHV (MJ/Nm	3):	50.95
	SUM HYDROCARBONS	99.461		FUEL DENSITY (SO	3):	0.74
NON-HYDROCARBONS:						
Nitrogen	N2	0.363		Standard Conditions per AS	3TM D3588-91 [60°F an	nd 14.696psia] and ISO
Oxygen	02	0		6976:1996-02-01[25, V(0;10		
Helium	He	0		Based on the fuel composit hydrocarbons may be prese		
Carbon Dioxide	CO2	0.162		in the fuel. The fuel must no		
Carbon Monoxide	CO	0		Waukesha recommends bo		
Hydrogen	H2	0		1) Dew point of the fuel gas		
Water Vapor	H2O	0		temperature of the gas at the 2) A fuel filter separator to be	•	•
	H20	0		natural gas.		ept commercial quality
	TOTAL FUEL	99.986		Refer to the 'Fuel and Lubri		
		00.000		Waukesha Application Eng fuels, or LHV and WKI* cal		r additional information on
				* Trademark of General Ele		
FUEL CONTAMINANTS			<i></i>	T . I O K . O		
Total Sulfur Compounds		0	% volume	Total Sulfur Comp		0 μg/BTU
Total Halogen as Cloride		0	% volume	Total Halogen as (Cloride	0 μg/BTU
Total Ammonia		0	% volume	Total Ammonia		0 µg/BTU
<u>Siloxanes</u>				Total Siloxanes (a	s Si)	0 μg/BTU
Tetramethyl silane		0	% volume			
Trimethyl silanol		0	% volume			
Hexamethyldisiloxane (L2)		0	% volume	Calculated fuel cont	aminant analysis	will depend on the
Hexamethylcyclotrisiloxane (D3)		0	% volume	entered fuel compos		-
Octamethyltrisiloxane (L3)		0	% volume	· · · · · · · · · · · · · · · · · · ·		0
Octamethylcyclotetrasiloxane (D4)		0	% volume			
Decamethyltetrasiloxane (L4)		0	% volume			
Decamethylcyclopentasiloxane (D	5)	0	% volume			
Dodecamethylpentasiloxane (L5)	,	0	% volume			
Dodecamethylcyclohexasiloxane (D6)	0	% volume			
Others	- /	0	% volume			
		0				

No water or hydrocarbon condensates are allowed in the engine. Requires liquids removal.

Underwood Compressor Station - Tyler County, West Virginia



NOTES

1. All data is based on engines with standard configurations unless noted otherwise.

2. Power rating is adjusted for fuel, site altitude, and site air inlet temperature, in accordance with ISO 3046/1 with tolerance of $\pm 3\%$.

3. Fuel consumption is presented in accordance with ISO 3046/1 with a tolerance of -0 / +5% at maximum rating. Fuel flow calculation based on fuel LHV and fuel consumption with a tolerance of -0/+5%. For sizing piping and fuel equipment, it is recommended to include the 5% tolerance.

5. Emission levels for engines with GE supplied 3-way catalyst are given at catalyst outlet flange. For all other engine models, emission levels are given at engine exhaust outlet flange prior to any after treatment. Values are based on a new engine operating at indicated site conditions, and adjusted to the specified timing and air/fuel ratio at rated load. Catalyst out emission levels represent emission levels the catalyst is sized to achieve. Manual adjustment may be necessary to achieve compliance as catalyst/engine age. Catalyst-out emission levels are valid for the duration of the engine warranty. Emissions are at an absolute humidity of 75 grains H2O/lb (10.71 g H2O/kg) of dry air. Emission levels may vary subject to instrumentation, measurement, ambient conditions, fuel quality, and engine variation. Engine may require adjustment on-site to meet emission values, which may affect engine performance and heat output. NOx, CO, THC, and NMHC emission levels are listed as a not to exceed limit, all other emission levels are estimated. CO2 emissions based on EPA Federal Register/Vol. 74, No. 209/Friday, October 30, 2009 Rules and Regulations 56398, 56399 (3) Tier 3 Calculation Methodology, Equation C-5.

6. Air flow is based on undried air with a tolerance of $\pm 7\%$.

7. Exhaust temperature given at engine exhaust outlet flange with a tolerance of \pm 75°F (42°C).

8. Exhaust gas mass flow value is based on a "wet basis" with a tolerance of $\pm 7\%$.

9. Inlet air restrictions based on full rated engine load. Exhaust backpressure based on 158 PSI BMEP and 1200 RPM. Refer to the engine specification section of Waukesha's standard technical data for more information.

10. Cooling circuit capacity, lube oil capacity, and engine dry weight values are typical.

11. Fuel must conform to Waukesha's "Gaseous Fuel Specification" S7884-7 or most current version. Fuel may require treatment to meet current fuel specification.

Heat exchanger sizing values given as the maximum heat rejection of the circuit, with applied tolerances and an additional 5% reserve factor.
 Fuel volume flow calculation in english units is based on 100% relative humidity of the fuel gas at standard conditions of 60°F and 14.696 psia

(29.92 inches of mercury; 101.325 kPa).

14. Fuel volume flow calculation in metric units is based on 100% relative humidity of the fuel gas at a combustion temperature of 25°C and metering conditions of 0°C and 101.325 kPa (14.696 psia; 29.92 inches of mercury). This is expressed as [25, V(0;101.325)].

15. Engine sound data taken with the microphone at 1 m (3.3 ft) from the side of the engine at the approximate front-to-back centerline. Microphone height was at intake manifold level. Engine sound pressure data may be different at front, back and opposite side locations. Exhaust sound data taken with microphone 1 meter (3.3 ft) away and 1 meter (3.3 ft) to the side of the exhaust outlet.

16. Due to variation between test conditions and final site conditions, such as exhaust configuration and background sound level, sound pressure levels under site conditions may be different than those tabulated above.

17. Cooling system design flow is based on minimum allowable cooling system flow. Cooling system maximum external restriction is defined as the allowable restriction at the minimum cooling system flow.

18. Continuous Power Rating: The highest load and speed that can be applied 24 hours per day, seven days per week, 365 days per year except for normal maintenance at indicated ambient reference conditions and fuel. No engine overload power rating is available.

19. emPact emission compliance available for entire range of operable fuels; however, fuel system and/or O2 set point may need to be adjusted in order to maintain compliance.

20. In cold ambient temperatures, heating of the engine jacket water, lube oil and combustion air may be required. See Waukesha Technical Data.

SPECIAL REQUIREMENTS

^{4.} Heat rejection tolerances are \pm 30% for radiation, and \pm 8% for jacket water, lube oil, intercooler, and exhaust energy.

Dehydrators

West Virginia Department of Environmental Protection

DIVISION OF AIR QUALITY : (304) 926-0475 WEB PAGE: http://www.wvdep.org

Division of Air Quality 40 CFR Part 63; Subpart HH & HHH Registration Form

Complete this form for any oil and natural gas production or natural gas transmission and storage facility that uses an affected unit under HH/HHH, whether subject or not.

Section A: Facility Description						
Affected facility actual annual average natural gas throughput (scf/day):176,000,000						
Affected facility actual annual average hydrocarbon liquid throughput: (bbl/day):195						
The affected facility processes, upgrades, or stores hydrocarbon liquids prior to custody transfer.	No					
The affected facility processes, upgrades, or stores natural gas prior to the point at which natural gas	No					
(NG) enters the NG transmission and storage source category or is delivered to the end user.						
The affected facility is: A prior to a NG processing plant a NG processing plant						
prior to the point of custody transfer and there is no NG processing plant						
	No					
distribution company or to a final end user (if there is no local distribution company).						
The affected facility exclusively processes, stores, or transfers black oil. Yes	6					
Initial producing gas-to-oil ratio (GOR):scf/bbl API gravity:degrees						
Section B: Dehydration Unit (if applicable) ¹]					
Description: Underwood Compressor Station Dehydrators (SV-3110 & SV-3210; FT-3110 & FT-3210; R-3	110					
& R-3210)						
Date of Installation:June 2016Annual Operating Hours:8,760Burner rating (MMbtu/hr):1.5						
Exhaust Stack Height (ft):TBDStack Diameter (ft):TBDStack Temp. (°F):TBD						
$Glycol Type: \square TEG \square EG \square Other:$						
Glycol Pump Type: Electric Gas If gas, what is the volume ratio?0.032ACFM/gpm						
Condenser installed? Xes No Exit Temp. 200_ °F Condenser Pressure _0psig						
Incinerator/flare installed? Xes No Destruction Eff98%						
Other controls installed? Yes No Describe:						
Wet Gas ² : Gas Temp.: _120_°F Gas Pressure _1,100 psig						
(Upstream of Contact Tower) Saturated Gas? Yes No If no, water content lb/MMSCF						
Dry Gas: Gas Flowrate(MMSCFD) Actual Design88 each						
(Downstream of Contact Tower) Water Content5.0lb/MMSCF						
Lean Glycol: Circulation rate (gpm) Actual ³ TBD Maximum ⁴ 7.9						
Pump make/model: Kimray 45015PV						
Glycol Flash Tank (if applicable): Temp.: <u>80</u> °F Pressure <u>5</u> psig Vented? Yes No						
If no, describe vapor control: Vent gas used in reboiler as fuel and as a backup would ge	o to					
the VRU system via the storage tanks						
Stripping Gas (if applicable): Source of gas: Dry gas, if used Rate _9 scfm						

 applicant provide th accomplished by su more detailed inform 2. Extended gas analysy Association (GPA) entrained liquids fro EPA Method TO-14 	 applicant provide this level of detail for all sources. The level of detail that is necessary is to establish where the custody transfer points are located. This can be accomplished by submitting a process flow diagram indicating custody transfer points and the natural gas flow. However, the DAQ reserves the right to request more detailed information in order to make the necessary decisions. 2. Extended gas analysis from the Wet Gas Stream including mole percents of C₁-C₈, benzene, ethylbenzene, toluene, xylene and n-Hexane, using Gas Processors Association (GPA) 2286 (or similar). A sample should be taken from the inlet gas line, downstream from any inlet separator, and using a manifold to remove entrained liquids from the sample and a probe to collect the sample from the center of the gas line. GPA standard 2166 reference method or a modified version of EPA Method TO-14, (or similar) should be used. 							
	s of gas or hydrocarbon flow rate.							
	Section C: Facility NESHAPS Subpart HH/HHH status							
	Subject to Subpart HH - applies, but is exempt through < 1 tpy benzene exemption							
Affected facility	Subject to Subpart HHH							
status:	\square Not Subject \square < 10/25 TPY							
(choose only one)	because: Affected facility exclusively handles black oil							
	\Box The facility wide actual annual average NG throughput is < 650 thousand							
	scf/day and facility wide actual annual average hydrocarbon liquid is < 250 bpd							
	No affected source is present							

NATURAL GAS GLYCOL DEHYDRATION UNIT DATA SHEET

		Manufact	urer and Model	T	BD
		Max Dry Gas Flow Rate (MMscf/day)		88	
		Design Heat	Input (MMBtu/hr)	1.5	
		Design Typ	be (DEG or TEG)	T	EG
	l Glycol	Sou	rce Status ²	Ν	4S
	tion Unit ata	Date Installed/	Modified/Removed ³	June	2016
		Regenerator	Still Vent APCD ⁴	F	FL
		Fuel H	IV (Btu/scf)	1,	174
		H ₂ S Cont	ent (gr/100 scf)		0
		Opera	tion (hrs/yr)	8,	760
Source ID #1	Vent	Reference ⁵	Potential Emissions ⁶	lbs/hr	tons/yr
		AP	NO _X	0.18	0.81
	Reboiler Vent	AP	СО	0.15	0.68
15E		AP	VOC	0.010	0.044
		AP	SO ₂	0.0011	0.0048
		AP	PM ₁₀	0.014	0.061
	Glycol Regenerator Still Vent	GRI-GLYCalc [™]	VOC	0.32	1.39
		GRI-GLYCalc TM	Benzene	0.0053	0.023
13E		GRI-GLYCalc [™]	Ethylbenzene	0.021	0.090
1512		GRI-GLYCalc [™]	Toluene	0.023	0.10
		GRI-GLYCalc [™]	Xylenes	0.089	0.39
		GRI-GLYCalc [™]	n-Hexane	0.0048	0.021
		GRI-GLYCalc [™]	VOC	0.65	2.83
14E		GRI-GLYCalc TM	Benzene	0.0004	0.0019
	Flash Gas	GRI-GLYCalc [™]	Ethylbenzene	0.0005	0.0022
ITL	Tank Vent	GRI-GLYCalc TM	Toluene	0.0011	0.0049
		GRI-GLYCalc [™]	Xylenes	0.0014	0.0061
		GRI-GLYCalc [™]	n-Hexane	0.010	0.044

		Manufact	urer and Model	TE	BD
		Max Dry Gas Flow Rate (mmscf/day)		88	
		Design Heat	Input (mmBtu/hr)	1.5	
		Design Typ	e (DEG or TEG)	TE	ĒG
	l Glycol	Sour	rce Status ²	М	IS
•	tion Unit ata	Date Installed/	Modified/Removed ³	June	2016
		Regenerator	Still Vent APCD ⁴	F	L
		Fuel H	IV (Btu/scf)	1,1	74
		H ₂ S Cont	ent (gr/100 scf)	()
		Opera	tion (hrs/yr)	8,7	60
Source ID #1	Vent	Reference ⁵	Potential Emissions ⁶	lbs/hr	tons/yr
		AP	NO _X	0.18	0.81
	Reboiler Vent	AP	СО	0.15	0.68
18E		AP	VOC	0.010	0.044
		AP	SO_2	0.0011	0.0048
		AP	PM ₁₀	0.014	0.061
		GRI-GLYCalc [™]	VOC	0.32	1.39
		GRI-GLYCalc [™]	Benzene	0.0053	0.023
16E	Glycol Regenerator Still Vent	GRI-GLYCalc [™]	Ethylbenzene	0.021	0.090
TOL		GRI-GLYCalc [™]	Toluene	0.023	0.10
		GRI-GLYCalc [™]	Xylenes	0.089	0.39
		GRI-GLYCalc [™]	n-Hexane	0.0048	0.021
		GRI-GLYCalc [™]	VOC	0.65	2.83
17E		GRI-GLYCalc [™]	Benzene	0.0004	0.0019
	Flash Gas	GRI-GLYCalc [™]	Ethylbenzene	0.0005	0.0022
	Tank Vent	GRI-GLYCalc [™]	Toluene	0.0011	0.0049
		GRI-GLYCalc [™]	Xylenes	0.0014	0.0061
		GRI-GLYCalc TM	n-Hexane	0.010	0.044

1. Enter the appropriate Source Identification Numbers for the glycol dehydration unit Reboiler Vent and glycol Regenerator Still Vent. The glycol dehydration unit Reboiler Vent and glycol Regenerator Still Vent should be designated RBV-1 and RSV-1, respectively. If the compressor station incorporates multiple glycol dehydration units, a Glycol Dehydration Unit Data Sheet shall be completed for each, using Source Identification #s RBV-2 and RSV-2, RBV-3 and RSV-3, etc.

- 2. Enter the Source Status using the following codes:
 - NS Construction of New Source MS
- ES **Existing Source**
- Modification of Existing Source
- RS Removal of Source

- 3. Enter the date (or anticipated date) of the glycol dehydration unit's installation (construction of source), modification or removal.
- 4. Enter the Air Pollution Control Device (APCD) type designation using the following codes:

5	-	None Flare Thermal Oxidizer		Condenser Condenser/Combustion Combination
э.	Enter the Pot	ential Emissions Data Reference designation	on using the	e following codes:
	MD	Manufacturer's Data	AP	AP-42

- $\begin{array}{cccc} MD & Manufacturer's Data & AP & AP-42 \\ GR & GRI-GLYCalc^{TM} & OT & Other _____ (please list) \end{array}$
- 6. Enter the Reboiler Vent and glycol Regenerator Still Vent Potential to Emit (PTE) for the listed regulated pollutants in lbs per hour and tons per year. The glycol Regenerator Still Vent potential emissions may be determined using the most recent version of the thermodynamic software model GRI-GLYCalcTM (Radian International LLC & Gas Research Institute). Attach all referenced Potential Emissions Data (or calculations) and the GRI-GLYCalc Aggregate Calculations Report to this Glycol Dehydration Unit Data Sheet(s). This PTE data shall be incorporated in the Emissions Summary Sheet.

Include a copy of the GRI-GLYCalcTM analysis. This includes a printout of the aggregate calculations report, which shall include emissions reports, equipment reports, and stream reports.

*An explanation of input parameters and examples, when using GRI-GLYCalcTM is available on our website.

Bulk Loading and Fugitives

Attachment L EMISSIONS UNIT DATA SHEET CHEMICAL PROCESS

	r chemical processes please fill out to plementary forms that have been o	this sheet and all supplementary forms (completed.	(see below) that apply. Please check all			
	Emergency Vent Summary Sheet Leak Sources Data Sheet Toxicology Data Sheet Reactor Data Sheet Distillation Column Data Sheet					
1.	Chemical process area name and Piping for Entire Facility. Piping n	equipment ID number (as shown in Equipment form.	quipment List Form)			
2.	Standard Industrial Classification 4923	Codes (SICs) for process(es)				
3.	List raw materials and 🗌 attach M Wet Natural Gas	4SDSs				
4.	List Products and Maximum Products	uction and 🗌 attach MSDSs				
De	scription and CAS Number	Maximum Hourly (lb/hr)	Maximum Annual (ton/year)			
	Dry Natural Gas	7.33 MMscf/hour	64,240 MMscf/year			
	Condensate	6.25 barrels/hour	54,750 barrels/year			
	Produced Water	1.875 barrels/hour	16,425 barrels/year			
5.	Complete the Emergency Vent Su	ummary Sheet for all emergency relief of	levices.			
6.						
7.	 Clearly describe below or attach to application Accident Procedures to be followed in the event of an accidental spill or release. TBD – Will reference Spill Prevention, Control and Countermeasure (SPCC) plan once developed and approved. 					

sheets (MSDS chemical entity sheet is not teratogenicity, unknown, and 8B. Describe any conducted by t in the environn	 A. Complete the <i>Toxicology Data Sheet</i> or attach to application a toxicology report (an up-to-date material safety data sheets (MSDS) may be used) outlining the currently known acute and chronic health effects of each compound or chemical entity emitted to the air. If these compounds have already been listed in Item 3, then a duplicate MSDS sheet is not required. Include data such as the OSHA time weighted average (TWA) or mutagenicity, teratogenicity, irritation, and other known or suspected effects should be addressed. Indicate where these are unknown, and provide references. B. Describe any health effects testing or epidemiological studies on these compounds that are being or may be conducted by the company or required under TSCA, RCRA or other federal regulations. Discuss the persistence in the environment of any emission (e.g. pesticides, etc.). 						
	cts - waste products status	s: (If source is subject to RCRA or 450 Q at (304) 926-3647.)	USR25, please contact the				
9A. Types and am	ounts of wastes to be dispos	sed:					
9B. Method of disp Carrier:	osal and location of waste d	isposal facilities: Phone:					
9C. Check here if a	approved USEPA/State Haza	ardous Waste Landfill will be used 🗌					
10. Maximum and	Projected Typical Operating	Schedule for process or project as a who	ble (circle appropriate units).				
circle units:	(hrs/day) hr/batch)	(days), (batches/day), (batches/week)	(days/yr), (weeks/year)				
10A. Maximum	24	7	52				
10B. Typical	24	7	52				
11. Complete a Re	eactor Data Sheet for each re	eactor in this chemical process.					
12. Complete a Di	stillation Column Data Sheel	t for each distillation column in this chem	ical process.				
Please propos		Reporting, and Testing , and reporting in order to demonstrate co ting in order to demonstrate compliance v					
MONITORING		RECORDKEEPING					
see Attachment C)	see Attachment O					
REPORTING		TESTING					
see Attachment C)	see Attachment O					
MONITORING. Please list and describe the process parameters and ranges that are proposed to be monitored in order to demonstrate compliance with the operation of this process equipment operation or air pollution control device. RECORDKEEPING. Please describe the proposed recordkeeping that will accompany the monitoring.							
REPORTING. Please describe the proposed frequency of reporting of the recordkeeping.							
TESTING. Please	TESTING. Please describe any proposed emissions testing for this process equipment or air pollution control device.						

LEAK SOURCE DATA SHEET

Source Category	Pollutant	Number of Source Components ¹	Number of Components Monitored by Frequency ²	Average Time to Repair (days) ³	Estimated Annual Emission Rate (Ib/yr) ⁴
Pumps⁵	light liquid VOC ^{6,7}				
	heavy liquid VOC ⁸				
	Non-VOC ⁹				
Valves ¹⁰	Gas VOC	250	TBD	1	4,576 – EE
	Light Liquid VOC	42	TBD	1	1,486 – EE
	Heavy Liquid VOC				
	Non-VOC				
Safety Relief Valves ¹¹	Gas VOC				
	Non VOC				
Open-ended Lines ¹²	VOC				
	Non-VOC				
Sampling Connections ¹³	VOC				
	Non-VOC				
Compressors	VOC	39	TBD	1	1,396 – EE
	Non-VOC				
Flanges	Gas VOC	836	TBD	1	1,326 – EE
	Light Liquid VOC	175	TBD	1	272 – EE
	Non-VOC				
Other	VOC				
	Non-VOC				

¹⁻¹³ See notes on the following page.

Attachment L EMISSIONS UNIT DATA SHEET GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form): Fugitive so no number assigned

1. Name or type and model of proposed affected source:
Fugitive emissions from venting episodes such as plant shutdowns and compressor start ups/shut downs.
 On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.
3. Name(s) and maximum amount of proposed process material(s) charged per hour:
4. Name(s) and maximum amount of proposed material(s) produced per hour:
- compressor blowdown - 0.059 tons VOC per event, 3.99 tons CO2e per event
- compressor startup - 0.006 tons VOC per event, 0.42 tons CO2e per event
- plant shutdown - 0.59 tons VOC per event, 39.88 tons CO2e per event
- pigging venting - 0.006 tons VOC per event, 0.40 tons CO2e per event
C. One chamical reactions if annihophic that will be involved in the concertion of singelly texter.
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:
none
The identification number which appears here must correspond to the air pollution control device

* The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

6.	6. Combustion Data (if applicable):						
	(a) Type and amount in appropriate units of fuel(s) to be burned:						
	(h)	<u>Oh anaia</u>					
	(D)	and ash		oposed fuei(s), e	excluding coal, ir	icluding maxim	um percent sulfur
	(c)	Theoreti	ical combustion	air requirement	(ACF/unit of fue	el):	
			@		°F and		psia.
	(d)	Percent	excess air:				
	(e)	Type an	d BTU/hr of bu	rners and all othe	er firing equipme	ent planned to b	be used:
	(f)	If coal is	proposed as a twill be fired:	source of fuel, id	dentify supplier a	and seams and	give sizing of the
			a wiii be fired.				
	(g)	Propose	ed maximum de	sign heat input:			× 10 ⁶ BTU/hr.
7.	Pro	jected or	perating schedu	ıle:			
Hc	ours/		not a regular schedule	Days/Week	not a regular schedule	Weeks/Year	not a regular schedule

8.	8. Projected amount of pollutants that would be emitted from this affected source if no control devices were used:					
@	@ venting events are uncontrolled °F and psia					
a.	NOx	lb/hr	grains/ACF			
b.	SO ₂	lb/hr	grains/ACF			
c.	со	lb/hr	grains/ACF			
d.	PM ₁₀	lb/hr	grains/ACF			
e.	Hydrocarbons	lb/hr	grains/ACF			
f.	VOCs	variable based on event lb/hr	grains/ACF			
g.	Pb	lb/hr	grains/ACF			
h.	Specify other(s)					
		lb/hr	grains/ACF			
		lb/hr	grains/ACF			
		lb/hr	grains/ACF			
		lb/hr	grains/ACF			

- NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.
 - (2) Complete the Emission Points Data Sheet.

	and reporting in order to demonstrate compliance Please propose testing in order to demonstrate
REPORTING	TESTING
see Attachment O	see Attachment O
	IE PROCESS PARAMETERS AND RANGES THAT ARE ISTRATE COMPLIANCE WITH THE OPERATION OF THIS CONTROL DEVICE.
RECORDKEEPING. PLEASE DESCRIBE THE PROP MONITORING.	POSED RECORDKEEPING THAT WILL ACCOMPANY THE
REPORTING. PLEASE DESCRIBE THE PRORECORDKEEPING.	OPOSED FREQUENCY OF REPORTING OF THE
TESTING. PLEASE DESCRIBE ANY PROPOSED EMI POLLUTION CONTROL DEVICE.	ISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR
	nance procedures required by Manufacturer to
maintain warranty N/A	

Attachment M. Air Pollution Control Device Sheets **NSCR Catalysts**

Attachment M Air Pollution Control Device Sheet (OTHER COLLECTORS)

Control Device ID No. (must match Emission Units Table): 1C – 11C, 15C, & 16C

Equipment Information

	Manufacturer: EMIT Technologies2.Control Device Name: 1C - 11C, 15C & 16C - Catalysts for C-2100 through C-2220 Type: NSCR Catalyst					
	ovide diagram(s) of unit describing capture synaptication of movers. If applicable, sta					
4. On	a separate sheet(s) supply all data and calcula	tions used in selecting or de	esigning this collection device.			
5. Pro	ovide a scale diagram of the control device show	ving internal construction.				
6. Sub	bmit a schematic and diagram with dimensions	and flow rates.				
	aranteed minimum collection efficiency for each to capture of pollutants	pollutant collected:				
8. Atta	ached efficiency curve and/or other efficiency in	formation.				
9. Des	sign inlet volume: 8,813 ACFN	1 10. Capacity:				
N/A 12. Atta con 13. Des	11. Indicate the liquid flow rate and describe equipment provided to measure pressure drop and flow rate, if any.					
	Gas Stream	Characteristics				
Are	4. Are halogenated organics present? □ Yes No Are particulates present? □ Yes □ No Are metals present? □ Yes □ No					
15. Inle	et Emission stream parameters:	Maximum	Typical			
	Pressure (mmHg): Not specified					
	Heat Content (BTU/scf):	1,400	1,175			
	Oxygen Content (%):	Not specified				
	Moisture Content (%):	Not specified				
	Relative Humidity (%): Not specified					

16.	Type of pollutant(s) of Particulate (type):		SOx	☐ Odor ⊠ Other NOx,	, CO, VOC, HCI	HO, CH4		
17.	Inlet gas velocity:	1	55 ft/sec	18. Pollutant s	specific gravity:			
19.	Gas flow into the coll 8,813 ACF @		20. Gas strea	tream temperature: Inlet: 1,223 °F Outlet: 1,223 °F				
21.	Gas flow rate: Design Maximum: Average Expected:	8,813 TBD	3 ACFM ACFM	22. Particulate	e Grain Loading Inlet: Outlet:	in grains/scf: N	√/A	
23.	Emission rate of eac	h pollutant (speci	fy) into and out	of collector:				
	Pollutant	IN Poll	utant	Emission	ollutant	Control		
		lb/hr	grains/acf	Capture Efficiency %	lb/hr	grains/acf	Efficiency %	
	A NOx	50.74			1.27		97.5	
	B CO	47.04			1.18		97.5	
					1:10			
	C VOC	1.74			0.28		84	
	C VOC D HCHO						84 90	
		1.74			0.28		- ·	
24.	D HCHO	1.74 0.19 4.81	nt TBD		0.28 0.019	eter 1.10	90 70	

Particulate Distribution

26. Complete the table:	Particle Size Distribution at Inlet to Collector	Fraction Efficiency of Collector
Particulate Size Range (microns)	Weight % for Size Range	Weight % for Size Range
0 – 2		
2-4		
4 - 6		
6 - 8		
8 – 10		
10 – 12		
12 – 16		
16 – 20		
20 - 30		
30 - 40		
40 – 50		
50 - 60		
60 - 70		
70 – 80		
80 - 90		
90 – 100		
>100		

27.	Describe	any a	air pollution	control	device	inlet	and	outlet	gas	conditioning	processes	(e.g.,	gas	cooling,	gas
	reheating	, gas	humidificati	ion): Nor	ne										

28. Describe the collection material disposal system: Catalyst elements can be cleaned and/or replaced; materials are not disposed on site.

29. Have you included Other Collectores Control Device in the Emissions Points Data Summary Sheet? yes

Please propose n	ig parameters. Please propose	and Testing eporting in order to demonstrate compliance with the testing in order to demonstrate compliance with the
MONITORING: see At	tachment O	RECORDKEEPING: see Attachment O
REPORTING: see Atta	achment O	TESTING: see Attachment O
MONITORING:	monitored in order to demons	ocess parameters and ranges that are proposed to be strate compliance with the operation of this process
RECORDKEEPING: REPORTING:	Please describe any proposed	cordkeeping that will accompany the monitoring. emissions testing for this process equipment on air
TESTING:	pollution control device. Please describe any proposed pollution control device.	emissions testing for this process equipment on air
	aranteed Control Efficiency for eac	
Due to variable loa typical based on e	expected operating conditions. Th	4: 70%. Icy may vary. The catalyst efficiencies listed above are le emission factors shown on the catalyst specification r the percent control efficiencies will be the same.
32. Manufacturer's Gu	aranteed Control Efficiency for eac	h air pollutant.
Inlet temperature rang controller must be set than 0.5 wt% sulfated a	ge is 750 F – 1250 F. Engine m properly with fuel heating value of ash. Catalyst must not be exposed	edures required by Manufacturer to maintain warranty. hust be operated between 50 – 100 % load. A/F ratio around 1400 Btu/scf. Engine lube oil shall contain less d to the following: antimony, arsenic, chromium, copper, ous, potassium, silicon, sodium, sulfur, tin, zinc.



QUOTE: QUO-17302-L3Z6

Prepared For: Clayton Brown ANTERO RESOURCES

INFORMATION PROVIDED BY WAUKESHA

Engine:	L7044GSI
Horsepower:	1680
RPM:	1200
Compression Ratio:	8.0
Exhaust Flow Rate:	8820 CFM
Exhaust Temperature:	1226 °F
Reference:	N/A
Fuel:	Natural Gas
Annual Operating Hours:	8760

Uncontrolled Emissions

	<u>g/bhp-hr</u>	<u>Lb/Hr</u>	<u>Tons/Year</u>
NOx:	13.50	50.00	219.00
CO:	12.50	46.30	202.78
THC:	2.30	8.52	37.31
NMHC	0.90	3.33	14.60
NMNEHC:	0.48	1.78	7.79
HCHO:	0.05	0.19	0.81
O2:	0.30 %		

POST CATALYST EMISSIONS

	% Reduction
NOx:	>97.5%
CO:	>97.5%
VOC:	>84.0%
HCHO:	>90.0%
CH4:	>70.0%

CONTROL EQUIPMENT

Catalyst Element

Model:	RT-3615-T
Catalyst Type:	NSCR, Stan
Substrate Type:	BRAZED
Manufacturer:	EMIT Techn
Element Quantity:	6
Element Size:	Rectangle 3

RT-3615-T NSCR, Standard Precious Group Metals BRAZED EMIT Technologies, Inc 6 Rectangle 36" x 15" x 3.5"

The information in this quotation, and any files transmitted with it, is confidential and may be legally privileged. It is intended only for the use of individual(s) within the company named above. If you are the intended recipient, be aware that your use of any confidential or personal information may be restricted by state and federal privacy laws



WARRANTY

EMIT Technologies, Inc. warrants that the goods supplied will be free from defects in workmanship by EMIT Technologies, Inc. for a period of two (2) years from date of shipment. EMIT Technologies, Inc. will not be responsible for any defects which result from imprope use, neglect, failure to properly maintain or which are attributable to defects, errors or omissions in any drawings, specifications, plans or descriptions, whether written or oral, supplied to EMIT Technologies, Inc. by Buyer.

Catalyst performance using an EMIT Air/Fuel ratio controller is dependent upon properly defined set-points, variable with engine and fuel gas composition. Air/fuel ratio controller performance is guaranteed, but not limited, to fuel gas with a HHV content of 1400 BTU/SCF.

Catalyst performance will be guaranteed for a period of 1 year from installation, or 8760 operating hours, whichever comes first. The catalyst shall be operated with an automatic air/fuel ratio controller. The performance guarantee shall not cover the effects of excessive ash masking due to operation at low load, improper engine maintenance, or inappropriate lubrication oil. The performance guarantee shall not cover the effects of continuous engine misfires (cylinder or ignition) exposing the catalyst be excessive exothermic reaction temperatures. In most cases, excluding thermal deactivation, catalyst performance is redeemable by means of proper washing (refer to EMIT Catalyst/Silencer Housing Manual for element wash information, or contact a local EMIT Sales representative).

The exhaust temperature operating range at the converter inlet is a minimum of 600°F for oxidation catalyst and 750 °F for NSCR catalyst, and a maximum of 1250°F.

If a properly functioning, high temperature shut down switch is not installed, thermal deactivation of catalyst at sustained temperatures above 1250°F is not covered. If excessive exposure to over oxygenation of NSCR catalyst occurs due to improperly functioning or non-existent Air/Fuel ratio control, then deactivation of catalyst is not warranted.

The catalyst conversion efficiencies (% reduction) will be guaranteed for engine loads of 50 to 100 percent. Standard Oxidation Catalyst conversion efficiencies (% reduction) will be guaranteed for fuel gas containing less than 1.5% mole fraction of non-methane, nonethane hydrocarbons. Applications where fuel gas exceeds this level will require a Premium Oxidation Catalyst to maintain guaranteed VOC conversion efficiencies.

Engine lubrication oil shall contain less than 0.5 wt% Sulfated Ash with a maximum allowable specific oil consumption of 0.7 g/bhp-hr. The catalyst shall be limited to a maximum ash loading of 0.022 lb/ft3. Phosphorous and zinc additives are limited to 0.03 wt%. New or Reconstructed engines must operate for a minimum of 50 hours prior to catalyst installation, otherwise the warranty is void.

The catalyst must not be exposed to the following know poisoning agents, including: antimony, arsenic, chromium, copper, iron, lead, lithium, magnesium, mercury, nickel, phosphorous, potassium, silicon, sodium, sulfur, tin, and zinc. Total poison concentrations in the fuel gas must be limited to 0.25 ppm or less for catalyst to function properly.

Shipment - Promised shipping dates are approximate lead times from the point of manufacture and are not guaranteed. EMIT Technologies, Inc. will not be liable for any loss, damage or delay in manufacture or delivery resulting from any cause beyond its control including, but not limited to a period equal to the time lost by reason of that delay. All products will be crated as per best practice to prevent any damage during shipment. Unless otherwise specified, Buyer will pay for any special packing and shipping requirements. Acceptance of goods by common carrier constitutes delivery to Buyer. EMIT Technologies, Inc. shall not be responsible for goods damaged or lost in transit.

Terms: Credit is extended to purchaser for net 30 time period. If payment is not received in the net 30 timeframe, interest on the unpaid balance will accrue at a rate of 1.5% per month from the invoice date.

Order Cancellation Terms: Upon cancellation of an order once submittal of a Purchase Order has occurred, the customer will pay a 25% restocking fee for Catalyst Housings, Catalyst Elements, and Air/Fuel Ratio Controllers; 50% restocking fee for Cooler Top Solutions Exhaust System Accessories, and other Custom Built Products; 100% of all associated shipping costs incurred by EMIT; 100% of all project expenses incurred by EMIT for Field Services.

Attachment N. Supporting Emissions Calculations

Emission Calculations

Emissions Summary Total

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia

UNCONTROLLED POTENTIAL EMISSION SUMMARY

Courses	NOx		C	:0	VOC		S	0 ₂	PN	-10	HAPs		Formaldehyde		CO ₂ e
Source	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	tpy
Engines															
Compressor Engine 1	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 2	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 3	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 4	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 5	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 6	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 7	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 8	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 9	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 10	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 11	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 12	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Compressor Engine 13	50.74	222.24	47.04	206.02	1.74	7.62	0.008	0.04	0.27	1.18	0.35	1.54	0.19	0.81	9,113
Turbines															
Microturbine Generator 1	0.24	1.05	0.66	2.89	0.06	0.26	0.02	0.09	0.04	0.18	0.006	0.03	0.004	0.02	3,499
Catalytic Heater for Generator Fuel	0.003	0.01	0.002	0.01	0.0002	0.0007	0.00002	0.00008	0.0002	0.001	0.00006	0.0002	0.000002	0.00001	12
Dehydrators															
TEG Dehydrator Still Vent 1					15.90	69.65					7.18	31.43			1,910
TEG Dehydrator Still Vent 2					15.90	69.65					7.18	31.43			1,910
TEG Dehydrator Flash Tank 1					32.28	141.39					0.68	2.96			5,988
TEG Dehydrator Flash Tank 2					32.28	141.39					0.68	2.96			5,988
Reboiler 1	0.18	0.81	0.15	0.68	0.01	0.04	0.001	0.005	0.01	0.06	0.003	0.02	0.0001	0.0006	771
Reboiler 2	0.18	0.81	0.15	0.68	0.01	0.04	0.001	0.005	0.01	0.06	0.003	0.02	0.0001	0.0006	771
<u>Combustors</u>															
Flare and Pilot															
Hydrocarbon Loading															
Truck Loadout					52.65	7.94					0.13	0.020			3
Fugitive Emissions															
Component Leak Emissions					1.03	4.53					0.02	0.09			107
Venting Emissions						11.46						0.19			778
Haul Road Dust Emissions									0.15	0.67					
Storage Tanks															
Produced Water Tanks					0.0002	0.0008					6.77E-08	2.97E-07			0.02
Settler Tank					128.90	564.59					3.94	17.25			1,427
Condensate Tanks					3.11	13.64					0.008	0.03			4
Total Facility PTE =	660.24	2,891.85	612.45	2,682.54	304.77	1,123.70	0.13	0.57	3.73	16.32	24.36	106.44	2.41	10.56	141,636

Emissions Summary Total

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia

CONTROLLED POTENTIAL EMISSION SUMMARY

Source	NOx		C	0	V	00	S	0 ₂	PN	1-10	HAPs		Formaldehyde		CO ₂ e
Source	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	tpy
Engines															
Compressor Engine 1	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 2	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 3	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 4	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 5	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 6	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 7	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 8	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 9	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 10	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 11	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 12	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
Compressor Engine 13	1.27	5.56	1.18	5.15	0.28	1.22	0.008	0.04	0.27	1.18	0.18	0.81	0.02	0.08	8,744
<u>Turbines</u>															
Microturbine Generator 1	0.24	1.05	0.66	2.89	0.06	0.26	0.02	0.09	0.04	0.18	0.006	0.03	0.004	0.02	3,499
Catalytic Heater for Generator Fuel	0.003	0.01	0.002	0.01	0.0002	0.0007	0.00002	0.00008	0.0002	0.001	0.00006	0.0002	0.000002	0.00001	12
Dehydrators															
TEG Dehydrator Still Vent 1															
TEG Dehydrator Still Vent 2															
TEG Dehydrator Flash Tank 1															
TEG Dehydrator Flash Tank 2															
Reboiler 1	0.18	0.81	0.15	0.68	0.66	2.87	0.001	0.005	0.01	0.06	0.02	0.07	0.0001	0.0006	895
Reboiler 2	0.18	0.81	0.15	0.68	0.66	2.87	0.001	0.005	0.01	0.06	0.02	0.07	0.0001	0.0006	895
Combustion															
Flare and Pilot	0.63	2.75	2.86	12.51	0.64	2.79	0.00001	0.00004	0.0001	0.0005	0.29	1.26			4,822
Hydrocarbon Loading															
Truck Loadout					52.65	7.94					0.13	0.020			3
Fugitive Emissions															
Component Leak Emissions					1.03	4.53					0.02	0.09			107
Venting Emissions						11.46						0.19			778
Haul Road Dust Emissions									0.15	0.67					
Storage Tanks															
Produced Water Tanks					0.000003	0.00002					1.35E-09	5.93E-09			0.0007
Settler Tank					2.58	11.29					0.079	0.35			29
Condensate Tanks					0.06	0.27					0.0002	0.0007			0.09
Total Facility PTE =	17.73	77.65	19.11	83.72	61.95	60.15	0.13	0.57	3.73	16.32	2.90	12.60	0.25	1.07	124,711

Controlled dehydrator still vent emissions are in the flare and pilot category.
 Controlled dehydrator flash tank emissions are in the reboiler category.

HAP Emissions Summary Total

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia

CONTROLLED POTENTIAL EMISSION SUMMARY

_	Ben	zene	Toluene		Ethylb	enzene	Xyle	enes	n-Hexane	
Source	lb/hr	tpy	lb/hr	tpy	lb/hr		tpy lb/hr		lb/hr	tpy
Engines								tpy		
Compressor Engine 1	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 2	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 3	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 4	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 5	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 6	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 7	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 8	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 9	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 10	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 11	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 12	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
Compressor Engine 13	0.022	0.096	0.0077	0.034	0.00034	0.0015	0.0027	0.012		
<u>Turbines</u>										1
Microturbine Generator 1	7.42E-05	3.25E-04	8.03E-04	3.52E-03	1.98E-04	8.66E-04	3.96E-04	1.73E-03		
Catalytic Heater for Generator Fuel										
Dehydrators										1
TEG Dehydrator Still Vent 1										
TEG Dehydrator Still Vent 2										
TEG Dehydrator Flash Tank 1										
TEG Dehydrator Flash Tank 2										
Reboiler 1	0.0004	0.0019	0.0011	0.005	0.0005	0.0022	0.0014	0.006	0.010	0.04
Reboiler 2	0.0004	0.0019	0.0011	0.005	0.0005	0.0022	0.0014	0.006	0.010	0.04
<u>Combustion</u>										í
Flare and Pilot	0.011	0.046	0.047	0.21	0.041	0.18	0.18	0.78	0.010	0.042
Hydrocarbon Loading										1
Truck Loadout	0.0015	0.00023	0.0067	0.0010	0.0046	0.00070	0.012	0.0018	0.10	0.016
Fugitive Emissions										í
Component Leak Emissions	0.00027	0.0012	0.00082	0.0036	0.00055	0.0024	0.0016	0.0071	0.017	0.073
Venting Emissions		0.0024		0.0085		0.0066		0.020		0.15
Haul Road Dust Emissions										
Storage Tanks										
Produced Water Tanks	5.02E-10	2.20E-09	4.89E-10	2.14E-09	1.04E-10	4.55E-10	2.22E-10	9.73E-10	3.82E-11	1.67E-10
Settler Tank	1.22E-03	5.35E-03	2.49E-03	1.09E-02	8.91E-04	3.90E-03	2.15E-03	9.40E-03	7.20E-02	3.15E-01
Condensate Tanks	1.74E-06	7.64E-06	7.92E-06	3.47E-05	5.50E-06	2.41E-05	1.43E-05	6.27E-05	1.25E-04	5.48E-04
Total Facility PTE =	0.30	1.31	0.16	0.68	0.05	0.22	0.23	0.99	0.22	0.68

Controlled dehydrator still vent emissions are in the flare and pilot category.
 Controlled dehydrator flash tank emissions are in the reboiler category.

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Compressor Engines

Source Information-Per Engine

Moukeeb		
vvaukesna	a L7044 GSI	
Compression		
Y	NSCR/AFRC	
1,680	hp	
8,267	Btu/(hp-hr)	
13.89	MMBtu/hr	
103.54	MMscf/yr	
11,820	scf/hr	
1,171	Btu/scf	
8,760	hrs/yr	
	Comp Y 1,680 8,267 13.89 103.54 11,820 1,171	

Notes:

1. Values from Waukesha specification sheet. Due to typical methane content in the fuel, the site horsepower is shown as 1674 hp; however, emissions are calculated at the max rating of 1680 hp.

2. Calculated values

3. Annual fuel consumption is 100% of maximum fuel consumption at 100% load.

Potential Emissions per Engine

		Controlled										
Pollutant	Emissio (Ib/MMBtu)	n Factor (g/bhp-hr)	E (lb/hr)	stimated Emissio (lb/yr)	ns ² (tpy)	Emissio (Ib/MMBtu)	n Factor (g/bhp-hr)	Esti (Ib/hr)	Estimated Emissions ² (lb/yr) (tpy)		Source of Emissions Factors	
NOx ^{1,4}		13.7	50.74		222.24		0.34	1.27		5.56	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled	
CO ^{1,4}		12.7	47.04		206.02		0.32	1.18		5.15	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled	
VOC ^{1,4}		0.47	1.74		7.62		0.075	0.28		1.22	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled	
SO ₂	5.88E-04		0.0082		0.036	5.88E-04		0.0082		0.036	AP-42, Chapter 3.2, Table 3.2-3	
PM _{2.5} /PM ₁₀	1.94E-02		0.27		1.18	1.94E-02		0.27		1.18	AP-42, Chapter 3.2, Table 3.2-3	
Total PM	1.94E-02		0.27		1.18	1.94E-02		0.27		1.18	AP-42, Chapter 3.2, Table 3.2-3	
1,1,2,2-Tetrachloroethane	2.53E-05		0.00035	3.08	0.0015	2.53E-05		0.00035	3.08	0.0015	AP-42, Chapter 3.2, Table 3.2-3	
1,3-Butadiene	6.63E-04		0.0092	80.66	0.040	6.63E-04		0.0092	80.66	0.040	AP-42, Chapter 3.2, Table 3.2-3	
Acetaldehyde	2.79E-03		0.039	339.44	0.17	2.79E-03		0.039	339.44	0.17	AP-42, Chapter 3.2, Table 3.2-3	
Acrolein	2.63E-03		0.037	319.98	0.16	2.63E-03		0.037	319.98	0.16	AP-42, Chapter 3.2, Table 3.2-3	
Benzene	1.58E-03		0.022	192.23	0.10	1.58E-03		0.022	192.23	0.10	AP-42, Chapter 3.2, Table 3.2-3	
Ethylbenzene	2.48E-05		0.00034	3.02	0.0015	2.48E-05		0.00034	3.02	0.0015	AP-42, Chapter 3.2, Table 3.2-3	
Formaldehyde ^{1,4}		0.05	0.19	1,622	0.81		0.01	0.019	162	0.081	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled	
Methanol	3.06E-03		0.042	372.29	0.19	3.06E-03		0.042	372.29	0.19	AP-42, Chapter 3.2, Table 3.2-3	
Methylene Chloride	4.12E-05		0.00057	5.01	0.0025	4.12E-05		0.00057	5.01	0.0025	AP-42, Chapter 3.2, Table 3.2-3	
РАН	1.41E-04		0.0020	17.15	0.0086	1.41E-04		0.0020	17.15	0.0086	AP-42, Chapter 3.2, Table 3.2-3	
Toluene	5.58E-04		0.0077	67.89	0.034	5.58E-04		0.0077	67.89	0.034	AP-42, Chapter 3.2, Table 3.2-3	
Xylenes	1.95E-04		0.0027	23.72	0.012	1.95E-04		0.0027	23.72	0.012	AP-42, Chapter 3.2, Table 3.2-3	
Other HAPs ²	2.10E-04		0.0029	25.52	0.013	2.10E-04		0.0029	25.52	0.013	AP-42, Chapter 3.2, Table 3.2-3	
Total HAPS			0.35	3,072	1.54			0.18	1,612	0.81		
Pollutant	Emissio (kg/MMBtu)	n Factor (g/bhp-hr)	E (Ib/hr)	stimated Emission (lb/yr) ⁴	ns ² (tpy) ⁴	Emissio (kg/MMBtu)	n Factor (g/bhp-hr)	Esti (Ib/hr)	mated Emissi (lb/yr) 4	ons ² (tpy) ⁴	Source of Emissions Factors	
CO21		529	1,959		8582		529	1,959			Manufacturer's Specs	
CH4 ^{1,4}		1.30	4.81		21.09		0.39	1.44		6.33	Manufacturer's Specs - uncontrolled, Catalyst Specs - controlled	
N ₂ O	0.0001		0.003		0.013	0.0001		0.0031		0.013	40 CFR Part 98, Subpart C, Table C-2	
CO ₂ e ²			2,081		9,113			1,996		8,744	40 CFR Part 98, Subpart A, Table A-1, effective January 2014	

Notes:

4. Due to variable load conditions, the catalyst efficiency may vary. The catalyst efficiencies used in the emissions are typical based on expected operating conditions. The catalyst specification sheet shows typical destruction efficiencies that were used in the calculations.

The emission factors shown on the catalyst specification sheet are not site specific, so those will vary; however the efficiencies will be the same.

Example Calculations

lb/hr = (g/hp-hr) * (hp) * (1 lb/453.6 g) or (lb/MMBtu) * (MMBtu/hr)

tpy = (MMscf/yr) * (Btu/scf) * (10⁶ Btu/MMBtu) * (g/hp-hr) / (Btu/hp-hr) * (1 lb/453.59 g) * (1 ton/2000 lb) or (MMscf/yr) * (Btu/scf) * (lb/MMBtu) * (1 ton/2000 lb)

Microturbine Generator Emission Calculations

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Microturbine Generators

Source Information

Emission Unit ID:	G	-8000
Make/Model	Capstone C	C600 Standard
Microturbine Rating ²	600	kWe
Number of Microturbines ²	1	unit
Net Heat Rate	10,300	Btu/kWhe
Heat Input ¹	6.18	MMBtu/hr
Operating Hours ²	8,760	hrs/yr
Notes:		

1) Calculated

2) The Capstone C600 package is made up of three (3) 200 kWe units that can operate individually. While all three units may not be operating all at once, potential emissions are calculated as though all three are operating at 8,760 hours per year.

Potential Emissions per Generator

		U	Incontrolled Controlled								
Pollutant	Emissio	on Factor	Esti	mated Emissi	ons ¹	Emissio	n Factor	Est	mated Emissi	ions ¹	Source of Emissions Factors
Foliutant	(lb/MMBtu)	(lb/MWhe)	(lb/hr)	(lb/yr)	(tpy)	(lb/MMBtu)	(lb/MWhe)	(lb/hr)	(lb/yr)	(tpy)	Source of Emissions Factors
NOx		0.40	0.24		1.05		0.40	0.24		1.05	Manufacturer Specifications
со		1.10	0.66		2.89		1.10	0.66		2.89	Manufacturer Specifications
VOC		0.10	0.06		0.26		0.10	0.06		0.26	Manufacturer Specifications
SO ₂	3.40E-03		0.02		0.09	3.40E-03		0.02		0.09	AP-42, Chapter 3.1, Table 3.1-2a
PM _{2.5} /PM ₁₀	6.60E-03		0.04		0.18	6.60E-03		0.04		0.18	AP-42, Chapter 3.1, Table 3.1-2a
1,3-Butadiene	4.30E-07		2.66E-06	0.02	1.16E-05	4.30E-07		2.66E-06	0.023	1.16E-05	AP-42, Chapter 3.1, Table 3.1-3
Acetaldehyde	4.00E-05		2.47E-04	2.17	1.08E-03	4.00E-05		2.47E-04	2.17	1.08E-03	AP-42, Chapter 3.1, Table 3.1-3
Acrolein	6.40E-06		3.96E-05	0.35	1.73E-04	6.40E-06		3.96E-05	0.35	1.73E-04	AP-42, Chapter 3.1, Table 3.1-3
Benzene	1.20E-05		7.42E-05	0.65	3.25E-04	1.20E-05		7.42E-05	0.65	3.25E-04	AP-42, Chapter 3.1, Table 3.1-3
Ethylbenzene	3.20E-05		1.98E-04	1.73	8.66E-04	3.20E-05		1.98E-04	1.73	8.66E-04	AP-42, Chapter 3.1, Table 3.1-3
Formaldehyde	7.10E-04		4.39E-03	38.44	1.92E-02	7.10E-04		4.39E-03	38.44	1.92E-02	AP-42, Chapter 3.1, Table 3.1-3
Naphthalene	1.30E-06		8.03E-06	0.07	3.52E-05	1.30E-06		8.03E-06	0.07	3.52E-05	AP-42, Chapter 3.1, Table 3.1-3
РАН	2.20E-06		1.36E-05	0.12	5.96E-05	2.20E-06		1.36E-05	0.12	5.96E-05	AP-42, Chapter 3.1, Table 3.1-3
Propylene Oxide	2.90E-05		1.79E-04	1.57	7.85E-04	2.90E-05		1.79E-04	1.57	7.85E-04	AP-42, Chapter 3.1, Table 3.1-3
Toluene	1.30E-04		8.03E-04	7.04	3.52E-03	1.30E-04		8.03E-04	7.04	3.52E-03	AP-42, Chapter 3.1, Table 3.1-3
Xylenes	6.40E-05		3.96E-04	3.46	1.73E-03	6.40E-05		3.96E-04	3.46	1.73E-03	AP-42, Chapter 3.1, Table 3.1-3
Total HAPS			0.006	55.62	0.03			0.006	55.62	0.03	
Pollutant	Emissio	on Factor	Esti	mated Emissi	ons ¹	Emissio	n Factor	Est	mated Emissi	ions ¹	Source of Emissions Factors
Folititant	(kg/MMBtu)	(lb/MWhe)	(lb/hr)		(tpy)	(kg/MMBtu)	(lb/MWhe)	(lb/hr)		(tpy)	
CO ₂		1,330	798		3,495		1,330	798		3,495	Manufacturer Specifications
CH₄	0.001		0.01		0.06	0.001		0.01		0.06	40 CFR Part 98, Subpart C, Table C-2
N ₂ O	0.0001		0.001		0.006	0.0001		0.001		0.006	40 CFR Part 98, Subpart C, Table C-2
CO ₂ e			799		3,499			799		3,499	40 CFR Part 98, Subpart A, Table A-1, effective January 2014

Example Calculations

lb/hr = (lb/Mwhe) * kWe * (1 MWe/1000 kWe) or (lb/MMBtu) * (MMBtu/hr) or (kg/MMBtu) * (MMBtu/hr) * (2.21 lb/kg)

tpy = (lb/hr) * (hr/yr) * (ton/2000 lb)

Natural Gas Fueled Catalytic Heater Emissions

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Location:	Tyler County, West Virginia
Source Description:	Catalytic Heater for Generator Fuel

Source Information

Emission Unit ID:	CATHT1		
Source Description:	Generator Fuel Heater		
Hours of Operation	8,760	hr/yr	
Design Heat Rate	0.024	MMBtu/hr	
Heater Efficiency	80%		
Fuel Heat Value	1,020	Btu/scf	
Fuel Use	0.26	MMscf/yr	

Emission Calculations per Heater

Pollutant	Emission Factor	Emissions	Emissions	Emission Factor
Folitiant	(Ib/MMscf)	(lb/hr)	(tpy)	Source
NO _X	100	0.0029	0.013	AP-42 Ch. 1.4 Table 1.4-1
CO	84	0.0025	0.011	AP-42 Ch. 1.4 Table 1.4-1
VOC	5.5	0.00016	0.00071	AP-42 Ch. 1.4 Table 1.4-2
PM ₁₀	7.6	0.00022	0.0010	AP-42 Ch. 1.4 Table 1.4-2
SO ₂	0.6	0.000018	0.000077	AP-42 Ch. 1.4 Table 1.4-2
Formaldehyde	0.075	0.000002	0.000010	AP-42 Ch. 1.4 Table 1.4-3
Total HAPs (including HCHO) ¹	1.9	0.00006	0.00024	AP-42 Ch. 1.4 Table 1.4-3
Pollutant	Emission Factor	Emissions	Emissions	Emission Factor
Follutant	(kg/MMBtu)	(lb/hr)	(tpy)	Source
Carbon Dioxide	53.06	2.81	12	40 CFR Part 98, Subpart C, Table C-1
Methane	0.001	0.0001	0.00023	40 CFR Part 98, Subpart C, Table C-2
Nitrous Oxide	0.0001	0.00001	0.000023	40 CFR Part 98, Subpart C, Table C-2
CO ₂ e		2.82	12	40 CFR Part 98, Subpart A, Table A-1

1. Only those HAP pollutants above detection thresholds were included.

Sample Calculations:

Fuel Consumption (MMscf/yr) = Heater Size (MMBtu/hr) * Hours of Operation (hrs/yr) Fuel Heat Value (Btu/scf) * Heater Efficiency

Emissions (tons/yr) = Emission Factor (lbs/MMscf) * Fuel Consumption (MMscf/yr)

2,000 (lbs/ton)

Dehydrator Emissions

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Dehydrator Units

Potential Emissions per Dehydrator

	Emission Unit ID:	SV-3110/SV-3210	Emission Unit ID:	FT-3110/FT-3210	
Pollutant	Dehydrato	r Still Vent	Flash Tank Gas		
Foliulant	(lb/hr)	(tpy)	(lb/hr)	(tpy)	
Uncontrolled Emissions ¹					
VOC	15.90	69.65	32.28	141.39	
Total HAPs	7.18	31.43	0.68	2.96	
Benzene	0.26	1.16	0.022	0.095	
Toluene	1.17	5.13	0.056	0.24	
Ethylbenzene	1.03	4.51	0.026	0.11	
Xylenes	4.47	19.59	0.069	0.30	
n-Hexane	0.24	1.04	0.50	2.21	
Methane	17.43	76.36	54.65	239.36	
Carbon Dioxide	0.17	0.74	0.98	4.29	
CO ₂ e	436	1,910	1,367	5,988	
Controlled Emissions ^{2,3}	FL-1	1000	R-3110/R-3210		
VOC	0.32	1.39	0.65	2.83	
Total HAPs	0.14	0.63	0.014	0.059	
Benzene	0.0053	0.023	0.0004	0.0019	
Toluene	0.023	0.10	0.0011	0.0049	
Ethylbenzene	0.021	0.090	0.0005	0.0022	
Xylenes	0.089	0.39	0.0014	0.0061	
n-Hexane	0.0048	0.021	0.010	0.044	
Methane	0.35	1.53	1.09	4.79	
Carbon Dioxide	0.17	0.74	0.98	4.29	
CO ₂ e	9	39	28	124	

¹Output from GRI-GLYCalc 4.0 for both the still vent and flash tank gas emissions

²Controlled emissions assume that the glycol still vent is equipped with a condenser and is controlled by

a combustor with at least 98% control efficiency. Controlled emissions are shown with FL-1000 in summary tables.

³Flash tank gas is used in the reboiler as the primary fuel source. However, in the case that gas cannot be used in the reboiler, the gas is sent to the primary/backup VRU system via the storage tanks for 98% control. Controlled emissions are shown with R-3110 and R-3210 in the summary tables.

Natural Gas Fueled Dehydrator Reboiler Combustion Emissions

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Location:	Tyler County, West Virginia
Source Description:	Dehydrator Reboilers

Source Information

Emission Unit ID:	R-3110 & R-3210		
Source Description:	Dehydrator Reboiler		
Hours of Operation	8,760	hr/yr	
Design Heat Rate	1.5	MMBtu/hr	
Heater Efficiency	0.8		
Fuel Heat Value	1,020	Btu/scf	
Fuel Use	16.1	MMscf/yr	

Emission Calculations per Reboiler

Pollutant	Emission Factor	Emissions	Emissions	Emission Factor
rondtant	(Ib/MMscf)	(lb/hr)	(tpy)	Source
NO _X	100	0.18	0.81	AP-42 Ch. 1.4 Table 1.4-1
СО	84	0.15	0.68	AP-42 Ch. 1.4 Table 1.4-1
VOC	5.5	0.010	0.044	AP-42 Ch. 1.4 Table 1.4-2
PM ₁₀	7.6	0.014	0.061	AP-42 Ch. 1.4 Table 1.4-2
SO ₂	0.6	0.0011	0.0048	AP-42 Ch. 1.4 Table 1.4-2
Formaldehyde	0.075	0.00014	0.00060	AP-42 Ch. 1.4 Table 1.4-3
Total HAPs (including HCHO)	1.9	0.0035	0.015	AP-42 Ch. 1.4 Table 1.4-3
Pollutant	Emission Factor	Emissions	Emissions	Emission Factor
Pollulani	(kg/MMBtu)	(lb/hr)	(tpy)	Source
Carbon Dioxide	53.06	175.89	770	40 CFR Part 98, Subpart C, Table C-1
Methane	0.001	0.003	0.01	40 CFR Part 98, Subpart C, Table C-2
Nitrous Oxide	0.0001	0.0003	0.001	40 CFR Part 98, Subpart C, Table C-2
CO ₂ e		176.08	771	40 CFR Part 98, Subpart A, Table A-1

Sample Calculations:

Fuel Consumption (MMscf/yr) = Heater Size (MMBtu/hr) * Hours of Operation (hrs/yr)

Fuel Heat Value (Btu/scf) * Heater Efficiency

Emissions (tons/yr) = Emission Factor (lbs/MMscf) * Fuel Consumption (MMscf/yr)

2,000 (lbs/ton)

Flare Combustion Emissions

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Flare for Dehydrator Still Vent Gas
Emission Unit ID:	FL-1000

Combusted Gas Emissions

Flare Heat Input :	9.21	MMBtu/hr
Hours of Operation:	8,760	hr/yr

Pollutant	Emission Factor ¹ (Ib/MMBtu)	Emissions (Ibs/hr)	Emissions (tons/yr)
Particulate Matter (PM/PM ₁₀ /PM _{2.5})	N/A - S	Smokeless Desig	gn
Nitrogen Oxides (NO _x)	0.068	0.63	2.74
Carbon Monoxide (CO)	0.31	2.86	12.51

¹ Emission Factors from Table 13.5-1 and 13.5-2 of AP-42 Section 13.5 (April 2015)

Pilot Emissions

Pilot Heating Value:	1,020	Btu/scf
Hours of Operation:	8,760	hr/yr
Total Pilot Natural Gas Usage:	1.64E-05	MMscf/hr

Pollutant	Emission Factor (Ib/MMscf)	Emissions (Ibs/hr)	Emissions (tons/yr)
Particulate Matter (PM/PM ₁₀ /PM _{2.5}) ²	7.6	1.25E-04	5.46E-04
Nitrogen Oxides (NOx)	100	1.64E-03	7.18E-03
Sulfur Dioxide $(SO_2)^2$	0.6	9.84E-06	4.31E-05
Carbon Monoxide (CO) ²	84	1.38E-03	6.03E-03
Volatile Organic Compounds (VOC) ²	5.5	9.02E-05	3.95E-04
Total HAPs ^{2,3}	1.88	3.08E-05	1.35E-04

² Emission Factors from AP-42 Tables 1.4-1, 1.4-2, 1.4-3, and 1.4-4 (7/98).

³ Sum of Emissions Factors published for pollutants classified as "HAPS" under AP-42 Table 1.4-3.

Total Flare Emissions

Pollutant	Emission Rate (Ibs/hr)	Emission Rate (tons/year)
Particulate Matter (PM/PM ₁₀ /PM _{2.5})	1.25E-04	5.46E-04
Nitrogen Oxides (NOx)	0.63	2.75
Sulfur Dioxide (SO ₂)	9.84E-06	4.31E-05
Carbon Monoxide (CO)	2.86	12.51
Volatile Organic Compounds (VOC)	9.02E-05	3.95E-04
Total HAPs	3.08E-05	1.35E-04

Greenhouse Gas Emissions

Pollutant	Emission Factor	Emissions	Emissions	Emission Factor
Foliutant	(kg/MMBtu)	(lb/hr)	(tpy)	Source
Carbon Dioxide	53.06	1,082	4,739	40 CFR Part 98, Subpart C, Table C-1
Methane	0.001	0.020	0.089	40 CFR Part 98, Subpart C, Table C-2
Nitrogen Dioxide	0.0001	0.0020	0.0089	40 CFR Part 98, Subpart C, Table C-2
CO ₂ e		1,083	4,744	40 CFR Part 98, Subpart A, Table A-1

Settling Tank Flashing Emissions

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Settling Tank
Emission Unit ID:	TK-9000

Settling Tank Flashing Emissions

Component	Uncontrolled Flashing Emissions ¹ (lb/hr)	Uncontrolled Flashing Emissions (tons/yr)	Controlled Flashing Emissions ^{2,3} (lb/hr)	Controlled Flashing Emissions ^{2,3} (tons/yr)
Methane	13.00	56.95	0.26	1.14
Ethane	31.90	139.70	0.64	2.79
Propane	45.56	199.56	0.91	3.99
i-Butane	12.01	52.60	0.24	1.05
n-Butane	30.60	134.02	0.61	2.68
i-Pentane	11.42	50.01	0.23	1.00
n-Pentane	13.12	57.48	0.26	1.15
i-Hexanes	5.62	24.62	0.11	0.49
Heptanes	3.28	14.36	0.066	0.29
Octanes	1.11	4.85	0.022	0.10
Nonanes	0.19	0.81	0.0037	0.016
Decanes+	0.02	0.07	0.00032	0.0014
n-Hexane	3.60	15.76	0.072	0.32
Benzene	0.06	0.27	0.0012	0.0053
Toluene	0.12	0.54	0.0025	0.011
Ethylbenzene	0.04	0.19	0.00089	0.0039
Xylenes	0.11	0.47	0.0021	0.0094
Nitrogen	0.06	0.27	0.063	0.27
Carbon Dioxide	0.17	0.74	0.17	0.74
Water	1.59	6.95	1.59	6.95
VOC Subtotal	126.85	555.61	2.54	11.11
HAP Subtotal	3.93	17.23	0.079	0.34
CO₂e Subtotal	325.23	1424.49	6.67	29.22
Total	173.57	760.22	5.25	23.01

Notes:

1. Flashing emissions calculated by ProMax 3.2. Flashing only occurs in the settling tank as all pressurized fluids flow into the settling tank and then separate out at atmospheric conditions to the condensate and produced water tanks.

2. Tanks are controlled by a VRU with assumed 98% capture efficiency; but will likely be higher as vapors are recycled back into the system

3. VRU-6000 is the primary VRU to collect storage tank vapors and VRU-6100 is the backup VRU in times when the primary VRU is undergoing maintenance or shutdown.

Storage Tank Working and Breathing Emissions

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Condensate, Settling, and Produced Water Tanks
Emission Unit ID:	TK-9000, TK-9100, TK-9110, TK-9200, TK-9210

ТАНК	Uncontrolled VOC	Uncontrolled Benzene	Uncontrolled Toluene	Uncontrolled Ethylbenzene	Uncontrolled Xylene	Uncontrolled n-Hexane	Uncontrolled CH₄	Uncontrolled CO ₂ e
DESCRIPTION	Emissions ¹	Emissions ¹	Emissions ¹	Emissions ¹	Emissions ¹	Emissions ¹	Emissions ¹	Emissions
	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)	(tons/yr)
400 bbl Hydrocarbon Storage Tank (TK-9200)	6.82	1.91E-04	8.67E-04	6.03E-04	1.57E-03	1.37E-02	0.080	2.01
400 bbl Hydrocarbon Storage Tank (TK-9210)	6.82	1.91E-04	8.67E-04	6.03E-04	1.57E-03	1.37E-02	0.080	2.01
500 bbl Settling Tank (TK-9000)	8.98	2.51E-04	1.14E-03	7.94E-04	2.07E-03	1.81E-02	0.11	2.65
400 bbl Produced Water Storage Tank ² (TK-9100)	0.00038	5.49E-08	5.35E-08	1.14E-08	2.43E-08	4.19E-09	0.00037	0.0093
400 bbl Produced Water Storage Tank ² (TK-9110)	0.00038	5.49E-08	5.35E-08	1.14E-08	2.43E-08	4.19E-09	0.00037	0.0093
TOTAL	22.62	0.00063	0.0029	0.0020	0.0052	0.045	0.27	6.69

	Controlled	Controlled						
TANK	VOC	Benzene	Toluene	Ethylbenzene	Xylene	n-Hexane	CH₄	CO ₂ e
DESCRIPTION	Emissions ^{1,3}	Emissions						
	(tons/yr)	(tons/yr)						
400 bbl Hydrocarbon Storage Tank (TK-9200)	0.14	3.82E-06	1.73E-05	1.21E-05	3.14E-05	2.74E-04	0.0016	0.047
400 bbl Hydrocarbon Storage Tank (TK-9210)	0.14	3.82E-06	1.73E-05	1.21E-05	3.14E-05	2.74E-04	0.0016	0.047
500 bbl Settling Tank (TK-9000)	0.18	5.03E-06	2.28E-05	1.59E-05	4.13E-05	3.61E-04	0.0021	0.062
400 bbl Produced Water Storage Tank ² (TK-9100)	0.0000077	1.10E-09	1.07E-09	2.27E-10	4.87E-10	8.37E-11	7.36E-06	0.00033
400 bbl Produced Water Storage Tank ² (TK-9110)	0.0000077	1.10E-09	1.07E-09	2.27E-10	4.87E-10	8.37E-11	7.36E-06	0.00033
TOTAL	0.45	1.27E-05	5.75E-05	4.00E-05	1.04E-04	9.10E-04	0.0053	0.16

Notes:

1. ProMax 3.2 used to calculate standing, working, and breathing (S,W,B) emissions

2. Produced water assumed to have no more than 10% hydrocarbon liquid

3. Tanks are controlled by a VRU with assumed 98% capture efficiency; but will likely be higher as vapors are recycled back into the system.

4. VRU-6000 is the primary VRU to collect storage tank vapors and VRU-6100 is the backup VRU in times when the primary VRU is undergoing maintenance or shutdown.

Truck Loading Emissions

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Production Liquids Truck Loadout
Emission Unit ID:	LDOUT1

AP - 42, Chapter 5.2 $L_{L} = 12.46 \times S \times P \times M / T$

- L_{L} = Loading Loss Emission Factor (lbs VOC/1000 gal loaded)
 - S = Saturation Factor
 - P = True Vapor Pressure of the Loaded Liquid (psia)
 - M = Vapor Molecular Weight of the Loaded Liquid (lbs/lbmol)
 - $T = Temperature of Loaded Liquid (^{O}R)$

VOC Emissions (tpy) = L_L (lbs VOC/1000 gal) * 42 gal/bbl * 365 days/year * production (bbl/day)

1000 gal * 2000 lbs/ton

						L	Production	VOC	Benzene	Toluene	E-Benzene	Xylene	n-Hexane	CH4	CO2e
Source	S ¹	P (psia) ²	M ³	T (ºF) ⁴	T (ºR)	(lb/1000 gal)	(bbl/day)	(tpy)	(tpy)	(tpy)	(tpy)	(tpy)	(tpy)	(tpy)	(tpy)
Condensate	0.6	11.8	41.1	65	524.75	6.88	150	7.91	0.00022	0.0010	0.00070	0.0018	0.016	0.093	2.33
Produced Water	0.6	0.31	18.6	65	524.75	0.08	45	0.03	4.12E-06	4.01E-06	8.52E-07	1.82E-06	3.14E-07	0.028	0.70

Notes: 1. Saturation factor from AP-42, Table 5.2-1 (Submerged loading (bottom loading): dedicated normal service)

2. True vapor pressure and molecular weight are estimated from tank-specific ProMax 3.2 simulations for both liquids.

3. Temperature based on the annual average temperature of Charleston, WV retrieved from ProMax working and breathing report.

4. HAP and CO2e emissions calculated with weight percentages of the working and breathing vent gas from the ProMax 3.2 simulation

Assume 1 truck loaded per hour, 180 bbl truck, for short term emissions

						L	Loading	VOC	Benzene	Toluene	E-Benzene	Xylene	n-Hexane	CH4	CO2e
Source	S ¹	P (psia) ²	M ³	T (ºF) ⁴	T (ºR)	(lb/1000 gal)	bbl/hr	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)
Condensate	0.6	11.8	41.1	65	524.75	6.88	180	52.02	0.0015	0.0066	0.0046	0.012	0.10	0.61	15.3
Produced Water	0.6	0.31	18.6	65	524.75	0.08	180	0.63	9.02E-05	8.79E-05	1.87E-05	4.00E-05	6.88E-06	0.60	15.3

Component Fugitive Emissions

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Fugitive Emissions - Component Leaks

		VOC Fug	itive Emissions	5		
Equipment Type and Service	Number of Units ¹	Hours of Operation (hours/yr)	THC Emission Factor ² (kq/hr-unit)	VOC Weight Fraction ³	THC Emissions (tpy)	VOC Emissions (tpy)
Flanges - Gas Service	836	8,760	3.90E-04	0.21	3.16	0.66
Valves - Gas Service	250	8,760	4.50E-03	0.21	10.89	2.29
Compressor Seals Gas Service	39	8,760	8.80E-03	0.21	3.32	0.70
Flanges - Liquid Service	175	8,760	1.10E-04	0.73	0.19	0.14
Valves - Liquid Service	42	8,760	2.50E-03	0.73	1.02	0.74
Total Emissions (tons/yr)					18.57	4.53

	HAPs Fugitive Emissions												
Equipment Type	Benzene	Benzene	Toluene	Toluene	Ethylbenzene	Ethylbenzene	Xylene	Xylene	n-Hexane	n-Hexane			
and Service	Weight	Emissions	Weight	Emissions	Weight	Emissions	Weight	Emissions	Weight	Emissions			
	Fraction ³	(tpy)	Fraction ³	(tpy)	Fraction ³	(tpy)	Fraction ³	(tpy)	Fraction ³	(tpy)			
Flanges - Gas Service	4.42E-05	0.00014	1.56E-04	0.00049	1.20E-04	0.00038	3.65E-04	0.0012	2.75E-03	0.0087			
Valves - Gas Service	4.42E-05	0.00048	1.56E-04	0.0017	1.20E-04	0.0013	3.65E-04	0.0040	2.75E-03	0.030			
Compressor Seals Gas Service	4.42E-05	0.00015	1.56E-04	0.00052	1.20E-04	0.00040	3.65E-04	0.0012	2.75E-03	0.0091			
Flanges - Liquid Service	3.55E-04	0.000066	7.24E-04	0.00013	2.58E-04	0.000048	6.22E-04	0.00012	2.09E-02	0.0039			
Valves - Liquid Service	3.55E-04	0.00036	7.24E-04	0.00074	2.58E-04	0.00026	6.22E-04	0.00063	2.09E-02	0.021			
Total Emissions (tons/yr)		0.0012		0.0036		0.0024		0.0071		0.073			

1) Component counts from similar facilities.

2) API average emission factors are for oil and gas production operations - Table 2.4, EPA Protocol for Equipment Leak Emission Estimates - 1995.

3) Gas and liquid weight fractions from representative analyses..

	GHG Fugitive Emissions													
Equipment Type	Number	Hours of	Emission	CH₄	CO ₂	CH₄	CO ₂	CO ₂ e						
and Service	of	Operation	Factor ²	Concentration ³	Concentration ³	Emissions	Emissions	Emissions						
	Units ¹	(hours/yr)	(scf/hr-unit)			(tpy)	(tpy)	(tpy)						
Flanges	1,011	8,760	0.003	0.98	0.011	0.55	0.017	13.72						
Valves - Gas Service	250	8,760	0.027	0.98	0.011	1.22	0.038	30.54						
Valves - Liquid Service	42	8,760	0.050	0.98	0.011	0.38	0.012	9.50						
Compressor Seals	39	8,760	0.300	0.98	0.011	2.11	0.065	52.94						
Total Emissions (tons/yr)						4.26	0.13	106.71						

1) Component counts from similar facilities.

2) Emission factors from 40 CFR Part 98 Subpart W, Table W1-A; Gas service where available, else light crude service

3) CH₄ and CO₂ concentrations as defined in 40 CFR Part 98.233(r)

Fugitive Emissions From Venting Episodes

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Fugitive Emissions-Venting Episodes

VOC Venting Emissions											
	Number	Amount	Molecular								
Type of Event ¹	Of	Vented per	Weight of	Total	VOC	VOC					
Type of Event	Events	Event	Vented Gas	Emissions	Weight	Emissions					
	(event/yr)	(scf/event)	(lb/lb-mol)	(ton/yr)	Fraction ⁴	(ton/yr)					
Compressor Blowdown ²	156	10,000	21.41	44.02	0.21	9.17					
Compressor Startup ³	156	1,050	21.41	4.62	0.21	0.96					
Plant Shutdown	2	100,000	21.41	5.64	0.21	1.18					
Pigging Venting	26	1,000	21.41	0.73	0.21	0.15					
Total Emissions (tons/yr)						11.46					

	HAPs Venting Emissions													
Type of Event ¹	Benzene	Benzene	Toluene	Toluene	Ethylbenzene	Ethylbenzene	Xylene	Xylene	n-Hexane	n-Hexane				
	Weight	Emissions	Weight	Emissions	Weight	Emissions	Weight	Emissions	Weight	Emissions				
	Fraction ⁴	(tpy)	Fraction ⁴	(tpy)	Fraction ⁴	(tpy)	Fraction ⁴	(tpy)	Fraction ⁴	(tpy)				
Compressor Blowdown ²	4.39E-05	0.0019	1.55E-04	0.0068	1.19E-04	0.0052	3.62E-04	0.016	2.72E-03	0.12				
Compressor Startup ³	4.39E-05	0.00020	1.55E-04	0.00072	1.19E-04	0.00055	3.62E-04	0.0017	2.72E-03	0.013				
Plant Shutdown	4.39E-05	0.00025	1.55E-04	0.00088	1.19E-04	0.00067	3.62E-04	0.0020	2.72E-03	0.015				
Pigging Venting	4.39E-05	0.000032	1.55E-04	0.00011	1.19E-04	0.000087	3.62E-04	0.00027	2.72E-03	0.0020				
Total Emissions (tons/yr)		0.0024		0.0085		0.0066		0.020		0.15				

	GHG Venting Emissions												
Type of Event ¹	Number Of Events	Amount Vented per Event	Molecular Weight of Vented Gas	CH₄ Weight	CO ₂ Weight	CH₄ Emissions	CO ₂ Emissions	CO ₂ e Emissions					
	(event/yr)	(scf/event)	(lb/lb-mol)	Fraction ⁴	Fraction ⁴	(ton/yr)	(ton/yr)	(tpy)					
Compressor Blowdown ²	156	10,000	21.41	0.57	0.0033	24.88	0.15	622.17					
Compressor Startup ³	156	1,050	21.41	0.57	0.0033	2.61	0.015	65.33					
Plant Shutdown	2	100,000	21.41	0.57	0.0033	3.19	0.019	79.77					
Pigging Venting	26	1,000	21.41	0.57	0.0033	0.41	0.0024	10.37					
Total Emissions (tons/yr)						31.10	0.18	777.63					

1) Estimated number of events and venting per event from engineering based on other facilities

2) Total number of compressor blowdowns based on 12 blowdowns per compressor.

3) Total number of compressor startups based on 12 starts per compressor.

4) Weight Fraction is from a gas analysis that will be typical for the facility

Fugitive Dust Emissions

Company:	Antero Midstream LLC
Facility Name:	Underwood Compressor Station
Facility Location:	Tyler County, West Virginia
Source Description:	Fugitive Dust Emissions

Gravel Access Road	Loaded Truck Weight ¹	Trips per year ²	Trips per day ²	•	Distance per round trip (truck in and out) ³	
	tons			feet	miles	miles
Condensate Tank Truck	40.00	365	1.0	4,700	0.89	325
Produced Water Tank Truck	40.00	365	1.0	4,700	0.89	325
Passenger Vehicles	3.00	1,095	3.0	4,700	0.89	975

Equation Parameter	PM-10/PM2.5	PM-Total
E , annual size-specific emission factor for PM ₁₀ & PM _{2.5} (upaved industrial roads) extrapolated for natural mitigation ⁶	see table below	see table below
k , Particle size multiplier for particle size range (PM ₁₀), (lb/VMT) (Source: AP-42 Table 13.2.2-2)	1.5	4.9
k , Particle size multiplier for particle size range (PM _{2.5}), (lb/VMT) (Source: AP-42 Table 13.2.2-2)	0.15	4.9
s , surface material silt content, (%) (Source: AP-42 Table 13.2.2-1)	4.8	4.8
W, mean weight (tons) of the vehicles traveling the road	17.8	17.8
a , constant for PM ₁₀ and PM _{2.5} on industrial roads (Source: AP-42 Table 13.2.2-2)	0.9	0.7
b , constant for PM ₁₀ and PM _{2.5} on industrial roads (Source: AP-42 Table 13.2.2-2)	0.45	0.45
P , number of "wet" days with at least 0.254 mm (0.01 in) of precipitation during the averaging period, based on AP-42 Figure 13.2.2-1.	160	160

$$E = \left[k \left(\frac{s}{12} \right)^a \times \left(\frac{W}{3} \right)^b \right] \times \left(365 - \frac{P}{365} \right)$$

Source of Equation: AP-42 Section 13.2.2

PM₁₀ Emissions

Emission Factor (Ib/VMT)	Vehicle miles traveled (VMT/yr)	Annual Uncontrolled PM ₁₀ Emissions (tpy)
0.82	1,625	0.67

PM_{2.5} Emissions

Emission Factor (Ib/VMT)	Vehicle miles traveled (VMT/yr)	Annual Uncontrolled PM _{2.5} Emissions (tpy)
0.082	1,625	0.067

PM- Total Emissions

Emission Factor (Ib/VMT)	Vehicle miles traveled (VMT/yr)	Annual Uncontrolled PM-Total Emissions (tpy)
3.23	1,625	2.62

Table Notes:

3. Distance per round trip is based on the proposed site layout. The one way distance is measured as 2,200 feet for the gravel access road and 150 feet on the dirt pad one way.

^{1.} Loaded truck weight is based on typical weight limit for highway vehicles.

^{2.} Based on production, it's assumed a maximum of one condensate truck (180 bbl truck) and one produced water truck (180 bbl truck) will be onsite per day.

Facility Gas Analysis

Γ			Component	
	MOL %	MW	Weight	Wt. Fraction
			lb/lb-mol	
Methane	75.469	16.04	12.11	0.57
Ethane	15.543	30.07	4.67	0.22
Propane	5.177	44.10	2.28	0.11
i-Butane	0.676	58.12	0.39	0.018
n-Butane	1.475	58.12	0.86	0.040
i-Pentane	0.348	72.15	0.25	0.012
n-Pentane	0.358	72.15	0.26	0.012
Hexanes+	0.347	100.00	0.35	0.016
n-Hexane	0.068	86.18	0.058	0.0027
Benzene	0.0012	78.11	0.0009	0.000044
Toluene	0.0036	92.14	0.0033	0.00016
Ethylbenzene	0.0024	106.17	0.0026	0.00012
Xylenes	0.0073	106.16	0.008	0.00036
Nitrogen	0.363	28.01	0.10	0.0047
Carbon Dioxide	0.162	44.01	0.071	0.0033
Totals	100.0		21.41	1.00
Molecular weight	21.41			
VOC weight fraction	0.21			
Methane weight fraction	0.57			
THC woight fraction	0.00			

Mounding worght naodon	0.07
THC weight fraction	0.99
VOC of THC wt fraction	0.21
CH4 of THC wt fraction	0.57
Benzene of THC wt fraction	0.000044
Toluene of THC wt fraction	0.00016
E-benzene of THC wt fraction	0.00012
Xylene of THC wt fraction	0.00036
n-Hexane of THC wt fraction	0.0027

Weigle Unit 1H analysis with BTEX relative fractions from similar wells

	MOL %	MW	Component Weight Ib/Ib-mol	Wt. Fraction
Methane	19.177	16.04	3.08	0.075
Ethane	25.098	30.07	7.55	0.18
Propane	24.448	44.10	10.78	0.26
i-Butane	4.889	58.12	2.84	0.069
n-Butane	12.456	58.12	7.24	0.18
i-Pentane	3.744	72.15	2.70	0.066
n-Pentane	4.304	72.15	3.11	0.076
Other Hexanes	1.543	86.18	1.33	0.032
Heptanes	0.774	100.20	0.78	0.019
Octanes	0.229	114.23	0.26	0.0064
Nonanes	0.034	128.26	0.044	0.0011
Decanes+	0.002	142.28	0.0031	0.000076
n-Hexane	0.988	86.18	0.85	0.021
Benzene	0.018	78.11	0.014	0.00035
Toluene	0.032	92.14	0.029	0.00072
Ethylbenzene	0.010	106.17	0.010	0.00026
Xylenes	0.024	106.16	0.025	0.00062
Nitrogen	0.053	28.01	0.015	0.00036
Carbon Dioxide	0.091	44.01	0.040	0.0010
Water	2.084	18.02	0.38	0.0091
Totals	100.00		41.07	1.00

Facility Tank Vent Gas Analysis

Molecular weight

41.07

VOC weight fraction	0.73
Methane weight fraction	0.075
THC weight fraction	0.99
VOC of THC wt fraction	0.74
CH4 of THC wt fraction	0.076
Benzene of THC wt fraction	0.00036
Toluene of THC wt fraction	0.00072
E-benzene of THC wt fraction	0.00026
Xylene of THC wt fraction	0.00062
n-Hexane of THC wt fraction	0.021

Tank vent gas is the Settling Tank flash gas stream from the ProMax 3.2 simulation

	MOL %	MOL %	MOL %	MOL %
	Blanche 1H	Hendershot 2H	Average	Water
Methane	3.925	4.898	4.412	0.4412
Ethane	4.741	7.946	6.344	0.6344
Propane	5.587	10.441	8.014	0.8014
i-Butane	1.733	3.134	2.434	0.2434
n-Butane	5.368	10.164	7.766	0.7766
i-Pentane	3.552	6.035	4.794	0.4794
n-Pentane	5.339	8.955	7.147	0.7147
Other Hexanes	4.649	7.234	5.942	0.5942
Heptanes	13.536	12.272	12.904	1.2904
Octanes	16.656	8.304	12.480	1.2480
Nonanes	7.581	4.253	5.917	0.5917
Decanes+	18.768	8.249	13.509	1.3509
n-Hexane	4.753	5.789	5.271	0.5271
Benzene	0.100	0.100	0.100	0.0100
Toluene	0.755	0.524	0.640	0.0640
Ethylbenzene	0.788	0.443	0.616	0.0616
Xylenes	2.143	1.221	1.682	0.1682
Nitrogen	0.013	0.011	0.012	0.0012
Carbon Dioxide	0.013	0.030	0.022	0.0022

Facility Pressurized Liquid Analysis

C10+ specific gravity	0.7837	0.7832	0.7835
C10+ MW	179.40	166.30	172.850
API	63.35	69.12	66.24

Liquid analysis is the average of two representative analyses from the field. The pressurized water analysis assumes 10% hydrocarbons.

GlyCalc

GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES Case Name: Underwood Compressor Station File Name: W:\20163815 Antero WV 2016 Comp Air Mods\2.0 Technical Information\Underwood CS\Attachment N\Dehy Runs\Underwood Dehy.ddf Date: February 08, 2016 DESCRIPTION: _____ Description: One (1) 88 MMscf/day TEG dehydration unit Kimray 45015 PV glycol pump Annual Hours of Operation: 8760.0 hours/yr WET GAS: _____ Temperature: 120.00 deg. F Pressure: 1100.00 psig Wet Gas Water Content: Saturated Component Conc. (vol %) _____ ____
 Carbon Dioxide
 0.1620

 Nitrogen
 0.3630

 Methane
 75.4690

 Ethane
 15.5430

 Propane
 5.1770

 Isobutane
 0.6760

 n-Butane
 1.4750

 Isopentane
 0.3480

 n-Pentane
 0.3580

 n-Hexane
 0.0680
 Other Hexanes 0.3470 Benzene 0.0012 Toluene 0.0036 Ethylbenzene 0.0024 Xylenes 0.0073 DRY GAS: _____ Flow Rate: 88.0 MMSCF/day Water Content: 5.0 lbs. H2O/MMSCF LEAN GLYCOL: _____ Glycol Type: TEG Water Content: 1.5 wt% H2O Flow Rate: 7.9 gpm PUMP: _____ Glycol Pump Type: Gas Injection Gas Injection Pump Volume Ratio: 0.032 acfm gas/gpm glycol

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Flash Control: Combustion device Flash Control Efficiency: 98.00 % Temperature: 80.0 deg. F Pressure: 5.0 psig

STRIPPING GAS:

Source of Gas: Dry Gas Gas Flow Rate: 9.000 scfm

REGENERATOR OVERHEADS CONTROL DEVICE:

Control Device: Temperature: Pressure:	200.0 deg. F
Destruction Efficiency: Excess Oxygen:	Combustion Device 98.0 % 0.0 %
Ambient Air Temperature:	0.0 deg. F

GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: Underwood Compressor Station File Name: W:\20163815 Antero WV 2016 Comp Air Mods\2.0 Technical Information\Underwood CS\Attachment N\Dehy Runs\Underwood Dehy.ddf Date: February 08, 2016

DESCRIPTION:

Description: One (1) 88 MMscf/day TEG dehydration unit Kimray 45015 PV glycol pump

Annual Hours of Operation: 8760.0 hours/yr

EMISSIONS REPORTS:

CONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.3486	8.368	1.5271
Ethane	0.1409	3.382	0.6172
Propane	0.0778	1.867	0.3408
Isobutane	0.0151	0.362	0.0661
n-Butane	0.0376	0.903	0.1648
Isopentane	0.0114	0.273	0.0499
n-Pentane	0.0137	0.329	0.0600
n-Hexane	0.0048	0.114	0.0209
Other Hexanes	0.0189	0.454	0.0828
Benzene	0.0053	0.127	0.0232
Toluene	0.0234	0.561	0.1025
Ethylbenzene	0.0206	0.494	0.0902
Xylenes	0.0894	2.146	0.3916
Total Emissions	0.8075	19.380	3.5368
Total Hydrocarbon Emissions	0.8075	19.380	3.5368
Total VOC Emissions	0.3179	7.630	1.3926
Total HAP Emissions	0.1434	3.442	0.6282
Total BTEX Emissions	0.1387	3.328	0.6074

UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane Ethane Propane Isobutane n-Butane Isopentane n-Pentane n-Hexane Other Hexanes Benzene	17.4329 7.0454 3.8904 0.7544 1.8813 0.5696 0.6845 0.2383 0.9453 0.2647	418.390 169.091 93.370 18.106 45.150 13.670 16.428 5.720 22.688 6.354	76.3562 30.8591 17.0401 3.3043 8.2400 2.4948 2.9981 1.0440 4.1405 1.1596
Toluene Ethylbenzene Xylenes	1.1703 1.0297 4.4727	28.088 24.712 107.345	5.1261 4.5100 19.5905

Page: 1

Total	Emissions	40.3797	969.113	Page: 2 176.8631
	Emissions Emissions	40.3797 15.9013 7.1758 6.9375	969.113 381.632 172.220 166.500	176.8631 69.6478 31.4301 30.3862

FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	1.0930	26.231	4.7871
Ethane	0.5539	13.294	2.4262
Propane	0.3113	7.472	1.3637
Isobutane	0.0568	1.363	0.2488
n-Butane	0.1382	3.316	0.6051
Isopentane	0.0367	0.880	0.1605
n-Pentane	0.0416	0.997	0.1820
n-Hexane	0.0101	0.242	0.0441
Other Hexanes	0.0476	1.142	0.2085
Benzene	0.0004	0.010	0.0019
Toluene	0.0011	0.027	0.0049
Ethylbenzene	0.0005	0.012	0.0022
Xylenes	0.0014	0.033	0.0061
Total Emissions	2.2925	55.020	10.0411
Total Hydrocarbon Emissions	2.2925	55.020	10.0411
Total VOC Emissions	0.6456	15.495	2.8278
Total HAP Emissions	0.0135	0.324	0.0592
Total BTEX Emissions	0.0034	0.083	0.0151

FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Methane	54.6477	1311.544	239.3568
Ethane	27.6962	664.709	121.3094
Propane	15.5668	373.603	68.1826
Isobutane	2.8399	68.157	12.4387
n-Butane	6.9076	165.783	30.2554
Isopentane	1.8326	43.983	8.0268
n-Pentane	2.0779	49.869	9.1010
n-Hexane	0.5038	12.091	2.2067
Other Hexanes	2.3802	57.124	10.4251
Benzene	0.0216	0.518	0.0945
Toluene	0.0558	1.340	0.2445
Ethylbenzene	0.0255	0.612	0.1117
Xylenes	0.0691	1.658	0.3025
Total Emissions	114.6246	2750.990	502.0556
Total Hydrocarbon Emissions	114.6246	2750.990	502.0556
Total VOC Emissions	32.2807	774.737	141.3894
Total HAP Emissions	0.6758	16.219	2.9599
Total BTEX Emissions	0.1720	4.127	0.7532

COMBINED	REGENERATOR	VENT/FLASH	GAS	EMISSIONS

Component	lbs/hr	lbs/day	tons/yr

Methane Ethane Propane Isobutane n-Butane	1.4416 0.6948 0.3891 0.0719 0.1758	34.598 16.676 9.339 1.725 4.219	Page: 3 6.3142 3.0434 1.7044 0.3149 0.7699
Isopentane	0.0480	1.153	0.2104
n-Pentane	0.0552	1.326	0.2420
n-Hexane	0.0148	0.356	0.0650
Other Hexanes	0.0665	1.596	0.2913
Benzene	0.0057	0.137	0.0251
Toluene	0.0245	0.588	0.1073
Ethylbenzene	0.0211	0.506	0.0924
Xylenes	0.0908	2.179	0.3976
Total Emissions	3.1000	74.400	13.5779
Total Hydrocarbon Emissions	3.1000	74.400	13.5779
Total VOC Emissions	0.9636	23.125	4.2204
Total HAP Emissions	0.1569	3.767	0.6874
Total BTEX Emissions	0.1421	3.411	0.6224

COMBINED REGENERATOR VENT/FLASH GAS EMISSION CONTROL REPORT:

Component	Uncontrolled tons/yr	Controlled tons/yr	% Reduction
Methane Ethane Propane Isobutane n-Butane	315.7129 152.1685 85.2226 15.7429 38.4953	6.3142 3.0434 1.7044 0.3149 0.7699	98.00 98.00 98.00 98.00 98.00 98.00
Isopentane n-Pentane n-Hexane Other Hexanes Benzene	10.5216 12.0991 3.2507 14.5656 1.2540	0.2104 0.2420 0.0650 0.2913 0.0251	98.00 98.00 98.00 98.00 98.00
Toluene Ethylbenzene Xylenes	5.3706 4.6217 19.8930	0.1073 0.0924 0.3976	98.00 98.00 98.00
Total Emissions	678.9187	13.5779	98.00
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	678.9187 211.0373 34.3900 31.1394	13.5779 4.2204 0.6874 0.6224	98.00 98.00 98.00 98.00 98.00

EQUIPMENT REPORTS:

CONDENSER AND COMBUSTION DEVICE

Condenser Outlet Temperature: 200.00 deg. F Condenser Pressure: 14.70 psia Condenser Duty: 2.20e-001 MM BTU/hr Produced Water: 15.64 bbls/day Ambient Temperature: 0.00 deg. F

Excess Oxygen: 0.00 % Combustion Efficiency: 98.00 % Supplemental Fuel Requirement: 2.20e-001 MM BTU/hr

Component	Emitted	Destroyed
Methane Ethane Propane Isobutane n-Butane	2.00% 2.00% 2.00% 2.00% 2.00%	98.00% 98.00% 98.00% 98.00% 98.00% 98.00%
Isopentane	2.00%	98.00%
n-Pentane	2.00%	98.00%
n-Hexane	2.00%	98.00%
Other Hexanes	2.00%	98.00%
Benzene	2.00%	98.00%
Toluene	2.00%	98.00%
Ethylbenzene	2.00%	98.00%
Xylenes	2.00%	98.00%

ABSORBER

Calculated Absorber Stages:	2.19	
Specified Dry Gas Dew Point:	5.00	lbs. H2O/MMSCF
Temperature:	120.0	deg. F
Pressure:	1100.0	
Dry Gas Flow Rate:		MMSCF/day
Glycol Losses with Dry Gas:	6.3613	lb/hr
Wet Gas Water Content:		
Calculated Wet Gas Water Content:	95.10	lbs. H2O/MMSCF
Calculated Lean Glycol Recirc. Ratio:	1.44	gal/lb H2O

Component	Remaining in Dry Gas	Absorbed in Glycol
Water	5.25%	94.75%
Carbon Dioxide	99.88%	0.12%
Nitrogen	99.99%	0.01%
Methane	99.99%	0.01%
Ethane	99.97%	0.03%
Propane	99.96%	0.04%
Isobutane	99.96%	0.04%
n-Butane	99.95%	0.05%
Isopentane	99.95%	0.05%
n-Pentane	99.94%	0.06%
n-Hexane	99.92%	0.08%
Other Hexanes	99.94%	0.06%
Benzene	96.89%	3.11%
Toluene	96.23%	3.77%
Ethylbenzene	95.76%	4.24%
Xylenes	93.98%	6.02%

FLASH TANK

Flash Control: Combustion device Flash Control Efficiency: 98.00 % Flash Temperature: 80.0 deg. F Flash Pressure: 5.0 psig

Component	Glycol	Page: Flash Gas	5
Water Carbon Dioxide Nitrogen Methane Ethane	0.34% 0.38% 1.41%	93.62% 99.66% 99.62% 98.59%	
Propane Isobutane n-Butane Isopentane n-Pentane	10.64%	93.56% 91.26% 89.36%	
n-Hexane Other Hexanes Benzene Toluene Ethylbenzene	92.81% 95.79%	7.19% 4.21%	
Xylenes	98.67%	1.33%	

REGENERATOR

Regenerator Stripping Gas:

Dry Draduct (Regenerator Stripping G	as:	
Dry Product G	Stripping Gas Flow Ra	ite: 9.000	0 scfm
	Component	Remaining in Glycol	
	Water Carbon Dioxide Nitrogen Methane Ethane	0.00% 0.00%	100.00% 100.00% 100.00%
	Propane Isobutane n-Butane Isopentane n-Pentane	0.00% 0.00% 2.65% 2.28%	100.00% 100.00%
	n-Hexane Other Hexanes Benzene Toluene Ethylbenzene	1.44% 3.44% 5.33% 8.18% 10.58%	96.56% 94.67% 91.82%
	Xylenes	13.09%	86.91%

STREAM REPORTS:

WET GAS STREAM

·						
	Temperature: Pressure: Flow Rate:	120.00 deg 1114.70 psia 3.67e+006 scfl Component	1	Conc.	Loading	
				(vol%)	(lb/hr)	

Water 2.00e-001 3.49e+002 Carbon Dioxide 1.62e-001 6.89e+002 Nitrogen 3.62e-001 9.83e+002 Methane 7.53e+001 1.17e+005 Ethane 1.55e+001 4.52e+004 Propane 5.17e+000 2.21e+004 Isobutane 6.75e-001 3.80e+003 n-Butane 1.47e+000 8.29e+003 Isopentane 3.47e-001 2.43e+003 n-Pentane 3.57e-001 2.50e+003 n-Hexane 6.79e-002 5.66e+002 Other Hexanes 3.46e-001 2.89e+003 Benzene 1.20e-003 9.06e+000 Toluene 3.59e-003 3.21e+001 Ethylbenzene 2.40e-003 2.46e+001 Xylenes 7.29e-003 7.49e+001 Total Components 100.00 2.07e+005

DRY GAS STREAM

120.00 deg. F 1114.70 psia 3.67e+006 scfh		
Component	Conc. (vol%)	Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	1.05e-002 1.62e-001 3.63e-001 7.55e+001 1.55e+001	6.88e+002 9.83e+002 1.17e+005
Isobutane n-Butane Isopentane	5.18e+000 6.76e-001 1.47e+000 3.48e-001 3.58e-001	3.80e+003 8.28e+003 2.43e+003
Other Hexanes Benzene	1.16e-003 3.46e-003	2.89e+003 8.78e+000 3.08e+001
Xylenes	6.86e-003	7.04e+001
 Total Components	100.00	2.06e+005

LEAN GLYCOL STREAM

Temperature: 120.00 deg. F Flow Rate: 7.92e+000 gpm Component Conc. Loading (wt%) (lb/hr) TEG 9.85e+001 4.39e+003 Water 1.50e+000 6.69e+001 Carbon Dioxide 1.78e-012 7.93e-011 Nitrogen 2.58e-013 1.15e-011 Methane 8.81e-018 3.93e-016

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Ethane 1.21e-007 5.39e-006 Propane 7.37e-009 3.29e-007 Isobutane 1.10e-009 4.91e-008 n-Butane 2.51e-009 1.12e-007 Isopentane 1.30e-004 5.78e-003 n-Pentane 1.66e-004 7.41e-003 n-Hexane 5.07e-005 2.26e-003 Other Hexanes 4.16e-004 1.85e-002 Benzene 3.33e-004 1.48e-002 Toluene 2.33e-003 1.04e-001 Ethylbenzene 2.72e-003 1.21e-001 Xylenes 1.51e-002 6.72e-001 Total Components 100.00 4.46e+003

RICH GLYCOL AND PUMP GAS STREAM

Temperature: 120.00 deg. F Pressure: 1114.70 psia Flow Rate: 8.84e+000 gpm NOTE: Stream has more than one p	phase.	
Component		Loading (lb/hr)
Water Carbon Dioxide Nitrogen	8.93e+001 8.11e+000 2.13e-002 9.72e-003 1.12e+000	3.98e+002 1.05e+000 4.77e-001
Propane Isobutane	5.72e-001 3.30e-001 6.18e-002 1.54e-001 4.18e-002	1.62e+001 3.04e+000 7.57e+000
n-Hexane Other Hexanes Benzene	4.89e-002 1.35e-002 5.95e-002 6.11e-003 2.70e-002	6.61e-001 2.92e+000 3.00e-001
Ethylbenzene Xylenes	2.39e-002 1.06e-001	
Total Components	100.00	4.91e+003

FLASH TANK OFF GAS STREAM

Isobutane 9.77e-001 2.84e+000

n-Butane 2.38e+000 6.91e+000 Isopentane 5.08e-001 1.83e+000 n-Pentane 5.76e-001 2.08e+000 n-Hexane 1.17e-001 5.04e-001 Other Hexanes 5.52e-001 2.38e+000 Benzene 5.52e-003 2.16e-002 Toluene 1.21e-002 5.58e-002 Ethylbenzene 4.80e-003 2.55e-002 Xylenes 1.30e-002 6.91e-002 Total Components 100.00 1.17e+002

FLASH TANK GLYCOL STREAM

Temperature: 80.00 deg. F Flow Rate: 8.58e+000 gpm		
Component		Loading (lb/hr)
Water Carbon Dioxide Nitrogen	9.15e+001 8.30e+000 1.39e-003 3.34e-005 4.30e-003	3.98e+002 6.68e-002 1.60e-003
Propane Isobutane n-Butane	8.25e-003 1.34e-002 4.08e-003 1.38e-002 4.55e-003	6.42e-001 1.95e-001 6.62e-001
n-Hexane Other Hexanes Benzene	6.77e-003 3.28e-003 1.12e-002 5.81e-003 2.65e-002	1.57e-001 5.39e-001 2.78e-001
Ethylbenzene Xylenes	2.39e-002 1.07e-001	
Total Components	100.00	4.79e+003

FLASH GAS EMISSIONS

Flow Rate: 7.45e+003 scfh Control Method: Combustion Device Control Efficiency: 98.00 Component Conc. Loading (vol%) (lb/hr) Water 6.20e+001 2.19e+002 Carbon Dioxide 3.74e+001 3.23e+002 Nitrogen 8.65e-002 4.75e-001 Methane 3.47e-001 1.09e+000 Ethane 9.39e-002 5.54e-001 Propane 3.60e-002 3.11e-001 Isobutane 4.98e-003 5.68e-002 n-Butane 1.21e-002 1.38e-001 Isopentane 2.59e-003 3.67e-002 n-Pentane 2.94e-003 4.16e-002 n-Hexane 5.96e-004 1.01e-002

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Other Hexanes 2.81e-003 4.76e-002 Benzene 2.81e-005 4.31e-004 Toluene 6.18e-005 1.12e-003 Ethylbenzene 2.45e-005 5.10e-004 Xylenes 6.63e-005 1.38e-003 Total Components 100.00 5.45e+002

REGENERATOR OVERHEADS STREAM

Pressure:	212.00 deg. F 14.70 psia 7.56e+003 scfh		
	Component		Loading (lb/hr)
	Carbon Dioxide Nitrogen Methane	9.22e+001 1.92e-002 2.62e-002 5.45e+000 1.18e+000	1.68e-001 1.46e-001 1.74e+001
	Isobutane n-Butane Isopentane	4.43e-001 6.51e-002 1.62e-001 3.96e-002 4.76e-002	7.54e-001 1.88e+000 5.70e-001
	Other Hexanes Benzene	1.70e-002 6.37e-002	9.45e-001 2.65e-001 1.17e+000
	Xylenes	2.11e-001	4.47e+000
	Total Components	100.00	3.71e+002

CONDENSER PRODUCED WATER STREAM

	200.00 deg. F 4.56e-001 gpm			
	Component		Loading (lb/hr)	(ppm)
	Carbon Dioxide Nitrogen Methane		2.35e-006 4.49e-004	
	Isobutane n-Butane Isopentane	6.24e-005 6.11e-006 1.86e-005 3.59e-006 4.45e-006	1.39e-005 4.25e-005 8.20e-006	1. 0. 0. 0. 0.
	Other Hexanes Benzene	1.10e-004 3.54e-004	8.62e-006 2.50e-004 8.07e-004	0. 0. 1. 4. 2.
	Xylenes	1.18e-003	2.69e-003	12.

CONDENSER RECOVERED OIL STREAM

Temperature: 200.00 deg. F

The calculated flow rate is less than 0.000001 $\# {\rm mol/hr}.$ The stream flow rate and composition are not reported.

CONDENSER VENT STREAM

Pressure:	200.00 deg. F 14.70 psia 2.75e+003 scfh		
	Component		Loading (lb/hr)
	Carbon Dioxide Nitrogen Methane	7.85e+001 5.26e-002 7.20e-002 1.50e+001 3.23e+000	1.68e-001 1.46e-001 1.74e+001
	Isobutane n-Butane Isopentane	1.22e+000 1.79e-001 4.46e-001 1.09e-001 1.31e-001	7.54e-001 1.88e+000 5.70e-001
	Other Hexanes Benzene	4.67e-002 1.75e-001	9.45e-001 2.64e-001 1.17e+000
	Xylenes	5.80e-001	4.47e+000
	Total Components	100.00	1.43e+002

COMBUSTION DEVICE OFF GAS STREAM

Temperature: 1000.00 deg. F Pressure: 14.70 psia Flow Rate: 1.18e+001 scfh		
Component		Loading (lb/hr)
Ethane Propane Isobutane	7.00e+001 1.51e+001 5.68e+000 8.35e-001 2.08e+000	1.41e-001 7.78e-002 1.51e-002
n-Hexane Other Hexanes	6.11e-001 1.78e-001	1.37e-002 4.77e-003 1.89e-002
Ethylbenzene	8.17e-001 6.24e-001 2.71e+000	2.06e-002

Total Components 100.00 8.07e-001

Attachment O. Monitoring, Recordkeeping, Reporting, and Testing Plans

Monitoring, Recordkeeping, Reporting, and Testing Plans

The following is a summary of the methods to comply with the requirements of West Virginia Division of Air Quality (WVDAQ) 45CSR13 rules and regulations for the Underwood Compressor Station, including federal and state regulatory requirements.

1. Summary of Key Operational Throughput Limits

- a. Maximum wet gas throughput into each Dehy: 88 MMscf/day or 32,120 MMscf/year.
- b. Maximum liquids loaded out: 2,989,350 gallons per year.
- c. Maximum fuel use of all compressor engines is 1,346,061,600 scf/year

2. Operational Requirements

- a. Compressor engines will operate with the catalytic converter in place at all times and will be fueled by natural gas only.
- b. Catalysts installed on all compressor engines will be operated per manufacturer instructions.
- c. Reciprocating compressor rod packing will be replaced within 36 months of last packing/startup or within 26,000 operating hours, whichever comes first.
- d. Microturbines will be fueled by natural gas only.
- e. Each Dehy Reboiler will operate at no more than 1.5 MMBtu/hr and fueled only by natural gas or off-gases from the Dehydrator flash tanks.
- f. No fuel-burning unit of any kind will have opacity greater than 10 percent based on a six minute block average observation.
- g. The Dehy Flare capacity will not exceed 9.2 MMBtu/hr, will achieve 98 percent destruction efficiency, will operate at all times that gas is vented to it, will have a flame present at all times, and will have no visible emissions other than for periods not to exceed a total of 5 minutes during any 2 consecutive hours.
- h. The flare will be operated per manufacturer instructions.
- i. Produced water, Condensate, and Settling storage tanks potential emissions will be routed to the VRUs with recovery greater than 98 percent at all times.
- j. Storage tanks will be covered and routed to a closed vent system with no detectable emissions.
- k. Liquid loadout trucks will use the submerged-fill method.
- I. Dehydrator still vents will be controlled by the flare.
- m. Dehydrator flash tank vent gas is to be used in the reboiler as fuel or routed to the VRU system.

3. Monitoring

- a. Non-certified engines will be stack tested within 1 year of startup and every 8,760 hours of operation thereafter.
- b. Catalyst inlet temperature will be monitored.

- c. Compressor run time or number of months since compressor rod repacking will be monitored or tracked.
- d. Daily, monthly, and rolling 12-month average wet gas throughput for the Dehy will be monitored.
- e. Initial Method 22 observation of the Reboiler exhaust and flare will be conducted for a minimum of 2 hours.
- f. Monthly Method 22 observations of the Reboiler exhaust and flare will be conducted for a minimum of 10 minutes each.
- g. Monthly olfactory, visual, and auditory inspections will be conducted of the tanks closed vent and control system (flare) for leaks or defects that could result in emissions. Leaks will be repaired as soon as practicable (no later than 5 days for first attempt).
- h. The presence of flare flame will continuously be monitored.
- i. Monthly and rolling twelve-month average amount of liquids loaded out will be monitored.

4. Recordkeeping

- a. Records will be kept for a minimum of 5 years.
- b. Records of inspection, observations, preventive maintenance, malfunctions, and shutdowns of all onsite equipment will be kept.
- c. Records of the date, time, duration of each time that a flame is not present at the flare and startup, shutdown, malfunctions of the flare will be kept.
- d. Records of engine maintenance and engine run time will be kept.
- e. Records of catalyst inlet temperature will be kept.
- f. Records of the actual annual average natural gas throughput in the dehy will be kept.

5. Notifications and Reports

- a. WVDAQ will be notified within 30 calendar days of commencement of construction.
- b. WVDAQ will be notified within 30 calendar days of startup.
- c. Upon startup, a Certificate to Operate (CTO) application will be filed and fees to WVDAQ will be paid for the period from startup to the following June 30 and then annually renew the CTO and pay fees. CTO will be maintained on-site.
- d. An annual report of compliance with 40 CFR 60 Subpart OOOO for the compressors and storage tanks (for settling tank only) will be submitted within 90 days after one year of operation (i.e., within 90 days after 12 months after initial startup).
- e. For stack testing, a protocol will be filed at least 30 days prior to test and WVDAQ and EPA will be notified of the test at least 15 days prior to test. Results will be reported within 60 days of the test.
- f. If operations are suspended for 60 days or more, WVDAQ will be notified within 2 weeks after the 60th day.

Attachment P. Public Notice

AIR QUALITY PERMIT NOTICE Notice of Application – Underwood Compressor Station

Notice is given that Antero Midstream LLC has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a 45CSR13 Construction Permit Modification for a Natural Gas Compressor Station located west of Centerville and south of WV Route 18, in Tyler County, West Virginia. The latitude and longitude coordinates are: 39.432520N, 80.871581W.

The applicant estimates the increased potential to discharge of the following Regulated Air Pollutants will be: Sulfur Dioxide (SO₂): 0.12 tpy; Particulate Matter less than 10 μ m (PM₁₀): 3.70 tpy; Particulate Matter less than 2.5 μ m (PM_{2.5}): 3.70 tpy; Benzene: 0.30 tpy; Toluene: 0.084 tpy; Xylenes: 0.010 tpy; and Carbon Dioxide equivalent (CO₂e): 27,140 tpy.

The applicant estimates the decreased potential to discharge of the following Regulated Air Pollutants will be: Nitrogen Oxides (NOx): 4.54 tons per year (tpy); Carbon Monoxide (CO): 4.21 tpy; Volatile Organic Compounds (VOC): 28.63 tpy; Ethylbenzene – 0.011 tpy; n-Hexane: 0.12 tpy; and Formaldehyde: 0.87 tpy.

Startup of modified operation is planned to begin on or about the 1st day of June 2016. Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1250, during normal business hours. Dated this the 15th day of February 2016.

By: Antero Midstream LLC Barry Schatz Midstream Environmental Supervisor 1615 Wynkoop Street Denver, CO 80202 Attachment R. Authority/Delegation of Authority

Attachment R AUTHORITY OF CORPORATION OR OTHER BUSINESS ENTITY (DOMESTIC OR FOREIGN)

TO: The West Virginia Department of Environmental Protection, Division of Air Quality

DATE: August 5 , 2015

ATTN.: Director

Corporation's / other business entity's Federal Employer I.D. Number _____46-5517375

The undersigned hereby files with the West Virginia Department of Environmental Protection, Division of Air Quality, a permit application and hereby certifies that the said name is a trade name which is used in the conduct of an incorporated business or other business entity.

Further, the corporation or the business entity certifies as follows:

(1) Luz Slauter and Barry Schatz (is/are) the authorized representative(s) and in that capacity may represent the interest of the corporation or the business entity and may

obligate and legally bind the corporation or the business entity.

(2) The corporation or the business entity is authorized to do business in the State of West Virginia.

(3) If the corporation or the business entity changes its authorized representative(s), the corporation or the business entity shall notify the Director of the West Virginia Department of Environmental Protection, Division of Air Quality, immediately upon such change.

Ward McNeilly, Vice President - Vice President Reserves Planning & Midstream

President or Other Authorized Officer (Vice President, Secretary, Treasurer or other official in charge of a principal business function of the corporation or the business entity)

(If not the President, then the corporation or the business entity must submit certified minutes or bylaws stating legal authority of other authorized officer to bind the corporation or the business entity).

Secretary

Antero Midstream LLC