

Compressor Station 119A

Air Permit Application



**Tennessee Gas Pipeline
Company, L.L.C.**
a Kinder Morgan company

Tennessee Gas
Pipeline Company
1001 Louisiana Street
Houston, TX 77002

January 30, 2015

Mr. William F. Durham, Director
West Virginia Department of Environmental Protection
Division of Air Quality
601 57th Street, SE
Charleston, West Virginia, 25304

**RE: NSR Permit Application
Tennessee Gas Pipeline Company, L.L.C.
Compressor Station 119A**

Dear Director Durham:

Enclosed are three copies of a New Source Review Permit Application pursuant to WV 45 CSR 13 for the construction of a new greenfield compressor station, Station 119A. A legal advertisement will be published in the next few days and proof of publication will be forwarded as soon as it is received. Enclosed is a check in the amount of \$4,500.

If you have any questions concerning this permit application, please contact myself at (713) 420-6318 or at Shrishti_Chhabra@kindermorgan.com.

Sincerely,

Shrishti Chhabra
Environmental Engineer III
Kinder Morgan, Inc.

Enclosures

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INTRODUCTION

Tennessee Gas Pipeline Company, L.L.C. (TGP), which is owned by Kinder Morgan, Inc., operates a 13,900 mile pipeline that transports natural gas from Louisiana, the Gulf of Mexico and south Texas to the northeast section of the United States (U.S.), including New York City and Boston.

As part of the Broad Run Expansion Project (BRE), TGP is proposing to construct a new green field compressor station (Station 119A) in Charleston, Kanawha County, West Virginia (WV). Station 119A will consist of one new compressor turbine and additional auxiliary equipment, as described below, and will be a minor source with respect to both the Title V Operating Program and Prevention of Significant Deterioration (PSD). Therefore, TGP is submitting this Regulation 13 Construction Permit to request approval to construct and operate Station 119A as a minor source under WV 45CSR 13, and to comply with the air permitting requirements and regulations of the state of WV. Operations at the facility are projected to commence in October 2017.

Attachments A through S include all required application information, figures, and forms, as summarized in the Table of Contents. Please note that an estimate of criteria and hazardous/toxic pollutant emissions is included within this permit application in Attachment N for all of the sources proposed at Station 119A.

FACILITY DESCRIPTION

Station 119A will be used to boost transmission pressures by compressing low pressure transmission gas and directing it into a high pressure transmission line. Natural gas will enter Station 119A from a transmission pipeline where one (1) Solar Turbines Titan 130-20502S natural gas fired compressor turbine, with a maximum design capacity of 168 million British Thermal Units per hour (MMBtu/hr), higher heating value (HHV) basis, will increase the line pressure. In addition, TGP is proposing to add one (1) new Caterpillar G 3516 LE natural gas-fired emergency generator, one Parker Boiler T-4600LR natural gas fired hydronic heater, and one new pipeline liquids storage tank.

Various support activities will be carried out at Station 119A in order to maintain proper operation of the compressor turbine, the pipeline, and any auxiliary equipment on-site.

Operations at Station 119A will be categorized under the Standard Industrial Classification (SIC) code 4922, *Natural Gas Transmission*, and under the North American Industry Classification System (NAICS) code 486210, *Pipeline Transportation of Natural Gas*.

All proposed combustion equipment at Station 119A will utilize only pipeline quality natural gas. Emissions of concern are primarily products of combustion: nitrogen oxides (NO_x), carbon monoxide (CO), and volatile organic compounds (VOC). TGP will employ good combustion practices on well-maintained engines along with the exclusive use of natural gas in order to minimize air emissions.

EMISSIONS CALCULATION METHODOLOGY

Emissions from the sources proposed at Station 119A will consist primarily of natural gas combustion emissions from the addition of the new Solar turbine. Additional emissions will occur from one new storage tank, natural gas combustion emissions from the new emergency generator and hydronic heater, from additional fugitive components, and from venting/blow downs. Emissions estimates for each of these sources have been calculated using the most appropriate information and the most current methodologies available to determine the facility's potential to emit (PTE), as described in the following sections, and as shown in Attachment N.

Solar Titan 130-20502S Compressor Turbine

CO, NO_x, VOC, and methane (CH₄) emissions from the new compressor turbine, 119-CT-01, are based on vendor supplied information. Sulfur dioxide (SO₂) and all particulate matter (PM) emissions are based on US EPA's "Emissions Factors & AP 42, Compilation of Air Pollutant Emission Factors" (AP-42), Table 3.1-2a, *Emission Factors for Criteria Pollutants and Greenhouse Gases from Stationary Gas Turbines*. Other greenhouse gas (GHG) emissions are based on 40 CFR Part 98, Subpart C, Tables C-1 and C-2, *Default CO₂ Emission Factors and High Heat Values for Various Types of Fuel and Default CH₄ and N₂O Emission Factors for Various Types of Fuel*.

All emission calculations have been based on a maximum HHV of 1,020 British thermal units per standard cubic feet (BTU/scf). Also note that VOC and CH₄ emissions have been based on assumed composition percent values of total unburned hydrocarbons (UHC). UHC emissions are assumed to be composed of 20 percent VOC, and 80 percent CH₄.

For a Titan 130-20502S unit at typical ambient operating temperatures (at 0°F or above), Solar Turbines states that: "Solar's gas turbine dry low NO_x emissions combustion system, known as SoLoNO_x, is designed to reduce NO_x, CO, and unburned UHC without penalizing stability or transient capabilities." The new turbine will be equipped with Solar's SoLoNO_x technology, which uses a "lean-premixed combustion technology to ensure uniform air/fuel mixture and to prevent formation of regulated pollutants". For SoLoNO_x operation at 0°F ambient temperatures or above, Solar Turbines guarantees that the following emission levels will be met:

- 1) 25.0 ppm NO_x at 15 percent oxygen (O₂).
- 2) 25.0 ppm CO at 15 percent O₂.
- 3) 25.0 ppm UHC at 15 percent O₂.

However, at subzero ambient operating temperatures, these emissions increase due to system control modifications required to maintain stable operation at very low temperatures. Since Solar does not provide a warranty for the lower emissions associated with the SoLoNO_x system at subzero temperatures, the turbine hourly emissions included in Attachment N are shown for operation at -10°F, 0°F, and at 50°F (50°F chosen as a conservative ambient operating temperature for the majority of the annual emissions as described below) to demonstrate this difference. More information

regarding Solar's *SoLoNO_x* emission system can be found in Attachment L (see Solar Turbines' Product Information Letter 167).

Annual emissions for the compressor turbine included in Attachment N take into consideration the emissions variations based on ambient temperatures, and incorporate the potential for subzero ambient temperatures to occur during operation. The annual emissions are therefore based on a conservative maximum of 100 hours of operation per year at ambient temperatures less than 0°F, and remaining hours at a conservative annual average ambient temperature of 50.0°F. This is a conservative estimate, as the turbine may operate up to 8,760 hours per year at *SoLoNO_x* guaranteed emission rates at temperatures above 0.0°F.

Start-up and shutdown emissions for the compressor turbine have also been included in the annual emission totals. Emission totals for start-up and shutdown operations have been determined based on Solar Turbines' Product Information Letter 170 (see Attachment L). Typical start-up and shutdown times are expected to each be less than 10 minutes.

Caterpillar G 3516 LE Emergency Generator

The new lean-burn natural gas emergency generator (Caterpillar Model G 3516 LE), 119-EG-03, will be used to provide electrical power during interruption of normal service. CO, NO_x, and VOC emissions from the new generator are based on applicable emission standards from 40 CFR 60 Subpart JJJJ, *Standards of Performance for Stationary Spark Ignition Internal Combustion Engines, Table 1* for emergency engines. TGP will either purchase a generator engine which will meet the NSPS JJJJ CO, NO_x, and VOC standards and perform emission testing as required, or will purchase an engine certified to meet these limits. CH₄, SO₂ and all PM emissions are based on AP-42, Table 3.2-2, *Uncontrolled Emission Factors for 4-Stroke Lean-Burn Engines*, and other GHG emissions are based on 40 CFR Part 98, Subpart C, Tables C-1 and C-2, *Default CO₂ Emission Factors and High Heat Values for Various Types of Fuel and Default CH₄ and N₂O Emission Factors for Various Types of Fuel*. Annual emissions estimates are based on a maximum of 500 hours of total operation per year.

Parker Boiler T-4600LR Hydronic Heater

Emissions from the hydronic heater, 119-WH-02, are based on AP-42, Table 1.4-2, *Emission Factors for Criteria Pollutants and Greenhouse Gases from Natural Gas Combustion* and on vendor provided data. The heater will be used for fuel gas conditioning purposes.

Fugitive Emissions

Fugitive emissions are expected from new components and piping utilized at the station for the purposes of conveying natural gas and other materials into, within, and out of the facility. Please note that the fugitive component counts represented in the fugitive emission calculations included in Attachment N have been estimated based on design data as well as on component counts at a similar natural gas compressor station. The estimation of fugitive emissions is based on U.S. EPA document, EPA-453/R-95-017 (Protocol for Equipment Leak Emission Estimates, 1995).

Storage Tank and Truck Loading Emissions

One (1) pipeline liquids storage tank, 119-PF-04, will be installed at Station 119A as part of BRE. Tank emissions have been estimated using E&P software, and account for both working losses and breathing losses, as well as flashing losses. Additionally, pipeline liquids truck loading emissions (119-LR-05) have been calculated using AP-42, Section 5.2, Equation 1, *Transportation and Marketing of Petroleum Liquids*, Section 5.2, Equation 1.

Venting/Blow Down Emissions

Station 119A will be equipped with a shutdown system that is able to block natural gas out of the station and blow down the station piping. System blow down will be directed to natural gas blowdown stacks. The shutdown system will be required to be inspected and tested on an annual basis. Natural gas will be vented from the blowdown stacks during the system tests. Gas venting and blowdown emissions are based on an assumed annual volume of natural gas released, and an estimated natural gas composition.



WEST VIRGINIA DEPARTMENT OF ENVIRONMENTAL PROTECTION
DIVISION OF AIR QUALITY

601 57th Street, SE
Charleston, WV 25304
(304) 926-0475
www.dep.wv.gov/daq

**APPLICATION FOR NSR PERMIT
AND
TITLE V PERMIT REVISION
(OPTIONAL)**

PLEASE CHECK ALL THAT APPLY TO **NSR (45CSR13)** (IF KNOWN):

- CONSTRUCTION** **MODIFICATION** **RELOCATION**
 CLASS I ADMINISTRATIVE UPDATE **TEMPORARY**
 CLASS II ADMINISTRATIVE UPDATE **AFTER-THE-FACT**

PLEASE CHECK TYPE OF **45CSR30 (TITLE V)** REVISION (IF ANY):

- ADMINISTRATIVE AMENDMENT** **MINOR MODIFICATION**
 SIGNIFICANT MODIFICATION

IF ANY BOX ABOVE IS CHECKED, INCLUDE TITLE V REVISION INFORMATION AS **ATTACHMENT S** TO THIS APPLICATION

FOR TITLE V FACILITIES ONLY: Please refer to "Title V Revision Guidance" in order to determine your Title V Revision options (Appendix A, "Title V Permit Revision Flowchart") and ability to operate with the changes requested in this Permit Application.

Section I. General

1. Name of applicant (as registered with the WV Secretary of State's Office): Tennessee Gas Pipeline Company, L.L.C.		2. Federal Employer ID No. (FEIN): 45-3953911	
3. Name of facility (if different from above): Compressor Station 119A		4. The applicant is the: <input type="checkbox"/> OWNER <input type="checkbox"/> OPERATOR <input checked="" type="checkbox"/> BOTH	
5A. Applicant's mailing address: 1001 Louisiana St. Houston, TX 77002		5B. Facility's present physical address: From Charleston, WV. Begin on Washington St until road ends. Turn left onto Iowa St. Take the 1st right onto 7th St and travel for 2.2 miles. Take slight right onto WV-62N/Washington St W and travel 1.7 miles. Turn right onto WV-501 N and travel for 2.9 miles. Turn right onto WV-622 N/Rocky Fork Rd and travel for 2.0 miles. Turn right onto Berry Ln.	
6. West Virginia Business Registration. Is the applicant a resident of the State of West Virginia? <input type="checkbox"/> YES <input checked="" type="checkbox"/> NO – If YES , provide a copy of the Certificate of Incorporation/Organization/Limited Partnership (one page) including any name change amendments or other Business Registration Certificate as Attachment A . – If NO , provide a copy of the Certificate of Authority/Authority of L.L.C./Registration (one page) including any name change amendments or other Business Certificate as Attachment A .			
7. If applicant is a subsidiary corporation, please provide the name of parent corporation: Kinder Morgan Energy Partners, L.P.			
8. Does the applicant own, lease, have an option to buy or otherwise have control of the <i>proposed site</i> ? <input checked="" type="checkbox"/> YES <input type="checkbox"/> NO – If YES , please explain: The applicant leases the proposed site. – If NO , you are not eligible for a permit for this source.			
9. Type of plant or facility (stationary source) to be constructed, modified, relocated, administratively updated or temporarily permitted (e.g., coal preparation plant, primary crusher, etc.): Natural Gas Transmission Facility		10. North American Industry Classification System (NAICS) code for the facility: 486210	

11A. DAQ Plant ID No. (for existing facilities only): N/A	11B. List all current 45CSR13 and 45CSR30 (Title V) permit numbers associated with this process (for existing facilities only): N/A	
All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.		
12A. <ul style="list-style-type: none"> - For Modifications, Administrative Updates or Temporary permits at an existing facility, please provide directions to the <i>present location</i> of the facility from the nearest state road; - For Construction or Relocation permits, please provide directions to the <i>proposed new site location</i> from the nearest state road. Include a MAP as Attachment B. <p>From Charleston, WV. Begin on Washington St until road ends. Turn left onto Iowa St. Take the 1st right onto 7th St and travel for 2.2 miles. Take slight right onto WV-62N/Washington St W and travel 1.7 miles. Turn right onto WV-501 N and travel for 2.9 miles. Turn right onto WV-622 N/Rocky Fork Rd and travel for 2.0 miles. Turn right onto Berry Ln. See Attachment B for map.</p>		
12.B. New site address (if applicable): TBD	12C. Nearest city or town: Charleston	12D. County: Kanawha
12.E. UTM Northing (KM): 4,255.99	12F. UTM Easting (KM): 437.43	12G. UTM Zone: 17
13. Briefly describe the proposed change(s) at the facility: Compressor Station 119A is a proposed natural gas transmission station.		
14A. Provide the date of anticipated installation or change: February 2016 - If this is an After-The-Fact permit application, provide the date upon which the proposed change did happen: NA		14B. Date of anticipated Start-Up if a permit is granted: October 2017
14C. Provide a Schedule of the planned Installation of/Change to and Start-Up of each of the units proposed in this permit application as Attachment C (if more than one unit is involved).		
15. Provide maximum projected Operating Schedule of activity/activities outlined in this application: Hours Per Day 24 Days Per Week 7 Weeks Per Year 52		
16. Is demolition or physical renovation at an existing facility involved? <input type="checkbox"/> YES <input checked="" type="checkbox"/> NO		
17. Risk Management Plans. If this facility is subject to 112(r) of the 1990 CAAA, or will become subject due to proposed changes (for applicability help see www.epa.gov/ceppo), submit your Risk Management Plan (RMP) to U. S. EPA Region III.		
18. Regulatory Discussion. List all Federal and State air pollution control regulations that you believe are applicable to the proposed process (<i>if known</i>). A list of possible applicable requirements is also included in Attachment S of this application (Title V Permit Revision Information). Discuss applicability and proposed demonstration(s) of compliance (<i>if known</i>). Provide this information as Attachment D .		
Section II. Additional attachments and supporting documents.		
19. Include a check payable to WVDEP – Division of Air Quality with the appropriate application fee (per 45CSR22 and 45CSR13).		
20. Include a Table of Contents as the first page of your application package.		
21. Provide a Plot Plan , e.g. scaled map(s) and/or sketch(es) showing the location of the property on which the stationary source(s) is or is to be located as Attachment E (Refer to Plot Plan Guidance) . - Indicate the location of the nearest occupied structure (e.g. church, school, business, residence).		
22. Provide a Detailed Process Flow Diagram(s) showing each proposed or modified emissions unit, emission point and control device as Attachment F .		

23. Provide a **Process Description** as **Attachment G**.

– Also describe and quantify to the extent possible all changes made to the facility since the last permit review (if applicable).

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

24. Provide **Material Safety Data Sheets (MSDS)** for all materials processed, used or produced as **Attachment H**.

– For chemical processes, provide a MSDS for each compound emitted to the air.

25. Fill out the **Emission Units Table** and provide it as **Attachment I**.

26. Fill out the **Emission Points Data Summary Sheet (Table 1 and Table 2)** and provide it as **Attachment J**.

27. Fill out the **Fugitive Emissions Data Summary Sheet** and provide it as **Attachment K**.

28. Check all applicable **Emissions Unit Data Sheets** listed below:

<input checked="" type="checkbox"/> Bulk Liquid Transfer Operations	<input type="checkbox"/> Haul Road Emissions	<input type="checkbox"/> Quarry
<input type="checkbox"/> Chemical Processes	<input type="checkbox"/> Hot Mix Asphalt Plant	<input type="checkbox"/> Solid Materials Sizing, Handling and Storage Facilities
<input type="checkbox"/> Concrete Batch Plant	<input type="checkbox"/> Incinerator	<input checked="" type="checkbox"/> Storage Tanks
<input type="checkbox"/> Grey Iron and Steel Foundry	<input type="checkbox"/> Indirect Heat Exchanger	

General Emission Unit, specify - **Line Heater, Generator, Turbine**

Fill out and provide the **Emissions Unit Data Sheet(s)** as **Attachment L**.

29. Check all applicable **Air Pollution Control Device Sheets** listed below:

<input type="checkbox"/> Absorption Systems	<input type="checkbox"/> Baghouse	<input type="checkbox"/> Flare
<input type="checkbox"/> Adsorption Systems	<input type="checkbox"/> Condenser	<input type="checkbox"/> Mechanical Collector
<input type="checkbox"/> Afterburner	<input type="checkbox"/> Electrostatic Precipitator	<input type="checkbox"/> Wet Collecting System

Other Collectors, specify **N/A**

Fill out and provide the **Air Pollution Control Device Sheet(s)** as **Attachment M**.

30. Provide all **Supporting Emissions Calculations** as **Attachment N**, or attach the calculations directly to the forms listed in Items 28 through 31.

31. **Monitoring, Recordkeeping, Reporting and Testing Plans.** Attach proposed monitoring, recordkeeping, reporting and testing plans in order to demonstrate compliance with the proposed emissions limits and operating parameters in this permit application. Provide this information as **Attachment O**.

➤ Please be aware that all permits must be practically enforceable whether or not the applicant chooses to propose such measures. Additionally, the DAQ may not be able to accept all measures proposed by the applicant. If none of these plans are proposed by the applicant, DAQ will develop such plans and include them in the permit.

32. **Public Notice.** At the time that the application is submitted, place a **Class I Legal Advertisement** in a newspaper of general circulation in the area where the source is or will be located (See 45CSR§13-8.3 through 45CSR§13-8.5 and **Example Legal Advertisement** for details). Please submit the **Affidavit of Publication** as **Attachment P** immediately upon receipt.

33. **Business Confidentiality Claims.** Does this application include confidential information (per 45CSR31)?

YES NO

➤ If **YES**, identify each segment of information on each page that is submitted as confidential and provide justification for each segment claimed confidential, including the criteria under 45CSR§31-4.1, and in accordance with the DAQ's "**Precautionary Notice – Claims of Confidentiality**" guidance found in the **General Instructions** as **Attachment Q**.

Section III. Certification of Information

34. **Authority/Delegation of Authority.** Only required when someone other than the responsible official signs the application. Check applicable **Authority Form** below:

<input type="checkbox"/> Authority of Corporation or Other Business Entity	<input type="checkbox"/> Authority of Partnership
<input type="checkbox"/> Authority of Governmental Agency	<input type="checkbox"/> Authority of Limited Partnership

Submit completed and signed **Authority Form** as **Attachment R**.

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

35A. **Certification of Information.** To certify this permit application, a Responsible Official (per 45CSR§13-2.22 and 45CSR§30-2.28) or Authorized Representative shall check the appropriate box and sign below.

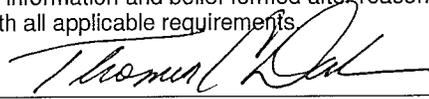
Certification of Truth, Accuracy, and Completeness

I, the undersigned **Responsible Official** / **Authorized Representative**, hereby certify that all information contained in this application and any supporting documents appended hereto, is true, accurate, and complete based on information and belief after reasonable inquiry I further agree to assume responsibility for the construction, modification and/or relocation and operation of the stationary source described herein in accordance with this application and any amendments thereto, as well as the Department of Environmental Protection, Division of Air Quality permit issued in accordance with this application, along with all applicable rules and regulations of the West Virginia Division of Air Quality and W.Va. Code § 22-5-1 et seq. (State Air Pollution Control Act). If the business or agency changes its Responsible Official or Authorized Representative, the Director of the Division of Air Quality will be notified in writing within 30 days of the official change.

Compliance Certification

Except for requirements identified in the Title V Application for which compliance is not achieved, I, the undersigned hereby certify that, based on information and belief formed after reasonable inquiry, all air contaminant sources identified in this application are in compliance with all applicable requirements.

SIGNATURE



(Please use blue ink)

DATE:

1-26-15

(Please use blue ink)

35B. Printed name of signer: **Thomas C. Dender**

35C. Title: **Vice President, Eastern Region**

35D. E-mail:
Tom_Dender@kindermorgan.com

35E. Phone: **713-420-3833**

35F. FAX:

36A. Printed name of contact person (if different from above): **Shrishti Chhabra**

36B. Title: **Environmental Engineer III**

36C. E-mail:
Shrishti_Chhabra@kindermorgan.com

36D. Phone: **713-420-6318**

36E. FAX:

PLEASE CHECK ALL APPLICABLE ATTACHMENTS INCLUDED WITH THIS PERMIT APPLICATION:

- | | |
|--|--|
| <input checked="" type="checkbox"/> Attachment A: Business Certificate | <input checked="" type="checkbox"/> Attachment K: Fugitive Emissions Data Summary Sheet |
| <input checked="" type="checkbox"/> Attachment B: Map(s) | <input checked="" type="checkbox"/> Attachment L: Emissions Unit Data Sheet(s) |
| <input checked="" type="checkbox"/> Attachment C: Installation and Start Up Schedule | <input checked="" type="checkbox"/> Attachment M: Air Pollution Control Device Sheet(s) |
| <input checked="" type="checkbox"/> Attachment D: Regulatory Discussion | <input checked="" type="checkbox"/> Attachment N: Supporting Emissions Calculations |
| <input checked="" type="checkbox"/> Attachment E: Plot Plan | <input checked="" type="checkbox"/> Attachment O: Monitoring/Recordkeeping/Reporting/Testing Plans |
| <input checked="" type="checkbox"/> Attachment F: Detailed Process Flow Diagram(s) | <input checked="" type="checkbox"/> Attachment P: Public Notice |
| <input checked="" type="checkbox"/> Attachment G: Process Description | <input checked="" type="checkbox"/> Attachment Q: Business Confidential Claims |
| <input checked="" type="checkbox"/> Attachment H: Material Safety Data Sheets (MSDS) | <input checked="" type="checkbox"/> Attachment R: Authority Forms |
| <input checked="" type="checkbox"/> Attachment I: Emission Units Table | <input checked="" type="checkbox"/> Attachment S: Title V Permit Revision Information |
| <input checked="" type="checkbox"/> Attachment J: Emission Points Data Summary Sheet | <input checked="" type="checkbox"/> Application Fee |

Please mail an original and three (3) copies of the complete permit application with the signature(s) to the DAQ, Permitting Section, at the address listed on the first page of this application. Please DO NOT fax permit applications.

FOR AGENCY USE ONLY – IF THIS IS A TITLE V SOURCE:

- Forward 1 copy of the application to the Title V Permitting Group and:
- For Title V Administrative Amendments:
 - NSR permit writer should notify Title V permit writer of draft permit,
- For Title V Minor Modifications:
 - Title V permit writer should send appropriate notification to EPA and affected states within 5 days of receipt,
 - NSR permit writer should notify Title V permit writer of draft permit.
- For Title V Significant Modifications processed in parallel with NSR Permit revision:
 - NSR permit writer should notify a Title V permit writer of draft permit,
 - Public notice should reference both 45CSR13 and Title V permits,
 - EPA has 45 day review period of a draft permit.

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

Kinder Morgan Energy Partners & Affiliates

No. 1140637

Check Date: 01/23/2015
(100040638)

WVDEP - DIV OF AIR QUALITY, 601 57TH STREET, SE, CHARLESTON WV 25304

Description	Voucher #	Date	PO Number	Gross Amount	Discount Amount	Net Amount Paid
PMTREQAIRPERMITFEE Kindly call X36318 when the check is ready to be picked up. This is an urgent request and has necessary approval. If the agency name is too long, please make the check payable to: WVDEP-DAQ. Attention of William Durham, West Virginia Department of Environmental Protection, Division of Air Quality. This is an urgent request with necessary approval.	11076342	01/21/15		\$4,500.00	\$0.00	\$4,500.00
Totals				\$4,500.00	\$0.00	\$4,500.00

Detach at Perforation Before Depositing Check
100040638



Kinder Morgan Energy Partners & Affiliates
1001 Louisiana Ste 1000
Houston, TX 77002

Wells Fargo Bank Ohio, N.A.
115 Hospital Drive
Van Wert, OH 45891
56-382/412

Check No. 1140637

Check Date:
01/23/2015

Check Amount
\$ *****4,500.00

PAY Four Thousand Five Hundred AND 00/100

TO THE ORDER OF

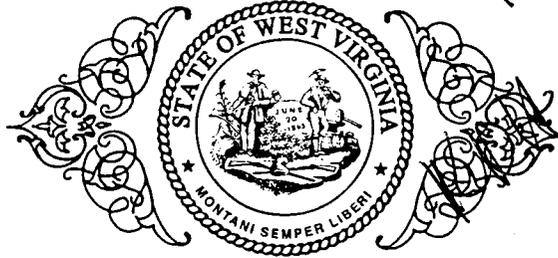
WVDEP - DIV OF AIR QUALITY
601 57TH STREET SE
CHARLESTON WV 25304

100040638

K. Dang

Attachment A

State of West Virginia



Certificate

I, Natalie E. Tennant, Secretary of State of the State of West Virginia, hereby certify that

TENNESSEE GAS PIPELINE COMPANY
(A DELAWARE Corporation)

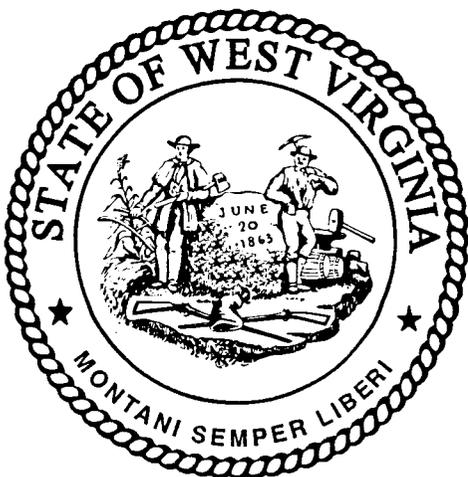
filed Articles of Conversion in my office as required by the provisions of the West Virginia Code and was found to conform to law.

Therefore, I issue this

CERTIFICATE OF CONVERSION

Converting the corporation and changing the name to:

TENNESSEE GAS PIPELINE COMPANY, L.L.C.
(A DELAWARE Limited Liability Company)



Given under my hand and the Great Seal of the State of West Virginia on
October 18, 2011

Natalie E. Tennant

Secretary of State

Delaware

PAGE 1

The First State

I, JEFFREY W. BULLOCK, SECRETARY OF STATE OF THE STATE OF DELAWARE DO HEREBY CERTIFY THAT THE ATTACHED IS A TRUE AND CORRECT COPY OF THE CERTIFICATE OF CONVERSION OF A DELAWARE CORPORATION UNDER THE NAME OF "TENNESSEE GAS PIPELINE COMPANY" TO A DELAWARE LIMITED LIABILITY COMPANY, CHANGING ITS NAME FROM "TENNESSEE GAS PIPELINE COMPANY" TO "TENNESSEE GAS PIPELINE COMPANY, L.L.C.", FILED IN THIS OFFICE ON THE THIRTIETH DAY OF SEPTEMBER, A.D. 2011, AT 6:46 O'CLOCK P.M.

AND I DO HEREBY FURTHER CERTIFY THAT THE EFFECTIVE DATE OF THE AFORESAID CERTIFICATE OF CONVERSION IS THE FIRST DAY OF OCTOBER, A.D. 2011, AT 8:05 O'CLOCK A.M.

FILED

OCT 18 2011

IN THE OFFICE OF
SECRETARY OF STATE



0414109 8100V

111096809

You may verify this certificate online
at corp.delaware.gov/authver.shtml


Jeffrey W. Bullock, Secretary of State
AUTHENTICATION: 9089637

DATE: 10-13-11

**CERTIFICATE OF CONVERSION
FROM A CORPORATION TO A
LIMITED LIABILITY COMPANY
PURSUANT TO SECTION 266
OF THE DELAWARE
GENERAL CORPORATION LAW
AND SECTION 18-214 OF THE
DELAWARE LIMITED LIABILITY COMPANY ACT**

This Certificate of Conversion of Tennessee Gas Pipeline Company (the "Corporation") effective on October 1, 2011, is being duly executed and filed by an authorized person of the Corporation to convert the Corporation to a Delaware limited liability company in accordance with Section 266 of the Delaware General Corporation Law (the "DGCL") and Section 18-214 of the Delaware Limited Liability Company Act (the "DLLCA").

1. The name of the Corporation set forth in its original Certificate of Incorporation was:

Tennessee Gas Transmission Company
2. The name of the Corporation immediately prior to filing this Certificate of Conversion was:

Tennessee Gas Pipeline Company
3. The jurisdiction of the Corporation immediately prior to filing this Certificate of Conversion was:

Delaware
4. The jurisdiction where the Corporation was first created is:

Delaware
5. The date the Certificate of Incorporation of the Corporation was filed is:

June 9, 1947
6. The name of the limited liability company (the "LLC") as set forth in its Certificate of Formation is:

Tennessee Gas Pipeline Company, L.L.C.
7. This conversion has been approved in accordance with the provisions of Section 266 of the DGCL and Section 18-214 of the DLLCA.
8. This Certificate of Conversion shall be effective at 8:05 a.m. Eastern Time on October 1, 2011.

FILED

OCT 18 2011

IN THE OFFICE OF
SECRETARY OF STATE

IN WITNESS WHEREOF, this Certificate of Conversion has been executed by an authorized person of the Corporation on the 29th day of September, 2011.

By: Stacy J. James
Stacy J. James
Corporate Secretary

**CERTIFICATE OF FORMATION
OF
TENNESSEE GAS PIPELINE COMPANY, L.L.C.**

This Certificate of Formation of Tennessee Gas Pipeline Company, L.L.C. (the "LLC") dated as of September 29, 2011, is being duly executed and filed by the undersigned, as an authorized person, to form a limited liability company under the Delaware Limited Liability Company Act, 6 Del. C. §§ 18-101, et. seq.

FIRST: The name of the LLC formed hereby is:

Tennessee Gas Pipeline Company, L.L.C.

SECOND: The address of the registered office of the LLC in the State of Delaware is:

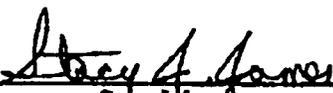
Corporation Trust Center
1209 Orange Street
New Castle County
Wilmington, Delaware 19801

THIRD: The name and address of the registered agent for services of process on the LLC in the State of Delaware are:

The Corporation Trust Company
Corporation Trust Center
1209 Orange Street
New Castle County
Wilmington, Delaware 19801

FOURTH: The Certificate of Formation shall be effective at 8:05 a.m. Eastern Time on October 1, 2011.

IN WITNESS WHEREOF, the undersigned has caused this Certificate of Formation to be executed, this 29th day of September, 2011.



Stacy J. James
Authorized Person

Natalie E. Tennant
Secretary of State
1900 Kanawha Blvd E.
Bldg 1, Suite 157-K
Charleston, WV 25305



Penney Barker, Manager
Corporations Division
Tel: (304)558-8000
Fax: (304)558-8381
www.wvssos.com

Hrs: 8:30 a.m. – 5:00 p.m. ET

FILE ONE ORIGINAL
(Two if you want a filed
stamped copy returned to you)
FEE: \$150

**WV APPLICATION FOR
CERTIFICATE OF AUTHORITY OF
LIMITED LIABILITY COMPANY**

Control # _____

****A certificate of existence from your home state of organization, dated during the current tax year, must accompany this application****

1. The name of the company as registered in its home state is: Tennessee Gas Pipeline Company, L.L.C.
and the state or country of organization is: Delaware

2. The name to be used in West Virginia will be:
[The name must contain one of the required terms such as "limited liability company" or abbreviations such as "LLC" or "PLLC". See instructions for complete list of acceptable terms and requirements for use of trade name]

Home State name as listed above, if available in WV
 DBA name _____
(ONLY if home state name is unavailable in WV)

3. The company will be a: [See instructions for limitations on professions which may form P.L.L.C. in WV. All members must have WV professional license.]

regular L.L.C.
 professional L.L.C. for the profession of _____

FILED

OCT 18 2011

IN THE OFFICE OF
SECRETARY OF STATE

4. The address of the designated office of the company in WV, if any, will be:

No. & Street: _____
City/State/Zip: _____

5. The street address of the principal office is:
and the mailing address (if different) is:

No. & Street: 1001 Louisiana St.
City/State/Zip: Houston, TX 77002
Street/Box: _____
City/State/Zip: _____

6. Agent of Process:
Properly designated person to whom notice of process may be sent, if any:

Name: C T Corporation System
Address: 5400 D Big Tyler Road
City/State/Zip: Charleston, West Virginia 25313

7. E-mail address where business correspondence can be received: esper.jett@elpaso.com

8. The company is: an at-will company, for an indefinite period
 a term company, for the term of _____ years, which will expire on _____.
9. The company is: member-managed. [List the names and addresses of all members]
 manager-managed. [List the names and addresses of all managers]

List the name(s) of the members/managers of the company (attach additional pages if necessary)

Name	Address	City, State, Zip
El Paso TGPC Investments, L.L.C.	1001 Louisiana St. Houston, TX 77002	

10. All or specified members of a limited liability company are liable in their capacity as members for all or specified debts, obligations or liabilities of the company. No--All debts, obligations and liabilities are those of the company
 Yes--Those persons who are liable in their capacity as members for all debts, obligations or liability of the company have consented in writing to the adoption of the provision or to be bound by the provision

11. The purpose for which this limited liability company is formed are as follows:
 (Describe the type(s) of business activity which will be conducted. for example. "real estate." "construction of residential and commercial buildings." "commercial printing." "professional practice of architecture.")

transport natural gas

12. The number of pages attached and included in this application is: 3

13. The requested date for the establishment of the limited liability company in WV is: the date & time of filing
 the following date _____ time _____

14. Contact and Signature Information:

a. Esper Jett 713-420-1477
 Contact Name Phone Number

b. Stacy J. James Corporate Secretary
 Print or type name of signer Title / Capacity of Signer

c. *Stacy J. James* 10/13/2011
 Signature Date

Delaware

PAGE 2

The First State

I, JEFFREY W. BULLOCK, SECRETARY OF STATE OF THE STATE OF DELAWARE DO HEREBY CERTIFY THAT THE ATTACHED IS A TRUE AND CORRECT COPY OF CERTIFICATE OF FORMATION OF "TENNESSEE GAS PIPELINE COMPANY, L.L.C." FILED IN THIS OFFICE ON THE THIRTIETH DAY OF SEPTEMBER, A.D. 2011, AT 6:46 O'CLOCK P.M.

AND I DO HEREBY FURTHER CERTIFY THAT THE EFFECTIVE DATE OF THE AFORESAID CERTIFICATE OF FORMATION IS THE FIRST DAY OF OCTOBER, A.D. 2011, AT 8:05 O'CLOCK A.M.

0414109 8100V

111096809

You may verify this certificate online
at corp.delaware.gov/authver.shtml




Jeffrey W. Bullock, Secretary of State
AUTHENTICATION: 9089637

DATE: 10-13-11

Delaware

PAGE 1

The First State

I, JEFFREY W. BULLOCK, SECRETARY OF STATE OF THE STATE OF DELAWARE, DO HEREBY CERTIFY "TENNESSEE GAS PIPELINE COMPANY, L.L.C." IS DULY FORMED UNDER THE LAWS OF THE STATE OF DELAWARE AND IS IN GOOD STANDING AND HAS A LEGAL EXISTENCE SO FAR AS THE RECORDS OF THIS OFFICE SHOW, AS OF THE TWELFTH DAY OF OCTOBER, A.D. 2011.

AND I DO HEREBY FURTHER CERTIFY THAT THE ANNUAL TAXES HAVE BEEN PAID TO DATE.

0414109 8300

111093206

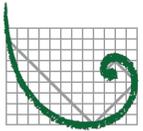
You may verify this certificate online
at corp.delaware.gov/authver.shtml




Jeffrey W. Bullock, Secretary of State
AUTHENTICATION: 9087127

DATE: 10-12-11

Attachment B



ERM
Environmental
Resources
Management

SITE LOCATION MAP

STATION 119A - BRE

TENNESSEE GAS PIPELINE, L.L.C.

CHARLESTON, KANAWHA COUNTY, WEST VIRGINIA

FIGURE

1

Attachment C

Attachment C

Schedule of Installation

Compressor Station 119A is scheduled to commence construction in February of 2016. The anticipated start-up date is October 2017.

Attachment D

Attachment D - Regulatory Discussion

This section outlines the State's air quality regulations that could be reasonably expected to apply to the proposed greenfield natural gas compressor station (Station 119A) based on activities expected to be conducted at the site and the expected emissions of regulated air pollutants. The West Virginia (WV) State Regulations address federal air quality regulations where WV has delegated authority of enforcement, including Prevention of Significant Deterioration (PSD) permitting, Title V permitting, New Source Performance Standards (NSPS), and National Emission Standards for Hazardous Air Pollutants (NESHAPs).

I. General State Requirements

45 CSR 02 – To Prevent and Control Particulate Air Pollution from Combustion of Fuel in Indirect Heat Exchangers

The hydronic heater, 119-WH-02, proposed at this site is an indirect heat exchanger; however, it is exempt from this requirement since it will have a heat input rating of less than 10 MMBtu/hr.

45 CSR 04 – To Prevent and Control the Discharge of Air Pollutants into the Air Which Causes or Contributes to an Objectionable Odor

Operations conducted at the compressor station will be subject to this requirement. Based on the nature of the process at the compressor station, the presence of objectionable odors is unlikely.

45 CSR 10 – To Prevent and Control Air Pollution from the Emission of Sulfur Oxides

The compressor turbine, 119-CT-01, proposed at Station 119A will combust natural gas and will be subject to this requirement. The purpose of this rule is to prevent and control air pollution from the emission of sulfur oxides. All fuel burning units will be subject to the weight emission standard for sulfur dioxide (SO₂). Fuel burning units which combust natural gas are exempt from the requirements of 45-10-8 – *Testing, Monitoring, Recordkeeping and Reporting*, per 45-10-10.3. Compressor turbine 119-CT-01 will burn only natural gas and is therefore exempt from the requirements of 45-10-8.

45 CSR 13 – Permits for Construction, Modification, Relocation and Operation of Stationary Sources of Air Pollutants

This Rule 13 permit application is being submitted for the operational activities proposed for Station 119A.

45 CSR 14 – Permits for Construction and Major Modification of Major Stationary Sources of Air Pollution for the Prevention of Significant Deterioration

Operation of equipment at this compressor station will not exceed the PSD emission thresholds as listed in this regulation. Please see the facility-wide potential to emit (PTE) summaries included in Attachment N.

Station 119A will be located in Kanawha County. The air quality of Kanawha County is designated by the U.S. EPA as either “better than normal standards” or “unclassified/attainment” for all criteria pollutants [40 CFR 81.318], and the county is designated as an ozone maintenance area. As such, new construction or modifications that result in emission increases are potentially subject to the PSD permitting regulations.

PSD applicability depends on the existing status of the facility (i.e. major or minor source) and the net emissions increase associated with the project. The major source threshold for PSD applicability is 250 tpy unless the source is included on a list of 28 specifically defined industrial source categories for which the PSD “major” source threshold is 100 tpy. Since Station 119A is not on the above U.S. EPA list, the PSD major source threshold is 250 tpy of any pollutant regulated by the Clean Air Act (CAA). Potential emissions of each criteria pollutant from the proposed facility will not exceed 250 tpy. The facility and project are therefore not subject to PSD review, as shown in Attachment N.

45 CSR 19 – Permits for Construction and Major Modification of Major Stationary Sources of Air Pollution Which Cause or Contributed to Nonattainment

Operation of equipment at TGP Station 119A will not exceed the major New Source Review (NSR) emission triggers. Operation of equipment at this compressor station will not exceed the PSD emission thresholds as listed in this regulation. Please see the facility-wide PTE summaries included in Attachment N.

45 CSR 25 – Control of Air Pollution from Hazardous Waste Treatment, Storage, and Disposal Facilities

No hazardous waste will be burned at this well site; therefore, it will not be subject to this hazardous waste rule.

45 CSR 30 – Requirements for Operating Permits

Operation of equipment at Station 119A will not require a Title V Operating Permit since potential emissions are below 100 tons per year (tpy) for all qualifying pollutants (see Attachment N).

II. *New Source Performance Standards*

45 CSR 16 - Standards of Performance for New Stationary Sources

The applicability of the following NSPS regulations to the proposed equipment and operations at TGP Station 119A is addressed below:

40 CFR 60 Subpart Dc (Standards of Performance for Small Industrial-Commercial-Institutional Steam Generating Units)

This regulation applies to steam generating units for which construction, modification, or reconstruction is commenced after June 9, 1989 and that have a maximum design heat capacity of 100 MMBtu/hr or less, but greater than or equal to 10 MMBtu/hr. The hydronic heater will have a heat input capacity of 4.6 MMBtu/hr and thus will not be subject to this regulation.

40 CFR 60 Subpart K (Standards of Performance for Storage Vessels for Petroleum Liquids)

This regulation applies to petroleum storage vessels with storage capacities greater than 40,000 gallons and constructed, reconstructed, or modified after June 11, 1973, and prior to May 19, 1978. There are no petroleum storage vessels with capacities greater than 40,000 gallons planned at Station 119A, and this regulation is therefore not applicable to the facility.

40 CFR 60 Subpart Ka (Standards of Performance for Storage Vessels for Petroleum Liquids)

This regulation applies to petroleum storage vessels with storage capacities greater than 40,000 gallons and constructed, reconstructed, or modified after May 18, 1978, and prior to June 23, 1984. There are no petroleum storage vessels with capacities greater than 40,000 gallons planned at Station 119A, and this regulation is therefore not applicable to the facility.

40 CFR 60 Subpart Kb (Standards of Performance for Volatile Organic Liquid Storage Vessels)

This regulation applies to volatile organic liquid storage vessels with storage capacities greater than or equal to 75 cubic meters (19,812 gallons) for which construction, reconstruction, or modification commenced after July 23, 1984. There are no petroleum storage vessels with capacities greater than 19,810 gallons planned at Station 119A, and this regulation is therefore not applicable to the facility.

40 CFR 60 Subpart GG (Standards of Performance for Stationary Gas Turbines)

The provisions of this Subpart are applicable to the following affected facilities: all stationary gas turbines with a heat input at peak load equal to or greater than 10.7 gigajoules per hour (10 million British Thermal Units per hour (MMBtu/hr)), based on the lower heating value of the fuel fired, which commence construction, modification, or reconstruction after October 3, 1977 [§60.330(a)-(b)].

However, 40 CFR 60 Subpart KKKK (see previous section) states that stationary combustion turbines regulated under Subpart KKKK are exempt from the requirements of Subpart GG [§60.4305(b)]. As the new compressor turbine, 119-CT-01, will be subject to Subpart KKKK, it is exempt from the requirements of Subpart GG.

40 CFR 60 Subpart KKK (Standards of Performance for Equipment Leaks of Volatile Organic Compound [VOC] from Onshore Natural Gas Processing Plants)

Station 119A will not be a natural gas processing plant as defined in this Subpart, and the facility will not engage in extraction of natural gas liquids from field gas or fractionate mixed natural gas liquids to natural gas products. Therefore, this regulation is not applicable.

40 CFR 60 Subpart LLL (Standards of Performance for Onshore Natural Gas Processing: SO₂ Emissions)

Station 119A will not operate sweetening units or sulfur recovery units, and will not be a natural gas processing plant. Therefore, this regulation is not applicable.

40 CFR 60 Subpart IIII (Standards of Performance for Stationary Compression Ignition Internal Combustion Engines)

This regulation is not applicable to Station 119A because the facility will not operate any stationary compression ignition internal combustion engines.

40 CFR 60 Subpart JJJJ (Standards of Performance for Stationary Spark Ignition Internal Combustion Engines)

Subpart JJJJ applies to owners and operators of stationary spark ignition (SI) internal combustion engines (ICE) that commence construction after June 12, 2006, depending on engine power and date of manufacture, and to owners and operators of all stationary SI ICE that are modified or reconstructed after June 12, 2006. The new emergency generator engine, 119-EG-03, will be manufactured and installed between 2016 and 2017, will have a 1,340 hp maximum rating, and thus will be subject to Subpart JJJJ.

The new emergency generator will meet the following emission standards from Subpart JJJJ, Table 1 [§60.4233(e)], and compliance will be demonstrated either via EPA certification or by emission testing:

1. NO_x limit of 2.0 g/HP-hr.
2. CO limit of 4.0 g/HP-hr.
3. VOC limit of 1.0 g/HP-hr.

The new emergency generator engine will be equipped with a non-resettable hour meter [§60.4237(a)]. As noted above, TGP will either 1) purchase an engine certified to meet Subpart JJJJ emission standards and will maintain documentation of the certification on site [§60.4245(a)(3)], or 2) purchase an engine which will meet the Subpart JJJJ emission standards, conduct an initial performance test, and conduct subsequent performance testing every 8,760 hours or 3 years, whichever comes first, thereafter to demonstrate compliance in accordance with §60.4244 [§60.4243(b)(2)(ii)]. If the engine is not certified, TGP will keep a maintenance plan and records of conducted maintenance and will, to the extent practicable, maintain and operate the engine in a manner consistent with good air pollution control practice for minimizing emissions [§60.4243(b)(2)(ii)].

The unit will be operated as follows in order to maintain its emergency unit status [§60.4243(d)]:

1. There is no time limit on the use of emergency stationary ICE in emergency situations.
2. Non-emergency hours, which include maintenance checks and readiness testing, provided that the tests are recommended by federal, state or local government, the manufacturer, the vendor, or the insurance company associated with the engine, will be limited to 100 hours per year unless records indicating that federal, state, or local standards require maintenance and testing of emergency ICE beyond 100 hours per calendar year are maintained.
3. For non-emergency situations other than maintenance or readiness testing, the emergency stationary ICE may be operated for up to 50 hours per calendar year. The 50 hours of operation in non-emergency situations are counted as part of the 100 hours per calendar year for maintenance and testing.

TGP will maintain all required records as follows [§60.4245]:

1. Maintenance conducted on the engine.
2. Documentation that the engine meets applicable emission standards.

3. Hours of operation.

Reporting requirements include submittal of an initial notification and performance test results, as applicable, and TGP will comply with these requirements.

40 CFR 60 Subpart KKKK (Standards of Performance for Stationary Combustion Turbines)

Stationary combustion turbines with a heat input at peak load equal to or greater than 10 MMBtu per hour, based on the higher heating value of the fuel, which commenced construction, modification, or reconstruction after February 18, 2005 are subject to this Subpart. The new compressor turbine, 119-CT-01, will have a heat input value of 168 MMBtu/hr based on the higher heating value of the fuel, and will thus be subject to Subpart KKKK.

The new compressor turbine will meet the following limits:

1. NO_x emission limit of 25 ppm at 15 percent O₂ or 150 nanograms per joule (ng/J) of useful output (1.2 pound per megawatt hour (lb/MWh)) [§60.4320]; and either
2. Total potential sulfur emissions limit of 875 ng SO₂/J (0.90 lb SO₂/MWh) [§60.4330(a)(2)], or
3. Fuel sulfur limit of 26 ng SO₂/J (0.060 lb SO₂/MMBtu) heat input

Attachment L includes manufacturer emissions and performance data, which guarantees that the NO_x limit above will be met. The abovementioned sulfur limits will be met through the use of pipeline quality natural gas as fuel. All associated equipment will be operated and maintained in a manner consistent with good air pollution control practices for minimizing emissions at all times including during startup, shutdown, and malfunction [§60.4333(a)].

As compressor turbine 119-CT-01 will be a lean premix stationary combustion turbine, TGP will perform initial and subsequent performance testing to demonstrate compliance with the applicable NO_x emission limit (25 ppm) [§60.4340(a)]. The subsequent testing will be conducted on an either an annual basis, or on a biannual basis if the previous performance test results are less than or equal to 75 percent of the 25 ppm NO_x emission limit for the turbine [§60.4340(a)].

As noted above, the use of natural gas will constitute compliance with SO₂ emission limitations, and initial and ongoing performance testing will not be required. Additionally, the total sulfur content of the compressor turbine's combustion fuel must be monitored, unless one of the exemptions listed in §60.4365 can be met. The exemptions are as follows:

1. The fuel quality characteristics in a valid purchase contract, tariff sheet or transportation contract for the fuel has potential sulfur emissions of less than 0.060 lb SO₂/MMBtu (26 ng SO₂/J) heat input [§60.4365(a)].
2. Fuel sampling data which show that the sulfur content of the fuel does not exceed 0.060 lb SO₂/MMBtu (26 ng SO₂/J) [§60.4365(b)].

For the new compressor turbine, the fuel used for operation is derived from the natural gas transported through TGP's pipeline system, and will meet the exemption criteria listed in #1 above.

A written report of the results of each performance test required under §60.4340(a) must be submitted by the 60th day following the completion of the performance test [§60.4375(b)]. TGP will submit the necessary reports for the new compressor turbine as required by this Subpart.

40 CFR 60, Subpart OOOO (Standards of Performance for Crude Oil and Natural Gas Production, Transmission and Distribution)

This Subpart establishes emission standards and compliance schedules for the control of volatile organic compounds (VOCs) and SO₂ emissions for affected facilities producing, transmitting, or distributing natural gas. Compressors located between the wellhead and the point of custody transfer to the natural gas transmission and storage segment are subject to this Subpart. Custody transfer is defined as the transfer of natural gas after processing and/or treatment in the producing operations. Station 119A will be located after the point of custody transfer, and thus compressor turbine 119-CT-01 will not be subject to this regulation. Storage vessels located in the natural gas transmission and storage segment that have the potential for VOC emissions equal to or greater than 6 tons per year (tpy) are also subject to this Subpart. The pipeline liquids storage vessel to be located at Station 119A has a VOC PTE less than 6 tpy, and thus will not be subject to this regulation.

III. Emission Standards for Hazardous Air Pollutants

45 CSR 34 – Emission Standards for Hazardous Air Pollutants

NESHAP regulations established in 40 CFR Part 61 and Part 63 regulate emission of air toxics. NESHAP standards primarily apply to major sources of hazardous air pollutants (HAPs), though some Subparts of Part 63 have been revised to include area (non-major) sources. The NESHAP regulations under 40 CFR Part 61 establish emission standards on the pollutant basis whereas 40 CFR Part 63 establishes the standards on a source category basis. Station 119A will not emit any singular HAP in excess of 10 tpy and will not emit combined HAPS in excess of 25 tpy, and will therefore be designated as an area source of HAPs. Please see the facility-wide PTE summaries included in Attachment N.

40 CFR 63 Subpart HHH (National Emission Standards for Hazardous Air Pollutants From Oil and Natural Gas Production Facilities).

This regulation applies to each new and existing glycol dehydration unit at natural gas transmission and storage facilities which are major sources of HAPs. A glycol dehydration unit is a device in which liquid glycol absorbent directly contacts a natural gas stream and absorbs water. Station 119A will not be a major source of HAPs and will not have a glycol dehydration unit, and thus will not be subject to this Subpart.

40 CFR 63 Subpart YYYY (National Emissions Standards for Hazardous Air Pollutants [HAP] for Stationary Combustion Turbines)

Stationary combustion turbines located at major sources of HAP emissions are subject to this Subpart. As the facility will not be a major source of HAP emissions, it is not subject to this Subpart [§60.6085(a)].

40 CFR 63 Subpart ZZZZ (National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines)

Stationary reciprocating internal combustion engines (RICE) located at an area source of HAPs that are new, existing, or reconstructed are subject to this Subpart. Stationary RICE at area sources of HAPs are considered “new” under this Subpart if construction is commenced on or after June 12, 2006. The new emergency generator (engine), 119-EG-03, will be exempt from Subpart ZZZZ because the engine will comply with all applicable requirements under 40 CFR 60 Subpart JJJJ [§60.6590(c)].

40 CFR 63 Subpart DDDDD (National Emission Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters)

Industrial, commercial, or institutional boilers or process heaters located at a major source of HAPs are subject to this Subpart. Station 119A will not be a major source of HAPs and therefore will not be subject to this Subpart.

40 CFR 63 Subpart JJJJJJ (National Emission Standards for Hazardous Air Pollutants for Industrial, Commercial, and Institutional Boilers Area Sources)

This Subpart applies to industrial, commercial, or institutional boilers at area sources of HAPs. Station 119A will be an area source of HAPs; however, the new hydronic heater 119-WH-02 will not meet the definition of a boiler defined in §63.11237, and it will therefore not be subject to any of the requirements of this Subpart.

IV. *Other Federal Requirements*

Maintenance Emissions and Federal Routing Maintenance, Repair, and Replacement Provisions (RMRR)

As part of normal operations of Station 119A, TGP will routinely conduct activities associated with maintenance and repair of the facility equipment. These maintenance and repair activities will include, but will not be limited to, compressor engine startup/shutdowns, calibrating equipment, changing orifice plates, deadweight testing, and changing equipment filters (e.g., oil filters, separator filters).

Furthermore, in order to ensure the reliability of natural gas deliveries to their customers, TGP may conduct equipment and component replacement activities that conform to the currently applicable federal laws and regulations.

40 CFR Parts 72 through 77 Acid Rain Regulations

Station 119A will not sell electricity and is a non-utility facility. Therefore, Station 119A will not be subject to the federal acid rain regulations found at 40 CFR Parts 72 through 77.

40 CFR 68 Chemical Accident Prevention and Risk Management Programs (RMP)

Station 119A will not be subject to the Chemical Accident Prevention Provisions (40 CFR 68.1). The facility will not be considered a stationary source under 40 CFR 68.3, Chemical Accident Prevention, because it is regulated under 49 CFR 192, U.S. Department of Transportation (DOT). Subpart B of 40 CFR 68 outlines requirements for Risk Management Programs (RMP) pursuant to Section 112(r) of the CAA. Applicability of the Subpart is determined based on the type and quantity of certain potentially hazardous and/or flammable chemicals stored at a facility. The RMP requirements will not apply to Station 119A, which will be operated and maintained in accordance with applicable rules of the DOT's Federal Safety Standards for Transportation of Natural and Other Gas by Pipeline codified at 49 CFR 192.

40 CFR 82 Stratospheric Ozone Protection Regulations

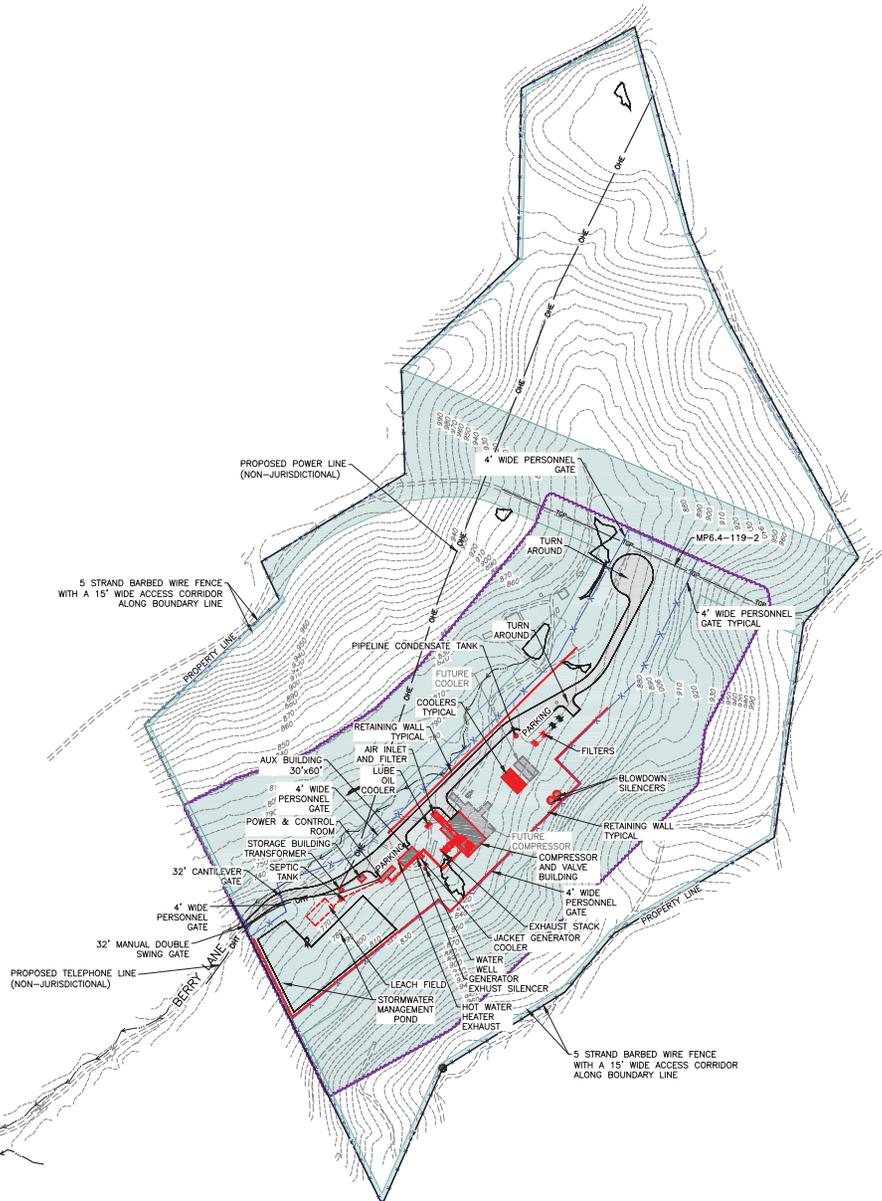
Subpart F, Recycling and Emissions Reductions, of 40 CFR Part 82, Protection of Stratospheric Ozone, generally requires that all repairs, service, and disposal of appliances containing Class I or Class II ozone depleting substances be conducted by properly certified technicians. The facility will comply with this regulation as applicable.

Attachment E

P:\CAD\PROJECTS\0101 - Air Broad Run\Sub\119A\119A-1-1.dwg PLOTTED BY: JENNIFER BERRY @ 11/14/2015 10:51 AM



REFERENCE DRAWINGS



LEGEND

PROPERTY LINE	---
EXISTING DRAINAGE FEATURES	→→→
6' CHAIN LINK FENCE	—x—x—x—x—
5 STRAND BARBED WIRE	—x—x—x—x—
STATION EQUIPMENT	—
TREES TO BE REMOVED	~ ~ ~
STATION ACCESS ROAD	▭
PERMANENT STATION AREA	▭

SITE STATISTICS

PROPERTY AREA	= 86.7 AC
PERMANENT STATION AREA	= 47.6 AC
TOTAL DISTURBED AREA	= 47.6 AC

C 01/14	BLJ	ISSUED FOR REVIEW	68152	JFO
B 11/14	BLJ	ISSUED FOR REVIEW	68152	JFO
A 10/17	BLJ	ISSUED FOR REVIEW	68152	JFO
NO. DATE	BY	DESCRIPTION	PROJ. D	APPR.



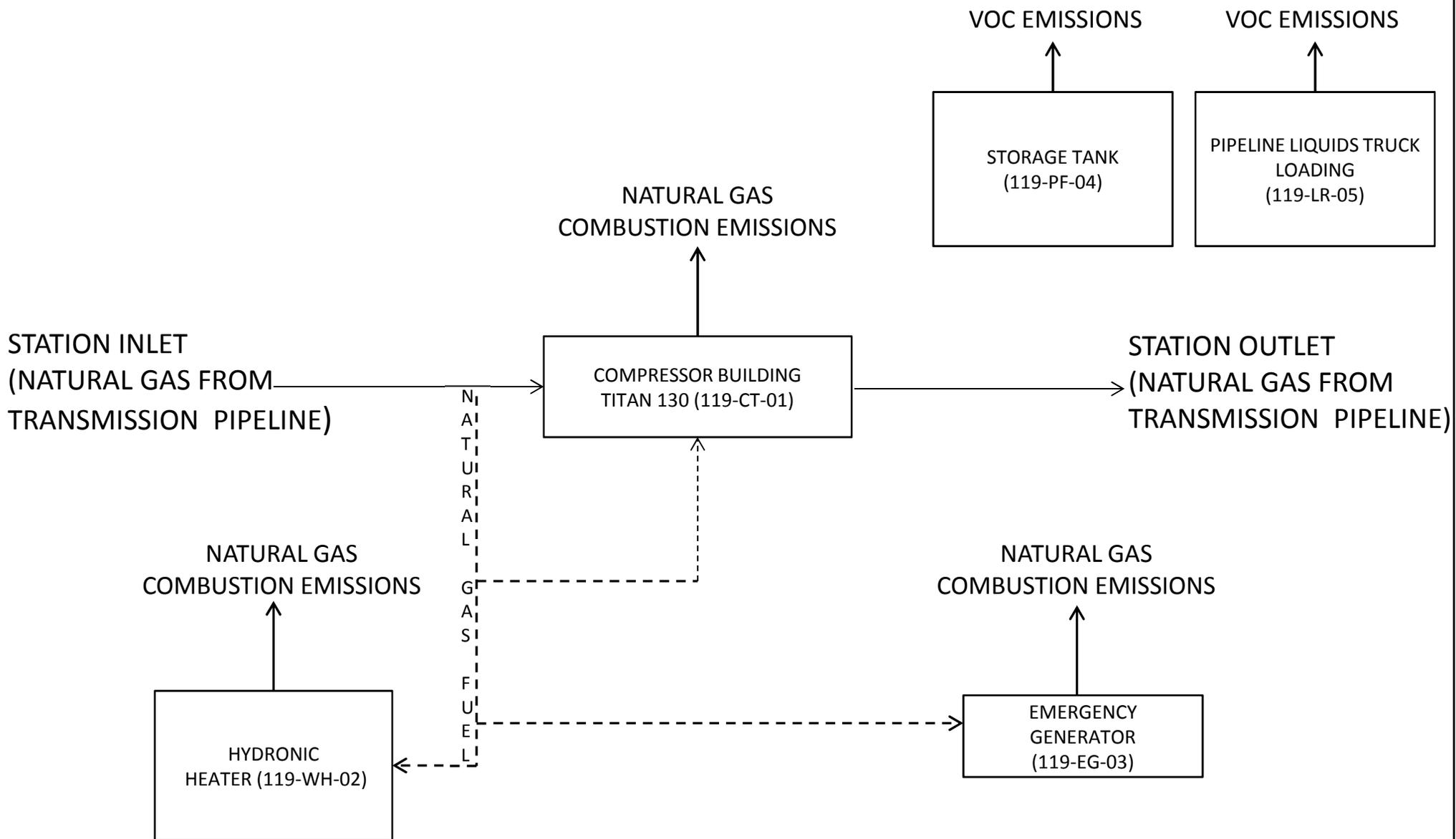
PLOT PLAN
BROAD RUN EXPANSION PROJECT
COMPRESSOR STATION 119A
BERRY LANE, CHARLESTON
KANAWHA COUNTY, WEST VIRGINIA

Division:	—	Op. Area:	—
State:	WEST VIRGINIA	Co./Par.:	KANAWHA
Section:	NA	Township:	NA
Range:	NA	Project ID:	68152
Drafter:	BLJ	Date:	09/19/2014
Checker:	LRS	Date:	09/19/2014
Appr:	JFO	Date:	09/19/2014
Scale:	1"=100'	Plot Name:	TO-C119A-A1-YA-10.DWG
PT. CODE	x	Sheet:	1 of 2

ISSUED FOR REVIEW
 January 14, 2015

Attachment F

Compressor Station 119A Simplified Process Flow Diagram



Attachment G

Attachment G

Process Description

Tennessee Gas Pipeline, L.L.C. is submitting this Rule 13 Permit Application for proposed greenfield Compressor Station 119A to comply with the permitting requirements of the state of West Virginia. Natural gas from the transmission pipeline will be routed and compressed through this station. Natural gas will be compressed to a higher pressure and discharged downstream into the sales line. The natural gas fired compressor turbine (119-CT-01) that is proposed at Station 119A is a Solar Titan 130-20502S turbine with a design capacity of 21,197 brake horsepower. Station 119A will also operate one (1) natural gas fired emergency generator (119-EG-03), one (1) natural gas fired hydronic heater (119-WH-02), and one (1) pipeline liquids storage tank (119-PF-04).

Attachment H

Product Name: MOBIL PEGASUS 1005

Revision Date: 23Mar2007

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REGULATORY DISPOSAL INFORMATION

RCRA Information: The unused product, in our opinion, is not specifically listed by the EPA as a hazardous waste (40 CFR, Part 261D), nor is it formulated to contain materials which are listed as hazardous wastes. It does not exhibit the hazardous characteristics of ignitability, corrosivity or reactivity and is not formulated with contaminants as determined by the Toxicity Characteristic Leaching Procedure (TCLP). However, used product may be regulated.

Empty Container Warning PRECAUTIONARY LABEL TEXT: Empty containers may retain residue and can be dangerous. DO NOT PRESSURIZE, CUT, WELD, BRAZE, SOLDER, DRILL, GRIND OR EXPOSE SUCH CONTAINERS TO HEAT, FLAME, SPARKS, STATIC ELECTRICITY, OR OTHER SOURCES OF IGNITION; THEY MAY EXPLODE AND CAUSE INJURY OR DEATH. Do not attempt to refill or clean container since residue is difficult to remove. Empty drums should be completely drained, properly bunged and promptly returned to a drum reconditioner. All containers should be disposed of in an environmentally safe manner and in accordance with governmental regulations.

SECTION 14 TRANSPORT INFORMATION

LAND (DOT) : Not Regulated for Land Transport

LAND (TDG) : Not Regulated for Land Transport

SEA (IMDG) : Not Regulated for Sea Transport according to IMDG-Code

AIR (IATA) : Not Regulated for Air Transport

SECTION 15 REGULATORY INFORMATION

OSHA HAZARD COMMUNICATION STANDARD: When used for its intended purposes, this material is not classified as hazardous in accordance with OSHA 29 CFR 1910.1200.

NATIONAL CHEMICAL INVENTORY LISTING: AICS, DSL, KECI, PICCS, TSCA

Special Cases:

Inventory	Status
ELINCS	Restrictions Apply

EPCRA: This material contains no extremely hazardous substances.

SARA (311/312) REPORTABLE HAZARD CATEGORIES: None.

SARA (313) TOXIC RELEASE INVENTORY: This material contains no chemicals subject to the supplier notification requirements of the SARA 313 Toxic Release Program.

The Following Ingredients are Cited on the Lists Below:

Chemical Name	CAS Number	List Citations
DIPHENYLAMINE	122-39-4	5, 9

Product Name: MOBIL PEGASUS 1005

Revision Date: 23Mar2007

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PHOSPHORODITHOIC ACID, O,O-DI C1-14-ALKYL ESTERS, ZINC SALTS (2:1) (ZDDP)	68649-42-3	15
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--REGULATORY LISTS SEARCHED--

1 = ACGIH ALL	6 = TSCA 5a2	11 = CA P65 REPRO	16 = MN RTK
2 = ACGIH A1	7 = TSCA 5e	12 = CA RTK	17 = NJ RTK
3 = ACGIH A2	8 = TSCA 6	13 = IL RTK	18 = PA RTK
4 = OSHA Z	9 = TSCA 12b	14 = LA RTK	19 = RI RTK
5 = TSCA 4	10 = CA P65 CARC	15 = MI 293	

Code key: CARC=Carcinogen; REPRO=Reproductive

SECTION 16	OTHER INFORMATION
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N/D = Not determined, N/A = Not applicable

THIS SAFETY DATA SHEET CONTAINS THE FOLLOWING REVISIONS:

No revision information is available.

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Internal Use Only

MHC: 0, 0, 0, 0, 0, 0

PPEC: A

DGN: 7082306XUS (1008352)

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Material Safety Data Sheet

SECTION 1 PRODUCT AND COMPANY IDENTIFICATION

Cat® NGEC™ (Natural Gas Engine Coolant)

Product Use: Antifreeze/Coolant

Product Number(s): CPS227813

Company Identification

Chevron Products Company
Global Lubricants
6001 Bollinger Canyon Road
San Ramon, CA 94583
United States of America

Transportation Emergency Response

CHEMTREC: (800) 424-9300 or (703) 527-3887

Health Emergency

Chevron Emergency Information Center: Located in the USA. International collect calls accepted. (800) 231-0623 or (510) 231-0623

Product Information

email : lubemsds@chevrontexaco.com

Product Information: 800-LUBE-TEK

MSDS Requests: 800-414-6737

SECTION 2 COMPOSITION/ INFORMATION ON INGREDIENTS

COMPONENTS	CAS NUMBER	AMOUNT
Ethylene Glycol	107-21-1	40 - 55 %weight
Diethylene glycol	111-46-6	1 - 5 %weight

SECTION 3 HAZARDS IDENTIFICATION

EMERGENCY OVERVIEW

- HARMFUL OR FATAL IF SWALLOWED
- POSSIBLE BIRTH DEFECT HAZARD - CONTAINS MATERIAL THAT MAY CAUSE BIRTH DEFECTS BASED ON ANIMAL DATA
- MAY CAUSE DAMAGE TO:
 - KIDNEY

IMMEDIATE HEALTH EFFECTS

Eye: Not expected to cause prolonged or significant eye irritation.

Skin: Contact with the skin is not expected to cause prolonged or significant irritation. Not expected to be harmful to internal organs if absorbed through the skin.

Ingestion: Toxic; may be harmful or fatal if swallowed.

Inhalation: The vapor or fumes from this material may cause respiratory irritation. Symptoms of respiratory irritation may include coughing and difficulty breathing. Breathing this material at concentrations above the recommended exposure limits may cause central nervous system effects. Central nervous system effects may include headache, dizziness, nausea, vomiting, weakness, loss of coordination, blurred vision, drowsiness, confusion, or disorientation. At extreme exposures, central nervous system effects may include respiratory depression, tremors or convulsions, loss of consciousness, coma or death.

DELAYED OR OTHER HEALTH EFFECTS:

Reproduction and Birth Defects: Contains material that may cause birth defects based on animal data.

Target Organs: Contains material that may cause damage to the following organ(s) following repeated ingestion based on animal data: Kidney

See Section 11 for additional information. Risk depends on duration and level of exposure.

SECTION 4 FIRST AID MEASURES

Eye: No specific first aid measures are required. As a precaution, remove contact lenses, if worn, and flush eyes with water.

Skin: No specific first aid measures are required. As a precaution, remove clothing and shoes if contaminated. To remove the material from skin, use soap and water. Discard contaminated clothing and shoes or thoroughly clean before reuse.

Ingestion: If swallowed, get immediate medical attention. Do not induce vomiting. Never give anything by mouth to an unconscious person.

Inhalation: Move the exposed person to fresh air. If not breathing, give artificial respiration. If breathing is difficult, give oxygen. Get medical attention if breathing difficulties continue.

SECTION 5 FIRE FIGHTING MEASURES

FIRE CLASSIFICATION:

OSHA Classification (29 CFR 1910.1200): Not classified by OSHA as flammable or combustible.

NFPA RATINGS: Health: 2 Flammability: 0 Reactivity: 0

FLAMMABLE PROPERTIES:

Flashpoint: Not Applicable

Autoignition: No Data Available

Flammability (Explosive) Limits (% by volume in air): Lower: Not Applicable Upper: Not Applicable

EXTINGUISHING MEDIA: Dry Chemical, CO₂, AFFF Foam or alcohol resistant foam.

PROTECTION OF FIRE FIGHTERS:

Fire Fighting Instructions: This material will not burn.

SECTION 6 ACCIDENTAL RELEASE MEASURES

Spill Management: Stop the source of the release if you can do it without risk. Contain release to prevent further contamination of soil, surface water or groundwater. Clean up spill as soon as possible, observing precautions in Exposure Controls/Personal Protection. Use appropriate techniques such as applying non-combustible absorbent materials or pumping. Where feasible and appropriate, remove

contaminated soil. Place contaminated materials in disposable containers and dispose of in a manner consistent with applicable regulations.

Reporting: Report spills to local authorities and/or the U.S. Coast Guard's National Response Center at (800) 424-8802 as appropriate or required.

SECTION 7 HANDLING AND STORAGE

Precautionary Measures: Do not get in eyes, on skin, or on clothing. Do not taste or swallow. Do not breathe vapor or fumes. Wash thoroughly after handling.

General Handling Information: Do not taste or swallow antifreeze or solution. Keep out of the reach of children and animals.

General Storage Information: Do not store in open or unlabeled containers.

Container Warnings: Container is not designed to contain pressure. Do not use pressure to empty container or it may rupture with explosive force. Empty containers retain product residue (solid, liquid, and/or vapor) and can be dangerous. Do not pressurize, cut, weld, braze, solder, drill, grind, or expose such containers to heat, flame, sparks, static electricity, or other sources of ignition. They may explode and cause injury or death. Empty containers should be completely drained, properly closed, and promptly returned to a drum reconditioner or disposed of properly.

SECTION 8 EXPOSURE CONTROLS/PERSONAL PROTECTION

GENERAL CONSIDERATIONS:

Consider the potential hazards of this material (see Section 3), applicable exposure limits, job activities, and other substances in the work place when designing engineering controls and selecting personal protective equipment. If engineering controls or work practices are not adequate to prevent exposure to harmful levels of this material, the personal protective equipment listed below is recommended. The user should read and understand all instructions and limitations supplied with the equipment since protection is usually provided for a limited time or under certain circumstances.

ENGINEERING CONTROLS:

Use process enclosures, local exhaust ventilation, or other engineering controls to control airborne levels below the recommended exposure limits.

PERSONAL PROTECTIVE EQUIPMENT

Eye/Face Protection: No special eye protection is normally required. Where splashing is possible, wear safety glasses with side shields as a good safety practice.

Skin Protection: No special protective clothing is normally required. Where splashing is possible, select protective clothing depending on operations conducted, physical requirements and other substances in the workplace. Suggested materials for protective gloves include: Natural rubber, Neoprene, Nitrile Rubber, Polyvinyl Chloride (PVC or Vinyl).

Respiratory Protection: Determine if airborne concentrations are below the recommended occupational exposure limits for jurisdiction of use. If airborne concentrations are above the acceptable limits, wear an approved respirator that provides adequate protection from this material, such as: Air-Purifying Respirator for Organic Vapors, Dusts and Mists.

Use a positive pressure air-supplying respirator in circumstances where air-purifying respirators may not provide adequate protection.

Occupational Exposure Limits:

Component	Agency	TWA	STEL	Ceiling	Notation
Ethylene Glycol	ACGIH	--	--	100 mg/m3	--

SECTION 9 PHYSICAL AND CHEMICAL PROPERTIES

Attention: the data below are typical values and do not constitute a specification.

Color: Purple

Physical State: Liquid

Odor: Faint or Mild

pH: 10 - 11

Vapor Pressure: 0.12 mmHg (Typical) @ 20 °C (68 °F)

Vapor Density (Air = 1): 2.1

Boiling Point: 108.9°C (228°F)

Solubility: Miscible

Freezing Point: -36.7°C (-34°F)

Specific Gravity: 1.13 @ 15.6°C (60.1°F) / 15.6°C (60.1°F)

Viscosity: No data available

Evaporation Rate: No Data Available

SECTION 10 STABILITY AND REACTIVITY

Chemical Stability: This material is considered stable under normal ambient and anticipated storage and handling conditions of temperature and pressure.

Hazardous Decomposition Products: Aldehydes (Elevated temperatures), Ketones (Elevated temperatures)

Hazardous Polymerization: Hazardous polymerization will not occur.

SECTION 11 TOXICOLOGICAL INFORMATION

IMMEDIATE HEALTH EFFECTS

Eye Irritation: The eye irritation hazard is based on evaluation of data for similar materials or product components.

Skin Irritation: The skin irritation hazard is based on evaluation of data for similar materials or product components.

Skin Sensitization: No product toxicology data available.

Acute Dermal Toxicity: The acute dermal toxicity hazard is based on evaluation of data for similar materials or product components.

Acute Oral Toxicity: The acute oral toxicity hazard is based on evaluation of data for similar materials or product components.

Acute Inhalation Toxicity: The acute inhalation toxicity hazard is based on evaluation of data for similar materials or product components.

ADDITIONAL TOXICOLOGY INFORMATION:

This product contains diethylene glycol (DEG). The estimated oral lethal dose is about 50 cc (1.6 oz) for an adult human. DEG has caused the following effects in laboratory animals: liver abnormalities, kidney damage and blood abnormalities. It has been suggested as a cause of the following effects in humans: liver abnormalities, kidney damage, lung damage and central nervous system damage.

This product contains ethylene glycol (EG). The toxicity of EG via inhalation or skin contact is expected to be slight at room temperature. The estimated oral lethal dose is about 100 cc (3.3 oz.) for an adult human. Ethylene glycol is oxidized to oxalic acid which results in the deposition of calcium oxalate crystals mainly in the brain and kidneys. Early signs and symptoms of EG poisoning may resemble those of alcohol intoxication. Later, the victim may experience nausea, vomiting, weakness, abdominal and muscle pain, difficulty in breathing and decreased urine output. When EG was heated above the boiling point of water, vapors formed which reportedly caused unconsciousness, increased lymphocyte count,

and a rapid, jerky movement of the eyes in persons chronically exposed. When EG was administered orally to pregnant rats and mice, there was an increase in fetal deaths and birth defects. Some of these effects occurred at doses that had no toxic effects on the mothers. We are not aware of any reports that EG causes reproductive toxicity in human beings.

SECTION 12 ECOLOGICAL INFORMATION

ECOTOXICITY

The toxicity of this material to aquatic organisms has not been evaluated. Consequently, this material should be kept out of sewage and drainage systems and all bodies of water.

ENVIRONMENTAL FATE

This material is expected to be readily biodegradable.

SECTION 13 DISPOSAL CONSIDERATIONS

Use material for its intended purpose or recycle if possible. Oil collection services are available for used oil recycling or disposal. Place contaminated materials in containers and dispose of in a manner consistent with applicable regulations. Contact your sales representative or local environmental or health authorities for approved disposal or recycling methods.

SECTION 14 TRANSPORT INFORMATION

The description shown may not apply to all shipping situations. Consult 49CFR, or appropriate Dangerous Goods Regulations, for additional description requirements (e.g., technical name) and mode-specific or quantity-specific shipping requirements.

DOT Shipping Description: Anti-freeze Preparations, Proprietary

Additional Information: Bulk shipments with a reportable quantity (5000 pounds) of ethylene glycol are a hazardous material. The Proper Shipping Name is: Environmentally Hazardous Substance, Liquid, N.O.S. (ethylene glycol), 9, UN3082, III, RQ (ethylene glycol).

IMO/IMDG Shipping Description: NOT REGULATED AS DANGEROUS GOODS FOR TRANSPORTATION UNDER THE IMDG CODE

ICAO/IATA Shipping Description: Anti-freeze Preparations, Proprietary; NOT REGULATED AS DANGEROUS GOODS FOR TRANSPORT UNDER ICAO

SECTION 15 REGULATORY INFORMATION

EPCRA 311/312 CATEGORIES:

1. Immediate (Acute) Health Effects:	YES
2. Delayed (Chronic) Health Effects:	YES
3. Fire Hazard:	NO
4. Sudden Release of Pressure Hazard:	NO
5. Reactivity Hazard:	NO

REGULATORY LISTS SEARCHED:

01-1=IARC Group 1 03=EPCRA 313
01-2A=IARC Group 2A 04=CA Proposition 65

01-2B=IARC Group 2B
02=NTP Carcinogen

05=MA RTK
06=NJ RTK
07=PA RTK

The following components of this material are found on the regulatory lists indicated.

Diethylene glycol 07
Ethylene Glycol 03, 05, 06, 07

CHEMICAL INVENTORIES:

All components comply with the following chemical inventory requirements: AICS (Australia), DSL (Canada), EINECS (European Union), ENCS (Japan), IECSC (China), PICCS (Philippines), TSCA (United States).

One or more components does not comply with the following chemical inventory requirements: KECI (Korea).

NEW JERSEY RTK CLASSIFICATION:

Refer to components listed in Section 2.

WHMIS CLASSIFICATION:

Class D, Division 1, Subdivision B: Toxic Material -
Acute Lethality

Class D, Division 2, Subdivision A: Very Toxic Material -
Teratogenicity and Embryotoxicity

SECTION 16 OTHER INFORMATION

NFPA RATINGS: Health: 2 Flammability: 0 Reactivity: 0

HMIS RATINGS: Health: 2* Flammability: 0 Reactivity: 0
(0-Least, 1-Slight, 2-Moderate, 3-High, 4-Extreme, PPE:- Personal Protection Equipment Index recommendation, *- Chronic Effect Indicator). These values are obtained using the guidelines or published evaluations prepared by the National Fire Protection Association (NFPA) or the National Paint and Coating Association (for HMIS ratings).

LABEL RECOMMENDATION:

Label Category : ANTIFREEZE/COOLANT 1 - AFC1

REVISION STATEMENT: This revision updates the following sections of this Material Safety Data Sheet:
1

Revision Date: July 25, 2006

ABBREVIATIONS THAT MAY HAVE BEEN USED IN THIS DOCUMENT:

TLV - Threshold Limit Value	TWA - Time Weighted Average
STEL - Short-term Exposure Limit	PEL - Permissible Exposure Limit
	CAS - Chemical Abstract Service Number
ACGIH - American Conference of Government Industrial Hygienists	IMO/IMDG - International Maritime Dangerous Goods Code
API - American Petroleum Institute	MSDS - Material Safety Data Sheet

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Revision Date: July 25, 2006

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Cat® NGEC™ (Natural Gas Engine
Coolant)
MSDS : 11116

9C-411

CVX - Chevron	NFPA - National Fire Protection Association (USA)
DOT - Department of Transportation (USA)	NTP - National Toxicology Program (USA)
IARC - International Agency for Research on Cancer	OSHA - Occupational Safety and Health Administration

Prepared according to the OSHA Hazard Communication Standard (29 CFR 1910.1200) and the ANSI MSDS Standard (Z400.1) by the Chevron Energy Technology Company, 100 Chevron Way, Richmond, California 94802.

The above information is based on the data of which we are aware and is believed to be correct as of the date hereof. Since this information may be applied under conditions beyond our control and with which we may be unfamiliar and since data made available subsequent to the date hereof may suggest modifications of the information, we do not assume any responsibility for the results of its use. This information is furnished upon condition that the person receiving it shall make his own determination of the suitability of the material for his particular purpose.

Attachment I

Attachment J

Attachment J
EMISSION POINTS DATA SUMMARY SHEET

Table 1: Emissions Data

Emission Point ID No. (Must match Emission Units Table & Plot Plan)	Emission Point Type ¹	Emission Unit Vented Through This Point (Must match Emission Units Table & Plot Plan)		Air Pollution Control Device (Must match Emission Units Table & Plot Plan)		Vent Time for Emission Unit (chemical processes only)		All Regulated Pollutants - Chemical Name/CAS ³ (Speciate VOCs & HAPS)	Maximum Potential Uncontrolled Emissions ⁴		Maximum Potential Controlled Emissions ⁵		Emission Form or Phase (At exit conditions, Solid, Liquid or Gas/Vapor)	Est. Method Used ⁶	Emission Concentration ⁷ (mg/m ³)
		ID No.	Source	ID No.	Device Type	Short Term ²	Max (hr/yr)		lb/hr	ton/yr	lb/hr	ton/yr			
119-EG-03	Upward Vertical Stack	119-EG-03	Emergency Generator	NA	NA	NA	NA	CO NO _x Total VOCs PM PM _{2.5} PM ₁₀ SO ₂ Total HAPs CO _{2e}	11.82 5.91 2.95 0.11 0.11 0.11 0.01 0.81 1,658	2.95 1.48 0.74 0.03 0.03 0.03 <0.01 0.20 415	11.82 5.91 2.95 0.11 0.11 0.11 0.01 0.81 1,658	2.95 1.48 0.74 0.03 0.03 0.03 <0.01 0.20 415	Gas	AP-42, 40 CFR 98, Vendor Data	NA
119-CT-01	Upward Vertical Stack	119-CT-01	Turbine	NA	NA	NA	NA	CO NO _x Total VOCs PM PM _{2.5} PM ₁₀ SO ₂ Total HAPs CO _{2e}	9.29 15.27 1.06 1.09 1.09 1.09 0.56 0.17 19,462	67.70 62.33 4.67 4.41 4.41 4.41 2.27 0.74 78,914	9.29 15.27 1.06 1.09 1.09 1.09 0.56 0.17 19,462	67.70 62.33 4.67 4.41 4.41 4.41 2.27 0.74 78,914	Gas	AP-42, 40 CFR 98, Vendor Guarantees	NA
119-WH-02	Upward Vertical Stack	119-WH-03	Hydronic Heater	NA	NA	NA	NA	CO NO _x Total VOCs PM PM _{2.5} PM ₁₀ SO ₂ Total HAPs CO _{2e}	0.25 0.11 0.03 0.05 0.05 0.05 <0.01 0.01 541	1.11 0.48 0.12 0.20 0.20 0.20 0.01 0.04 2,371	0.25 0.11 0.03 0.05 0.05 0.05 <0.01 0.01 541	1.11 0.48 0.12 0.20 0.20 0.20 0.01 0.04 2,371	Gas	AP-42, 40 CFR 98, Vendor Data	NA
119-PF-04	Vent	119-PF-04	Pipeline Liquids Storage Tank	NA	NA	NA	NA	Total VOC Total HAPs	0.05 <0.01	0.2 0.01	0.05 <0.01	0.2 0.01	Gas	E&P Software	NA

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit emissions are not typically considered to be fugitive and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugitive emission activities.

¹ Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.

- ² Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (ie., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).
- ³ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. **LIST** Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. **DO NOT LIST** H₂, H₂O, N₂, O₂, and Noble Gases.
- ⁴ Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- ⁵ Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
- ⁶ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).
- ⁷ Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmv) are used. If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m³) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO₂, use units of ppmv (See 45CSR10).

**Attachment J
EMISSION POINTS DATA SUMMARY SHEET**

Table 2: Release Parameter Data								
Emission Point ID No. <i>(Must match Emission Units Table)</i>	Inner Diameter (ft.)	Exit Gas			Emission Point Elevation (ft)		UTM Coordinates (km)	
		Temp. (°F)	Volumetric Flow ¹ (acfm) <i>at operating conditions</i>	Velocity (fps)	Ground Level <i>(Height above mean sea level)</i>	Stack Height ² <i>(Release height of emissions above ground level)</i>	Northing	Easting
119-EG-03	1	873	7,663	127.72	800	20	4,256.17	437.51
119-CT-01	8x8 square	935	238,003	65.97	800	71	4,255.99	437.43
119-WH-02	1.83	450	4,894	24.36	800	20	4,256.17	437.51
119-PF-04	NA	Ambient	NA	NA	NA	15	4,256.17	437.51

Attachment K

Attachment K

FUGITIVE EMISSIONS DATA SUMMARY SHEET

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not typically considered to be fugitive, and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET.

Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS
1.) Will there be haul road activities? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No <input type="checkbox"/> If YES, then complete the HAUL ROAD EMISSIONS UNIT DATA SHEET.
2.) Will there be Storage Piles? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No <input type="checkbox"/> If YES, complete Table 1 of the NONMETALLIC MINERALS PROCESSING EMISSIONS UNIT DATA SHEET.
3.) Will there be Liquid Loading/Unloading Operations? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No <input checked="" type="checkbox"/> If YES, complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET.
4.) Will there be emissions of air pollutants from Wastewater Treatment Evaporation? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No <input type="checkbox"/> If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
5.) Will there be Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, open-ended valves, sampling connections, flanges, agitators, cooling towers, etc.)? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No <input checked="" type="checkbox"/> If YES, complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS UNIT DATA SHEET.
6.) Will there be General Clean-up VOC Operations? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No <input type="checkbox"/> If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
7.) Will there be any other activities that generate fugitive emissions? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No <input type="checkbox"/> If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form.
If you answered "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions Summary."

FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants Chemical Name/CAS ¹	Maximum Potential Uncontrolled Emissions ²		Maximum Potential Controlled Emissions ³		Est. Method Used ⁴
		lb/hr	ton/yr	lb/hr	ton/yr	
Haul Road/Road Dust Emissions Paved Haul Roads	N/A	N/A	N/A	N/A	N/A	N/A
Unpaved Haul Roads	N/A	N/A	N/A	N/A	N/A	N/A
Storage Pile Emissions	N/A	N/A	N/A	N/A	N/A	N/A
Loading/Unloading Operations	VOC HAP	21.23 0.84	0.01 <0.01	21.23 0.84	0.01 <0.01	AP-42
Wastewater Treatment Evaporation & Operations	N/A	N/A	N/A	N/A	N/A	N/A
Equipment Leaks	VOCs HAP CO ₂ e	0.6 0.1 365	2.4 0.4 1,599	0.6 0.1 365	2.4 0.4 1,599	EPA- 453
General Clean-up VOC Emissions	N/A	N/A	N/A	N/A	N/A	N/A
Other	N/A	N/A	N/A	N/A	N/A	N/A

¹ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. DO NOT LIST H₂, H₂O, N₂, O₂, and Noble Gases.

² Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

³ Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁴ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

Attachment L

Attachment L
EMISSIONS UNIT DATA SHEET
GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on *Equipment List Form*): **119-CT-01**

1. Name or type and model of proposed affected source: Solar Turbines, Titan 130-20502S 21,197 hp 168 MMBtu/hr
2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.
3. Name(s) and maximum amount of proposed process material(s) charged per hour: NA
4. Name(s) and maximum amount of proposed material(s) produced per hour: NA
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants: NA

* The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

Attachment L
EMISSIONS UNIT DATA SHEET
GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on *Equipment List Form*): **119-CT-01**

<p>1. Name or type and model of proposed affected source:</p> <p>Solar Turbines, Titan 130-20502S 21,197 hp 168 MMBtu/hr</p>
<p>2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.</p>
<p>3. Name(s) and maximum amount of proposed process material(s) charged per hour:</p> <p>NA</p>
<p>4. Name(s) and maximum amount of proposed material(s) produced per hour:</p> <p>NA</p>
<p>5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:</p> <p>NA</p>

* The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

6. Combustion Data (if applicable):					
(a) Type and amount in appropriate units of fuel(s) to be burned:					
Natural Gas Fuel – As Required					
(b) Chemical analysis of proposed fuel(s), excluding coal, including maximum percent sulfur and ash:					
NA					
(c) Theoretical combustion air requirement (ACF/unit of fuel):					
NA	@	NA	°F and	NA	psia.
(d) Percent excess air: NA					
(e) Type and BTU/hr of burners and all other firing equipment planned to be used:					
NA					
(f) If coal is proposed as a source of fuel, identify supplier and seams and give sizing of the coal as it will be fired:					
NA					
(g) Proposed maximum design heat input: NA × 10 ⁶ BTU/hr.					
7. Projected operating schedule:					
Hours/Day	24	Days/Week	7	Weeks/Year	52

8. Projected amount of pollutants that would be emitted from this affected source if no control devices were used:

@	NA	°F and	Ambient	psia
a. NO _x		15.27 lb/hr	NA	grains/ACF
b. SO ₂		0.56 lb/hr	NA	grains/ACF
c. CO		9.29 lb/hr	NA	grains/ACF
d. PM/PM ₁₀ /PM _{2.5}		1.09 lb/hr	NA	grains/ACF
e. Hydrocarbons		NA lb/hr	NA	grains/ACF
f. VOCs		1.06 lb/hr	NA	grains/ACF
g. Pb		NA lb/hr	NA	grains/ACF
h. Specify other(s)				
CO _{2e}		19,462 lb/hr	NA	grains/ACF
Total HAPs		0.17 lb/hr	NA	grains/ACF
		lb/hr	NA	grains/ACF
		lb/hr	NA	grains/ACF

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

(2) Complete the Emission Points Data Sheet.

9. Proposed Monitoring, Recordkeeping, Reporting, and Testing
 Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

MONITORING
See Attachment O

RECORDKEEPING
See Attachment O

REPORTING
See Attachment O

TESTING
See Attachment O

MONITORING. PLEASE LIST AND DESCRIBE THE PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OPERATION OF THIS PROCESS EQUIPMENT OPERATION/AIR POLLUTION CONTROL DEVICE.

RECORDKEEPING. PLEASE DESCRIBE THE PROPOSED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.

REPORTING. PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORDKEEPING.

TESTING. PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR POLLUTION CONTROL DEVICE.

10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty

NA

STATION 119 EMISSION AND PERFORMANCE DATE ESTIMATES

SOLAR TURBINES INCORPORATED
 ENGINE PERFORMANCE CODE REV. 4.13.1.15.9
 CUSTOMER: Kinder Morgan Inc
 JOB ID: 3U531

DATE RUN: 11-Aug-14
 RUN BY: Kanat Ilter

--- SUMMARY OF ENGINE EXHAUST ANALYSIS ---
 POINT NUMBER 1

HP=21197, %Full Load=100.0, Elev= 800ft, %RH= 60.0, Temperature=-10.0F

GENERAL INPUT SPECIFICATIONS

ENGINE FUEL: CHOICE GAS
 29.08 in Hg AMBIENT PRESSURE
 60.0 percent RELATIVE HUMIDITY
 0.0004 --- SP. HUMIDITY (LBM H2O/LBM DRY AIR)

FUEL GAS COMPOSITION (VOLUME PERCENT)
 LHV (Btu/Scf) = 942.3 SG = 0.5808 W.I. @60F (Btu/Scf) = 1236.3
 Gas Fuel Suitability (GFS)# 28021

Methane (CH4) = 94.7142
 Ethane (C2H6) = 4.7045
 Propane (C3H8) = 0.1616
 I-Butane (C4H10) = 0.0106
 N-Butane (C4H10) = 0.0139
 I-Pentane (C5H12) = 0.0028
 N-Pentane (C5H12) = 0.0013
 Hexane (C6H14) = 0.0019
 Heptane (C7H16) = 0.0014
 Octane (C8H18) = 0.0007
 Carbon Dioxide (CO2) = 0.0876
 Nitrogen (N2) = 0.2994
 Sulfur Dioxide (SO2) = 0.0001

STANDARD CONDITIONS FOR GAS VOLUMES: Temperature: 60 deg F Pressure:
 29.92 in Hg
 NORMAL CONDITIONS FOR GAS VOLUMES: Temperature: 32 deg F Pressure:
 29.92 in Hg

GENERAL OUTPUT DATA

7304. lbm/hr FUEL FLOW
 2745.80 Scfm FUEL FLOW
 21254. Btu/lbm LOWER HEATING VALUE
 942. Btu/Scf LOWER HEATING VALUE
 95742. Scfm EXHAUST FLOW @ 14.7 PSIA & 60F
 257526. Acfm ACTUAL EXHAUST FLOW CFm
 432697. lbm/hr EXHAUST GAS FLOW
 4605.4 deg R ADIA STOICH FLAME TEMP, CHOICE GAS
 4602.2 deg R ADIA STOICH FLAME TEMP, SDNG
 28.59 --- MOLECULAR WEIGHT OF EXHAUST GAS
 58.45 --- AIR/FUEL RATIO

EXHAUST GAS ANALYSIS

ARGON	CO2	H2O	N2	O2	
0.91	3.03	5.90	75.76	14.41	VOLUME PERCENT WET
0.96	3.22	0.00	80.51	15.31	VOLUME PERCENT DRY
5478.	20157.	16077.	321196.	69780.	lbm/hr

0.75 2.76 2.20 43.98 9.55 g/(g FUEL)

100% load								
Ambient Temp, F	NOx (ppm)	NOx (lb/hr)	CO (ppm)	CO (lb/hr)	UHC (ppm)	UHC (lb/hr)	Exhaust Temp (F)	Exhaust Flow (lb/hr)
-10	42	26.0	100	37.7	50	10.8	898	432,697

--- SUMMARY OF ENGINE EXHAUST ANALYSIS ---
POINT NUMBER 1

HP=21065, %Full Load=100.0, Elev= 800ft, %RH= 60.0, Temperature= 0.0F

GENERAL INPUT SPECIFICATIONS

ENGINE FUEL: CHOICE GAS

29.08 in Hg AMBIENT PRESSURE
60.0 percent RELATIVE HUMIDITY
0.0006 --- SP. HUMIDITY (LBM H2O/LBM DRY AIR)

FUEL GAS COMPOSITION (VOLUME PERCENT)

LHV (Btu/Scf) = 942.3 SG = 0.5808 W.I. @60F (Btu/Scf) = 1236.3

Methane (CH4) = 94.7142
Ethane (C2H6) = 4.7045
Propane (C3H8) = 0.1616
I-Butane (C4H10) = 0.0106
N-Butane (C4H10) = 0.0139
I-Pentane (C5H12) = 0.0028
N-Pentane (C5H12) = 0.0013
Hexane (C6H14) = 0.0019
Heptane (C7H16) = 0.0014
Octane (C8H18) = 0.0007
Carbon Dioxide (CO2) = 0.0876
Nitrogen (N2) = 0.2994
Sulfur Dioxide (SO2) = 0.0001

STANDARD CONDITIONS FOR GAS VOLUMES: Temperature: 60 deg F Pressure: 29.92 in Hg
NORMAL CONDITIONS FOR GAS VOLUMES: Temperature: 32 deg F Pressure: 29.92 in Hg

!!! PLEASE, SUBMIT INQUIRY ON GAS FUEL SUITABILITY TO SAN DIEGO !!!

GENERAL OUTPUT DATA

7187. lbm/hr FUEL FLOW
2702.11 Scfm FUEL FLOW
21254. Btu/lbm LOWER HEATING VALUE
942. Btu/Scf LOWER HEATING VALUE
94086. Scfm EXHAUST FLOW @ 14.7 PSIA & 60F
253667. Acfm ACTUAL EXHAUST FLOW CFm
425147. lbm/hr EXHAUST GAS FLOW
4615.7 deg R ADIA STOICH FLAME TEMP, CHOICE GAS
4612.5 deg R ADIA STOICH FLAME TEMP, SDNG
28.59 --- MOLECULAR WEIGHT OF EXHAUST GAS
58.36 --- AIR/FUEL RATIO

EXHAUST GAS ANALYSIS

ARGON	CO2	H2O	N2	O2	
0.91	3.03	5.94	75.73	14.39	VOLUME PERCENT WEI
0.96	3.22	0.00	80.51	15.30	VOLUME PERCENT DRY
5381.	19832.	15910.	315514.	68501.	lbm/hr
0.75	2.76	2.21	43.90	9.53	g/(g FUEL)

--- SUMMARY OF ENGINE EXHAUST ANALYSIS ---
POINT NUMBER 2

HP=19839, %Full Load=100.0, Elev= 800ft, %RH= 60.0, Temperature= 50.0F

GENERAL INPUT SPECIFICATIONS

ENGINE FUEL: CHOICE GAS
29.08 in Hg AMBIENT PRESSURE
60.0 percent RELATIVE HUMIDITY
0.0047 --- SP. HUMIDITY (LBM H2O/LBM DRY AIR)

FUEL GAS COMPOSITION (VOLUME PERCENT)
LHV (Btu/Scf) = 942.3 SG = 0.5808 W.I. @60F (Btu/Scf) = 1236.3

Methane (CH4)	= 94.7142
Ethane (C2H6)	= 4.7045
Propane (C3H8)	= 0.1616
I-Butane (C4H10)	= 0.0106
N-Butane (C4H10)	= 0.0139
I-Pentane (C5H12)	= 0.0028
N-Pentane (C5H12)	= 0.0013
Hexane (C6H14)	= 0.0019
Heptane (C7H16)	= 0.0014
Octane (C8H18)	= 0.0007
Carbon Dioxide (CO2)	= 0.0876
Nitrogen (N2)	= 0.2994
Sulfur Dioxide (SO2)	= 0.0001

STANDARD CONDITIONS FOR GAS VOLUMES: Temperature: 60 deg F Pressure: 29.92 in Hg
NORMAL CONDITIONS FOR GAS VOLUMES: Temperature: 32 deg F Pressure: 29.92 in Hg

!!! PLEASE, SUBMIT INQUIRY ON GAS FUEL SUITABILITY TO SAN DIEGO !!!

GENERAL OUTPUT DATA

6628.	lbm/hr	FUEL FLOW
2491.63	Scfm	FUEL FLOW
21254.	Btu/lbm	LOWER HEATING VALUE
942.	Btu/Scf	LOWER HEATING VALUE
86185.	Scfm	EXHAUST FLOW @ 14.7 PSIA & 60F
238003.	Acfm	ACTUAL EXHAUST FLOW CFm
388475.	lbm/hr	EXHAUST GAS FLOW
4662.4	deg R	ADIA STOICH FLAME TEMP, CHOICE GAS
4659.1	deg R	ADIA STOICH FLAME TEMP, SDNG
28.51	---	MOLECULAR WEIGHT OF EXHAUST GAS
57.82	---	AIR/FUEL RATIO

EXHAUST GAS ANALYSIS

ARGON	CO2	H2O	N2	O2	
0.90	3.04	6.60	75.22	14.24	VOLUME PERCENT WEI
0.96	3.25	0.00	80.53	15.25	VOLUME PERCENT DRY
4896.	18211.	16190.	287081.	62089.	lbm/hr
0.74	2.75	2.44	43.32	9.37	g/(g FUEL)

TITAN 130-20502S
 CS/MD
 59F MATCH
 GAS
 TLA-2S REV. 1.1

DATA FOR NOMINAL PERFORMANCE

Fuel Type	CHOICE GAS		
Elevation	feet	800	
Inlet Loss	in H2O	4.0	
Exhaust Loss	in H2O	6.0	
Accessory on GP Shaft	HP	44.9	
Engine Inlet Temp.	deg F	0	50.0
Relative Humidity	%	60.0	60.0
Elevation Loss	HP	614	578
Inlet Loss	HP	332	319
Exhaust Loss	HP	185	183
Driven Equipment Speed	RPM	8308	8348
Optimum Equipment Speed	RPM	8308	8348
Gas Generator Speed	RPM	11220	11220
Specified Load	HP	FULL	FULL
Net Output	Power	HP	21065 19839
Fuel Flow		mmBtu/hr	152.76 140.86
Heat Rate		Btu/HP-hr	7252 7100
Therm Eff		%	35.085 35.836
Inlet Air Flow	lbm/hr	419427	383189
Engine Exhaust Flow	lbm/hr	425147	388475
PCD	psiG	244.1	230.9
Compensated PTIT	deg F	1362	1390
PT Exit Temperature	deg F	907	935
Exhaust Temperature	deg F	902	935

FUEL GAS COMPOSITION (VOLUME PERCENT)

LHV (Btu/Scf) = 942.3 SG = 0.5808 W.I. @60F (Btu/Scf) = 1236.3

Methane (CH4)	= 94.7142
Ethane (C2H6)	= 4.7045
Propane (C3H8)	= 0.1616
I-Butane (C4H10)	= 0.0106
N-Butane (C4H10)	= 0.0139
I-Pentane (C5H12)	= 0.0028
N-Pentane (C5H12)	= 0.0013
Hexane (C6H14)	= 0.0019
Heptane (C7H16)	= 0.0014
Octane (C8H18)	= 0.0007
Carbon Dioxide (CO2)	= 0.0876
Nitrogen (N2)	= 0.2994
Sulfur Dioxide (SO2)	= 0.0001

STANDARD CONDITIONS FOR GAS VOLUMES: Temperature: 60 deg F Pressure: 29.92 in Hg
NORMAL CONDITIONS FOR GAS VOLUMES: Temperature: 32 deg F Pressure: 29.92 in Hg

!!! PLEASE, SUBMIT INQUIRY ON GAS FUEL SUITABILITY TO SAN DIEGO !!!

This performance was calculated with a basic inlet and exhaust system. Special equipment such as low noise silencers, special filters, heat recovery systems or cooling devices will affect engine performance. Performance shown is "Expected" performance at the pressure drops stated, not guaranteed.

SoLoNO_x Products: Emissions in Non-SoLoNO_x Modes

Leslie Witherspoon

Solar Turbines Incorporated

PURPOSE

Solar's gas turbine dry low NO_x emissions combustion systems, known as SoLoNO_x[™], have been developed to provide the lowest emissions possible during normal operating conditions. In order to optimize the performance of the turbine, the combustion and fuel systems are designed to reduce NO_x, CO and unburned hydrocarbons (UHC) without penalizing stability or transient capabilities. At very low load and cold temperature extremes, the SoLoNO_x system must be controlled differently in order to assure stable operation. The required adjustments to the turbine controls at these conditions cause emissions to increase.

The purpose of this Product Information Letter is to provide emissions estimates, and in some cases warrantable emissions for NO_x, CO and UHC, at off-design conditions.

Historically, regulatory agencies have not required a specific emissions level to be met at low load or cold ambient operating conditions, but have asked what emissions levels are expected. The expected values are necessary to appropriately estimate emissions for annual emissions inventory purposes and for New Source Review applicability determinations and permitting.

COLD AMBIENT EMISSIONS ESTIMATES

Solar's standard temperature range warranty for gas turbines with SoLoNO_x combustion is $\geq 0^{\circ}\text{F}$ (-20°C). The *Titan*[™] 250 is an exception, with a lower standard warranty at $\geq -20^{\circ}\text{F}$ (-29°C). At ambient temperatures below 0°F , many of Solar's turbine engine models are controlled to increase pilot fuel to improve flame stability and emissions are higher. Without the increase in pilot fuel at temperatures below 0°F the engines may exhibit combustor rumble, as operation may be near the lean stability limit.

If a cold ambient emissions warranty is requested, a new production turbine configured with the latest combustion hardware is required. For most models this refers to the inclusion of Cold Ambient Fuel Control Logic.

Emissions warranties are not offered for ambient temperatures below -20°F (-29°C). In addition, cold ambient emissions warranties cannot be offered for the *Centaur*[®] 40 turbine.

Table 1 provides expected and warrantable (upon Solar's documented approval) emissions levels for Solar's SoLoNO_x combustion turbines. All emissions levels are in ppm at 15% O₂. Refer to Product Information Letter 205 for *Mercury*[™] 50 turbine emissions estimates.

For information on the availability and approvals for cold ambient temperature emissions warranties, please contact Solar's sales representatives.

Table 2 summarizes “expected” emissions levels for ambient temperatures below 0°F (–20°C) for Solar’s *SoLoNOx* turbines that do not have current production hardware or for new production hardware that is not equipped with the cold ambient fuel control logic. The emissions levels are extrapolated from San Diego factory tests and may vary at extreme temperatures and as a result of variations in other parameters, such as fuel composition, fuel quality, etc.

For more conservative NOx emissions estimate for new equipment, customers can refer to the New Source Performance Standard (NSPS) 40CFR60, subpart KKKK, where the allowable NOx emissions level for ambient temperatures < 0°F (–20°F) is 150 ppm NOx at 15% O₂. For pre-February 18, 2005, *SoLoNOx* combustion turbines subject to 40CFR60 subpart GG, a conservative estimate is the appropriate subpart GG emissions level. Subpart GG levels range from 150 to 214 ppm NOx at 15% O₂ depending on the turbine model.

Table 3 summarizes emissions levels for ambient temperatures below –20°F (–29°C) for the *Titan 250*.

Table 1. Warrantable Emissions Between 0°F and –20°F (–20° to –29°C) for New Production

Turbine Model	Fuel System	Fuel	Applicable Load	NOx, ppm	CO, ppm	UHC, ppm
<i>Centaur 50</i>	Gas Only	Gas	50 to 100% load	42	100	50
	Dual Fuel	Gas	50 to 100% load	72	100	50
<i>Taurus</i> [™] 60	Gas Only or Dual Fuel	Gas	50 to 100% load	42	100	50
<i>Taurus 65</i>	Gas Only	Gas	50 to 100% load	42	100	50
<i>Taurus 70</i>	Gas Only or Dual Fuel	Gas	50 to 100% load	42	100	50
<i>Mars</i> [®] 90	Gas Only	Gas	50 to 100% load	42	100	50
<i>Mars 100</i>	Gas Only or Dual Fuel	Gas	50 to 100% load	42	100	50
<i>Titan 130</i>	Gas Only or Dual Fuel	Gas	50 to 100% load	42	100	50
<i>Titan 250</i>	Gas Only	Gas	40 to 100% load	25	50	25
	Gas Only	Gas	40 to 100% load	15	25	25
<i>Centaur 50</i>	Dual Fuel	Liquid	65 to 100% load	120	150	75
<i>Taurus 60</i>	Dual Fuel	Liquid	65 to 100% load	120	150	75
<i>Taurus 70</i>	Dual Fuel	Liquid	65 to 100% load	120	150	75
<i>Mars 100</i>	Dual Fuel	Liquid	65 to 100% load	120	150	75
<i>Titan 130</i>	Dual Fuel	Liquid	65 to 100% load	120	150	75

Table 2. Expected Emissions below 0°F (–20°C) for SoLoNOx Combustion Turbines

Turbine Model	Fuel System	Fuel	Applicable Load	NOx, ppm	CO, ppm	UHC, ppm
<i>Centaur 40</i>	Gas Only or Dual Fuel	Gas	80 to 100% load	120	150	50
<i>Centaur 50</i>	Gas Only	Gas	50 to 100% load	120	150	50
	Dual Fuel	Gas	50 to 100% load	120	150	50
<i>Taurus 60</i>	Gas Only or Dual Fuel	Gas	50 to 100% load	120	150	50
<i>Taurus 65</i>	Gas Only	Gas	50 to 100% load	120	150	50
<i>Taurus 70</i>	Gas Only or Dual Fuel	Gas	50 to 100% load	120	150	50
<i>Mars 90</i>	Gas Only	Gas	80 to 100% load	120	150	50
<i>Mars 100</i>	Gas Only or Dual Fuel	Gas	50 to 100% load	120	150	50
<i>Titan 130</i>	Gas Only or Dual Fuel	Gas	50 to 100% load	120	150	50
<i>Centaur 40</i>	Dual Fuel	Liquid	80 to 100% load	120	150	75
<i>Centaur 50</i>	Dual Fuel	Liquid	65 to 100% load	120	150	75
<i>Taurus 60</i>	Dual Fuel	Liquid	65 to 100% load	120	150	75
<i>Taurus 70</i>	Dual Fuel	Liquid	65 to 100% load	120	150	75
<i>Mars 100</i>	Dual Fuel	Liquid	65 to 100% load	120	150	75
<i>Titan 130</i>	Dual Fuel	Liquid	65 to 100% load	120	150	75

Table 3. Expected Emissions below –20°F (–29°C) for the Titan 250 SoLoNOx Combustion Turbine

Turbine Model	Fuel System	Fuel	Applicable Load	NOx, ppm	CO, ppm	UHC, ppm
<i>Titan 250</i>	Gas Only	Gas	40 to 100% load	70	150	50

COLD AMBIENT PERMITTING STRATEGY

There are several permitting options to consider when permitting in cold ambient climates. Customers can use a tiered permitting approach or choose to permit a single emission rate over all temperatures. Historically, most construction and operating permits were silent on the ambient temperature boundaries for SoLoNOx operation.

Some customers have used a tiered permitting strategy. For purposes of compliance and annual emissions inventories, a digital thermometer is installed to record ambient temperature. The amount of time is recorded that the ambient temperature falls below 0°F. The amount of time below 0°F is then used with the emissions estimates shown in Tables 1 and 2 to estimate “actual” emissions during sub-zero operation.

A conservative alternative to using the NOx values in Tables 1, 2 and 3 is to reference 40CFR60 subpart KKKK, which allows 150 ppm NOx at 15% O₂ for sub-zero operation.

For customers who wish to permit at a single emission rate over all ambient temperatures, inlet air heating can be used to raise the engine inlet air temperature (T₁) above 0°F. With inlet air heating to keep T₁ above 0°F, standard emission warranty levels may be offered.

Inlet air heating technology options include an electric resistance heater, an inlet air to exhaust heat exchanger and a glycol heat exchanger.

If an emissions warranty is desired and ambient temperatures are commonly below –20°F (–29°C), inlet air heating can be used to raise the turbine inlet temperature (T₁) to at least –20°F. In such cases, the values shown in Table 1 can be warranted for new production.

EMISSIONS ESTIMATES IN NON-SOLONOX MODE (LOW LOAD)

At operating loads < 50% (<40% load for the *Titan 250*) on natural gas fuel and < 65% (< 80% load for *Centaur 40*) on liquid fuels, *SoLoNOx* engines are controlled to increase stability and transient response capability. The control steps that are required affect emissions in two ways: 1) pilot fuel flow is increased, increasing NOx emissions, and 2) airflow through the combustor is increased, increasing CO emissions. Note that the load levels are approximate. Engine controls are triggered either by power output for single-shaft engines or gas producer speed for two-shaft engines.

A conservative method for estimating emissions of NOx at low loads is to use the applicable NSPS: 40CFR60 subpart GG or KKKK. For projects that commence construction after February 18, 2005, subpart KKKK is the applicable NSPS and contains a NOx level of 150 ppm @ 15% O₂ for operating loads less than 75%.

Table 4 provides estimates of NOx, CO, and UHC emissions when operating in non-*SoLoNOx* mode for natural gas or liquid fuel. The estimated emissions can be assumed to vary linearly as load is decreased from just below 50% load for natural gas (or 65% load for liquid fuel) to idle.

The estimates in Table 4 apply for any product for gas only or dual fuel systems using pipeline quality natural gas. Refer to Product Information Letter 205 for *Mercury 50* emissions estimates.

Table 4. Estimated Emissions in non-*SoLoNOx* Mode

Ambient	Fuel System	Engine Load	NOx, ppm	CO, ppm	UHC, ppm
<i>Centaur 40/50, Taurus 60/65/70, Mars 90/100, Titan 130</i>					
≥ -20°F (-29°C)	Natural Gas	Less than 50%	70	8,000	800
		Idle	50	10,000	1,000
< -20°F (-29°C)	Natural Gas	Less than 50%	120	8,000	800
		Idle	120	10,000	1,000
<i>Titan 250</i>					
≥ -20°F (-29°C)	Natural Gas	Less than 40%	50	25	20
		Idle	50	2,000	200
< -20°F (-29°C)	Natural Gas	Less than 40%	70	150	50
		Idle	70	2,000	200
<i>Centaur 50, Taurus 60/70, Mars 100, Titan 130</i>					
≥ -20°F (-29°C)	Liquid	Less than 65%	120	1,000	100
		Idle	120	10,000	3,000
< -20°F (-29°C)	Liquid	Less than 65%	120	1,000	150
		Idle	120	10,000	3,000
<i>Centaur 40</i>					
≥ -20°F (-29°C)	Liquid	Less than 80%	120	1,000	100
		Idle	120	10,000	3,000
< -20°F (-29°C)	Liquid	Less than 80%	120	1,000	150
		Idle	120	10,000	3,000

Solar Turbines Incorporated
9330 Sky Park Court
San Diego, CA 92123-5398

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Emission Estimates at Start-up, Shutdown, and Commissioning for SoLoNO_x Combustion Products

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Solar Turbines Incorporated

PURPOSE

The purpose of this Product Information Letter (PIL) is to provide emission estimates for start-up and shutdown events for *Solar*[®] gas turbines with *SoLoNO_x*[™] dry low emissions combustion systems. The commissioning process is also discussed.

INTRODUCTION

The information presented in this document is representative for both generator set (GS) and compressor set/mechanical drive (CS/MD) combustion turbine applications. Operation of duct burners and/or any add-on control equipment is not accounted for in the emissions estimates. Emissions related to the start-up, shutdown, and commissioning of combustion turbines will not be guaranteed or warranted.

Combustion turbine start-up occurs in one of three modes: cold, warm, or hot. On large, utility size, combustion turbines, the start-up time varies by the “mode”. The start-up duration for a hot, warm, or cold *Solar* turbine is less than 10 minutes in simple-cycle and most combined heat and power applications.

Heat recovery steam generator (HRSG) steam pressure is usually 250 psig or less. At 250 psig or less, thermal stress within the HRSG is minimized and, therefore, firing ramp-up is not limited. However, some combined heat and power plant applications will desire or dictate longer start-up times, therefore emissions assuming a 60-minute start are also estimated.

A typical shutdown for a *Solar* turbine is <10 minutes. Emissions estimates for an elongated shutdown, 30-minutes, are also included.

Start-up and shutdown emissions estimates for the *Mercury*[™] 50 engine are found in PIL 205.

For start-up and shutdown emissions estimates for conventional combustion turbines, landfill gas, digester gas, or other alternative fuel applications, contact Solar's Environmental Programs Department.

START-UP SEQUENCE

The start-up sequence, or getting to *SoLoNO_x* combustion mode, takes three steps:

1. Purge-crank
2. Ignition and acceleration to idle
3. Loading / thermal stabilization

During the “purge-crank” step, rotation of the turbine shaft is accomplished with a starter motor to remove any residual fuel gas in the engine flow path and exhaust. During “igni-

tion and acceleration to idle,” fuel is introduced into the combustor and ignited in a diffusion flame mode and the engine rotor is accelerated to idle speed.

The third step consists of applying up to 50% load¹ while allowing the combustion flame to transition and stabilize. Once 50% load is achieved, the turbine transitions to *SoLoNOx* combustion mode and the engine control system begins to hold the combustion primary zone temperature and limit pilot fuel to achieve the targeted nitrogen oxides (NO_x), carbon monoxide (CO), and unburned hydrocarbons (UHC) emission levels.

Steps 2 and 3 are short-term transient conditions making up less than 10 minutes.

SHUTDOWN PROCESS

Normal, planned cool down/shutdown duration varies by engine model. The *Centaur*[®] 40, *Centaur* 50, *Taurus*[™] 60, and *Taurus* 65 engines take about 5 minutes. The *Taurus* 70, *Mars*[®] 90 and 100, *Titan*[™] 130 and *Titan* 250 engines take about 10 minutes. Typically, once the shutdown process starts, the emissions will remain in *SoLoNOx* mode for approximately 90 seconds and move into a transitional mode for the balance of the estimated shutdown time (assuming the unit was operating at full-load).

START-UP AND SHUTDOWN EMISSIONS ESTIMATES

Tables 1 through 5 summarize the estimated pounds of emissions per start-up and shutdown event for each product. Emissions estimates are presented for both GS and CS/MD applications on both natural gas and liquid fuel (diesel #2). The emissions estimates are calculated using empirical exhaust characteristics.

COMMISSIONING EMISSIONS

Commissioning generally takes place over a two-week period. Static testing, where no combustion occurs, usually requires one week and no emissions are expected. Dynamic testing, where combustion will occur, will see the engine start and shutdown a number of times and a variety of loads will be placed on the system. It is impossible to predict how long the turbine will run and in what combustion / emissions mode it will be running. The dynamic testing period is generally followed by one to two days of “tune-up” during which the turbine is running at various loads, most likely within low emissions mode (warranted emissions range).

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¹ 40% load for the *Titan* 250 engine on natural gas. 65% load for all engines on liquid fuel (except 80% load for the *Centaur* 40).

**Table 1. Estimation of Start-up and Shutdown Emissions (lbs/event) for SoLoNOx Generator Set Applications
10 Minute Start-up and 10 Minute Shutdown
Natural Gas Fuel**

Data will NOT be warranted under any circumstances

	Centaur 40 4701S			Centaur 50 6201S			Taurus 60 7901S			Taurus 65 8401S			
	NOx (lbs)	CO (lbs)	UHC (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO ₂ (lbs)
Total Emissions per Start (lbs)	0.6	58.1	3.3	0.8	75.0	4.3	0.8	78.5	4.5	0.9	85.8	4.9	523
Total Emissions per Shutdown (lbs)	0.3	25.5	1.5	0.4	31.1	1.8	0.4	34.7	2.0	0.4	38.2	2.2	237

	Taurus 70 10801S			Mars 90 13002S GSC			Mars 100 16002S GSC			Titan 130 20501S			Titan 250 30002S				
	NOx (lbs)	CO (lbs)	UHC (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO ₂ (lbs)	
Total Emissions per Start (lbs)	1.1	103.9	5.9	1.4	129.0	7.4	1.6	151.2	8.6	2.1	195.6	11.2	1,194	2.5	22.7	1.5	1,925
Total Emissions per Shutdown (lbs)	1.3	110.7	6.3	1.7	147.9	8.4	1.9	166.8	9.5	2.4	210.0	12.0	1,303	3.0	19.9	1.5	1,993

Assumes ISO conditions: 59F, 60% RH, sea level, no losses
Assumes unit is operating at full load prior to shutdown.
Assumes natural gas fuel; ES 9-98 compliant.

**Table 2. Estimation of Start-up and Shutdown Emissions (lbs/event) for SoLoNOx Generator Set Applications
60 Minute Start-up and 30 Minute Shutdown
Natural Gas Fuel**

Data will NOT be warranted under any circumstances

	Centaur 40 4701S				Centaur 50 6201S				Taurus 60 7901S				Taurus 65 8401S			
	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)
Total Emissions per Start (lbs)	4.1	219.4	13.0	3,420	5.0	272.4	16.1	4,219	5.7	299.8	17.8	4,780	6.1	326.5	19.3	5,074
Total Emissions per Shutdown (lbs)	1.8	121.1	7.1	1,442	2.3	163.3	9.5	1,834	2.5	163.5	9.6	1,994	2.6	177.2	10.4	2,119

	Taurus 70 10801S				Mars 90 13002S				Mars 100 16002S				Titan 130 20501S				Titan 250 30002S			
	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)
Total Emissions per Start (lbs)	7.6	410.3	24.2	6,164	10.5	570.8	33.7	8,641	11.3	583.5	34.6	9,691	13.8	740.4	43.8	11,495	14.6	75.5	7.3	16,253
Total Emissions per Shutdown (lbs)	3.3	223.0	13.0	2,588	4.3	277.0	16.2	3,685	4.8	308.1	18.0	4,056	6.0	405.3	23.7	4,826	6.2	52.6	4.1	7,222

Assumes ISO conditions: 59F, 60% RH, sea level, no losses.

Assumes unit is operating at full load prior to shutdown.

Assumes natural gas fuel; ES 9-98 compliant.

**Table 3. Estimation of Start-up and Shutdown Emissions (lbs/event) for SoLoNOx CS/MD Applications
10 Minute Start-up and 10 Minute Shutdown
Natural Gas Fuel**

Data will NOT be warranted under any circumstances

	Centaur 40 4702S				Centaur 50 6102S				Taurus 60 7802S			
	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)
Total Emissions per Start (lbs)	0.7	64.4	3.7	392	0.8	69.1	4.0	469	0.7	64.3	3.7	410
Total Emissions per Shutdown (lbs)	0.3	30.2	1.7	181	0.4	35.4	2.0	217	0.4	33.0	1.9	204

	Taurus 70 10302S				Mars 90 13002S C.SMD				Mars 100 16002S C.SMD				Titan 130 20502S				Titan 250 30002S			
	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)
Total Emissions per Start (lbs)	0.8	73.1	4.2	519	1.2	109.3	6.2	805	1.4	123.5	7.1	829	1.9	176.9	10.1	1,161	2.6	26.2	1.7	1,794
Total Emissions per Shutdown (lbs)	1.1	93.4	5.3	575	1.5	132.6	7.6	817	1.7	149.2	8.5	920	2.4	207.6	11.9	1,272	2.9	19.1	1.4	1,918

Assumes ISO conditions: 59F, 60% RH, sea level, no losses.
Assumes unit is operating at full load prior to shutdown.
Assumes natural gas fuel; ES 9-98 compliant.

**Table 4. Estimation of Start-up and Shutdown Emissions (lbs/event) for SoLoNOx Generator Set
10 Minute Start-up and 10 Minute Shutdown
Liquid Fuel (Diesel #2)**

Data will NOT be warranted under any circumstances

	Centaur 40 4701S			Centaur 50 6201S			Taurus 60 7901S			
	NOx (lbs)	CO (lbs)	UHC (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	
Total Emissions per Start (lbs)	1.3	44.5	7.4	1.7	59.0	9.8	1.7	59.8	9.9	636
Total Emissions per Shutdown (lbs)	0.6	17.3	2.8	0.7	21.2	3.4	0.8	23.5	3.8	286

	Taurus 70 10801S			Mars 100 16002S GSC			Titan 130 20501S			
	NOx (lbs)	CO (lbs)	UHC (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	
Total Emissions per Start (lbs)	2.3	78.5	13.0	3.4	114.1	18.8	4.3	147.5	24.4	1,547
Total Emissions per Shutdown (lbs)	2.5	73.6	12.0	3.8	111.4	18.1	4.7	139.1	22.6	1,677

Assumes ISO conditions: 59F, 60% RH, sea level, no losses.

Assumes unit is operating at full load prior to shutdown.

Assumes #2 Diesel fuel; ES 9-98 compliant.

**Table 5. Estimation of Start-up and Shutdown Emissions (lbs/event) for SoLoNOx Generator Set
60 Minute Start-up and 30 Minute Shutdown
Liquid Fuel (Diesel #2)**

Data will NOT be warranted under any circumstances

	Centaur 40 4701S			Centaur 50 6201S			Taurus 60 7901S					
	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)
Total Emissions per Start (lbs)	11.7	194.7	30.9	4,255	15.2	271.9	43.3	5,302	14.7	282.6	45.0	5,962
Total Emissions per Shutdown (lbs)	4.4	84.7	13.6	1,816	6.7	164.3	27.0	2,334	6.3	159.0	26.0	2,515

	Taurus 70 10801S			Mars 100 16002S			Titan 130 20501S					
	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)	NOx (lbs)	CO (lbs)	UHC (lbs)	CO2 (lbs)
Total Emissions per Start (lbs)	18.4	360.3	57.4	7,375	29.1	552.0	87.7	11,685	34.4	677.0	108.0	13,731
Total Emissions per Shutdown (lbs)	8.0	207.8	34.1	3,156	12.3	302.6	49.4	4,970	15.0	388.5	63.7	5,876

Assumes ISO conditions: 59F, 60% RH, sea level, no losses.

Assumes unit is operating at full load prior to shutdown.

Assumes #2 Diesel fuel; ES 9-98 compliant.

Attachment L

Affected Sources Data

NATURAL GAS COMPRESSOR/GENERATOR ENGINE DATA SHEET

Source Identification Number ¹		119-EG-03	
Engine Manufacturer and Model		CATERPILLAR G 3516 LE	
Manufacturer's Rated bhp/rpm		1,340 BHP @ 1400 RPM	
Source Status ²		New Source (NS)	
Date Installed/Modified/Removed ³		2016	
Engine Manufactured/Reconstruction Date ⁴		NA	
Is this a Certified Stationary Spark Ignition Engine according to 40CFR60 Subpart JJJJ? (Yes or No) ⁵		TBD	
Engine, Fuel and Combustion Data	Engine Type ⁶	LB4S	
	APCD Type ⁷	NA	
	Fuel Type ⁸	PG	
	H ₂ S (gr/100 scf)	0.25	
	Operating bhp/rpm	1,340 BHP @ 1400 RPM	
	BSFC (Btu/bhp-hr)	7,405 @ 100% load	
	Fuel throughput (ft ³ /hr)	10,964	
	Fuel throughput (MMft ³ /yr)	96	
	Operation (hrs/yr)	500	
Reference ⁹	Potential Emissions ¹⁰	lbs/hr	tons/yr
NSPS JJJJ	NO _x	5.91	1.48
NSPS JJJJ	CO	11.82	2.95
NSPS JJJJ	VOC	2.95	0.74
AP-42 Chapter 3.2	SO ₂	0.01	<0.01
AP-42 Chapter 3.2	PM ₁₀	0.11	0.03
AP-42 Chapter 3.2	Formaldehyde	0.59	0.15

Attachment L

Affected Sources Data

1. Enter the appropriate Source Identification Number for each natural gas-fueled reciprocating internal combustion compressor/generator engine located at the compressor station. Multiple compressor engines should be designated CE-1, CE-2, CE-3 etc. Generator engines should be designated GE-1, GE-2, GE-3 etc. If more than three (3) engines exist, please use additional sheets.
2. Enter the Source Status using the following codes:

NS	Construction of New Source (installation)	ES	Existing Source
MS	Modification of Existing Source	RS	Removal of Source
3. Enter the date (or anticipated date) of the engine's installation (construction of source), modification or removal.
4. Enter the date that the engine was manufactured, modified or reconstructed.
5. Is the engine a certified stationary spark ignition internal combustion engine according to 40CFR60 Subpart JJJJ. If so, the engine and control device must be operated and maintained in accordance with the manufacturer's emission-related written instructions. You must keep records of conducted maintenance to demonstrate compliance, but no performance testing is required. If the certified engine is not operated and maintained in accordance with the manufacturer's emission-related written instructions, the engine will be considered a non-certified engine and you must demonstrate compliance according to 40CFR§60.4243a(2)(i) through (iii), as appropriate.

Provide a manufacturer's data sheet for all engines being registered.

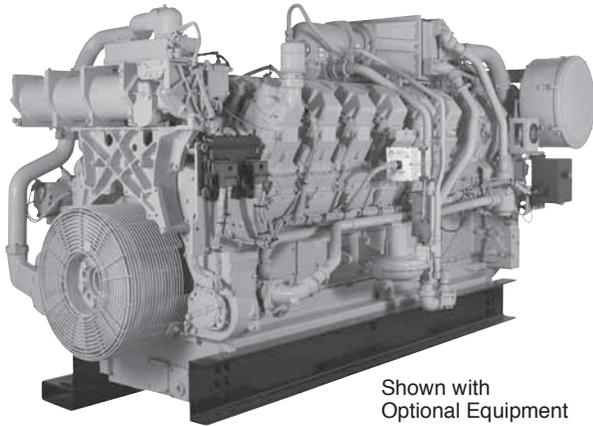
6. Enter the Engine Type designation(s) using the following codes:

LB2S	Lean Burn Two Stroke	RB4S	Rich Burn Four Stroke
LB4S	Lean Burn Four Stroke		
7. Enter the Air Pollution Control Device (APCD) type designation(s) using the following codes:

A/F	Air/Fuel Ratio	IR	Ignition Retard
HEIS	High Energy Ignition System	SIPC	Screw-in Precombustion Chambers
PSC	Prestratified Charge	LEC	Low Emission Combustion
NSCR	Rich Burn & Non-Selective Catalytic Reduction	SCR	Lean Burn & Selective Catalytic Reduction
8. Enter the Fuel Type using the following codes:

PQ	Pipeline Quality Natural Gas	RG	Raw Natural Gas
----	------------------------------	----	-----------------
9. Enter the Potential Emissions Data Reference designation using the following codes. Attach all referenced data to this *Compressor/Generator Data Sheet(s)*.

MD	Manufacturer's Data	AP	AP-42	
GR	GRI-HAPCalc TM	OT	Other _____	(please list)
10. Enter each engine's Potential to Emit (PTE) for the listed regulated pollutants in pounds per hour and tons per year. PTE shall be calculated at manufacturer's rated brake horsepower and may reflect reduction efficiencies of listed Air Pollution Control Devices. Emergency generator engines may use 500 hours of operation when calculating PTE. PTE data from this data sheet shall be incorporated in the *Emissions Summary Sheet*.



Shown with
Optional Equipment

CAT® ENGINE SPECIFICATIONS

V-16, 4-Stroke-Cycle

Bore	1 70 mm (6.7 in.)
Stroke	1 90 mm (7.5 in.)
Displacement	6 9 L (4210 cu. in.)
Aspiration	Turbocharged-Aftercooled
Digital Engine Management	
Governor and Protection	Electronic (ADEM™ A3)
Combustion	Low Emission (Lean Burn)
Engine Weight, net dry (approx)	8 015 kg (17,670 lb)
Power Density	8 kg/kW (13.2 lb/bhp)
Power per Displacement	1 9.3 bhp/L
Total Cooling System Capacity	2 17.7 L (57.5 gal)
Jacket Water	2 00.6 L (53 gal)
Aftercooler Circuit	1 7 L (4.5 gal)
Lube Oil System (refill)	4 24 L (112 gal)
Oil Change Interval	1 000 hours
Rotation (from flywheel end)	Counterclockwise
Flywheel and Flywheel Housing	SAE No. 00
Flywheel Teeth	1 83

FEATURES

Engine Design

- Proven reliability and durability
- Ability to burn a wide spectrum of gaseous fuels
- Robust diesel strength design prolongs life and lowers owning and operating costs
- Broad operating speed range

Emissions

Meets U.S. EPA Spark Ignited Stationary NSPS Emissions for 2007/8

Lean Burn Engine Technology

Lean-burn engines operate with large amounts of excess air. The excess air absorbs heat during combustion reducing the combustion temperature and pressure, greatly reducing levels of NOx. Lean-burn design also provides longer component life and excellent fuel consumption.

Advanced Digital Engine Management

ADEM A3 control system providing integrated ignition, speed governing, protection, and controls, including detonation-sensitive variable ignition timing. ADEM A3 has improved: user interface, display system, shutdown controls, and system diagnostics.

Ease of Operation

Side covers on block allow for inspection of internal components

Full Range of Attachments

Large variety of factory-installed engine attachments reduces packaging time

Testing

Every engine is full-load tested to ensure proper engine performance.

Gas Engine Rating Pro

GERP is a PC-based program designed to provide site performance capabilities for Cat® natural gas engines for the gas compression industry. GERP provides engine data for your site's altitude, ambient temperature, fuel, engine coolant heat rejection, performance data, installation drawings, spec sheets, and pump curves.

Product Support Offered Through Global Cat Dealer Network

More than 2,200 dealer outlets

Cat factory-trained dealer technicians service every aspect of your petroleum engine

Cat parts and labor warranty

Preventive maintenance agreements available for repair-before-failure options

S•O•SSM program matches your oil and coolant samples against Caterpillar set standards to determine:

- Internal engine component condition
- Presence of unwanted fluids
- Presence of combustion by-products
- Site-specific oil change interval

Over 80 Years of Engine Manufacturing Experience

Over 60 years of natural gas engine production

Ownership of these manufacturing processes enables Caterpillar to produce high quality, dependable products.

- Cast engine blocks, heads, cylinder liners, and flywheel housings
- Machine critical components
- Assemble complete engine

Web Site

For all your petroleum power requirements, visit www.catoilandgas.cat.com.

STANDARD EQUIPMENT

Air Inlet System

Air cleaner — intermediate-duty with service indicator

Control System

A3 ECU

Air-fuel ratio control

Cooling System

Thermostats and housing

Jacket water pump

Aftercooler water pump

Aftercooler core for sea-air atmosphere

Aftercooler thermostats and housing

Exhaust System

Watercooled exhaust manifolds

Flywheels & Flywheel Housings

SAE No. 00 flywheel

SAE No. 00 flywheel housing

SAE standard rotation

Fuel System

Gas pressure regulator

Natural gas carburetor

Ignition System

A3 ECU

Instrumentation

PL1000 Advisor panel

Lubrication System

Crankcase breather — top mounted

Oil cooler

Oil filter — RH

Oil bypass filter

Oil pan — shallow

Oil sampling valve

Turbo oil accumulator

Mounting System

Rails, engine mounting — 254 mm (10 in)

Protection System

Electronic shutoff system

Gas shutoff valve

General

Paint — Cat yellow

Vibration damper and guard — dual 484 mm (23 in)

OPTIONAL EQUIPMENT

Air Inlet System

Remote air inlet adapters

Precleaner

Charging System

Battery chargers

Charging alternators

Cooling System

Aftercooler core

Thermostatic valve

Temperature switch

Connections

Expansion and overflow tank

Water level switch gauge

Exhaust System

Flexible fittings

Elbows

Flange

Flange and exhaust expanders

Rain cap

Mufflers

Fuel System

Low pressure gas conversions

Propane gas valve and jet kits

Fuel filter

Instrumentation

PL1000 communications modules

Lubrication System

Oil bypass filter removal and oil pan accessories

Sump pump

Air prelube pump

Manual prelube pump

Lubricating oil

Mounting System

Rails

Vibration isolators

Power Take-Offs

Front accessory drives

Auxiliary drive shafts and pulleys

Front stub shaft

Pulleys

Protection System

Explosion relief valves, status control box interconnect wiring harness

Starting System

Air starting motor

Air pressure regulator

Air silencer

Electric air start controls

Electric starting motors — dual 24-volt

Starting aids

Battery sets (24-volt dry), cables, and rack

General

Flywheel inertia weight

Guard removal

Engine barring group

Premium 8:1 pistons

Premium cylinder heads

TECHNICAL DATA

G3516 LE Gas Petroleum Engine

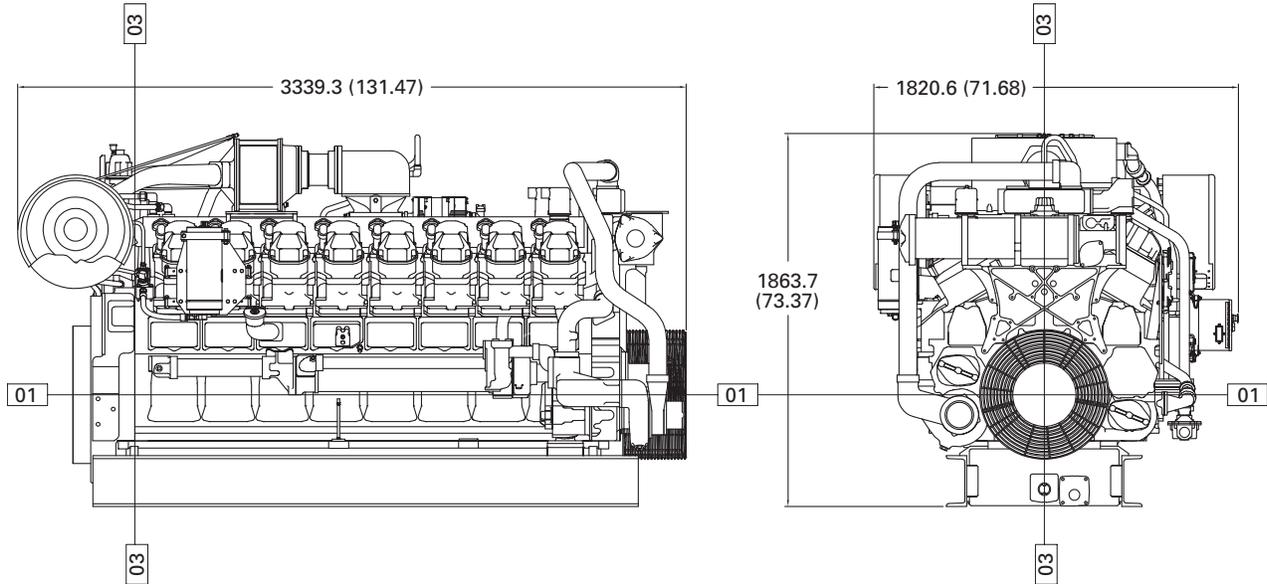
Fuel System	D	2 g NOx NTE Rating 2 M8618-01 D	g NOx NTE Rating M8620-01
Engine Power			
@ 100% Load b	kW (bhp) 9	99 (1340) 8	58 (1150)
@ 75% Load b	kW (bhp) 7	49 (1004) 6	43 (862)
Engine Speed rp	m	1400 1	200
Max Altitude @ Rated Torque			
a nd 38°C (100°F) m	(ft) 3	04.8 (1000) 1	219.2 (4000)
Sp eed Turndown @ Max Altitude, R ated Torque, and 38°C (100°F) %	2	5 9	.2
SCAC Temperature °	C (°F) 5	4 (130) 5	4 (130)
Emissions*			
N Ox g	/bkW-hr (g/bhp-hr) 2	.68 (2) 2	.68 (2)
C O g	/bkW-hr (g/bhp-hr) 2	.49 (1.86) 2	.35 (1.75)
C O ₂ g	/bkW-hr (g/bhp-hr) 6	32 (471) 6	24 (466)
VO C** g	/bkW-hr (g/bhp-hr) 0	.35 (0.26) 0	.4 (0.3)
Fuel Consumption***			
@ 100% Load MJ/	bkW-hr (Btu/bhp-hr) 1	0.48 (7405) 1	0.36 (7324)
@ 75% Load MJ/	bkW-hr (Btu/bhp-hr) 1	0.79 (7628) 1	0.76 (7605)
Heat Balance			
H eat Rejection to Jacket Water			
@ 100% Load b	kW (Btu/mn) 7	41 (42,123) 6	39 (36,343)
@ 75% Load b	kW (Btu/mn) 6	16.7 (35,075) 5	54 (31,480)
H eat Rejection to Aftercooler			
@ 100% Load b	kW (Btu/mn) 1	67.8 (9546) 1	31.9 (7509)
@ 75% Load b	kW (Btu/mn) 1	08.6 (6179) 7	2.2 (4108)
H eat Rejection to Exhaust			
@ 100% Load			
LHV to 25° C (77° F)	bkW (Btu/mn) 8	37.8 (47,643) 6	94.6 (39,536)
@ 75% Load			
LHV to 25° C (77° F)	bkW (Btu/mn) 6	30.4 (35,848) 5	24.1 (29,806)
Exhaust System			
Exh aust Gas Flow Rate			
@ 100% Load m	³/min (cfm) 2	17.0 (7663) 1	82.9 (6460)
@ 75% Load m	³/min (cfm) 1	63.8 (5785) 1	38.9 (4905)
Exh aust Stack Temperature			
@ 100% Load °	C (°F) 4	67.22 (873) 4	52.2 (846)
@ 75% Load °	C (°F) 4	67.22 (873) 4	50.5 (843)
Intake System			
Ai r Inlet Flow Rate			
@ 100% Load m	³/min (scfm) 8	0.6 (2847) 6	9.5 (2453)
@ 75% Load m	³/min (scfm) 6	0.8 (2147) 5	2.8 (1864)
Gas Pressure kPa	g (psig) 2 (3)	41.5-275.8 2 5-40) (3)	41.5-275.8 5-40)

*at 100% load and speed, all values are listed as not to exceed

**Volatile organic compounds as defined in U.S. EPA 40 CFR 60, subpart JJJJ

***ISO 3046/1

GAS PETROLEUM ENGINE



DIMENSIONS		
Length mm	(in.) 3	339.3 (131.47)
Width mm	(in.) 1	820.6 (71.68)
Height mm	(in.) 1	863.7 (73.37)
Shipping Weight kg	(lb) 8	015 (17,670)

Note: General configuration not to be used for installation. See general dimension drawings for detail (drawing #289-2971).

Dimensions are in mm (inches).

RATING DEFINITIONS AND CONDITIONS

Engine performance is obtained in accordance with SAE J1995, ISO3046/1, BS5514/1, and DIN6271/1 standards.

Transient response data is acquired from an engine/generator combination at normal operating temperature and in accordance with ISO3046/1 standard ambient conditions. Also in accordance with SAE J1995, BS5514/1, and DIN6271/1 standard reference conditions.

Conditions: Power for gas engines is based on fuel having an LHV of 33.74 kJ/L (905 Btu/cu ft) at 101 kPa (29.91 in. Hg) and 15° C (59° F). Fuel rate is based on a cubic meter at 100 kPa (29.61 in. Hg) and 15.6° C (60.1° F). Air flow is based on a cubic foot at 100 kPa (29.61 in. Hg) and 25° C (77° F). Exhaust flow is based on a cubic foot at 100 kPa (29.61 in. Hg) and stack temperature.

Materials and specifications are subject to change without notice. The International System of Units (SI) is used in this publication. CAT, CATERPILLAR, their respective logos, ADEM, "Caterpillar Yellow" and the "Power Edge" trade dress, as well as corporate and product identity used herein, are trademarks of Caterpillar and may not be used without permission.

Attachment L
EMISSIONS UNIT DATA SHEET
GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on *Equipment List Form*): **119-WH-02**

1. Name or type and model of proposed affected source: Hydronic Heater 4.60 MMBtu/hr
2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.
3. Name(s) and maximum amount of proposed process material(s) charged per hour: NA
4. Name(s) and maximum amount of proposed material(s) produced per hour: NA
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants: NA

* The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

6. Combustion Data (if applicable):					
(a) Type and amount in appropriate units of fuel(s) to be burned:					
Natural Gas Fuel – As Required					
(b) Chemical analysis of proposed fuel(s), excluding coal, including maximum percent sulfur and ash:					
NA					
(c) Theoretical combustion air requirement (ACF/unit of fuel):					
NA	@	NA	°F and	NA	psia.
(d) Percent excess air: NA					
(e) Type and BTU/hr of burners and all other firing equipment planned to be used:					
NA					
(f) If coal is proposed as a source of fuel, identify supplier and seams and give sizing of the coal as it will be fired:					
NA					
(g) Proposed maximum design heat input: NA × 10 ⁶ BTU/hr.					
7. Projected operating schedule:					
Hours/Day	24	Days/Week	7	Weeks/Year	52

8. Projected amount of pollutants that would be emitted from this affected source if no control devices were used:

@	NA	°F and	Ambient	psia
a. NO _x		0.11 lb/hr	NA	grains/ACF
b. SO ₂		<0.01 lb/hr	NA	grains/ACF
c. CO		0.25 lb/hr	NA	grains/ACF
d. PM/PM ₁₀ /PM _{2.5}		0.05 lb/hr	NA	grains/ACF
e. Hydrocarbons		NA lb/hr	NA	grains/ACF
f. VOCs		0.03 lb/hr	NA	grains/ACF
g. Pb		NA lb/hr	NA	grains/ACF
h. Specify other(s)				
CO _{2e}		541 lb/hr	NA	grains/ACF
Total HAPs		0.01 lb/hr	NA	grains/ACF
		lb/hr	NA	grains/ACF
		lb/hr	NA	grains/ACF

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

(2) Complete the Emission Points Data Sheet.

9. Proposed Monitoring, Recordkeeping, Reporting, and Testing
 Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

MONITORING
See Attachment O

RECORDKEEPING
See Attachment O

REPORTING
See Attachment O

TESTING
See Attachment O

MONITORING. PLEASE LIST AND DESCRIBE THE PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OPERATION OF THIS PROCESS EQUIPMENT OPERATION/AIR POLLUTION CONTROL DEVICE.

RECORDKEEPING. PLEASE DESCRIBE THE PROPOSED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.

REPORTING. PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORDKEEPING.

TESTING. PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR POLLUTION CONTROL DEVICE.

10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty

NA

PO# 6501955-0-STAT
REFERENCE: AFE 62018 -TGP STATION 315 - ROSE LAKE
ACTIVITY: 620183680999999

ONE (1) PARKER BOILER T4600LR,
DIRECT FIRED HOT WATER GLYCOL BOILER SKID MOUNTED



BOILER MANUFACTURER

PARKER BOILER

5930 BANDINI BLVD
LOS ANGELES, CA 90040
TEL: 323-727-9800
FAX: 323-722-2848
www.parkerboiler.com

KINDER MORGAN, INC

1001 LOUISIANA ST, STE 1000
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PARKER BOILER CO.

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WEB SITE: www.parkerboiler.com • E-MAIL: sales@parkerboiler.com

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Fax. (323) 722-2848

**EMISSION DATA FOR METAL FIBER PREMIX NATURAL GAS FIRED
BURNER SYSTEMS ON PARKER BOILERS**

The following is our approximation of the Emission Levels from our boilers. Emissions may vary, based on Boiler and Field Conditions.

			<u>PPM @ 3%O2</u>		
1.	HC (Hydrocarbons)	60		=	.031 Lbs./ 1.0 Million BTU/HR
2.	CO (Carbon Monoxide)	60		=	.0552 Lbs./ 1.0 Million BTU/HR
3.	SO2 (Sulfur Dioxide)	NIL		=	NIL
4.	NOx (Nitrous Oxides)	20		=	.024 Lbs./ 1.0 Million BTU/HR
5.	PM-15 (Particulate Matter)			<	.01 Lbs./ 1.0 Million BTU/HR

By multiplying these levels by the BTU input in millions, you can calculate the Lbs./Hr. Emissions based on full firing of the subject boiler.

Contact Parker Boiler should you have any questions.

Attachment L EMISSIONS UNIT DATA SHEET STORAGE TANKS

Provide the following information for each new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT www.epa.gov/tnn/tanks.html), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<http://www.epa.gov/tnn/chief/>).

I. GENERAL INFORMATION (required)

1. Bulk Storage Area Name Storage Tank Area	2. Tank Name Pipeline Liquids Storage Tank
3. Tank Equipment Identification No. (as assigned on <i>Equipment List Form</i>) 119-PF-04	4. Emission Point Identification No. (as assigned on <i>Equipment List Form</i>) 119-PF-04
5. Date of Commencement of Construction (for existing tanks) NA	
6. Type of change <input checked="" type="checkbox"/> New Construction <input type="checkbox"/> New Stored Material <input type="checkbox"/> Other Tank Modification	
7. Description of Tank Modification (if applicable) NA	
7A. Does the tank have more than one mode of operation? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No (e.g. Is there more than one product stored in the tank?)	
7B. If YES, explain and identify which mode is covered by this application (Note: A separate form must be completed for each mode).	
7C. Provide any limitations on source operation affecting emissions, any work practice standards (e.g. production variation, etc.): NA	

II. TANK INFORMATION (required)

8. Design Capacity (specify barrels or gallons). Use the internal cross-sectional area multiplied by internal height. <p style="text-align: center;">3,760 gallons</p>	
9A. Tank Internal Diameter (ft) <p style="text-align: center;">8</p>	9B. Tank Internal Height (or Length) (ft) <p style="text-align: center;">10</p>
10A. Maximum Liquid Height (ft) <p style="text-align: center;">10</p>	10B. Average Liquid Height (ft) <p style="text-align: center;">8</p>
11A. Maximum Vapor Space Height (ft) <p style="text-align: center;">8</p>	11B. Average Vapor Space Height (ft) <p style="text-align: center;">6</p>
12. Nominal Capacity (specify barrels or gallons). This is also known as "working volume" and considers design liquid levels and overflow valve heights. <p style="text-align: center;">3,760 gallons</p>	

13A. Maximum annual throughput (gal/yr) 7,520	13B. Maximum daily throughput (gal/day) 10
14. Number of Turnovers per year (annual net throughput/maximum tank liquid volume) 2	
15. Maximum tank fill rate (gal/min) TBD	
16. Tank fill method <input type="checkbox"/> Submerged <input type="checkbox"/> Splash <input checked="" type="checkbox"/> Bottom Loading	
17. Complete 17A and 17B for Variable Vapor Space Tank Systems <input checked="" type="checkbox"/> Does Not Apply	
17A. Volume Expansion Capacity of System (gal)	17B. Number of transfers into system per year
18. Type of tank (check all that apply): <input checked="" type="checkbox"/> Fixed Roof <input checked="" type="checkbox"/> vertical <input type="checkbox"/> horizontal <input type="checkbox"/> flat roof <input checked="" type="checkbox"/> cone roof <input type="checkbox"/> dome roof <input type="checkbox"/> other (describe) <input type="checkbox"/> External Floating Roof <input type="checkbox"/> pontoon roof <input type="checkbox"/> double deck roof <input type="checkbox"/> Domed External (or Covered) Floating Roof <input type="checkbox"/> Internal Floating Roof <input type="checkbox"/> vertical column support <input type="checkbox"/> self-supporting <input type="checkbox"/> Variable Vapor Space <input type="checkbox"/> lifter roof <input type="checkbox"/> diaphragm <input type="checkbox"/> Pressurized <input type="checkbox"/> spherical <input type="checkbox"/> cylindrical <input type="checkbox"/> Underground <input type="checkbox"/> Other (describe)	

III. TANK CONSTRUCTION & OPERATION INFORMATION (optional if providing TANKS Summary Sheets)

19. Tank Shell Construction: <input type="checkbox"/> Riveted <input type="checkbox"/> Gunitite lined <input type="checkbox"/> Epoxy-coated rivets <input checked="" type="checkbox"/> Other (describe) TBD		
20A. Shell Color grey/light	20B. Roof Color grey/light	20C. Year Last Painted NA
21. Shell Condition (if metal and unlined): <input checked="" type="checkbox"/> No Rust <input type="checkbox"/> Light Rust <input type="checkbox"/> Dense Rust <input type="checkbox"/> Not applicable		
22A. Is the tank heated? <input type="checkbox"/> YES <input checked="" type="checkbox"/> NO		
22B. If YES, provide the operating temperature (°F)		
22C. If YES, please describe how heat is provided to tank.		
23. Operating Pressure Range (psig): Atmospheric to		
24. Complete the following section for Vertical Fixed Roof Tanks		<input type="checkbox"/> Does Not Apply
24A. For dome roof, provide roof radius (ft)		
24B. For cone roof, provide slope (ft/ft) 0.0625		
25. Complete the following section for Floating Roof Tanks		<input checked="" type="checkbox"/> Does Not Apply
25A. Year Internal Floaters Installed:		
25B. Primary Seal Type: <input type="checkbox"/> Metallic (Mechanical) Shoe Seal <input type="checkbox"/> Liquid Mounted Resilient Seal <input type="checkbox"/> Vapor Mounted Resilient Seal <input type="checkbox"/> Other (describe):		
25C. Is the Floating Roof equipped with a Secondary Seal? <input type="checkbox"/> YES <input type="checkbox"/> NO		
25D. If YES, how is the secondary seal mounted? (check one) <input type="checkbox"/> Shoe <input type="checkbox"/> Rim <input type="checkbox"/> Other (describe):		
25E. Is the Floating Roof equipped with a weather shield? <input type="checkbox"/> YES <input type="checkbox"/> NO		

25F. Describe deck fittings; indicate the number of each type of fitting:		
ACCESS HATCH		
BOLT COVER, GASKETED:	UNBOLTED COVER, GASKETED:	UNBOLTED COVER, UNGASKETED:
AUTOMATIC GAUGE FLOAT WELL		
BOLT COVER, GASKETED:	UNBOLTED COVER, GASKETED:	UNBOLTED COVER, UNGASKETED:
COLUMN WELL		
BUILT-UP COLUMN – SLIDING COVER, GASKETED:	BUILT-UP COLUMN – SLIDING COVER, UNGASKETED:	PIPE COLUMN – FLEXIBLE FABRIC SLEEVE SEAL:
LADDER WELL		
PIP COLUMN – SLIDING COVER, GASKETED:	PIPE COLUMN – SLIDING COVER, UNGASKETED:	
GAUGE-HATCH/SAMPLE PORT		
SLIDING COVER, GASKETED:	SLIDING COVER, UNGASKETED:	
ROOF LEG OR HANGER WELL		
WEIGHTED MECHANICAL ACTUATION, GASKETED:	WEIGHTED MECHANICAL ACTUATION, UNGASKETED:	SAMPLE WELL-SLIT FABRIC SEAL (10% OPEN AREA)
VACUUM BREAKER		
WEIGHTED MECHANICAL ACTUATION, GASKETED:	WEIGHTED MECHANICAL ACTUATION, UNGASKETED:	
RIM VENT		
WEIGHTED MECHANICAL ACTUATION GASKETED:	WEIGHTED MECHANICAL ACTUATION, UNGASKETED:	
DECK DRAIN (3-INCH DIAMETER)		
OPEN:	90% CLOSED:	
STUB DRAIN		
1-INCH DIAMETER:		
OTHER (DESCRIBE, ATTACH ADDITIONAL PAGES IF NECESSARY)		

26. Complete the following section for Internal Floating Roof Tanks		<input checked="" type="checkbox"/> Does Not Apply
26A. Deck Type: <input type="checkbox"/> Bolted <input type="checkbox"/> Welded		
26B. For Bolted decks, provide deck construction:		
26C. Deck seam:		
<input type="checkbox"/> Continuous sheet construction 5 feet wide <input type="checkbox"/> Continuous sheet construction 6 feet wide <input type="checkbox"/> Continuous sheet construction 7 feet wide <input type="checkbox"/> Continuous sheet construction 5 × 7.5 feet wide <input type="checkbox"/> Continuous sheet construction 5 × 12 feet wide <input type="checkbox"/> Other (describe)		
26D. Deck seam length (ft)	26E. Area of deck (ft ²)	
For column supported tanks:	26G. Diameter of each column:	
26F. Number of columns:		

IV. SITE INFORMATION (optional if providing TANKS Summary Sheets)

27. Provide the city and state on which the data in this section are based. See attached summary sheets
28. Daily Average Ambient Temperature (°F)
29. Annual Average Maximum Temperature (°F)
30. Annual Average Minimum Temperature (°F)
31. Average Wind Speed (miles/hr)
32. Annual Average Solar Insulation Factor (BTU/(ft ² ·day))
33. Atmospheric Pressure (psia)

V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)

34. Average daily temperature range of bulk liquid: See attached summary sheets			
34A. Minimum (°F)	34B. Maximum (°F)		
35. Average operating pressure range of tank:			
35A. Minimum (psig)	35B. Maximum (psig)		
36A. Minimum Liquid Surface Temperature (°F)	36B. Corresponding Vapor Pressure (psia)		
37A. Average Liquid Surface Temperature (°F)	37B. Corresponding Vapor Pressure (psia)		
38A. Maximum Liquid Surface Temperature (°F)	38B. Corresponding Vapor Pressure (psia)		
39. Provide the following for <u>each</u> liquid or gas to be stored in tank. Add additional pages if necessary.			
39A. Material Name or Composition	Pipeline Liquids		
39B. CAS Number			
39C. Liquid Density (lb/gal)			
39D. Liquid Molecular Weight (lb/lb-mole)			
39E. Vapor Molecular Weight (lb/lb-mole)			

Attachment L

EMISSIONS UNIT DATA SHEET

BULK LIQUID TRANSFER OPERATIONS

Furnish the following information for each new or modified bulk liquid transfer area or loading rack, as shown on the *Equipment List Form* and other parts of this application. This form is to be used for bulk liquid transfer operations such as to and from drums, marine vessels, rail tank cars, and tank trucks.

Identification Number (as assigned on <i>Equipment List Form</i>): 119-LR-05				
1. Loading Area Name: Tank Truck Loading Area				
2. Type of cargo vessels accommodated at this rack or transfer point (check as many as apply): <input type="checkbox"/> Drums <input type="checkbox"/> Marine Vessels <input type="checkbox"/> Rail Tank Car <input checked="" type="checkbox"/> Tank Trucks				
3. Loading Rack or Transfer Point Data:				
Number of pumps	1			
Number of liquids loaded	1			
Maximum number of marine vessels, tank trucks, tank cars, and/or drums loading at one time	1			
4. Does ballasting of marine vessels occur at this loading area? <input type="checkbox"/> Yes <input type="checkbox"/> No <input checked="" type="checkbox"/> Does not apply				
5. Describe cleaning location, compounds and procedure for cargo vessels using this transfer point: NA				
6. Are cargo vessels pressure tested for leaks at this or any other location? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No If YES, describe:				
7. Projected Maximum Operating Schedule (for rack or transfer point as a whole):				
Maximum	Jan. - Mar.	Apr. - June	July - Sept.	Oct. - Dec.
hours/day	As Needed			
days/week	As Needed			
weeks/quarter	As Needed			

8. Bulk Liquid Data <i>(add pages as necessary)</i> :		
Pump ID No.		NA
Liquid Name		Wastewater
Max. daily throughput (1000 gal/day)		7.52
Max. annual throughput (1000 gal/yr)		7.52
Loading Method ¹		SUB
Max. Fill Rate (gal/min)		90
Average Fill Time (min/loading)		60
Max. Bulk Liquid Temperature (°F)		60 °F
True Vapor Pressure ²		7.70
Cargo Vessel Condition ³		U
Control Equipment or Method ⁴		NA
Minimum control efficiency (%)		NA
Maximum Emission Rate	Loading (lb/hr)	VOC – 21.23 Total HAP – 0.84
	Annual (lb/yr)	VOC – 29.57 Total HAP – 1.17
Estimation Method ⁵		EPA AP-42
¹ BF = Bottom Fill SP = Splash Fill SUB = Submerged Fill		
² At maximum bulk liquid temperature		
³ B = Ballasted Vessel, C = Cleaned, U = Uncleaned (dedicated service), O = other (describe)		
⁴ List as many as apply (complete and submit appropriate <i>Air Pollution Control Device Sheets</i>): CA = Carbon Adsorption LOA = Lean Oil Adsorption CO = Condensation SC = Scrubber (Absorption) CRA = Compressor-Refrigeration-Absorption TO = Thermal Oxidation or Incineration CRC = Compression-Refrigeration-Condensation VB = Dedicated Vapor Balance (closed system) O = other (describe)		
⁵ EPA = EPA Emission Factor as stated in AP-42 MB = Material Balance TM = Test Measurement based upon test data submittal O = other (describe)		

<p>9. Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.</p>	
<p>MONITORING</p> <p>TGP will comply with all monitoring requirements set forth in the permit that is issued.</p>	<p>RECORDKEEPING</p> <p>TGP will comply with all recordkeeping requirements set forth in the permit that is issued.</p>
<p>REPORTING</p> <p>TGP will comply with all reporting requirements set forth in the permit that is issued.</p>	<p>TESTING</p> <p>TGP will comply with all testing requirements set forth in the permit that is issued.</p>
<p>MONITORING. PLEASE LIST AND DESCRIBE THE PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OPERATION OF THIS PROCESS EQUIPMENT OPERATION/AIR POLLUTION CONTROL DEVICE.</p>	
<p>RECORDKEEPING. PLEASE DESCRIBE THE PROPOSED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.</p>	
<p>REPORTING. PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORDKEEPING.</p>	
<p>TESTING. PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR POLLUTION CONTROL DEVICE.</p>	
<p>10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty</p> <p>NA</p>	

Attachment M

Attachment M

Air Pollution Control Devices

There are no proposed air pollution control devices at Station 119A. The combustion turbine will utilize Solar Turbines' *SoLoNO_x* technology, as described in the emissions calculation methodology included in this application, as well as in the Solar Turbines manufacturer data included in Attachment L. This technology is part of the unit design.

Attachment N

Table N-1 Equipment List

Emission Point ID	Source	Manufacturer	Model/Type	Rated Capacity ⁽¹⁾	Heat Input (MMBTU/Hr)
119-CT-01	Compressor Turbine	Solar Turbines	Titan 130-20502S	21,197 hp	168.0
119-EG-03	Emergency Generator	Caterpillar	G 3516 LE	1,340 hp	11.18
119-WH-02	Hydronic Heater	Parker Boiler	T4600LR	-	4.60
FUG	Fugitive Emissions	-	-	-	-
V/BD	Venting/Blowdown Emissions	-	-	-	-
119-PF-04	Pipeline Liquids Storage Tank	-	-	3,760 gal	-
119-LR-05	Pipeline Liquids Truck Loading	-	-	-	-

1. The rated capacity for the compressor turbines is based on 100% load operation at -10°F ambient temperature.

Table N-2 Summary of Potential Emissions

Emission Point ID	Source Description	CO		NO _x		PM		PM _{2.5}		PM ₁₀		SO ₂		VOC		Total HAP		CO ₂ e	
		lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
119-CT-01	Compressor Turbine	9.29	67.70	15.27	62.33	1.09	4.41	1.09	4.41	1.09	4.41	0.56	2.27	1.06	4.67	0.17	0.74	19,462	78,914
119-EG-03	Emergency Generator	11.82	2,95	5.91	1.48	0.11	0.03	0.11	0.03	0.11	0.03	0.01	<0.01	2.95	0.74	0.81	0.20	1,658	415
119-WH-02	Hydronic Heater	0.25	1.11	0.11	0.48	0.05	0.20	0.05	0.20	0.05	0.20	<0.01	0.01	0.03	0.12	0.01	0.04	541	2,371
FUG	Fugitive Emissions	-	-	-	-	-	-	-	-	-	-	-	-	0.56	2.44	0.09	0.41	365	1,599
V/BD	Venting/Blowdown Emissions	-	-	-	-	-	-	-	-	-	-	-	-	0.03	0.13	<0.01	<0.01	361	1,580
119-PF-04	Pipeline Liquids Storage Tank	-	-	-	-	-	-	-	-	-	-	-	-	0.05	0.20	<0.01	0.01	Neg.	Neg.
119-LR-05	Pipeline Liquids Truck Loading	-	-	-	-	-	-	-	-	-	-	-	-	21.23	0.01	0.84	<0.01	Neg.	Neg.
Facility-Wide:		21.4	71.8	21.3	64.3	1.2	4.6	1.2	4.6	1.2	4.6	0.6	2.3	25.9	8.3	1.9	1.4	22,387	84,878

**Solar Turbines Titan 130-20502S Compressor Turbine (119-CT-01)
Potential to Emit Calculations**

Source Designation:	119-CT-01
Manufacturer:	Solar Turbines
Model:	Titan 130-20502S
Fuel Used:	Natural Gas
Control Device:	N/A
Emission Point Name:	119-CT-01

	Ambient Temperature (°F): -10	Ambient Temperature (°F): 0	Ambient Temperature (°F): 50
Power (hp):	21,197	21,065	19,839
Lower Heating Value (LHV) (Btu/scf):	942	942	942
Lower Heating Value (LHV) (Btu/lbm):	21,254	21,254	21,254
Maximum Higher Heating Value (HHV) (Btu/scf):	1,020	1,020	1,020
Fuel Flow (lbm/hr):	7,304	7,187	6,628
Fuel Flow (scfm):	2,746	2,702	2,492
Fuel Flow (scf/hr):	164,748	162,127	149,498
Heat Input (LHV) (MMBtu/hr):	155.2	152.8	140.9
Heat Input (HHV) (MMBtu/hr):	168.0	165.4	152.5

Performance data for -10°F, 0 °F, and 50 °F based on Solar Turbines Emission and Performance Data Estimates for Titan 130-20502S (18 Nov 2014, 16 Dec 2014, 23 Dec 2014).

Operational Parameters:

Total Annual Hours of Operation (hr/yr):	8,760
Annual Hours of Operation at 50 °F (hr/yr):	8,660
Annual Hours of Operation at -10 °F (hr/yr):	100
Ratio HHV:LHV	1.08
Number of Identical Units:	1

Start-up and Shutdown Emissions:

Annual Number of Start-ups:	150
Annual Number of Shutdowns:	150

Pollutant	Start-up Emissions			Shutdown Emissions			Reference
	lb/event	lb/hr	tpy	lb/event	lb/hr	tpy	
CO	177	3.03	13.27	208	3.55	15.57	1
NO _x	1.90	0.03	0.14	2.40	0.04	0.18	1
VOC	2.02	0.03	0.15	2.38	0.04	0.18	1, 2
CO ₂	1,161	19.88	87.08	1,272	21.78	95.40	1
CH ₄	8.08	0.14	0.61	9.52	0.16	0.71	1, 2
Total GHG		20.02	87.68		21.94	96.11	1
Total CO ₂ e		23.34	102.23		25.86	113.25	1

1. Start-up and Shutdown Emissions based on Solar Turbines Incorporated Product Information Letter 170: Emission Estimates at Start-up, Shutdown, and Commissioning for SoLoNO_x Combustion Products (13 June 2012). Emission estimates provided do not include SO₂, PM, N₂O, or any HAPs.
2. VOCs assumed to be 20% of UHC and CH₄ assumed to be 80% of UHC.

Solar Turbines Titan 130-20502S Compressor Turbine (119-CT-01) (Continued)

Criteria Pollutant & Greenhouse Gas Emission Factors During Operation at Subzero and Normal Operating Temperatures:

Pollutant	Emission Factors at Various Ambient Temperatures					
	Value, -10°F	Value, 0°F	Value, 50°F	Units	LHV/HHV	Reference
CO	37.70	9.29	8.54	lb/hr	NA	1
NO _x	26.00	15.27	14.02	lb/hr	NA	1
SO ₂	3.40E-03	3.40E-03	3.40E-03	lb/MMBtu	HHV	2
VOC	2.16	1.06	0.98	lb/hr	NA	1
PM (Filterable + Condensable)	6.60E-03	6.60E-03	6.60E-03	lb/MMBtu	HHV	2
PM ₁₀ (Filterable + Condensable)	6.60E-03	6.60E-03	6.60E-03	lb/MMBtu	HHV	2
PM _{2.5} (Filterable + Condensable)	6.60E-03	6.60E-03	6.60E-03	lb/MMBtu	HHV	2
CO ₂	53.06	53.06	53.06	kg/MMBtu	HHV	3
CH ₄	8.64	4.26	3.91	lb/hr	NA	1
N ₂ O	1.00E-04	1.00E-04	1.00E-04	kg/MMBtu	HHV	4

References

- Emission factors taken from Solar Turbines performance data for the Titan 130-20502S at ambient temperatures of -10°F, 0°F, and 50°F (18 Nov 2014, 16 Dec 2014, 23 Dec 2014). VOCs assumed to be 20% of UHC and CH₄ assumed to be 80% of UHC.
- AP-42, 5th ed., Section 3.1: Stationary Gas Turbines, Table 3.1-2a: Emission Factors for Criteria Pollutants and Greenhouse Gases from Stationary Gas Turbines (April 2000). Conservatively assumes PM (Filterable + Condensable) = PM10 = PM2.5
- 40 CFR Part 98 Subpart C, Table C-1: Default CO₂ Emission Factors and High Heat Values for Various Types of Fuel, for natural gas.
- 40 CFR Part 98 Subpart C, Table C-2: Default CH₄ and N₂O Emission Factors and High Heat Values for Various Types of Fuel, for natural gas.

Normal Operation Criteria Pollutant & Greenhouse Gas Potential Emissions Calculations:

Pollutant	Potential Emissions (Excluding SU/SD)				
	lb/hr, 0°F	lb/hr, 50°F	Reference	tpy	Reference
CO	9.29	8.54	1	36.98	6
NO _x	15.27	14.02	1	60.71	6
SO ₂	0.56	0.52	2	2.24	6
VOC	1.06	0.98	1	4.23	6
PM (Filterable + Condensable)	1.09	1.01	2	4.36	6
PM ₁₀ (Filterable + Condensable)	1.09	1.01	2	4.36	6
PM _{2.5} (Filterable + Condensable)	1.09	1.01	2	4.36	6
Total CO ₂ e	19,462	17,945	3	77,704	6
Total GHG	19,349	17,842	4	77,254	6
CO ₂	19,344	17,838	5	77,237	6
CH ₄	4.26	3.91	1	16.94	6
N ₂ O	0.04	0.03	5	0.15	6

References/Sample Calculations:

- See emission factor table above.
- Potential Emissions (lb/hr) Excluding SU/SD at Each Ambient Temperature (°F) = Emission Factor_{HHV} (lb/MMBtu) at (°F) * Heat Input_{HHV} (MMBtu/hr) at (°F). *Sample calculation:*
 $0.56 \text{ (lb SO}_2\text{/hr)} = 3.4\text{E-}03 \text{ (lb SO}_2\text{/MMBtu)} * 165.4 \text{ (MMBtu/hr)}$
- Total CO₂e (lb/hr) Excluding SU/SD at Each Ambient Temperature (°F) = CO₂ Emissions (lb/hr) at (°F) + [CH₄ Emissions (lb/hr) at (°F) * Global Warming Potential] + [N₂O Emissions (lb/hr) at (°F) * Global Warming Potential]. *Sample calculation:*
 $19,462 \text{ (lb CO}_2\text{e/hr)} = 19,344 \text{ (lb CO}_2\text{/hr)} + [4.26 \text{ (lb CH}_4\text{/hr)} * 25] + [0.04 \text{ (lb N}_2\text{O/hr)} * 298]$
- Total GHG (lb/hr) Excluding SU/SD at Each Ambient Temperature (°F) = CO₂ Emissions (lb/hr) at (°F) + CH₄ Emissions (lb/hr) at (°F) + N₂O Emissions (lb/hr) at (°F). *Sample calculation:*
 $19,349 \text{ (lb GHG/hr)} = 19,344 \text{ (lb CO}_2\text{/hr)} + 4.26 \text{ (lb CH}_4\text{/hr)} + 0.04 \text{ (lb N}_2\text{O/hr)}$
- Potential Emissions (lb/hr) Excluding SU/SD at Each Ambient Temperature (°F) = Emission Factor_{HHV} (kg/MMBtu) at (°F) * 2.204628 (lb/kg) * Heat Input_{HHV} (MMBtu/hr) at (°F). *Sample calculation:*
 $0.04 \text{ (lb N}_2\text{O/hr)} = 1.\text{E-}04 \text{ (kg N}_2\text{O/MMBtu)} * 2.204628 \text{ (lb/kg)} * 165.4 \text{ (MMBtu/hr)}$
- Annual (tpy) emissions at normal operation of each pollutant, excluding SU/SD emissions, assume 8,660 hours per year of operation at 50°F. The average annual ambient temperature of the compressor station location is between 50°F and 59°F, and as emissions are expected to decrease as ambient temperature increases, potential annual emissions for the majority of each operating year (8,660 hours) were based a conservative ambient operating temperature of 50°F. Potential Emissions (tpy) at Normal Operation Excluding SU/SD at Each Ambient Temperature (°F) = Potential Emissions (lb/hr) at (50°F) * Operating Hours Assumed Per Year at 50°F / 2,000 (lb/ton). *Sample calculation:*
 $36.98 \text{ (tons CO}_2\text{/yr)} = 8.54 \text{ (lb CO}_2\text{/hr)} * 8,660 \text{ (hr/yr)} / 2,000 \text{ (lb/ton)}$

Solar Turbines Titan 130-20502S Compressor Turbine (119-CT-01) (Continued)

Sub-Zero Operation Criteria Pollutant & Greenhouse Gas Potential Emissions Calculations:

Pollutant	Potential Emissions (Excluding SU/SD)			
	lb/hr (-10°F)	Reference	tpy (-10°F)	Reference
CO	37.70	1	1.89	6
NO _x	26.00	1	1.30	6
SO ₂	0.57	2	0.03	6
VOC	2.16	1	0.11	6
PM (Filterable + Condensable)	1.11	2	0.06	6
PM ₁₀ (Filterable + Condensable)	1.11	2	0.06	6
PM _{2.5} (Filterable + Condensable)	1.11	2	0.06	6
Total CO _{2e}	19,884	3	994.2	6
Total GHG	19,666	4	983.3	6
CO ₂	19657	5	982.9	6
CH ₄	8.64	1	0.43	6
N ₂ O	0.04	5	0.00	6

References/Sample Calculations:

- See emission factor table above.
- Potential Emissions (lb/hr) Excluding SU/SD at -10°F = Emission Factor_{HHV} (lb/MMBtu) at (-10°F) * Heat Input_{HHV} (MMBtu/hr) at (-10°F). *Sample calculation:*
 $0.57 \text{ (lb SO}_2\text{/hr)} = 3.4\text{E-}03 \text{ (lb SO}_2\text{/MMBtu)} * 168 \text{ (MMBtu/hr)}$
- Total CO_{2e} (lb/hr) Excluding SU/SD at -10°F = CO₂ Emissions (lb/hr) at (-10°F) + [CH₄ Emissions (lb/hr) at (-10°F) * Global Warming Potential] + [N₂O Emissions (lb/hr) at (-10°F) * Global Warming Potential]. *Sample calculation:*
 $19,884 \text{ (lb CO}_2\text{e/hr)} = 19,657 \text{ (lb CO}_2\text{/hr)} + [8.64 \text{ (lb CH}_4\text{/hr)} * 25] + [0.04 \text{ (lb N}_2\text{O/hr)} * 298]$
- Total GHG (lb/hr) Excluding SU/SD at -10°F = CO₂ Emissions (lb/hr) at (-10°F) + CH₄ Emissions (lb/hr) at (-10°F) + N₂O Emissions (lb/hr) at (-10°F). *Sample calculation:*
 $19,666 \text{ (lb GHG/hr)} = 19,657 \text{ (lb CO}_2\text{/hr)} + 8.64 \text{ (lb CH}_4\text{/hr)} + 0.04 \text{ (lb N}_2\text{O/hr)}$
- Potential Emissions (lb/hr) Excluding SU/SD at -10°F = Emission Factor_{HHV} (kg/MMBtu) at (-10°F) * 2.204628 (lb/kg) * Heat Input_{HHV} (MMBtu/hr) at (-10°F). *Sample calculation:*
 $0.04 \text{ (lb N}_2\text{O/hr)} = 3.65\text{E-}02 \text{ (kg N}_2\text{O/MMBtu)} * 2.204628 \text{ (lb/kg)} * 168 \text{ (MMBtu/hr)}$
- Annual (tpy) emissions at sub-zero operation, excluding SU/SD emissions, of each pollutant assume 100 hours per year of operation at -10°F ambient temperature.
 Potential Emissions (tpy) at Sub-Zero Operation Excluding SU/SD (-10°F) = Potential Emissions (lb/hr) at (-10°F) * Operating Hours Assumed Per Year at -10°F / 2,000 (lb/ton). *Sample calculation:*
 $1.89 \text{ (tons CO}_2\text{/yr)} = 37.7 \text{ (lb CO}_2\text{/hr)} * 100 \text{ (hr/yr)} / 2,000 \text{ (lb/ton)}$

Solar Turbines Titan 130-20502S Compressor Turbine (119-CT-01) (Continued)

Potential Criteria Pollutant & Greenhouse Gas Potential Emissions Including Normal and Sub-Zero Operation:

Pollutant	Potential Emissions (Excluding SU/SD)		Potential Emissions (Including SU/SD)	
	tpy	Reference	tpy	Reference
CO	38.86	1	67.70	2
NO _x	62.01	1	62.33	2
SO ₂	2.27	1	2.27	2
VOC	4.34	1	4.67	2
PM (Filterable + Condensable)	4.41	1	4.41	2
PM10 (Filterable + Condensable)	4.41	1	4.41	2
PM2.5 (Filterable + Condensable)	4.41	1	4.41	2
Total CO _{2e}	78,698	1	78,914	2
Total GHG	78,237	1	78,432	2
CO ₂	78,220	1	78,402	2
CH ₄	17.37	1	18.69	2
N ₂ O	0.15	1	0.15	2

References/Sample Calculations:

- Total Potential Emissions (tpy), excluding SU/SD, of each pollutant assume 100 hours per year of operation at -10°F and 8,660 hours of operation at 50°F.
 Total Potential Emissions (tpy), excluding SU/SD = Potential Emissions (tpy) (-10°F) + Potential Emissions (tpy) (50°F) (excluding SU/SD). *Sample calculation:*
 $38.86 \text{ (tons CO/yr Total)} = 1.89 \text{ (tons CO/yr @ -10F)} + 36.98 \text{ (tons CO/yr @ 50F)}$
- Total Potential Emissions (tpy), including SU/SD, of each pollutant assume 100 hours per year of operation at -10°F and 8,660 hours of operation at 50.0°F.
 Total Potential Emissions (tpy), Including SU/SD = [Potential Emissions (tpy) (-10°F) + Potential Emissions (tpy) (50°F) (excluding SU/SD)] + Start-up Emissions + Shutdown Emissions. *Sample calculation:*
 $67.7 \text{ (tons CO/yr Total)} = 1.89 \text{ (tons CO/yr @ -10F)} + 36.98 \text{ (tons CO/yr @ 50F)} + 13.27 \text{ (tons CO/yr for Start-Ups)} + 15.57 \text{ (tons CO/yr for Shutdowns)}$

Normal Operation Hazardous Air Pollutant Emission Factors and Potential Emission Calculations:

HAP	Emission Factor (HHV)			Potential Emissions		
	Value	Units	Reference	lb/hr	tpy	Reference
1,3-Butadiene	4.30E-07	lb/MMBtu	1	7.11E-05	3.11E-04	2, 3
Acetaldehyde	4.00E-05	lb/MMBtu	1	6.61E-03	2.90E-02	2, 3
Acrolein	6.40E-06	lb/MMBtu	1	1.06E-03	4.64E-03	2, 3
Benzene	1.20E-05	lb/MMBtu	1	1.98E-03	8.69E-03	2, 3
Ethylbenzene	3.20E-05	lb/MMBtu	1	5.29E-03	2.32E-02	2, 3
Formaldehyde	7.10E-04	lb/MMBtu	1	1.17E-01	5.14E-01	2, 3
Naphthalene	1.30E-06	lb/MMBtu	1	2.15E-04	9.42E-04	2, 3
PAH	2.20E-06	lb/MMBtu	1	3.64E-04	1.59E-03	2, 3
Propylene Oxide	2.90E-05	lb/MMBtu	1	4.80E-03	2.10E-02	2, 3
Toluene	1.30E-04	lb/MMBtu	1	2.15E-02	9.42E-02	2, 3
Xylene	6.40E-05	lb/MMBtu	1	1.06E-02	4.64E-02	2, 3
Total HAP				0.17	0.74	

References/Sample Calculations:

- AP-42, 5th ed., Section 3.1: Stationary Gas Turbines, Table 3.1-3: Emission Factors for Hazardous Air Pollutants from Natural Gas-Fired Stationary Gas Turbines (April 2000).
- Potential Emissions (lb/hr) = Emission Factor (lb/MMBtu) * Heat Input_{HHV} at 0°F (MMBtu/hr). *Sample calculation:*
 $1.06E-03 \text{ (lb Acrolein/hr)} = 6.4E-06 \text{ (lb Acrolein/MMBtu)} * 165.4 \text{ (MMBtu/hr)}$
- Potential Emissions (tons/yr) = (lb/hr)_{Potential} × (Annual Hours of Operation) × (1 ton/2,000 lb). *Sample calculation:*
 $4.64E-03 \text{ (tons Acrolein/yr)} = 1.06E-03 \text{ (lb Acrolein/hr)} * 8760 \text{ (hr/yr)} * 1 \text{ ton/2,000 lb}$

**Caterpillar G 3516 LE Emergency Generator (119-EG-03)
Potential to Emit Calculations**

Source Designation:	119-EG-03
Manufacturer:	Caterpillar
Model:	G 3516 LE
Stroke Cycle:	4
Type of Burn:	Lean
Fuel Used:	Natural Gas
Lower Heating Value (LHV) (Btu/scf):	905.0
Higher Heating Value (HHV) (Btu/scf):	1,020
Ratio HHV:LHV	1.13
Engine Rating (bhp):	1,340
Fuel Flow (scfm):	183
Heat Input at 100% Load (MMBtu/hr) (LHV):	9.92
Heat Input at 100% Load (MMBtu/hr) (HHV):	11.2
Fuel Consumption (Btu/bhp-hr) (100% Load)	7,405
Control Device:	N/A

Operational Parameters:

Annual Hours of Operation (hr/yr):	500
Number of Identical Units	1

Emission Factors:

Pollutant	Emission Factor Basis			
	Value	Units	LHV/HHV	Reference
CO	4.00	g/bhp-hr	HHV (Assumed)	1
NO _x	2.00	g/bhp-hr	HHV (Assumed)	1
SO ₂	0.00	lb/MMBtu	HHV	2
VOC	1.00	g/bhp-hr	HHV (Assumed)	1
PM (Filterable + Condensable)	9.98E-03	lb/MMBtu	HHV	2, 3
PM ₁₀ (Filterable + Condensable)	9.98E-03	lb/MMBtu	HHV	2, 3
PM _{2.5} (Filterable + Condensable)	9.98E-03	lb/MMBtu	HHV	2, 3
Non-Biogenic CO ₂	53.060	kg/MMBtu	HHV	4
CH ₄	1.25	lb/MMBtu	HHV	2
N ₂ O	0.00	kg/MMBtu	HHV (Assumed)	5

References

1. NO_x, CO, and VOC emissions are based on 40 CFR 60 Subpart JJJJ emission limits, Table 1.
2. AP-42, 5th ed., Section 3.2: Natural Gas-fired Reciprocating Engines, Table 3.2-2: Uncontrolled Emission Factors for 4-Stroke Lean-Burn Engines (July 2000).
3. Conservatively assumes PM (Filterable + Condensable) = PM₁₀ = PM_{2.5}
4. 40 CFR Part 98 Subpart C, Table C-1: Default CO₂ Emission Factors and High Heat Values for Various Types of Fuel, for natural gas.
5. 40 CFR Part 98 Subpart C, Table C-2: Default CH₄ and N₂O Emission Factors and High Heat Values for Various Types of Fuel, for natural gas.

Criteria Pollutant & Greenhouse Gas Emissions Calculations:

Pollutant	Emission Factor (HHV)		Potential Emissions	
	lb/MMBtu	Reference	lb/hr	tpy
CO	1.06	1	11.82	2.95
NO _x	0.53	1	5.91	1.48
SO ₂	0.00	-	0.01	0.002
VOC	0.26	1	2.95	0.74
PM (Filterable + Condensable)	9.98E-03	-	0.11	0.03
PM ₁₀ (Filterable + Condensable)	9.98E-03	-	0.11	0.03
PM _{2.5} (Filterable + Condensable)	9.98E-03	-	0.11	0.03
Total CO ₂ e			1,658	415
Total GHG			1,322	331
Non-Biogenic CO ₂	116.977	2	1,308	327
CH ₄	1.25	-	13.98	3.49
N ₂ O	0.00	2	0.00	0.00

Caterpillar G 3516 LE Emergency Generator (119-EG-03) (Continued)

References:

1. Converted emission factors from g/bhp-hr to lb/MMBtu to calculate all emissions on a consistent basis.
 $EF (lb/MMBtu) = EF (g/bhp-hr) * (1 lb/453.592g) * Engine Rating (hp) / Heat Input (MMBtu/hr)$
 $1.06 (lb CO/MMBtu) = 4 (g CO/bhp-hr) / 453.592 (g/lb) * 1,340 (bhp) / 11.18 (MMBtu/hr)$
2. Converted emission factors from kg/MMBtu to lb/MMBtu to calculate all emissions on a consistent basis.
 $EF (lb/MMBtu) = EF (kg/MMBtu) * (2.20462 lb/kg)$
 $2.2E-04 (lb N2O/MMBtu) = 1.E-04 (kg N2O/MMBtu) * 2.20462 (lb/kg)$

Sample Calculations:

Potential Emissions (lb/hr) = Emission Factor (lb/MMBtu) * Heat Input_{HHV} (MMBtu/hr)

$0.11 (lb PM/hr) = 9.98E-03 (lb PM/MMBtu) * 11.18 (MMBtu/hr)$

Potential Emissions (tons/yr) = (lb/hr)_{Potential} × (Annual hours of operation) × (1 ton/2,000 lb)

$0.03 (tons PM/yr) = 0.11 (lb PM/hr) * 500 hr/yr * 1 ton/2,000 lb$

Hazardous Air Pollutant Emissions Calculations:

HAP	Emission Factor (HHV)		Potential Emissions	
	lb/MMBtu	Reference	lb/hr	tpy
1,1,2,2-Tetrachloroethane	4.00E-05	1	4.47E-04	1.12E-04
1,1,2-Trichloroethane	3.18E-05	1	3.56E-04	8.89E-05
1,3-Butadiene	2.67E-04	1	2.99E-03	7.47E-04
1,3-Dichloropropene	2.64E-05	1	2.95E-04	7.38E-05
2-Methylnaphthalene	3.32E-05	1	3.71E-04	9.28E-05
2,2,4-Trimethylpentane	2.50E-04	1	2.80E-03	6.99E-04
Acenaphthene	1.25E-06	1	1.40E-05	3.49E-06
Acenaphthylene	5.53E-06	1	6.18E-05	1.55E-05
Acetaldehyde	8.36E-03	1	9.35E-02	2.34E-02
Acrolein	5.14E-03	1	5.75E-02	1.44E-02
Benzene	4.40E-04	1	4.92E-03	1.23E-03
Benzo(b)fluoranthene	1.66E-07	1	1.86E-06	4.64E-07
Benzo(e)pyrene	4.15E-07	1	4.64E-06	1.16E-06
Benzo(g,h,i)perylene	4.14E-07	1	4.63E-06	1.16E-06
Biphenyl	2.12E-04	1	2.37E-03	5.93E-04
Carbon Tetrachloride	3.67E-05	1	4.10E-04	1.03E-04
Chlorobenzene	3.04E-05	1	3.40E-04	8.50E-05
Chloroform	2.85E-05	1	3.19E-04	7.97E-05
Chrysene	6.93E-07	1	7.75E-06	1.94E-06
Ethylbenzene	3.97E-05	1	4.44E-04	1.11E-04
Ethylene Dibromide	4.43E-05	1	4.95E-04	1.24E-04
Flouranthene	1.11E-06	1	1.24E-05	3.10E-06
Flourene	5.67E-06	1	6.34E-05	1.59E-05
Formaldehyde	5.28E-02	1	5.90E-01	1.48E-01
Methanol	2.50E-03	1	2.80E-02	6.99E-03
Methylene Chloride	2.00E-05	1	2.24E-04	5.59E-05
n-Hexane	1.11E-03	1	1.24E-02	3.10E-03
Naphthalene	7.44E-05	1	8.32E-04	2.08E-04
PAH	2.69E-05	1	3.01E-04	7.52E-05
Phenanthrene	1.04E-05	1	1.16E-04	2.91E-05
Phenol	2.40E-05	1	2.68E-04	6.71E-05
Pyrene	1.36E-06	1	1.52E-05	3.80E-06
Styrene	2.36E-05	1	2.64E-04	6.60E-05
Tetrachloroethane	2.48E-06	1	2.77E-05	6.93E-06
Toluene	4.08E-04	1	4.56E-03	1.14E-03
Vinyl Chloride	1.49E-05	1	1.67E-04	4.17E-05
Xylene	1.84E-04	1	2.06E-03	5.14E-04
Total HAP			0.81	0.20

References:

1. AP-42, 5th ed., Section 3.2: Natural Gas-fired Reciprocating Engines, Table 3.2-2: Uncontrolled Emission Factors for 4-Stroke Lean-Burn Engines (July 2000).

Sample Calculations:

Potential Emissions (lb/hr) = Emission Factor (lb/MMBtu) * Fuel Consumption_{HHV} (MMBtu/hr)

$5.75E-02 (lb Acrolein/hr) = 5.14E-03 (lb Acrolein/MMBtu) * 11.18 (MMBtu/hr)$

Potential Emissions (tons/yr) = (lb/hr)_{Potential} × (Annual hours of operation) × (1 ton/2,000 lb).

$1.44E-02 (tons Acrolein/yr) = 5.75E-02 (lb Acrolein/hr) * 500 (hr/yr) * 1 ton/2,000 lb$

**Parker Boiler T4600LR Hydronic Heater (119-EG-03)
Potential to Emit Calculations**

Source Designation:	119-EG-03
Manufacturer:	Parker Boiler
Model:	T4600LR
Fuel Used:	Natural Gas
Lower Heating Value (LHV) (Btu/scf):	942
Higher Heating Value (HHV) (Btu/scf):	1,020
Heat Input (MMBtu/hr) (LHV):	4.25
Heat Input (MMBtu/hr) (HHV):	4.60
Hourly Fuel Consumption (scf/hr):	4,510
Fuel Flow (scfm):	75.2
Control Device:	N/A

Operational Parameters:

Annual Hours of Operation (hr/yr):	8,760
Annual Fuel Consumption (MMscf/yr):	39.5
Number of Identical Units:	1

Emission Factors:

Pollutant	Emission Factor Basis			
	Value	Units	LHV/HHV	Reference
CO	0.06	lb/MMBtu	HHV (Assumed)	1
NO _x	0.02	lb/MMBtu	HHV (Assumed)	1
SO ₂	0.60	lb/MMscf	HHV	2
VOC	6.20E-03	lb/MMBtu	HHV (Assumed)	1
PM (Filterable + Condensable)	0.01	lb/MMBtu	HHV	1, 3
PM ₁₀ (Filterable + Condensable)	0.01	lb/MMBtu	HHV	1, 3
PM _{2.5} (Filterable + Condensable)	0.01	lb/MMBtu	HHV	1, 3
Non-Biogenic CO ₂	53.1	kg/MMBtu	HHV	4
CH ₄	0.02	lb/MMBtu	HHV	1
N ₂ O	1.00E-04	kg/MMBtu	HHV (Assumed)	5

References

1. Parker Industrial Boiler, Emission Data for Metal Fiber Premix Natural Gas Fired Burner Systems on Parker Boilers (September 27, 2013). VOCs assumed to be 20% of UHC and CH₄ assumed to be 80% of UHC.
2. AP-42, 5th ed., Section 1.4: Natural Gas Combustion, Table 1.4-2: Emission Factors for Criteria Pollutants and Greenhouse Gases from Natural Gas Combustion.
3. Conservatively assumed PM = PM₁₀ = PM_{2.5}
4. 40 CFR Part 98 Subpart C, Table C-1: Default CO₂ Emission Factors and High Heat Values for Various Types of Fuel, for natural gas.
5. 40 CFR Part 98 Subpart C, Table C-2: Default CH₄ and N₂O Emission Factors and High Heat Values for Various Types of Fuel, for natural gas.

Parker Boiler T4600LR Hydronic Heater (119-EG-03)(Continued)**Criteria Pollutant & Greenhouse Gas Emissions Calculations:**

Pollutant	Emission Factor (HHV)		Potential Emissions	
	lb/MMBtu	Reference	lb/hr	tpy
CO	0.06	-	0.25	1.11
NO _x	0.02	-	0.11	0.48
SO ₂	5.88E-04	1	2.71E-03	0.01
VOC	6.20E-03	-	0.03	0.12
PM (Filterable + Condensable)	0.01	-	0.05	0.20
PM ₁₀ (Filterable + Condensable)	0.01	-	0.05	0.20
PM _{2.5} (Filterable + Condensable)	0.01	-	0.05	0.20
Total CO ₂ e			541	2,371
Total GHG			538	2,357
Non-Biogenic	117	2	538	2,357
CH ₄	0.02	-	0.11	0.50
N ₂ O	2.20E-04	2	1.01E-03	4.44E-03

References:

1. Converted emission factors from lb/MMscf to lb/MMBtu to calculate all emissions on a consistent basis.

$$EF (\text{lb/MMBtu}) = EF (\text{lb/MMscf}) * HHV (\text{MMscf/MMBtu})$$

$$5.88E-04 (\text{lb SO}_2/\text{MMscf}) = 0.6 (\text{lb SO}_2 / \text{MMscf}) / 1020 (\text{Btu/scf})$$

2. Converted emission factors from kg/MMBtu to lb/MMBtu to calculate all emissions on a consistent basis.

$$EF (\text{lb/MMBtu}) = EF (\text{kg/MMBtu}) * (2.20462 \text{ lb/kg})$$

$$2.2E-04 (\text{lb N}_2\text{O/MMBtu}) = 1.E-04 (\text{kg N}_2\text{O/MMBtu}) * 2.20462 (\text{lb/kg})$$

Sample Calculations:

$$\text{Potential Emissions (lb/hr)} = \text{Emission Factor (lb/MMBtu)} / \text{Heating Value}_{\text{HHV}} (\text{Btu/scf})$$

$$0.05 (\text{lb PM/hr}) = 0.01 (\text{lb PM/MMBtu}) * 4.6 (\text{MMBtu/hr})$$

$$\text{Potential Emissions (tons/yr)} = (\text{lb/hr})_{\text{Potential}} * (\text{Annual hours of operation}) * (1 \text{ ton}/2,000 \text{ lb})$$

$$0.2 (\text{tons PM/yr}) = 0.05 (\text{lb PM/hr}) * 8760 (\text{hr/yr}) * 1 \text{ ton}/2,000 \text{ lb}$$

Parker Boiler T4600LR Hydronic Heater (119-EG-03)(Continued)

Hazardous Air Pollutant Emissions Calculations:

HAP	Emission Factor (HHV)		Potential Emissions	
	lb/MMBtu	Reference	lb/hr	tons/yr
2-Methylnaphthalene	2.35E-08	1	1.08E-07	4.74E-07
3-Methylchloranthrene	1.76E-09	1	8.12E-09	3.56E-08
7,12-Dimethylbenz(a)anthracene	1.57E-08	1	7.22E-08	3.16E-07
Acenaphthene	1.76E-09	1	8.12E-09	3.56E-08
Acenaphthylene	1.76E-09	1	8.12E-09	3.56E-08
Anthracene	2.35E-09	1	1.08E-08	4.74E-08
Arsenic	1.96E-07	2	9.02E-07	3.95E-06
Benz(a)anthracene	1.76E-09	1	8.12E-09	3.56E-08
Benzene	2.06E-06	1	9.47E-06	4.15E-05
Benzo(a)pyrene	1.18E-09	1	5.41E-09	2.37E-08
Benzo(b)fluoranthene	1.76E-09	1	8.12E-09	3.56E-08
Benzo(g,h,i)perylene	1.18E-09	1	5.41E-09	2.37E-08
Benzo(k)fluoranthene	1.76E-09	1	8.12E-09	3.56E-08
Beryllium	1.18E-08	2	5.41E-08	2.37E-07
Cadmium	1.08E-06	2	4.96E-06	2.17E-05
Chromium	1.37E-06	2	6.31E-06	2.77E-05
Chrysene	1.76E-09	1	8.12E-09	3.56E-08
Cobalt	8.24E-08	2	3.79E-07	1.66E-06
Dibenzo(a,h)anthracene	1.18E-09	1	5.41E-09	2.37E-08
Dichlorobenzene	1.18E-06	1	5.41E-06	2.37E-05
Fluoranthene	2.94E-09	1	1.35E-08	5.93E-08
Fluorene	2.75E-09	1	1.26E-08	5.53E-08
Formaldehyde	7.35E-05	1	3.38E-04	1.48E-03
n-Hexane	1.76E-03	1	8.12E-03	0.04
Indeno(1,2,3-cd)pyrene	1.76E-09	1	8.12E-09	3.56E-08
Manganese	3.73E-07	2	1.71E-06	7.51E-06
Mercury	2.55E-07	2	1.17E-06	5.14E-06
Naphthalene	5.98E-07	1	2.75E-06	1.20E-05
Nickel	2.06E-06	2	9.47E-06	4.15E-05
Phenanthrene	1.67E-08	1	7.67E-08	3.36E-07
Pyrene	4.90E-09	1	2.25E-08	9.88E-08
Selenium	2.35E-08	2	1.08E-07	4.74E-07
Toluene	3.33E-06	1	1.53E-05	6.72E-05
Total HAP			8.51E-03	0.04

References

1. AP-42, 5th ed., Section 1.4: Natural Gas Combustion, Table 1.4-3: Emission Factors for Speciated Organic Compounds from Natural Gas Combustion.
2. AP-42, 5th ed., Section 1.4: Natural Gas Combustion, Table 1.4-4: Emission Factors for Metals from Natural Gas Combustion.

Sample Calculations:

Potential Emissions (lb/hr) = Emission Factor (lb/MMBtu) * Fuel Consumption_{HHV} (MMBtu/hr)

$$9.47E-06 \text{ (lb Benzene/hr)} = 2.06E-06 \text{ (lb Benzene/MMBtu)} * 4.6 \text{ (MMBtu/hr)}$$

Potential Emissions (tons/yr) = (lb/hr)_{Potential} × (Annual hours of operation) × (1 ton/2,000 lb).

$$4.15E-05 \text{ (tons Benzene/yr)} = 9.47E-06 \text{ (lb Benzene/hr)} * 8760 \text{ (hr/yr)} * 1 \text{ ton/2,000 lb}$$

**Fugitive Emissions (FUG)
Potential to Emit Calculations**

Source Designation:	FUG
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Operational Parameters:

Annual Hours of Operation (hr/yr):	8,760
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Fugitive Natural Gas Emissions:

Equipment	Service	Emission Factor		Source Count ^[2]	Total HC Potential Emissions		VOC Weight Fraction	VOC Emissions tpy	CH ₄ Weight Fraction	CH ₄ Emissions tpy	HAP Weight Fraction	HAP Emissions tpy
		lb/hr/source	Reference		lb/hr	tpy						
Connectors	Gas	4.41E-04	1	3,309	1.46	6.4	0.0020	0.01	0.95	6.05	0.00002	0.00012
Flanges	Gas	8.60E-04	1	290	0.25	1.1	0.0020	0.00	0.95	1.03	0.00002	0.00002
Others	Gas	1.94E-02	1	95.6	1.85	8.1	0.0020	0.02	0.95	7.69	0.00002	0.00015
Valves	Gas	9.92E-03	1	1,147	11.4	49.8	0.0020	0.10	0.95	47.18	0.00002	0.00095
Open Ended Lines	Gas	4.41E-03	1	26	0.11	0.49	0.0020	0.00	0.95	0.47	0.00002	0.00001
Connectors	Light Oil	4.63E-04	1	336	0.16	0.68	0.56	0.38	0.38	0.26	0.10	0.06813
Flanges	Light Oil	2.43E-04	1	90	0.02	0.10	0.56	0.05	0.38	0.04	0.10	0.00956
Others	Light Oil	1.65E-02	1	14	0.23	1.01	0.56	0.57	0.38	0.38	0.10	0.10139
Valves	Light Oil	5.51E-03	1	97	0.53	2.34	0.56	1.31	0.38	0.88	0.10	0.23416
Total					16.0	70.1	-	2.4	-	64.0	-	0.4

- EPA Protocol for Equipment Leaks Emissions Estimate (EPA-453/R-95-017) Table 2-4; Oil and Gas Production Operations Average Emission Factor.
- Component counts for flanges and valves in gas service are estimated based on design data. Counts for other components in gas service are each assumed to be equal to 20% of Station 106's existing gas service component counts. Component counts for equipment in light oil service are each assumed to be equal to the same Station 106 component counts.

Sample Calculations:

Potential Emissions (lb/hr) = Emission Factor (lb/hr/source) * Source Count

$$1.46 \text{ (lb HC from connectors in gas service/hr)} = 4.41E-04 \text{ (lb/hr/source)} * 3309 \text{ (source count)}$$

Potential Emissions (tons/yr) = (lb/hr)_{total gas} * Hours of Operation (hr/yr) / (2,000 lb)

$$6.39 \text{ (tons HC from connectors in gas service/yr)} = 1.46 \text{ (lb HC/hr)} * 8760 \text{ (hr/yr)} / 2000 \text{ lb/ton}$$

Gas Speciated Fugitive Natural Gas Emissions:

Pollutant	Wt. Fraction ^[1] %
Non-VOC	
Methane	94.66%
Ethane	4.75%
VOC	
Propane	0.16%
i-Butane	0.01%
n-Butane	0.01%
i-Pentane	0.003%
n-Pentane	0.001%
C6 Plus	0.004%
Total VOC	0.20%
HAP	
n-Hexane	0.002%

Gas speciation based on a natural gas average hydrocarbon composition for a similar site.

Condensate Speciated Fugitive Natural Gas Emissions:

Pollutant	Wt. Fraction %
Non-VOC	
Methane	37.6%
Ethane	6.4%
VOC	
Propane	10.1%
i-Butane	0.4%
n-Butane	7.4%
Pentane	5.6%
C6 Plus	32.5%
Total VOC	56.0%
HAP	
n-Hexane	9.9%
Benzene	0.1%
Total HAP	10.0%

Condensate speciation based on November 2009 KY application submittal for Station 114.

**Gas Venting/Blowdown Emissions (V/BD)
Potential to Emit Calculations**

Source Designation:	V/BD
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Operational Parameters:

Annual Volume of Natural Gas Release (MMscf/yr) ^[1] :	3
Density Air, 60 °F, 1 atm (lb/ft ³):	0.077
Specific Gravity Natural Gas:	0.582
Density Natural Gas, 60 °F, 1 atm (lb/ft ³):	0.045
Annual Mass of Natural Gas Release (lb/yr):	133,500
Annual Mass of Natural Gas Release (tpy):	67

Gas Venting/Blowdown Emissions:

Pollutant	Weight Fraction (%)	Emissions	
		(lb/hr)	(tpy)
<i>Non-VOC</i>			
Methane	94.66%	14.4	63.2
Ethane	4.75%	0.72	3.17
<i>VOC</i>			
Propane	0.16%	0.02	0.11
i-Butane	0.01%	0.0016	0.01
n-Butane	0.01%	0.0021	0.01
i-Pentane	0.003%	0.0004	0.002
n-Pentane	0.001%	0.0002	0.001
C6 Plus	0.004%	0.001	0.003
Total VOC	0.20%	0.03	0.13
<i>HAP</i>			
n-Hexane	0.002%	0.0003	0.0013

1. Annual Volume of Natural Gas Release based on estimated
2. Weight fractions of natural gas based on 90 day average from Station 110 completed over April, May, and June of 2014.

**Storage Tanks (119-PF-04)
Potential to Emit Calculations**

Source Designation:	119-PF-04
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Tank Parameters

Source	Type of Tank	Contents	Capacity	Throughput	Tank Diam.	Tank Length	Paint Color	Paint Condition
			(gal)	gal/yr	ft	ft		
119-PF-04	Vertical, fixed	Pipeline Liquids	3,760	7,520	8	10	Light Grey	Good

Potential Emissions^[1]

Source	Contents	Total VOC Emissions		HAP Emissions	
		lb/hr	tpy	lb/hr	tpy
119-PF-04	Pipeline Liquids	0.05	0.20	0.002	0.01

1. Emissions were calculated using E&P Software. See attached E&P output.

* Project Setup Information *

Project File : Z:\Eastern Pipelines\AIR\NEW\TGP\Broad Run & UMPF\Broad Run Expansion\Tanks Run_WV.e
 Flowsheet Selection : Oil Tank with Separator
 Calculation Method : AP42
 Control Efficiency : 100.0%
 Known Separator Stream : Low Pressure Gas
 Entering Air Composition : No

Filed Name : Tennessee Gas Pipeline, Broad Run Expansion Project, WV
 Date : 2015.01.16

* Data Input *

Separator Pressure : 552.00[psig]
 Separator Temperature : 77.00[F]
 Molar GOR : 0.0500
 Ambient Pressure : 14.70[psia]
 Ambient Temperature : 60.00[F]
 C10+ SG : 0.8990
 C10+ MW : 166.00

-- Low Pressure Gas -----

No.	Component	mol %
1	H2S	0.0000
2	O2	0.0000
3	CO2	0.0000
4	N2	0.0000
5	C1	69.4535
6	C2	6.3060
7	C3	6.7857
8	i-C4	0.2039
9	n-C4	3.7724
10	i-C5	2.2997
11	n-C5	0.0000
12	C6	7.7373
13	C7+	0.0000
14	Benzene	0.0379
15	Toluene	0.0000
16	E-Benzene	0.0000
17	Xylenes	0.0000
18	n-C6	3.4036
19	224Trimethylp	0.0000

C7+ Molar Ratio: C7 : C8 : C9 : C10+
 1.0000 1.0000 1.0000 1.0000

-- Sales Oil -----

Production Rate : 0.5[bbl/day]
 Days of Annual Operation : 365 [days/year]
 API Gravity : 46.0
 Reid Vapor Pressure : 7.70[psia]
 Bulk Temperature : 80.00[F]

-- Tank and Shell Data -----

Diameter : 8.00[ft]
 Shell Height : 10.00[ft]
 Cone Roof Slope : 0.06
 Average Liquid Height : 8.00[ft]
 Vent Pressure Range : 0.06[psi]
 Solar Absorbance : 0.54

-- Meteorological Data -----

City : Charleston, WV
 Ambient Pressure : 14.70[psia]
 Ambient Temperature : 60.00[F]
 Min Ambient Temperature : 44.00[F]
 Max Ambient Temperature : 65.50[F]
 Total Solar Insolation : 1123.00[Btu/ft^2*day]

 * Calculation Results *

-- Emission Summary -----

Item	Uncontrolled [ton/yr]	Uncontrolled [lb/hr]
Total HAPs	0.010	0.002
Total HC	0.243	0.055
VOCs, C2+	0.218	0.050
VOCs, C3+	0.201	0.046

Uncontrolled Recovery Info.

Vapor	11.8100 x1E-3	[MSCFD]
HC Vapor	11.1300 x1E-3	[MSCFD]
GOR	23.62	[SCF/bbl]

-- Emission Composition -----

No	Component	Uncontrolled [ton/yr]	Uncontrolled [lb/hr]
1	H2S	0.001	0.000
2	O2	0.000	0.000
3	CO2	0.012	0.003
4	N2	0.001	0.000
5	C1	0.025	0.006
6	C2	0.017	0.004
7	C3	0.034	0.008
8	i-C4	0.018	0.004
9	n-C4	0.059	0.013
10	i-C5	0.026	0.006
11	n-C5	0.032	0.007
12	C6	0.010	0.002
13	C7	0.010	0.002
14	C8	0.004	0.001
15	C9	0.001	0.000
16	C10+	0.000	0.000
17	Benzene	0.001	0.000
18	Toluene	0.000	0.000
19	E-Benzene	0.000	0.000
20	Xylenes	0.000	0.000
21	n-C6	0.007	0.002
22	224Trimethylp	0.000	0.000
	Total	0.258	0.059

-- Stream Data -----

No.	Component	MW	LP Oil mol %	Flash Oil mol %	Sale Oil mol %	Flash Gas mol %	W&S Gas mol %	Total Emissions mol %
1	H2S	34.80	0.0508	0.0377	0.0000	0.6656	0.0000	0.4837
2	O2	32.00	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
3	CO2	44.01	0.2437	0.1047	0.0000	6.7852	0.0001	4.9302
4	N2	28.01	0.0102	0.0005	0.0000	0.4655	0.0001	0.3383
5	C1	16.04	0.9543	0.1738	0.0000	37.6955	0.0001	27.3898
6	C2	30.07	0.6701	0.3944	0.0000	13.6469	0.0001	9.9159
7	C3	44.10	2.1827	1.8560	0.0514	17.5629	2.2197	13.3682
8	i-C4	58.12	1.1269	1.0684	0.4674	3.8807	9.1341	5.3170
9	n-C4	58.12	4.6091	4.4760	2.6691	10.8742	36.6013	17.9078
10	i-C5	72.15	3.1066	3.1125	2.7362	2.8280	15.2156	6.2147
11	n-C5	72.15	5.0558	5.0931	4.7863	3.2984	19.5128	7.7313
12	C6	86.16	4.1726	4.2443	4.5165	0.7994	5.6808	2.1340

13	C7	100.20	10.3655	10.5720	11.6638	0.6458	5.0621	1.8532
14	C8	114.23	10.8426	11.0685	12.3681	0.2088	1.7645	0.6341
15	C9	128.28	5.5127	5.6291	6.3152	0.0358	0.3223	0.1141
16	C10+	166.00	45.9695	46.9460	52.7836	0.0064	0.0663	0.0228
17	Benzene	78.11	0.5685	0.5793	0.6312	0.0611	0.4498	0.1674
18	Toluene	92.13	0.2132	0.2176	0.2425	0.0062	0.0497	0.0181
19	E-Benzene	106.17	0.0711	0.0726	0.0814	0.0007	0.0056	0.0020
20	Xylenes	106.17	0.6802	0.6945	0.7789	0.0055	0.0473	0.0169
21	n-C6	86.18	3.5939	3.6591	3.9413	0.5272	3.8676	1.4404
22	2,2,4-Trimethylp	114.24	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
	MW		123.89	125.75	130.75	36.33	68.55	45.14
	Stream Mole Ratio		1.0000	0.9792	0.9714	0.0208	0.0078	0.0286
	Heating Value	[BTU/SCF]				1909.45	3799.14	2426.08
	Gas Gravity	[Gas/Air]				1.25	2.37	1.56
	Bubble Pt. @ 100F	[psia]	56.28	21.39	4.72			
	RVP @ 100F	[psia]	126.75	82.72	30.54			
	Spec. Gravity @ 100F		0.800	0.803	0.812			

**Pipeline Liquids Truck Loading (119-LR-05)
Potential to Emit Calculations**

Source Designation:	119-LR-05
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Chemical Parameters

Chemical	Vapor Mol. Weight ^[1]	Avg. Vapor Pressure ^[1]	Avg. Temperature ^[2]	Saturation Factor ^[3]	Throughput ^[4]
	(lb/lb-mol)	(psia)	(deg. R)		Mgal/yr
Pipeline Liquids	45.14	7.70	520	0.6	7.52

References:

1. Vapor molecular weight and vapor pressure based on E&P output for Pipeline Liquids Storage Tank 119-PF-04.
2. Based on average ambient temperature data for the area.
3. Saturation Factor based on "Submerged loading: dedicated normal service" in Table 5.2-1 of AP-42, Ch. 5.2.
4. Assumed that two turnovers of the pipe liquids tank could be loaded out via truck per year.

Total Potential Emissions

Source	Total Loading Losses ^[1]		Pump Capacity ^[2]	Max Hourly Losses
	Average	Annual		
	(lbs/Mgal)	(tpy)	(gal/min)	lb/hr
Pipeline Liquids Truck Loading	5.00	0.02	90	27.0

References:

1. AP-42, Ch. 5.2, Equation 1 (Loading Loss = $12.46 \times (\text{Saturation Factor} \times \text{TVP} \times \text{Molecular Weight}) / \text{Temp.}$)
2. Assumed pump rate.

Speciated Potential Emissions

Source	Contents	VOC Weight Fraction ^[1] (%)	HAP Weight Fraction ^[1] (%)	Total VOC Emissions		Total HAP Emissions	
				lb/hr	tpy	lb/hr	tpy
Pipeline Liquids Truck Loading	Pipeline Liquids	79%	3%	21.23	0.01	0.84	<0.01

References:

1. VOC and HAP weight fractions are based on 119-PF-04 tank emissions speciation.

Attachment O

Attachment O

Monitoring, Recordkeeping, Reporting, Testing

TGP will comply with all of the monitoring, recordkeeping, reporting, and testing requirements set forth in the issued permit for Station 119A.

Attachment P

AIR QUALITY PERMIT NOTICE

Notice of Application

Notice is given that Tennessee Gas Pipeline, L.L.C. has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a General Permit for a compressor station operation located in Charleston, Kanawha County, West Virginia. The latitude and longitude coordinates are: 38.450855 and -81.716714.

The applicant estimates the maximum potential to discharge the following regulated air pollutants on a facility-wide basis will be:

Particulate Matter (PM) = 4.6 tpy
Sulfur Dioxide (SO₂) = 2.3 tpy
Volatile Organic Compounds (VOC) = 8.3 tpy
Carbon Monoxide (CO) = 71.8 tpy
Nitrogen Oxides (NO_x) = 64.3 tpy
Hazardous Air Pollutants (HAPs) = 1.4 tpy
Carbon Dioxide Equivalent (CO_{2e}) = 84,878 tpy

Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1227, during normal business hours.

Dated this the 30th day of January, 2015.

By: Tennessee Gas Pipeline Company, L.L.C.
Shrishti Chhabra
Environmental Engineer III
1001 Louisiana St.
Houston, TX 77002

Attachment Q

Attachment Q

Business Confidential Claims

There is no confidential information associated with this permit application.

Attachment R

Attachment R

Authority Forms

Since this application is signed by the "Responsible Official," this section is not applicable.

Attachment S

Attachment S

Title V Permit Revision Information

Attachment S is not being provided with this permit application since the site does not currently possess a Title V Permit.